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18752 (1 of 2)

FINAL REPORT
PART ONE
OPTIMIZATION OF EL MEX
SALINES SOLAR PONDS AND
BY-PRODUCT INVESTIGATION
UNIDO AUTHORIZATION PROJECT

April, 1989

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ABSTRACT: This is Part One of a Two Part Final Report on pre-feasibility studies authorized by the United Nations Industrial Development Organization Project DP/EGY/87/017. This report provides a summary and conclusions written in non-technical language. The more technical information is shown in Part Two under separate cover. There are two main subjects discussed. The first is optimization of El Mex Salines sodium chloride production, and the second is a discussion of by-products.

1. SUMMARY AND CONCLUSIONS

In GSL's judgement, quality of sodium chloride at El Mex will continuously worsen unless the practice of recycling bitterns is stopped. Bitterns should be held in a holding pond or discharged back to the sea.

Formation of mixed K_2SO_4 salts by solar evaporation does not appear possible. The high humidity at El Mex site does not provide a high enough driving force to favor evaporation of water from concentrated bitterns.

The alternative to evaporation by solar energy is artificial heat. Use of artificial heat in evaporative crystallizers to produce K_2SO_4 from brine is not practiced by GSL or anyone else that we are aware of. This would need additional research.

Production of $MgOH$ to form MgO could be possible by adding lime or dolomite. This is a possibility at El Mex. Some details are given in this report.

Sodium chloride production and quality can be improved at both El Mex and Borg El Arab. This can be achieved through use of sequential ponding methods and discontinuation of bitterns recycle.

One of the main areas of emphasis in this report is to change both pond operating procedures and pond configuration. This change will improve both the quantity and quality of sodium chloride and is necessary if by-product production becomes a reality in the future. GSL believes these changes will be absolutely necessary in the future if El Mex is to survive as a salt producing facility. Since the changes are needed even if by-products are not produced, GSL recommends they be made as soon as possible. The changes will require special planning and control as explained in this report.

2. RECOMMENDATIONS

The biggest problem facing El Mex Salines now is high $MgCl_2$ in feed to El Mex salt crystallizers ponds. This can be solved by preventing bitterns from recycling back to the preconcentration ponds. If recycling of bitterns is stopped, the following positive results will occur.

- A. Better salt will crystallize because it will contain less encapsulated $MgCl_2$ and $MgSO_4$.
- B. Salt production will increase because evaporation of crystallization ponds will increase when $MgCl_2$ content is lowered.
- C. Potential for by-products will increase because bitterns can be concentrated to their maximum values permitted under El Mex weather conditions.
- D. Technical information can be gained for later use in locations at Borg El Arab and Port Said in addition to El Mex.

It is therefore recommended that the following steps be taken.

- 1. Construct a canal or system to flow brine from the Alexandria Petrochemical Company to El Mex pre-concentration pond without mixing it with bitterns from the crystallizer.
- 2. Flow bitterns into a holding pond and let it concentrate to be used as by-product feed stock. If it is not used a by-product feed, it can be discharged back to the sea or dead-headed at the holding pond.
- 3. After $MgCl_2$ in the large pre-concentration pond has lowered, the pond should be divided in two. This will increase production of NaCl crystallizer feed brine and increase purity of salt in the crystallizer.
- 4. Manage bitterns concentration to do the following:
 - a) Concentrate bitterns to maximum values permitted by El Mex weather.
 - b) Obtain technical data from this brine as it concentrates to obtain evaporation information in detail and to follow mineral and brine chemistry.
 - c) Make final plans for by-product manufacturing as data is obtained.

This last item, c, can be done without losing any time in the development of by-products. Development of by-products will require that all of the above items be implemented. Even if no by-products are to be made, Items 1 through 4 should be done if El Mex Salines is to survive. The $MgCl_2$ concentration is now approaching a critical point and salt quality will become worse if the practice of bitterns recycle is not stopped.

It should be understood that before any chance of economical development of by-products can be undertaken, salt bitterns must be managed differently and cannot be recycled. Therefore the recommendations of items 1 through 5 are a first step in by-product manufacturing. It will take several years to build the necessary dikes, structures and then concentrate the bitterns. The work should start immediately. If it is found that it is uneconomical to produce by-products, concentrated bitterns can simply be held in a pond. If the holding ponds are too full and more space cannot be found, the brine can be pumped back to the sea as it is done in other well designed facilities around the world.

If it is decided to pump brine back to the sea, the sea water feed line could be used in the evaporation months to feed sea water and in the winter months to pump bitterns back out from the ponds to the sea.

It is also recommended that plans be made at Borg El Arab to divide the large first pre-concentration pond in two parts and to either pump the bitterns back to the Mediterranean Sea or store it. Under no circumstances should it be recycled.

It is suggested that a marketing survey be made to determine how much $MgCl_2 \cdot 6H_2O$ flake could be sold in Egypt and adjacent countries. If enough sales could be made, El Mex is in a good position to produce it as a by-product.

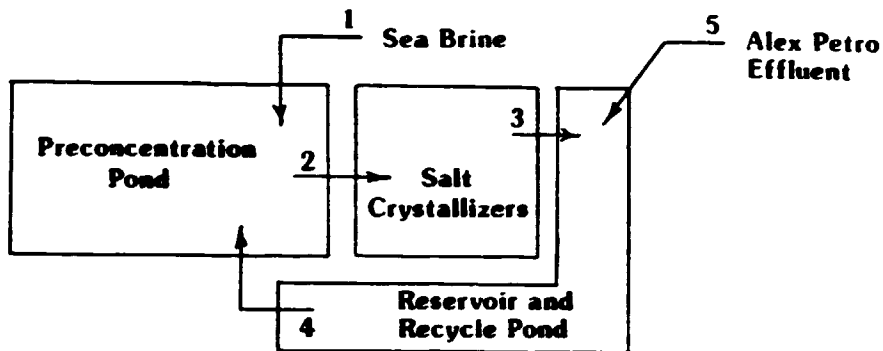
There is a good possibility of producing MgO , however more work must be done to determine whether high enough grade can be produced economically.

3. DISCUSSION

This information is written specifically for supervisors, personnel, managers and directors so they can have a better understanding of complex solar pond systems. This understanding is needed to follow the recommendations and proposals of this report.

3.1 Solar Ponds

The basic system of El Mex solar ponds is shown:



The system is called a closed one because there are no bleed streams or discharge of minerals except for the product, sodium chloride. With time, the other minerals will increase in concentration. These minerals will eventually build up to high levels in the pre-concentration pond. Subsequent feed to salt crystallizer will force contamination to unacceptable levels.

Concentration level of magnesium in the pre-concentration pond at El Mex is near 1.4% Mg⁺⁺. This is 10 times higher than comparable pre-concentration ponds of other large sea salt facilities. It is even higher than concentrated sea water that is saturating in NaCl.

Sea water at Port Said or Borg El Arab, for example, will begin to crystallize NaCl at a Mg++ concentration of 1.04%. This is significantly less than El Mex's 1.4%. Good quality salt can be made at 1.04% (26° Be) with relative ease. Quality salt can also be made at 1.4%, but only with a special sequential pond system that will be explained later. 1.4% Mg++ is equivalent to 1.23 specific gravity (27° Be). Brine is normally discarded at 28.5° Be. At El Mex, however, brine has been discarded at 29 and even 30° Be.

The effect of Mg++ on evaporation is significant. Evaporation of 1.4% brine at El Mex is 130 centimeters per year. Evaporation of sea water saturated brine is 156 centimeters. The difference is (156-130)/130 or 20%.

If a system is developed to stop the recycle of Mg++, evaporation can be increased by near 20%. As a result, production will also be increased and salt quality will improve.

Both production and quality can be increased by ending the practice of recycling salt bitterns. El Mex is not the only facility that recycles bitterns. GSL has observed other operations that do the same. The most common reasons given for recycling are (1) The bitterns contain NaCl and it is recycled to recover it, and (2) Operators don't know what else to do with it.

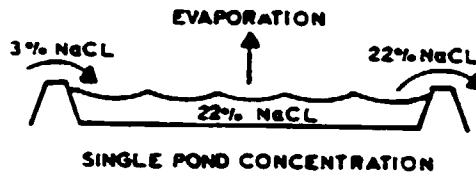
Bitterns contain NaCl, but it also contains MgCl₂, MgSO₄, and KCl, all of which are impurities to NaCl. Impurities slow down evaporation. It can be rigorously shown that saving bitterns for its NaCl content has an opposite effect.

Recycling bitterns because one doesn't know what else to do with it is a poor choice compared to other alternatives. One alternative is to use a salt crystallizer and store it. If more space is needed, a section of the pre-concentration pond should be diked off to make a reservoir pond where bitterns can be left to evaporate further and be stored. It should never be allowed to re-enter the regular salt producing system again. The evaporation area needed to store bitterns is more than offset by increased evaporation of pre-concentrated pond area not mixed with bitterns.

In the case of El Mex, bitterns could be pumped through the sea brine feed line back to the sea. This could be done in winter when the line is not being used.

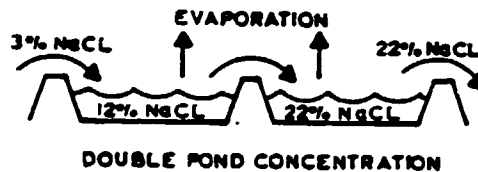
3.1.1 Brine Sequencing

Suppose it is desired to evaporate brine and concentrate it from 3% NaCl to 22%. One way to do this would be to place it in a single pond as illustrated on the following page.



In order to extract a 22% NaCl solution, one must wait until the whole pond has concentrated to 22%.

Now assume the pond is divided in half as shown in the next illustration. Here we see that only one pond must be concentrated to 22% NaCl. The first pond need only be concentrated to 12%. The single pond has an average concentration of 22% but the double pond has a concentration of $(12\% + 22\%) \div 2$ or 17%.



A three pond system will lower concentration even further.

There are distinct advantages to lower average concentration. One is that it is obviously faster and easier to concentrate brine to 17% compared to 22%. This means brine is concentrated in the spring quickly and prepares brine for salt crystallizer earlier than could be done with a single pond system.

The other reason is that lower concentration means higher evaporation. High evaporation means more salt production.

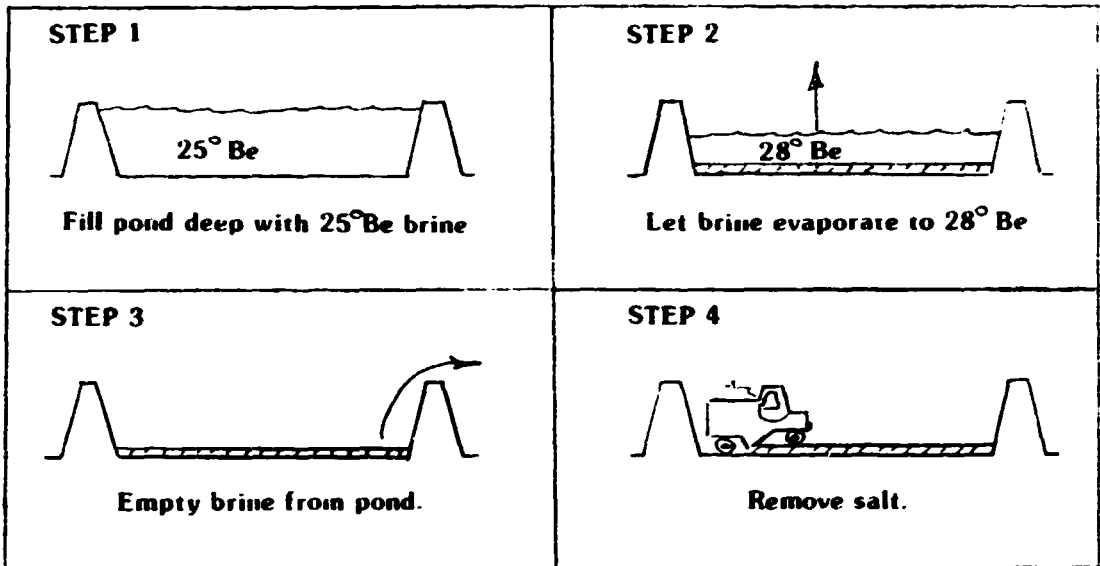
Technical details and mathematical proofs are shown in Part Two of the final report.

3.1.2 Continuous Flow Through Ponds.

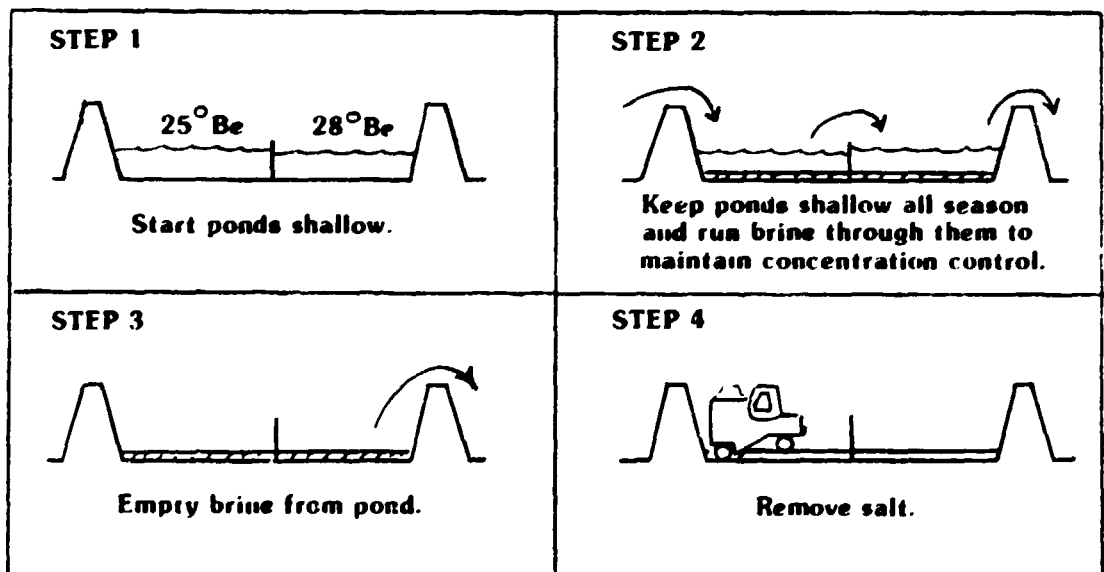
There are two flows generally used in solar ponds. One is a batch system where brine is flowed into a salt crystallizer to a pre-determined depth and then allowed to evaporate down. At the end of the season, brine will have concentrated from 25°Be to its end point, 28° Be.

The other system is to start brine early in the season at a shallow depth and to continuously feed it brine all season. The rate one feeds the pond depends on brine concentration end point desired. Both systems are illustrated in the next figure.

System One. Batch



System Two, Continuous Flow



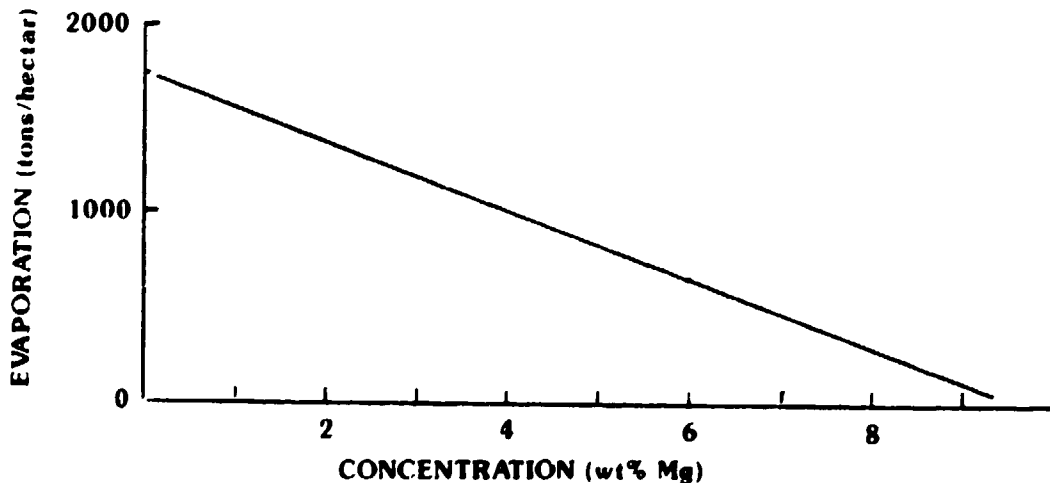
Continuous flow systems are better than batch for the following reasons:

1. Brine can be kept shallow which results in higher evaporation, larger salt crystals and higher purity. These are all explained in the technical section of this report (Part Two).
2. Brine can be flowed through a series of two or three salt crystallizers. This will also result in higher evaporation and higher purity.
3. Flowing brine will result in better concentration control than can be obtained by batch systems.
4. Constant flow techniques through series ponds must be used to make highly concentrated brine needed in by-product manufacturing.

3.1.3 Evaporation Rates in Solar Ponds.

Water is transferred from a brine surface to the atmosphere when the vapor pressure of water is less in air than in the brine. The most significant method to increase vapor pressure in brine is to heat it. This is done by the sun. Another way is to reduce water vapor pressure in the air. This is also done indirectly by the sun and with wind. Another way still is to reduce concentration of minerals in the brine. This latter method is tricky because most solar pond objectives are to concentrate brines which produces just the opposite effect.

A typical evaporation curve on El Mex brine in July is shown.



Notice two very important parts to this curve. One is that evaporation decreases as brine concentrates. The second is that at a given concentration, brine ceases to evaporate. At El Mex, the high summer humidity causes magnesium chloride brines to cease evaporating at a relatively low concentration level. This level is too low to produce by-products K_2SO_4 and $MgCl_2 \cdot 6H_2O$ by conventional methods.

3.2 Suggested Procedure to Upgrade El Mex Solar Pond System

A decision to make or not to make arcanite, magnesium or both will not change the need to isolate bitterns at El Mex. Isolation of this brine is a necessary step and plans to do so should be made immediately.

Even if it were decided to go ahead with by-product manufacturer today, it would still require a few years to make all the needed changes and concentrate bitterns before any real by-product manufacture could begin.

Time is important because conversion of El Mex solar pond system will be slow and should be started now. In addition, operators must learn new methods of operation. The following plan is suggested.

Step One. Isolate Bitterns

Isolating bitterns will require a canal or pipeline for Alexandria's Petrochemical plant effluent. This should be done immediately. This is all that is needed to insure that El Mex salt quality will begin to improve in future years and so will production. At the same time, a positive step will have been taken for possible by-product production. Full scale data can be obtained from actual large pan bitterns ponds to verify evaporation rates that are now only estimated from small pans. As soon as the bitterns are isolated, magnesium concentration in all other ponds will begin to decrease and crystallized salt quality will begin to improve.

Step Two. Run Salt Crystallizer in series with continuous brine flow.

Brine should be run continuously from pond to pond for the entire summer. Set weirs, pumps and canals such that brine can flow from pond to pond until it is discharged into the bitterns holding area.

Step Three. Preconcentration Pond Sub-division

When step one is complete, magnesium in the pre-concentration pond will begin to decrease. This is desired. It will take a minimum of one season and preferably two evaporation seasons before the magnesium is at a low enough level to sub-divide the pre-concentration

pond. If the pond is sub-divided before this time, magnesium concentration will begin to increase uncontrollably with possible disastrous results. It is important that the effects of pond sub-division be understood. Computer runs and descriptions are given in Part Two of the final report to help the reader more fully understand the outcome of pond sub-division.

Even more sub-divisions should be considered in 4 or 5 years to maximize production of sodium chloride and grade.

Step Four. By-Product production.

It will require at least two seasons after bitterns are isolated to generate a reserve of brine for by-product production. During this time data can be collected and feasibility studies continued to make a final decision on the best alternatives for production or feasibility.

Steps 1, 2 and 3 should be taken even if it is desired not to produce by-products. In GSL's opinion, Step 1 is absolutely needed and should be planned immediately. Steps 2 and 3 are optional if only NaCl is produced. Better quality NaCl will result, however, and quantity will improve. If by-products are to be made, Step 1 will be necessary and Steps 2 and 3 will also be needed. It is therefore suggested that all these steps be planned now. If it is desired later not to produce by-products, then nothing will be lost. However, if the steps are not implemented and it is later desired to make by-products, a delay of several years will result.

3.2.1 Illustrations

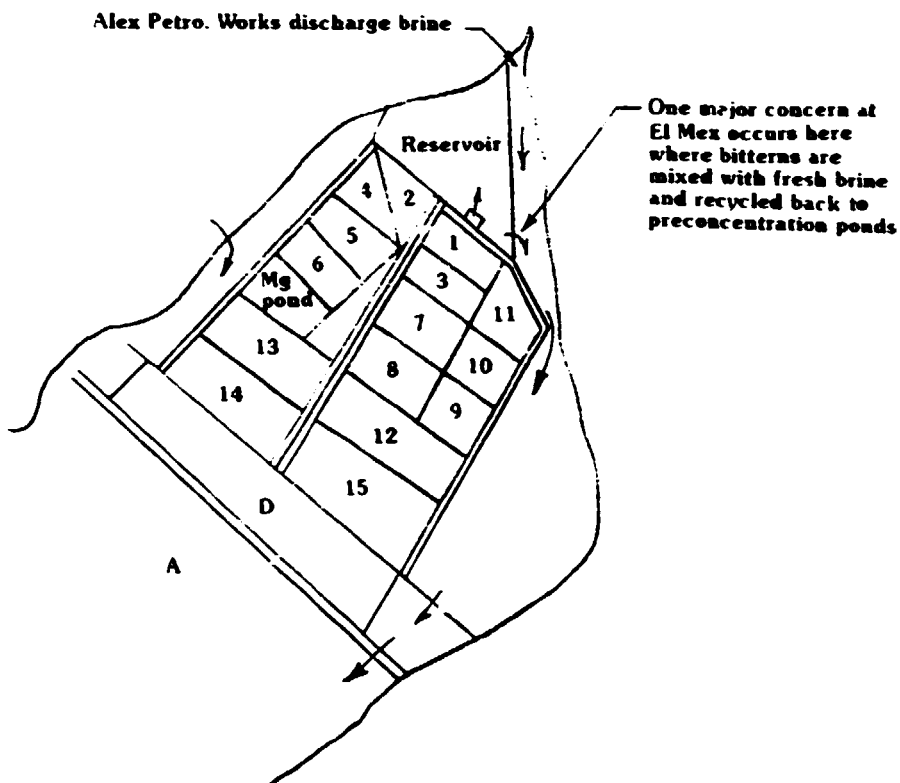
The following few pages show some illustrations of upgrading El Mex ponds. These illustrations are based on the limited knowledge GSL has of El Mex pond system. The main points are to isolate bitterns and place salt ponds in series flow.

Alex Petrochemical Company effluent brine must be separated from bitterns by making a flow path down one side of the pond system. This will require capital cost for diking.

Additional capital will be needed to construct bitterns holding ponds and to convert salt ponds into series flow. In addition, special training will be needed to show operators and engineers the art of continuous series flow of brine to produce high quality NaCl.

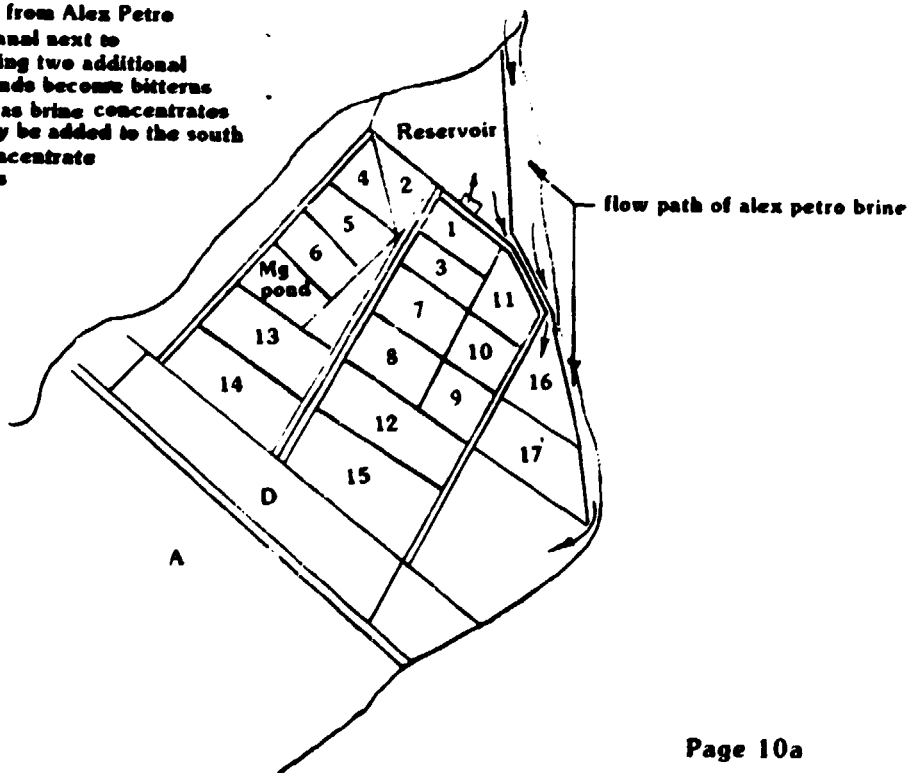
PRESENT STATUS OF EL MEX PONDS

GSL has not been given a detailed drawing of El Mex pond system with locations of all canals, pump stations, bridges and buildings. The sketches shown are estimated by GSL and may not contain all details



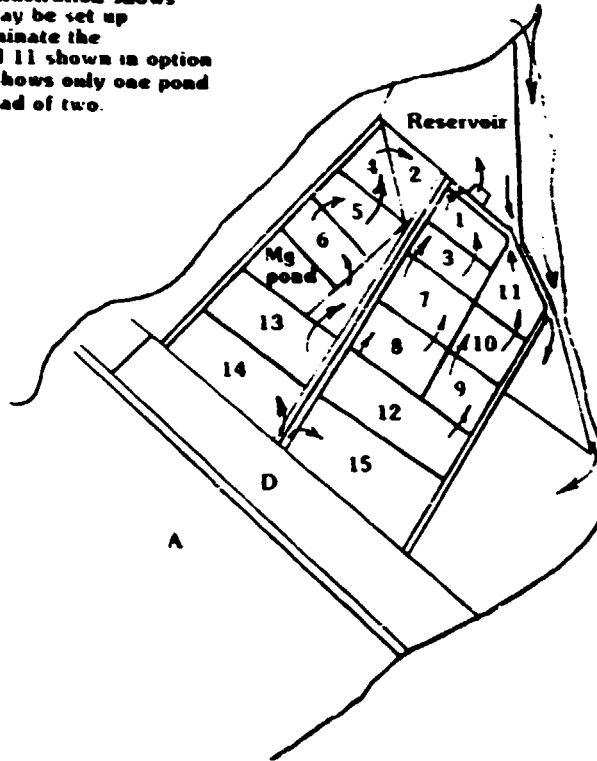
OPTION ONE

Bitterns are isolated from Alex Petro brine by making a canal next to pond 11 and by making two additional ponds. These two ponds become bitterns holding areas. Later as brine concentrates additional ponds may be added to the south if it is desired to concentrate more for by-products



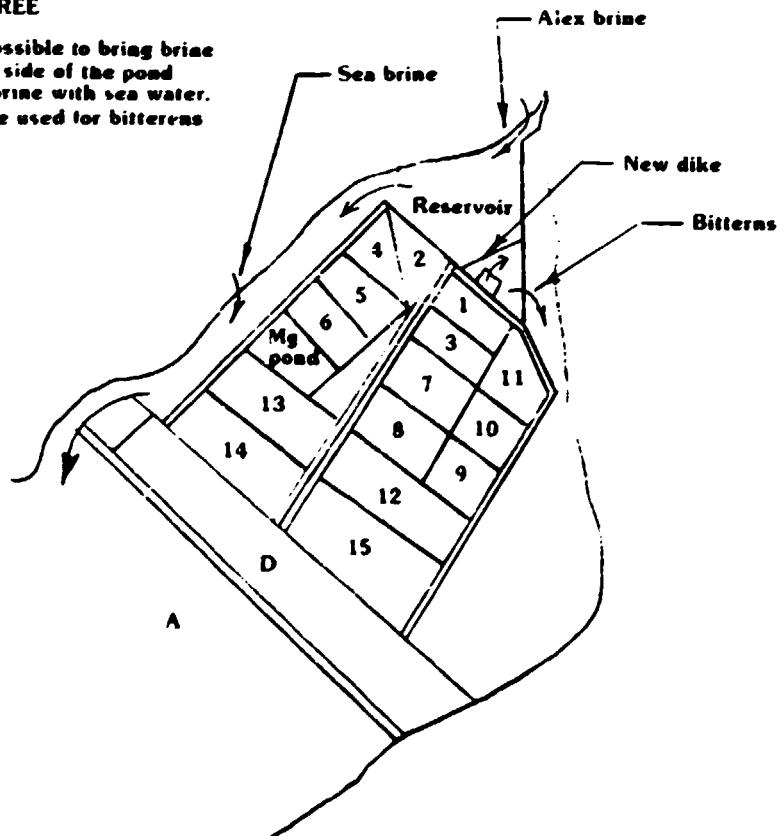
OPTION TWO

There are a variety of ways bitterns can be isolated. This illustration shows how salt ponds may be set up in series flow and eliminate the canal East of pond 11 shown in option one. This illustration shows only one pond made to the east instead of two.



OPTION THREE

Perhaps it would be possible to bring brine around the north west side of the pond system and mix Alex brine with sea water. The east pond would be used for bitterns holding.



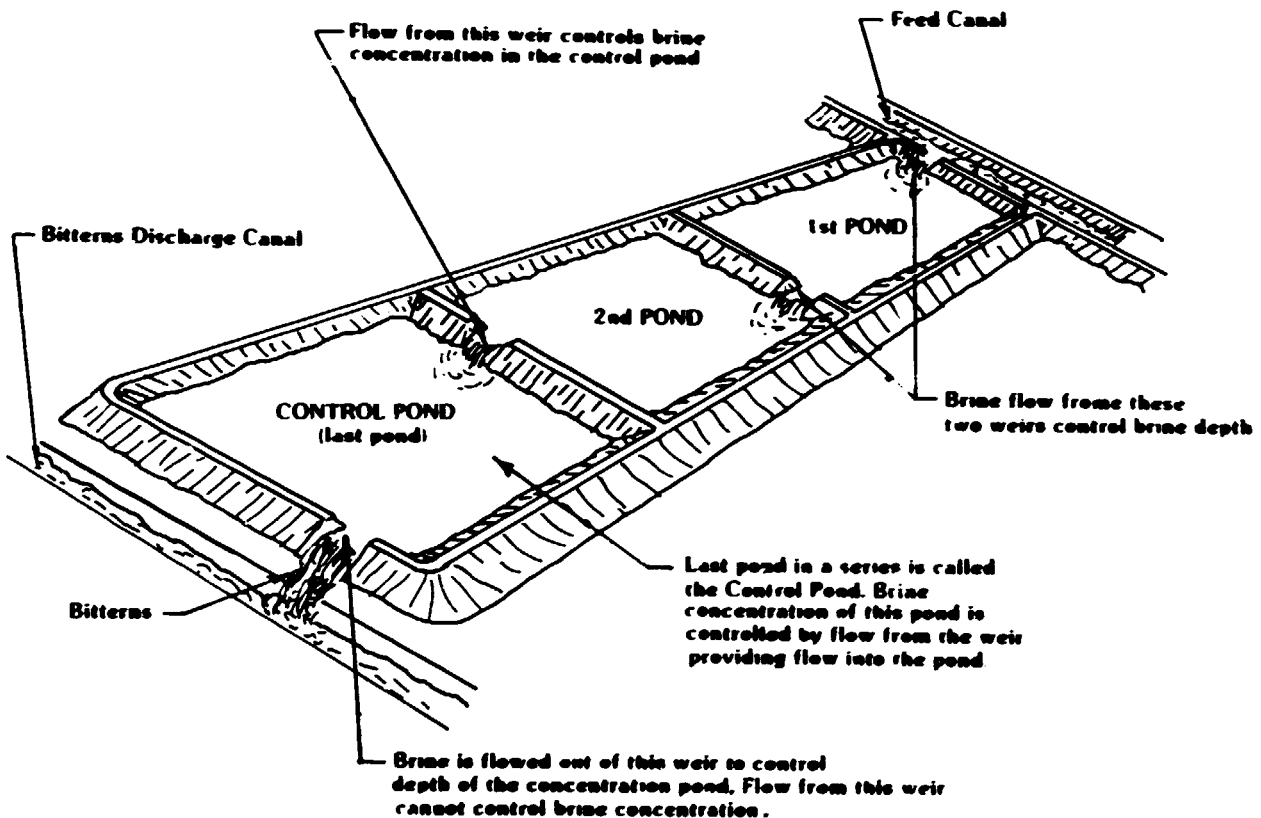
Series Flow System

Ponds should be run all season at a low level of about 30 centimeters where possible. Flow rate into ponds will be continuous and controlled by two indicators. The first is concentration in the last pond of the flow series. If the concentration is high, then more flow will be introduced into the pond. If the concentration is low, then flows will be reduced or stopped until concentration increases to the desired level.

This control is easily done at El Mex. The large intermediate pond labeled "D" in the illustration is a good surge area. This brine is allowed to flow into Pond 15 via the canal as shown. Brine from 15 flows through an open weir to Pond 9. Brine in Pond 9 is held between 29 and 30° Be (2.6 to 3½ Mg). If Pond 9 is too high in concentration, more brine from Pond 12 is allowed to enter. The water evaporated from Pond 12 and the brine flowed from 12 to 9 is replaced by brine flow from 15. Brine lost from 15 is replaced by brine from Pond D.

The following figure illustrates these control principles. Series flow through at least two ponds will increase purity of salt and production. Three or four ponds in series will increase it even more.

ILLUSTRATION OF SERIES FED PONDS

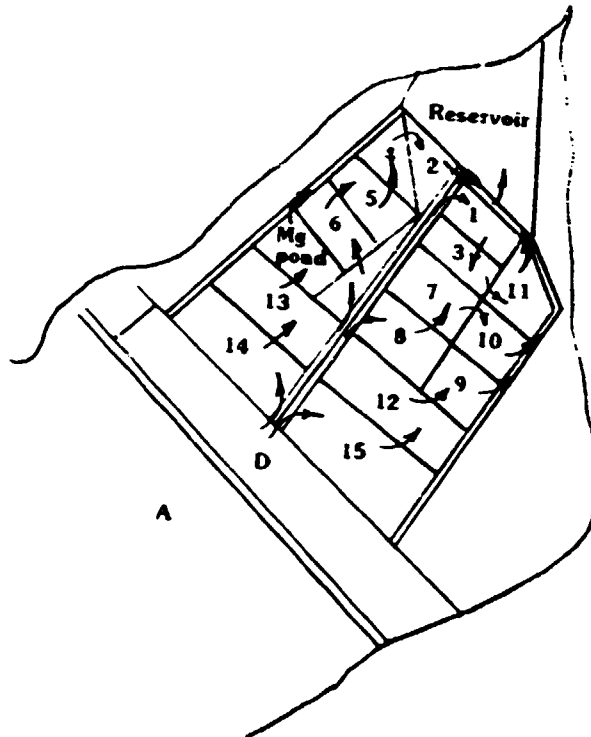


Key in the operation of a series pond system is the weir flowing into the last pond. If control pond concentration is too high, simply increase the weir flow to the pond. If concentration is low, slow down the feed or stop it completely.

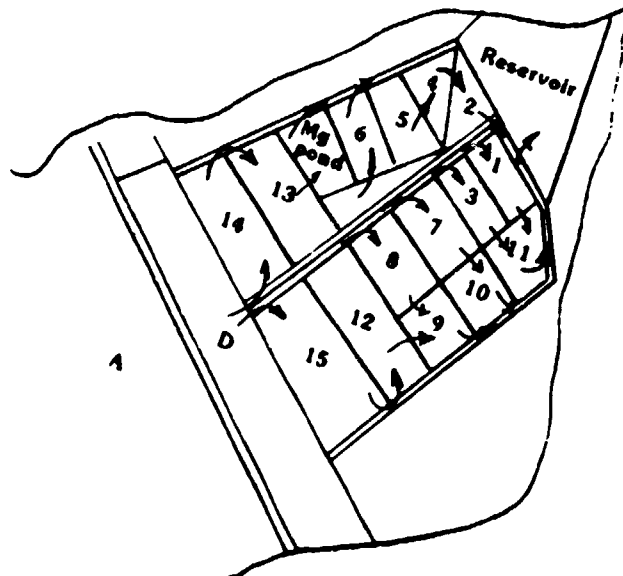
It is also desirable to have brine flowing through the ponds continuously during the evaporation season. A good grade is produced at 30 centimeters depth and 29 Be bitterns.

SEQUENTIAL FLOW AT EL MEX

The ponds at El Mex would produce more salt and better quality if they run in series. At least three ponds should be run together and the flow should be continuous. This procedure is different than now practiced at El Mex. The following figure illustrates one possibility.



The actual flow will depend on many factors. GSL does not know where the weir placements are. It may be easier to use canals as shown in the next illustration.



3.3 Discussion of K_2SO_4 Production

El Mex Salines is a solar pond system producing a bitterns brine containing potassium, magnesium, sulfate, sodium and chloride ions. Since capital money has already been spent on this large complex, a study has been made to investigate the possibility of concentrating these bitterns in the same solar ponds. The concentrated brine would then be used to deposit mixed salts of epsomite, kainite, carnallite, and halite. The salt mixture would contain 8-10% potassium and near 20% sulfate. This mixture would be removed from solar ponds, purified in a refinery and sold as potassium sulfate.

Great Salt Lake Minerals & Chemicals Corporation (GSL) has the technology to produce potassium sulfate as described above. They are the worlds largest producers of K_2SO_4 from solar ponds.

It has been found however that brine at El Mex will not evaporate well at high concentrations. Evaporation studies made by GSL from El Mex data indicates that brine saturated in potassium will not evaporate. The rate at which brine will evaporate depends on its concentration and time of year. The best time of year is June, July and August. Evaporation of brine at this period of time is:

$$\text{Evaporation} = 18 - .26x$$

$$\text{where } x = \text{moles } MgCl_2 / 1000 \text{ moles } H_2O$$

If this equation is solved for x when evaporation is 3 centimeters per month, $x = 57.7$ moles $MgCl_2 / 1000 H_2O$. At this concentration, brine is not even saturated in potassium and salt production per hectare is low. At higher concentration, evaporation ceases before sufficient potassium salts can be crystallized to finish off the brine. These conditions do not favor an economical production of potassium bearing salts.

It is recommended however that an attempt be made to concentrate salt bitterns to as high a concentration as possible for the following reasons.

1. Bitterns should be isolated from the system even if by-products are not made. The reasons for this have already been explained.
2. Actual evaporation of highly concentrated brine has not been verified. Isolation of bitterns as suggested could provide needed information to see exactly how far brines can be concentrated and how to better design for possible K_2SO_4 and magnesium salt production.

3.3.1 Possible K_2SO_4 Production Rates

El Mex has a reserve of brine and a salt bed. Normally sea water will be concentrated from very low values of sodium and magnesium. At El Mex, sea water is flowed over a salt floor where salts are dissolved and the sea brine is enriched. It is estimated that there are 10,000,000 ton of salt in the bed. It is also estimated that salt in the ocean feed brine is 500,000 to 1,000,000 ton of salt per year depending on whether draining water (15,000,000 ton per year) contains salt or not. It appears that a rate of 1,000,000 ton per year of halite can easily be sustained for the next 15 to 20 years.

According to El Mex personnel, evaporation can support a feed rate from the sea of 37,000,000 ton per year. Since sea brine contains 0.038% potassium, then $37 \times 10^6 \times .00038 = 14,060$ ton is entering into the solar pond area each year. Once a bittern concentration area is set up, plant efficiencies and brine entrainment losses are considered, production rate from sea brine alone can only be 7,030 ton per year of potassium or 15,500 ton K_2SO_4 .

