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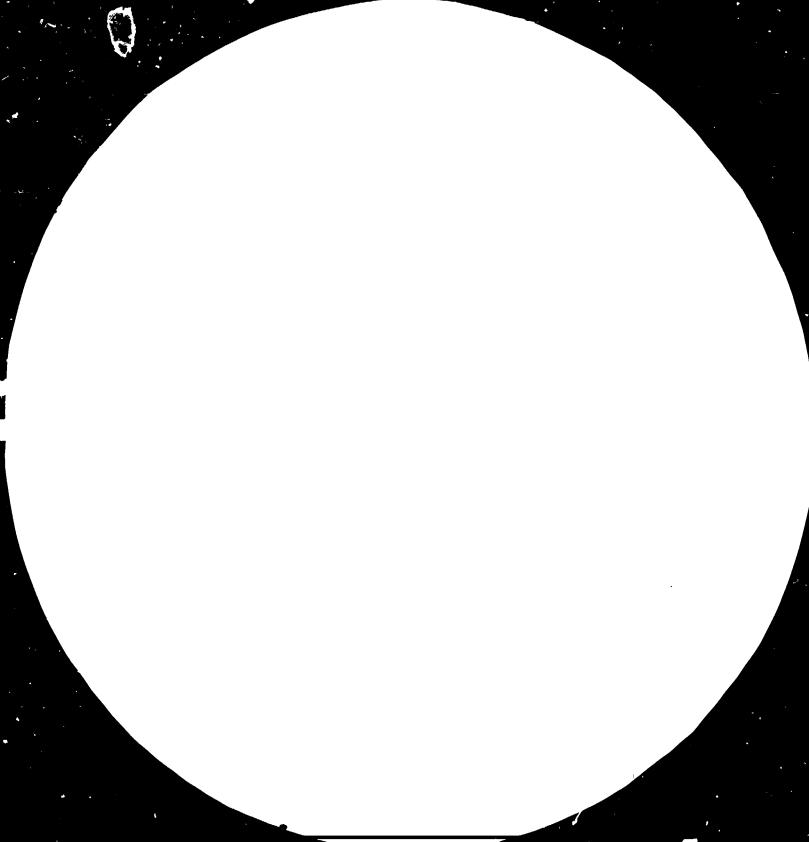
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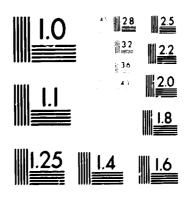
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1985

FINAL REPORT

Dr T.NAGABHUSHANAM Chief Technical Adviser UNIDO PROJECT ST/BRA/81/T01

Brazil. DEVELOPMENT OF CARBON FIBER TECHNOLOGY,

(July 1982 - Dec 1984)

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A WORD OF THANKS

I thank Prof. E.Fitzer, Special Technical Adviser, for having confidence in me, for introducing to this Project and for his help in assisting me to solve all the problems related to the Project.

I thank Mr M.A. Youseff, UNIDO Inter-regional Adviser for his timely cooperation, assistance from his side whenever I looked for it.

I thank Mr Niels Brandt, Chief, Section for Latin America and the Caribbean for his cooperation, moral support.

I thank Mr P.Koenz, Resident Representative and his staff for their constant and immediate assistance to the Project and to me.

I thank Dr A.Soto Krebs, SIDFA and his staff for their constant assistance and cooperation.

I thank T.Cel Kessel, National Project Coordinator, for his keer involvement in the Project activities, providing the required facilities and for creating a congenial atmosphere in the group.

I thank Capt Scyllas Souza da Costa, the Carbon Fiber Group Leader, for his personal involvement in the Project and for showing utmost enthusiasm to provide all that required at his level to the bench workers in the group.

Lastly, though not least, I thank all the counterpart scientists involved in the Project, who listened to me, cooperated with me, appreciated the objectives of the Project and did their best in achieving the objectives of the Project.

PERSONAL COMMENTS

During my 30 months stay and especially at the time of beginning when I joined the Project, Prof. Fitzer, the Special Technical Adviser of the Project had been mainly instrumental in advising me in all aspects of the Project. His constant advise and assistance had been immense use to me in discharging my duties. His scientific consultations to us and introductions to the experts and industrialists and industries in the developed countries had a positive effect on the project. What success has been achieved in this Project could not have been achieved without his timely advice and assistance.

Eventhough things were not clear at the beginning of 1982, with the induction of T.Cel Kessel as National Chief of the Project, the situation has completely changed. T.Cel Kessel has personally involved in the Project activities in spite of his busy activities as the Chief of the Division. It is he, who managed to get whatever needed for the Project. Without his timely solving of the Project problems, the Project would not have achieved its goals.

Above all, the credit should go to the counterpart scientific Group Leade: Capt Scyllas Souza da Costa and his group. These are the main people who absorbed the shocks from the administrative and technical experts and welcomed the suggestions and were always cooperative. I should say it is an excellent group that CTA/PMR could have. The maximum credit should go to these bench workders. I had excellent cooperations from Capt Scyllas Souza da Costa and all the sub-group chiefs and individuals who were involved in the Project.

FISIBA people who were involved in the precursor developmental activities, especially Vicente Nonato de Sa was very cooperative to me and to our Project.

UNIDO office in Vienna and Brasilia gave me extreme cooperation. Mr Youseff, the Senior Inter-regional Adviser gave me excellent support in discharging my duties. Mr Soto Krebs had always been at our doors to help us in our local problems, and his collegue Detlev's assistance was utmost importance.

The UNDP office, Resident Representative, Mr Peter Koenz and his associates were constantly assisting us in all requirements.

-i.i.-

1.0- POSITION AT THE TIME OF ARRIVAL

I arrived at the Project site Centro Técnico Aeroespacial (CTA), São José dos Campos, São Paulo, on IstJuly 82. My job activities are munly to train the Project staff in precursor work, polymerization and to act as Chief Technical Adviser of the Project.

Position of the Group

At the time of my arrival, there were:

- No polymerization activities
- No spinning activities
- No lab. facilities to conduct experiments
- No building facilities for precursor group and surface treatment group and
 Technical personnel were insufficient.

Eventhough, research activities were going on, heat treatment no systematic experiments were planned and conducted. Only one step oxidation and one step carbonization was going on using CTA made heat treatment equipment.

Characterization of the raw materials and end products was lacking. The developmental activities after my arrival are herewith brought out year wise.

2.0- DEVELOPMENTAL ACTIVITIES IN THE PRECURSOR WORK

2.1- Activites in 1982

i - Polymerization Studies

For the first time, the group was trained in the polymerization of acrylcnitrile in the presence of commonmers like methylacrylate in aqueous medium. Free radical polymerization methods were introduced. Initiator system such as potassium persulfate-bisulfite was used to polymerize the vinylmonomers. The polymers synthesized were purified and characterized by viscometric methods outside PMR/CTA as there were no facilities at that time in CTA.

Table 1 gives some of the results of polymerizations. Meanwhile, in August 1982, the lab. model wet spinning assembly arrived (supplied by UNLDO) at the Project site. As the spinning experiments require larger quantity of the polymers, and as CTA group had only a small polymer-

ization vessals, ie 100 to 200 grams capacity and had no comonomers, it is felt important to standardize the spinning experiments using Fibras Sintéticas da Bahia S.A. (FISTBA) supplied commercial acrylic polymers. The polymerization experiments were postponed to a later date. The activities were concentrated on spinning of acrylic fibers, in order to standardize the spinning aparameters.

Table 1 - Results of polymerization

POLYMER NO	REDUCED VISCOSITY
1	4.46
2	2.45
3	2.21
4	2.89
5	2.84
6	3.19
7	6.06

Monomers: acrylonitrile: 94%

Methylacrylate: 6%

ii - Studies in Spinning

with the arrival of Lab. Model Wet Spinning Ass mply supplied by UNIDO, the activities started in spinning acrylic fibers using the commercial acrylic polymer supplied by FISIRA. The line diagram of the spinning equipment is given in Figure 1. In order to standardize the working condition of this equipment, preliminary spinning experiments were commenced using 23% polymer in N N dimethylformamide (DMF). The results of initial fiber spinning were presented in Table 2. Later, several experiments were made in spinning ing variations in the spin pump speed and successive coagulation, etc.

iii - DSC Studies of the Soun Fibers

With the availability of UNIDO supplied differential scanning calorimeter, it was possible to carry out preliminary studies on CTA spun fibers. The results would through light on the cyclization and stabilization parameters. The DSC results are presented in Table 3.

GUIDED ROLLER WASH BATH VACCUM THERMOSTAT SECONDARY STRETCH BATH DOPE HOPPER COAGULATION HOT PIN BATH WINDING GODET GODET GODET GODET GODET THERMOSTAT SPIN PUMP PRIMARY COAGULATION BATH SPINNERET SPIN PIPE

A,B: COOLING IN-LET AND OUT-LET

FIG. 1 = SPINNIG ASSEMBLEY

TABLE 2 - PRELIMINARY SPINNING RESULTS

	·			•				
SPINNING Nº	STRETCH RATIO	TENSILE STH Kg/mm ²	MODULUS Kg/mm ²	DENSITY G/m ³				
1	2.35	7.6	236	1.17				
2 3 7	2.35	19.4	545	1.17				
3	2.25	17.7	600	1.18				
7	3.3	14.3	393	1.18				
8	3.3 .	43.3	1297	1.16				
9	3.3	35.7	990	1.17				
10	3.6	39.3	960	1.16				
11	3.6	17.6	408	1.15				
12	3.6	20.95	426	1.15				
13	3.6	17.4	376	1.16				
14	3.5	33.7	937 😯	1.15				
15	3.5	33.7	937	1.15				
16	.\$	32.2	415	1.18				
17	4	21.4	354	1.19				
18	4	22.5	320	1.19				
19	4	21.8	466	1.18				
20	4	22.1	325	1.17				
21	4	21.6	335	1.17				
22	4	21.9	362	1.17				
23	4	20.2	335	1.17				

TABLE 3 - DSC RESULTS OF CTA SPUN ACRYLIC FIBERS

SAMPLE	ORDER	FREQUENCY FACTOR	ACTIVATION ENERGY	CORRELATION			
	REACTION (n)	(min ⁻¹)	(KJ/MOL)	(\$)			
1	1,05	6.0×10	101,3	99,79			
2	1,09	3.0×10	99,2	99,53			
3	1,04	1.9×10	96,7	99,50			
7	1,04	8.3×10	104,2	99,92			
1 2 3 7 8	1,02	5.4×10	102,2	99,75			
9	1,06	3,9 x 10	100,5	99,84			
10	0,96	3,8 x 10	100,5	99,85			
11	1,02	4,6 x 10	100,9	99,92			
12	1,01	2,3 x 10	108,7	99,71			
13	1,05	1,6 x 10	106,9	99,89			
	• 00	0.7 10	104,5	99,80			
14	1,08	9,7 x 10	107.8	99,84			
15	1,05	1,9 x 10	107.8	99,80			
16	1,08	$2,4 \times 10$	108,9	99,58			
17	1,13	2.8×10	102,4	99,92			
17A	1,08	8,8 x 10	102,4	33,32			
18	1,08	1.2×10	105,7	99,87			
19	1,12	$3,7 \times 10$	99,8	99,89			
20	1,13	1,3 x 10	94, L	99,95			
21	1,13	6.5×10	102,5	99,92			
22	1,12	5,9 x 10	101,9	99,76			
22A	1,15	4.3 x 10	100,3	99,84			
22A 23	1,15	4,3 x 10	100,3	99,84			
23	1,10	7,0 8 20	,	•			

2.2- Activities in 1983

i - Activities in Spinning at CTA

Numerous spinning experiments were conducted using Lab. Model Wet Spinning Assembly shown in Figure 1. For example, a few studies are mentioned here.

CASE I

Polymer concentration : 23% in DMF

Stretch ratio : 5

Composition of primary coagulation bath: 50/50 DMF $\mathrm{H}_2\mathrm{O}$

Composition of second coagulation bath : 0-4% DMF in water

Composition of stretch bath : 6% DMF in water

Composition of tash bath : water Temperature coagulation bath : $1^{\circ}C$ Temperature of second coagulation bath : $28^{\circ}C$ Temperature of hot plate : $143^{\circ}C$

CASE II

The temperature of coagulation bath was varied from G-8°C and the composition of coagulation bath was fixed at 40° DMF in water, stretch ratio was 4. All other conditions were same as in Case I.

In view of the above systematic experiments, Case I and II, the following observations were made:

- 1- Second coagulation bath (Figure 1) had an observable effect on the physical properties of final fibers.
- . 2- Tensile strength of the final fibers found to increase up to a 10% DMF concentration in the 2^{nd} bath (figure 2).
 - 3- Over and above 10% DMF concentration in the 2^{nd} coagulation bath the tensile strength of the fibers was not effected or had minimum effect (Figure 2).
 - 4- Young's modulus found to increase up to about 30% DMF concentration in $2^{\mbox{nd}}$ coagulation bath (Figure 2).
 - 5- Young's modulus found to decrease when (DMF) was increased above 30% (Figure 2).
 - 6- The increase in the coagulation temperature had decreasing effect on the physical properties of the fiber (Figure 3).

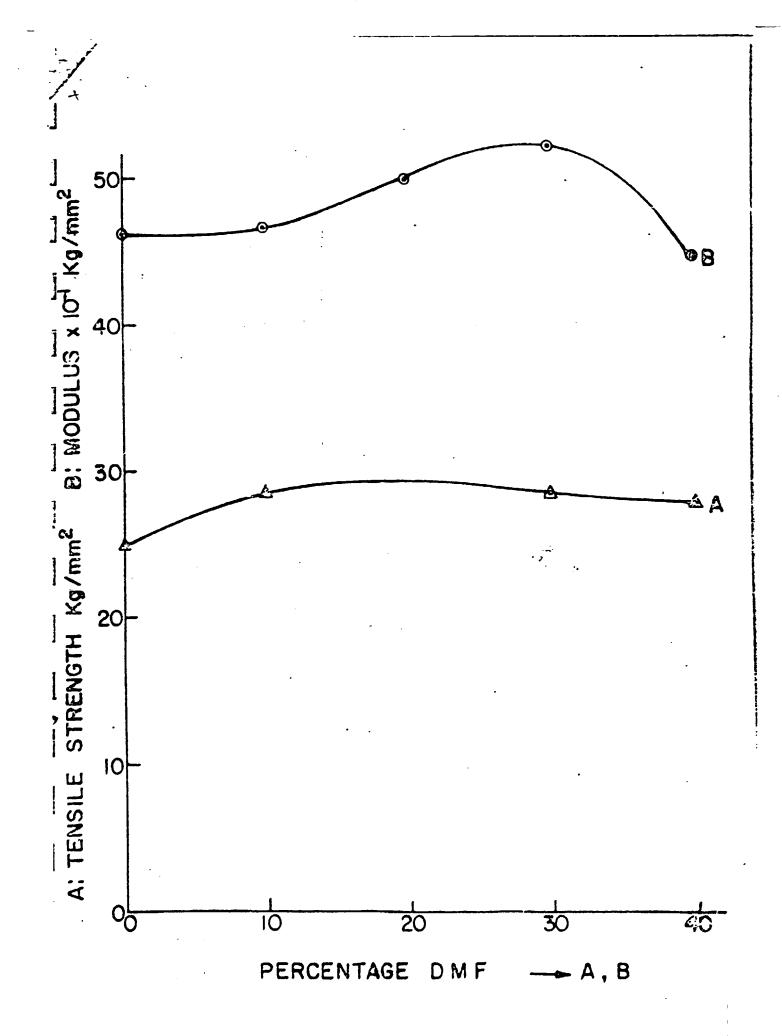
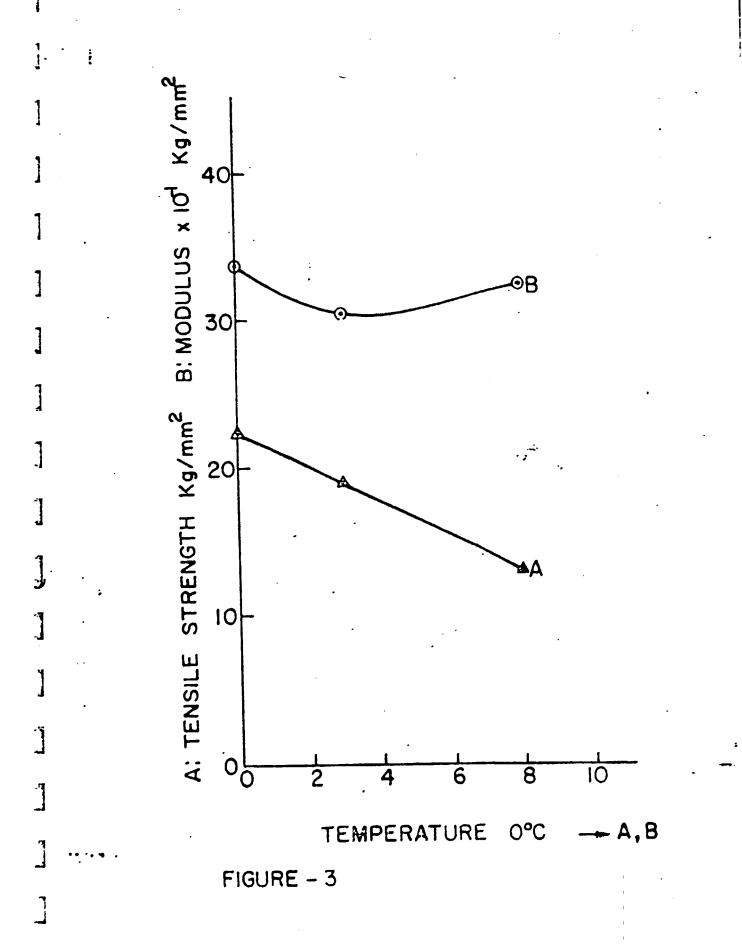


FIGURE -2



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From these observations, it may be concluded that slow coagulation would yield final fibers with favourable physical properties when the DMF concentration of the 2nd coagulation bath is less than 30% which could be due to the further slow diffision of solvent into the 2nd coagulation bath which would have resulted in the increase of proto fibrile density which in turn would reflect in physical properties of the final fibers. Also it was found lower temperature in the coagulation bath, would also result in high density fibers.

CASE III

Effect of pH of the coagulation bath on physical properties of the acrylic fibers.

Spinning conditions :

Polymer concentration: 24% in DMF

Coagulation bath : 50/50 DMF: H₂0

Spinnerette hole dia.: 0,08mm

NO of holes : 50

Spin pump temperature: 60°C

Draw ratio : 5.6

Hot spin temperature: 143°C

Composition of stretch bath: 6% DMF, temp.: 3, C

Coagulation bath temperature: Varied

pH of the coaquiation bath : Varied

In each spinning experiment, the polymer dope was filtered before introducing into the dope hopper. The dope hopper containing the polymer solution was devaccuated before spinning.

The following observations were made:

- Under the same pH and at different temperatures, the cross section of the final fibers found to change from kidney shape at lower pH values, ie, pHs 2.8, 3.8, 6.6 to circular at higher pH values, ie, pHs 9.1, 10.8.
- However, under the same temperature and in different pH values, there was not much effect on the cross section, showing that pH may not effect on the structural aspects of the fibers. However, in certain cases at high pHs voids are noticed in the optical microscopy.
- Density decreased with an increase in the pH of the coagulation

bath, thereby effecting the mechanical properties of the final fibers.

- The increase in pH values found to have diminishing effect in general on tensile strength values of the fibers. At coagulation temperatures of 4°C, 15°C, 20°C, 25°C a decreasing trend in general was observed. However, there are some discrepancies in some places. Overall picture is that there is a decreasing effect.
- -- Modulus values are also in general decreased with increasing pH, however, a decrease and increase and decreasing tendencies were observed. The general trend, however, is of decreasing order. These decreasing trends in tensile strength and modulus would have resulted due to decreasing values of density with increasing pH.

CASE IV

Effect of spin pump speed, size and speed of take-up godet on physical properties of acrylic fibers

In wet spinning, the denier of the fiber depends on several spinning parameters such as, spin pump speed, spin pump size (that controle the pumping of polymer dope into the coaquilation bath), spinnerette hole diameter, number of spinning holes, take-up speed and hot stretch conditions. While keeping all conditions constant, the fineness of the fiber could be improved by increasing the number of holes of the spinnerette. In cases where there are no spinnerettes with a higher number of holes (in our cases we have only 100 holes spinnerette), the fineness can be improved by reducing the spin pump speed there by controlling the polymer pumping into the coagulation bath. When this is also achieved maximum the next parameter that can be used to get the fine fibers is by reducing the spin pump size. However, when the minimum size pump has already been used, then the take-up speed of the first godet could be increased which facilitates to increase the speed of the subsequent godet. This will not only give fine fibers, but also would increase the speed of production. However, when doing so, one may sacrifice the density of the fiber unless the length of coagulation path is increased. Eventhough various reports are available in literature systematic studies on these parameters are lacking and also most of the results are in patent form. In view of this, a systematic study is conducted using different spin pumps, spin pump speeds, take up roller speeds under identical conditions.

spinning conditions in Case IV were:

Polymer concentration : 23% in DMF

Viscosity of spinning solution

at 50°C by ball fall method : time: 23

Coagulation bath composition : 50/50 DMF H₂0

Spinnerette holes : 100

Spinneratte dia. : 0,1 mm

Composition of wash bath : Baths 1 and 3 water

Composition of stretch bath : 6% DMF
Temperature of coagulation bath : 2-3°C
Temperature of hot pin : 170°C

Maintaing the above spinning conditions, in general, the other variables were changed as given in Table 4.

TABLE 4 - SPINNING RESULTS

SPIN PUMP SPEED METERS/MINUTE		SPEED OF TAKE UP GODET 1 METERS/MINUTE	MAXIMUM STRETCH OBTAINED	DENIER OF THE FIBER
stze	3.0	5	7.0	3.990
umps /Rev.	2.0	5	7.0	2.470
nd - m	1.4	- 5	6.4	1.828
Spin pump .6cm ³ /Rev	1.4	7	6.7	1.560
	1.4	5	6.2	1.430
size	1.4	6	5.4	1.370
	1.4	7	5.7	1.009
Spin pump s .4cm ³ /Rev 1.4 1.4		7	6.0	1.020
ıtın .4c	1.4	7	6.3	0.970
્ જે	1.4	8.	5.6	0.960

Using spin pump of size 0,6 cm³/Rev when the speed of the spin pump is — 3M/m a stretch ratio of 7 could be obtained which resulted in a denier of 3.99. When the spin pump is further reduced to 2M/m a stretch ratio of 7 is achieved (difficult), but the denier of the fiber reduced. A further reduced to 1.828. This shows that a decrease in rate of

TABLE 5 - BEST SPINNING RESULTS OF 1983 (LAB. MODEL)

	STRETCH RATIO	DENIER	TENSILE STRENGTH GPa	MODULUS CPa
	5.6	3.79	0.36	5.8
EARLY 1983	5.6	8.20	0.38	5.4
	5.6	1.92	0.34	7.8
	4.9	1.35	0.28 0.34	7.72 9.24
2 nd HALF OF 1983	6.0	1.02	0.28	8.04
	6.3 5.6	0.94	0.421	7.73 9.86

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pumping of polymer into the coagulation would yield finer fiber keeping all other spinning conditions constant. However, the reduction in the speed of the pump will impose a constrain in the maximum obtainable stretch ratio keeping stretch bath conditions constant. Beyond these limits the fibers were breaking in the stretch bath. However, by increasing the take-up godet to 5m/m to 7m/m a slight raise in stretch ratio and denier could be achieved.

When the pump size was further decreased from 0.6 to 0.4 cm³/Rev. still finer fibers could be obtained. As shown in Table 4, when the take-up godet speed is changed, very fine fibers could be obtained.

However, the rise in the speed of take—up godet would impose some restriction in spinning. A quicker removal of the fiber from the coagulation bath might effect the density of the fiber which may in turn result in weaker fibers. In such case, one should compensate by increasing the coagulation path.

On the basis of these experiments, the following conclusions were made:

- A decrease in size of the spin pump would yield fine fiber due to the reduction in the pumping of polymer into the coagulation bath.
- Decrease in spin pump speed would also yield finer fibers due to the above reason.
- Care should be taken to compensate the residence time of proto fiber in the coagulation bath by increasing spinning path.
- The reduction in spin pump size and spin pump speed would impose restrictions on obtainable draw ratio.

Later on hundreds of experiments were conducted. The variations in spinning parameters included spin pump speeds, no of holes in the spinnerette, size of the spinnerette hole, dope composition, etc. The best spinning results of 1983 are represented in Table 5. The results during the later half of the year are comparable with some of commercial fibers.

ii - <u>Spinning Activities at FISIPA</u> (Fibras Sintéticas da Bahia S.A., Camaçari, Bahia)

Meanwhile the pilot plant spinning assembly supplied by UNIDO has arrived. This was assembled at the previously agreed site FISIPA. The

visit of Prof. Falkai was planned at the final stages of the commissioning of this equipment. Myself and Dr Falkai visited again the FISIBA, and the pilot plant spirning assembly site and rectified the small defects and started the initial spinning experiments. The FISIBA scientists were trained in several of the spinning experiments. FISIBA, though a fiber producing industry had no previous wet spinning experience. They were trained in understanding the spinning conditions and crucial points. The preliminary spinning results at FISIBA towards the end of 1983 are presented in Table 6. After the preliminary testing in FISIBA at the plant site remaining tests like density measurements were performed at CTA. In view of the fact that the density of the fiber was less it was adviced to them to perform a set experiments consisting the variations in polymer composition. The experiences in the bench scale experiments at FISIBA enabled to identity and to improve the properties of fibers in the pilot plant. Also, the scientists trained at CTA by me and Falkai further helped the FISIRA people in commissioning the preliminary spinning experiments. In view of mutual contacts between CTA scientists and FISIBA people, the properties of the fibers at the pilot plant were improved. These contacts and the interest shown by FISIBA were slowly growing and FISIBA and its parent organization COPENE - Petroquímica do Nordeste S.A. were understanding the pote talk of carbon fibers. This is very good for a project of this type for further industrialization of this technology in the country.