The present reserve in the ponds is estimated at 24 million ton in the pre-concentration pond. The concentration of this brine is 0.3 percent of potassium. This is less than 1/2 the concentration expected from previous reports given to GSL (See reference 3). The total reserve of K is only 72,000 ton. In the 7 square kilometers salt crystallizer, the 3,500,000 million ton of brine contains only 24,500 ton of potassium. This is a combined equivalent of 215,017 ton K_2SO_4 . Since only 50% can be recovered as solid product, then 107,500 ton K_2SO_4 is a potential product.

If this 107,500 ton were to be harvested over ten years and combined with the potential of 15,500 ton per year from sea brine, only 26,250 ton can be produced. Possible conversion of an external recycle of muriate of potash (KCl) could boost production to 40,000 ton per year. In GSL's opinion, this is a small amount and it would be difficult to justify the capital expense.

It is also well to note that ten years after production starts, the present reserve of K_2SO_4 will be depleted and only 15,500 ton per year from the sea could be produced.

The use of Borg El Arab to supplement El Mex K_2SO_4 does not appear feasible. A plant could not be justified at both places. This means that salts from Borg El Arab would need to be transported from there to El Mex. Mixed salts would contain less than 9% potassium and it would require about 13 ton of salts to make one ton of K_2SO_4 . At best, cost of harvest and haul plus

handling at Borg El Arab and El Mex would place the cost at well over 7 dollars per ton. The expenditure to get it into a plant at El Mex would be \$7.00 times 13 or \$91 per ton K_2SO_4 . Add this to a processing cost at the plant of \$30 plus depreciation of the plant and it would exceed the sale price of K_2SO_4 . There would be no payback.

In the case of MgO production, it could be possible to use Borg El Arab bitterns. The brine could be treated with lime to make MgOH. The MgOH could then be filtered and sent to El Mex where MgO could be produced from it. More details on this are given in another section of this report.

3.4 K_2SO_4 Plant Process

Assume that salts can be obtained. These salts will be processed in a plant having the flow as shown on Figure 4. The process has several advantages because only water is used as a conversion media. If the flow of Figure 4 is simplified to only flow stream in and out of the plant, a simple picture of the process can be seen. The following illustration shows these streams.

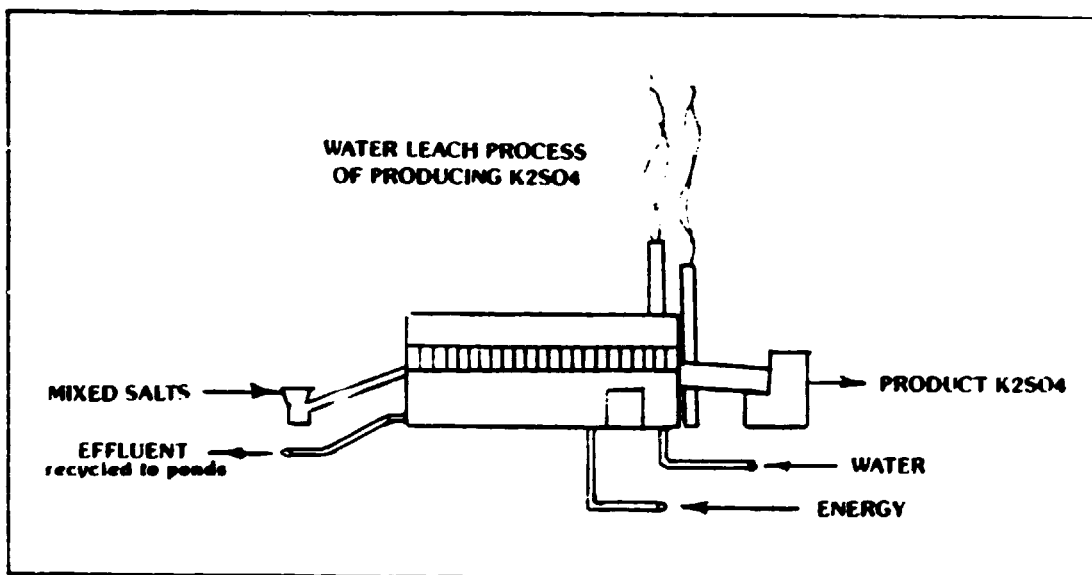
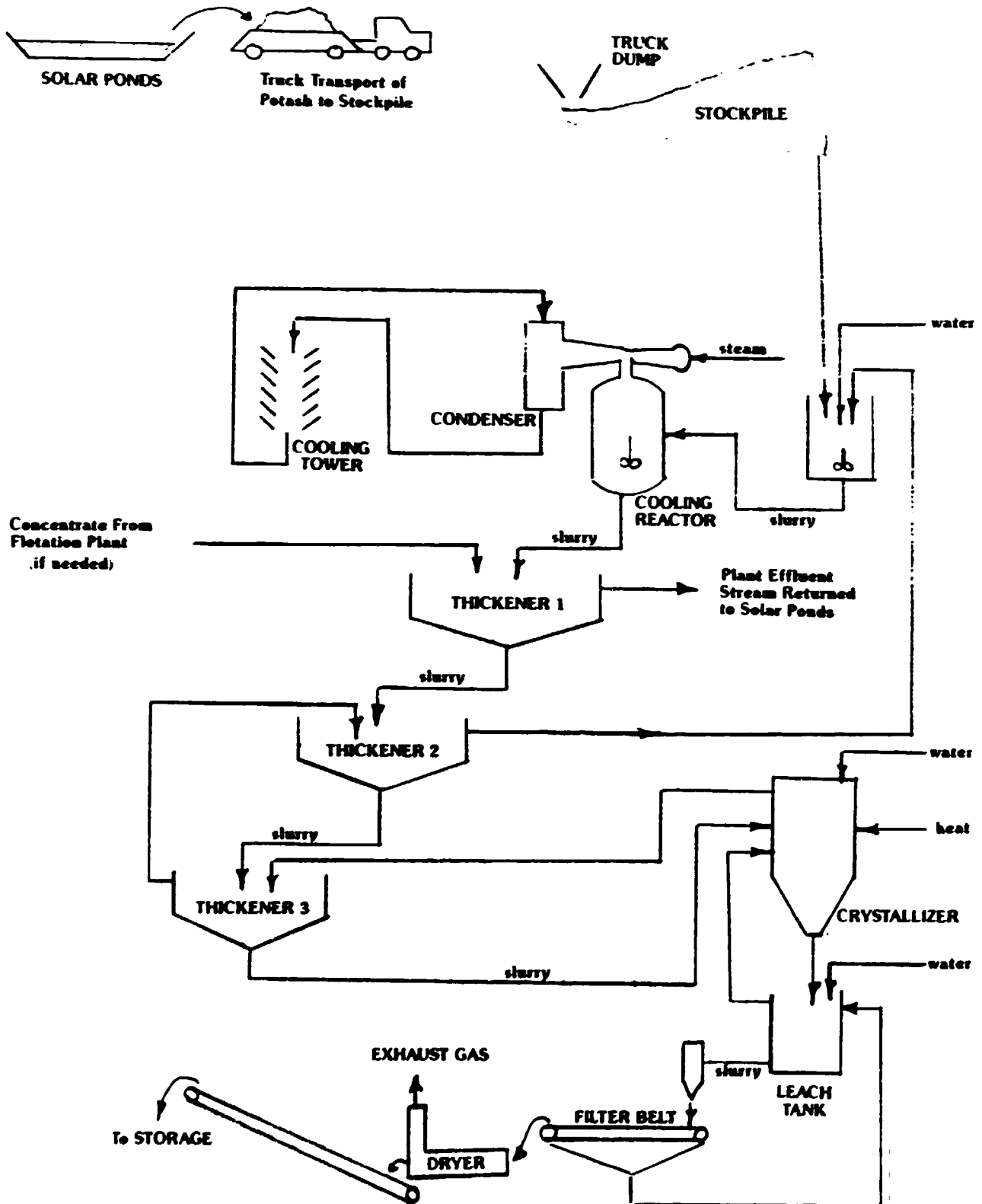


FIGURE 4

POTASSIUM SULFATE PLANT CIRCUIT PURIFICATION, CLEANING, AND CRYSTALLIZATION OF POTASSIUM SULFATE, K_2SO_4 , FROM MIXED SALTS



There are only four streams plus the energy input. Water flows counter-current to solids. The water dissolves out impurities resulting in a purified product K_2SO_4 . The cleansing water becomes saturated in potassium and sodium. It also contains impurities of magnesium sulfate and chlorides.

The overall efficiency is not very good because a lot of potassium is dissolved with the impurities and discharged from the plant with the effluent. This effluent is recycled back to the solar ponds where the impurities are separated out and the potassium is re-deposited and returned back to the plant a year later. Figure 4 shows the overall pond flow with the refinery included.

In an attempt to reduce potassium losses via the plant effluent and increase plant efficiency, the effluent is cooled. This is done at GSL with stream extractors and evaporation cooling. The weather in Alexandria however, does not favor evaporative cooling and plant operation would need to be limited during the colder months of December, January and February or artificial cooling would be necessary. Potassium salts are sensitive to temperature and impurities $NaCl$ and $MgCl_2$ are not. Thus losses of potassium are reduced by cooling the effluent stream and forcing potassium salts (usually schoenite) to crystallize while $NaCl$ and $MgCl_2$ remain in the effluent and are rejected back to the pond system.

Even though the production of K_2SO_4 does not look promising from a solar pond standpoint, the plant flow and capital expenditure has been given as a measuring stick. GSL is not aware of anyone else producing K_2SO_4 from sea brine. This indicates that production from sea water is not easily accomplished. It has been tried at some of the largest salt works in the world, such as Exportadora del Sal in Baja, Mexico, but without success. It was also tried at Lake McLeod in Western Australia by Texada Corporation. It too was unsuccessful.

It is understood, however, that the French are having some limited success in production of K_2SO_4 and MgO from their salt works. Perhaps they could be approached for technology. The director of technology at Salines du Midi is Mr. Denis Drummond. His address is shown later in this report.

Other methods of making K_2SO_4 are discussed in Appendix One.

COST ESTIMATE FOR A K_2SO_4 PLANT

- Basis:
1. Plant runs December through April only.
 2. Production rate is 300 ton per hour.
 3. 14,000 ton of KCl will be converted to K_2SO_4 each year.
 4. Total yearly production is 40,000 ton.

This cost estimate for a K_2SO_4 plant is based on a cost if the plant were to be built at GSL's site in Ogden, Utah. The following summarizes costs.

A. EQUIPMENT COSTS

Conveyors	\$1,014,862
Cooling Tower	106,714
Crystallizer	437,226
Field Erected Tanks	573,348
Hoppers	314,000
Spouting	120,000
Apron Feeders	184,450
Screw Conveyors	16,500
Bag Conveying Equipme :	26,670
Secondary Crusher	20,180
Primary Crushers	47,870
Shop Fabricated Tanks	27,224
Belt Scales	61,386
Track Scales	45,044
Vibrating Feeder	11,614
Roll Crusher	5,770
Bag Crusher	23,848
Agitators	128,904
Dryer	215,430
Thickeners	490,598
Belt Extractor	74,000
DSM Screens	27,036
Belt Filter	174,884
Vibrating Screens	35,522
Wet Cyclone	16,922
Heat Exchanger	36,980
Fire Pump	12,818
Jet Slinger	6,626
Pumps, Cast Iron	15,634
Pumps, Vertical	26,680
Pumps, Slurry	57,500
Sealine for Thickener Tanks	8,000

Lump Breaker with Conveyor	147,870
Tramp Metal Remover	12,738
Gates and Diverters	49,750
Dust Collectors (Scrubbers)	32,808
Bin System	68,000
Condensor Pumps	10,000
Bridge Cranes and Hoists	62,000
Heating Equipment	80,000
Raw Water Supply	13,000
Plant Supply Equipment	<u>240,800</u>
	Total
	\$5,081,286
	Tax
	120,000
	Freight
	140,000
	Erection Costs
	<u>600,000</u>
Grand Total Erected Equipment	\$5,941,286 U.S.

B. Earthwork	600,000
C. Concrete	500,000
D. Structural	1,775,000
E. Electrical	1,220,000
F. Piping	1,440,000
G. Insulation	166,000
H. Instrumentation	538,300
I. Painting	318,000
J. Miscellaneous	<u>1,400,000</u>
Total Direct Cost	\$13,893,586

Construction Overhead	980,000
Engineering	1,600,000
Contractor Fees	650,000
Owners Supervision	650,000
Contingency (20%)	<u>2,800,000</u>
Subtotal	\$20,573,386
Spare Parts	2,000,000
Grand Total for Turn Key Plant	\$22,500,000

Notes:

- 1) Connected horsepower is 4200.
- 2) Capacity is 300 tph.
- 3) Granulation of product is not included in cost.
- 4) Changes to ponds or harvest equipment is not included in cost. Stockpile and reclaim are included.

Direct Operation Manpower

Operation

4 shift foremen

29 plant operators as follows:

- 5 crusher operators
- 5 wet process operators
- 5 control board operators
- 5 dryer operators
- 5 laborers
- 4 loadout operators

Support personnel

- 4 stockpile and reclaim operators
- 13 maintenance personnel (experienced)
- 1 General Foreman
- 1 Instrumentation Engineer
- 2 Electricians
- 5 Laboratory Technicians
- 2 Support Engineers

Total direct manpower 61

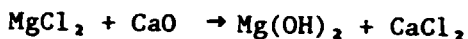
Indirect manpower as needed:

- Sales force
- Accounting
- Plant Manager
- Superintendent

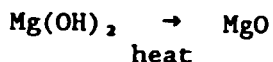
Note that harvest, pond operations and pond modification costs are not included in the above outline.

3.4 Discussion of MgCl₂ and MgO production.

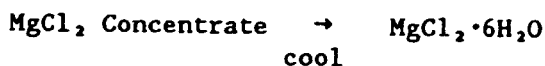
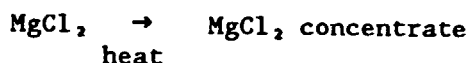
El Mex brines can be concentrated to contain 6% Mg in the ponds. This magnesium can be removed by reacting it with lime.



The MgOH solids are then filtered and impurities of CaSO₄, CaCl₂, MgSO₄, NaCl, etc. are removed. The purified MgOH is then converted to MgO:



MgCl₂·6H₂O Flake can also be easily produced from the brine.



MgCl₂·4H₂O, MgCl₂·2H₂O or other hydrated forms can be made depending on how much water is removed in the heating step.

Figure 5 shows a flow sheet for MgCl₂ flake. This product is produced at GSL in several grades. Production of MgCl₂·6H₂O is relatively easy and would be a good product for El Mex if it can be marketed.

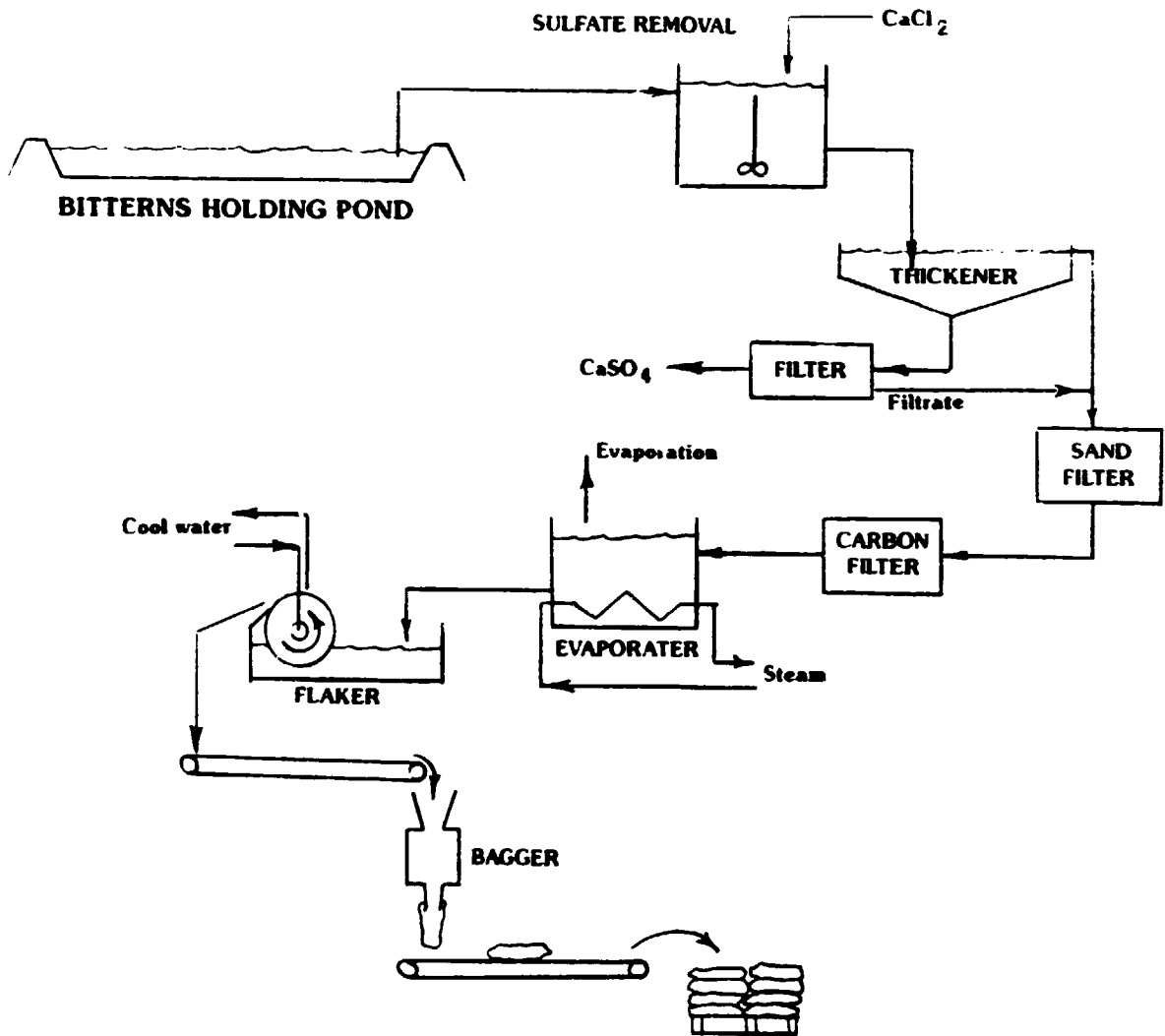
The flake can be made into 6,5,4 or 3 water of hydration by controlling the concentration of magnesium in the evaporator. A concentration of 12% magnesium will produce bischoffite (MgCl₂·6H₂O). Concentration of higher magnesium will produce a flake with lower water.

All flake must be bagged immediately because it is hygroscopic. Magnesium chloride is used in oxychloro cements, ion exchange resins and certain specialty chemicals applications.

3.4.1 Magnesium Reserves and Production at El Mex.

Magnesium is 1.35% in reserve brine and 0.13 in the sea. Applying the same principles of production as K₂SO₄, there is an equivalent of $37 \times 10^6 \times .0013 = 48,100$ ton Mg per year in the feed and $24,000,000 \times .0135 + 3,500,000 \times .015 = 376,500$ ton or 37,650 ton over a ten year depletion. Total potential for the first ten years at 50% recovery is 70,000 ton per year MgO. Long range is 40,000 ton MgO per year from El Mex.

FIGURE 5
MAGNESIUM CHLORIDE FLAKING CIRCUIT
 $MgCl_2 \cdot 6H_2O$



Add this to possible feed stock from Borg El Arab and a long range MgO production facility at El Mex could be a possibility.

Capital and Operating Expenses to Produce $MgCl_2 \cdot 6H_2O$

At GSL flaked $MgCl_2$ must be low in sulfate and sodium and it must be white. $CaCl_2$ is added to reduce SO_4 levels. The resulting gypsum particles are fine and difficult to separate from the solution. Thickening and filtering are needed to remove particles. A carbon filter and a sand filter are used to remove the dark color usually associated with highly concentrated bitterns.

Capital expense is based on a system as shown in the flow diagram. There are several alternatives however. SO_4 can be removed by heating, for example. The sulfate ion has a reverse solubility and heating drives out kieserite ($MgSO_4 \cdot 6H_2O$).

Basis: Plant runs all year. 10,000 ton per year $MgCl_2 \cdot 6H_2O$
6% Bitterns can be made in ponds.

Equipment Cost

Sulfate removal tanks	30,000
Thickener	100,000
Drum Filter	75,000
Sand Filter	50,000
Carbon Filter	50,000
Evaporator tanks (two)	30,000
Boiler	85,000
Heating Equipment	20,000
Flaker	25,000
Bagger	80,000
Pumps	55,000
Bridge cranes and hoists	12,000
Agitator	18,000
Heat exchanger	10,000
Conveyor belts	35,000
Bin systems	15,000
Screw conveyors	10,000
Plant supply	<u>50,000</u>
Total	750,000
Tax	
Freight	23,000
Erection	<u>100,000</u>
	873,000

Earthwork	20,000
Concrete	50,000
Structural	34,000
Electrical	25,000
Piping	75,000
Insulation	5,000
Instrumentation	12,000
Painting	22,000
Miscellaneous	<u>50,000</u>
Total Direct Cost	1,166,000

Construction Overhead	100,000
Engineering	120,000
Contractors Fees	100,000
Owners, Supervisors	50,000
Contingency (20%)	<u>250,000</u>
SubTotal	1,786,000
Spare Parts	<u>50,000</u>
Grand Total	\$1,836,000

Discussion of MgO Production, Flow and Capital Expenses.

GSL has not produced MgO. There are several facilities that do produce it from brine however. The Israelis have been doing it from MgCl₂ brines at their Dead Sea Works operation. They were assisted by Sulzer Escher Wyss and by Babcock International. They may possibly have the technology. Possible contacts to each facility are listed below.

Dr. Edward Kratz
Senior Technologist
Sulzer Escher Wyss
P.O. Box
CH-8023
Zurich, Switzerland

Mr. Derek Gosden
Babcock Woodall-Duckham Ltd.
11 The Boulevard
Crawley, Sussex
RH10 10X
England

It is also understood that the French are doing some work in developing MgO from sea brine and they may be willing to joint venture or supply technology through an arrangement of mutual benefit.

Dennis Drummond
Compagnie Des Saline du Midi
Et Salines De L'est
51 Rue D'Anjou F 75002
Paris, France

Magnesium Oxide Plant Flow Description

One major possibility for magnesium production at El Mex is the reaction of lime with MgCl₂ brine. This is done commercially by several companies. At Freeport, Texas lime is reacted with sea brine. Sea brine has only 2.2 g/l of MgO equivalent where El Mex brine at 6% Mg contains over 100 g/l.

Production of magnesium compounds from bitterns water is made possible by the almost complete insolubility of Mg(OH)₂ in water. Reaction of lime of dolomite with bitterns produces Mg(OH)₂ from MgCl₂ or MgSO₄ in solution.

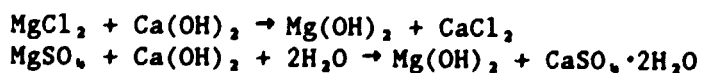


FIGURE 6
MAGNESIA FROM EL MEX BITTERNS

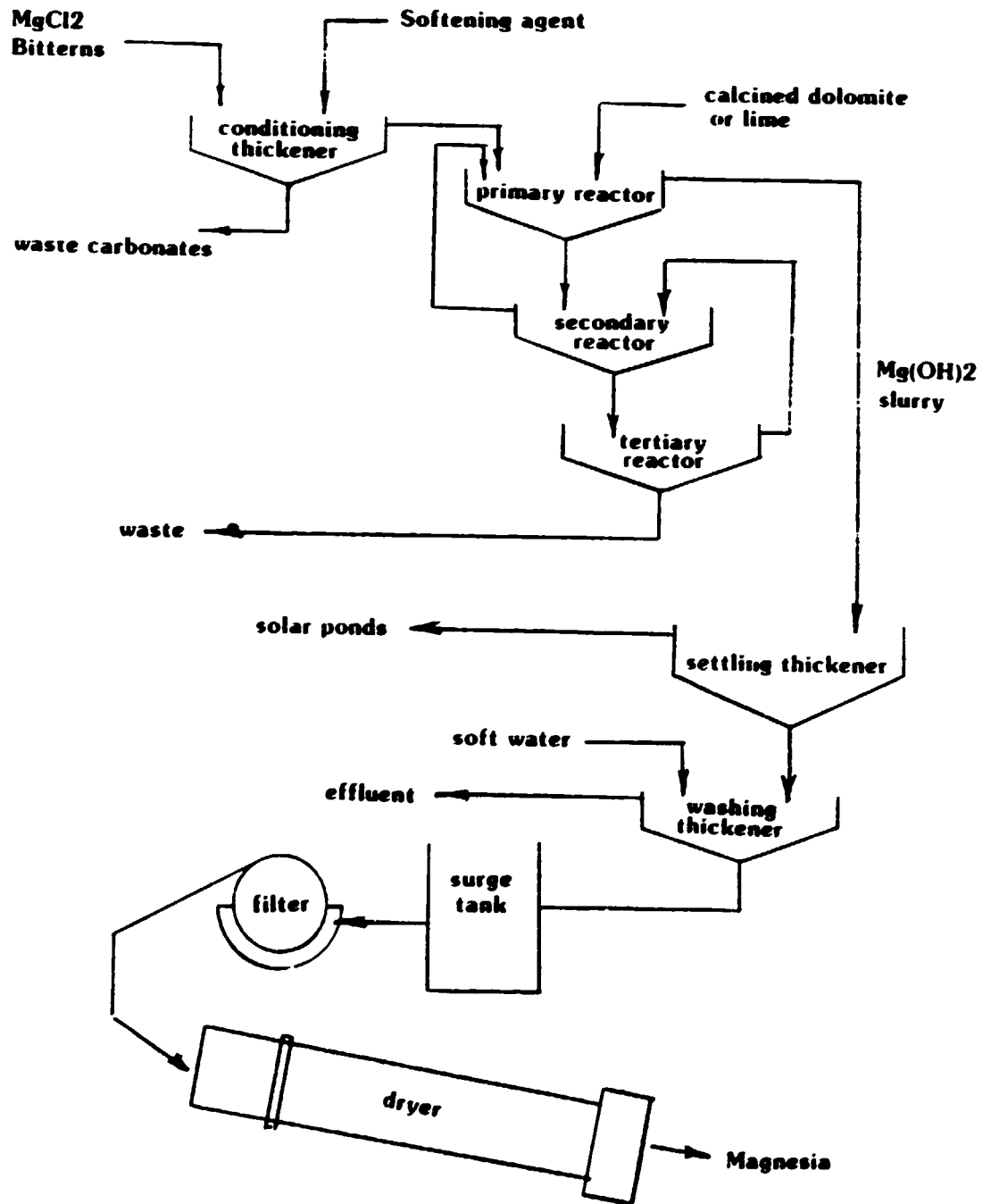
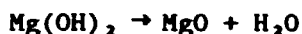


Figure 7 shows a flow chart for producing magnesium compounds used in pharmaceuticals, tooth powders, antacid remedies, anti-caking agents (for table salt) and paint fillers.

MgOH becomes the basis for making MgO via calcination



Other processes require the following steps:

1. Water softening with lime or calcined dolomite
2. Preparation of a purified lime or slurry
3. Removal of precipitated Mg(OH)_2
4. Purification of Mg(OH)_2
5. Filtering of slimes
6. Firing of Mg(OH)_2 to form MgO

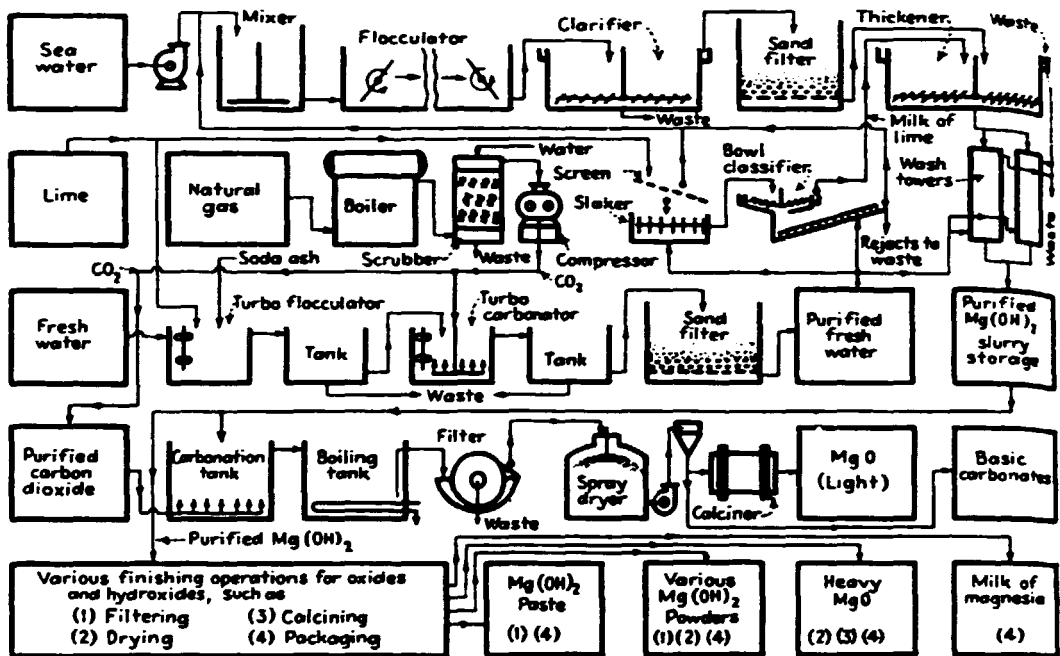
Magnesium compounds have been made from sea water or concentrated sea brine by the following companies.

Dow Chemical Company at Freeport and Velaco, Texas
Merck and Company, San Francisco, California
FMC, Newark, California
Kaiser Chemical Division, Moss Landing, California
H.K. Porter Co., Pascagoula, Florida

Figure 7 shows a flow chart for Mg(OH)_2 from sea water and dolomite. Calcined dolomite is added in enough quantity to pre-test the brine bitterns and remove any carbonate. At El Mex this may not be necessary because carbonates have mostly been removed by concentrating the sea water in solar ponds. Any remaining calcined dolomite would work well to soften the brine. The softened bitterns then flow to reactors where more dolomite (or lime) is added to precipitate Mg(OH)_2 .

Mg(OH)_2 is a very fine particle suspension which overflows with liquors from the reactor. The fine Mg(OH)_2 is difficult to collect and dewater. Several thickening steps are required and considerable space is needed for these thickeners. Even with thickening and filtration, the Mg(OH)_2 cake still contains high moisture. The cake is then dried at temperatures up to 1800°F to produce various grades of magnesia.

FIGURE 7



Purified magnesium compounds from sea water at South San Francisco. (Nerck & Co.)

REFERENCES

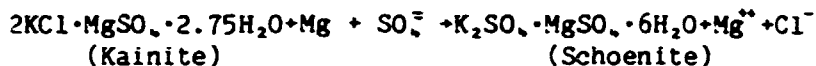
1. Concentration Path of El Mex Brine and Ocean Brine by GSL Solar Consultants & Advisors, Inc., September, 1988.
2. Brine Evaporation at El Mex Salines, November, 1988.
3. Field Report of El Mex Salines Salt Works and its potential to produce potassium sulfate and other by-products, by David Butts, April, 1987.

APPENDIX ONE
VARIOUS METHODS USED TO PRODUCE K_2SO_4

It is possible to float schoenite as done at Great Salt Lake Minerals but efficiency of a kainite float is reported to be much better than schoenite. Floating the two at the same time is inefficient. It is therefore important to remain in the kainite phase.

2.1.2 Conversion of Kainite to Schoenite

The second step in the process is to convert kainite to schoenite as shown in the following equation:



Of course this conversion must be done in conditions where schoenite is stable and kainite is unstable. A source of sulfate is also needed. This needed sulfate is made later in the schoenite decomposition step. Kainite cannot be efficiently decomposed into K_2SO_4 directly. The conversion to schoenite however is relatively easy.

Figure 2 shows all of the process flow steps after flotation. Enriched kainite is transferred into an agitated reactor tank where it is mixed with high sulfate brine. This brine is saturated in schoenite and arcanite having just come from the schoenite decomposition crystallizer circuit. (See the figure). This reactor mixture is next pumped to a thickener where conversion of any unreacted kainite is completed.

Conversion of kainite to schoenite is relatively easy and fast. Enriched kainite is already of small particle (-28 mesh). A high sulfate brine is mixed with it and therefore conversion is rapid.

2.3.3 Schoenite Conversion Enhancement

The final process step is conversion of schoenite to arcanite. Both the conversion of kainite to schoenite and schoenite to arcanite are dependent on the sulfate concentrated in the liquor. High sulfate forces kainite to schoenite and high K_2SO_4 forces higher efficiency in the conversion of schoenite to arcanite. For this reason an enhancement step is used in the process called syngenite.

Liquid from the schoenite thickening step is reacted with gypsum in a mixing tank to form syngenite.

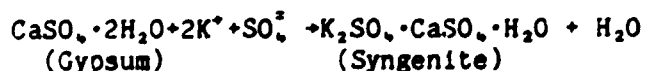


FIGURE 1.
KAINITE FLOTATION STEP

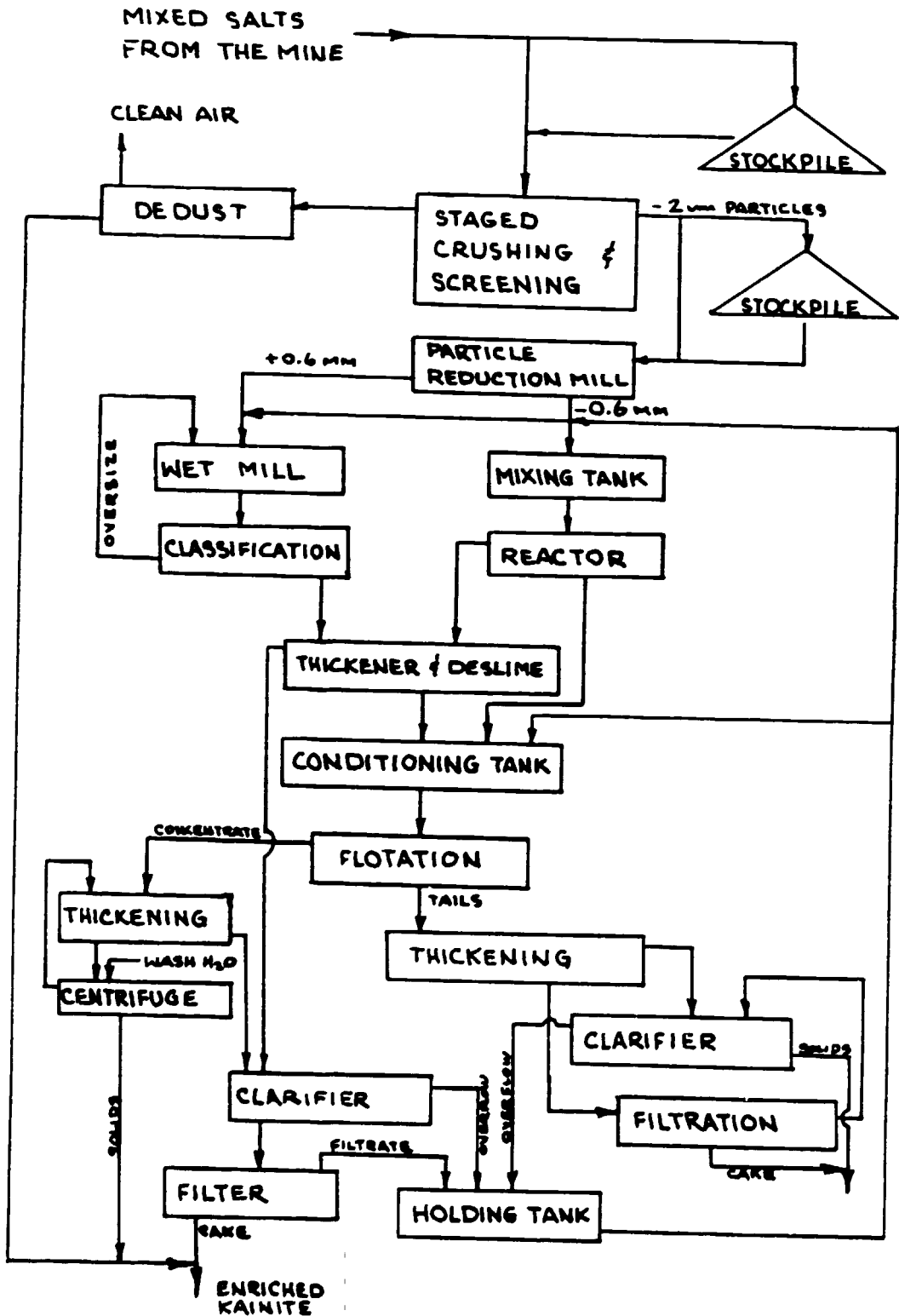
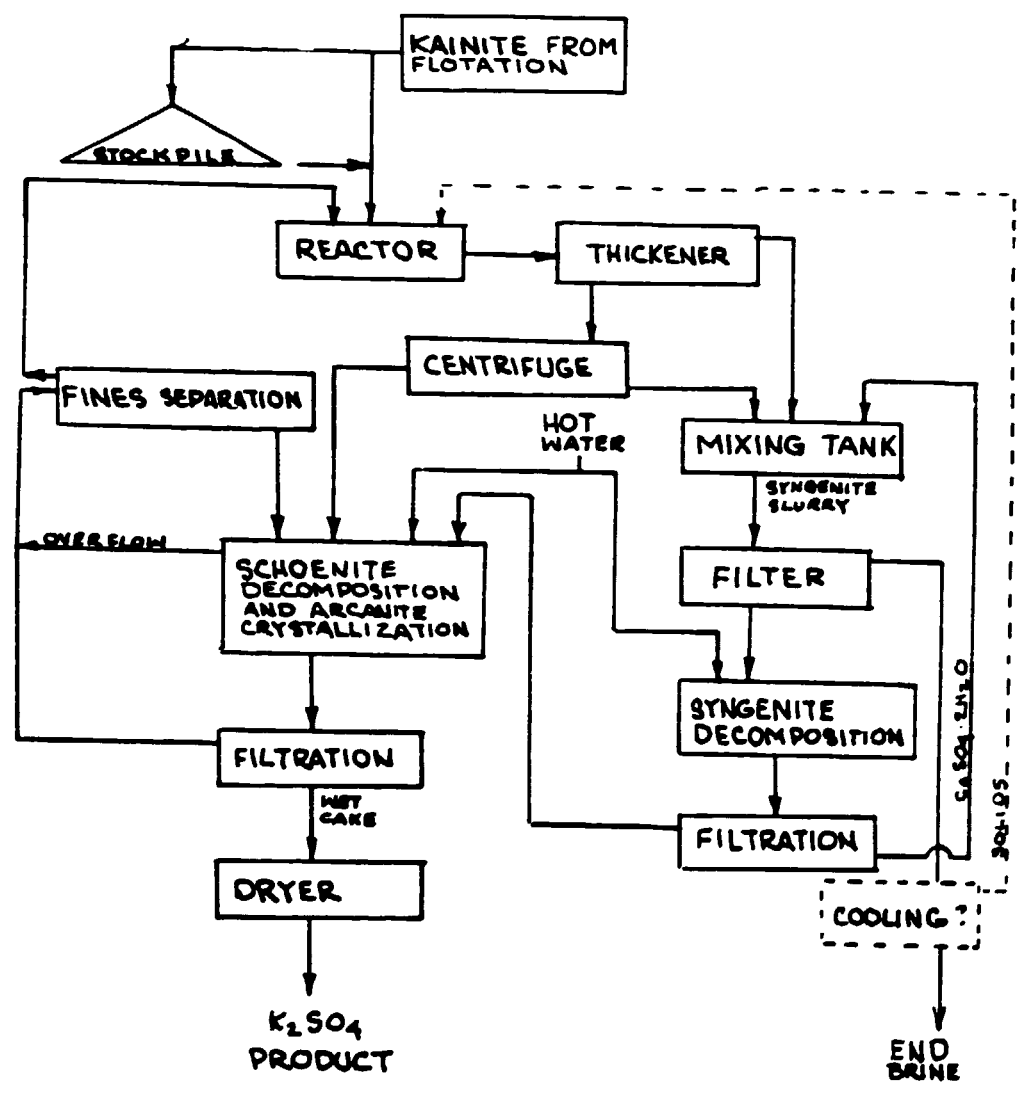
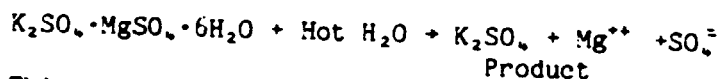


FIGURE 2.
KAINITE TO SCHOENITE CONVERSION
AND SCHOENITE DECOMPOSITION STEPS.