TABLE 6 - PRELIMINARY SPINNING RESULTS AT PILOT PLANT IN FISIBA

Spinning n ^o	Stretch	Final Denier	TS GPa	Modulus GPa	Density
1	4	5.77	2.22	` -	•
2	2.99	3.1	1.616×10^{-1}	4.31	1.43
. 3	3	2.2	2.449×10^{-1}	5.292	1.14
4	4.11	1.9	2.711×10^{-1}	5.542	1.14
5	4.47	1.9	3.163×10^{-1}	6.119	1.13
6	4.94	1.84	3.21×10^{-1}	5.36	1.18

2.3 - Activities in 1984

i - Spinning Activities at CTA

In order to conduct the preliminary heat treatment experiments on CTA spun fibers, the fibers were spun with selected best conditions of 1983 in larger quantities. Single spinnings were conducted for 7-8 hours with lab spinning assembly at CTA. This time constrain is because of the dope container capacity. However, the fibers were thus spun for prolonged times in a rumber of times keeping the spinning parameters constant. The spinnerette used at CTA had only a minimum of 100 holes. Thus the fibers from a number of bobbins were pooled together. To make this, the precursor group constructed an equipment. These fibers were pooled into a tow consisting of at least 1000 filaments and preliminary heat treatment experiments were conducted at CTA. Upon the analysis of preliminar results on the heat treatment of the CTA spun fibers, it was felt necessary:

- To increase the density of the fiber
- To further stretch the fibers while spinning.

In view of these observations, a set of spin ingrements were designed by me to increase the density of the fiper and to heat stretch the fiber in spinning. These included the spinning with increased dope concentrations and increase path length of coagulation bath.

ii - Spinning Activities in FISIBA

Upon my advice to change the spinning conditions such as dope concentration, etc., FISIRA people have spun fibers again. The spun fibers were sent to CTA. The results of the fibers are given below in Table 7.

TABLE 7 - SPINNING RESULTS AT FISIBA IN 1984

SPINNING NO	FINAL CENIER	TS CPa x 10 ⁻¹	MODULUS GPa	DENSITY
7	1.64	. 3.53	6.258	1.19
	1.71	8.19	5.75	1.15

iii - Studies in Polymerizations

Meanwhile the UNIDO supplied polymerization reactors chemical reagents, initiators and monomers arrived at CTA, polymerization experiments were conducted in smaller scale initially using two monomers, ie acrylonitrile and methylacrylate, and acrylonitrile, methylacrylate and itaconic acid. The smaller scale polymerizations were of 1 litre capacity. These polymerizations were conducted in aquous medium. The polymeris were filtered, dried and characterized. The results are given in Tables 8 and 9.

TABLE 8 - RESULTS OF POLYMERIZATION CONDUCTED IN 1 LITTER CAPACITY USING TWO MONOMERS, ie ACRYLONITRILE AND METHYLACRYLATE

EXPERIMENTS	AN (%)	MA (%)	· TEMPER.	TIME (h)	QUANT. (g)	(\$) Aleid			
A - 1 2 3 4 5 6 7	97 97 97 97 97 97	3 3 3 3 3 3	40- 35- 40- 50- 60- 70- 80	5 5 5 5 5 5 5	104,70 84,91 171,52 171,50 173,94 164,71 172,00	52,35 42,455 85,76 85,75 86,97 82,355 86,00			
B - 8 9 10 11 12	96 96 96 96 96	4 4 4 4	40 60 50 70 80	5 5 5 5	71,71 109,77 157,72 185,24 179,11	35,855 54,885 78,86 92,62 89,555			
C- 13 14 15 16 17 18	95 95 95 95 95 95	5 5 5 5 5	40 40 50 70 80 60	5 5 5 5 5	29,95 58,73 26,84 142,40 165,10 83,56	14,975 29,365 13,42 71,20 82,55 41,78			
D- 19 20 21 22 23	98 98 98 98 98	2 2 2 2 2 2	40 50 60 70 80	5 5 5	53,57	26,7 85			
E- 24 25 26 27 28	99 99 99 99 99	1 1 1 1	50 70 40 60 80	5 5 5 5 5					

TABLE 9 - RESULTS OF POLYMERIZATION CONDUCTED IN 1 LITER CAPACITY USING THREE MONOMERS - ACRYLONITRILA (AN), METHYL ACRYLATE (MA) AND ITACONIC ACID (ITA)

EXPERIMENTS	AN (%)	MA · (%)	ITA (%)	TEMPER. (^O C)	TIME (h)	QUANT. (g)	(%)
A - 29 : 30 31 32 33	96 96 96 96	3 . 3 3 3	1 1 1 1	40 · 60 70 50 80	5 - 5 5 5 5		
B - 34 35 36 37 38 39	95 95 95 95 95 95	4- 4 4 4 4 4	1 1 1 1 1	50 60 70 40 80 80	5 5 5 5 5		-
C - 40 41 42 43 44	94 94 94 94 94	5 5 5 5	1 1 1 1	70 60 80 40 50	5 5 5 5 5		
D - 45 46 47 48 49	94 94 94 94 94	4 4 4 4	2 2 2 2 2	50 40 60 70 80	5 5 5 5 5		
E - 50 51 52 53 54	94 94 94 94 94	3 3 3 3	2 2 2 2 2	40 60 50 70 80	5 5 5 5		
F - 55 . 56 . 57 . 58 . 59	95 95 95 95 95	3 3 3 3	2 2 2 · 2 2	40 50 60 70 80	5 5 5 5		

iv - Planning in Polymerizations

Also several of the polymerizations were planned and the following plan was given to the precursor group:

Planned Polymerization Experiments:

- Polymerization in one liter capacity variation in temperature
- Polymerization in one liter capacity constant temperature
- Polymerization of acrylonitrile in variation in temperature the presence of two comonomers (third monomer)
- Polymerization of acrylonitrile in constant temperature the presence of two componers
- Polymerization of acrylonitrile in the presence of two componers
- Polymerization of acrylonitrile in the presence of two commonomers
- Characterization of these copolymers
- variations in temperature (third monomer)
- constant temperature (third monomer)

v - Scaling up of Polymerization to Higher Capacity

- A Scale up of acrylic polymerizations (using monomers, acrylonitrile and methylacrylate) to 5 liter capacity should be continued.
- B Scale up of acrylic polymerizations (using monomers, acrylenitrile, methylacrylate and itaconic acid) should be continued after the analysis of the preliminary results.

2.4- Additional Spinning Studies

i - Spinning of CTA Acrylic Polymers

In future, the best of CTA polymers have to be spun using the previous and modified spinning parameters. The group was advised by me on this. I have also advised the group to prepare polymers of type B in 10 liter capacity after looking at the initially spun A and B CTA polymers. These polymers have to spun using the previously developed spinning conditions.

ii - Planning in New Spinning Methods

Spinning of acrylics polymers using inorganic spinning solvents:

I have advised and gave the planned sheets of the type enclosed to spin

the acrylic fibers using inorganic solvents. Inorganic solvents would permit in using high spinning temperature in the coagulation bath which would result in circularity in cross section of spun fibers. These inorganic solvents could be sodium thiocynate and zinc chloside. Representative planned sheets are enclosed as Tables 10 and 11.

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DATE:

SPINNING VARIABLE

POLIM.CONC.: Different polymer concentrations, ie 10-30% have to be used in 55% NaScN COMPO.COMG. PWIH: Diff.solvent/H2O compositions have to tried (10 to 30% Na3dN)

SPINNERHT HOLE DIA.: Available spinneretts have to be used

SPINNERET Nº OF ROLES: Spinnerette with higher spinnerette holes to be used

POLYMER BATCH No: use Tin polyment

to be determined every line VISCOSITY:

AT TEMP. :

Conditions	ر مر	Spi Ինո	in up		Spec	eds (of		oc i		h Rai	_	S P.	t. ath	0	ده ور:	Den:	ier	Are .	g/cm ³	٠ ٠,	•		- [15]	(m)	: or	(TC:	
	Jemp Spin Bloc	Size	71 m/m111	G /mim/m	යි දෙ/min	תוש/נו	m/min	m/min	Temp. Joag.Bat	Jo - dino:	Temp.oc	Temp.oc Comp.	Temp. OC	Сопр.	St.Ratio	Hot plate	l'et	Dry	Cross A	Density g/cm ³	Cross >	5 DNF in fibre	TS kgil/m=-	N Kg:		Freq. 35	.:. (K.)	
Use best of									l				<u> </u>															
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TAPLE 11 - PLASTING OF SPINNING USING ZINCCHLORIDE.

SPINNING VARIABLE

NOTE: Detail sheet were given to the Precursor Group

DATE:

WHIM.CONC.: Use 10 to 25% polymer compositions and arrive opt.compsitions

CONFO.COAG.RATH: Use 20 to 50% ZnCl2 concentration and arrive at good composition

STYLNERET HOLE DIA.: Use available spinnerettes

SMINNERET NO OF ROLES: Use spinnerette with maximum no of holes

POLYMER BATCH No: Use CTA polymer

VISCOSITY:

AT TEMP. :

Conditions	' l	Sp: Pur	np		Spe	eds	of		ာ လူ	,	h Par	ths 3	S	t. ath		၁၀ ခ	Den	ier	Area	g/cm5	ů			- E			(70:	
Patch no	Spin Bloc	Size	RPM m/min	G m/min	R m/min	S m/min	S m/min	S m/min	Temp.	Temp. oc	Temp.oc	Temp.oc Comp.	Тетр. ^о С	Comp.	St.Ratio	Hot plate	Net	Dry	Cross Ar	Density	Cross Sec.	on fibre	1S kg L/ma-	N.	Order (a)	Freq Fa.		Supply 1
Use best of p	prev	ious	spi	nnir	g re	sult	s ar	d mo	di fy	whe	reve	r an	d wh	enev	er r	equi	red.											!
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3.0 - Development Activities in Heat Treatment

3.1- Activities in 1982

i - Position at the Time of my Arrival

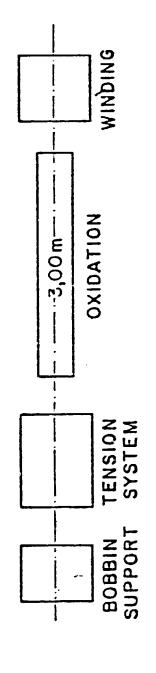
Just before my arrival, the previous Chief Technical Adviser, Dr O.P.Bahl left the Project. At Centro Tecnico Aeroespacial, the heat treatment activities were abandoned on FISIBA commercial grade fibers, the research and developmental activities started already using imported special grade acrylic fibers supplied by Courtaulds, England. At this time, the developmental activities on heat treatment were conducted using the heat treatment system of the type shown in Figure 4. The best results on FISIBA fibers at the end of 1981 are shown in Table 12.

ii - Activities After my Arrival

Several studies were conducted in 1982. Several of the parameters in heat treatments were changed due to the advices of other experts who visited the project site. The studies were concentrated mainly using Courtauld's SAF precursor. Several of experiments were conducted in heat treatment.

Tables 13 and 14 and figures 5 and 6 show some of the initial studies on Courtauld's fibers on the effect of heat treatment temperature on tensile strength and modulus. The best results of heat treatment studies in 1982 are represented in Table 14A (continuous process) and table 14B (discontinuous process). Also, in order to find out the effect of air flux during oxidation stage, several experiments were conducted both in the presence and absence of moved air. The results are presented in Table 15.

FIGURE 4 - I OLD SYSTEM



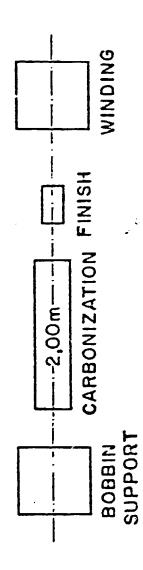


TABLE 12 - BEST RESULTS OF 1981 - ONE STEP OXIDATION (FISIBA PRECURSOR)

		OXIDATION			CARBO	NIZATION	CARBON FIBERS PROPERTIES		
,	ELONGATION	TEMPERATURE OC	RES.TIME MIN.	ATMOSPHERE	TEMPERATURE OC	RES.TIME MIN.	ATMOSPHERE	T.S.	MODULUS
CORTINUOUS PROCESS	+7	230	180 ·	AIR -	1000	120	ARGON	200x10 ³ PSi 1,38 GPa	20x10 ⁶ PS1 138 GPa
DISCONT. PROCESS.	+6	220	220	FORCED A1R	1000	120	ARGON	345x10 ³ PSi 2,30 GPa	26x10 ⁶ PSi 180 GPa

TABLE 13 - EFFECT OF CAPBONIZATION TEMPERATURE

CARBON TEMP.	DENSIT:	CROSS AREA 10 ⁻⁵ mm ²	TENSILE STRENGTH (GPa)	TENSILE MODULUS (GPa)
1000	1,80	37,3	1,7 + 0,5	180 [±] 27
1100	1,76	36,9	2,1 + 0,6	190 - 22
1200	1,76	37,1	2,2 - 0,5	180 - 23
1300	1,75	36,3	$2,6 \div 0,7$	200 ⁺ 25
1400	1,75	35,4	2,7 + 0,6	212 - 31
1500	1,75	34,8	2,1 - 0,6	215 🛨 29
1600	1,77	35,3	$1,6 \stackrel{+}{-} 0,4$	215 ± 23
1800	1,77	35,5	$1,6 \stackrel{+}{-} 0,5$	216 - 23
2000	1,79	34,5	1,5 ± 0,4	245 - 29
2250	1,81	34,8	1,8 - 0,4	222 - 36
2500	1,86	33,5	1,9 + 0,5	279 [±] 36

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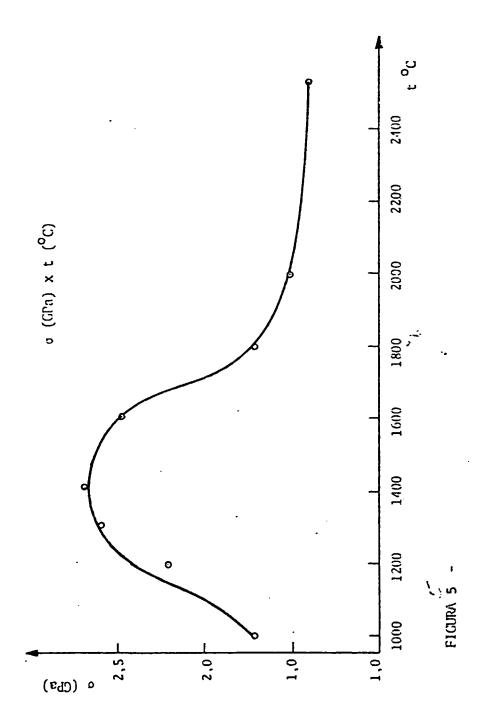
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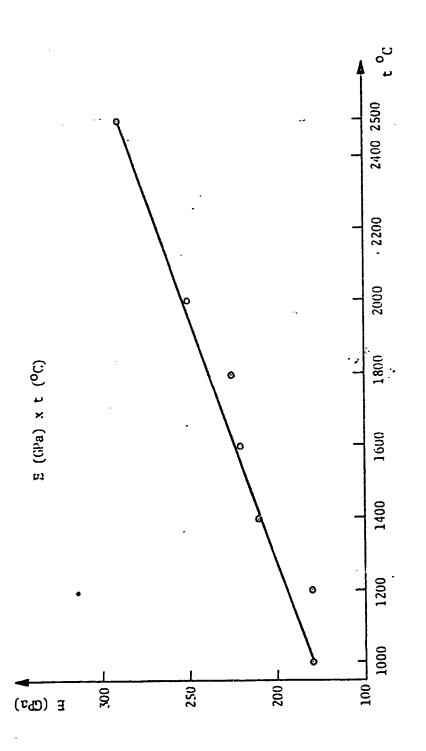
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TABLE 14 - EFFECT OF STRETCH DURING CARBONIZATION

STRETCH	DENSITY g/cm ³	CROSS AREA	TENSILE STRENGTH (GPa)	TENSILE MODULUS (CPa)
0	1,80	38,4	2,1 + 0,4	176 - 30
5	1,78	35,4	2,2 - 0,4	199 - 35
10	1,77	35,1	2,5 + 0,3	203 [±] 19
15	1,78	32,9	2,8 - 0,4	210 - 25
	0 5 10	g/cm ³ 0 1,80 5 1,78 10 1,77	g/cm ³ 10 ⁻⁵ man ² 0 1.80 38.4 5 1.78 35.4 10 1.77 35.1	$\begin{array}{cccccccccccccccccccccccccccccccccccc$





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FIGURA 6 -

TABLE 14A- BEST RESULTS OF 1982 (COURTAULDS SAF PAN)

CONTINUOUS PROCESS

ELONGATION PRE-STRETCH	TEMPERATURE PRE-STRETCH OC	PRE-OXID. TEMP. OC	OXIDATION TEMP. OC	RES.TIME PRE-OXID. MIN.		ATM.	TEMP. CARB. * OC	RES.TIME CARB. MIN.	ATM. CARB.	T.S.	MODULUS
+6	190	220	230	60	120	ΛIR	1100	120	ARGON	275x10 ³ PSi 1,90 GPa	21×10 ⁶ PSi 145 GPa

* SHRINKAGE = (8-9)%

TABLE 14B - BEST RESULTS OF 1982 (COURTAULDS SAF PAN)

DISCONTINUOUS PROCESS

ELONGATION OXID.	TEMPERATURE OXID. OC	RES,TIME MIN.	ATMOSPHERE OXID.	TEMPERATURE CARB. * OC	RES.TIME MIN.	ATMOSPHERE CARB.	T.S.	MODULUS
+6	220	200	FORCED AIR	1100	120	ARGON	350×10 ³ PSi 240 GPa	2,8x10 ⁶ PSi 193 GPa

* SHRINKAGE = (8-9)%

TABLE 15 - EFFECT OF AIR FLUX ON THE PHYSICAL PROPERTIES OF CARBON FIBERS

					MULIM	AIR FLUX					
Stretching:	19	0 ⁰ С	23	0°C	26	5 ⁰ C	1000°C	1000°C	1000°C	1000 ⁰ C	1000 ⁰ C
Ratio	Density	Weight/m	l'ensi ty	Weight/m	Density	Weight/m	Density	Weight/m	Cross Arca	Tensile	Tensile
(\$)	(g/cm ³)	(ang)	(g/cm ³)	(nıg)	(g/cm ³)	(mg)	(g/cm ³)	(mg)	(µm²)	Strength (GPa)	Modulus (GPa)
-5	1,21	779	1,35	806	1,43	795	1,77	451	42,5	2,4 ± 0,7	199 ± 32
Ü	1,21	711	1,35	749	1,43	755	1,77	422	39,7	2,0 = 0,6	204 [±] 28
+5	1,21	690	1,35	698	1,43	725	1,77	404	38,0	2,2 + 0,7	214 [±] 52
+10	1,21	668	1,35	693	1,43	707	1,77	400	37,7	2,8 + 0,4	220 ± 30
				Ŋ	ITH FLUX	OF 35L AIR	/MIN.				
-5	1,21	765	1,32	816	1,46	793	1,75	450	42,8	2,1 ± 0,4	166 [±] 16
0	1,21	740	1,30	758	1,46	780	1,75	438	41,7	1,8 - 0,5	156 - 25
+\$	1,21	714	1,30	714	1,46	727	1,75	413	39,3	2,0 - 0,6	188 [±] 28
+10	1,21	673	1,30	674	1,46.	693	1,75	405	38,6	2,7 = 0,5	197 ± 19

3.2- Activities in 1983

In view of the so-far gained experience, a few modifications were effected in the design of the existing lab. model processing equipment. For easy handling and temperature control, the existing stabilization furnace was cut into two. UNIDO supplied trios were introduced in between the furnaces for easy controlling of the movement of the fiber during processing. The modified versions are shown in Fig.7 and 7A which also include the winding equipment supplied by UNIDO.

Meanwhile CTA/PMR has built a new building for the carbon fiber group, the oxidation and carbonization processing equipment was assembled in line for the continuous processing in the new building.

In view of the several of the experiments conducted by the group and due to availability of useful results, I inspired the group to present the results in the American Carbon Society in 1983 in San Diego. The group and myself identified the subject and more vigorous studies were conducted on these lines. Also the expert Th. Mueller was very much helpful in this venture. Prof. Fitzer had also encouraged the group. This is for the first time the CTA/PMR Carbon Fiber wroup presenting results in an outside Conference. In view of these effects, a paper (Annex I) was presented. The results were appreciated by the participants in the Conference.

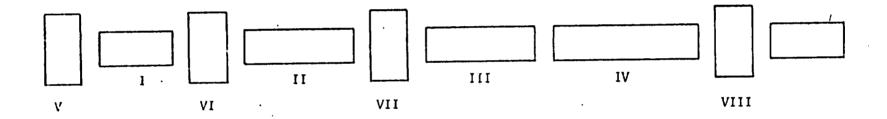
3.3- Activities in 1984

i - Studies in Heat Treatment

As per the advice of the expert Dr Kalnin, experiments were conducted by modifying the processing conditions. The main aspect of these studies were modified stabilization temperatures. Stabilization studies were conducted at three stabilization temperatures, ie, 220-230°C, 250-270°C and 270-300°C. From these studies it was observed that closer the individual furnaces, better properties were obtained. DSC experiments were conducted at every stage of heat treatment. Some of the results using three stabilization experiments are presented in Table 16 and Figures 8 and 9.

In order to explore the additional oxidents, studies were conducted

FIGURE 7 - LINE DIAGRAM OF PROCESSING EQUIPMENT USED FOR RESULTS IN TABLE 16, FIGURES 8, 9.



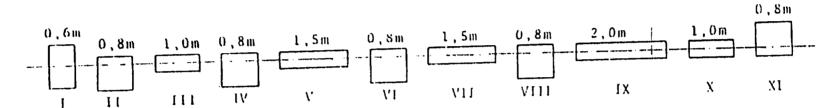
I, II, III - Stabilization furnaces

IV - Carbonization furnaces

V, VI, VII, VIII- Trios

1X - Bobbin

FIGURE 7A - NEW INSTALLATION OF CARBON FIBER PROCESSING EQUIPMENT



I - P.A.N.