Syngenite is then filtered. The syngenite cake is then reacted with hot water where all of the K_2SO_4 is dissolved. $CaSO_4$ is not soluble in hot water and it is recycled back for reuse to make more syngenite in the mixing tank.

The leach water liquor pregnant in arcanite (K_2SO_4) is sent to a schoenite decomposition crystallizer where solid phase K_2SO_4 is formed. Magnesium sulfate is more soluble in hot water than potassium sulfate. Therefore, when a hot solution of K_2SO_4 is mixed with schoenite the following reaction will occur:



This reaction is discussed in more detail in the next section.

2.1.4 Schoenite Decomposition

Schoenite decomposition is based on the different solubilities of K_2SO_4 and $MgSO_4$ in water as shown in Figure 3. Note that the solubility of $MgSO_4$ is higher than K_2SO_4 . When water is reacted with schoenite, K_2SO_4 is left as a solid and becomes the final product after filtering and drying. Of course, some K_2SO_4 is also dissolved in the process but some is recovered later in the syngenite process.

It is seen that $MgSO_4$ is not used up in the process and the liquor is recycled back to the kainite schoenite reactor.

A few details of the process and operation follows:

Figure 3 shows the solubility of a K_2SO_4 - $MgSO_4$ - H_2O system. All values are shown in grams per 100 grams of water. Figure 4 shows a development of mass balance equation to determine decomposition efficiency.

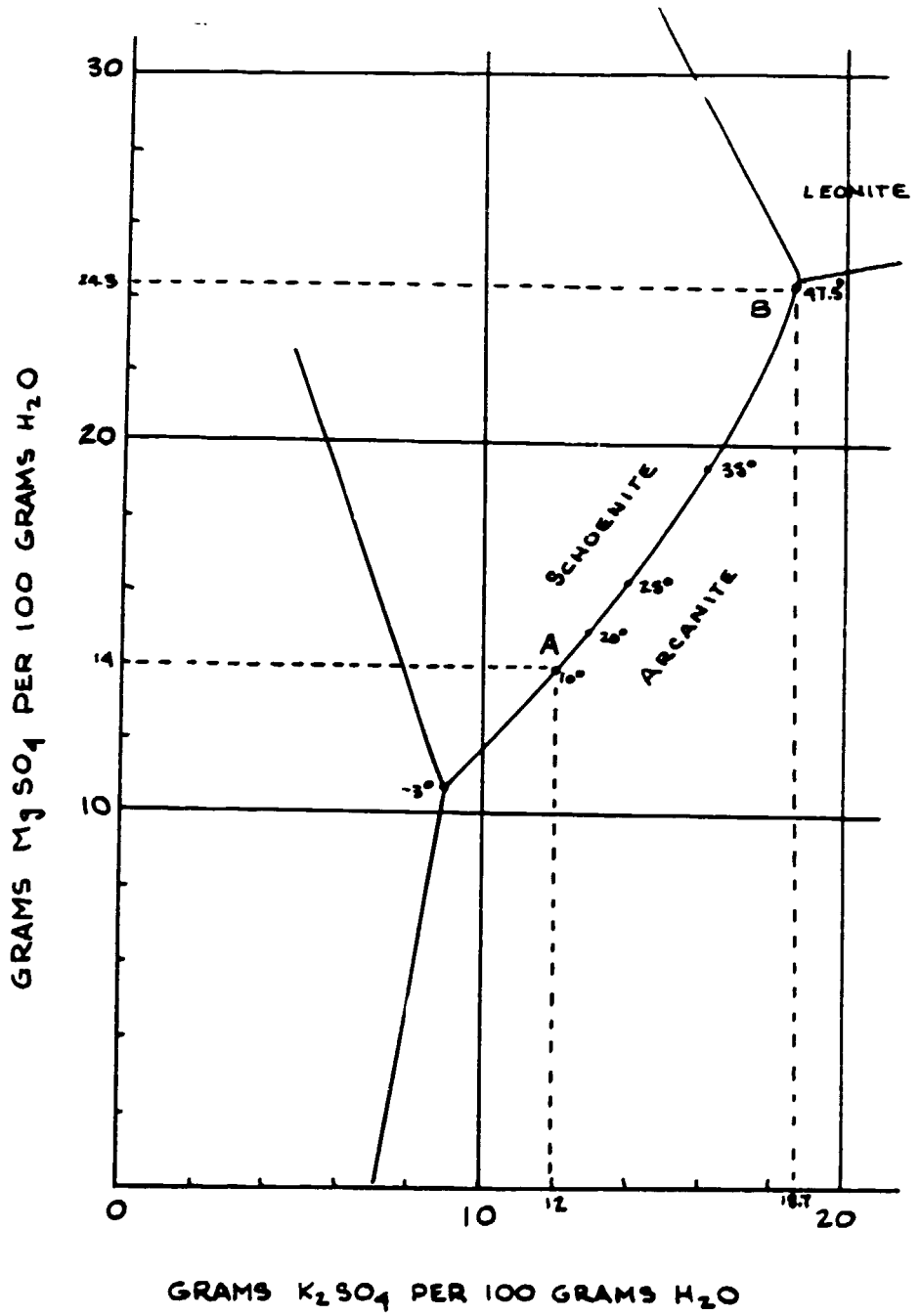
Point A on Figure 3 is the solubility of K_2SO_4 and $MgSO_4$ at $10^\circ C$. 12 grams of K_2SO_4 and 14 grams of $MgSO_4$ will dissolve in 100 grams of water. This is 9.5% K_2SO_4 and 11.1% $MgSO_4$. From this it is calculated that 269 ton of end liquor will be formed in the decomposition reaction. 187 ton of water must be added and 17.7 ton of solid K_2SO_4 will be formed. Potassium recovery from schoenite at 10° and pure water is therefore: $17.7/43.3$ or 41%.

If the same reaction is carried out at $47.3^\circ C$, Point B on Figure 3, the solubility of K_2SO_4 is 18.7 and 24.3 for $MgSO_4$. Using these numbers:

176.0 tons liquor is formed
96.3 tons of H_2O is added
20.2 tons of K_2SO_4 solids are formed

FIGURE 3

SOLUBILITY IN THE SYSTEM $K_2SO_4 - MgSO_4 - H_2O$



Recovery is 20.2/43.3 or 47%. Note how much less water is used at the higher temperature. Cooling of this water will later yield schoenite for re-use in the crystallizer.

A gain in recovery is seen by increasing temperature. Decomposition of schoenite can be done at any temperature between -3°C and 47°C. Efficiency of conversion is highest at 47°C, but heat must also be added and economics must be studied to see if the added energy cost justifies the increase in efficiency.

Overall conversion efficiency of 40+50% is indeed low. Use of Syngenite will increase efficiency by creating a water solution already containing K_2SO_4 . Any K_2SO_4 in the decomposition water means an equivalent amount K_2SO_4 will not be dissolved from schoenite and will consequently remain as solid SOP.

Crystallizer decomposition end liquor is relatively free of NaCl, and $MgCl_2$. This liquid is also saturated in schoenite and arcanite. It is therefore a valuable liquor to be recycled back and mixed with incoming kainite. Here the liquor dissolves soluble impurities and converts kainite to schoenite. It has been shown how this conversion forms $MgCl_2$. $MgCl_2$ is highly soluble and will actually depress the solubility of others salts.

Thus K_2SO_4 and $MgSO_4$ in the original liquor is forced out of the solution as it is mixed with kainite. $MgCl_2$ enters the solution. The salts forced out of solution form more schoenite which is fed back to the schoenite decomposition crystallization step. This increases the overall recovery of potassium in the combined steps to over 60%. The theoretical yield is as high as 67% but equilibrium of salts with brines are never reached and recovery is somewhat less.

Recovery of even 60 to 65% is still low. Use of the syngenite step is reported to bring recoveries up to 70 to 75% and chilling or cooling of effluent streams has been reported to bring up conversion efficiency as high as 82%. Both potassium and sulfate are temperature sensitive. Cooling forces $MgSO_4$ and K_2SO_4 salts to crystallize. These salts can be filtered and returned to the reactor. From the information given, GSL is not sure where cooling is done in the streams, if done at all, but one possible location is indicated on the flow streams of Figure 2.

It is quite possible that even after the syngenite step and cooling, there is still an excess of SO_4 salts in the end liquor that can be used for the reaction:

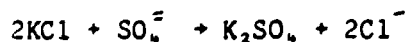
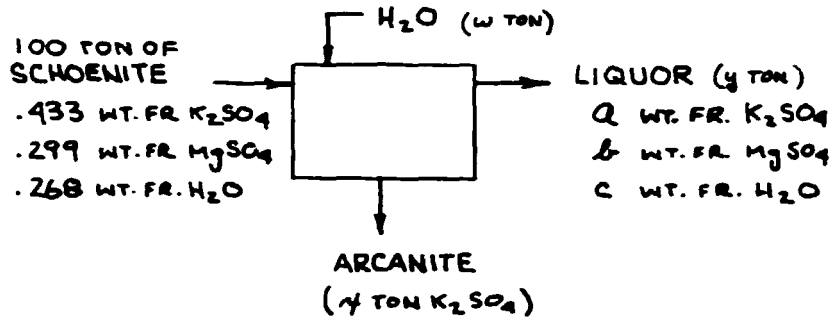


FIGURE 4.

SCHOENITE DECOMPOSITION MATERIAL BALANCE



	IN	OUT
WATER BALANCE:	$(100)(.268) + w$	$= (y)(c)$
$MgSO_4$ BALANCE:	$(100)(.299)$	$= (y)(b)$
K_2SO_4 BALANCE:	$(100)(.433)$	$= (y)(a) + r$

* AT $10^\circ C$: $a = .0952$, $b = .111$ & $c = .794$

FROM $MgSO_4$ BALANCE $29.9 = y(-.111)$, $y = 269.4$ TON

FROM WATER BALANCE $26.8 + w = (269.4)(.794)$
 $w = 187.1$ TON

FROM K_2SO_4 BALANCE $43.3 = (269.4)(.0952) + r$
 $r = 17.65$

THEREFORE: WATER TO PRODUCT RATIO = 10.6
 % POTASSIUM RECOVERY = 41 %

* AT $47.5^\circ C$: $a = .131$, $b = .1699$, $c = .70$

$MgSO_4$ BALANCE $29.9 = (y)(.1699)$, $y = 176$ TON

K_2SO_4 BALANCE $43.3 = (176)(.131) + r$, $r = 20.2$ TON

H_2O BALANCE $26.8 + w = (176)(.70)$, $w = 96.4$

THEREFORE: WATER TO PRODUCT RATIO = 4.77
 % POTASSIUM RECOVERY = 47 %

* CALCULATED FROM DATA OF FIGURE .

Such a practice has been optimized at GSL. The viability of such a conversion depends on cost of KCl, sale price of K_2SO_4 , and conversion efficiency.

2.1.5 Potassium Magnesium Sulfate (SOP/Mg)

Appendix 10/2 of reference (5) shows a cost table of SOP/Mg having 30-32% K_2O content. This product is apparently made by combining Schoenite with SOP. A section of Figure 2 is shown on the next page to indicate one way this could be done.

Appendix 10/2 also implies that .2925 ton of SOP is combined with schoenite to make one ton of product. The amount of schoenite is therefore 1-.2925 or .7075 ton.

It is also shown that 1.021 ton of kainite is needed. It is assumed that this is the amount of kainite needed to make .7075 ton of schoenite. 1.021 ton of kainite contains .1604 ton of potassium and .7075 ton of schoenite contains .1374 ton. Conversion efficiency is therefore $.1374/.1604$ or 85.7%.

The preceding calculation is based on pure substance. Pure SOP contains 54% K_2O , but SOP produced in Sicily has an average of 51%. SOP/Mg produced has an average of 31% K_2O . In order to produce a mixture having this concentration, a nearly pure schoenite must be combined with the 51% K_2O SOP. This balance is shown:

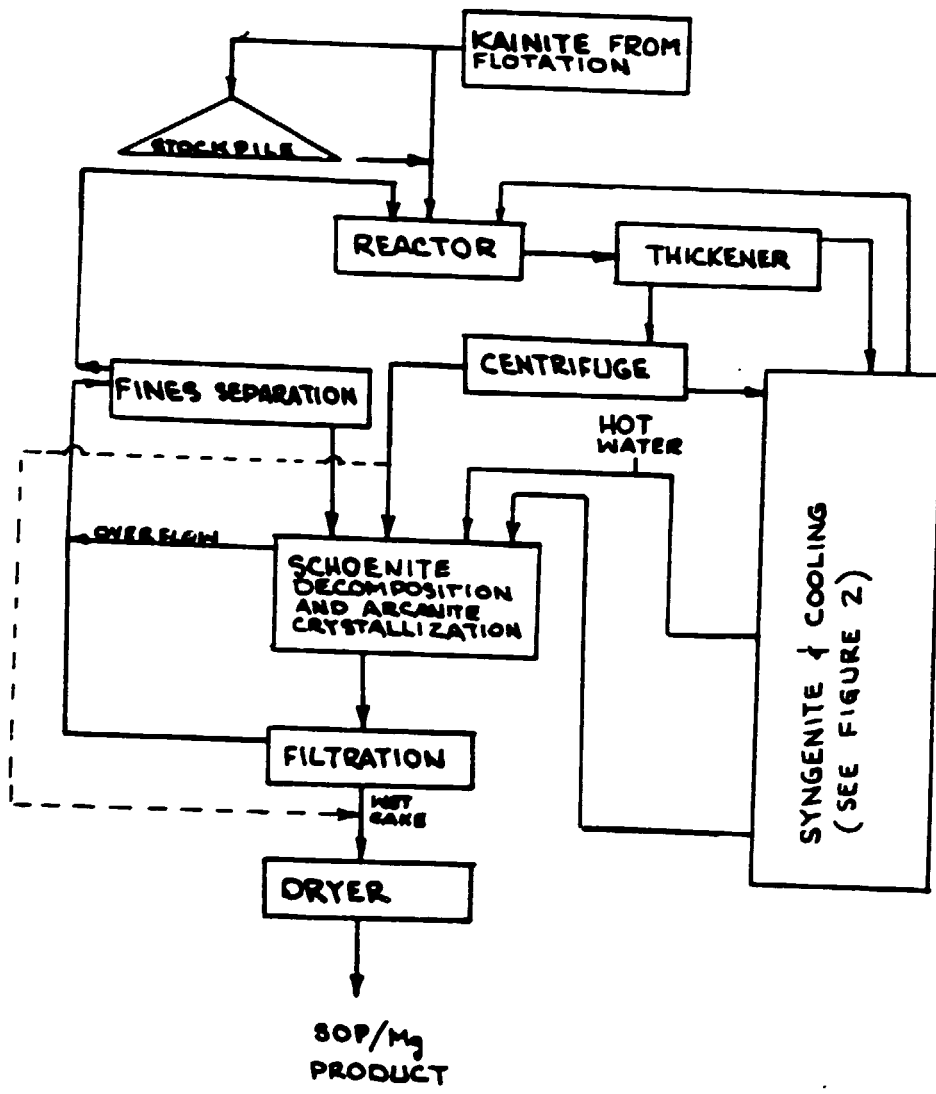
$$\frac{(.2925 \text{ TON SOP})(.51 K_2O) + (.7075 \text{ TON SCHOENITE})(.234 K_2O)}{1 \text{ TON SOP/Mg}} = .315 \text{ WT. \% } K_2O$$

Because SOP produced contains 51% K_2O , compared to 54% K_2O in pure SOP, the schoenite from which it is made must also be impure. If all impurities in schoenite become impurities in K_2SO_4 , then schoenite produced for the crystallizer must contain 22% K_2O and not 23.4% in the pure substance. This means that .73 ton of impure schoenite is added to 51% K_2O SOP. When the mixture is dried .024 ton of hydrated water is driven off. This is about 10% of total hydrated water. The final result is to have one ton of dried SOP/Mg at 31% K_2O .

2.2 Relevant Competitive Process in Production of K_2SO_4

There are other salts that can be used to produce K_2SO_4 . Even KCl is used as a base raw material to be reacted with H_2SO_4 , Na_2SO_4 , or gypsum. Since K_2SO_4 is more valuable than KCl, attempts are being made to convert KCl to the more valuable product. Price differences between the two varies with time and location.

PRODUCTION OF POTASSIUM-MAGNESIUM
SULFATE, SOP/M₃, 31% K₂O.



If one ton of KCl is converted completely to K₂SO₄, the conversion efficiency ton to ton would be 118%. This means that even at a conversion efficiency of 35%, one ton of KCl will still make 1 ton of K₂SO₄.

2.1.1 Conversion From KCl with Sulfuric Acid

Reaction of H₂SO₄ with KCl is practiced by some companies. the reaction is shown:



More acid is then added to complete the reaction.

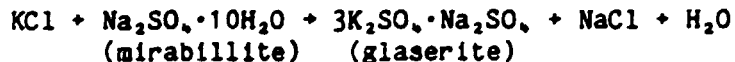


The process is carried out in Mannheim furnaces. It has been reported that the same conversion can be carried out in a fluidized bed reactor. This type reactor is used by Climax Chemical Corporation but they have not reported any details concerning their reactor design. Raw material cost is obviously high because the basis relies on purchase of potassium chloride in addition to sulfuric acid. Economics is better if the producer has its own source of KCl. The competitive position of KCl-H₂SO₄ conversion against natural production depends on location, raw material cost and value of HCl.

Product K₂SO₄ is 90-95% K₂SO₄ with 1-2% chloride and 3-4% sulfuric acid. The acid is sometimes neutralized with calcium carbonate. Creation of HCl is usually a disadvantage unless an outlet for HCl can be found. Even if an outlet can be found, the Mannheim process does not appear to be a serious competition because of the high energy requirements (.15 ton fuel oil per ton K₂SO₄). Toxicity and corrosion problems of HCl and large capital investment for each production unit are other problems.

2.2.2 Glaserite Process

Another method of K₂SO₄ production is reaction of mirabilite with KCl. This is done in two steps:



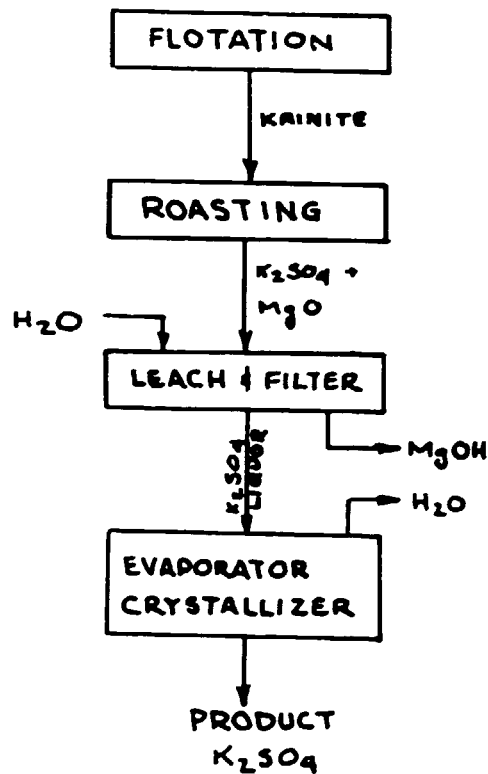
Glaserite is then dewatered and reacted with more KCl:



Work has been progressing on this project for over 20 years, but a viable process has not emerged. Most of the work has been done by the Potash Corporation of Saskatchewan. They have their own source of both KCl and Na₂SO₄. One can only estimate that they have not found an economical process. One reason may be the related inefficient recovery of only 60%.

2.2.3 Kainite Roasting

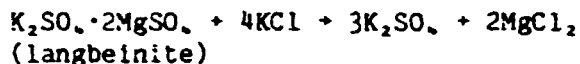
A process developed by N.L. Industries mixes KCl with Kainite followed by roasting and leaching. The process was never brought to the production stage, however. Since N.L., (now AMAX), had an abundance of kainite but still never used the process, it must not have been of enough economical value to try it. The process is patented, U.S. 3432250 by L.W. Ferris. The basic flow is shown:



The process is obviously energy intensive, high capital cost and generates HCl which must be handled and disposed.

2.2.4 Langbeinite Process

In Carlsbad, International Minerals and Chemicals Corporation (IMC) has produced K_2SO_4 from langbeinite. There are several methods of doing this but the one that seems to be the most economical is the reaction of KCl.



If a smaller amount of KCl is used, potassium magnesium sulfate can be generated.



Potassium magnesium sulfate (schoenite) is sold directly as a fertilizer. It has application in soils low in magnesium. Production has been limited to the volume of langbeinite and KCl dust generated in the respective production of SulpoMag and KCl.

2.2.5 Mixed Salts - Water Leach Process

Great Salt Lake Minerals & Chemicals Corporation uses a water leach process to produce K_2SO_4 . The basic concept of the process is to convert a mixture of magnesium, potassium, and sodium salts into Schoenite ($K_2SO_4 \cdot MgSO_4 \cdot 6H_2O$). Schoenite is then decomposed into arcanite (K_2SO_4).

A variety of different minerals can be converted to schoenite. Some of the reactions are shown below:



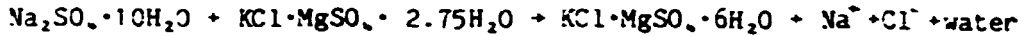
$MgSO_4 \cdot 7H_2O$, epsomite, may occur as $MgSO_4 \cdot 6H_2O$, hexahydrate, or in lower hydrated forms. $KCl \cdot MgSO_4 \cdot 2.75H_2O$, kainite, is often shown with 3 waters of hydration.



KCl may occur in the ponds as sylvinite ($KCl + NaCl$) or through decomposition of carnallite ($KCl \cdot MgCl_2 \cdot 6H_2O$) as shown below. However it can also be added from other sources in amounts needed to meet increased market demand. Adding KCl is controlled to use excess $MgSO_4$ in the system. No other chemicals are needed such as H_2SO_4 , $CaSO_4$, or other sulfate salts. Neither is any additional equipment needed. The KCl need only be added at a strategic location to maximize recovery.



In this reaction carnallite is decomposed by water to form KCl and KCl reacts with epsomite. Feed salts almost always contain halite (NaCl) and sometimes mirabilite ($\text{Na}_2\text{SO}_4 \cdot 10\text{H}_2\text{O}$). Enough water is added to remove impurities such as sodium, magnesium and chloride.



Schoenite is then converted to K_2SO_4 by the reaction with water. The basic process is a counter current flow of water with salts.

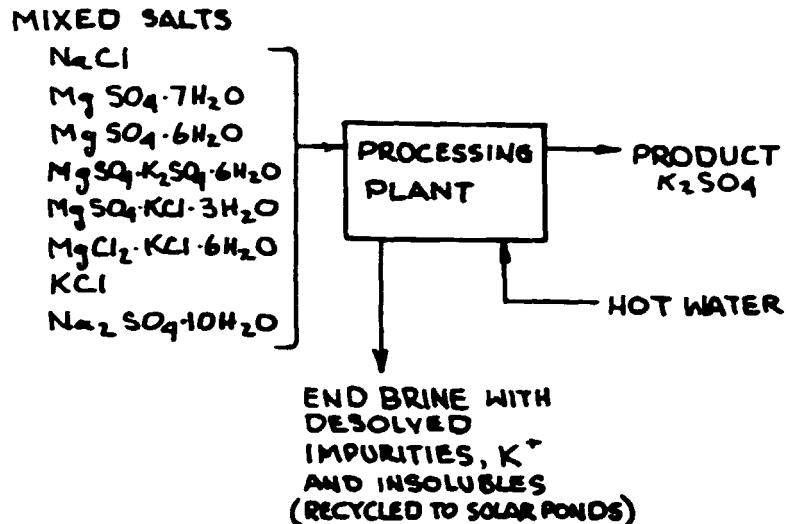
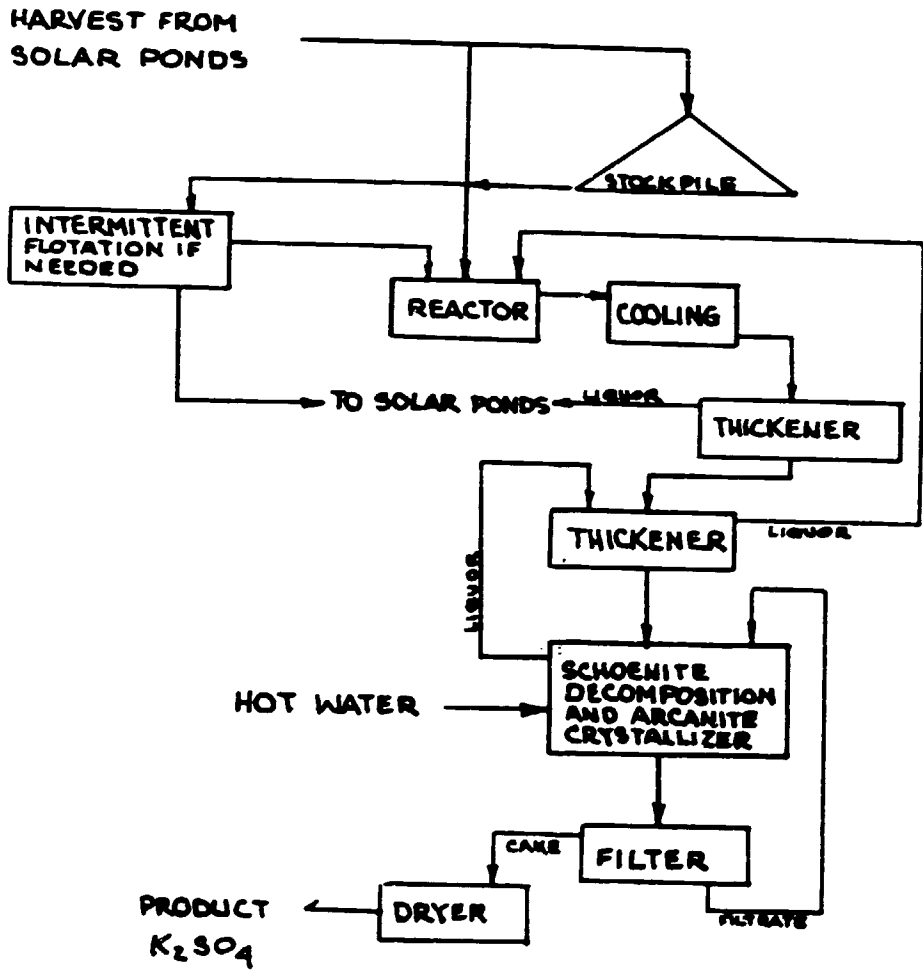


Figure 5 shows a flow chart of the process. The process is similar to the one at Pasquasia and Casteltermeni in that salts are converted to schoenite and schoenite is decomposed into K_2SO_4 .

This process has several advantages. One is that only water is added to the salt mixture. No other chemicals are used. This eliminates any ecology problems of toxic waste or expensive reagents.

It has one disadvantage in that the overall recovery is not high and this necessitates processing of the effluent brine to recover potassium. At GSL this is done with solar ponds. Effluent is flowed out into the ponds where water is evaporated and crystallized potassium salts are recovered, mixed with other harvested salts and process as already explained.

FIGURE 5
MIXED SALTS - WATER LEACH PROCESS



Occasionally salts are harvested having excess sodium chloride. The water leach process becomes less efficient with high sodium in feed salts. When this happens a side stream of salts is diverted into a flotation plant. These salts are converted to schoenite in reactor tanks and then schoenite and SO_4 salts are floated away from halite. These enriched salts are returned to the water leach plant and processed as normal.

The actual schoenite decomposition step in the crystallizer is the same as already explained and shown in Section 2.1.1.

At GSL up to 20,000 acres of solar ponds have been used to evaporate water from brines of the Great Salt Lake. Crystallized potassium salts from the solar ponds form feed stock to the plant. Plant effluent is also returned to solar ponds where all of the potassium is recovered and sent back to the plant the following year. Plant effluent is cooled before leaving the plant and some potassium is recovered in the form of schoenite.

2.2.6 Other Processes in the Mediterranean Area

GSL is familiar with operations in the Mediterranean area where research is underway to produce K_2SO_4 . Tekel at the Camalti works in Turkey has already expanded its pond system and facilities to produce higher grade salt. They wish to produce K_2SO_4 as a by-product. In Egypt, at El Max Salines in Alexandria, evaluations of K_2SO_4 are underway, and in Tunisia, at Zarzis, a pilot plant has been operated.

Israel has been involved in research to produce K_2SO_4 . The Arab Potash Company is also thinking of developing a chemical complex at their Dead Sea operation. Their plans include K_2SO_4 production.

Many have been interested in producing K_2SO_4 from ocean brines as a by-product from salt operations. This has been studied extensively, but to date no viable operation is now working. Several million of dollars were expended in research at Exportadora del Sal in Baja California to make K_2SO_4 . The project was abandoned in 1976.

These studies and expenditures have not resulted in a single K_2SO_4 production facility and indicate that competition from these sources is not going to be a problem in the near future.

Possible future production of K_2SO_4 in Tunisia does not appear to be of serious consequence or a competitive threat in the Mediterranean. The plan for commercial operation has not been completed. If a plant is built, it would take five years from now to bring it to steady state production. The actual production is energy intensive and has several process steps that will make production costs high.

El Max Salines in Alexandria is quite serious about producing K_2SO_4 . they have a unique operation but they are still in a pre-feasibility stage. GSL estimates that they will have high production costs if they decide to produce SOP. They also have a small reserve and at

best they could not produce over 40,000 ton per year. Life of these reserves is only 10 years. Egypt will likely remain an importer of K_2SO_4 even if they do produce SOP because they are projecting uses of 100,000 ton per year in 1990. Presently all K_2SO_4 used by Egypt is imported.

The same is true for all Middle East and Mediterranean countries. Even if they produce their own K_2SO_4 , they will likely consume more than they make and the projected consumption in the 1990's is increasing.

2.2.7 Salar de Atacama

The Salar de Atacama in Chili has a large reserve of potash. This reserve has not been exploited except for lithium. Some attention is now being given to produce KCl, K_2SO_4 , and boric acid. Amax Corporation has been investigating production of these salts.

The natural brines at the Salar are low in sulfate. Chloride is the controlling cation, but some K_2SO_4 can also be made. Costs will be high since the Salar is in a remote area without any infrastructure and 150 km from the sea. It will be many years before it will come on stream as a potash producer and when it does, it should not offer competition in the Mediterranean area.

2.2.8 China

China is scheduled to increase their production facility of KCl by an additional 200,000 ton in 1989. This production will come from the Qinghai Province. There are no sulfate in the brine at Qinghai. In 1995 they plan to increase production to one million ton and produce some K_2SO_4 . this SOP must be produced with acid or gypsum. In any case, there will be little if any competition from the Chinese. Their source of potash is over 1,000 km from sea ports, production of sulfate of potash will be high and China will likely use all it makes.

APPENDIX TWO

LIST OF EVAPORITE MINERALS AND NOMENCLATURE

MARINE EVAPORITE MINERALS

<u>COMMON NAME</u>	<u>FORMULA</u>	<u>MOLECULAR WEIGHT</u>	<u>% K</u>	<u>% Na</u>	<u>% Mg</u>	<u>% Ca</u>	<u>% Cl</u>	<u>% SO₄</u>	<u>% H₂O</u>
Anhydrite	CaSO ₄	136.14				29.44		70.56	
Arcanite (Sulfate of Potash)	K ₂ SO ₄	174.25	44.88					55.12	
Astrakanite (Bloodite)	Na ₂ SO ₄ ·MgSO ₄ ·4H ₂ O	334.46		13.75	7.27			57.44	21.56
Bischofite	MgCl ₂ ·6H ₂ O	203.30			11.95		34.88		53.17
Calcium Chloride	CaCl ₂	110.99				36.11	63.89		
Carnallite	KCl·MgCl ₂ ·6H ₂ O	277.85	14.07		8.75		38.28		38.90
Epsomite	MgSO ₄ ·7H ₂ O	246.47			9.86			38.97	51.17
Glaserite (Aphthitalite)	3K ₂ SO ₄ ·Na ₂ SO ₄	664.80	35.29	6.92				57.79	
Glauber's Salt	Na ₂ SO ₄ ·10H ₂ O	322.19		14.27				29.81	55.92
Halite	NaCl	58.44		39.34			60.66		
Hexahydrate	MgSO ₄ ·6H ₂ O	228.45			10.64			42.05	47.31
Kainite	KCl·MgSO ₄ ·3H ₂ O	248.96	15.71		9.76		14.24	38.58	21.71
Kieserite	MgSO ₄ ·H ₂ O	138.38			17.56			69.42	13.02
Langbeinite	K ₂ SO ₄ ·2MgSO ₄	414.98	18.84		11.72			69.44	
Leonite	K ₂ SO ₄ ·MgSO ₄ ·4H ₂ O	366.68	21.33		6.63			52.39	19.65
Loeweite	Na ₂ SO ₄ ·MgSO ₄ ·2.5H ₂ O	307.44		14.95	7.91			62.49	14.65
Magnesium Chloride	MgCl ₂	95.21			25.53		74.47		
Magnesium Sulfate	MgSO ₄	120.35			20.19			79.81	
Polyhalite	K ₂ SO ₄ ·MgSO ₄ ·2CaSO ₄ ·2H ₂ O	602.92	12.97		4.03	13.29		61.73	5.98
Salt Cake (Thenardite)	Na ₂ SO ₄	142.04		32.37				67.63	
Schoenite (Picromerite)	K ₂ SO ₄ ·MgSO ₄ ·6H ₂ O	402.71	19.42		6.04			47.70	26.84
Sylvite (Muriate of Potash)	KCl	74.55	52.44				47.56		
Syngenite	K ₂ SO ₄ ·CaSO ₄ ·H ₂ O	328.41	23.81			12.20		58.50	5.49
Vanthoffite	3Na ₂ SO ₄ ·MgSO ₄	546.47		25.24	4.45			70.31	

Atomic Weights*

K	39.0983
Na	22.98977
Mg	24.305
Ca	40.08
Cl	35.453
S	32.06
O	15.9994
H	1.0079

*Based on Sargent-Welch periodic chart - 1979

Molecular Weights

H ₂ O	18.0152
SO ₄	96.0576

NOMENCLATURE

- Activator A chemical added to a flotation circuit that aids the collector in adhering to the mineral face.
- Activity Coefficient A factor used to convert concentration to activity to account for non-ideal solution behavior.
- Ax bar A bar with an ax head welded on the end of it for cleaning salt crystals off of weir logs. (See Figure A-1)
- Backhoe Heavy equipment with a bucket on an arm for digging (See Figure A-2)
- Belly Dump Truck A tractor trailer rig where the trailer is enclosed on all four sides and has gates on the bottom of the trailer for unloading (See Figure A-3)
- Cleaner cells Flotation cells to refloat froth concentrate from initial flotation cells. Generally used to enhance rejection of undesirable contaminants.
- Collector The primary reagent in a flotation circuit. Its usual function is to selectively coat the mineral to be floated with an organic film.
- Common Ion Effect Salt A and B are different salts with a common ion. If Salt A is added to a saturated solution of Salt B, Salt B will precipitate to maintain equilibrium.
- Concentrate The final product of a flotation circuit.
- Conditioning of floors The process of flooding a new pond with brine to displace all the subsurface waters in the pond with brine.
- Conversion The conversion of a salt, or a mixture of salts to a new mineralogy by reaction with a new brine. Often this entails temperature control to enhance the process.
- Counter-current Decantation A series of steps where a solid and liquid are mixed and then separated before the next mixing step. The solid and liquid move in opposite directions through the series of steps.
- Cut-off Point A term used in any operation to denote a point at which an operation is no longer viable.
- Defrother A chemical used to eliminate air bubbles from a process stream.
- Depressant A chemical added to a flotation circuit that suppresses the flotation of undesirable minerals.
- Dike A wall of earth that encloses a body of water or brine (See Figure A-4)
- Dispersant A chemical added to any circuit that causes fine particles to stay suspended in the liquor.
- Dozer A piece of heavy equipment that moves on tracks and has a vertical blade mounted on front for pushing material (See Figure A-5).

- Dragline A piece of equipment used to build dikes and canals.
(See Figure A-9)
- Dry Diagram A phase diagram that does not show the water content on one of the axes.
- Drying Up Point The concentration of a brine at the point the pond dries up.
- Efficiency A measurement of the effectiveness of an operation. Different from recovery in that it measures variation from theoretical recovery.
- Encapsulation The trapping of brine or impurities within a single salt crystal.
- End Dump Truck (10 Wheeler) A truck with the bed enclosed by four walls and the bed can be tipped to unload through a swing tail gate (See Figure A-6)
- Entrainment Brine trapped in the voids between salt crystals.
- Entrainment Factor The ratio of weight of brine to the weight of dry salt in a wet salt.
- Equilibrium A state where there is no further change in the system after time.
- Equilibrium constant (Solubility product) A salt has the chemical formula $a_x b_y$. The equilibrium constant for this salt in solution is the product $a^x b^y$.
- Evaporation The loss of water from a water or brine surface, usually measured in inches per day.
- Evaporation Path A plot of one brine component relative to another component to show how the concentration of the single component changes as the brine concentrates from evaporation.
- Evaporite A mineral produced by evaporation of a brine.
- Extraneous Water Water added to a process from unmetered or unmonitored sources such as pipe flushing.
- Flocculent A chemical added to any system that enhances settling of suspended solids.
- Front end Loader A piece of heavy equipment with a wide bucket on the front for scooping and loading material (Refer to Figure A-7)
- Froth Paddles Devices used in flotation to speed the flow of the froth from the flotation cells.
- Froth Texture The physical texture of a flotation froth.
- Frother A chemical added to a flotation circuit to aid recovery by helping to establish a good, workable froth.
- Harvester Heavy equipment that is used to recover a salt from solar ponds (See Figure A-8).
- Harvest-to-product ratio(H/P) The ratio of total feed tons to the product tons.

- Heat of Crystallization The energy released when a salt crystallizes.
- Insols Particles that are insoluble in water or the dissolving medium.
- Interstitial Having to do with the voids between salt crystals in a deposit.
- Inverse Lever Law When two solutions represented by two points on a phase diagram are mixed, the resulting solution lies on the line between the two points. The ratio of the lengths of the two segments is proportional to the ratio the amounts of each solution that were mixed.
- Ion Exchange The exchange of ions in the brine with ions in subsurface brines and clays of the pond floor.
- Ionic Concentration The total moles of ions in solution on a mono-valent basis per 1000 moles of water.
- Janecke Phase Diagram A square shaped plot of equilibrium brine concentrations with reciprocal salt pairs at the ends of the diagonals.
- Leakage Brine loss through porous pond floors and dikes, usually measured in inches per day.
- Level Control A term used in a wide variety of operations to describe control of any vessel to exact levels to aid in controlling a process.
- Mix Rule A line drawn between two points on a phase diagram represents the mixing of the two solutions represented by those points.
- Mother Liquor The brine from which a particular salt was precipitated from.
- Pan A metal evaporation pan used to measure evaporation rates (See Figure A-1').
- Phase A part of a system that is uniform throughout in chemical composition and physical properties.
- Phase Rule (Gibbs) For systems in which pressure, temperature and concentration are the only variables, the number of degrees of freedom equals the number of components minus the number of phases plus two.
- Pond A body of brine enclosed by dikes.
- Quadruple Point The point on a phase diagram where four different salts are in equilibrium with a solution.
- Reciprocal Salt Pair Two salts that have common anions (negative charged ions)
- Recovery The percentage of the total amount of a desired material fed through a process that is recovered as product.
- Regression A mathematical technique used to develop a relationship between experimental variables. Functions thus developed are called regression lines and are thought to represent the best fit of the experimental data.