II - Trio nº 1

III - pre-stretching

IV - trio nº 2

y - stabilization furnace nº 1

VI - trio nº 3

VII - stabilization furnace nº 2

VIII- trio nº 4

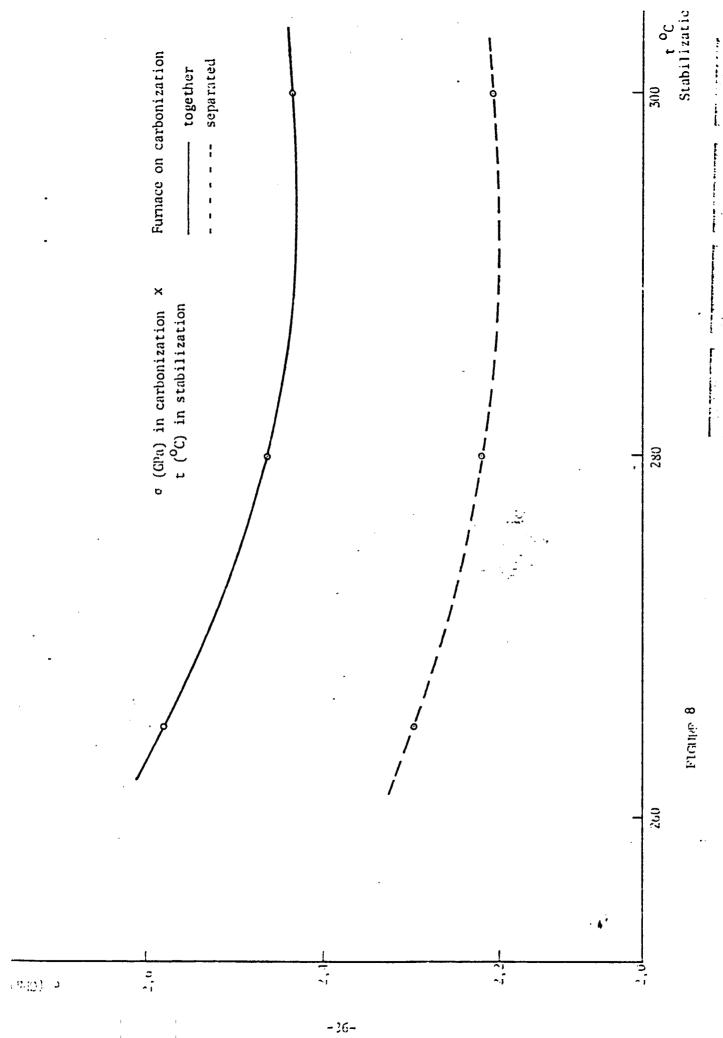
IX - pre-carbonization furnace

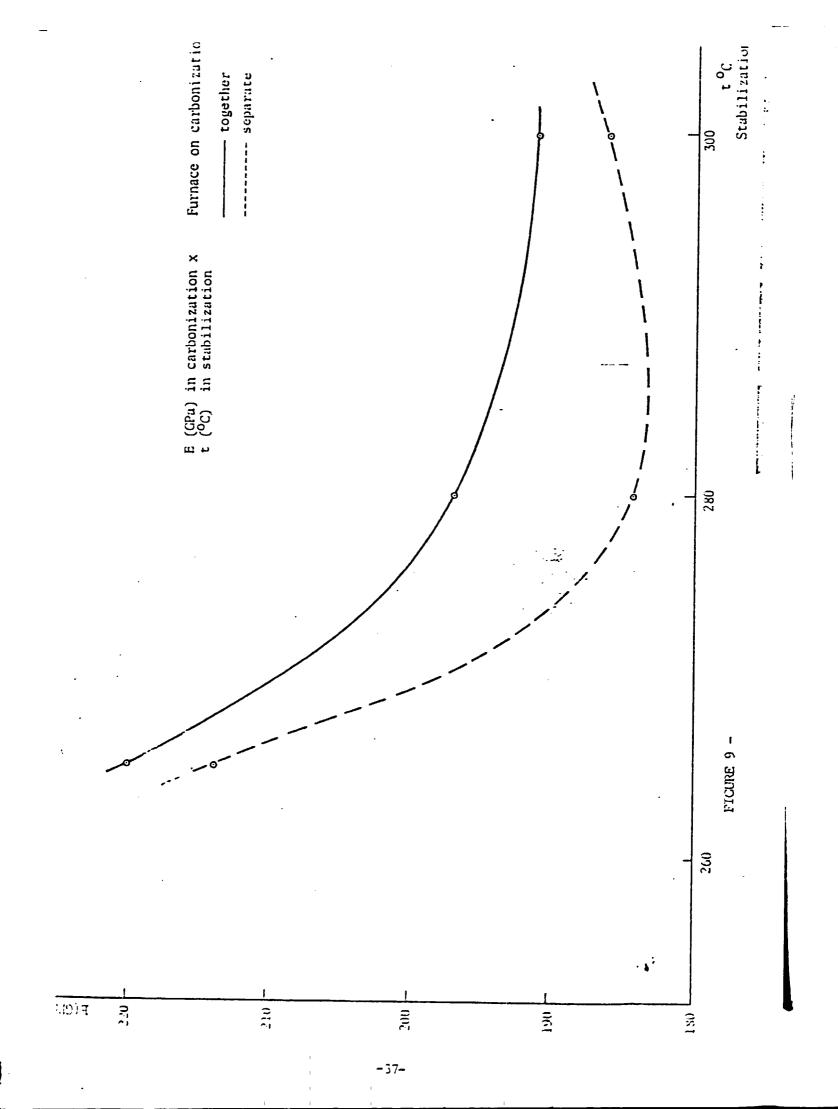
X - carbonization furnace

XI - winding

16 - RESULTS OF CARBONIZATION USING 3 STAGES STABILIZATION

	•	. 1		S	TEP 11	·s	TEP 11	Ι				S7	EP IV		
		···	·								TOGETHER		S	EPARETED)
Temperature OC	²⁰⁰ A	200 _B	²⁴⁰ C	230 _A	230 _B	²⁸⁰ C	265 _A	280 _B	³⁰⁰ C	1.100 _A	1.100 _B	1.100 _C	1.100 _A	1.100 _B	1.100
Linear density (mg/m)	676	676	723	708	708	732	718	704	697	382	351	350	371	344	356
Volume density (g/cm ³)	1,22	1,22	1,36	1,38	1,38	1,46	1,45	1,48	1,51	1,14	1,72	1,72	1,72	1,70	1,76
DSC Fest (°C)	217	217	245	255	255	310	*	*	*	-	-		<u>.</u>	-	-
tm (°C)	308	308	328	343	343	350	*	*	À	-	-	_	-	-	-
ւհ (⁰ Մ)	2,79	2,79	0,763	0,550	0,550	0,210	*	*	*	-	-	-	-	-	-
Young's modulus (GPa)	10,6	10,6	7,2	8,34	8,34	6,47	9,32	9,12	9,05	220	197	192	214	184	187
Tensile strength ((Pa)	0,58	0,58	0,31	0,35	0,35	0,21	0,24	0,22	0,21	2,58	2,47	2,39	2,30	2,22	2,31
	A	В	C	A	B 	c	,; 	В	C	A	B	C	A	. <u> </u>	c
* Complete	1														





using NO_2 as the oxidants. It was observed that NO_2 stabilization did not improve the physical properties. These results were presented in Carbon 84 Conference in France (Annex II).

ii - Activities in Oxidized Polyacrylonitrile (PAN-Ox)

PAN-Ox is a good substitute for Asbestos. It is a heat resistant material and has several of industrial applications. Some of the companies which participated in the Conference at CTA were interested to use oxidized polyacrylonitrile fiber as thermally resistant materials. A company ASBERIT has tested CTA PAN-Ox material and were pleased to inform us that it can be used and they have a demand of 60 ton per year. The physical properties of this PAN-Ox are given in Table 17. As per the requirement of the ASBERIT company about 3.0 Kg of the processed PAN-Ox fiber were sent for testing at ASBERIT Co.

TABLE 17 - PHYSICAL PROPERTIES OF CTA
OXIDIZED FIBER

Fiber no : CTA PAN OX-1

Tensile strength : 0.175 GPa

Modulus : 6.577 GPaDensity : 1.498 g/cm^3

Denier : 1.0888

Elongation : 10%

Nº of filaments : 18000

Tenacity : 1.3 gm/denier

1.29 gm/dtex

Breaking strength: 1.57 gm

Filament dtex : 1.2088

Heating temp.final: 300°C, (first 230)

Residence time : 120 minutes

4.0 - Developmental Activities in Surface Treatment

Surface treatment of carbon fibers is very important to form good composite with resin. The bonding of resin to the fiber depends mainly on the groups present on the surface of the carbon fibers. Poor bonding results, poor properties in final composites. The surface treatment to carbon fiber is done by different methods. For example, electrolytic oxidation, acid treatment alkali electrolysis, thermal oxidation, etc. In our group we have initiated surface treatment by electrolytic processo.

4.1 - Activities in 1982

At the time of my arrival, a few experiments were already conducted using nitric acid for the surface treatment of the carbon fibers. Due to non availability of uniformly processed carbon fiber, the developmental activities were postponed. However, attempts were made to acquire the materials and personnel for this development.

4.2 - Activities in 1983

With the formation of a group in surface treatment, the activities restarted. Anodic oxidation equipment was assembled by the CTA group in view of the information and assistance given by UNIDO experts, a few surface treatment experiments were conducted using CTA processed carbon fibers. A 20% surphuric acid was used as the electrolyte. About 125 meters of the fiber was surface treated. Unidirectional composites were made using epoxy resin DER 383 (Dow) and curing agent DEH 50 (Dow These composites were tested. In the subsequent experiments, the graphice electrode used earlier was replaced. Modifications were made using glassy carbon tube made out of polyperfural alcohol resin in CTA. Also subsequently several other modifications were made in the electrolytic cell. Also the experimental conditions such as current density, electrolyte were changed and several of the experiments were conducted. Meanwhile, it is felt that we should get untreated carbon fibers from a commercial firm and surface treat them in order to standardize the surface treatment work. In view of our latest contacts with RK Textiles UK, sample of the untreated carbon fiber was obtained and surface treated with improved parameters. The Tables 18, 19, 20, 21 and 2? shows some of the results of surface treatment.

TABLE 18 - TYPES OF FIBERS USED FOR SURFACE TREATMENT

SAPLE	TYPE OF FIBERS
1	PMR 428
2	PMR 429
3	PMR 432
4	SIGRAFIL
5	RK

TABLE 19 - DENSITIES OF SURFACE TREATED AND UNTREATED FIBERS

SAMPLE	NON SURFACE TREATED g/cm ³	SUPFACE TREA g/cm ³	TED.
1	1,75	1,78	-
2	1,75	1,76	-
3	1,75	1,79	
4		1,78	
5	1,74	1,74	

TABLE 20 - PROPERTIES OF SINGLE FILAMENTS

Sam le	TREAT: EVT	TENSILE STRENGTH	MODULUS
		(@a)	E (GPa)
1	NT	2,4	190
	T	2,19	171
2	NT	2,4	190
	T	3,1	186
3	NT	2,7	190
	T	2,56	188
. 4	T	2,34	196
5	NT	3,25	222
	T	2,20	212

NT = Non-surface treated

T = Surface treated

TABLE 21 - PRIPERTIES OF CARBON FIBERS/EPOXY RESIN COMPOSITES (VOLUME FRACTION: AROUND 60%)

SAMPLE	TREATHENT	FLEXUPAL STRENGTH FS (MPa)	MODULUS E (GPa)
1	NT	1121	70
	T	988	80,5
2	T	973	79,5
3	NT	1614	117,5
	T	1100	81,2
4	т	1520	123,7

Table 22 - INTERLAMINAR SHEAR STRENGTH - ILSS

SAMPLE AND TREATMENT	ILSS (MPa)
2 T	45,3
3 T	42,0
4 T	54,1
5 NT	41,1
5 T (step 1)	49,8
5 T (step 2)	46,3
5 T (step 3)	40,6
5 T (step 4)	50,5

(Steps 1 to 4 = different current densities)

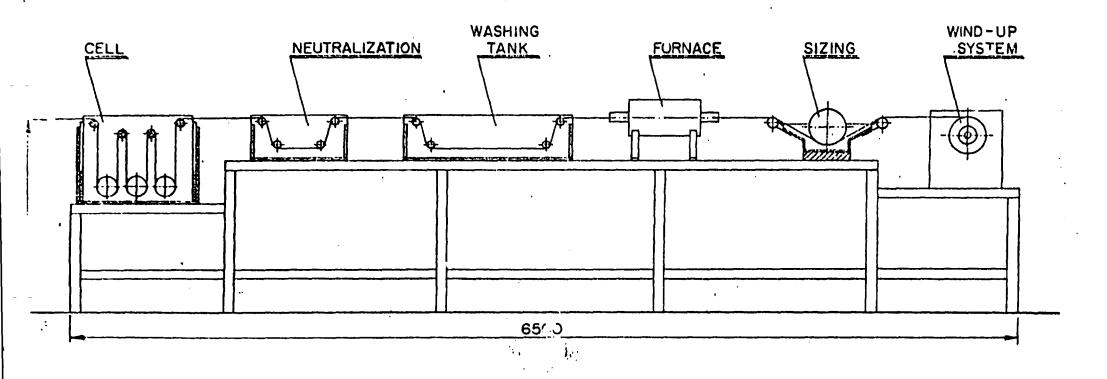
4.3 - Activities in 1984

i - Pilot Plant Surface Treatment Apparatus

Eventhough currantly batch scale surface treatment work is goin on in order to fix the surface treatment parameters, the final objective is to introduce a surface treatment equipment in line with the carbonization processing equipment. Such as equipment should be able to process 6 K tow at the rate of 1 to 30 m/h. After a detail analysis a cell was designed. Contacts were also made with local companies for the construction of this cell. This cell after completion will look like figure 10.

ii - Sizing

An equipment has been fabricated for the sizing of the surface treated carbon fibers. This will also go on line in the total carbonization equipment. A few batch scale experiments were already performed for sizing using 2% epoxy resin DER 757 (Dow) dissolved in acetone.



igure 10- LAY - OUT OF THE CARBON FIBRE PILOT PLANT SURFACE TREATMENT UNIT

5.0- CONFERENCE IN APPLICATIONS OF CARBON FIBERS

In order to expose the local scientists about the extensive applications of carbon fibers and to consolidate hitherto obtained results in PAR/CTA, an international conference on the applications of carbon fibers was planned to be field in CTA during Dec 1983 under the sponsorship of CTA, UNIDO and UNESSTD. About nine experts in the field were invited to give conference lectures on applications of carbon fibers in their respective countries. The deliberations were held in CTA from 5th Dec - 7th Dec. Also participants from developing countries like Argentina, China, Egypt, Korea and Mexico have participated and benefited by the conference procedings. About 212 participants from Brazil attended the conference. On 8th and 9th Dec UNIDO, UNDP, UNFSSTD representatives together with the invited experts visited FISIBA to witness the developmental activities on UNIDO supplied pilot plant spinning assembly. The final conference report is enclosed as Annex III.

6.0- PROJECT ACTIVITIES - GENERAL

The general aspects of Project developmental activities were reported to UNDP in form half yearly progress reports and to UNIDO in form Project Evaluation Reports.

7.0- ANALYSIS

Detailed analysis with respect to the outputs activities and objectives were brought out in the latest UNIDO Project Evaluation Peport,

Annex IV. The comments of UNIDO Project Evaluation unit are worth to note on 1984 PER, ie Annex IV.

8.0 - ADDITIONAL OUTPUTS

The additional outputs achieved but not mentioned in the Project Document are worth noting.

- For pilot line of carbon fiber processing, a new building became necessary and was built.
- ii New clean conditioned laboratories were built for chemical, analytical and testing purpose within the Carbon Fiber Project.
 PAN-Ox activities with ASPERIT Co have started.
- iii Utilities for the pilot plant carbonization furmace were supplied by CTA.
- iv A group of experienced personnal in composites were included who would work in the 2nd phase on applications of carbon fibers, if approved.
- v An international conference on carbon fibers conducted with the sponsor ship of CTA/UNIDO/UNFSSTD.
- vi Additional testing and analytical apparatus not entired in the Project Document were developed, such as: denier more, flash evaporator, fiber density measuring equipment, equipment to measure critical solution time, etc.
- vii 2nd phase document on applications of carbon fibers completed and sent to the Government for the submission to UNDP/UNIDO.

9.0 - INDUSTRIALIZATION OF CARBON FIBER TECHNOLOGY

Industrialization activities involvement of COPENE - Petroquímica do Nordeste S.A.