Retention Time The time a process element will spend in a vessel or the volume of the vessel divided by the process stream flow rate.

Road Grader (Patrol, 16 Patrol) heavy equipment with a vertical blade between the front and rear wheels for leveling or piling up a windrow (See Figure A-10).

Rougher cells Primary flotation cells.

Salt 1. NaCl (Halite) or 2. Any evaporite mineral.

Saturated Solution A solution that has the maximum concentration of a specified component.

Scavenger cells Secondary flotation cells.

Scraper A self-loading piece of equipment used to transport material (See Figure A-11).

Settling Rate The rate at which solids will settle through a liquid.

Slimes Extremely fine insoluble material found in many processes, typically clays and shales.

Slurry The suspension of solids in liquid.

Soaking When ponds are flooded with brine, the surface and subsurface water will mix or exchange with the brine. A dry soil will soak up the brine until it is saturated.

Soils Index Number A measure of soil permeability.

Stacker An inclined conveyor belt on wheels used to stockpile salt (See Figure A-12).

Stoichiometric The conservation of atoms in a chemical reaction.

Tailings Material rejected by a flotation circuit.

Tipple A drive-over structure where belly dump trucks can unload (See Figure A-13).

Triangular Phase Diagram A triangular shaped plot of equilibrium brine concentrations for a 3 component system.

Triple Point The point on a phase diagram where three different salts are in equilibrium with a solution.

Tyler Mesh The number of openings per linear inch of screen.

Wear Any loss of metal or other materials to the combined effects of corrosion and abrasion.

Weir A wood structure that holds back brine or regulates the flow of brine over the structure. The structure is slotted so 4 inch by 4 inch wood logs can be added to or taken from the weir to raise or lower the pond level. (See Figure A-14).

Wet Diagram

A phase diagram that has water content indicated on one of the axes.

Windrow

A long, uniform pile of material.

APPENDIX THREE
HOW TO BRAINSTORM

BRAINSTORMING

Brainstorming is a method of group thinking that produces many ideas fast. Such ideas are needed in overall solar pond design because there are so many variables and alternatives in solar pond layout, operation and design.

Brainstorming is ineffective if done improperly. Care should be taken when people get together for a "Brainstorming Session". Each brainstorming session should be organized with a Chairman, Recorder and participants. The session should brainstorm one subject at a time and each session must have the following rules.

1. No criticism. The session is open to ideas. Each idea is listed on a blackboard or written on a paper. Beware of killer phrases such as "It won't work"; "We don't have time"; "We've tried that"; "We've never done it that way before".
2. No judging. A permissive atmosphere must exist. All ideas are accepted without any judgement. This allows for complete thinking and allows for the bad ideas to be mentioned and recorded. Often, the bad ideas turn out to be the best ones.
3. Quantity. The more people, the better. The greater the number of ideas, the greater the the probability of good ones.
4. Evaluation. After all of the ideas are listed, they must be evaluated. Related ideas are combined. The validity of the ideas are then proven and the poor ideas are eliminated. Often the evaluation is done with all participants remaining, but many times it is done with only the key project engineer who may call in others later to help evaluate the ideas.
5. Processing. Once the better ideas are chosen, they must be developed or processed into a design.

The chairman see that the rules are followed. No criticism and no judging will be permitted until the evaluation and processing step is reached.

Brainstorming is an effective engineering tool, especially in various phases of solar pond design and problem solving.

APPENDIX FOUR

PAPER ON MAGNESIUM COMPOUNDS

724 MAGNESIUM COMPOUNDS

MAGNESIUM NITRIDE. Magnesium nitride, Mg_3N_2 , is a white powder which crystallizes from saturated solutions in the form of the three hydrates, $Mg_3(NH_4)OH_6$ (± 21.15 to $10.5^\circ C$), $Mg_3(NH_4)_2OH_4$ (10.5 to $29.5^\circ C$), and $Mg_3(NH_4)_3OH_2$ (above $29.5^\circ C$). The solubility is 51.58 g $Mg_3(NH_4)_3OH_2$ per 100 g water at $29.5^\circ C$; 38.0 g at $10.5^\circ C$; and 21.2 g at $-21.15^\circ C$. The solution as well as the crystallized hydrates decompose readily on heating, with evolution of nitrogen oxide. The hydrates can be prepared by dissolving magnesium amide in nitrous acid (obtained by absorption of nitrogen sesquioxide N_2O_3 in ice water) at a temperature below $-5^\circ C$. The solution is evaporated under vacuum within the desired temperature range. An alcohol solution of $Mg_3(NH_4)_3OH_2$ can be prepared by adding alcohol to a stoichiometric mixture of finely pulverized $MgSO_4 \cdot 7H_2O$ and sodium nitrite, and stirring and filtering. The hydrated salts are deliquescent and decompose even on standing in closed containers.

Magnesium nitride is formed when nitrogen oxides are absorbed by solid $Mg(OH)_2$ at $25-35^\circ C$. (1) Magnesium nitrate is formed at the same time and the salts are separated from $Mg(OH)_2$ by aqueous leaching. Although it has been tested as an additive to reduce the corrosion rate of passive concrete reinforcements (2), it has little industrial importance.

Bibliography for Magnesium Nitride

1. F. S. Dorn, *Tr. Amer. Chem. Soc.*, **101**, 37 (1901).
2. G. I. Tsvetkov, S. G. Tsvetkova, and V. B. Il'inski, *Zh. Fiz. Khim.*, **35**, 124 (1961).

MAGNESIUM OXIDE AND HYDROXIDE. Magnesium oxide (magnesia), MgO , occurs indefinitely in nature as the mineral periclase. Magnesium oxide is also the end product of the thermal decomposition of numerous magnesium compounds. Physical properties of purified magnesium oxide are listed in Table 1.

Table 1. Physical Properties of Magnesium Oxide

Property	Value
crystal form	trigonal
lattice parameter, \AA	$a = 4.20$
color	colorless
index of refraction	1.716
density, g/cm ³ (25°C)	3.28
hardness, Mohs	5.5 to 6.0
melting point, $^\circ C$	2800
boiling point, $^\circ C$	est. 3600
thermal expansion coefficient, $10^{-6}/^\circ C$	10.66
electrical resistivity, ohm-cm at 25°C	2×10^{10}
at 100°C	3×10^{10}
at 200°C	4×10^{10}
at 300°C	5×10^{10}
heat of fusion at 2810°C, cal/mole	15,300
heat capacity at 25°C, cal/mol-deg (mole)	10.86 (10 cal/mol-deg)
at 100°C	Temp. range 251-261.7°C
at 200°C	10.662
solubility in water, g/100 ml	0.0002

The physical properties of commercial magnesium oxides vary greatly with the nature of the initial material, time and temperature of decomposition, and trace impurities. Many commercial oxides show surprisingly stable pseudocrystal structures derived from the starting materials, although all primary particles have an face-crystal structure. The specific gravity of magnesium oxide obtained by crystallization after fusion is in fair agreement with the value of 3.58 calculated from x-ray data. However, specific gravity determinations on MgO obtained by calcination of precipitated $Mg(OH)_2$ at different temperatures have yielded the following figures:

temperature, $^\circ C$	600	710	850	1000	1200	1400	1500
specific gravity	2.91	3.04	3.22	3.39	3.48	3.52	3.56

The elemental properties of magnesium oxide vary considerably with the temperature and time of calcination of the initial material. The increase in density resulting from increasing calcination temperature is paralleled by a decrease in reactivity. MgO prepared in the temperature range from 100 to 1000°C (from magnesium hydroxide or basic magnesium carbonate) is readily soluble in dilute acids and hydrates rapidly even in cold water.

Fused magnesium oxides are virtually insoluble in concentrated acids and are indifferent to water unless very finely pulverized. The oxides prepared below 1000°C, which are easily hydrated with water, are known as *calcined-burned magnesia*. The unreactive magnesia, prepared at higher temperatures, are called *dead-burned or water magnesia*. The hydration rate of various magnesium oxides is determined by the active surface area, and may vary from a few hours in the case of the reactive oxides obtained at low temperatures to months or even years for the dead-burned grades. The heat of formation of MgO is 143.81 kcal/mole at $25^\circ C$. The highly reflective power of magnesium oxide in the visible spectrum has led to its use as a white color standard. Magnesium oxide is a poor electric conductor at low temperatures, but conductivity increases rapidly with rising temperature (see Table 1).

The hydration of reactive grades of magnesium oxide leads to the formation of **magnesium hydroxide**, $Mg(OH)_2$. The physical properties of purified magnesium hydroxide are given in Table 2. Magnesium hydroxide crystallizes in the form of

Table 2. Physical Properties of Magnesium Hydroxide

Property	Value
crystal form	trigonal
lattice parameter, \AA	$a = 3.11$
color	colorless
index of refraction	1.596, 1.560
density	2.36
hardness, Mohs	2.8
melting point, $^\circ C$	decomp. 3470
solubility in water g/100 ml (10°C)	0.0000
at 100°C	0.0004

microal hexagonal plates. Even the apparent relations magnesium hydroxide obtained by precipitation from magnesium salt solutions with alkalis show the same x-ray diffraction pattern as the coarse crystalline variety.

Thermal decomposition of magnesium hydroxide begins above 350°C, although much higher temperatures are required to remove the last traces of water. Both magnesium oxide and hydroxide absorb moisture and carbon dioxide from the air. Reactive grades of MgO and Mg(OH)₂ are gradually converted into the basic carbonate, 3MgO · 2H₂O, which is sufficiently hygroscopic to the atmosphere.

Magnesium hydroxide is found in nature, as the mineral brucite, usually together with magnesite (MgCO₃) of which it is a hydration product, or in the form of neohydrins in deposits of serpentine (3MgO · 2SiO₂ · 2H₂O), magnesite (MgCO₃), or dolomite (CaCO₃ · MgCO₃).

Manufacture

Magnesium oxide is produced by calcination of magnesium carbonates or magnesium hydroxide. It can also be produced economically by decomposition of magnesium chloride or magnesium sulfate. Magnesium oxide is produced in a number of different grades designed for various special uses. Dead-burned magnesite or magnesite is a dense highly refractory product used almost exclusively in the manufacture of basic refractory bricks. Pure magnesium oxide has a softening temperature of about 2800°C. The use of additives, such as alumina, silica, calcium oxide, or equivalent iron oxides, lowers the softening temperature considerably (1-3). Most natural magnesites contain sufficient quantities of impurities to yield a dead-burned or fluxed product at calcining temperatures of about 1400°C. Relatively pure grades of magnesium hydroxide obtained by precipitation from seawater require the addition of ferric oxide (in amounts of from 2 to 7%) or of other additives in order to permit fluxing and recrystallization at the maximum temperatures of an air- or gas-fired rotary kiln (100°C).

The rotary kiln used in calcining magnesite and dolomite to produce refractory grade products are large kilns ranging in size of 6 to 11 ft in diam and up to 400 ft in length. The kilns are lined with magnesite or magnesite-chrome brick. The conditions of the calcination process can be closely controlled in these kilns by adjustments in the speed of rotation, inclination of the tube, and feed rate. Thermal efficiency can be increased by preheating the feed material with the exhaust gases. The kilns are counter-current and the maximum temperature is reached near the discharge end. If the stack gases contain entrained particles of feed material the gas is air-quenched to about 300°C, and the entrained dust is removed by electrostatic precipitators (1).

The recovered dust can be sold for soil conditioner or for various fillers. Certain grades of magnesite are produced by calcining magnesite, dolomite, or magnesium hydroxide at temperatures lower than 1000°C. The calcine-burned materials are reactive and can be used for the preparation of magnesium chloride (by chlorination in the presence of carbon), oxychloride cements, desulfurizing agents, and other processes requiring a reactive magnesium.

Temperatures required for rapid decomposition of magnesite are between 600 and 700°C. Dolomite decomposes rapidly at temperatures between 700 and 800°C. Some dolomites behave like mechanical mixtures of magnesite and calcite with a very sharp and extended break in the decomposition curve, while others behave like true double compounds, have a far less pronounced break in the decomposition curve, and cover only a narrow range of temperature. Strips of decomposition of dolomites, especially the best type, makes possible a "selective calcination" in which only the

unintended carbonate is decomposed to oxide and the calcium carbonate is virtually untouched. Optimum conditions for selective calcination have to be determined for each type of dolomite. Generally, a maximum temperature of 800°C is adequate for decomposition of nearly all of the magnesium carbonate. (Type calcium carbonate begins decomposition at 825°C and pure magnesium carbonate begins to decompose at 320°C.) In some cases, subsidiary separation of the two components of the partially or selectively calcined dolomites can be made by mechanical means, such as screening, air separation, or hydraulic classification. Industrially sized rotary kilns are not satisfactory for closely controlled calcinations at low temperatures as the surface temperatures reached in the firing zone exceed 1000°C, the temperature at which CaCO₃ begins to decompose. Externally heated rotary kilns or air-heating furnaces can be used.

Magnesium oxide can be produced from magnesium chloride or sulfate with simultaneous recovery of the acid components. Magnesium chloride can be completely decomposed in a temperature range between 1400 and 1700°C. Magnesium sulfate is generally decomposed in a reducing atmosphere such as S, H₂, H₂, or CO. Magnesium sulfite decomposes at a temperature from 1100 to 1300°C. A process to recover MgO and HCl from pitch waste briques was used from 1933 to 1961 by International Minerals & Chemical Corporation at their Coal-bowl, New Mexico, plant (4,5). The products of the process were industrial refractory and electrical refractory grades of magnesite, and 37% hydrochloric acid. The use of pitch waste briques to prepare MgO, 6H₂O flake to be used in the decomposition step requires an initial step to remove the bulk of the K, Na, and SO₄ ions. The step used at Coal-bowl was a precipitation of KCl, NaCl, and KCl · MgSO₄ · 6H₂O (kanite) from the liquor by a simple evaporation and recycling process. Another purification process, which was patented, but not used at Coal-bowl, was the removal of sulfates by precipitation as gypsum by the addition of calcium chloride solution to the feed liquor (6). The relatively pure MgO solution was concentrated to 10.5% MgO in boiling kettles (final temperature 182°C). The MgO, 6H₂O was then flaked to MgO, 6H₂O by cooling on rotary drum flakers. The MgO, 6H₂O was partially dehydrated in a Rotoc-Zenve drier at a final temperature of about 150°C. The product from this drier contained 62.6% MgO. Decomposition to MgO and HCl occurred in a standard 7 × 70 ft rotary kiln.

The final temperature in the decomposition kiln was about 740°C. The solids discharged from the decomposition kiln contained about 87% MgO, 12% MgSO₄, 2.5% NaCl, 2.5% KCl, and 0-2.5% residual MgO. A peculiar characteristic of the magnesium oxide obtained in the decomposition step was the lack of chemical reactivity compared to products obtained by calcination of magnesium hydroxide or carbonate. This was true in spite of the low decomposition temperature (510-500°C). Physically, the product showed no significant change when heated in the temperature range between 510 and 1050°C. The residual impurities, NaCl, KCl, and MgSO₄, were removed and a synthetic process was found by mixing the impure MgO from the decomposition kiln with carbonaceous material (carbon black or fuel oil) in a ball mill and firing the mixture at a temperature of about 1620°C. Virtually no decomposition or sintering of the formed pellets occurred in the flame zone of the high-temperature furnace kiln unless fairly large quantities of other refractory oxides were added to the kiln feed. The impurities were removed in the high temperature kiln by volatilization of the chlorides and decomposition of the sulfate compounds (7).

The Aluminum Company of Canada has developed a process (8) in which magne-

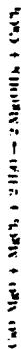
728 MAGNESIUM COMPOUNDS

esium oxide may be recovered from ground dolomite or ferrous ores. The ground ore is leached with a mixture of carbon dioxide and sulfur dioxide.

The addition of CaCl_2 to the leaching step improves the leaching reaction rate, improves the recovery of MgO from 55% to more than 92%, and keeps the pH of the solution of calcium to less than 3.7 in the magnesium solution. The resulting magnesium basicity solution can be treated by precipitation and calcining to recover magnesium oxide.

Highly reactive grades of magnesium oxide used in the rubber and pharmaceutical industries are prepared from basic magnesium carbonate or magnesium hydroxide in small, externally heated rotary kilns. The feed and temperature conditions are controlled to produce a magnesium oxide containing between 5 and 15% residual moisture and carbon dioxide.

Magnesium hydroxide can be produced by precipitation from solutions of magnesium salts or by slaking a reactive magnesium oxide. The most important commercial method is the precipitation of Mg(OH)_2 from seawater and brines (2). In the earlier attempts to produce Mg(OH)_2 directly from seawater, charred lime was used as a precipitant, but it was soon recognized that equally satisfactory products could be obtained by precipitating with much more concentrated lime slurries or even dry pulverized lime or calcined dolomite. Calcined dolomite reacts with the MgCl_2 in seawater as:



thus increasing the yield of magnesium hydroxide from a given volume of seawater or brine.

Seawater and brines contain certain amounts of dissolved and suspended solid impurities. These impurities must be removed by a pretreatment (2). The removal of impurities is accomplished by precipitating a portion of the magnesium content used in the raw feed solution with calcium oxide or hydroxide. This pre-precipitate settles in thickers, calcium carbonate, silica, ferric oxide, and other impurities and is removed as a sludge after sedimentation in a thickener. The main precipitation is then accomplished by mixing the charred lime or seawater with the calculated amount of calcium hydroxide and concentrating the precipitated magnesium hydroxide in large settling tanks or thickeners. The low concentration of magnesium in seawater (about 2.2 g MgO liter) requires that very large volumes of liquid be processed; therefore, the thickening equipment is very large. Thickeners with diameters on the order of 220 ft are used in modern plants. The concentrated slurry underflow from the thickeners contains about 10-15% magnesium hydroxide. The removal of residual soluble impurities is accomplished by countercurrent washing with fresh water in thickeners as large as the original sedimentation tanks. The purified underflow from the wash step is filtered on large (14 ft diam X 18 ft long) rotary vacuum filters. The filter cake is from 25 to 50% Mg(OH)_2 . Kaiser Refractories sells a small portion of the filter cake to the paper industry (2). The filter cake can be dried or calcined directly. A pharmaceutical grade of Mg(OH)_2 can be obtained by spray-drying the washed slurry.

The precipitation of Mg(OH)_2 from seawater using calcium carbonate (CaCO_3) has been studied (9). Acetylene is produced by this method according to the reaction:



One of the major problems in the precipitation of magnesium hydroxide from seawater or brines on a large scale has been the low settling and filtration rate of the product. Extensive development work has been done for the purpose of obtaining more rapidly settling and more readily filterable precipitates. A quicker settling and coarser filtering precipitate reduces capital expenditure and operating costs. A reduction in the reactivity of the precipitant (lime or calcium hydroxide) by control of the slaking conditions and burning temperatures or by the addition of unslaked lime or dolomite to the cold brine, generally results in the formation of precipitates with better settling characteristics (10,11). Introduction of a portion of the precipitated slurry into the precipitation zone (12) or the continuous addition of flocculating agents also improves settling rates of the magnesium hydroxide. The addition of small amounts of additives to the brine has been found useful to give a better settling precipitate (13). In most cases the improvement in the settling characteristics takes place at the expense of purity of the final product, because of contamination with adsorbed flocculants or occlusion of residual impurities.

A method to produce more readily filterable magnesium hydroxide by precipitation with an excess of Ca(OH)_2 present for at least 2 hr at a temperature of 40-80°C has been patented (14). In this process water washing of the filter cake produces a magnesium hydroxide of high bulk density and high purity.

Economic Aspects; Specifications; Analysis

The U.S. production figures for magnesium and magnesium hydroxide for 1959 and 1963 are given in Table 3 (15).

Table 3. U.S. Production of Magnesium and Magnesium Hydroxide for 1959, 1963, Short Tons

	1959	1960	1963	1963
magnesium				
metal-lumped	51,093	46,057	50,072	51,849
refined	517,041	505,011	506,908	575,723
desalinated dolomite	1,087,707	1,049,260	1,092,750	1,857,438
special magnesium				1,949,053
100% MgO base				
extra light and light	1,833	2,429	2,353	2,400
heavy	20,133	21,765	22,963	17,400
magnesium hydroxide				
100% and technical				
100% Mg(OH)_2 base	208,406	309,015	382,100	357,597
				430,840

The prices quoted in February 1964 for various grades of magnesium were (16): calcined, technical, medium light bags, freight equated, 25.75 to 26.54/1b; technical, synthetic, rubber grade, light bags, carload lots, freight equated, 28.75 to 30.00/1b; calcined technical, synthetic, rubber grade, extra light bags, carload lots 28.50/1b; calcined, technical, heavy, foil laminar, Nevada, carload lots in bags, 553-short tons for 100%; 520-short tons for 95%, and 501-short tons for 95%; 100% XVII light bags, 39.50/1b and 100% XVII heavy bags, 40.00/1b. The price quoted for NF XI processed magnesium hydroxide in drums, 500 lb of net, fish works, was 24.5 to 25.50/1b.

The analytical methods used for magnesium oxides are generally the same as those listed for magnesium carbonates. The specifications for USP grades of magne-

7. U.S. Pat. 2,504,373 (August 27, 1951); W. B. Dancy, in *International Minerals and Chemical Corp.*
8. *Chem. Week* 90, No. 26, 40 (June 30, 1952)
9. S. Takahashi, T. Hatake, and F. Okada, *Daikin Kagaku Kagaku Kenkyu Hokoku* 11, 123 (1953); *Ultrahigh Purity Chem. Ind.* 64, 107 (1956)
10. U.S. Pat. 2,124,002 (July 10, 1938); A. G. MacIntyre, Westway Chemical Specialties Corp.
11. U.S. Pat. 2,191,500 (Feb. 27, 1949); W. H. J. van der Hoff, C. H. Martin (to Morton Salt Co.)
12. U.S. Pat. 2,405,655 (July 30, 1949); H. A. Robinson, H. L. Frensdorff, and H. S. Spencer (to Dow Chemical Co.)
13. *Chem. Rev.* 60, 443 (June 18, 1945); Kahlert-Schlag, *Verst. Abt. Chem. U.S.A.*
14. U.S. Pat. 3,080,215 (March 19, 1963); W. Alden and J. Bryant (to Dow Chemical Co.)
15. *Materials Handbook*, U.S. Dept. of Interior, Bureau of Mines, U.S. Govt. Printing Office, Washington, D.C., 1959, 1962
16. *Oil, Paint and Varnish* 100 (Feb. 28, 1960)

MAGNESIUM PHOSPHATE. See Phosphoric acid and phosphates.

MAGNESIUM SULFATE. Magnesium sulfate, MgSO₄, cannot be obtained from solution, but only from dehydration of one of the hydrates. The best known hydrates of MgSO₄ are the monohydrate, MgSO₄ · H₂O, which occurs in nature as the mineral kieserite, and the heptahydrate, MgSO₄ · 7H₂O (epsom salt), which occurs in nature as the mineral epsomite. Physical properties of anhydrous magnesium sulfate and the monom and heptahydrates are listed in Table I.

Table I. Physical Properties of Magnesium Sulfate and the Monom and Heptahydrates

Property	Anhydrous magnesium sulfate	Monohydrated magnesium sulfate	Heptahydrated magnesium sulfate
crystal form	orthorhombic	orthorhombic	rhombic (monoclinic)
color	colorless	colorless	colorless
index of refraction	1.52, 1.515, 1.50	1.53, 1.515, 1.50	1.435, 1.455, 1.461
density	2.66	2.47 (2.57)	1.99 (1.86)
melting point, °C	1124 (decomp)	1124 (decomp)	67.5 (at 1 atm)
boiling point, °C	decomp	decomp	712 (at 2 atm)
hardness, Mohs	3.0-3.5	3.0-3.5	2.0-2.5
heat of fusion, cal/mole	3340 at 1127°C		
heat capacity, cal/mole (mole)	26.7 (280-327°K)	1.52 (°K)	90 (200-310°K)
solubility in water, g/100 ml H ₂ O	599, 715 ⁰⁰	68, 1 ⁰⁰	71 ⁰⁰ , 101 ⁰⁰

Magnesium sulfate heptahydrate exists in a stable rhombic (D), and in an unstable monoclinic (D) form. The rhombic form is the stable phase in aqueous solutions at normal temperatures. The unstable monoclinic form crystallizes below 21°C under certain conditions.

Solubility relations in the MgSO₄ · H₂O system are very complex due to numerous metastable phases and slow equilibrium adjustments. Van't Hoff (1) and D'Ans (2) have compiled the most reliable data. The various hydrates of magnesium sulfate tend to form supersaturated solutions with metastable solid phases and several hydrates may coexist in apparent equilibrium with the aqueous solution at various temperatures. Numerous old references are without value, particularly those that do not

include a maximum of 1.5% calcium oxide (40% less on ignition, 2% alkali and soluble salts, 0.1% acid insoluble substances, 0.05% iron, 0.001% heavy metals, and 0.0012% arsenic. Specifications of refractory-grade magnesia made by different U.S. producers vary but a typical analysis is MgO, 98.5%; SiO₂, 0.4%; Al₂O₃, 0.2%; CaO, 1.0%; Fe₂O₃, 0.25%; and bulk density 100 lb./ft.³. The USP assay method is based on the solution of an ignited sample of magnesium oxide in 1N sulfuric acid and back titration with 1N sodium hydroxide. This value is corrected for CaO, which is not removed separately by the oxalate method. When larger amounts of impurities are present, an accurate determination of SiO₂ (by evaporation with hydrochloric acid and redissolution with hydrofluoric acid), Fe₂O₃, and Al₂O₃ (as hydroxides with ammonia, double precipitation) and of SO₃ (as BaSO₄) is necessary, with precipitation of the magnesium as Mg(OH)₂ and subsequent ignition.

Uses

The most important applications of magnesium oxide are in the manufacture of refractories, magnesium metal, and oxyacetylene reagents. Impure grades are also used as components in mixed fertilizers, with magnesium as fifth in the series of elements required for plant nutrition and as an essential ingredient for the formation of chlorophyll.

An electrically fused grade of pure magnesium oxide is used in the manufacture of high-temperature crucibles, and a fused polymerized oxide finds extensive application in the manufacture of heating elements for electric ranges. Purified magnesium oxide is the starting material in the preparation of numerous magnesium salts and other compounds. Considerable amounts are consumed by the dry-cleaning industry as desolventing agents for solvents. The reactive grades of the oxide find use as neutralizing agents and vulcanization accelerators in the compounding of neoprene and other rubbers. Magnesium oxide is used as an absorbent and catalyst in the epichlorohydrin process for the recovery of uranium oxide from uranium ores. Numerous catalytic compositions used in the preparation of organic compounds contain magnesium oxide. It is also an ingredient of various pharmaceutical and cosmetic formulations, such as dentifrices and powders. Magnesium oxide, USP XVII, is used essentially like the hydroxide and carbonate. The principal uses of magnesium hydroxide are in medicine, as an antacid and laxative, primarily in the form of the aqueous suspension known as milk of magnesia, USP XVII. Much of the latter is prepared by dilution of a 40% paste of magnesium hydroxide, which is obtained by vacuum filtration of a washed seawater precipitate. Milk of magnesia is also prepared by precipitating Mg(OH)₂ from a solution of magnesium sulfate with caustic soda. A medicinal grade of dried magnesium hydroxide is used in tablet formulations for the same purpose.

Bibliography for Magnesium Oxide and Hydroxide

1. C. R. H. Shephard and S. I. Siedel, *Chem. Eng.* 72, 150 (July 19, 1955)
2. C. R. H. Shephard and S. I. Siedel, *Chem. Eng.* 72, 54 (August 2, 1955)
3. C. R. H. Shephard and S. I. Siedel, *Chem. Eng.* 72, 98 (August 16, 1955)
4. E. H. Naylor, *Chem. Eng.* 63, 160 (August 1954)
5. C. R. H. Shephard and W. B. Dancy, *International Minerals and Chemical Corp. Rept.* No. 10-117 (1955)
6. U.S. Pat. 2,778,912 (August 10, 1956); W. B. Dancy, in *International Minerals and Chemical Corp.*

APPENDIX FIVE

PRIMARY VENDORS IN THE U.S. POTASH INDUSTRY

TABLE I
Primary Vendors to the U.S. Potash Industry

<u>Item</u>	<u>Vendor</u>	<u>Address</u>	<u>Telephone</u>
Ball and Rod Mills	Allis-Chalmers	P.O. Box 2219 Appleton, Wisconsin 54913	414-734-9831
	Denver Equipment Div. Joy Manufacturing	P.O. Box 340 Denver, Colorado 80903	303-471-3443
Crushers	Allis-Chalmers	P.O. Box 2219 Appleton, Wisconsin 54913	414-734-3443
	Stedman Machine Company	500 Indiana Avenue Aurora, Indiana 47001	812-926-0038
	Pennsylvania Crusher	Box 100 Broomall, PA 19008	215-544-7200
Crystallization Equipment	Swenson	15700 Lathrop Avenue Harvey, Illinois 60426	312-331-5500
	HPD, Inc.	1717 North Naper Blvd. Naperville, Illinois 60540	312-357-7330
Dryers	Allis-Chalmers	P.O. Box 2219 Appleton, Wisconsin 54913	414-734-9831
	Louisville Drying	232 East Main Louisville, Kentucky 40202	502-583-7646
	Renneburg	2639 Boston Street Baltimore, Maryland 21224	301-732-1665

TABLE I (continued)

<u>Item</u>	<u>Vendor</u>	<u>Address</u>	<u>Telephone</u>
Filtration Equipment	EIMCO Process Equipment	P.O. Box 300 Salt Lake City, Utah 84110	801-526-2000
	Dorr-Oliver	77 Havemeyer Lane Stamford, Connecticut 06904	203-358-3200
	Denver Equipment	P.O. Box 340 Denver, Colorado 80903	303-471-3443
Flotation Equipment	Denver Equipment	P.O. Box 340 Denver, Colorado 80903	303-471-3443
	Wemco	P.O. Box 15619 Sacramento, California 95852	916-929-9363
Flotation Reagents	Sherex Chemical Co.	P.O. Box 646 Dublin, Ohio 43017	614-764-6659
	Arnak	8401 West 47th Street McCook, Illinois 60525	312-442-7100
	American Cyanamid	Wayne, New Jersey 07470	201-831-3197
Pumps	Allis Chalmers	P.O. Box 512 Milwaukee, Wisconsin 53201	414-734-9831
	Gorman-Rupp	P.O. Box 1217 Mansfield, Ohio 44901	419-886-3001
	Denver Equipment	P.O. Box 15619 Denver, Colorado 80903	303-471-3443

TABLE I (continued)

<u>Item</u>	<u>Vendor</u>	<u>Address</u>	<u>Telephone</u>
Screens	C-E Tyler	8200 Tyler Blvd. Mentor, Ohio 44060	216-255-9131
	Rotex	1257 Knowlton Street Cincinnati, Ohio 45223	513-541-1236
	Sweco, Inc.	P.O. Box 4151 Los Angeles, California 90051	213-726-1177
Technical Consulting	Great Salt Lake Minerals & Chemicals Corporation	P.O. Box 1190 Ogden, Utah 84402	801-731-3100
Testing Facilities	International Fertilizer Development Center (IFDC)	Muscle Shoals, Alabama 35660	205-386-2593
	United States Bureau of Mines, Salt Lake Research Center	729 Arapeen Drive Salt Lake City, Utah 84113	801-524-5350

Final Report

Part Two

**Optimization of EI Mex
Salines Solar Ponds and
By-Product Investigation**

Volume 10 from 1 disk 02 - 3564
 Directory of A: \

ELMEX	DAT	936	3-08-90	9:28a
BORGBASE	DAT	1099	3-08-90	11:30a
ELMEXMOD	EXE	52768	11-15-89	12:08p
ELMEXMOD	BAK	54782	11-15-89	12:23p
Two-POND	DAT	1070	3-07-90	1:05p
Two-POND		56228	3-07-90	1:10p
Two-POND	END	704	3-07-90	1:11p
BORGBASE		58807	3-08-90	11:35a
NO-RCYL	DAT	937	3-08-90	9:24a
NO-RCYL		33061	3-08-90	9:27a
NO-RCYL	END	627	3-08-90	9:27a
ELMEX		33059	3-08-90	9:39a
ELMEX	END	625	3-08-90	9:40a
BORGBASE	END	709	3-08-90	11:35a
ELMEXRPT	DOC	41472	11-13-89	3:28p
ELMEXED	COM	61180	1-18-89	9:17a
ELMEXMOD	PAS	54782	12-18-89	8:10a
		17 Files)	754176 bytes	free

18752 (2 of 2)

Final Report
Part Two
Optimization of El Mex
Salines Solar Ponds and
By-Product Investigation
UNIDO Project DP/EGY/87/017
February 1990

By GSL Consulting Engineer
David Butts
Chad McCleary

ABSTRACT:

This report is Part Two of a final report authorized by the United Nations Industrial Development Organization (UNIDO). This report is a technical evaluation of El Mex Pond System. A computer program and operating disk is included.

REFERENCES

The following reports and books have been written as part of this study.

<u>Name</u>	<u>No. of Pages</u>
1. Report of First Mission to El Mex Salines. Fact Finding. Test Procedures and Complete Analytical Analysis Instruction. January 1988, David Butts and J.C. McLaughlin.	154
2. Work Book Problems for use with Hewlett Packard Advanced Scientific Calculator 28S. April 1988, Chad McCleary and David Butts.	50
3. Lecture and Training Series on Solar Ponding. Prepared for El Nasr Salines Company, Alexandria, Egypt. March, 1988, Chad McCleary and David Butts.	114
4. First test on the Concentration of El Mex Pond Brine. April 1988, David Butts, Chad McCleary.	40
5. Report on Second Mission to El Mex Salines, May 1 to May 20, 1988. Training and Establishing of Data Base. June, 1988, David Butts and Chad McCleary.	22
6. Concentration Path of El Mex Brine and Ocean Brine. September 1988, David Butts.	59
7. Brine Evaporation at El Mex Salines. November 1988, David Butts.	67
8. Draft Report, Optimization of El Mex Salines Solar Ponds and By-Product Investigation. December 1988, David Butts and Chad McCleary.	40
9. Final Report, Part One, Optimization of El Mex Salines Solar Ponds and By-Product Investigation. April 1989, David Butts and Chad McCleary.	57

SUMMARY

This final report includes a disk that can be used to run pond operations seminars for Port Said, El Mex Salines, and Borg El Arab. It will require someone familiar with personal computers, disk operating systems (DOS), and solar ponds. If special training is needed, GSL can supply training. Training time will take only two days.

GSL has already made many runs and conclusions are basically the same as reported earlier. These conclusions are summarized once again:

1. Stop recycle of bittern at El Mex Salines (this has already been done in 1989).
2. Establish better weather data and evaporation rates. Correlate this data with actual production rates and then use the data to optimize ponds at El Mex and Borg El Arab. (Again, this has been started in 1988, but correlation to production rates was never made.)
3. Establish a brine profile as a function of evaporation. (This was done at GSL, see report Reference 6.)
4. Plenty of bittern brine is produced at El Mex to supply magnesium for production of MgO. GSL is not an expert in MgO and therefore some name references were given. Since then, a company who has made MgO from sea bittern has been located. They have been contacted and said they would be willing to supply technology. They are:

Mr. M. Hariharaswamy, Senior Superintendent
Tata Chemicals
Mithapur-361 345
Jamnagar Dist.
Gujarat State, India

Telex: 116427 (Head office, Bombay)
Telephone: 204 9131 (Head office)

5. GSL does not recommend K_2SO_4 by-product production at the present time. There are two main reasons:
 - a. Evaporation of highly concentrated brine appears marginal and more study is needed in this area.
 - b. There are not very large reserves of potassium and production of K_2SO_4 could not be sustained for over ten years.
6. Proper sequencing of brine at all three salt works will increase quality of salt. This is especially true at El Mex Salines where production of 99.5 salt (dry basis) should be possible just as it is done at many similar salt works in the world. Recommendations for the brine sequence has been given in previous reports.
7. The computer program can be used to aid in long range planning and operation at El Mex and Borg El Arab. We suggest two or three engineers be

assigned to learn how to use it to better understand and operate their solar pond systems.

I. INTRODUCTION

In 1987, GSL consultant David Butts visited El Mex Salines in Alexandria, to observe their pond system and make comments concerning possible by-product production of K_2SO_4 , $MgCl_2$, and MgO .

It was evident that changes could be made that would increase production of $NaCl$ and also improve grade and quality. It was not possible to determine by-product production capabilities because data was lacking. GSL proposed that tests be made to obtain the data. Specifically, evaporative rates and brine chemistry as a function of evaporation in high concentration ranges was needed.

Approval for the tests was made and funded by the United Nations Development Program (UNDP) through the International Center in Vienna. The supervising agency would be UNIDO, Project DP/EGY/87/017. In January of 1988, work was begun.

Since then, nine reports have been written. Lectures and training of El Mex personnel have been conducted and extensive bench test work at Great Salt Lake Minerals & Chemicals Corporation (GSL) have been completed.

A final report is written in two parts. Part One was completed in April of 1989 and hand delivered to El Mex Salines, El Nasr Salines and Mining and Refractory Industrial Corporation personnel in Cairo and Alexandria. In this report, it was suggested that formation of K_2SO_4 mixed salts and other by-product salts did not look promising. Formation of MgO via lime addition (or dolomite) did have promise. The report also made suggestions how sodium chloride production could be increased. It was also reported that salt quality and quantity could be increased with a change of brine management.

Part Two of the final report is shown herein. GSL has requested that actual production rate of $NaCl$ be supplied so that the data could be used as a base. Also, that all evaporation data up to date be submitted to GSL. As of now, this data has not been received and so the report is submitted without it.

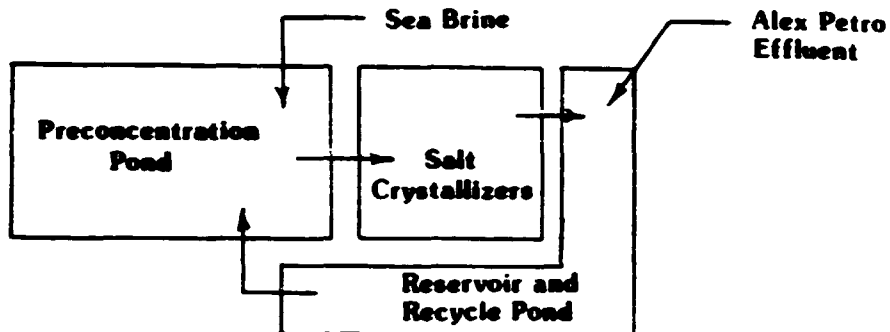
The main emphasis of this report is pond modeling, computer use to optimize ponds, and comments pertaining to both El Mex Salines and Borg el Arab solar pond system.

II. DISCUSSION

All of the following discussions and examples are based on a computer model as illustrated in the Appendix of this report. The actual program is also on a disk and can be executed on an IBM or compatible personal computer by entering the name ELMEXMOD. This program has been written especially for El-Mex Salines but can be used by Port Said and Borg el Arab. Some details of program execution and use are found in this report.

Base Case

For years, El Mex Salines has operated a closed pond system. This system is shown below:



In this system, none of the impurities or minerals other than NaCl are removed. The net result is brine now high in Magnesium concentration. This high magnesium results in suppressed evaporation rates and poor quality salt.

Case One. Base Case

A step-by-step procedure will show how to run this case on the computer. First, it is expected that the operator knows the basic operation of a PC.

1. Change the computer default drive to the "A" drive.
2. Type: ELMEXMOD and press the ENTER key.

3. The following screen will appear:

```
          GGG          SSS          LLLL
        GGGGGGGGG      SSSSSSSSS      LLLL
      GGGG  GGGG      SSSS  SSSS      LLLL
    GGGG      GGGG      SSSS          LLLL
  GGGG          SSSS          LLLL
GGGG          SSSS          LLLL
GGGG      GGGGGG          SSSS      LLLL
GGGG      GGGG          SSSS      LLLL
  GGGG  GGGG      SSSS  SSSS      LLLL
    GGGGGGGGG      SSSS  SSSS      LLLLLLLLLLLLLL
      GGGGG          SSSSSSS      LLLLLLLLLLLLLL

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          El Mex Model Version 1.01

Press <Enter> to continue.
```

4. Press ENTER and the next screen appears.

```
What INPUT data file do you want to read?
```

5. Type ELMEX.DAT or the name of any other data file you may want to use. Data may be in any ASCII file. See the Appendix for a description of data files. After typing ELMEX.DAT, press ENTER. The screen will now look like this:

```
What INPUT data file do you want to read? ELMEX.DAT
Read input file ELMEX.DAT OK?
```

6. Type Y (for yes) and the data screen will appear. ELMEX.DAT data screen, for example, will appear as shown below.

```
Data read from ELMEX.DAT:
Pond Pond Currnt Tar          Ion Weight Percents      Pond  Pond  Salt
Name Area Depth Depth Inventory %K      %Na  %Mg  %Cl  %SO4 Max Flow Rec. Dis.
      (Hect) (cm) (cm)  (Tons)
Lake   0    0    0    0 0.04  1.05  0.13  1.90  0.26 1000000 0.0 0.00
PND1 2500  100  100 30538767 0.41  7.07  1.75 15.35  2.57  500000 1.0 0.05
PND2  500   50   50 3109028 0.50  7.02  2.16 15.14  3.17  400000 0.0 0.01
HRV1  400   30   30 1522103 0.67  5.73  2.87 14.57  4.20  300000 0.0 0.00
Is all the data correct? <Y> or <N>
```

7. If the data is correct, type Y and the screen will ask the question:

What month do the calculations begin in?

8. Type the number or name of the months you wish to begin. For example, type 6 for June, and press ENTER. The next screen will appear.

What day in June do the calculations begin?

9. Type in the day and ENTER. 1 is used in this example. The next question then appears.

What is the evaporation factor for this run?

10. Now type in the evaporation factor. Evaporation is based on evaporation from pans at El Mex Weather Station as outlined in report Reference 7. If one wants to use this data directly, the factor would be 1. If weather for the year is 10% above normal then a 1.1 factor would be used. The example uses 1. Type 1 and ENTER.

What is the precipitation factor for this run?

11. The precipitation factor for normal rainfall is 1. Type 1 ENTER.

Evaporation Factor = 1.000
Precipitation Factor = 1.000
Are these correct?

12. The screen (above) now asks for a verification of both the evaporation factor and the precipitation factor. If they are correct, type Y.

How many months do you want the calculations to run?

13. Now type in the number of months you want the computer to simulate the pond system. For example, say you are beginning in June 1990 and want to run to the end of December 1993. This is 42 months. Type 42 and press ENTER.

What file do you want the monthly totals written to?

14. Now the above question is asked. As the computer calculates what is happening in the pond system, it must store its calculation somewhere. This data can then be looked at later. You can name the file anything you want so long as it follows standard MS-DOS rules. In this example, let's call the file "BASECASE." Type BASECASE and press ENTER.

Do you want to keep a daily material balance file? <Y> or <N>

15. The screen now asks if you want to keep a daily material balance file. In most cases, the answer is no. A daily file will include complete details and trace all ions each day. It is a good analytical tool, but is time consuming, requires a lot of printout paper, and in most cases is not needed. Type N and press ENTER.
16. The computer now begins calculating and shows you its progress on the screen. When it is finished, the screen now looks like this:

```
Calculating Year: 5  
Calculating Day:  
Calculating Pond:
```

```
What file do you want the ending conditions written to?
```

17. A new file is asked for. This file will keep the pond status at the end of the fifth year. This is handy to compare to the starting condition (June 1, 1990) or to use later as the starting conditions of another computer run. Let's call the ending condition BASECASE.END. Type BASECASE.END and press ENTER.

Calculating Year: 5
Calculating Day:
Calculating Pond:

what file do you want the ending conditions written to? BASECASE.END
write ending conditions to BASECASE.END. OK?

18. The computer now confirms that you want the file saved to BASECASE.END. Type Y and the run is complete.

A:Y

The computer now returns to the DOS prompt. You may run again by executing ELMEXMOD or stop here and call up the data file just completed.

To continue, we will call up the three data files, ELMEX.DAT, BASECASE, AND BASECASE.END. Type PRINT ELMEX.DAT and then press ENTER. The following will be printed:

This is the set-up for the El Mex system as it is presently run. The Lake is the concentration of the open ocean. The line of asterisks may be moved to accomodate more comments. Notice that ponds whose names begin with H are assumed to be harvestable. The net deposit of the system is summed from these harvestable ponds.

Pond Name (Hect.)	Area (Hect.)	Current Target		Ion Weight Percents					Max. Flow (Tons/d)	Rec. Dsv.	Salt Fact.
		Depth (cm)	Depth (cm)	K	Na	Mg	Cl	SO4			
Lake	0	0	0	0.04	1.05	0.13	1.90	0.26	1000000	0	0.00
PND1	2500	100	100	0.41	7.07	1.75	15.35	2.57	500000	1	0.05
PND2	500	50	50	0.50	7.02	2.16	15.14	3.17	400000	0	0.01
HRV1	400	30	30	0.67	5.73	2.87	14.57	4.20	300000	0	0.00

Next, type PRINT BASECASE and push ENTER. the data for each month over the time specified will be printed. These pages are shown in the Appendix. The summary of each year is shown below. SEE APPENDIX A

El Mex Model Summary File "BASECASE"
 Evaporation factor is 1.000 Precipitation factor is 1.000

 Summary of year 1
 Months Calculated = June to December
 Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	0	0	0	0	0	-529	-288	-257	-223	-181	-121	-68	-1668
PND2	0	0	0	0	0	216	232	226	183	132	89	35	1112
HRV1	0	0	0	0	0	170	184	180	141	99	62	19	854
Total	0	0	0	0	0	-143	128	148	100	50	29	-14	298
Net	0	0	0	0	0	170	184	180	141	99	62	19	854

Summary of year 2
 Months Calculated = January to December
 Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	-26	-23	-81	-153	-212	-232	-253	-250	-220	-178	-120	-67	-1816
PND2	22	46	124	185	211	225	228	220	181	128	86	33	1688
HRV1	8	25	90	140	166	179	185	179	141	99	61	19	1291
Total	4	48	133	172	165	172	160	148	101	49	28	-15	1164
Net	8	25	90	140	166	179	185	179	141	99	61	19	1291

Summary of year 3

Months Calculated = January to December

Deposit in thousands of tons.

	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
Pond													
PND1	-24	-21	-80	-150	-208	-228	-248	-245	-216	-175	-118	-65	-1780
PND2	20	43	122	179	208	217	222	215	172	124	85	31	1637
HRV1	7	24	90	139	165	179	184	178	140	98	62	17	1283
Total	2	46	133	167	165	168	158	147	96	47	28	-17	1141
Net	7	24	90	139	165	179	184	178	140	98	62	17	1283

Summary of year 4

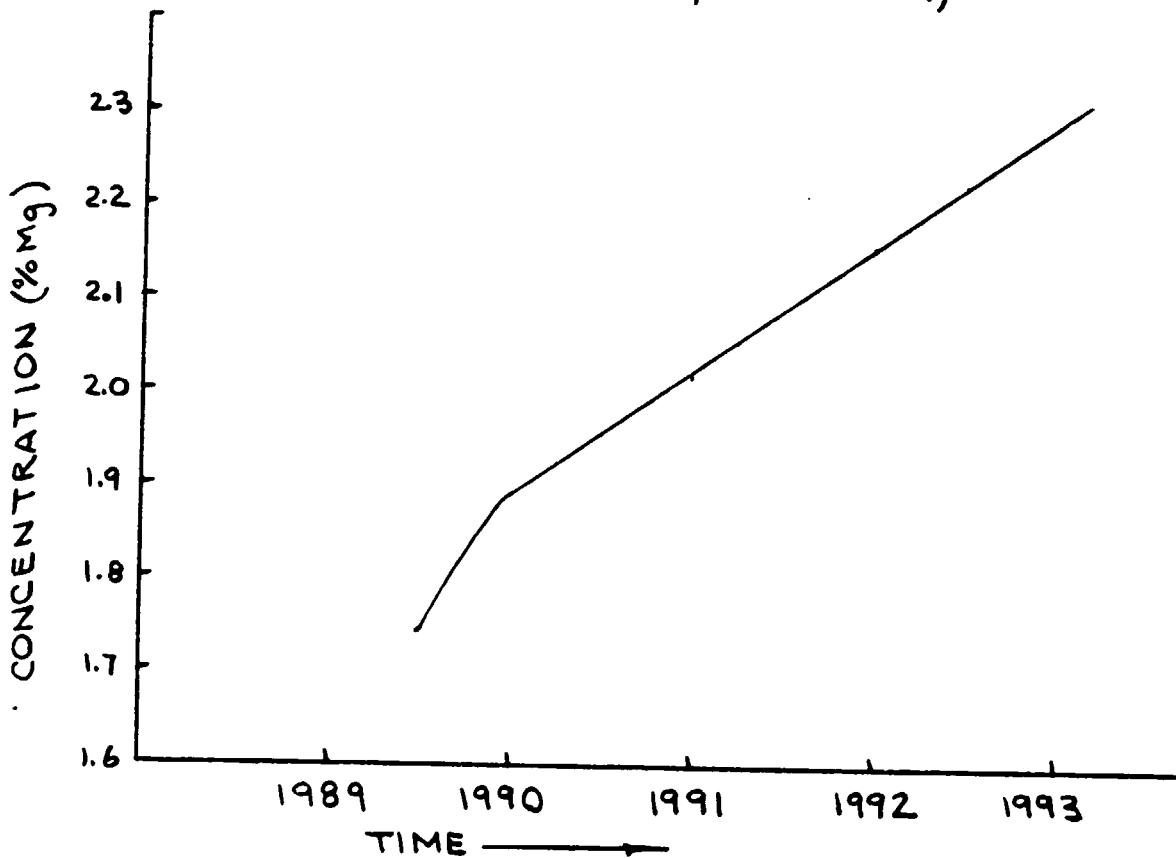
Months Calculated = January to December

Deposit in thousands of tons.

	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
Pond													
PND1	-25	-24	-80	-148	-204	-223	-243	-240	-211	-172	-116	-65	-1750
PND2	19	42	120	173	203	209	215	210	165	122	82	29	1588
HRV1	9	26	90	138	165	178	183	178	139	98	61	18	1283
Total	3	44	130	164	164	164	155	148	94	48	27	-18	1121
Net	9	26	90	138	165	178	183	178	139	98	61	18	1283

The computer ran the 42-month period which began June 1, 1989 and ends December 31, 1992. A plot of magnesium concentrates for the period is shown on Graph 1. Note how concentrations continually increase.

GRAPH I
CONCENTRATION OF MAGNESIUM
VERSUS TIME IN EL MEX 1ST
POND WITH BITTERN'S RECYCLE
(SEE BASE CASE, APPENDIX A)



Now print out the "BASECASE.END" data. This shows the pond status at the end of this 42-month period. All ionic concentrations are shown. Notice, for example, that the pond concentration has increased from 1.75 percent Mg in June of 1989 to 2.24 percent in December of 1992.

Ending Conditions File
 Start Conditions From :ELMEX.DAT
 Model run covered 5 years.
 Model ran 42 months.
 The first month run was June.
 The last month run was December.
 The evaporation factor was 1.000.
 The precipitation factor was 1.000.

```
*****
Lake      0      0      0      0.04  1.05  0.13  1.90  0.26  1000000  0.0  0.00
PND1     2500   100   100   0.56  6.87  2.24  15.93  3.54   500000  1.0  0.05
PND2      500    50    50   0.65  6.33  2.59  15.95  4.10   400000  0.0  0.01
HRV1      400    30    30   0.73  5.79  2.93  15.94  4.63   300000  0.0  0.00
```

Of course, all of this is based on an estimated evaporation rate, which, according to the yearly print out, should produce near 1,283,000 tons of NaCl per year. Suppose El Mex only produces 900,000 tons per year as a matter of record. This means that the evaporation rate is too high. If we multiply 1.283000 by a factor of .70 (900,000 ÷ 1283000) then the correct value of 900,000 tons would be obtained. This .70 factor can be placed in the computer when it asks for an evaporative factor. This is a type of calculation step that will correct calculations to duplicate actual conditions at El Mex.

Since GSL does not know actual conditions at El Mex, a factor of 1.0 will be used.

Case 1. No Recycle

Now an exact duplicate of the Base Case will be run, except recycle brine will be eliminated. This run is also shown in the Appendix. The starting data is shown on the next page. Note that the data is identical to the base case except for a "1" in the "Rec" column has been replaced by a "0" meaning that the pond is not receiving any recycled brine. A "1" means the pond is receiving recycled brine from the last salt crystallizer.

Note in the no recycle case, magnesium in the first concentration pond has decreased from 1.75% Mg down to 0.51 in just 42 months. This will be a tremendous boost to salt quality and will also result in much higher salt production in the future. (See Appendix B)

This is the set-up for the El Mex pond system without bitterns recycle. The Lake is the concentration of the open ocean. The line of asterisks may be moved to accomodate more comments. Notice that ponds whose names begin with H are assumed to be harvestable. The net deposit of the system is summed from these harvestable ponds.

Pond Name	Area (Hect.)	Current Target		Ion Weight Percents					Max. Flow (Tons/d)	Rec.	Salt Dsv. Fact.
		Depth (cm)	Depth (cm)	K	Na	Mg	Cl	SO4			
Lake	0	0	0	0.04	1.05	0.13	1.90	0.26	1000000	0	0.00
PND1	2500	100	100	0.41	7.07	1.75	15.35	2.57	500000	0	0.05
PND2	500	50	50	0.50	7.02	2.16	15.14	3.17	400000	0	0.01
HRV1	400	30	30	0.67	5.73	2.87	14.57	4.20	300000	0	0.00

Case 2. Series Pond Operation

It has already been suggested that salt crystallizer brine not be recycled. This will increase crystallized salt purity and will also increase the overall evaporative rates caused by lower magnesium concentration.

Crystallizer ponds placed in series will also increase both salt quality and quantity. The next case shows a computer run and an explanation how this is done.

ELMEX.DAT data file represents a starting point for the computer.

LAKE - sea brine. PND 1 - the large, 25 square kilometer preconcentration pond. PND 2 is the second preconcentration pond and HRV1 represents the salt crystallizer. The brine sequence is Sea → Preconcentration Pond #1 → Preconcentration Pond #2 → Salt Pond. To simulate a two salt pond system, the single salt pond of Base Case or Case 1 must be divided in two. This can be done as follows:

1. Start the program as done in Base Case by executing ELMEXMOD. When the computer asks for the data file, type in the name of the file desired or, if the desired file is non-existent, type ELMEX.DAT and push ENTER. The file will now appear on the screen and a question will be asked:

```

Data read from elmex.dat:
Pond Name Area Depth Current Target Inventory %K %Na %Mg %Cl %SO4 Max Flow Rec. Salt Dsv. Fact.
(Hect.) (cm) (cm) (Tons)
Lake 0 0 0 0 0.04 1.05 0.13 1.90 0.26 1000000 0 0.00
PND1 2500 100 100 30638757 0.41 7.07 1.75 15.35 2.57 500000 0 0.05
PND2 500 50 50 313428 0.50 7.02 2.16 15.14 3.17 400000 0 0.01
HRV1 400 30 30 1822103 0.67 5.73 2.87 14.57 4.20 300000 0 0.00
(is all the data correct? Y or N)

```

Press the N key and another question will be asked at the bottom of the screen:

```
**User specified error in input data.**
Do you want to read a different file? <Y> or <N>
```

Now you can push Y and enter a different file, or you can press N and change the ELMEX.DAT file. In this case we will change the existing file. Type N. The screen now changes to add two more lines.

```
**User specified error in input data.**
Do you want to read a different file? <Y> or <N> N
Program will exit to the editor with elmex.dat
Press <Enter> to continue.
```

Press ENTER and a new screen appears as shown next.

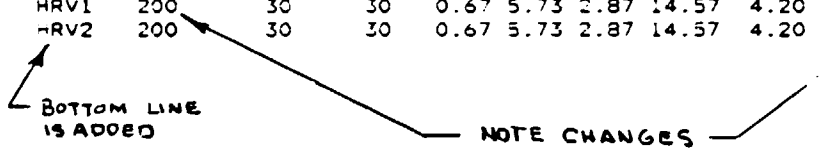
```
ELMEX.DAT                      L:16    C:1    B:1                      QVR AI
This is the set-up for the El Mex system as it is presently run.
The Lake is the concentration of the open ocean.
The line of asterisks may be moved to accommodate more comments.
Notice that ponds whose names begin with H are assumed to be harvestable.
The net deposit of the system is summed from these harvestable ponds.
```

Pond Name (Hect.)	Area	Current Depth		Target Ion Weight Percents					Max. Flow (Tons/d)	Rec. Dsv.	Salt Fact.
		(cm)	(m)	K	Na	Mg	Cl	SO4			
Lake	0	0	0	0.04	1.05	0.13	1.90	0.25	1000000	0	0.00
PND1	2500	100	100	0.41	7.07	1.75	15.35	2.57	500000	1	0.05
PND2	500	50	50	0.50	7.02	2.16	15.14	3.17	400000	0	0.01
HRV1	400	30	30	0.67	5.73	2.87	14.57	4.20	300000	0	0.00

This screen is actually a text editor called EDWIN. Changes can now be made to this data and then stored for use in the program. We will change the HRV1 pond by dividing it in half. Move the cursor down to the Area (Hect) space on the HRV1 line and overtype this 4 with a 2. This will change the salt area from 400 hectares (4 square kilometers) to 200 hectares. Now push ENTER and the cursor will move to the blank space just under HRV1. Type HRV2 and duplicate everything else as shown for HRV1. The screen should now look like this:

```
ELMEX.DAT          0112   0:07  8:773          DVR AI   SAVE
This is the set-up for the El Mex system as it is presently run.
The lake is the concentration of the open ocean.
The line of asterisks may be moved to accomodate more comments.
Notice that ponds whose names begin with H are assumed to be harvestable.
The net deposit of the system is summed from these harvestable ponds.
```

Pond Name (Hect.)	Area (Hect.)	Current Depth (cm)	Target Depth (cm)	Ion weight Percents					Max. Flow (Tons/d)	Rec.	Salt Dis. Fact.
				K	Na	Mg	Cl	SO4			
Lake	0	0	0	0.04	1.05	0.13	1.90	0.26	1000000	0	0.00
PND1	2500	100	100	0.41	7.07	1.75	15.35	2.57	500000	0	0.05
PND2	500	50	50	0.50	7.02	2.16	15.14	3.17	400000	0	0.01
HRV1	200	30	30	0.67	5.73	2.87	14.57	4.20	300000	0	0.00
HRV2	200	30	30	0.67	5.73	2.87	14.57	4.20	300000	0	0.00



Now press CTRL K X or F1 and the data will be saved in the file ELMEX.DAT. The old data in ELMEX.DAT will be lost. The screen will now look like this:

```
Data read from elmex.dat:
```

Pond Name	Area (Hect)	Depth (cm)	Currt Depth (cm)	Inventory (Tons)	%K	%Na	%Mg	%Cl	%SO4	Pond Max Flow (m ³ /d)	Pond Rec.	Salt Dis. Fact.
Lake	0	0	0	0	0.04	1.05	0.13	1.90	0.26	1000000	0.0	0.00
PND1	2500	100	100	30638767	0.41	7.07	1.75	15.35	2.57	500000	0.0	0.05
PND2	500	50	50	3109028	0.50	7.02	2.16	15.14	3.17	400000	0.0	0.01
HRV1	200	30	30	761052	0.67	5.73	2.87	14.57	4.20	300000	0.0	0.00
HRV2	200	30	30	761052	0.67	5.73	2.87	14.57	4.20	300000	0.0	0.00

Is all the data correct? <Y> or <N>

If it is desired not to over-write the ELMEX.DAT file, this can also be done. Place the cursor at the beginning of the text and push CTRL K B. Then place the cursor at the end of the text file and push CTRL K K. This will mark the block. Then, push CTRL K W. The question at the top of the screen asks: What File Name? Type in the new name you want for the file such as ELMEX2.DAT. Now the data file will be stored without destroying the old file. To exit back to ELMEXMOD, push CTRL K Q and follow screen print instructions.

The question is asked:

Is all the data correct? <Y> or <N>

Press Y and the screen now advances to the question of normal routine. Enter in the same time, evaporation, and precipitation data as was done for the Base Case. Call the data file TWO-PNDS and the end file TWO-PNDS.END. Now print out the files. These files are shown in the Appendix of the report. A summary of the fourth year is shown below.

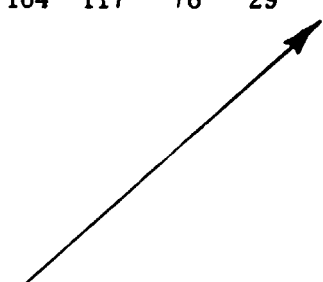
Summary of year 4

Months Calculated = January to December

Deposit in thousands of tons.

	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
Pond	-----												
PND1	-49	-44	-159	-246	-344	-349	-396	-379	-334	-280	-168	-99	-2847
PND2	47	74	157	224	255	273	279	274	228	168	121	64	2163
HRV1	13	23	58	87	102	109	114	110	90	65	44	20	839
HRV2	4	13	47	72	86	92	97	92	73	52	31	8	667
Total	15	66	102	138	100	124	93	98	58	5	29	-6	822
Net	18	36	105	159	188	201	211	203	164	117	76	29	1506

Note that the salt deposited is 1,506,000 tons in the salt ponds, compare this to the base case of 1,283,000. This increase of 223,000 tons is the result of simply placing salt crystallizer in series flow and not recycling concentrated brine.



With the computer program, a variety of cases can be made to optimize the ponds. GSL has run several cases and depending on the accuracy of the evaporation, much can be done to increase production.

Borg El Arab

The computer program can also be used for the Borg El Arab pond system. simply create a data file for Borg El Arab to start with and the computer will begin with that.

Borg El Arab is much different than El Mex Salines because it does not have a sodium chloride floor. All salt must rely on the sea.

As understood by GSL, Borg El Arab is 24 square kilometers in size or 2,400 hectares. This area is divided into one large 2,000 hectare concentration pond and 400 hectare crystallization ponds. The concentration pond is divided by a cement factory road. There is about 300 hectare of preconcentration pond on one side and 1,700 hectares on the other.

If we assume that the salt ponds will be run in series, then the pond system will be run as shown below:

This is the setup for the Borg El Arab system of ponds.
 The lake is the concentration of the open ocean.
 The line of asterisks may be moved to accommodate more comments.
 Notice that ponds whose names begin with H are assumed to be harvestable.
 The net deposit of the system is summed from these harvestable ponds.
 In this standard state the ponds are filled with ocean brine and then run in sequence for 5 years.

Pond Name (Hect.)	Area (Hect.)	Current Target		K	Ion Weight		Percent		Max. Flow (Tons)	Rec. (Days)	Salt Prod. (Tons)
		Depth (cm)	Depth (cm)		Na	Mg	01	04			
Lake	0	0	0	0.04	1.05	0.13	1.90	0.25	1000000	0	0.00
PND1	1700	50	50	0.04	1.05	0.13	1.90	0.25	500000	0	0.00
PND2	300	50	50	0.04	1.05	0.13	1.90	0.25	400000	0	0.00
HRV1	200	30	30	0.04	1.05	0.13	1.90	0.25	300000	0	0.00
HAR2	100	30	30	0.04	1.05	0.13	1.90	0.25	200000	0	0.00

The computer print out of Appendix E shows that steady state production is near 700,000 TPY if ponds are run in series. There also appears to be a mismatch in pond area ratios. If these ratios are adjusted even more salt could be produced. It is suggested, however, that no changes be made until several years running and evaporative and production rates can be used to optimize the ponds as indicated by computer model runs.

Computer Model Details

The computer program enclosed is quite comprehensive. It has the program to dissolve salts from the bottom of the floor if salt is present. The amount of salt it dissolves is controlled by the computer operator. Evaporation, rain, pump flow rates, pond size, concentrates, depth, and bittern recycle, can also be specified by the computer operator.

The user can also follow a complete material balance through the pond day by day. This is time consuming but in time it may be very important to see what is really happening in a pond system.

GSL can provide specialized training in the detailed use of the model if needed.

The next page shows an example of the pond material balance from July 24 to July 25.

"Mass Balance = 0.000" means that TONS IN minus TONS OUT = 0.000, a perfect balance. Anything other than 0.000 is unsatisfactory. Notice that each pond is tested for Mass, Mg, and Na.

The disk included with this book is formatted 1.2 meg. This is done so that more storage space can be used on the disk. If the user runs out of space, then some files must be removed. One way to overcome this problem is to copy the disk to a hard disk and then execute the program from the hard disk. Another way is to simply place in another data storage floppy disk.

If a 1.2 meg formatted disk is not compatible with El Mex computer, GSL can supply a 360K or 720K formatted disk.

01

Beginning Inventory	Flow In	Recycle In	=	Ending Inventory	Flow Out	Salt Deposit	Evaporation
9433544	159360	0	=	9436792	67996	0	98116
39621	207	0	=	39542	236	0	0
321684	1673	0	=	321038	2319	0	0

Balance =	0.000	Mg Balance =		0.000	Na Balance =		0.000

02

1721958	64189	0	=	1721958	52411	0	16810
11814	269	0	=	11814	362	0	0
95046	2319	0	=	95046	2909	0	0

Balance =	0.000	Mg Balance =		0.000	Na Balance =		0.000

03

714184	52411	0	=	713252	39332	3373	10633
3213	362	0	=	3122	452	0	0
61777	2909	0	=	59955	3402	1329	0

Balance =	0.000	Mg Balance =		0.000	Na Balance =		0.000

04

762865	39332	0	=	760959	30000	2874	8364
22657	452	0	=	22218	391	0	0
43712	3402	0	=	44265	1719	1131	0

Balance =	0.000	Mg Balance =		0.000	Na Balance =		0.000

05

Beginning Inventory	Flow In	Recycle In	=	Ending Inventory	Flow Out	Salt Deposit	Evaporation
9426792	161329	0	=	9425811	64189	0	98122
39542	210	0	=	39483	269	0	0
321038	1694	0	=	320546	2186	0	0

Balance =	0.000	Mg Balance =		0.000	Na Balance =		0.000

06

1721958	64189	0	=	1721429	47900	0	16817
11814	269	0	=	11755	329	0	0
95046	2186	0	=	94589	2644	0	0

Balance =	0.000	Mg Balance =		0.000	Na Balance =		0.000

07

713252	47900	0	=	712714	37791	0	10647
3122	329	0	=	3021	430	0	0
59955	2644	0	=	59422	3177	0	0

Balance =	0.000	Mg Balance =		0.000	Na Balance =		0.000

08

760959	3791	0	=	760202	2700	3122	8427
22218	430	0	=	21860	738	0	0
44265	3177	0	=	44643	1571	1228	0

Balance =	0.000	Mg Balance =		0.000	Na Balance =		0.000

APPENDIX A
BASE CASE RUN

File Names

Starting Conditions	ELMEX.DAT
Ending Conditions	BASECASE.END
Running File	BASECASE

This is the set-up for the El Mex system as it is presently run.
 The Lake is the concentration of the open ocean.
 The line of asterisks may be moved to accomodate more comments.
 Notice that ponds whose names begin with H are assumed to be harvestable.
 The net deposit of the system is summed from these harvestable ponds.

Pond Name	Area (Hect.)	Current Target		Ion Weight Percents					Max. Flow (Tons/d)	Rec.	Salt Dsv. Fact
		Depth (cm)	Depth (cm)	K	Na	Mg	Cl	SO4			
Lake	0	0	0	0.04	1.05	0.13	1.90	0.26	1000000	0	0.00
PND1	2500	100	100	0.41	7.07	1.75	15.35	2.57	500000	1	0.05
PND2	500	50	50	0.50	7.02	2.16	15.14	3.17	400000	0	0.01
HRV1	400	30	30	0.67	5.73	2.87	14.57	4.20	300000	0	0.00

Ending Conditions File
 Start Conditions From :ELMEX.DAT
 Model run covered 5 years.
 Model ran 42 months.
 The first month run was June.
 The last month run was December.
 The evaporation factor was 1.000.
 The precipitation factor was 1.000.

Lake	0	0	0	0.04	1.05	0.13	1.90	0.26	1000000	0.0	0
PND1	2500	100	100	0.56	6.87	2.24	15.93	3.54	500000	1.0	0
PND2	500	50	50	0.65	6.33	2.59	15.95	4.10	400000	0.0	0
HRV1	400	30	30	0.73	5.79	2.93	15.94	4.63	300000	0.0	0

El Mex Model Summary File "BASECASE"

Evaporation factor is 1.000 Precipitation factor is 1.000

Year = 1 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	104863	1.74	99.9	1.75	-529080
PND2	48.3	74100	2.26	50.0	2.29	216367
HRV1	28.5	51663	3.04	30.0	3.06	169778
Total Monthly Salt Deposit =						-142934
Harvestable Salt Deposit =						169778

Year = 1 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.3	125981	1.76	99.9	1.77	-288402
PND2	47.9	95476	2.30	50.0	2.31	231588
HRV1	28.1	73020	3.04	30.0	3.02	184385
Total Monthly Salt Deposit =						127571
Harvestable Salt Deposit =						184385

Year = 1 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	125889	1.78	99.9	1.79	-257107
PND2	47.9	96350	2.31	50.0	2.32	225680
HRV1	28.1	74467	3.00	30.0	3.00	179550
Total Monthly Salt Deposit =						148124
Harvestable Salt Deposit =						179550

Year = 1 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.5	103677	1.80	99.9	1.80	-223320
PND2	48.3	79173	2.33	50.0	2.33	182550
HRV1	28.4	61395	3.00	30.0	3.00	141086
Total Monthly Salt Deposit =						100316
Harvestable Salt Deposit =						141086

Year = 1 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.6	71804	1.81	100.0	1.81	-180554
PND2	48.8	54922	2.34	50.0	2.35	132025
HRV1	28.9	42881	2.99	30.0	3.00	98855
Total Monthly Salt Deposit =						50326
Harvestable Salt Deposit =						98855

Year = 1 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.7	47747	1.82	100.0	1.82	-121429
PND2	49.2	36226	2.35	50.0	2.36	88637
HRV1	29.3	28458	2.99	30.0	3.00	61771
Total Monthly Salt Deposit =						28980
Harvestable Salt Deposit =						61771

Year = 1 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	18100	1.82	100.0	1.82	-67981
PND2	49.7	13704	2.36	50.0	2.37	35459
HRV1	29.7	11495	2.97	30.0	2.96	18531
Total Monthly Salt Deposit =						-13991
Harvestable Salt Deposit =						18531

Summary of year 1

Months Calculated = June to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	0	0	0	0	0	-529	-288	-257	-223	-181	-121	-68	-1668
PND2	0	0	0	0	0	216	232	226	183	132	89	35	1112
HRV1	0	0	0	0	0	170	184	180	141	99	62	19	854
Total	0	0	0	0	0	-143	128	148	100	50	29	-14	298
Net	0	0	0	0	0	170	184	180	141	99	62	19	854

Year = 2 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	7973	1.82	100.0	1.82	-25817
PND2	49.9	5238	2.38	50.0	2.39	22033
HRV1	29.9	4282	2.96	30.0	2.96	7912
Total Monthly Salt Deposit =						4128
Harvestable Salt Deposit =						7912

Year = 2 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	17140	1.82	100.0	1.82	-23376
PND2	49.7	10842	2.41	50.0	2.43	45795
HRV1	29.8	7323	3.01	30.0	3.03	25382
Total Monthly Salt Deposit =						47801
Harvestable Salt Deposit =						25382

Year = 2 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.7	83574	1.83	100.0	1.85	-81414
PND2	48.6	68402	2.39	50.0	2.32	123884
HRV1	28.6	57625	2.99	30.0	2.85	90122
Total Monthly Salt Deposit =						132592
Harvestable Salt Deposit =						90122

Year = 2 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.5	100190	1.85	99.9	1.86	-152738
PND2	48.4	75846	2.37	50.0	2.36	184732
HRV1	28.5	58051	2.97	30.0	2.95	139928
Total Monthly Salt Deposit =						171921
Harvestable Salt Deposit =						139928

Year = 2 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	131583	1.86	99.9	1.89	-211873
PND2	47.9	104424	2.38	50.0	2.32	210918
HRV1	27.9	84253	2.99	30.0	2.85	165932
Total Monthly Salt Deposit =						164977
Harvestable Salt Deposit =						165932

Year = 2 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.3	131140	1.88	99.9	1.90	-232137
PND2	47.9	100785	2.39	50.0	2.37	224784
HRV1	28.0	78055	3.00	30.0	2.93	178854
Total Monthly Salt Deposit =						171501
Harvestable Salt Deposit =						178854

Year = 2 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.3	145567	1.90	99.9	1.92	-252730
PND2	47.6	115536	2.39	50.0	2.35	227863
HRV1	27.7	92956	2.99	30.0	2.88	184733
Total Monthly Salt Deposit =						159867
Harvestable Salt Deposit =						184733

Year = 2 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	135330	1.92	99.9	1.94	-250256
PND2	47.8	106209	2.41	50.0	2.38	219907
HRV1	27.9	84246	2.99	30.0	2.91	178719
Total Monthly Salt Deposit =						148370
Harvestable Salt Deposit =						178719

Year = 2 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.5	100434	1.94	99.9	1.93	-219958
PND2	48.4	76057	2.42	50.0	2.47	180731
HRV1	28.5	58055	2.99	30.0	3.09	140642
Total Monthly Salt Deposit =						101416
Harvestable Salt Deposit =						140642

Year = 2 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.6	84713	1.95	100.0	1.95	-178121
PND2	48.6	68214	2.42	50.0	2.46	128231
HRV1	28.6	56174	2.96	30.0	3.03	98968
Total Monthly Salt Deposit =						49078
Harvestable Salt Deposit =						98968

Year = 2 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.8	46392	1.96	100.0	1.95	-120443
PND2	49.2	35059	2.45	50.0	2.50	86478
HRV1	29.3	27210	2.99	30.0	3.10	61485
Total Monthly Salt Deposit =						27520
Harvestable Salt Deposit =						61485

Year = 2 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	24607	1.96	100.0	1.96	-67000
PND2	49.6	20546	2.44	50.0	2.47	32922
HRV1	29.6	18387	2.95	30.0	3.00	18677
Total Monthly Salt Deposit =						-15463
Harvestable Salt Deposit =						18677

Summary of year 2

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	-26	-23	-81	-153	-212	-232	-253	-250	-220	-178	-120	-67	-1816
PND2	22	46	124	185	211	225	228	220	181	128	86	33	1688
HRV1	8	25	90	140	166	179	185	179	141	99	61	19	1291
Total	4	48	133	172	165	172	160	148	101	49	28	-15	1164
Net	8	25	90	140	166	179	185	179	141	99	61	19	1291

Year = 3 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	4320	1.96	100.0	1.95	-24232
PND2	49.9	1840	2.49	50.0	2.51	19595
HRV1	30.0	968	3.02	30.0	3.03	6829
Total Monthly Salt Deposit =						2191
Harvestable Salt Deposit =						6829

Year = 3 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	20072	1.95	100.0	1.95	-21318
PND2	49.7	14201	2.53	50.0	2.54	42913
HRV1	29.7	10875	3.07	30.0	3.08	24188
Total Monthly Salt Deposit =						45783
Harvestable Salt Deposit =						24188

Year = 3 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.7	83313	1.97	100.0	1.97	-80131
PND2	48.7	68210	2.47	50.0	2.48	122429
HRV1	28.6	57260	2.98	30.0	3.02	90233
Total Monthly Salt Deposit =						132531
Harvestable Salt Deposit =						90233

Year = 3 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.5	128148	1.99	99.9	2.00	-150226
PND2	47.9	104541	2.46	50.0	2.44	178539
HRV1	27.9	87056	2.99	30.0	2.94	139010
Total Monthly Salt Deposit =						167323
Harvestable Salt Deposit =						139010

Year = 3 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	128965	2.00	99.9	2.01	-208332
PND2	47.9	101905	2.47	50.0	2.49	208450
HRV1	28.0	81544	3.00	30.0	3.04	165223
Total Monthly Salt Deposit =						165341
Harvestable Salt Deposit =						165223

Year = 3 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	153856	2.02	99.9	2.02	-227616
PND2	47.5	124058	2.47	50.0	2.52	216658
HRV1	27.5	101341	2.98	30.0	3.09	178617
Total Monthly Salt Deposit =						167658
Harvestable Salt Deposit =						178617

Year = 3 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	159963	2.04	99.9	2.04	-248128
PND2	47.4	130349	2.49	50.0	2.53	222360
HRV1	27.4	107756	2.99	30.0	3.08	184048
Total Monthly Salt Deposit =						158280
Harvestable Salt Deposit =						184048

Year = 3 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	158215	2.06	99.9	2.06	-245388
PND2	47.4	129613	2.50	50.0	2.53	214546
HRV1	27.4	107757	2.99	30.0	3.06	178095
Total Monthly Salt Deposit =						147252
Harvestable Salt Deposit =						178095

Year = 3 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.5	144225	2.07	99.9	2.09	-215775
PND2	47.7	120823	2.51	50.0	2.48	172229
HRV1	27.6	103256	2.99	30.0	2.92	139907
Total Monthly Salt Deposit =						96362
Harvestable Salt Deposit =						139907

Year = 3 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.7	92252	2.09	100.0	2.10	-174848
PND2	48.5	76058	2.51	50.0	2.48	124143
HRV1	28.5	64033	2.98	30.0	2.91	98196
Total Monthly Salt Deposit =						47491
Harvestable Salt Deposit =						98196

Year = 3 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.8	48147	2.09	100.0	2.09	-118206
PND2	49.2	36989	2.52	50.0	2.54	84784
HRV1	29.3	29068	2.98	30.0	3.02	61614
Total Monthly Salt Deposit =						28192
Harvestable Salt Deposit =						61614

Year = 3 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	34323	2.09	100.0	2.11	-65326
PND2	49.4	30670	2.57	50.0	2.48	30798
HRV1	29.4	28774	3.04	30.0	2.86	17078
Total Monthly Salt Deposit =						-17451
Harvestable Salt Deposit =						17078

Summary of year 3

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	-24	-21	-80	-150	-208	-228	-248	-245	-216	-175	-118	-65	-1780
PND2	20	43	122	179	208	217	222	215	172	124	85	31	1637
HRV1	7	24	90	139	165	179	184	178	140	98	62	17	1283
Total	2	46	133	167	165	168	158	147	96	47	28	-17	1141
Net	7	24	90	139	165	179	184	178	140	98	62	17	1283

Year = 4 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	3647	2.11	100.0	2.10	-25443
PND2	49.9	1174	2.51	50.0	2.53	19334
HRV1	30.0	0	2.89	30.0	2.91	9069
Total Monthly Salt Deposit =						2960
Harvestable Salt Deposit =						9069

Year = 4 Month = February Beginning Day = 1 Days Run This Month = 29

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	9742	2.10	100.0	2.09	-23635
PND2	49.8	3808	2.57	50.0	2.62	42036
HRV1	29.9	145	3.00	30.0	3.07	25517
Total Monthly Salt Deposit =						43918
Harvestable Salt Deposit =						25517

Year = 4 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.7	89899	2.11	100.0	2.11	-79642
PND2	48.6	75019	2.55	50.0	2.58	119722
HRV1	28.5	64056	2.99	30.0	3.06	89767
Total Monthly Salt Deposit =						129847
Harvestable Salt Deposit =						39767

Year = 4 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.5	151850	2.12	99.9	2.14	-147756
PND2	47.6	128741	2.55	50.0	2.51	173120
HRV1	27.4	111359	3.00	30.0	2.93	138435
Total Monthly Salt Deposit =						163799
Harvestable Salt Deposit =						138435

Year = 4 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	145315	2.14	99.9	2.14	-204376
PND2	47.7	118635	2.55	50.0	2.58	203202
HRV1	27.6	98269	3.01	30.0	3.05	164773
Total Monthly Salt Deposit =						163597
Harvestable Salt Deposit =						164773

Year = 4 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	186934	2.16	99.9	2.16	-222813
PND2	47.0	157776	2.55	50.0	2.57	208606
HRV1	26.9	135187	2.98	30.0	3.01	177949
Total Monthly Salt Deposit =						163743
Harvestable Salt Deposit =						177949

Year = 4 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	195253	2.17	99.9	2.19	-242716
PND2	46.9	166275	2.57	50.0	2.53	214869
HRV1	26.7	143850	3.00	30.0	2.90	183129
Total Monthly Salt Deposit =						155282
Harvestable Salt Deposit =						183129

Year = 4 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	165308	2.19	99.9	2.19	-239938
PND2	47.3	136859	2.57	50.0	2.62	209567
HRV1	27.3	114752	2.99	30.0	3.07	177971
Total Monthly Salt Deposit =						147600
Harvestable Salt Deposit =						177971

Year = 4 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.5	173602	2.21	99.9	2.22	-211019
PND2	47.2	150730	2.59	50.0	2.55	165085
HRV1	27.0	133213	2.99	30.0	2.90	139459
Total Monthly Salt Deposit =						93524
Harvestable Salt Deposit =						139459

Year = 4 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.7	99912	2.22	100.0	2.23	-171599
PND2	48.4	83930	2.60	50.0	2.57	121510
HRV1	28.3	71864	2.99	30.0	2.94	97905
Total Monthly Salt Deposit =						47816
Harvestable Salt Deposit =						97905

Year = 4 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.8	55967	2.23	100.0	2.22	-116382
PND2	49.1	45078	2.61	50.0	2.64	82114
HRV1	29.1	37181	2.99	30.0	3.04	61387
Total Monthly Salt Deposit =						27119
Harvestable Salt Deposit =						61387

 Year = 4 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.9	33935	2.23	100.0	2.24	-64711
PND2	49.5	30382	2.62	50.0	2.59	29288
HRV1	29.4	28352	3.01	30.0	2.93	17665
Total Monthly Salt Deposit =						-17758
Harvestable Salt Deposit =						17665

Summary of year 4

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Month												Tot
	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	
PND1	-25	-24	-80	-148	-204	-223	-24	-240	-211	-172	-116	-65	-1750
PND2	19	42	120	173	203	209	215	210	165	122	82	29	1588
HRV1	9	26	90	138	165	178	183	178	139	98	61	18	1283
Total	3	44	130	164	164	164	155	148	94	48	27	-18	1121
Net	9	26	90	138	165	178	183	178	139	98	61	18	1283

APPENDIX B

**Pond Model Run identical to BASECASE (Appendix A)
but with no recycle of bittern to preconcentration pond.**

This is the set-up for the El Mex pond system without bitterns recycle.
 The Lake is the concentration of the open ocean.
 The line of asterisks may be moved to accomodate more comments.
 Notice that ponds whose names begin with H are assumed to be harvestable.
 The net deposit of the system is summed from these harvestable ponds.