COPENE - Petroquímica do Nordeste S.A. is interested in scaling up activities. In view of this, visits were made from both sides ie CTA and COPENE. A document prepared by COPENE is under examination at CTA. COPENE is very much enthusiastic to scale up carbonization and in producing PAN-Ox.

10.0- ANALYSIS ON COUNTERPART SCIENTISTS SELF-RELIANCE AND INDEPENDENCE

In course of 2.1/2 years of my stay, I have seen the steady growth in the counterpart scientist's confidence and self-reliance. They have improved very much in solving the problems by themselves. Now I can see a good change from dependence to independence. At the beginning, everything was taken for granted and was done as told. Slowly this changed from how to why. The counterpart scientists are looking answers for questions. This gave them self-thinking capacity.

The initial dependence on experts has declined in course of time as one may notice from the figure 11. The counterpart scientists who were trained at CTA are helping the people in FISIBA in scale-up activities. The initial and first paper (Annex 1) consisting CTA results were presented by CTA counterpart scientist in 1983 with a maximum help and backing of international experts. In 1984, the counterpart scientists gained confidence and presented additional results (Annex II) in France, with minimum assistance and backing. This shows the confidence of the counterpart scientist.

Based on the knowledge gained due to the visits of UNIDO experts, the counterpart scientists are now thinking new areas of research within this Carbon Fiber Group.

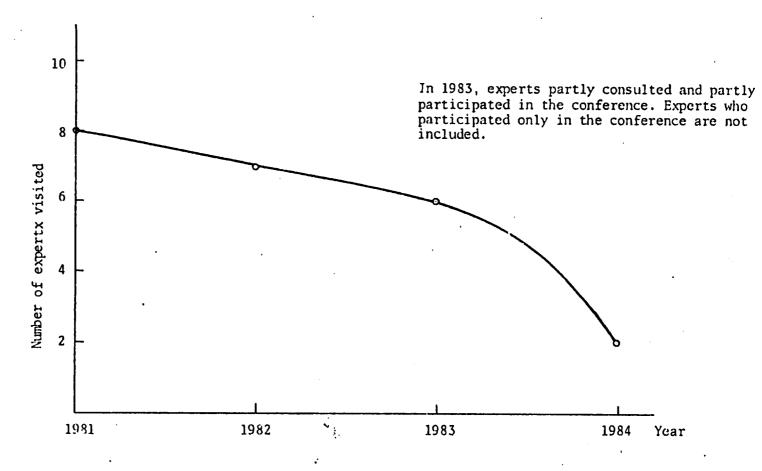


Figure 11.

11.0- RECOMMENDATIONS

i - In R & D Activities

- The Precursor Group should synthesis more polymers as mentioned in Chapter 2.3 and should characterize the same.
- The Precursor Group should spin acrylic polymers and develop new spinning procedures and develop new parameters as mentioned in Chapter 2.4.
- The Precursor Group should advise these to FISIBA.
- The Heat Treatment Group should work with pilot plant C-fiber plant continuously for week at least without stopping.
- The Heat Treatment Group should process the commercial acrylic fibers for PAN-Ox applications, and also explore industries to use carbon fiber on commercial level application such as activated filters, etc.
- The Surface Treatment Group should introduce the surface treatment equipment in the line as soon as possible.
- The composites group should be given materials and analyse the processed carbon fibers in form of composites.
- Whenever necessary, scientific workshops may be conducted to appraise the latest development in this technology.

ii - General Nature

- The 2nd phase on applications of carbon fibers should be started in continuation of the present project in order to consolidate the achievements obtained in the present project.
- All attempts should be made not to loose the so far UNIDU trained counterpart scientists in the development of this technology.
- The terms for cooperation with COPENE to industrialize the carbon fiber technology developed in this Project should be finalized as early as possible. Necessary assistance should be given to COPENE in their venture to industrialize carbon fibers.

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INFLITENCE OF PROCESSING VARIABLES ON CARBON FIBRE PROPERTIES IN A CONTINUOUS PROCESSING SYSTEM

T.NACABEUSHANAN, TH.MULLER", A.E.SIMIONATO, J.L.GOMES DA SILVA

CENTRO TÉCNICO AEROESPACIAL - IPD - POR São José dos Campos, São Paulo, Brasil

LANCOUCTION

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Young's modulus and tensile strength of carbon fibres depend strongly on the preferred orientation of carbon layers in the fibres (ref. 1, 2, 3). The preferred orientation of these layers can be increased by stretching the fibres during all stages of C-fibre production. In case of PAN-based C-fibres the prestretching of the initial PAN-fibres is most effective in order to increase modulus (rof. 4, 5) and tensile strength (ref. 5, 6). Tensile strangth, however, is influenced by defects in the fibres, which can be created in all steps of the process. Especially the oxidation of PAN is very sensitive with respect to the creation of defects, so that the various parameters of this step must be optimized in order to obtain high quality carbon fibres (ref. 7, 8, 9).
This paper is concerned with the influ-

ance of the degree of prestretching and oxidation process parameters on intermediate products and on the properties of resulting C-fibres from PAN:

EFFERINGER

A commercially available special PAH-fibre (S.A.P.1/6E/1.22 from COURTAULDS, ref. 19): was used for the studies. The procersing into carbon fibres was done in four subsequent continuous steps:

- A- Prestretching from 0 to 15% in hot air at 150°C
- 8- Oxidation at constant length in hot air at
- 8- Oxidation at constant length in hot air at 265°C constant length length length in hot air at 265°C constant length l
 - ing a shrinkage of about 7%.

For the steps A, B and C a tube furnace of 3 m length was used, through which the fibres have been drawn by roller system. In the oxidation steps B and C the amount of forced air and the residence time have been . varied. For carbonization (step D) the fibres have been drawn through a tube furnace purged with ergan without variations of residence time and final temperature.

The properties of the fibre as density, young's modulus, tensile strength and the mass changes were determined after each pro cassing step. For density measurements a float sink method was used (ref. 5). The mechanical properties of the fibres were measured on an Instrum at a gauge length of 25 mm and a cross head speed of 2,5 mm/min. in case of C-fibres and 10 cm/min. for the other fibres.

RESULTS

The increase in fibre density gives information on the progress of oxidation. As can be seen in Figure 1, during the prestretching at 190°C (step A) nearly no oxidation occurs. During step B (oxidation at 230°C) the density increased by 0,15 g/cm. Applied forced air flow reduces the density increase. forced air flow causes an opposite effect on the further density increase during step C. Nearly no influence of air flow on the total density increase after steps A to C can be detected.

The young's modulus of the precursor fibre decreased continuously during the steps A to C (Table 1). Forced air flow diminishes this decrease. Increased preferred orientation achieved by prestretching in step A, causes higher absolute values for the modulus, while the highest applied prescretching (15%) reduces the modulus again slightly.

The influence of prestretching on the modulus of the resulting carbon fibres is shown in Figure 2. As expected, the modulus increases with increased degree of prestretching. Increased air flow during oxidation steps B and C diminishes, the modulus of C-fibres for lower degree of prestretching.

SUZCHART

An influence of the investigated process variables, prestretching and forced air flow the oxidation steps can be found at the intermediage products and on the finally resulting carbon fibres. Changes in the air flow mainly influence the intermediate products after step B and C as found by the density measurements. No or low air flow rate accelerates the strongly exothermic cyclization is step B auto catalytically by the unsufficient heat transfer from the fibre to the zir. The oxygen uptake during exidation of PAN requires at least partly cyclized fibres (ref.5, 11), so that it can be assumed that it occurs mainly during stop C. High air flow rates facilitate this difusion controlled rates.

The iecreasing modulus of fibres after the oxidation step B and C support these explanations.

The legree of prestretching influences mainly the modulus of the resulting carbon fibres. Increasing preferred orientation achieved by prescretching of the PAN-fibre increases the modulus.

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ACKIOULEDGENENT

The authors are highly thankful to Prof. E.Fitzer, University of Karlsruhe, W. Germany for his constant encouragement, inspiration, sustained interest and for his valuable comments in the work, to T. Cel Resset, Chief of the Division for his interest, support and facilities and to United Nation Industrial Dewelopment Organization (Vienna) for sponsoring the project.

- * UNIDO expert, formaly was at University of Lowell, Dept of Chemistry, Lovell, Mass., 01854, USA
- se UNIDO expert, formaly was at Institute Fur Chemische Technik, University of Karlsruhe, West Germany:

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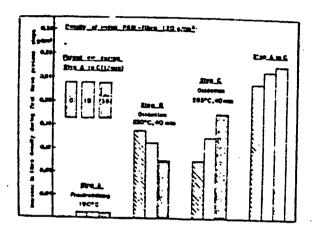


Figura 1. Increase of fibre density ACTOR process steps A, 5 and C.

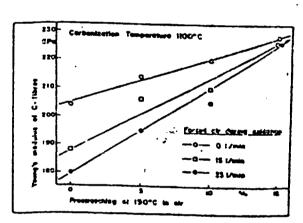


Figure 2. Influence of prestretching on the young's modulus of resulting carbon fibres.

Table 1. Young's modulus of fibres after process step A, B and C (Initial modulus of PAN precursor fibres was 10.8 GPa

FORCED AIR FLOW L/MIN.)		0				15				35			
DEGREE OF FRESTR	ETCHING	0	5	10	15	0	5	10	15	0	5	10	15
	STEP A	10.0	11.1	11.7	11.4	8.5	10.0	9.8	8.9	10.1	10.6	11.6	10.5
YOUNG'S MCDULES OF FIBRES (G74)	STEP 3	7.1	7.6	7.2	6.3	7.5	3.5	7.7	5.9	7.6	9.5	9.3	7.:
STEP C		6.4	6. 7	6.8	6.4	6.4	. 7.3	7.2	6.0	7.6	7.6	7.5	6.9

CARBON FIBRE GHARACTERISTICS OBTAINED FROM STABILIZED PAN IN NO2 ATMOSPHERE

A.E.SIMIONATO AND J.L.GOMES DA SILVA CENTRO TÉCNICO AEROESPACIAL - IPD - PMR SÃO JOSÉ DOS CAMPOS, SÃO PAULO, BRASIL

SYNOPSIS

It is shown that NO_2 decreases the time required to stabilized PAN fibres suitable for carbon fibre production. There is also a modest improvement in strength. NO_2 in excess, however, is found to be deletereous. It merely modifies the chemical kinetics of the stabilization process and is not incorporated in the structure of the material.

INTRODUCTION

An important step in the production of good quality carbon fibres is the stabilization of the PAN precursors at 265°C in air. This process is rather slow for continuous fibre manufacture and requires acceleration in commercial applications. Marinkovic (1) and Bahl (2) have suggested the use of SU2 at this important stage. It is reported that SU2 accelerates the stabilization process and improves the strength of the carbon product to some extent. It is also claimed that the SU2 is incorporated in the surface of the fibres. In many ways NU2 behaves chemically in a similar way to SU2 and so we decided to experiment with this oxidizing agent to improve the rate of continuous fibre production in our carbon fibre plant.

EXPERIMENTAL DETAILS

In this series of experiments we used polyacrilonitrile 1/6K/1.22 produced by Courtaulds. There were three stages in the process:

Ia - Either stabilization in air for 40 min. at constant length at 230°C, or

Ib - Stabilization in NO2/air mixtures for a range of residence times at constant length also at 230°C,

II - Stabilization in NO₂/air mixtures for a range of residence times at constant length at 265°C,

III- Carbonization in argon, allowing shrinkage to 1000°C.

For stages I and II we used furnace, Im long with a device for maintaining the length constant. For stage Ia the residence time was 40 minutes (ref.3). In stage Ib we used NO2 in concentrations of 5 to 30% in air and residence times of 10 to 60 minutes. In stage II we used NO2 in concentrations of 10 to 40% in air and residence times of 10 to 60 minutes. In stage III, the residence time was 60 minutes with a shrinkage of between 7 and 14%. After each stage of stabilization, specimens were analysed by DSC (Dupont) and IR (Perkin Elmer) to determine the degree of stabilization. Density measurements were also made to this end. The tensile strength and Young's Modulus were determined only after step 2 using an Instron with cross-head speed of 10mm per minute. After stage 3, the density, strength and Modulus of elasticity were measured to determine the quality of the carbon fibre produced. The cross-head speed of the Instron, in this case, was 2.5mm per minute.

RESULTS

Some of results are summarized in tables I-II-III and figure 1.

DISCUSSION

It is interesting to compare the results in tables I and II with those of table III (weight loss). The highest weight loss during carbonization occured after the use of high concentrations of NO2 (46%) during stabilization, bringing with it a marked reduction in mechanical properties (probably because of structural damage). It is interesting to determine why high concentrations of NO2 produce such drastic deteriorations in mechanical properties of fibres whereas lower concentration of NO2 produce modest improvements in strength (table I). Moreover, carbon fibres with poorer harmhanical properties are produced when stabilization takes place in shorter

times using an atmosphere of NO₂ in air in both stages of stabilization. In the IR analysis, it is noted (figure 1) that there is a tendency to reduce the removal of the nitrile groups in the presence of NO₂. This decrease is proportional to the concentration of NO₂. In stage II, however, it may be seen that all the analyses made at every stage did not show the presence of any group containing nitrogen, showing that no nitrogen groups are incorporated in the molecular structure of the treated fibres.

CONCLUSIONS

Treatment with NO_2 like SO_2 , produces a modest improvement in the strength of carbon fibre and accelerates the stabilization stage in continuous fibre production. NO_2 alters the chemical kinetics in the stabilization of PAN fibre, but in contrast with SO_2 , is not incorporated in the PAN structure.

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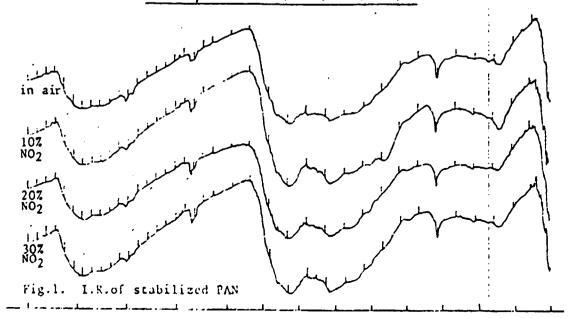
TABLE I- Tensile strength of carbon fibres after carbonization (1000°C)

TABLE II— Young's Modulus of carbon fibres after carbonization (1000°C)

	0:	xidati	on T	ime (r	ain.)		Z	0	xidat	ion T	ime (min.)	
NO ₂	10	20	30	40	50	60	NO ₂	10	20	30	40	50	60
0	1,54	1,58	1,93	2,16	2,04	1,72	0	147	169	163	142	124	121
10	1,42	1,92	1,91	2,06	1,86	1,59	10	148	160	157	148	151	127
20	1,70	1,93	2,23	2,18	1,79	1,86	20	153	157	169	160	158	155
30	1,97	1,70	1,70	1,68	1,60	1,48	30	160	149	153	148	144	141
. 40	1,76	1,38	1,30	1,15	1,16	1,07	40	158	137	142	111-	112	107

TABLE III- Weight loss % after carbonization (1000°C)

Z	Ox i	Oxidation Time (min.)											
NO ₂	10	?J	30	40	50	60							
0	37,9	37,9	41,6	40,8	38,9	39,4							
10	36,5	37,9	37,9	37,9	38,1	39,1							
20	39,4	39,6	39,7	40,3	40,3	41,7							
30	38,0	37,9	37,9	39,6	41,7	41,9							
40	42,0	42,4	43,9	44,3	45,2	48,4							



FINAL REPORT OF THE "INTERNATIONAL CONFERENCE ON CARRON FIBER APPLICATIONS"

The Government of Brazil, through the Centro Técnico Aeroespacial (CTA), organized and hosted an International Conference on Carbon Fibre Applications, from 5-9 December 1983, at São José dos Campos (SP) and Camaçari (BA). The Conference was co-sponsored by the United Nations Financing System for Science and Technology for Development (UNFSSTD) and the United Nations Industrial Development Organization (UNIDO).

The purpose of the Conference was, on the one hand, to present the results of a successful project on "Optimization and Development of Carbon Fibre Technology", which is being implemented at CTA with the financial co-operation of UNFSSTD and the technical assistance of UNIDO, and share such results with representatives of invited developing countries which have reached a similar technological and industrial level so that they are interested in the production and/or use of carbon fibres and composites.

On the other hand, the Conference served the purpose of demonstrating the great variety of applications of carbon fibres and composites in aerospace and transportation as well as in marine, recreational and biomedical uses. This was achieved through the co-operation of a group of high level experts from some developed countries.

Finally, the Conference focused, in more general terms, on the identification of methods and mechanisms on which an efficient technical co-operation among interested developing countries would be based with a view to sharing the experience which each of these countries has with regard to production and/or applications of carbon fibres and composites and, thus, strenghten the scientific and technological capacity of these countries.

China has been working, since approximately 1960, in the development of carbon fibre technology and its industrial applications and the development and production of resins for composites with the fibre.

India, with the help of UNIDO, developed competence for the production of appropriate precursors for carbon fibre, the production of the fibre itself and its use in many industrial applications. At present, India is making a strong effort to acquire capacity to internally produce resins for more sophisticated applications of the fibre.

Brazil, with the financial support of the UNFSSTD and having UNIDO as the executing agency, has developed capacity for the production of the PAN precursor, to produce carbon fibre and to produce composites for many industrial applications with the fibre. It is expected that, by the end of 1984, Brazil completes the development of the knowledge for the production of carbon fibre up to the industrial scale.

Korea

Argentina, Egypt and Mexico have been using carbon fibre composites in industrial applications since many years.

Through all those activities, a substantial capacity, in the chain that goes from the production of the precursor for the carbon fibre up to its application, has been developed in those developing countries; a substantial amount of information has been acquired or generated. The levels of capacitations acquired by each country is different from country to country in the different parts of the chain, though they can be complementary.

In spite of all the efforts being made, there are big tasks to be performed by those countries to complete their capacities in this field and, from there on, to cope with new developments in the field. All this can be quite costly and will need sustained international assistance.

In view of all those facts, it is clear that there exists the evident possibility for the developing countries attending this meeting to cooperate.

In this context, UNFSSTD and UNIDO understand their role as that of providing an interactive mechanism to help to catalyze co-operative activities of developing and developed countries - of governments, universities, research laboratories, public and private enterprise and financing institutions - with a view to finding appropriate solutions for the problems of acquisition, assimilation and application of carbon fibre and composite technology for the benefit of the economic and social development of those countries.

The efforts of the countries, and the external support by the United Nations Systems, should be able to draw on co-ordinated services from every interested country that can provide them, to any interested country that needs them, and they must be able to do this on a reliable and sustained basis.

In this spirit, participants from Argentina, Brazil, China, Egypt, (India), Korea and Mexico have discussed possible subjects and mechanisms of co-operation in the field of production and application of carbon fibres and composites and have come to the following conclusions:

- 1. With a view to gaining the full support of the competent Government authorities of the countries represented at the Conference, the participants agree to establish the necessary contacts to such authorities, inform these fully on the results of the Conference and recommended follow-up activities and convey to them the importance of co-operation in this field.
- 2. In order to assure that each participating country be fully informed on relevant activities related to the production and application of carbon fibres and composites undertaken in the other participating countries, the participants identify the need for an information network covering such activities which, in the first stage of co-operation, could function on an informal basis. As a first step, such network would gather and disseminate the information actually available in each participating country on past or ongoing activities and experiences.

- 4. ______ into consideration the absence of norms and standards in the ______ of carbon fibres and composites, the participants agree to the _____ to develop common standards for their countries so as to enable _____ to exchange raw materials, intermediate and end-products of _____ on specifications and of controlled quality. For the same purpose, ____ on rules for certification should be elaborated.
- 5. The regard to the above identified needs and others, which the second consultations of each participating country may consider; articipants of this Conference see an important role for the least ations System, especially UNFSSTD and UNIDO, to provide the second mechanisms for the identification and mobilization of least edge technical and financial resources.

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INTERNAL EVALUATION SYSTEM Liefest Evaluation Report

Part II — Pulid GLAS UNCH ASSUSSAMAY (Self-evidence)

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	A research and development team fully trained and with the experience to keep adapting the technology used in other countries to produce curronfibers or relate material, or to further improve the technology alread, in use in Brazil, or to conduct h and h work related to other similar materials from the laboratory scale to the industrial scale.									
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ENCHOSURI. 1

Completed bench scale standardization in heat treatment and spinning. Now in the process of scaling up. New omidising systems studied. New spinning experiments based on preliminary carbonization studies of CTA precursor have already commenced. Methods improved in surface treatment experiments with sizing systems commenced. The training of one of the counterpart scientists in USA through UNID helped him to fabricate prepreg laminate equipment and analysis. T.Cel Kessel counterpart group leader's study tour with two of his collegues helped him in advising his group at CTA what he gained in the tour.

ENCLOSURE 2

Bonch scale carbonization and spinning experiments almost completed. The teem has been trained by the competent experts. The overall world activities in this field were emposed to the team by conducting it institutes symposium in carbon fibers and by inviting experts competent in the field. Filot plant equipment arrived. Work already started to scale up. The counterpart scientists went abroad on study tours and fellowship to get themselves acquinted with latest developments in the field. Two of the counterparts are attending a conference in France and presenting a paper in carbon conference. Another counterpart scientist is to attend a UNIPO's implant group training in Austria in Oct/Nov 84. National Coordinator and two of his cellegues recently visited Europe on study tour which helped them in adapting to the local needs. Thus the team has formed and exposed to the activities elsewhere in the world and adapting to the local needs.

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ENCLOSURE 3

Technology to produce carbon fibers of the appropriate quality and the corresponding precursor, using national raw materials. All this technology transferred to the industrial system.

ENCLOSURE 4

Carbon fibers with comparable properties with those of commercial fibers were produced. Acrylic fibers of commercially comparable properties were also produced. The scaling up to pilot plant already commenced. All the utilities to pilot plant carbonization furnace are being completed. The acrylic fibers produced from national raw material are being standardized for carbon fiber processing. The team is capable of analysing new raw materials for carbon fiber processing and fiber spinning.

ENCLOSURE 5

Good quality carbon fibers and precursors fibers already developed in the bench level. Scale-up activities already commenced. The industry already involved. COPENE - Petroquímica do Nordeste S.A., the parent organization of FISIDA - Fibras Sintéticas da Bahia S.A. is very much interested in these developmental activities.

ENCLOSURE 6

knowledge and techniques to characterize and test the raw materials as well as the final products for the production of the precursor and carbon fiber.

ENCLOSURE 7

The team has characterised the raw materials available precursor fibers and has been conducting experiments to analyse the intermediate and final products. Also characterised the commercially available final products.

ENCLOSURE 8

The team is now capable of performing this activity confidently. Acquired required knowledge to characterise the raw materials and final products.

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This provide friend in spirit is given in the project discourant and important of payer or necessary wing some form

ENCLOSURE 9

Physical facilities completed in such a way that the trained staff can properly perform their tasks. The additions in this second phase will include:

- pilot equipment for spinning the polyacrilonitrile precursor;
- modified pilet line (including surface treatment) for the production of carbon fibers;
- auxiliary equipment for electron microscopy X-ray diffraction, differential thermal analysis, electronic measurements, photography;
- other minor equipment.

ENCLOSURE 10

Achieved almost as far as required for the project.

Pilot plant for spinning polyacrylonitrile precursor acquired, work already commenced on this equipment at industrial site at FIGIRA, Salvador.

Equipment for pilot line acquired. The utilities are almost completed.

Preliminary activities are being commenced.

Most of the auxiliary equipment as for required to the project obtained.

Most of the minor equipment required has been purchased or fabricated by CTA.

ENCLOSURE 11

Most of the factors in this output achieved. The remaining are sure of achieving.

C.	Callical	Assumptions

1. History describe these assumptions, explicit or implicit which, while outside of project management control, are called to production of one or more of the outputs listed above (e.g. projected industry demand or med).

Conference on embon fiber applications to appraise the local industrial involvement of the local industries to produce carbon fibers involvement of local industries which could use these fibers.

2. For each assumption, describe what has or has not taken place, or seems most likely to take place, and the actual or possible effect of such change on producing the outputs/results originally intended (e.g. if industry demand has not developed as projected, what is the probable cause), including what remedial actions, if any, can or should be taken by any of the tripartite parties:

A conference was conducted on application of carbon fibers. About 200 participants from industries, institutes, government organization appreciated the application of these fibers.

A-major pretrochemical industry COPENI - Petroquimica do Nordeste S.A., the parent organization of FISIRA has shown interest in the industrialization of these fibers and visited the project site to have the first hand information of this technology. The neighbouring civil commuter plains manufacturer EMRAMER expressed its plans of using carbon fibers. All these are positive effects for the project.

ASSESSMENT

D. Project (hypothesic) Approach and Design

1. Repeat project (immediate) objective as it appears in latest Prodoc/PDS, or as subsequently modified by tripe total decision:

See enclosure 12.

2. Given project experience to date, including the original assumptions made and any changes which have occurred in the project environment, is the project hypothesis still valid, i.e. if the outputs are produced as planned then is it reasonable to assume that the project objective(s) will be successfully achieved?

yes no, explain cannot determine, explain

Most of the outputs are achieved.

A strong enthusiastic group has formed.

Most of the technology on banch scale completed, industry already involved.

Knowledge on techniques is acquired by the group.

Most of the physical facilities were provided.

The remains are sure of achieving.

ENCLOSUM 12

The immediate objectives are:

i- to complete the formation of the scientific and technical capability to be able to industrially produce carbon fiber precursors, carbon fibers and its composite structural materials and to further develop the technologies involved in that process, from the laboratory scale up to the industrial scale. This means training the appropriate personnel and forming the corresponding teams, not only for the production process for the carbon fiber, but also to determine the chemical, physical and mechanical characteristics of the raw materials, intermediate and final products;

ii- to optimize the continuous process for the production of carbon fiber which has already been developed up to the bench scale by the CTA; to further develop it up to the pilot plant scale until sufficient knowledge and experience has been developed, so as to transfer it to the production system;

iii- to generate the information necessary to produce the precursor fiber and to transfer it to the production system;

iv- to complete the minimum necessary equipment and physical infrastructure in such a way that the teams formed through the project can appropriately perform their tasks.