Pond Name	Area (Hect.)	Depth (cm)	Current Target		Ion Weight Percents					Max. Flow (Tons/d)	Rec.	Dsv. Fact.
			Depth (cm)		K	Na	Mg	Cl	SO4			
Lake	0	0	0		0.04	1.05	0.13	1.90	0.26	1000000	0	0.00
PND1	2500	100	100		0.41	7.07	1.75	15.35	2.57	500000	0	0.05
PND2	500	50	50		0.50	7.02	2.16	15.14	3.17	400000	0	0.01
HRV1	400	30	30		0.67	5.73	2.87	14.57	4.20	300000	0	0.00

Ending Conditions File
 Start Conditions From :NO-RCYL.DAT
 Model run covered 5 years.
 Model ran 42 months.
 The first month run was June.
 The last month run was December.
 The evaporation factor was 1.000.
 The precipitation factor was 1.000.

Lake	0	0	0		0.04	1.05	0.13	1.90	0.26	1000000	0.0	0.00
PND1	2500	100	100		0.14	9.66	0.51	16.07	0.92	500000	0.0	0.05
PND2	500	50	50		0.31	8.72	1.12	16.05	1.99	400000	0.0	0.01
HRV1	400	30	30		0.80	5.72	2.98	15.84	5.14	300000	0.0	0.00

El Mex Model Summary File "NO-RCYL"

Evaporation factor is 1.000 Precipitation factor is 1.000

Year = 1 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	102531	1.69	99.9	1.62	-682059
PND2	48.3	72173	2.25	50.0	2.25	207040
HRV1	28.6	49733	3.04	30.0	3.06	169558
Total Monthly Salt Deposit =						-305461
Harvestable Salt Deposit =						169558

Year = 1 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	115867	1.54	99.9	1.47	-658686
PND2	48.1	86140	2.20	50.0	2.15	209769
HRV1	28.3	63706	3.03	30.0	3.00	184189
Total Monthly Salt Deposit =						-264728
Harvestable Salt Deposit =						184189

Year = 1 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	103120	1.41	99.9	1.36	-612504
PND2	48.3	73687	2.10	50.0	2.06	213406
HRV1	28.5	51774	3.00	30.0	3.00	179780
Total Monthly Salt Deposit =						-219319
Harvestable Salt Deposit =						179780

Year = 1 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.3	80494	1.32	99.9	1.28	-494001
PND2	48.7	55382	2.03	50.0	2.00	182023
HRV1	28.9	37588	3.00	30.0	3.00	141611
Total Monthly Salt Deposit =						-170367
Harvestable Salt Deposit =						141611

Year = 1 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.6	53715	1.25	100.0	1.23	-377782
PND2	49.1	36014	1.98	50.0	1.96	136973
HRV1	29.3	23952	2.99	30.0	2.99	99425
Total Monthly Salt Deposit =						-141384
Harvestable Salt Deposit =						99425

Year = 1 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.7	34739	1.21	100.0	1.20	-242854
PND2	49.4	22187	1.96	50.0	1.95	96567
HRV1	29.6	14399	2.99	30.0	3.00	62094
Total Monthly Salt Deposit =						-81193
Harvestable Salt Deposit =						62094

Year = 1 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	13611	1.19	100.0	1.19	-138590
PND2	49.8	8161	1.95	50.0	1.96	44001
HRV1	29.8	5950	2.97	30.0	2.97	18621
Total Monthly Salt Deposit =						-75968
Harvestable Salt Deposit =						18621

Summary of year 1

Months Calculated = June to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	0	0	0	0	0	-682	-659	-613	-494	-378	-243	-139	-3206
PND2	0	0	0	0	0	207	210	213	182	137	97	44	1090
HRV1	0	0	0	0	0	170	184	180	142	99	62	19	855
Total	0	0	0	0	0	-305	-265	-219	-170	-141	-84	-76	-1261
Net	0	0	0	0	0	170	184	180	142	99	62	19	855

Year = 2 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	6831	1.18	100.0	1.18	-53243
PND2	49.9	3043	1.96	50.0	1.97	30664
HRV1	29.9	2090	2.96	30.0	2.96	7911
Total Monthly Salt Deposit =						-14667
Harvestable Salt Deposit =						7911

Year = 2 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.8	14344	1.18	100.0	1.17	-39322
PND2	49.8	6741	1.99	50.0	2.00	55870
HRV1	29.9	3216	3.00	30.0	3.03	25558
Total Monthly Salt Deposit =						42106
Harvestable Salt Deposit =						25558

Year = 2 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.6	45196	1.15	100.0	1.14	-153277
PND2	49.2	28572	1.99	50.0	1.96	135416
HRV1	29.4	17744	3.08	30.0	3.07	88784
Total Monthly Salt Deposit =						70923
Harvestable Salt Deposit =						88784

Year = 2 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.3	73309	1.11	99.9	1.08	-305947
PND2	48.8	47688	1.91	50.0	1.87	196336
HRV1	29.0	30336	3.07	30.0	3.04	138693
Total Monthly Salt Deposit =						29081
Harvestable Salt Deposit =						138693

Year = 2 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.3	81702	1.05	99.9	1.02	-416003
PND2	48.6	52685	1.81	50.0	1.77	225169
HRV1	28.9	32435	3.01	30.0	3.00	167365
Total Monthly Salt Deposit =						-23470
Harvestable Salt Deposit =						167365

Year = 2 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	86503	0.99	99.9	0.96	-431040
PND2	48.5	53939	1.73	50.0	1.70	243305
HRV1	28.9	31258	3.00	30.0	3.00	181097
Total Monthly Salt Deposit =						-6638
Harvestable Salt Deposit =						181097

Year = 2 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	84034	0.94	99.9	0.91	-450019
PND2	48.6	51134	1.67	50.0	1.64	254025
HRV1	29.0	28440	3.00	30.0	3.00	187307
Total Monthly Salt Deposit =						-8687
Harvestable Salt Deposit =						187307

Year = 2 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	99.2	79551	0.89	99.9	0.87	-432142
PND2	48.6	47401	1.61	50.0	1.58	249342
HRV1	29.0	25433	3.00	30.0	3.00	181431
Total Monthly Salt Deposit =						-1370
Harvestable Salt Deposit =						181431

Year = 2 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	99.4	64778	0.85	100.0	0.83	-368156
PND2	48.9	37328	1.57	50.0	1.55	208027
HRV1	29.2	19504	3.00	30.0	3.00	142565
Total Monthly Salt Deposit =						-17564
Harvestable Salt Deposit =						142565

Year = 2 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	99.6	44479	0.82	100.0	0.81	-293426
PND2	49.2	25169	1.54	50.0	1.53	153549
HRV1	29.5	13087	2.99	30.0	2.99	100014
Total Monthly Salt Deposit =						-39863
Harvestable Salt Deposit =						100014

Year = 2 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	99.7	29581	0.80	100.0	0.80	-193163
PND2	49.5	15662	1.53	50.0	1.53	108587
HRV1	29.7	7858	2.99	30.0	3.00	62408
Total Monthly Salt Deposit =						-22168
Harvestable Salt Deposit =						62408

Year = 2 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	99.8	12113	0.80	100.0	0.79	-111880
PND2	49.8	5514	1.53	50.0	1.54	53515
HRV1	29.9	3304	2.98	30.0	2.97	18587
Total Monthly Salt Deposit =						-39777
Harvestable Salt Deposit =						18587

Summary of year 2

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	-53	-39	-153	-306	-416	-431	-450	-432	-368	-293	-193	-112	-3248
PND2	31	56	135	196	225	243	254	249	208	154	109	54	1914
HRV1	8	26	89	139	167	181	187	181	143	100	62	19	1302
Total	-15	42	71	29	-23	-7	-9	-1	-18	-40	-22	-40	-32
Net	8	26	89	139	167	181	187	181	143	100	62	19	1302

Year = 3 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	6964	0.79	100.0	0.79	-46123
PND2	49.9	2099	1.55	50.0	1.56	39437
HRV1	30.0	1161	2.97	30.0	2.97	7812
Total Monthly Salt Deposit =						1127
Harvestable Salt Deposit =						7812

Year = 3 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.8	14228	0.79	100.0	0.79	-37437
PND2	49.8	5299	1.58	50.0	1.59	65813
HRV1	29.9	1786	3.00	30.0	3.02	25683
Total Monthly Salt Deposit =						54059
Harvestable Salt Deposit =						25683

Year = 3 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.6	38753	0.78	100.0	0.77	-127451
PND2	49.3	20727	1.58	50.0	1.56	147647
HRV1	29.6	9855	3.07	30.0	3.07	89404
Total Monthly Salt Deposit =						109600
Harvestable Salt Deposit =						89404

Year = 3 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.3	63066	0.78	100.0	0.75	-248265
PND2	48.9	35667	1.53	50.0	1.50	213329
HRV1	29.3	18292	3.07	30.0	3.04	139345
Total Monthly Salt Deposit =						104410
Harvestable Salt Deposit =						139345

Year = 3 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.3	71430	0.73	100.0	0.72	-346120
PND2	48.8	40785	1.46	50.0	1.43	242759
HRV1	29.2	20541	3.02	30.0	3.00	167946
Total Monthly Salt Deposit =						64586
Harvestable Salt Deposit =						167946

Year = 3 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	76888	0.70	100.0	0.69	-369240
PND2	48.7	42685	1.40	50.0	1.38	260281
HRV1	29.1	19974	3.00	30.0	3.00	181848
Total Monthly Salt Deposit =						72889
Harvestable Salt Deposit =						181848

Year = 3 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	75866	0.68	100.0	0.67	-392905
PND2	48.7	41429	1.35	50.0	1.33	270169
HRV1	29.1	18712	3.00	30.0	3.00	187995
Total Monthly Salt Deposit =						65259
Harvestable Salt Deposit =						187995

Year = 3 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	72632	0.65	100.0	0.64	-383454
PND2	48.7	39088	1.31	50.0	1.30	263560
HRV1	29.2	17102	3.00	30.0	3.00	181993
Total Monthly Salt Deposit =						62100
Harvestable Salt Deposit =						181993

Year = 3 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	59945	0.63	100.0	0.63	-331725
PND2	49.0	31213	1.28	50.0	1.28	219805
HRV1	29.3	13376	3.00	30.0	3.00	142938
Total Monthly Salt Deposit =						31018
Harvestable Salt Deposit =						142938

Year = 3 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.6	41429	0.62	100.0	0.62	-267268
PND2	49.3	21190	1.27	50.0	1.26	161888
HRV1	29.6	9105	2.99	30.0	2.99	100192
Total Monthly Salt Deposit =						-5187
Harvestable Salt Deposit =						100192

Year = 3 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.7	28051	0.61	100.0	0.61	-178946
PND2	49.5	13316	1.27	50.0	1.27	115231
HRV1	29.7	5503	2.99	30.0	3.00	62577
Total Monthly Salt Deposit =						-1138
Harvestable Salt Deposit =						62577

Year = 3 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.8	11704	0.61	100.0	0.61	-103816
PND2	49.8	4398	1.27	50.0	1.28	59234
HRV1	29.9	2191	2.98	30.0	2.98	18483
Total Monthly Salt Deposit =						-26098
Harvestable Salt Deposit =						18483

Summary of year 3

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	-46	-37	-127	-248	-346	-369	-393	-383	-332	-267	-179	-104	-2833
PND2	39	66	148	213	243	260	270	264	220	162	115	59	2059
HRV1	8	26	89	139	168	182	188	182	143	100	63	18	1306
Total	1	54	110	104	65	73	65	62	31	-5	-1	-26	533
Net	8	26	89	139	168	182	188	182	143	100	63	18	1306

Year = 4 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.9	7272	0.61	100.0	0.61	-45459
PND2	49.9	1739	1.29	50.0	1.30	44862
HRV1	30.0	816	2.98	30.0	2.98	7686
Total Monthly Salt Deposit =						7088
Harvestable Salt Deposit =						7686

Year = 4 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.8	14602	0.61	100.0	0.61	-39083
PND2	49.7	4849	1.32	50.0	1.32	71946
HRV1	29.9	1354	3.00	30.0	3.02	25712
Total Monthly Salt Deposit =						58575
Harvestable Salt Deposit =						25712

Year = 4 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.6	36898	0.60	100.0	0.60	-122426
PND2	49.4	18015	1.32	50.0	1.31	154708
HRV1	29.6	7113	3.05	30.0	3.06	89906
Total Monthly Salt Deposit =						122188
Harvestable Salt Deposit =						89906

Year = 4 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.3	58800	0.59	100.0	0.58	-228148
PND2	49.0	30283	1.29	50.0	1.27	222728
HRV1	29.4	12863	3.06	30.0	3.05	139724
Total Monthly Salt Deposit =						134304
Harvestable Salt Deposit =						139724

Year = 4 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.3	66562	0.58	100.0	0.57	-316305
PND2	48.8	34905	1.24	50.0	1.22	252304
HRV1	29.3	14700	3.04	30.0	3.03	167635
Total Monthly Salt Deposit =						103634
Harvestable Salt Deposit =						167635

Year = 4 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	73618	0.56	100.0	0.55	-346732
PND2	48.7	38479	1.20	50.0	1.18	268915
HRV1	29.2	15829	3.01	30.0	3.00	181906
Total Monthly Salt Deposit =						104089
Harvestable Salt Deposit =						181906

Year = 4 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	72428	0.55	100.0	0.54	-372010
PND2	48.7	37074	1.16	50.0	1.14	278686
HRV1	29.2	14347	3.00	30.0	3.00	188299
Total Monthly Salt Deposit =						94975
Harvestable Salt Deposit =						188299

Year = 4 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.2	69679	0.53	100.0	0.53	-364846
PND2	48.8	35301	1.13	50.0	1.12	271195
HRV1	29.3	13303	3.00	30.0	3.00	182277
Total Monthly Salt Deposit =						88627
Harvestable Salt Deposit =						182277

Year = 4 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.4	57853	0.52	100.0	0.52	-317555
PND2	49.0	28343	1.11	50.0	1.11	226379
HRV1	29.4	10496	3.00	30.0	3.00	143131
Total Monthly Salt Deposit =						51955
Harvestable Salt Deposit =						143131

Year = 4 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.5	39932	0.52	100.0	0.51	-256217
PND2	49.3	19121	1.10	50.0	1.10	166725
HRV1	29.6	7036	3.00	30.0	3.00	100178
Total Monthly Salt Deposit =						10687
Harvestable Salt Deposit =						100178

Year = 4 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	99.7	27548	0.51	100.0	0.51	-173318
PND2	49.5	12322	1.10	50.0	1.11	119152
HRV1	29.7	4525	3.00	30.0	3.00	62554
Total Monthly Salt Deposit =						8388
Harvestable Salt Deposit =						62554

Year = 4 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.8	11882	0.51	100.0	0.51	-103358
PND2	49.8	4147	1.11	50.0	1.12	62692
HRV1	29.9	1936	2.98	30.0	2.98	18576
Total Monthly Salt Deposit =						-22090
Harvestable Salt Deposit =						18576

Summary of year 4

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	-45	-39	-122	-228	-316	-347	-372	-365	-318	-256	-173	-103	-2685
PND2	45	72	155	223	252	269	279	271	226	167	119	63	2140
HRV1	8	26	90	140	168	182	188	182	143	100	63	19	1308
Total	7	59	122	134	104	104	95	89	52	11	8	-22	762
Net	8	26	90	140	168	182	188	182	143	100	63	19	1308

APPENDIX C

The El Mex pond run with two salt crystallizers in series
and no bitterns recycle

This is the set-up for the El Mex pond system with two salt ponds in series and no bitterns recycle to pre-concentration ponds.
 The Lake is the concentration of the open ocean.
 The line of asterisks may be moved to accomodate more comments.
 Notice that ponds whose names begin with H are assumed to be harvestable.
 The net deposit of the system is summed from these harvestable ponds.

Pond Name	Area (Hect.)	Depth (cm)	Current Target		Ion Weight Percents				Max. Flow (Tons/d)	Rec.	Salt Dsv. Fact.
			Depth (cm)	K	Na	Mg	Cl	SO4			
Lake	0	0	0	0.04	1.05	0.13	1.90	0.26	1000000	0	0.00
PND1	2500	100	100	0.41	7.07	1.75	15.35	2.57	500000	0	0.05
PND2	500	50	50	0.50	7.02	2.16	15.14	3.17	400000	0	0.01
HRV1	200	30	30	0.67	5.73	2.87	14.57	4.20	300000	0	0.00
HRV2	200	30	30	0.67	5.73	2.87	14.57	4.20	300000	0	0.00

Ending Conditions File
 Start Conditions From :elmex2.dat
 Model run covered 5 years.
 Model ran 42 months.
 The first month run was June.
 The last month run was December.
 The evaporation factor was 1.000.
 The precipitation factor was 1.000.

Lake	0	0	0	0.04	1.05	0.13	1.90	0.26	1000000	0.0	0.00
PND1	2500	100	100	0.14	9.69	0.49	16.07	0.89	500000	0.0	0.05
PND2	500	50	50	0.29	8.84	1.05	16.06	1.87	400000	0.0	0.01
HRV1	200	30	30	0.48	7.70	1.74	15.93	3.69	300000	0.0	0.00
HRV2	200	30	30	0.84	5.57	3.08	15.79	5.39	300000	0.0	0.00

El Mex Model Summary File "two-ponds"
 Evaporation factor is 1.000 Precipitation factor is 1.000

Year = 1 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	126186	1.67	99.8	1.58	-765047
PND2	47.9	96352	2.19	50.0	2.15	196552
HRV1	26.1	84855	2.61	30.0	2.44	89717
HRV2	26.6	73671	2.98	30.0	2.86	85343
Total Monthly Salt Deposit =						-393435
Harvestable Salt Deposit =						175060

Year = 1 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	108935	1.52	99.9	1.45	-674753
PND2	48.2	78782	2.15	50.0	2.10	211874
HRV1	26.8	66638	2.51	30.0	2.47	98548
HRV2	27.3	55208	2.97	30.0	2.94	93195
Total Monthly Salt Deposit =						-271136
Harvestable Salt Deposit =						191743

Year = 1 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	107426	1.39	99.9	1.33	-612509
PND2	48.2	77924	2.06	50.0	1.99	215117
HRV1	26.9	66179	2.45	30.0	2.34	96721
HRV2	27.3	55214	2.96	30.0	2.85	90301
Total Monthly Salt Deposit =						-210370
Harvestable Salt Deposit =						187022

Year = 1 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.3	82149	1.30	100.0	1.25	-504677
PND2	48.6	56858	1.98	50.0	1.92	184228
HRV1	27.7	47020	2.40	30.0	2.30	78506
HRV2	28.1	38051	2.94	30.0	2.83	71285
Total Monthly Salt Deposit =						-170657
Harvestable Salt Deposit =						149792

Year = 1 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.6	50313	1.23	100.0	1.21	-369234
PND2	49.2	32334	1.95	50.0	1.91	140363
HRV1	28.7	25518	2.39	30.0	2.32	56222
HRV2	29.0	19428	2.98	30.0	2.92	49497
Total Monthly Salt Deposit =						-123152
Harvestable Salt Deposit =						105719

Year = 1 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.7	31521	1.19	100.0	1.18	-249432
PND2	49.5	18733	1.92	50.0	1.92	98365
HRV1	29.2	14042	2.37	30.0	2.40	37118
HRV2	29.4	10086	2.99	30.0	3.03	30880
Total Monthly Salt Deposit =						-83068
Harvestable Salt Deposit =						67999

Year = 1 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.9	9565	1.18	100.0	1.17	-110570
PND2	49.8	3961	1.94	50.0	1.95	44924
HRV1	29.8	2229	2.45	30.0	2.48	13833
HRV2	29.9	1172	3.07	30.0	3.10	8314
Total Monthly Salt Deposit =						-43499
Harvestable Salt Deposit =						22147

Summary of year 1

Months Calculated = June to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	0	0	0	0	0	-765	-675	-613	-505	-369	-249	-111	-3286
PND2	0	0	0	0	0	197	212	215	184	140	98	45	1091
HRV1	0	0	0	0	0	90	99	97	79	56	37	14	471
HRV2	0	0	0	0	0	85	93	90	71	49	31	8	429
Total	0	0	0	0	0	-393	-271	-210	-171	-123	-83	-43	-1295
Net	0	0	0	0	0	175	192	187	150	106	68	22	899

Year = 2 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.9	8882	1.17	100.0	1.17	-53260
PND2	49.9	5136	1.96	50.0	1.96	30764
HRV1	29.8	4173	2.48	30.0	2.47	8039
HRV2	29.8	3832	3.07	30.0	3.04	3071
Total Monthly Salt Deposit =						-11386
Harvestable Salt Deposit =						11110

Year = 2 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.8	18540	1.16	100.0	1.15	-60070
PND2	49.7	10957	1.96	50.0	1.96	56265
HRV1	29.6	8565	2.48	30.0	2.48	17846
HRV2	29.7	6899	3.05	30.0	3.05	12310
Total Monthly Salt Deposit =						26351
Harvestable Salt Deposit =						30156

Year = 2 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.6	49379	1.13	100.0	1.11	-201603
PND2	49.2	32599	1.91	50.0	1.89	136387
HRV1	28.7	26375	2.39	30.0	2.40	51973
HRV2	28.9	20884	3.00	30.0	3.06	44998
Total Monthly Salt Deposit =						31756
Harvestable Salt Deposit =						96972

Year = 2 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.3	74744	1.08	100.0	1.06	-320324
PND2	48.7	48761	1.83	50.0	1.81	198982
HRV1	28.0	38871	2.31	30.0	2.32	79694
HRV2	28.4	30065	2.98	30.0	3.03	70094
Total Monthly Salt Deposit =						28446
Harvestable Salt Deposit =						149788

Year = 2 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.3	79987	1.03	99.9	1.00	-407970
PND2	48.6	50612	1.78	50.0	1.74	228812
HRV1	27.9	39284	2.26	30.0	2.27	94036
HRV2	28.4	29106	2.99	30.0	3.05	83508
Total Monthly Salt Deposit =						-1613
Harvestable Salt Deposit =						177545

Year = 2 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	86913	0.97	99.9	0.95	-432184
PND2	48.5	54112	1.68	50.0	1.67	245574
HRV1	27.8	41424	2.19	30.0	2.22	101953
HRV2	28.3	30055	2.98	30.0	3.05	90445
Total Monthly Salt Deposit =						5788
Harvestable Salt Deposit =						192398

Year = 2 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	86270	0.92	99.9	0.89	-456269
PND2	48.5	53218	1.62	50.0	1.59	255480
HRV1	27.8	40452	2.13	30.0	2.13	106226
HRV2	28.4	29087	2.96	30.0	2.99	93767
Total Monthly Salt Deposit =						-797
Harvestable Salt Deposit =						199993

Year = 2 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	84597	0.87	100.0	0.85	-439022
PND2	48.6	52418	1.56	50.0	1.51	249848
HRV1	27.8	40036	2.08	30.0	1.99	103541
HRV2	28.4	29085	2.95	30.0	2.83	90982
Total Monthly Salt Deposit =						5349
Harvestable Salt Deposit =						194523

Year = 2 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.3	67058	0.83	100.0	0.81	-374445
PND2	48.8	39450	1.51	50.0	1.47	209615
HRV1	28.4	29013	2.05	30.0	1.94	84116
HRV2	28.8	20059	2.95	30.0	2.79	71540
Total Monthly Salt Deposit =						-9175
Harvestable Salt Deposit =						155656

Year = 2 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.6	42864	0.80	100.0	0.79	-310251
PND2	49.3	23270	1.48	50.0	1.47	155471
HRV1	29.0	15921	2.01	30.0	2.00	60561
HRV2	29.4	9718	2.91	30.0	2.90	50504
Total Monthly Salt Deposit =						-43715
Harvestable Salt Deposit =						111065

Year = 2 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.7	33001	0.79	100.0	0.78	-203695
PND2	49.4	19010	1.47	50.0	1.45	109643
HRV1	29.2	14001	2.02	30.0	1.95	40575
HRV2	29.4	10088	2.93	30.0	2.83	31573
Total Monthly Salt Deposit =						-21904
Harvestable Salt Deposit =						72148

Year = 2 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.9	10365	0.78	100.0	0.77	-118938
PND2	49.8	3495	1.46	50.0	1.47	55221
HRV1	29.9	1274	2.01	30.0	2.05	17747
HRV2	29.9	0	2.88	30.0	2.93	9984
Total Monthly Salt Deposit =						-35986
Harvestable Salt Deposit =						27731

Summary of year 2

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	-53	-60	-202	-320	-408	-432	-456	-439	-374	-310	-204	-119	-3378
PND2	31	56	136	199	229	246	255	250	210	155	110	55	1932
HRV1	8	18	52	80	94	102	106	104	84	61	41	18	766
HRV2	3	12	45	70	84	90	94	91	72	51	32	10	653
Total	-11	26	32	28	-2	6	-1	5	-9	-44	-22	-36	-27
Net	11	30	97	150	178	192	200	195	156	111	72	28	1419

Year = 3 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.9	6980	0.77	100.0	0.77	-44478
PND2	49.9	1937	1.49	50.0	1.50	40810
HRV1	29.9	516	2.09	30.0	2.12	11328
HRV2	30.0	0	2.95	30.0	2.97	4031
Total Monthly Salt Deposit =						11691
Harvestable Salt Deposit =						15359

Year = 3 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.8	14150	0.77	100.0	0.77	-38196
PND2	49.8	4996	1.51	50.0	1.53	67302
HRV1	29.8	2138	2.18	30.0	2.23	20777
HRV2	29.9	377	3.03	30.0	3.09	12452
Total Monthly Salt Deposit =						62335
Harvestable Salt Deposit =						33229

Year = 3 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.5	49403	0.76	100.0	0.75	-175663
PND2	49.1	31399	1.47	50.0	1.44	148593
HRV1	28.7	24894	2.04	30.0	1.96	55814
HRV2	29.0	19445	2.91	30.0	2.84	46177
Total Monthly Salt Deposit =						74920
Harvestable Salt Deposit =						101991

Year = 3 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.3	66837	0.74	99.9	0.72	-259530
PND2	48.8	39138	1.43	49.9	1.37	217507
HRV1	28.4	28807	2.00	30.0	1.84	84102
HRV2	28.8	20051	2.95	29.9	2.74	70601
Total Monthly Salt Deposit =						112680
Harvestable Salt Deposit =						154703

Year = 3 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.3	63846	0.71	100.0	0.70	-354568
PND2	48.9	32380	1.37	50.0	1.38	245669
HRV1	28.7	20302	1.94	30.0	2.02	98754
HRV2	29.2	9727	2.93	30.0	3.11	84906
Total Monthly Salt Deposit =						74762
Harvestable Salt Deposit =						183660

Year = 3 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	79276	0.68	100.0	0.67	-380658
PND2	48.6	44763	1.32	50.0	1.32	262302
HRV1	28.1	31533	1.87	30.0	1.96	106657
HRV2	28.7	20036	2.90	30.0	3.08	91886
Total Monthly Salt Deposit =						80187
Harvestable Salt Deposit =						198542

Year = 3 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	78882	0.66	100.0	0.65	-408204
PND2	48.6	44192	1.28	50.0	1.27	271626
HRV1	28.2	30889	1.83	30.0	1.89	110867
HRV2	28.7	19385	2.89	30.0	3.03	95198
Total Monthly Salt Deposit =						69487
Harvestable Salt Deposit =						206065

Year = 3 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	77110	0.63	100.0	0.62	-400242
PND2	48.6	43403	1.24	50.0	1.22	264381
HRV1	28.2	30500	1.79	30.0	1.79	107843
HRV2	28.8	19399	2.88	30.0	2.90	92323
Total Monthly Salt Deposit =						64306
Harvestable Salt Deposit =						200166

Year = 3 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.4	59301	0.61	100.0	0.61	-341665
PND2	49.0	30188	1.21	50.0	1.22	222143
HRV1	28.7	19194	1.78	30.0	1.85	87885
HRV2	29.2	10045	2.91	30.0	3.05	72279
Total Monthly Salt Deposit =						40642
Harvestable Salt Deposit =						160164

Year = 3 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.5	43910	0.60	100.0	0.60	-282288
PND2	49.2	23493	1.19	50.0	1.20	163000
HRV1	29.0	15888	1.75	30.0	1.82	63388
HRV2	29.4	9707	2.86	30.0	3.00	51275
Total Monthly Salt Deposit =						-4626
Harvestable Salt Deposit =						114663

Year = 3 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.7	34076	0.59	100.0	0.59	-200564
PND2	49.4	19317	1.18	50.0	1.17	116051
HRV1	29.2	14044	1.75	30.0	1.72	43211
HRV2	29.4	10118	2.86	30.0	2.80	32498
Total Monthly Salt Deposit =						-8803
Harvestable Salt Deposit =						75709

Year = 3 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.8	11362	0.59	100.0	0.59	-110039
PND2	49.8	3781	1.18	50.0	1.19	61170
HRV1	29.8	1310	1.76	30.0	1.81	19876
HRV2	29.9	0	2.84	30.0	2.88	10335
Total Monthly Salt Deposit =						-18658
Harvestable Salt Deposit =						30211

Summary of year 3

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Month												Tot
	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	
PND1	-44	-38	-176	-260	-355	-381	-408	-400	-342	-282	-201	-110	-2996
PND2	41	67	149	218	246	262	272	264	222	163	116	61	2081
HRV1	11	21	56	84	99	107	111	108	88	63	43	20	811
HRV2	4	12	46	71	85	92	95	92	72	51	32	10	664
Total	12	62	75	113	75	80	69	64	41	-5	-9	-19	559
Net	15	33	102	155	184	199	206	200	160	115	76	30	1474

Year = 4 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.9	7989	0.59	100.0	0.59	-49045
PND2	49.9	2238	1.20	50.0	1.21	46659
HRV1	29.9	559	1.84	30.0	1.87	13462
HRV2	30.0	0	2.91	30.0	2.92	4402
Total Monthly Salt Deposit =						15478
Harvestable Salt Deposit =						17864

Year = 4 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.8	15154	0.58	100.0	0.58	-44086
PND2	49.7	5103	1.23	50.0	1.24	73987
HRV1	29.8	1914	1.92	30.0	1.96	23285
HRV2	29.9	94	2.99	30.0	3.04	12933
Total Monthly Salt Deposit =						66119
Harvestable Salt Deposit =						36218

Year = 4 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.6	41439	0.58	100.0	0.57	-159141
PND2	49.3	22305	1.20	50.0	1.21	156692
HRV1	29.1	15382	1.82	30.0	1.87	58250
HRV2	29.4	9762	2.89	30.0	3.01	46520
Total Monthly Salt Deposit =						102321
Harvestable Salt Deposit =						104770

Year = 4 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.3	68089	0.57	100.0	0.56	-245670
PND2	48.8	39406	1.17	50.0	1.13	224316
HRV1	28.3	28806	1.77	30.0	1.62	87201
HRV2	28.8	20067	2.91	30.0	2.67	71654
Total Monthly Salt Deposit =						137501
Harvestable Salt Deposit =						158855

Year = 4 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.3	64899	0.55	100.0	0.55	-343593
PND2	48.9	32619	1.13	50.0	1.12	255287
HRV1	28.6	20260	1.69	30.0	1.69	102080
HRV2	29.2	9702	2.84	30.0	2.87	86111
Total Monthly Salt Deposit =						99885
Harvestable Salt Deposit =						188190

Year = 4 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	71115	0.54	100.0	0.53	-349381
PND2	48.7	35361	1.11	50.0	1.11	272752
HRV1	28.5	21682	1.69	30.0	1.76	109403
HRV2	29.1	10051	2.92	30.0	3.10	91726
Total Monthly Salt Deposit =						124499
Harvestable Salt Deposit =						201129

Year = 4 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	79912	0.53	100.0	0.52	-396031
PND2	48.6	44432	1.07	50.0	1.05	278893
HRV1	28.1	30864	1.61	30.0	1.59	114002
HRV2	28.7	19380	2.82	30.0	2.80	96587
Total Monthly Salt Deposit =						93451
Harvestable Salt Deposit =						210589

Year = 4 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.2	69196	0.51	100.0	0.51	-378660
PND2	48.8	34372	1.05	50.0	1.05	273669
HRV1	28.5	21014	1.61	30.0	1.64	110486
HRV2	29.1	9710	2.87	30.0	2.97	92480
Total Monthly Salt Deposit =						97976
Harvestable Salt Deposit =						202966

Year = 4 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.3	60253	0.50	100.0	0.50	-334003
PND2	48.9	30445	1.03	50.0	1.03	227960
HRV1	28.7	19192	1.59	30.0	1.64	90473
HRV2	29.2	10042	2.86	30.0	2.98	73138
Total Monthly Salt Deposit =						57568
Harvestable Salt Deposit =						163611

Year = 4 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.5	44632	0.50	100.0	0.49	-280139
PND2	49.2	23700	1.01	50.0	1.01	167509
HRV1	29.0	15911	1.56	30.0	1.57	65333
HRV2	29.3	9738	2.81	30.0	2.82	51907
Total Monthly Salt Deposit =						4610
Harvestable Salt Deposit =						117240

Year = 4 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.7	25393	0.49	100.0	0.49	-167869
PND2	49.5	9793	1.02	50.0	1.04	121458
HRV1	29.6	4156	1.64	30.0	1.70	44327
HRV2	29.8	63	2.95	30.0	3.07	31392
Total Monthly Salt Deposit =						29308
Harvestable Salt Deposit =						75719

Year = 4 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	99.8	12468	0.49	100.0	0.49	-99175
PND2	49.8	4553	1.04	50.0	1.05	64226
HRV1	29.8	2074	1.72	30.0	1.74	20241
HRV2	29.9	1056	3.08	30.0	3.08	8343
Total Monthly Salt Deposit =						-6365
Harvestable Salt Deposit =						28584

Summary of year 4

Months Calculated = January to December

Deposit in thousands of tons.

	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
Pond													
PND1	-49	-44	-159	-246	-344	-349	-396	-379	-334	-280	-168	-99	-2847
PND2	47	74	157	224	255	273	279	274	228	168	121	64	2163
HRV1	13	23	58	87	102	109	114	110	90	65	44	20	839
HRV2	4	13	47	72	86	92	97	92	73	52	31	8	667
Total	15	66	102	138	100	124	93	98	58	5	29	-6	922
Net	18	36	105	159	188	201	211	203	164	117	76	29	1506

APPENDIX D

Pond Model

ELMEXMOD

Source Code

program ElMexModel;

{ Version 1.01, October 31, 1989. The program ElMexMod is a model which simulates salt production in solar ponds given the weather conditions at the El Nasr Salines Co. El Mex site. The evaporation data and the control point for the system are internally set in the program and can't be changed without recompiling the program. The only input to the program is the input data file and user supplied information. Version 1.01 update allows the user to use any editor desired by renaming the editor ELMEXED with the same extension as the original program had.

The basic operation of the program follows:

1. A GSL header is displayed with the version of the program.
2. The program requests the name of a data file for system setup. This file sets up the pond system. Certain conventions are used in the set up. These are explained later. After the data is read it is displayed and the user has the option of changing the data.
3. Next the program requests information for the specific run.
4. The program calculates the current run. The program calculates each pond each day. The calculational procedure for each day is to begin with the last pond. The evaporation is determined for the pond through the evaporation data. The flow from the last pond is determined by looking at a control point. The recycle flow is set to the brine flowing from the last pond. Once the outflow is known a material balance is done by assuming no inflow. The balance is iterative on the amount of salt deposited. Once the resulting Na material balance matches what the equilibrium Na value should be within the tolerance the balance is completed. New weight percents are calculated for all ions from the material by a material balance on each ion. Next a flow required to keep the pond at a target level is calculated. This flow is mixed with the brine that was remaining in the pond. The daily statistics are for the pond are recorded and the calculation proceeds to the next pond. This is done each day of each month of each year for the duration of the run.
5. At the end of each day the program will print a material balance file if the user has requested it. Otherwise, the records are kept to be printed at the end of each month and year.
6. At the completion of the loops through the ponds, days, month and years the statistics files are closed and the program requests a file name for the ending conditions file. This file is kept so an additional run can be made to continue the current simulation. After this file is written the program terminates.

Notes for Turbo Pascal programmers: This program has been compiled in Turbo Pascal Version 5.5. The program was written to be compatible with any type of display unit and any type of PC based hardware. The program doesn't require the use of a numeric coprocessor but it will use it if available. This is accomplished through the use of the compiler directives \$E and \$N. The \$M directive allows the program to open an external editing program while running.

There are three units used by the program; the two standard units dos and crt and a unit called StrUnit. StrUnit manipulates and generates string variables. For the program to compile the compiler must locate the StrUnit.TPU file as well as the .TPU files for both dos and crt.

The program is straight forward in the method of programming. Simple procedures used throughout the program are the first procedures to be listed. The procedure BalancePond does the bulk of the calculational portion of the program. BalancePond has the sub procedures which take care of determining the flow from the last pond (LastPondFlowOut), maintaining the target level in each pond (AdjustLevel) and determining the ion weight percents (Chem). All calculations are done in metric tons and weight percents. Record variables are used liberally to facilitate programming.

This program was written by Dave Butts and Chad McCleary of
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Ogden, Utah
84402

Tel. 801-731-3100 }

```
{SM 8192,0,0}                                { Leave memory for child process. }
{SE+}                                         { Emulation processor switch. }
{SN+}                                         { Numeric processor switch. }
uses dos, crt, StrUnit;

const
  MaxPonds = 15;
  MaxMonths = 100;
  Editor = 'ELMEXED ';
  delayvalue = 100;
  bell = #7;
  ProgramVersion = 1.01;

{ The evaporation data is the monthly evaporation expressed as tons per
  hectare per month. Likewise, the rain is expressed as tons per hectare
  per month. The evapdat array contains the constants to make functional
  (linear) evaporation calculations based on the weight percent magnesium. }

evapdat: ARRAY[1..13, 1..4] OF REAL =
  { Inter. Slope Rain Days }
  (( 805.0, 115.0, 410.0, 31), { January }
  ( 956.0, 129.5, 390.0, 28), { February }
  ( 1167.0, 144.0, 110.0, 31), { March }
  ( 1533.0, 181.0, 20.0, 30), { April }
  ( 1700.0, 181.0, 0.0, 31), { May }
  ( 1810.0, 187.0, 0.0, 30), { June }
  ( 1810.0, 187.0, 0.0, 30), { July }
  ( 1810.0, 187.0, 0.0, 31), { August }
  ( 1533.0, 181.0, 10.0, 30), { September }
  ( 1167.0, 144.0, 50.0, 31), { October }
  ( 956.0, 129.5, 140.0, 30), { November }
  ( 805.0, 115.0, 340.0, 30), { December }
  (15730.0, 1777.0, 1470.0, 365)); { Year }

MonthNames : array[1..12] of string[9] = { Names of the months. }
  ('January', 'February', 'March', 'April',
  'May', 'June', 'July', 'August',
  'September', 'October', 'November', 'December');

MonthDays : array[1..12, 1..3] of integer = { Ordinal days of the months. }
  { FirstDay LastDay Counter }
  (( 1, 31, 1),
  ( 32, 59, 2),
  ( 60, 90, 3),
  ( 91, 120, 4),
  ( 121, 151, 5),
  ( 152, 181, 6),
  ( 182, 212, 7),
  ( 213, 243, 8),
  ( 244, 273, 9),
  ( 274, 304, 10),
  ( 305, 334, 11),
  ( 335, 365, 12));
```

```
{ Molecular Weights of the Ions }
MW: array[1..6] of real =
  ( 39.0938*2, { K2 }
    22.98977*2, { Na2 }
    24.305,     { Mg }
    35.453*2,  { Cl2 }
    96.0596,   { SO4 }
    18.0152 ); { H2O }
```

```
{ These values control the convergence for pond balancing. }
MaxIterations = 100;
Tol = 0.0000000001;
```

type

```
PondRecord = RECORD
```

```
  Name       : STRING[4];
  Area       : REAL;
  Depth      : REAL;
  TargetDepth : REAL;
  Inventory  : REAL;
  K          : REAL;
  Na         : REAL;
  Mg         : REAL;
  Cl         : REAL;
  SO4        : REAL;
  MaxFlow    : REAL;
  Recycle    : REAL;
  OutFlow    : REAL;
  SDFact     : REAL;
```

```
end;
```

```
PondData = array[0.. MaxPonds] of PondRecord;
```

```
MonthRecord = RECORD
```

```
  Name       : STRING;
  FirstDay   : INTEGER;
  LastDay    : INTEGER;
  Counter    : INTEGER;
```

```
end;
```

```
MonthInfo = array[1..12] of MonthRecord;
```

```
DayStatRecord = RECORD
```

```
  BeginningInventory : REAL;
  Mg0                : REAL;
  Na0                : REAL;
  InFlow             : REAL;
  Mg1                : REAL;
  Na1                : REAL;
  Recycle            : REAL;
  Mg2                : REAL;
  Na2                : REAL;
  EndingInventory    : REAL;
  Mg3                : REAL;
  Na3                : REAL;
  OutFlow            : REAL;
  Evaporation        : REAL;
  SaltDeposit        : REAL;
```

```
end;
```

```
DayStats = array[0.. MaxPonds] of DayStatRecord;
```

```

MonthStatRecord = RECORD
  DailyDepthSum      : REAL;
  DailyOutFlowSum    : REAL;
  DailyMgSum         : REAL;
  EndingDepth       : REAL;
  EndingMg          : REAL;
  DailySaltDepositSum : REAL;
end;
MonthStats = array[0..MaxPonds] of MonthStatRecord;

var
  Command: STRING[127];           { String for executing dos commands. }

  { RECORD Variables }
  MonthData : MonthStats;           { The monthly statistics. }
  DayData   : DayStats;            { The daily material balance statistics. }
  Months    : MonthInfo;           { The record of month data. }
  Ponds     : PondData;            { The array of pond information. }
  { The Yearly Statistics }
  YearData : array[1..12, 1..MaxPonds] of REAL;

  { File Name Variables }
  InFileName,           { Pond system initial condition file name. }
  BalOutFileName,      { Daily material balance file name. }
  OutFileName,         { Monthly and yearly summary file name. }
  EndingFileName : STRING;      { Ending conditions file name. }

  { File Variables for OutPut }
  BalOutFile,           { Daily material balance file. }
  OutFile : TEXT;      { Monthly and yearly summary file. }

  { Various Input and Output Variables }
  InChar : CHAR;
  DisplayDay,
  InString: STRING;

  { Counter Variables }
  i, j, InVal, CodeVar,
  Pond, LastPond,
  Day, BeginDay, BeginningDay, DaysRun, FirstMonth, LastMonth,
  Month, BeginMonth, EndMonth, MonthsRun, NumberOfMonths,
  Year, NumberOfYears: INTEGER;
  PreviousOutFlow, PreviousMg : REAL;

  { Balance Variables }
  Tr, Kr, Mgr, Nar, Clr, SO4r: REAL;      { The recycle flow and weight %. }
  Tin, Kin, Main, Mgin, Clin, SO4in: REAL; { The flow into the pond. }
  Tout, Tb, Kb, Nab, Mgb, Clb, SO4b: REAL; { The beginning inventory. }
  Tf, Kf, Naf, Mgf, Clf, SO4f, H2O: REAL; { The values calculated in Chem. }
  W, EvapFact, PrecipFact : REAL;        { The evaporation for the pond. }
  Cp, CpRange : REAL;                    { Last pond flow controls. }
  iotest : INTEGER; { Input Output checking flag. }

  { Flags for controlling Calculations, Printing and Reading }
  FirstDay, MonthPrn, BalancePrint, ReadFile, EvapChanged,
  ControlChanged: BOOLEAN;

procedure WaitForEnter;

  { The procedure WaitForEnter displays a prompt
  on the screen, and waits for the user to press
  the Enter key }

begin
  writeln;                                     { WaitForEnter }
  write ('Press <Enter> to continue. ');
  readln;
  writeln;
end;                                           { WaitForEnter }

```

```

function Density( x : REAL) : REAL;

    { The Density function calculates the density of a
      brine given the weight percent Mg++ in the brine.
      The value returned is tons per cubic meter. }

begin;
    if x <= 0.0 then
        begin
            gotoxy ( 10, 15);
            writeln ('The value of x in density function is ',x:6:2);
            write ('What is a valid value for x in pond ',Ponds[Pond].Name,' ?');
            readln (x);
            end;
        Density := 1.1788 * EXP( LN (x) * 0.0695);
    end;
    { Density }

procedure GSLHeader;
    { The GSLHeader program clears the screen and displays the GSL
      Solar Consultants and Advisors logo.
      The program uses the following procedures from the CRT unit:
      CLRSCR
      gotoxy }

begin;
    clrscr;
    TextColor (15);
    gotoxy (18, 3);
    write ('      GGG          SSS          LLLL');
    gotoxy (18, 4);
    write ('  GGGGGGGGG      SSSSSSSSS      LLLL');
    gotoxy (18, 5);
    write (' GGGG  GGGG  SSSS  SSSS  LLLL');
    gotoxy (18, 6);
    write ('GGGG      GGGG  SSSS          LLLL');
    gotoxy (18, 7);
    write ('GGGG          SSSS          LLLL');
    gotoxy (18, 8);
    write ('GGGG          SSSS          LLLL');
    gotoxy (18, 9);
    write ('GGGG          SSSS          LLLL');
    gotoxy (18, 10);
    write ('GGGG  GGGGGG          SSSS          LLLL');
    gotoxy (18, 11);
    write ('GGGG  GGGG          SSSS          LLLL');
    gotoxy (18, 12);
    write (' GGGG  GGGG  SSSS  SSSS  LLLL');
    gotoxy (18, 13);
    write ('  GGGGGGGGG      SSSS  SSSS  LLLLLLLLLLLLLL');
    gotoxy (18, 14);
    write ('      GGGG          SSSSSSS      LLLLLLLLLLLLLL');
    gotoxy (18, 16);
    write ('          SOLAR CONSULTANTS and ADVISORS');
    gotoxy (18, 17);
    write ('          El Max Model Version ',ProgramVersion:4:2);
    writeln;
    WaitForEnter;
end;
    { GSLHeader }

```

```
procedure Input;
```

```
{ Procedure Input begins by loading the Months record with the names, first days, last days and month number of each month. The procedure then goes on to reading a data file which contains the initial conditions for the pond system. If the boolean variable is set to TRUE the procedure requests a file name for reading. Otherwise it reads the current file. The procedure returns the number of ponds in the system and the name of the file read. The read section skips over all lines up to and including a line of 40 asterisks, (*). This line signals the beginning of the data section. }
```

```
var
```

```
FileStart : STRING[30]; { String flag in the to signal read start. }  
tempStart : STRING[6];  
InFile : TEXT; { Data file name. }  
j : INTEGER;
```

```
procedure ChangeEvapControl;
```

```
{ This procedure allows the user to change the evaporation and/or the control point data of the system. There are two sub procedures, ChangeEvap and ChangeControl. }
```

```
type
```

```
charsetType = SET OF CHAR;
```

```
var
```

```
MenuChars : charsetType;
```

```
procedure ChangeEvap;
```

```
begin
```

```
{ ChangeEvap }
```

```
clrscr;
```

```
gotoxy (10, 10);
```

```
write ('You've selected change the evaporation data.');
```

```
gotoxy (10, 11);
```

```
write ('Do you want to continue? ');
```

```
InChar := upcase(readkey);
```

```
write (InChar);
```

```
delay (delayvalue);
```

```
while InChar = 'Y' do
```

```
begin
```

```
EvapChanged := True;
```

```
gotoxy (10, 11);
```

```
clreol;
```

```
write ('What month to change the data for? Numbers only. ');
```

```
readln (Month);
```

```
gotoxy (10, 11);
```

```
clreol;
```

```
write ('Changing evaporation data for ',Months[Month].Name);
```

```
gotoxy (10, 12);
```

```
clreol;
```

```
write ('What is the intercept for ',Months[Month].Name,'? ');
```

```
readln (EvapDat [Month, 1]);
```

```
gotoxy (10, 13);
```

```
clreol;
```

```
write ('What is the slope for ',Months[Month].Name,'? ');
```

```
readln (EvapDat [Month, 2]);
```

```
gotoxy (10, 14);
```

```
clreol;
```

```
write ('What is the rain for ',Months[Month].Name,'? ');
```

```
readln (EvapDat [Month, 3]);
```

```
gotoxy (10, 15);
```

```
clreol;
```

```
write ('Do you want to change another? ');
```

```
InChar := upcase(readkey);
```

```
write (InChar);
```

```
delay (delayvalue);
```

```
end;
```

```
end;
```

```
{ ChangeEvap }
```

```

procedure ChangeControl;
begin
    ControlChanged := True;
    clrscr;
    gotoxy (10, 10);
    write ('You've selected change the control point. ');
    gotoxy (10, 11);
    write ('The current control point is ', Cp:4:2, '. ');
    gotoxy (10, 12);
    write ('The current control range is ', CpRange:4:2, '. ');
    repeat
        begin
            gotoxy (10, 15);
            clreol;
            gotoxy (10, 13);
            clreol;
            write ('What is the new control point? ');
            readln (Cp);
            gotoxy (10, 14);
            clreol;
            write ('What is the new control range? ');
            readln (CpRange);
            gotoxy (10, 15);
            write ('Are these values correct? ');
            InChar := upcase(readkey);
            write (InChar);
            delay (delayvalue);
        end;
    until InChar = 'Y';

end;
{ ChangeControl }

begin
    MenuChars := ['E', 'C', 'B', 'N'];
    clrscr;
    gotoxy (10, 10);
    write ('The change flag was detected while reading ', InFileName, '. ');
    gotoxy (10, 11);
    write ('Do you want to change <E>vaporation data ');
    gotoxy (10, 12);
    write ('                <C>ontrol point data ');
    gotoxy (10, 13);
    write ('                <B>oth ');
    gotoxy (10, 14);
    write ('                <N>othing ');
    repeat
        begin
            gotoxy (10, 15);
            clreol;
            write ('Enter the first letter of your choice ');
            InChar := upcase(readkey);
            write (InChar);
            delay (delayvalue);
        end;
    until InChar in MenuChars;
    if InChar = 'E' then ChangeEvap;
    if InChar = 'C' then ChangeControl;
    if InChar = 'B' then
        begin
            ChangeControl;
            ChangeEvap;
        end;
    InChar := 'N';

end;
{ ChangeEvapControl }

```

```

begin
                                                    { Input }

for i := 1 to 12 do
    begin
        with Months[i] do
            begin
                Name := MonthNames[i];
                FirstDay := MonthDays[i, 1];
                LastDay := MonthDays[i, 2];
                Counter := MonthDays[i, 3];
            end;
        end;
    repeat
        begin
            if ReadFile then
                begin
                    repeat
                        begin
                            clrscr;
                            gotoxy (5, 10);
                            write ('What INPUT data file do you want to read? ');
                            readln (InFileName);
                            gotoxy(5, 11);
                            write ('Read input file ',InFileName,' OK? ');
                            InChar := upcase(readkey);
                            writeln (InChar);
                            delay (delayvalue);
                        end;
                    until InChar = 'Y';
                end;
                assign (InFile, InFileName);      { Open the input file for reading. }
            reset (InFile);
        end;
        {SI-}
        {SI+}
        iotest := ioreult;
        if iotest <> 0 then
            begin
                writeln (InFileName,' wasn''t found. Try again.');
```

..

```

                WaitForEnter;
            end;
        until iotest = 0;
    repeat
        readln (InFile, tempStart, FileStart);
        until FileStart = '*****';
        if tempStart = 'CHANGE' then ChangeEvapControl;
        i := 0;
    while not eof (InFile) do
        begin
            with Ponds[ i ] DO
                begin
                    readln (InFile, Name,
                        Area,
                        Depth,
                        TargetDepth,
                        K,
                        Na,
                        Mg,
                        Cl,
                        SO4,
                        MaxFlow,
                        Recycle,
                        SDFact);
                end;
                inc(i);
            end;
        close (InFile);
        LastPond := i - 1;
    } Begin reading the data. }

```

```

if LastPond > MaxPonds then
  begin
    gotoxy (10, 20);
    writeln ('Maximum number of ponds is limited to ',MaxPonds:3,'. ');
    writeln (InFileName, ' has ',LastPond:3,' ponds. ');
    writeln ('Please check your input data. ');
    WaitForEnter;
    Input;
  end;
Ponds[0].Inventory := 0.0;           { Calculate the inventory for each pond. }
for i := 0 TO LastPond DO
  begin
    with Ponds[i] DO
      begin
        Inventory := Area * Depth * 100.0 * Density(Mg);
      end;
    end;
end;
                                                                    { Input }

procedure WriteEndingConditionsFile;
{ This procedure writes the ending conditions to a file that can be used as
  the starting file for another run. }

var
  EndingFile : text;

begin
                                                                    { WriteEndingConditionsFile }
  repeat
    begin
      write (bell);
      gotoxy (10, 20);
      clrEOL;
      write ('What file do you want the ending conditions written to? ');
      readln (EndingFileName);
      gotoxy (10, 21);
      clrEOL;
      write ('Write ending conditions to ',EndingFileName,'. OK? ');
      InChar := upcase(readkey);
      write (InChar);
      delay (delayvalue);
    end;
  until InChar = 'Y';
  assign (EndingFile, EndingFileName);
  rewrite (EndingFile);
  writeln (EndingFile, 'Ending Conditions File');
  writeln (EndingFile, 'Start Conditions From :',InFileName);
  writeln (EndingFile, 'Model run covered ',NumberOfYears:2,' years. ');
  writeln (EndingFile, 'Model ran ',NumberOfMonths,' months. ');
  writeln (EndingFile, 'The first month run was ',Months[FirstMonth].Name,
    '. ');
  writeln (EndingFile, 'The last month run was ',Months[LastMonth].Name, '. ');
  writeln (EndingFile, 'The evaporation factor was ',EvapFact:5:3,'. ');
  writeln (EndingFile, 'The precipitation factor was ',PrecipFact:5:3,'. ');
  writeln (EndingFile, '*****',
    '*****');
  for Pond := 0 to LastPond do
    begin
      with Ponds[Pond] do
        begin
          writeln (EndingFile, Name, ' ', round(Area):5, ' ', round(Depth):4, ' ',
            round(TargetDepth):4, ' ', K:6:2, Na:6:2, Mg:6:2, Cl:6:2,
            SO4:6:2, MaxFlow:9:0, ' ', Recycle:3:1, ' ', SDFact:4:2);
        end;
      end;
    close (EndingFile);
  end;
                                                                    { WriteEndingConditionsFile }
end;

```



```
function Evap : REAL;
```

```
{ The Evap function calculates the evaporation
  at the El Max site for a given Mg weight percent and a
  given month. The evaporation is expressed in tons per
  hectare per day. This evaporation function can be
  modified by changing the constant array, evapdat}
```

```
var
```

```
  x, a, b, rain, days: REAL;
```

```
begin
```

```
{ Evap }
```

```
  x := Ponds[Pond].Mg;
```

```
  a := evapdat[month, 1];
```

```
  b := evapdat[month, 2];
```

```
  rain := evapdat[month, 3];
```

```
  days := evapdat[month, 4];
```

```
  Evap := ((a - b * x) * EvapFact - rain * PrecipFact) / days;
```

```
end;
```

```
{ Evap }
```

```
procedure ShowData;
```

```
{ Procedure ShowData displays the pond data that has been read and asks the
  user to confirm that the data is correct. If the user signals an error in
  the pond data ShowData asks if a new file should be read or if editing of
  the current file should be done.
```

```
If editing is requested the procedure exits to the text editor EDWIN with
  the file that was just read. Upon completion of EDWIN the file is re-read
  and displayed again.
```

```
If a new file is requested the procedure simply informs procedure Input of
  the request.
```

```
The procedure ShowData ends when the user signals the data to be correct. }
```

```
begin
```

```
{ ShowData }
```

```
  repeat
```

```
    { Show the data until the user OK's it. }
```

```
    begin
```

```
      { Echo what was read. }
```

```
      clrscr;
```

```
      writeln ('Data read from ', InFileName, ':');
```

```
      writeln ('Pond Pond Curnt Tar                               Ion Weight Percents',
```

```
              '      Pond Pond Salt');
```

```
      writeln ('Name Area Depth Depth Inventory %K      %Na      %Mg      %Cl ',
```

```
              '%SO4 Max Flow Rec. Dis.');
```

```
      writeln ('      (Hect) (cm) (cm) (Tons)                               ',
```

```
              '      (m^3/d)          Fact');
```

```
      for i := 0 to LastPond do
```

```
        begin
```

```
          with Ponds[i] do
```

```
            begin
```

```
              writeln (Name, ' ',
```

```
                      Area:4:0, ' ',
```

```
                      Depth:3:0, ' ',
```

```
                      TargetDepth:3:0, ' ',
```

```
                      Inventory:8:0, ' ',
```

```
                      K:4:2, ' ',
```

```
                      Na:5:2, ' ',
```

```
                      Mg:5:2, ' ',
```

```
                      Cl:5:2, ' ',
```

```
                      SO4:5:2, ' ',
```

```
                      MaxFlow:8:0, ' ',
```

```
                      Recycle:1:1, ' ',
```

```
                      SDFact:4:2);
```

```
            end;
```

```
          end;
```

```
        end;
```

```

write ('Is all the data correct? <Y> or <N> ');
InChar := UPCASE(READKEY);
write (InChar);
delay (delayvalue);

if InChar = 'N' then { User saw an error in the data read. }
begin
  gotoxy (1, 22);
  write ('**User specified error in input data.**');
  gotoxy (1, 23);
  write ('Do you want to read a different file? <Y> or <N> ');
  InChar := UPCASE (READKEY);
  write (InChar);
  delay (delayvalue);

  if InChar = 'Y' then { Read a new file if desired... }
  begin
    InChar := 'N';
    ReadFile := TRUE;
  end
else
  begin
    gotoxy (1, 24);
    write ('Program will exit to the editor with '+InFileName);
    WaitForEnter;
    Command := Editor + InFileName;
    SwapVectors;
    Exec(GetEnv('COMSPEC'), '/C ' + Command);
    SwapVectors;
    if DosError <> 0 then
      WriteLn('Could not execute COMMAND.COM');
    WriteLn;
    ReadFile := FALSE;
  end;
  Input;
end;
until InChar = 'Y';
end; { ShowData }

```

```

procedure MaterialBalancePrint;
{ This procedure prints the material balance to the Balout file. The material
  balance is printed at the end of each days calculation. The DayData array
  contains the material balance information for each pond, each day. }

begin { MaterialBalancePrint }
  writeln (BalOutFile);
  writeln (BalOutFile, Months[Month].Name + ' ' + DisplayDay);
  writeln (BalOutFile, '      Beginning Flow  Recycle  Ending      ',
    'Flow Salt ');
  writeln (BalOutFile, '      Inventory In      In      = Inventory Out      ',
    'Deposit Evaporation');
  for Pond := 1 to LastPond do
  begin
    { First print the mass balance. }
    write (BalOutFile, Ponds[Pond].Name);
    writeln (BalOutFile, ' -----',
      ' -----');
  end
end

```

```

with DayData[Pond] do
begin
  writeln (BalOutFile, 'Mass ',
    round(BeginningInventory):9, ' ',
    round(InFlow):6, ' ',
    round(Recycle):6, ' = ',
    round(EndingInventory):9, ' ',
    round(OutFlow):6, ' ',
    round(SaltDeposit):5, ' ',
    round(Evaporation):5);
  writeln (BalOutFile, 'Mg ',
    round(BeginningInventory*Mg0/100.0):8, ' ',
    round(InFlow*Mg1/100.0):5, ' ',
    round(Recycle*Mg2/100.0):5, ' = ',
    round(EndingInventory*Mg3/100.0):8, ' ',
    round(OutFlow*Mg0/100.0):5, ' ',
    0:4, ' ',
    0:7);
  writeln (BalOutFile, 'Na ',
    round(BeginningInventory*Na0/100.0):8, ' ',
    round(InFlow*Na1/100.0):5, ' ',
    round(Recycle*Na2/100.0):5, ' = ',
    round(EndingInventory*Na3/100.0):8, ' ',
    round(OutFlow*Na0/100.0):5, ' ',
    round(SaltDeposit*0.3934):6, ' ',
    0:7);
  writeln (BaloutFile, '-----',
    '-----');
  writeln (BaloutFile, 'Mass Balance = ', abs(BeginningInventory+
    InFlow+
    Recycle-
    EndingInventory-
    OutFlow-
    SaltDeposit-
    Evaporation):7:3, ' ',
    'Mg Balance = ', abs((BeginningInventory*Mg0/100.0)+
    (InFlow*Mg1/100.0)+
    (Recycle*Mg2/100.0)-
    (EndingInventory*Mg3/100.0)-
    (OutFlow*Mg0/100.0)):7:3, ' ',
    'Na Balance = ', abs((BeginningInventory*Na0/100.0)+
    (InFlow*Na1/100.0)+
    (Recycle*Na2/100.0)-
    (EndingInventory*Na3/100.0)-
    (OutFlow*Na0/100.0)-
    (SaltDeposit*0.3934)):7:3);
  writeln(BaloutFile);
end;
end;
end;
{ with DayData }
{ for Pond loop }
{ MaterialBalancePrint }

```

```

procedure GetStartConditions;
    { Request the beginning month, beginning day, output file etc. }
var
    InString, InChar : STRING;
    i, InVal, CodeVar : INTEGER;

begin
    { GetStartConditions }
    repeat
        { The beginning month. }
        begin
            Month := 0;
            clrscr;
            gotoxy (5, 10);
            write ('What month do the calculations begin in? ');
            readln (InString);
            InString := InitialCap (Instring);
            val ( InString, InVal, CodeVar );
            i := 0;
            repeat
                begin
                    inc(i);
                    if Months[i].Counter = InVal then
                        begin
                            Month := i;
                        end
                    else if copy(Months[i].Name, 1, 4) = copy(InString, 1, 4) then
                        begin
                            Month := i;
                        end;
                end;
            until (Month = 1) or (i = 12);
            if Month <> 1 then
                begin
                    gotoxy (10, 20);
                    clrscr;
                    writeln (InString, ' isn''t recognized as a month. ');
                    writeln ('Please enter either the complete name or the number. ');
                    WaitForEnter;
                end;
            end;
        until (Month > 0) and (Month < 12);
        FirstMonth := Month;
        repeat
            { The beginning day. }
            gotoxy (5, 10);
            clrscr;
            write ('What day in ', Months[Month].Name, ' do the calculations begin? ');
            readln (Day);
            Day := Months[Month].FirstDay + Day - 1;
        until (Day <= Months[Month].LastDay) and
            (Day >= Months[Month].FirstDay);
        repeat
            begin
                gotoxy (5, 10);
                clrscr;
                write ('What is the evaporation factor for this run? ');
                readln (EvapFact);
                gotoxy (5, 10);
                clrscr;
                write ('What is the precipitation factor for this run? ');
                readln (PrecipFact);
                gotoxy (5, 10);
                clrscr;
                write (' Evaporation Factor = ', EvapFact:5:3);
                gotoxy (5, 11);
                clrscr;
                write ('Precipitation Factor = ', PrecipFact:5:3);
                gotoxy (5, 12);
                clrscr;
                write ('Are these correct? ');
                InChar := upcase(readkey);
                write (InChar);
                delay (delayvalue);
            end;
        end;
    end;
end;

```



```

procedure ZeroMonthData;
                                { Procedure to zero out the monthly data record. }
begin
                                { ZeroMonthData }
  for i := 1 to LastPond do
    begin
      with MonthData[i] do
        begin
          DailyDepthSum      := 0.0;
          DailyOutFlowSum    := 0.0;
          DailyMgSum         := 0.0;
          EndingDepth        := 0.0;
          EndingMg           := 0.0;
          DailySaltDepositSum := 0.0;
        end;
      end;
    end;
                                { ZeroMonthData }

procedure ZeroYearData;
                                { Procedure to zero out the yearly data record. }
begin
                                { ZeroYearData }
  for i := 1 to 12 do
    begin
      for j := 1 to LastPond do
        begin
          YearData [i, j] := 0.0;
        end;
      end;
    end;
                                { ZeroYearData }

procedure BalancePond;
{ This procedure uses Wegstien convergence acceleration to close on the
  amount of salt deposited. A first guess of the salt deposit is made
  by removing the evaporation water then calculating the new sodium weight
  percent. The new magnesium value is calculated also, both by material
  balance. }
const
  tol2 = 0.00000001;

var
  Mgc, Nac, Saltc, Salte : REAL;           { The estimated values. }
  CalculateAllIons: BOOLEAN; { Flag to calculate ion wt. % after balance. }
  Iterations : INTEGER;
  Saltc1, Saltc2, Delta1, Delta2,
  Intercept, Slope : REAL;                 { Wegstien convergence variables. }

procedure Chem(x : REAL);                 { Chem }
  { The Chem Procedure calculates the weight percent of
    the ions in El Mex brine given the weight percent Mg++.
    The procedure assumes only five ions in solution.
    The K+, Cl- and the SO4-- ions are calculated by material
    balance. The Mg++ and Na+ ions are calculated in the procedure
    BalancePond. The Na+ ion calculation done in this procedure
    is the equilibrium value. }

```

```

var
  H2O      : REAL;

begin
  if CalculateAllIons then
    begin
      Naf := ((Tb - Tout) * Nab + Tr * Nar - Saltc * 39.34) / Tf;
      Clf := ((Tb - Tout) * Clb + Tr * Clr - Saltc * 60.66) / Tf;
      Kf := ((Tb - Tout) * Kb + Tr * Kr) / Tf;
      SO4f := ((Tb - Tout) * SO4b + Tr * SO4r) / Tf;
    end
  else
    begin
      Naf := 10.5397 - 1.5951*x - 0.0359*x*x + 0.0095*x*x*x;
    end;
end;

```

{ Chem }

{ Chem }

```

procedure LastPondFlowOut;

```

```

{ Procedure LastPondFlowOut determines the flow from the last pond.
  If it is the first day of calculations the flow is set to 1/2
  the maximum flow from the pond. Otherwise, the flow from the last
  pond is determined by comparing the Mg concentration in the last
  pond, x, with what it was the day before, xp. The procedure also
  uses an upper and lower limit on the desired Mg concentration to
  determine whether to flow maximum or not at all. The procedure returns
  the flow from the last pond as Tr, the recycle flow, and Mgr, Nar as
  the recycle concentrations of Mg and Na respectively. }

```

```

var
  x, K1, K2 : REAL;
  ControlValue : REAL;

begin
  K1 := Cp + CpRange;
  K2 := Cp - CpRange;
  x := Ponds[Pond].Mg;
  if PreviousOutFlow = 0.0 then ControlValue := 150.0;
  if PreviousOutFlow <> 0.0 then ControlValue := 0.0;
  if x >= K1 then
    { Beginning of the decision tree. }
    begin
      DayData[Pond].OutFlow := Ponds[Pond].MaxFlow;
    end
  else if x <= K2 then
    begin
      DayData[Pond].OutFlow := 0.0;
    end
  else if FirstDay then
    begin
      DayData[Pond].OutFlow := Ponds[Pond].MaxFlow * 0.10;
      FirstDay := FALSE;
      ControlValue := 0.0
    end
  else
    begin
      if PreviousMg > x then
        { Decreasing Mg weight percent }
        begin
          if x < Cp then
            begin
              DayData[Pond].OutFlow := (PreviousOutFlow+ControlValue) * 0.9;
            end
          else if x > Cp then
            begin
              DayData[Pond].OutFlow := PreviousOutFlow;
            end;
          end;
        end;
      end;
    end;
end;

```

{ LastPondFlowOut }

```

end
else if PreviousMg < x then    ( Increasing Mg weight percent )
begin
  if x > Cp then
  begin
    DayData[Pond].OutFlow := (PreviousOutFlow+ControlValue) * 1.1;
  end
  else if x < Cp then
  begin
    DayData[Pond].OutFlow := PreviousOutFlow;
  end;
end;
end;                                     ( End of the decision tree. )
if DayData[Pond].OutFlow > Ponds[Pond].MaxFlow then
begin
  DayData[Pond].OutFlow := Ponds[Pond].MaxFlow;
end
else if DayData[Pond].OutFlow < 0.0 then
begin
  DayData[Pond].OutFlow := 0.0;
end;
PreviousMg := x;
PreviousOutFlow := DayData[Pond].OutFlow;
end;                                     ( LastPondFlowOut )

```

```

procedure AdjustLevel;
{ Procedure AdjustLevel determines the flow from the pond feeding the
current pond to come closest to the target depth. It cannot exceed
the maximum flow from the pond feeding the current pond. After the
procedure determines the required flow it calculates the new concen-
trations and depth. These values are set for the current pond and
the flow is set for the pond feeding the current pond. Note that the
local variables for procedure Balance are global for AdjustLevel and
the program ElMaxModel global variables are known in AdjustLevel. }

```

```

var
  depth : REAL;

begin                                     ( AdjustLevel )
  Ponds[Pond].Depth := Tf / (Density(Mgf) *
                             Ponds[Pond].Area * 100.0); { Current depth in cm. }
  if Ponds[Pond].Depth <= Ponds[Pond].TargetDepth then
    Tin := (Ponds[Pond].TargetDepth - Ponds[Pond].Depth) *
           Ponds[Pond].Area * 100.0 * Density(Mgin);
  if Tin > Ponds[Pond-1].MaxFlow then
    Tin := Ponds[Pond-1].MaxFlow;
  Kf := (Kf*Tf + Kin * Tin) / (Tf + Tin); { Mix the Flows. }
  Naf := (Naf*Tf + Nain*Tin) / (Tf + Tin);
  Mgf := (Mgf*Tf + Mgin*Tin) / (Tf + Tin);
  Clf := (Clf*Tf + Clin*Tin) / (Tf + Tin);
  SO4f := (SO4f*Tf + SO4in*Tin) / (Tf + Tin);
  Tf := Tf + Tin;
  if Ponds[Pond].Depth < 0.5 then
  begin
    gotoxy (10, 20);
    writeln ('The depth of pond ',Ponds[Pond].Name,' is ',
            Ponds[Pond].Depth:5:2,' cm. ');
    gotoxy (10, 21);
    writeln ('This may indicate ',Ponds[Pond].Name,' is drying up. ');
    gotoxy (10, 22);
    writeln ('Pond ',Ponds[Pond].Name,' may not be getting enough ',
            'brine from ',Ponds[Pond - 1].Name,'. ');
    gotoxy (10, 23);
    writeln ('Please check the Maximum Outflow parameter of pond ',
            Ponds[Pond - 1].Name,' in ',InFileName);
    WaitForEnter;
    for i := 0 to 3 do
    begin
      gotoxy (10, 20+i);
      clrscr;
    end;
  end;
end;                                     ( AdjustLevel )

```


begin

{ BalancePond }

```
if Pond = LastPond then      { First get the flow out of the last pond. }
begin
  LastPondFlowOut;
  Kr := Ponds[LastPond].K;
  Nar := Ponds[LastPond].Na;
  Mgr := Ponds[LastPond].Mg;
  Clr := Ponds[LastPond].Cl;
  SO4r := Ponds[LastPond].SO4;
end;

Tin := 0.0;      { Initialize the pond flows to balance nomenclature. }
Kin := Ponds[Pond-1].K;
Nain := Ponds[Pond-1].Na;
Mgin := Ponds[Pond-1].Mg;
Cljn := Ponds[Pond-1].Cl;
SO4in := Ponds[Pond-1].SO4;
Tout := DayData[Pond].OutFlow;
Tb := Ponds[Pond].Inventory;
Kb := Ponds[Pond].K;
Nab := Ponds[Pond].Na;
Mgb := Ponds[Pond].Mg;
Clb := Ponds[Pond].Cl;
SO4b := Ponds[Pond].SO4;
Tr := DayData[LastPond].OutFlow * Ponds[Pond].Recycle;
W := Ponds[Pond].Area * Evap;

CalculateAllIons := false;
{ Generates the first guess for the salt deposit. }
Tf := Tb + Tr - W - Tout;      { Mass Balance }
Nac := ((Tb - Tout) * Nab + Tr * Nar) / Tf;      { Na Balance }
Mgf := ((Tb - Tout) * Mgb + Tr * Mgr) / Tf;      { Mg Balance }
Chem (Mgf);      { Chem calculates Naf from Mgf }
Deltal := Nac - Naf;
Saltc1 := Tf * Deltal / 39.34;      { A first estimate of the deposit. }
Tf := Tb + Tr - W - Tout - Saltc1;
Nac := ((Tb - Tout) * Nab + Tr * Nar - Saltc1 * 39.34) / Tf;
Mgf := ((Tb - Tout) * Mgb + Tr * Mgr) / Tf;
Chem (Mgf);
Deltal := Nac - Naf;
Saltc2 := Saltc1 * 1.1;      { The initial second estimate is a 10% increase. }
i := 0;
repeat
begin
  Tf := Tb + Tr - W - Tout - Saltc2;
  Nac := ((Tb - Tout) * Nab + Tr * Nar - Saltc2 * 39.34) / Tf;
  Mgf := ((Tb - Tout) * Mgb + Tr * Mgr) / Tf;
  Chem (Mgf);
  Delta2 := Nac - Naf;
  if abs(Delta2) > tol then      { Beginning of Wegstien acceleration. }
  begin
    Slope := (Deltal - Delta2) / (Saltc1 - Saltc2);
    Intercept := Delta2 - Slope * Saltc2;
    Saltc1 := Saltc2; { Update the estimate and value. }
    Deltal := Delta2;
    if abs(slope) < tol2 then
    begin
      Saltc2 := abs(Saltc2) * 1.5;
    end
  else
  begin
    Saltc2 := -Intercept / Slope;
  end;
  end;
  inc(i);
end;
until (abs(Nac - Naf) <= tol) or (i > maxiterations);
```

```

if i > maxiterations then
begin
gotoxy (10, 20);
writeln ('Maximum iterations exceeded. ');
WaitForEnter;
end;
Saltc := Saltc2;
if Saltc < 0.0 then { Control how much salt can be dissolved. }
begin
Saltc := Saltc * Ponds[Pond].SDFact;
Tf := Tb + Tr - W - Tout - Saltc;
Mgf := ((Tb - Tout) * Mgb + Tr * Mgr) / Tf;
CalculateAllIons := true;
Chem (Mgf);
end
else
begin
CalculateAllIons := true;
Chem (Mgf);
end;
AdjustLevel;
with DayData[Pond] do { Keep the daily flow record. }
begin
BeginningInventory := Tb;
Mg0 := Mgb;
Na0 := Nab;
EndingInventory := Tf;
Mg3 := Mgf;
Na3 := Naf;
InFlow := Tin;
Mg1 := Mgin;
Na1 := Nain;
Recycle := Tr;
Mg2 := Mgr;
Na2 := Nar;
OutFlow := Tout;
Evaporation := W;
SaltDeposit := Saltc;
end;
DayData[Pond-1].OutFlow := Tin;
with MonthData[Pond] do
begin
DailyDepthSum := DailyDepthSum + Ponds[Pond].Depth;
DailyOutFlowSum := DailyOutFlowSum + Tout;
DailyMgSum := DailyMgSum + Mgf;
DailySaltDepositSum := DailySaltDepositSum + Saltc;
end;
with Ponds[Pond] do { Reset the Ponds array to the calculated values. }
begin
Inventory := Tf;
K := Kf;
Na := Naf;
Mg := Mgf;
Cl := Clf;
SO4 := SO4f;
Depth := Inventory / (Density(Mg) * Area * 100.0);
end;
end; { BalancePond }

procedure MonthlySummaryPrint;
{ This procedure writes the monthly summary to the Out file. The procedure
uses the MonthData array to print the output. The MonthData array is
zeroed at the end of each month. }

```

```

var
  SaltDepositTotal, NetDeposit : REAL;

begin
  writeln (OutFile);
  if Month = 1 then
    begin
      writeln (OutFile, 'Year = ', Year:2, ' Month = ', MonthNames[Month],
        ' Beginning Day = ', BeginningDay,
        ' Days Run This Month = ', DaysRun:2);
    end
  else
    begin
      writeln (OutFile, 'Year = ', Year:2, ' Month = ', MonthNames[Month],
        ' Beginning Day = ', BeginningDay-MonthDays[Month-1, 2],
        ' Days Run This Month = ', DaysRun:2);
    end;
  writeln (OutFile,
    ' Average Average Average');
  writeln (OutFile,
    ' Daily Daily Daily Ending Ending Salt');
  writeln (OutFile,
    ' Pond Depth Flow Mg % Depth Mg % Deposit');
  writeln (OutFile,
    '-----');
  SaltDepositTotal := 0.0;
  NetDeposit := 0.0;
  for Pond := 1 to Lastpond do
    begin
      with MonthData[Pond] do
        begin
          writeln (OutFile,
            Ponds[Pond].Name, ' ', (DailyDepthSum / DaysRun):5:1, ' ',
            round(DailyOutFlowSum / DaysRun):6, ' ',
            (DailyMgSum / DaysRun):5:2, ' ',
            Ponds[Pond].Depth:5:1, ' ',
            Ponds[Pond].Mg:5:2, ' ', round(DailySaltDepositSum):7);
          SaltDepositTotal := SaltDepositTotal + DailySaltDepositSum;
          if upcase(Ponds[Pond].Name[1]) = 'H' then
            begin
              NetDeposit := NetDeposit + DailySaltDepositSum;
            end;
        end;
      end;
    end;
  writeln (OutFile,
    ' Total Monthly Salt Deposit = '
    round(SaltDepositTotal):8);
  writeln (OutFile,
    ' Harvestable Salt Deposit = '
    round(NetDeposit):8);
  writeln (OutFile,
    '-----');
end;
{ MonthlySummaryPrint }

procedure YearlySummaryPrint;
{ This procedure writes the yearly deposit statistics to the Outfile.
  The procedure uses the YearData record array. }
var
  PondTotal, MonthTotal, MonthTotalNet, MonthsTotalSum, MonthsTotalSumNet
  : REAL;
begin
  writeln (OutFile);
  writeln (OutFile, 'Summary of year ', Year);
  writeln (OutFile, 'Months Calculated = ', MonthNames[BeginMonth], ' to ',
    MonthNames[EndMonth]);
  writeln (OutFile, ' Deposit in thousands of tons. ');
  writeln (OutFile,
    ' Jan Feb Mar Apr May Jun Jly Aug Sep ',
    ' Oct Nov Dec Tot ');
  writeln (OutFile, 'Pond -----',
    '-----');
end;
{ YearlySummaryPrint }

```

```

for Pond := 1 to LastPond do
  begin
    write (OutFile, Ponds[Pond].Name, ' ');
    PondTotal := 0.0;
    for Month := 1 to 12 do
      begin
        write (OutFile, (YearData[ Month, Pond]/1000.0):5:0);
        PondTotal := PondTotal + (YearData[ Month, Pond]/1000.0);
      end;
      writeln (OutFile, PondTotal:7:0);
    end;
    writeln (OutFile, '-----',
    '-----');
  write (OutFile, 'Total');
  MonthsTotalSum := 0.0;
  for Month := 1 to 12 do
    begin
      MonthTotal := 0.0;
      MonthTotalNet := 0.0;
      for Pond := 1 to LastPond do
        begin
          MonthTotal := MonthTotal + (YearData[ Month, Pond]/1000.0);
          if upcase(Ponds[Pond].Name[1]) = 'H' then
            begin
              MonthTotalNet := MonthTotalNet + (YearData[ Month, Pond]/1000.0);
            end;
          end; { end of the pond loop }
          write (OutFile, MonthTotal:5:0);
          MonthsTotalSum := MonthsTotalSum + MonthTotal;
          MonthsTotalSumNet := MonthsTotalSumNet + MonthTotalNet;
        end; { end of the months loop }
        writeln (OutFile, MonthsTotalSum:7:0);
        write (OutFile, 'Net ');
        MonthsTotalSumNet := 0.0;
        for Month := 1 to 12 do
          begin
            MonthTotalNet := 0.0;
            for Pond := 1 to LastPond do
              begin
                if upcase(Ponds[Pond].Name[1]) = 'H' then
                  begin
                    MonthTotalNet := MonthTotalNet + (YearData[ Month, Pond]/1000.0);
                  end;
                end; { end of the pond loop }
                write (OutFile, MonthTotalNet:5:0);
                MonthsTotalSumNet := MonthsTotalSumNet + MonthTotalNet;
              end; { end of the months loop }
              writeln (OutFile, MonthsTotalSumNet:7:0);
            end;
            { YearlySummaryPrint }
          begin
            { ElMexModel }
            GSLHeader; { Clear the screen and display the GSL Header. }
            Cp := 3.0; { Set the starting control point. }
            CpRange := 0.1;
            EvapChanged := FALSE;
            ControlChanged := FALSE;
            ReadFile := true; { Now get all the information to run the model. }
            Input; { First the pond system. }
            ShowData; { Echo/confirm the pond system. }
            GetStartConditions; { Get the starting conditions. }
            assign (OutFile, OutFileName); { Open the file(s) for output. }
            rewrite (OutFile);
            writeln (OutFile, 'El Mex Model Summary File "' + OutFileName + '"');
            if EvapChanged then
              writeln (OutFile, 'Evaporation data was changed for this run. ');
            if ControlChanged then
              writeln (OutFile, 'Control data was changed for this run. ');
            writeln (OutFile, 'Evaporation factor is ', EvapFact:5:3,
            ' Precipitation factor is ', PrecipFact:5:3);
          end;
        end;
      end;
    end;
  end;

```

```

if BalancePrint then
begin
  assign (BalOutFile, BalOutFileName);
  rewrite (BalOutFile);
  writeln (BalOutFile, 'El Mex Material Balance File ' + BalOutFileName + '');
);
end;
MonthsRun := 0;      ( The calculational part of the program begins here. )
FirstDay := true;
Year := 1;
while Year <= NumberOfYears do      ( Loop through the years. )
begin
  ZeroYearData;
  clrscr;      ( This sets up a display to show where the calculations are. )
  gotoxy (12, 6);
  write (' Calculating Year: ', Year);
  gotoxy (12, 7);
  write (' Calculating Day: ');
  gotoxy (12, 8);
  write (' Calculating Pond: ');
  if ((NumberOfMonths + Month - MonthsRun) >= 12) then
  begin      ( The last month for the current year. )
    EndMonth := 12;
  end
  else
  begin
    EndMonth := NumberOfMonths + Month - MonthsRun - 1;
  end;
  BeginMonth := Month;
  while Month <= EndMonth do      ( Loop through the months. )
  begin
    ZeroMonthData;
    beginningDay := Day;
    DaysRun := 0;

    while Day <= Months[Month].LastDay do      ( Loop through the days. )
    begin
      ZeroDayData;
      str (Day - Months[Month].FirstDay + 1, DisplayDay);
      gotoxy (30, 7);
      write (' ' + Months[Month].Name + ' ' + DisplayDay);
      clreol;

      for Pond := LastPond downto 1 do      ( Loop through the ponds. )
      begin
        gotoxy (30, 8);
        write (' ' + Ponds[Pond].Name);
        BalancePond;

        end;      ( End of the pond loop. )
      if BalancePrint then MaterialBalancePrint;
      inc(Day);
      inc(DaysRun);
    end;      ( End of the days loop. )
    MonthlySummaryPrint;
    for Pond := 1 to LastPond do
    begin
      YearData[Month, Pond] := MonthData[Pond].DailySaltDepositSum;
    end;
    Day := Months[Month + 1].FirstDay;
    LastMonth := Month;
    inc(MonthsRun, 1);
    inc(Month, 1);
  end;      ( End of the months loop. )

  ( At the end of each year display the pond statistics
  then write the statistics to a file. )
  EndMonth := Month - 1;
  if Year <= NumberOfYears then YearlySummaryPrint;

  Month := 1;
  Day := 1;
  inc(Year, 1);

  END;      ( End of the years loop. )
  close(outFile);
  if balancePrint then close (BaloutFile);
  WriteEndingConditionsFile;
  clrscr;

```

END.;

(ElMexModel)

APPENDIX E

Borg el Arab Run

6 Years Starting with Sea Brine

This is the setup for the Borg El Arab system of ponds.
 The Lake is the concentration of the open ocean.
 The line of asterisks may be moved to accommodate more comments.
 Notice that ponds whose names begin with H are assumed to be harvestable.
 The net deposit of the system is summed from these harvestable ponds.
 In this starting state the ponds are filled with ocean brine and then
 run in sequence for 6 years.

Pond Name	Area (Hect.)	Current Depth		Target Ion Weight Percents					Max. Flow (Tons/d)	Red. Es.	Salt Fact.
		(cm)	(cm)	K	Na	Mg	Cl	SO4			
Lake	0	0	0	0.04	1.05	0.13	1.90	0.26	1000000	0	0.00
PND1	1700	50	50	0.04	1.05	0.13	1.90	0.26	500000	0	0.00
PND2	300	50	50	0.04	1.05	0.13	1.90	0.26	100000	0	0.00
HRV1	200	30	30	0.04	1.05	0.13	1.90	0.26	300000	0	0.00
HAR2	200	30	30	0.04	1.05	0.13	1.90	0.26	500000	0	0.00

Ending Conditions File
 Start Conditions From :BORGBASE.DAT
 Model run covered 6 years.
 Model ran 72 months.
 The first month run was January.
 The last month run was December.
 The evaporation factor was 1.000.
 The precipitation factor was 1.000.

Lake	0	0	0	0.04	1.05	0.13	1.90	0.26	1000000	0.0	0.00
PND1	1700	50	50	0.13	3.41	0.42	6.17	0.84	500000	0.0	0.00
PND2	300	50	50	0.21	5.55	0.69	10.05	1.38	400000	0.0	0.00
HRV1	200	30	30	0.35	8.65	1.15	15.82	2.30	300000	0.0	0.00
HAR2	200	30	30	0.91	5.73	2.97	15.26	5.95	300000	0.0	0.00

El Mex Model Summary File 18ORGBASE

Evaporation factor is 1.000 Precipitation factor is 1.000

Year = 1 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.8	9150	0.15	50.0	0.14	0
PND2	49.7	5223	0.14	50.0	0.14	0
HRV1	29.7	2615	0.14	30.0	0.15	0
HAR2	29.9	0	0.14	30.0	0.15	0
Total Monthly Salt Deposit =						0
Harvestable Salt Deposit =						0

Year = 1 Month = February Beginning Day = 1 Days Run This Month = 29

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.7	14547	0.15	50.0	0.15	0
PND2	49.5	3290	0.15	50.0	0.16	0
HRV1	29.5	4151	0.16	30.0	0.17	0
HAR2	29.8	0	0.16	30.0	0.17	0
Total Monthly Salt Deposit =						0
Harvestable Salt Deposit =						0

Year = 1 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.5	24672	0.16	50.0	0.18	0
PND2	49.2	14049	0.17	50.0	0.19	0
HRV1	29.3	7063	0.19	30.0	0.22	0
HAR2	29.7	0	0.21	30.0	0.24	0
Total Monthly Salt Deposit =						0
Harvestable Salt Deposit =						0

Year = 1 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.3	36090	0.19	50.0	0.20	0
PND2	48.9	20533	0.21	50.0	0.23	0
HRV1	29.0	10321	0.25	30.0	0.19	0
HAR2	29.5	0	0.29	30.0	0.25	0
Total Monthly Salt Deposit =						0
Harvestable Salt Deposit =						0

Year = 1 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.2	18718	0.22	50.0	0.23	0
PND2	48.2	21929	0.26	50.0	0.28	0
HRV1	29.0	11054	0.53	30.0	0.38	0
HAR2	29.5	0	0.43	30.0	0.51	0
Total Monthly Salt Deposit =						0
Harvestable Salt Deposit =						0

Year = 1 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.2	11894	0.25	50.0	0.26	0
PND2	48.7	23737	0.31	50.0	0.33	0
HRV1	28.9	11350	0.43	30.0	0.47	0
HAR2	29.5	0	0.61	30.0	0.71	0
Total Monthly Salt Deposit =						0
Harvestable Salt Deposit =						0

Year = 1 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.2	41144	0.27	50.0	0.28	0
PND2	48.7	23202	0.36	50.0	0.38	0
HRV1	28.9	11497	0.52	30.0	0.57	0
HAR2	29.5	0	0.84	30.0	0.96	0
Total Monthly Salt Deposit =						0
Harvestable Salt Deposit =						0

Year = 1 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.2	40128	0.29	50.0	0.30	0
PND2	48.8	22953	0.41	50.0	0.43	0
HRV1	29.0	11806	0.62	30.0	0.66	0
HAR2	29.5	0	1.11	30.0	1.26	31796
Total Monthly Salt Deposit =						31796
Harvestable Salt Deposit =						31796

Year = 1 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.7	24774	0.31	50.0	0.32	0
PND2	48.9	17751	0.44	50.0	0.46	0
HRV1	29.1	10438	0.57	30.0	0.72	0
HAR2	29.5	0	1.40	30.0	1.54	5034
Total Monthly Salt Deposit =						5034
Harvestable Salt Deposit =						5034

Year = 1 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.5	24090	0.32	50.0	0.33	0
PND2	49.3	13752	0.47	50.0	0.48	0
HRV1	29.4	7137	0.75	30.0	0.77	0
HAR2	29.7	0	1.65	30.0	1.75	3848
Total Monthly Salt Deposit =						3848
Harvestable Salt Deposit =						3848

Year = 1 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.5	17414	0.33	50.0	0.33	0
PND2	49.5	9754	0.49	50.0	0.50	0
HRV1	29.6	4917	0.79	30.0	0.80	0
HAR2	29.8	0	1.82	30.0	1.89	2725
Total Monthly Salt Deposit =						2725
Harvestable Salt Deposit =						2725

Year = 1 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.3	8758	0.33	50.0	0.34	0
PND2	49.7	4601	0.50	50.0	0.51	0
HRV1	29.3	2078	0.82	30.0	0.83	0
HAR2	29.9	0	1.93	30.0	1.96	1226
Total Monthly Salt Deposit =						1226
Harvestable Salt Deposit =						1226

Summary of Salt

Months Calculated - January to December

Deposit in thousands of tons.

	Jan	Feb	Mar	Apr	May	Jun	Jul	Aug	Sep	Oct	Nov	Dec	Total
POND													
PND1	0	0	0	0	0	0	0	0	0	0	0	0	0
PND2	0	0	0	0	0	0	0	0	0	0	0	0	0
HRV1	0	0	0	0	0	0	0	0	0	0	0	0	0
HAR2	0	0	0	0	0	0	0	52	50	38	27	12	167
Total	0	0	0	0	0	0	0	52	50	38	27	12	167
Net	0	0	0	0	0	0	0	52	50	38	27	12	167

Year = 2 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.8	6684	0.34	50.0	0.34	0
PND2	49.8	3380	0.51	50.0	0.52	0
HRV1	29.9	1342	0.24	30.0	0.35	0
HAR2	29.9	0	1.98	30.0	2.01	2569
Total Monthly Salt Deposit =						2569
Harvestable Salt Deposit =						2569

Year = 2 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.7	11559	0.34	50.0	0.35	0
PND2	49.6	6103	0.52	50.0	0.53	0
HRV1	29.7	2305	0.37	30.0	0.38	0
HAR2	29.9	0	2.05	30.0	2.09	16246
Total Monthly Salt Deposit =						16246
Harvestable Salt Deposit =						16246

Year = 2 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.6	21952	0.35	50.0	0.35	0
PND2	49.3	12347	0.54	50.0	0.55	0
HRV1	29.5	6295	0.90	30.0	0.92	0
HAR2	29.7	0	2.21	30.0	2.21	41976
Total Monthly Salt Deposit =						41976
Harvestable Salt Deposit =						41976

Year = 2 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.1	31197	0.56	50.0	0.56	0
PND2	48.9	2161	0.58	50.0	0.57	0
HRV1	29.1	11275	1.00	30.0	0.97	0
HAR2	29.5	0	2.48	30.0	2.56	7414
Total Monthly Salt Deposit =						7414
Harvestable Salt Deposit =						7414

Year = 2 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.1	36733	0.57	50.0	0.57	0
PND2	48.9	21165	0.58	50.0	0.57	0
HRV1	29.1	11295	1.00	30.0	1.02	0
HAR2	29.5	0	2.32	30.0	2.97	7600
Total Monthly Salt Deposit =						7600
Harvestable Salt Deposit =						7600

Year = 2 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.1	48761	0.57	50.0	0.58	0
PND2	48.9	31795	0.58	50.0	0.58	0
HRV1	29.6	21047	0.94	30.0	0.93	0
HAR2	29.1	10052	2.55	30.0	2.58	7490
Total Monthly Salt Deposit =						7490
Harvestable Salt Deposit =						7490

Year = 2 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.1	39693	0.58	50.0	0.58	0
PND2	48.8	22532	0.60	50.0	0.61	0
HRV1	29.0	11538	0.98	30.0	1.02	0
HAR2	29.5	0	2.80	30.0	3.01	8321
Total Monthly Salt Deposit =						8321
Harvestable Salt Deposit =						8321

Year = 2 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
RND1	49.0	47070	0.33	50.0	0.33	0
RND2	49.0	32217	0.60	50.0	0.60	0
HRV1	29.6	20482	0.94	30.0	0.95	0
HARD	29.8	0	2.51	30.0	2.50	6641
Total Monthly Salt Deposit =						6641
Harvestable Salt Deposit =						6641

Year = 3 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
RND1	49.5	12537	0.39	50.0	0.39	0
RND2	49.0	13216	0.61	50.0	0.61	0
HRV1	29.2	2132	1.00	30.0	1.04	0
HARD	29.6	0	2.20	30.0	2.27	63437
Total Monthly Salt Deposit =						63437
Harvestable Salt Deposit =						63437

Year = 2 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
RND1	49.6	31483	0.39	50.0	0.39	0
RND2	49.1	21663	0.62	50.0	0.61	0
HRV1	29.1	15558	1.00	30.0	0.93	168
HARD	29.3	9826	2.22	30.0	2.42	45602
Total Monthly Salt Deposit =						45770
Harvestable Salt Deposit =						45770

Year = 2 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
RND1	49.7	16568	0.39	50.0	0.39	0
RND2	49.5	9104	0.61	50.0	0.62	0
HRV1	29.6	4397	0.96	30.0	0.99	0
HARD	29.8	0	2.50	30.0	2.58	29983
Total Monthly Salt Deposit =						29983
Harvestable Salt Deposit =						29983

Year = 1967 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Average Daily Depth	Average Daily Flow	Average Daily Mg %			
PND1	49.3	3874	0.40	50.0	0.40	0
PND2	49.2	3892	0.60	50.0	0.53	0
HRV1	29.3	1530	1.00	30.0	1.02	0
HAR2	29.7	0	2.61	30.0	2.63	1114
Total Monthly Salt Deposit =						1114
Harvestable Salt Deposit =						1104

Summary of year 1967
 Months calculated = January to December
 Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	July	Aug	Sep	Oct	Nov	Dec	Total
PND1	0	0	0	0	0	0	0	0	0	0	0	0	0
PND2	0	0	0	0	0	0	0	0	0	0	0	0	0
HRV1	0	0	0	0	0	0	0	0	0	0	0	0	0
HAR2	9	16	42	64	76	75	83	76	65	46	30	11	597
Total	9	16	42	64	76	75	83	76	65	46	30	11	597
Net	9	16	42	64	76	75	83	76	65	46	30	11	597

Year = 1967 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Average Daily Depth	Average Daily Flow	Average Daily Mg %			
PND1	49.9	3811	0.40	50.0	0.40	0
PND2	49.2	2632	0.64	50.0	0.64	0
HRV1	29.9	303	1.04	30.0	1.06	0
HAR2	30.0	0	2.65	30.0	2.67	6160
Total Monthly Salt Deposit =						6160
Harvestable Salt Deposit =						6160

Year = 1967 Month = February Beginning Day = 1 Days Run This Month = 29

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Average Daily Depth	Average Daily Flow	Average Daily Mg %			
PND1	49.3	10612	0.40	50.0	0.40	0
PND2	49.7	5372	0.65	50.0	0.66	0
HRV1	29.3	2147	1.08	30.0	1.10	3049
HAR2	29.7	0	2.71	30.0	2.75	15446
Total Monthly Salt Deposit =						18495
Harvestable Salt Deposit =						18495

Year = 0 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	19.5	11441	0.41	30.0	0.41	0
PND2	48.4	27776	0.65	30.0	0.65	0
HRV1	28.6	13336	1.11	30.0	1.11	2727
HAR2	29.1	10360	2.88	30.0	2.88	4530
Total Monthly Salt Deposit =						7417
Harvestable Salt Deposit =						6747

Year = 1 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	19.5	11568	0.40	30.0	0.40	0
PND2	48.7	27746	0.65	30.0	0.65	0
HRV1	28.6	13356	1.06	30.0	1.04	2804
HAR2	29.1	10360	2.8	30.0	2.62	65408
Total Monthly Salt Deposit =						7012
Harvestable Salt Deposit =						7012

Year = 2 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	19.5	15382	0.41	30.0	0.41	0
PND2	48.7	20461	0.65	30.0	0.67	0
HRV1	28.6	10544	1.09	30.0	1.12	2940
HAR2	29.1	10275	2.85	30.0	2.05	80602
Total Monthly Salt Deposit =						83541
Harvestable Salt Deposit =						83541

Year = 3 Month = June Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	19.2	19014	0.41	30.0	0.41	0
PND2	48.5	32211	0.64	30.0	0.65	0
HRV1	28.6	21338	1.02	30.0	1.05	4268
HAR2	29.1	10027	2.61	30.0	2.75	82415
Total Monthly Salt Deposit =						86683
Harvestable Salt Deposit =						86683

Year = 5 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.1	18871	0.41	30.0	0.41	0
PND2	48.8	21741	0.55	30.0	0.55	0
HRV1	29.6	11767	1.05	30.0	1.05	11767
HAR2	29.1	8718	2.80	30.0	2.42	8618
Total Monthly Salt Deposit =						24152
Harvestable Salt Deposit =						24152

Year = 5 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.1	18844	0.41	30.0	0.41	0
PND2	48.8	22047	0.55	30.0	0.55	0
HRV1	29.6	11451	1.03	30.0	1.03	0
HAR2	29.3	0	2.69	30.0	2.71	84000
Total Monthly Salt Deposit =						84000
Harvestable Salt Deposit =						84000

Year = 5 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.3	41807	0.41	30.0	0.41	0
PND2	48.7	27557	0.55	30.0	0.54	0
HRV1	29.8	13860	1.04	30.0	0.99	1232
HAR2	29.2	10063	2.74	30.0	2.51	66293
Total Monthly Salt Deposit =						74175
Harvestable Salt Deposit =						74175

Year = 5 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.5	22332	0.41	30.0	0.41	0
PND2	49.3	12320	0.63	30.0	0.66	0
HRV1	29.4	6161	1.03	30.0	1.06	0
HAR2	29.7	0	2.64	30.0	2.77	47594
Total Monthly Salt Deposit =						47594
Harvestable Salt Deposit =						47594

Year = 3 Month = November Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.7	34136	0.41	50.0	0.41	0
PND2	49.8	3560	0.68	50.0	0.67	0
HRV1	29.5	4137	1.09	30.0	1.11	2475
HAR2	30.5	0	2.95	30.0	2.93	3145
Total Monthly Salt Deposit =						5620
Harvestable Salt Deposit =						3594

Year = 3 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.3	7679	0.42	50.0	0.42	0
PND2	49.2	3740	0.68	50.0	0.68	0
HRV1	29.3	1168	1.14	30.0	1.16	3523
HAR2	30.0	0	2.96	30.0	2.98	9355
Total Monthly Salt Deposit =						17378
Harvestable Salt Deposit =						17278

Summary of year 3

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	July	Aug	Sep	Oct	Nov	Dec	Total
PND1	0	0	0	0	0	0	0	0	0	0	0	0	0
PND2	0	0	0	0	0	0	0	0	0	0	0	0	0
HRV1	0	3	13	3	3	4	7	0	7	0	2	9	56
HAR2	6	15	46	65	81	32	38	84	67	48	31	9	624
Total	6	18	59	73	84	37	45	84	74	48	34	18	680
Net	6	18	59	73	84	37	45	84	74	48	34	13	630

Year = 4 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.9	5595	0.42	50.0	0.42	0
PND2	49.8	2476	0.69	50.0	0.69	0
HRV1	29.9	471	1.19	30.0	1.21	8460
HAR2	30.0	11	2.99	30.0	3.00	3693
Total Monthly Salt Deposit =						12153
Harvestable Salt Deposit =						12153

Year = 4 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.3	10906	0.42	50.0	0.42	0
PND2	48.8	8196	0.70	50.0	0.70	0
HRV1	29.0	1470	1.24	30.0	1.24	3121
HAR2	29.6	737	3.06	30.0	3.06	12651
Total Monthly Salt Deposit =						31824
Harvestable Salt Deposit =						31824

Year = 4 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.3	23733	0.42	50.0	0.42	0
PND2	48.8	14496	0.70	50.0	0.70	0
HRV1	29.4	3608	1.24	30.0	1.22	1768
HAR2	29.6	3191	3.06	30.0	3.06	44239
Total Monthly Salt Deposit =						52007
Harvestable Salt Deposit =						52007

Year = 4 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.3	37144	0.42	50.0	0.42	0
PND2	48.8	23324	0.69	50.0	0.69	0
HRV1	29.0	14573	1.20	30.0	1.17	5559
HAR2	29.4	5923	3.06	30.0	3.04	68239
Total Monthly Salt Deposit =						73798
Harvestable Salt Deposit =						73798

Year = 4 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.2	41569	0.42	50.0	0.42	0
PND2	48.8	26372	0.68	50.0	0.68	0
HRV1	29.9	16760	1.15	30.0	1.13	1629
HAR2	29.3	6705	3.02	30.0	3.00	81751
Total Monthly Salt Deposit =						83381
Harvestable Salt Deposit =						83381

Year = 4 Month = June Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
PND1	49.2	49467	0.42	50.0	0.42	0
PND2	48.6	48043	0.67	50.0	0.67	0
HRV1	23.8	7146	1.10	30.0	1.10	2127
HAR2	29.3	8078	3.00	30.0	3.00	40004
Total Monthly Salt Deposit =						42001
Harvestable Salt Deposit =						40501

Year = 4 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
PND1	49.2	48706	0.42	50.0	0.42	0
PND2	48.6	28485	0.67	50.0	0.67	0
HRV1	23.8	17757	1.10	30.0	1.09	1124
HAR2	29.3	6487	3.00	30.0	3.00	91285
Total Monthly Salt Deposit =						92723
Harvestable Salt Deposit =						92728

Year = 4 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
PND1	49.2	43737	0.42	50.0	0.42	0
PND2	48.7	27496	0.67	50.0	0.67	0
HRV1	23.8	17114	1.09	30.0	1.08	330
HAR2	29.3	6205	3.00	30.0	3.00	38411
Total Monthly Salt Deposit =						39241
Harvestable Salt Deposit =						39241

Year = 4 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
PND1	49.3	36855	0.42	50.0	0.42	0
PND2	48.9	22827	0.67	50.0	0.67	0
HRV1	29.0	13900	1.09	30.0	1.09	2193
HAR2	29.4	5039	3.00	30.0	3.00	69693
Total Monthly Salt Deposit =						71886
Harvestable Salt Deposit =						71886

Year = 4 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.5	15018	0.42	50.0	0.42	0
PND2	49.0	15723	0.57	50.0	0.57	0
HRV1	29.5	3454	1.09	30.0	1.10	2041
HAR2	29.6	3448	3.00	30.0	3.00	49066
Total Monthly Salt Deposit =						51107
Harvestable Salt Deposit =						51107

Year = 4 Month = November Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.6	13115	0.42	50.0	0.42	0
PND2	49.5	10799	0.58	50.0	0.58	0
HRV1	29.6	6152	1.11	30.0	1.12	4040
HAR2	29.7	2168	3.00	30.0	3.00	30252
Total Monthly Salt Deposit =						34891
Harvestable Salt Deposit =						34891

Year = 4 Month = December Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.3	3348	0.42	50.0	0.42	0
PND2	49.7	4432	0.59	50.0	0.59	0
HRV1	29.8	1768	1.15	30.0	1.15	5702
HAR2	29.9	365	2.98	30.0	2.99	9153
Total Monthly Salt Deposit =						14855
Harvestable Salt Deposit =						14855

Summary of year 4

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	Jly	Aug	Sep	Oct	Nov	Dec	Tot
PND1	0	0	0	0	0	0	0	0	0	0	0	0	0
PND2	0	0	0	0	0	0	0	0	0	0	0	0	0
HRV1	3	9	3	6	2	2	1	1	2	2	4	6	31
HAR2	4	13	44	68	82	88	91	88	70	49	31	9	637
Total	12	22	52	74	83	91	93	89	72	51	35	15	698
Net	12	22	52	74	83	91	93	89	72	51	35	15	38

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.9	3868	0.42	50.0	0.42	0
PND2	49.3	2759	0.70	50.0	0.70	0
HRV1	29.9	382	1.17	30.0	1.19	7466
HAR2	30.0	328	3.99	30.0	2.99	3787
Total Monthly Salt Deposit =						11294
Harvestable Salt Deposit =						11294

Year = 5 Month = February Beginning Day = 1 Days Run This Month = 28

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.3	10841	0.42	50.0	0.43	0
PND2	49.7	5092	0.70	50.0	0.70	0
HRV1	29.3	2365	1.21	30.0	1.23	9716
HAR2	29.9	626	3.01	30.0	3.02	12789
Total Monthly Salt Deposit =						22501
Harvestable Salt Deposit =						22501

Year = 5 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.5	23747	0.43	50.0	0.43	0
PND2	49.3	14512	0.70	50.0	0.70	0
HRV1	29.4	8586	1.23	30.0	1.22	8362
HAR2	29.6	3136	3.05	30.0	3.05	44351
Total Monthly Salt Deposit =						52715
Harvestable Salt Deposit =						52715

Year = 5 Month = April Beginning Day = 1 Days Run This Month = 30

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.3	37136	0.43	50.0	0.42	0
PND2	48.9	23321	0.70	50.0	0.69	0
HRV1	29.0	14523	1.20	30.0	1.17	6560
HAR2	29.4	3858	3.05	30.0	3.04	68347
Total Monthly Salt Deposit =						74908
Harvestable Salt Deposit =						74908

Year = 5 Month = May Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.2	41590	0.42	50.0	0.42	0
PND2	48.8	26402	0.68	50.0	0.68	0
HRV1	28.3	16751	1.15	30.0	1.13	1809
HAR2	29.2	6598	3.00	30.0	3.00	31771
Total Monthly Salt Deposit =						34687
Harvestable Salt Deposit =						34687

Year = 5 Month = June Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.2	45514	0.42	50.0	0.42	0
PND2	48.8	28726	0.68	50.0	0.68	0
HRV1	28.3	17987	1.12	30.0	1.11	2991
HAR2	29.2	6718	3.00	30.0	3.00	88040
Total Monthly Salt Deposit =						91534
Harvestable Salt Deposit =						91534

Year = 5 Month = July Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.2	45569	0.42	50.0	0.42	0
PND2	48.8	28558	0.68	50.0	0.67	0
HRV1	28.3	17314	1.10	30.0	1.10	2171
HAR2	29.2	6544	3.00	30.0	3.00	91274
Total Monthly Salt Deposit =						93445
Harvestable Salt Deposit =						93445

Year = 5 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average Daily Depth	Average Daily Flow	Average Daily Mg %	Ending Depth	Ending Mg %	Salt Deposit
PND1	49.2	43844	0.42	50.0	0.42	0
PND2	48.7	27562	0.67	50.0	0.67	0
HRV1	28.3	17170	1.09	30.0	1.09	1360
HAR2	29.3	6261	3.00	30.0	3.00	28419
Total Monthly Salt Deposit =						89779
Harvestable Salt Deposit =						89779

Year = 10 Month = September Beginning Day = 1 Days Run This Month = 30
Average Daily Average Average
Daily Daily Daily Ending Ending Salt
Tons Depth Flow Mg % Depth Mg % Deposit

IND1	19.8	16308	0.42	50.0	0.42	0
IND2	49.9	22945	0.68	50.0	0.68	0
HRV1	19.8	10930	1.13	30.0	1.13	3317
HARD	29.9	2341	2.97	30.0	2.97	8712
Total Monthly Salt Deposit =						11429
Harvestable Salt Deposit =						11429

Year = 10 Month = October Beginning Day = 1 Days Run This Month = 31
Average Daily Average Average
Daily Daily Daily Ending Ending Salt
Tons Depth Flow Mg % Depth Mg % Deposit

IND1	19.8	16721	0.42	50.0	0.42	0
IND2	49.9	22931	0.68	50.0	0.68	0
HRV1	19.8	10728	1.13	30.0	1.13	3298
HARD	29.9	2348	2.99	30.0	2.99	8718
Total Monthly Salt Deposit =						11112
Harvestable Salt Deposit =						11112

Year = 10 Month = November Beginning Day = 1 Days Run This Month = 30
Average Daily Average Average
Daily Daily Daily Ending Ending Salt
Tons Depth Flow Mg % Depth Mg % Deposit

IND1	19.8	16114	0.42	50.0	0.42	0
IND2	49.9	22878	0.68	50.0	0.68	0
HRV1	19.8	12221	1.13	30.0	1.13	3617
HARD	29.9	2341	2.99	30.0	2.99	8732
Total Monthly Salt Deposit =						14254
Harvestable Salt Deposit =						14254

Year = 10 Month = December Beginning Day = 1 Days Run This Month = 31
Average Daily Average Average
Daily Daily Daily Ending Ending Salt
Tons Depth Flow Mg % Depth Mg % Deposit

IND1	19.8	3392	0.42	50.0	0.42	0
IND2	49.9	4480	0.68	50.0	0.68	0
HRV1	19.8	2022	1.13	30.0	1.13	5996
HARD	29.9	910	2.97	30.0	2.97	9246
Total Monthly Salt Deposit =						14842
Harvestable Salt Deposit =						14842

Summary of Year 5

Months Calculated = January to December

Deposit in thousands of tons

Pond	Jan	Feb	Mar	Apr	May	Jun	Jul	Aug	Sep	Oct	Nov	Dec	Total
PND1	0	0	0	0	0	0	0	0	0	0	0	0	0
PND2	0	0	0	0	0	0	0	0	0	0	0	0	0
HRV1	1	12	1	7	5	5	2	1	2	2	4	5	38
HAR2	4	10	14	88	82	88	91	88	70	19	51	8	602
Total	11	22	15	75	65	71	73	70	72	31	25	13	714
Net	11	22	15	75	65	71	73	70	72	31	25	13	714

Year = 5 Month = January Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	49.9	5272	0.42	50.0	0.42	0
PND2	49.8	2765	0.69	50.0	0.70	0
HRV1	29.9	788	1.17	30.0	1.19	7479
HAR2	50.0	319	2.97	30.0	2.97	3880
Total Monthly Salt Deposit =						11359
Harvestable Salt Deposit =						11359

Year = 5 Month = February Beginning Day = 1 Days Run This Month = 29

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	49.3	10695	0.43	50.0	0.43	0
PND2	49.7	5545	0.70	50.0	0.71	0
HRV1	29.8	2192	1.22	30.0	1.24	10300
HAR2	29.9	437	3.00	30.0	3.02	12839
Total Monthly Salt Deposit =						23139
Harvestable Salt Deposit =						23139

Year = 5 Month = March Beginning Day = 1 Days Run This Month = 31

Pond	Average			Ending Depth	Ending Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	49.5	23772	0.43	50.0	0.43	0
PND2	49.3	14543	0.71	50.0	0.70	0
HRV1	29.4	8616	1.23	30.0	1.22	8554
HAR2	29.6	3192	3.06	30.0	3.05	44313
Total Monthly Salt Deposit =						62867
Harvestable Salt Deposit =						52867

Year : 4 Month : April Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Depth	Flow	Mg %	Depth	Mg %	Deposit
PND1	49.2	45378	0.42	50.0	0.42	0
PND2	48.6	28569	0.68	50.0	0.68	0
HRV1	28.3	17822	1.10	30.0	1.10	2350
HAR2	29.2	6550	3.00	30.0	3.00	91276
Total Monthly Salt Deposit =						93626
Harvestable Salt Deposit =						93626

Year : 4 Month : May Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Depth	Flow	Mg %	Depth	Mg %	Deposit
PND1	49.2	45378	0.42	50.0	0.42	0
PND2	48.6	28569	0.68	50.0	0.68	0
HRV1	28.3	17822	1.10	30.0	1.10	2350
HAR2	29.2	6550	3.00	30.0	3.00	91276
Total Monthly Salt Deposit =						94276
Harvestable Salt Deposit =						94276

Year : 4 Month : June Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Depth	Flow	Mg %	Depth	Mg %	Deposit
PND1	49.2	45378	0.42	50.0	0.42	0
PND2	48.6	28569	0.68	50.0	0.68	0
HRV1	28.3	17822	1.12	30.0	1.11	3155
HAR2	29.2	6550	3.00	30.0	3.00	98310
Total Monthly Salt Deposit =						101485
Harvestable Salt Deposit =						91485

Year : 4 Month : July Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Depth	Flow	Mg %	Depth	Mg %	Deposit
PND1	49.2	45378	0.42	50.0	0.42	0
PND2	48.6	28569	0.68	50.0	0.68	0
HRV1	28.3	17822	1.10	30.0	1.10	2350
HAR2	29.2	6550	3.00	30.0	3.00	91276
Total Monthly Salt Deposit =						93626
Harvestable Salt Deposit =						93626

Year = 6 Month = August Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.2	10867	0.42	50.0	0.42	0
PND2	48.7	11589	0.67	50.0	0.67	0
HRV1	29.3	11131	1.09	30.0	1.09	1120
HAR2	29.1	5094	3.00	30.0	3.00	68424
Total Monthly Salt Deposit =						69573
Harvestable Salt Deposit =						69573

Year = 6 Month = September Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.3	36885	0.42	50.0	0.42	0
PND2	48.9	22866	0.67	50.0	0.67	0
HRV1	29.0	13926	1.09	30.0	1.10	2801
HAR2	29.4	5064	3.00	30.0	3.00	69717
Total Monthly Salt Deposit =						72518
Harvestable Salt Deposit =						72518

Year = 6 Month = October Beginning Day = 1 Days Run This Month = 31

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.5	25733	0.42	50.0	0.42	0
PND2	49.0	15851	0.67	50.0	0.68	0
HRV1	29.5	7590	1.10	30.0	1.10	1936
HAR2	29.6	3579	2.99	30.0	2.99	49112
Total Monthly Salt Deposit =						51097
Harvestable Salt Deposit =						51097

Year = 6 Month = November Beginning Day = 1 Days Run This Month = 30

Pond	Average	Average	Average	Ending	Ending	Salt
	Daily	Daily	Daily			
Depth	Flow	Mg %	Depth	Mg %	Deposit	
PND1	49.6	18193	0.42	50.0	0.42	0
PND2	49.5	10883	0.68	50.0	0.68	0
HRV1	29.5	6244	1.11	30.0	1.12	3936
HAR2	29.7	2351	2.99	30.0	2.99	30945
Total Monthly Salt Deposit =						34880
Harvestable Salt Deposit =						34880

Pond	Average			Initial Mg %	End Mg %	Salt Deposit
	Daily Depth	Daily Flow	Daily Mg %			
PND1	49.8	5376	0.41	10.0	1.40	0
PND2	49.1	4184	0.38	50.0	1.29	0
HRV1	29.3	1007	1.15	10.0	1.15	5535
HAR2	26.0	911	2.97	10.0	2.97	4252
Total Monthly Salt Deposit :						14184
Harvestable Salt Deposit :						11854

Summary of year 6

Months Calculated = January to December

Deposit in thousands of tons.

Pond	Jan	Feb	Mar	Apr	May	Jun	July	Aug	Sep	Oct	Nov	Dec	Total
PND1	0	0	0	0	0	0	0	0	0	0	0	0	0
PND2	0	0	0	0	0	0	0	0	0	0	0	0	0
HRV1	7	10	9	8	3	3	2	2	3	2	1	6	58
HAR2	4	17	44	68	82	88	91	88	70	49	31	7	638
Total	11	27	53	76	84	91	94	90	73	51	35	13	796
Net	11	27	53	76	84	91	94	90	73	51	35	13	796