1	•		
	•	3.	Given the status of producing the individual intended outputs/results as indicated above, what is your jetly more of the probability of indeessibily producing the overall final results seasonably on schedule, within the results to be supplied, and in the quantity, type and quality required?
7			□ impossible □ improbable □ likely □ highly likely □ certain □ cannot determine
-3		4.	ls a project redesign necessary?
7		5.	if yes, at what level?
-	•		□ development level □ project approach/all levels □ development hypothesis □ outputs □ project (immediate) object □ work programme
1	•		
*	E.	٥٠	erall Conclusions and Recommendations
		1.	On the basis of your ratings above, provide a concise narrative evaluation statement of progress to date, including any relevant and significant information not included above:
1			The group has become strong both in number and kind. Thinking capacity of the group has improved. The counterpart scientists are capable of analysing the problems. The self confidence in the counterpart scientists is growing. This is a overall positive approach in achieving the goals and objectives of the project. The leader-ship of T.Cel Kessel was given morale to the group. The enthusiasm and encourage given to the group personell is yet another positive factor.
			Also see enclosure 13.
		2.	Describe fully the actions or decisions recommended by project maining to improve the efficiency and effectiveness of project operations, including responsible units and suggested larget dates.* Summarize units "Actions kequired" on Part I — PER Face Sheet:
			The "Actons required" in the previous PER were accomplished. Centro Técnico Aeroes pacial inducted the more qualified personnel into gha group and completed the mort of the facilities. Now in the process of providing utilities like inert gas, refrigeration, compressed air, etc. UNIDO has purchased all of the requirements requested by CTA.
	•		It is now recommended that Centro Tecnico Aeroespacial should complete providing the utilities as early as possible to use pilot plant carbonization furnace. Necessary arrangements must be made to run the carbonization furnace continuously, at least for weak without interruption. However, it is recommended to follow up this project activities with a 2 nd follow up phase to consolidate and directly apply to industrial application.
			Continued in Enclosure 14.
	•		
		3.	When was the last tripartite review or tripartite in-depth evaluation held? Tripartite review. Dec. 2.1903 (dutt and type)
		4.	When is the next tripartite review or in-depth evaluation scheduled? <u>November 1984. Tripartite Faviorial</u> (due and type)
		5.	Given the above conclusions, is an in-depth evaluation necessary in the near future (regardless of whether or not or when, one is included in the Prodoc or PDS)? □ yes □ no
		• /.	rio and transfer is necessary

In order to consolidate the activities and to expose others CTA conducted an international conference on application of carbon fiber during first week of December 1983, invited participants from other developing countries like, Argentina, China, Egypt, Korea and Mexico, and experts in the field from developed countries. All participants including those 200 participants from Brazil, appreciated the project activities at the project site.

The precursor group of the project has standerdised the spinning parameters, with respect to major spinning variables under DEF spinning conditions. Fibers comparable with most of the commercial fibers were produced from the polymer obtained from FISIBA. Qualitative experiments to scale up the spinning experiments have already been started at a fiber industry FISIBA in Salvador. A few fiber bobins spun from the pilot plant spinning assembly have been tested at CTA.

A heat treatment group has almost completed the newly designed experiments in carbonization as per the instructions of expert IIL. Walnin. Also in order to explore other oxidising atmosphere in the exidation stage, the group has completed exidation studies using nitrogen dioxide. Extremtly systematic studies are being conducted to evaluate oxidation and carbonization properties for CTA spun fiber from FISIDA polymer. Various oxidazation temperatures, resident times were used. Parameters such as elongation, density, mechanical properties were determined. Also on the best oxidised fibers, carbonization studies already commenced. The shrinkage, wight loss, density, mechanical properties have been determined on some of these fibers. Spinning experiments are being modified based on these results. Active work is going on to assemble the pilot plant carbonization furnace. The required utilities are being provided.

Surface treatment experiments were conducted with a modified set-up and using untreated RK Company supplied carbon fibers. These studies would give an idea to standardize the surface treatment on CTA made carbon fibers. The treated fibers were used to unidirectional laminates using epoxy resins. The flexural, interlaminar shear strength, etc. were determined. Also sizing was introduced after the surface treatment as it is required to keep the fibers tog.ther.

Counterpart scientist, Alvaro Luiz de Sousa Comez Filho was trained in UEA on composites and analysis. As a result of this training, the follow each:

develop vacum buy moulding for preparing prepreg laminates and develop enalysis a techniques.

T.Cel Resert the counterpart Project Leader, went on study tour along with two of his collegues for discussions with persons in kk Company who are experienced in carbon fiber technology and who well oxidation ovens and carbonization furnace. T.Cel Ressel could have the first hand information on the possible purchase aspects of these equipment. T.Cel Ressel visited UNIDO for discussions with regards to the II phase project. This tour helped him in understanding and appreciating the potential of carbon fibers.

Some of experts who attended the Conference also consulted the group.

ENCLOSURE 14

Output no 1 has already achieved. However, the team should be in constant contact with developmental activities elsewhere in the world. Further improvement in English language will help the counterpart scientist in interacting with people outside Brazil and could help in using the literature.

Output no 2. Most of the output 2 achieved. However, the counterpart should now work on UNIEC purchased pilot plant carbonization furnace and should work continuously a 24 hrs basis, and should produce PAN-ox and carbon fibers.

Output 3. This has already been achieved.

Output 4. As far as required have been completed. However, since the pilot plant carbonization furnace arrived recently all the utilities should be completed as soon as possible to work on this equipment.

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I. SIDFA:

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2. Backstopping officer:

The project had a difficult start due to the fact that no adequate counterpart personact were available. However, due to the effects of the Entired Project Director and the Director of CTA the situation changed promptly. The Scientific Advisor to the project was very helpful in putting the project on solid basis and gave a great deal of assistance in recruitment of the best available consultants in this field, and was very helpful in placement of trainees and in the study tours.

He also made it possible to get an excellent Chief Technical Advisor who helped in training and maturation of the team that can now function alone although it would have been desirable that he would have stryed another year. The project will be extended to the end of 1985 because a Phase II of the project is actually being prepared, the objectives being to assist in the applications of the Carbon Fibres and it is desirable that the Phase II will be a normal continuation of Phase I. On the whole the project has achieved its objectives and can be considered as a successful; project.

G. What distribution of this PER is recommended?

The completed PER after endursement will be sent to: CTA, SIDFA, DIO, PC/EVI., Registry

If you suggest a liftional distribution please indicate

7.	Resident Representative		targeted beneficiarie.
D	UNOP Beedquarters	\Box	input for solizibiled teleparties review or in-dopth evaluation
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A. Causal Factors Checklist	ايد		7		:
(Fill out and attach to PER)	No. applicable		As antispated		-
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TECHNICAL ASPECTS	_			-	
I. Personnel				.	ı İ
a) Job descriptions appropriate to project/local needs			X	. {	
b) Experts' qualifications compared to job descriptions			X		
c) Adequacy of international expertise to project/local needs			X		_
d) Ability of international staff to enantuniente knowledge to local staff			Σ.	!	_
c) Assimilation of knowledge by national staff	_!!		X		
f) Availability of technically qualified local personnel	_			Y	_
r) UNIDO man-yenis available	_			X.	
h) Government man-years available				X	_
Other factors and/or comments:			ı		
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2. Project Approach					
a) Adequacy of project funding			<u> X</u>		
b) Adequacy of povernment funding				X	_
c) Appropriate to project function (purpose)			_;_		
d) Appropriate to local needs and demand			X		-
e) Appropriate to local cateral/technological conditions	_		_:_	i	! _
f) Dissentination/multiplier effect to expertise provided	_			X	_
g) Complementary with other expertise existing/provided			X	!	į .
h) Adequacy of national counterpart institution	-		_Х_		_
i) Availability of reliable data/statistics		<u>X</u>	إ	_	-
Other factors and/or comments:	1 1		j	į	į
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3. Equipment]]		.,		ĺ
a) Quality of equipment procured with international resources			Х		<u>;</u>
b) Local capability to maintain/repair project equipment	_	7	i		L
c) Quality of equipment procured/available from government resources	- !		- <u>X</u>		-
d) Adequacy of equipment to local technological needs	-		<u> </u>		L
c) Timeliness of second of necessary equipment			<u> </u>		-
Installation face of configurant	_		X		į –
Complementality between equipment and training Complementarity between equipment and expertise			- <u>X</u> -	1	Ļ
h) Complementarity between comment and expertise Other factors and/or comments:	-				-
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4. Training (on-the-job and fellowship)			,		İ
a) Suitability of training to trainzes' backgrounds	_		X X		!_
o) Suitability of training to trainees' assigned positions			- 3	- -	-
c) Suitability of training to local needs			:		i. .
d) Suppliebles of transia, to local calter detechnological actaining	-		- X -	. .	
c) Length of training 12 Length of training institution (fellowship training out)		•••	<i>.</i>	•	
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p) Opportunity of transes to apply new knowledge					<u>.</u>
5) Suitability of equations (weeking materials	-			;	!
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A. C	Cousul Factors — Checklist	ێ		2	·
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2. UNID	OO Hendquarters				
a) Supp	est ha preparing technical parts of draft project documents	1]		X
	ort in developing technical approach			Ÿ	
	ili adaguacy of technical backstopping	!			
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	ince/assistance on design/evaluation methodology	i- —			<u></u> .
	v/rp_roprinteness of procedural guidelines	 -	-		i .
	y provision of project is ads		<u> </u>		İ
	ome to requests for assistance	¦			
	ort in obtaining supplies		- -		X
	ort in letting sub-contracts	 ;			<u>.</u> ^_!
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	ont of salaries/allowances/expenses ance on local political/institutional situation		-	<u>X</u> .	<u> </u>
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	duration with related projects versultment of international staff	<u> </u>			<u> </u>
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	y procurement of equipment		-	X	
	y placement of fellows	 		·	
	y regly to communications	ļ	!	<u>X</u>	
	loess of ciples to queries	!		<u>:</u>	
	er on policies and procedures	ļ. — .	;		!
	assignment of project authority/responsibility Tactors and/or comments:		!		
Wher	O office provided excellent support in conducting CTA/UNIDO/ STD spensored conference at CTA. ever UNIDO representatives were in the Project site, a rotal ort was given aspecially to the Group working and this fredect, an of encouragement and appreciation was given. This is very assary in the development of this type of technologies.				
	r Industrial Development Field Adviser's Office			!	
i) Suppo	ort in preparing technical parts of draft project documents				li
) Suppo	ort in establishing and defining objectives			7.	_
) Suppo	ort in developing technica! approach	i			7
d) Guida	ince on project background	i		- <u>;;</u>	1 %
c) Guida	mee on national political/institutional situation	i —		χ	!1
f) Guide	ance on UNIDO procedures and policies			7.	
r) Gind:	ince/assistance on local administrative formalities			У.	
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	fuctors and/or comments:				• •
SILF	We office also has played an important part in the seconds of WENIDO/UNYSSTD conference conducted at CTA.				

	Γ	Perfe	· · ·	· · · · ·	
		<u> </u> ;	*****		<u>;</u>
A. Caural Factors — Checklist	1	-	pa.r	0 -	ř.
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z. Government	1				
a) Provision of physical facilities and equipment	<u> </u>			Ä	X
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c) Prevision of office material/equipment	∤ —.	-	X X	!	
d) Provision of transport facilities e) Provizion of storage facilities	{ —		X		
e) Provision of storage facilities (1) Provision of counterpart staff	-		X		
g) Prayision of funds	i		Z		
h) Guidane, on administrative formalities			X		
i) Support in undertaking administrative formalities				<u>y</u>	
j) Maintenance and repair of equipment	<u> </u>		Σ.	<u> </u>	
k) Avrilability of policy and management officials	ļ	!	X		
Other factors and/or comments:	j				.
The counterpart coordinator T.Cel Kessel has taken special interest in]				l
the success of conference. At all stages, he has been confiding with CIA in the general management and methodology in the development of this	ļ				
technology. His active participation bousted the confidence in the group			•		
pursuance and encouraged them in active participation in the developmental activities.	! \$				
5. Other Participating Agencies	\				ļ
a) Timely terroity sort of staff	X				
Timely purchase/provision of equipment Timely observant of follows	X				
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EXTERNAL FACTORS					1
a) Government incontineness to change	-		Х		, ;
b) Continuity in economic/social/industrial policy			X		
c) References of relevent legislation	X				
d) Support by industry organizations	<u> </u>			<u> </u>	
c) Suppost by other organizations (specify)	X				
() Co-ordination among Government arencies	X			<u> </u>	
Other factors and/or comments:					
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R..F. FILE:

Brasilia August 7th, 1984.

COMMENT FOR ENDORSEMENT OF PER COVERING PERIOD DEC 2nd 83 - JUNE 29th 84 OF ERA/81/T01 - (PAG 5)

Enclosed is herewith PER with the following comments (1):

- a) Starting January 1984, Brig. Piva took office as Director of "Centro Tecnológico Aeroespacial" (CTA). He is a PhD from Massachussets Institute of Technology (MIT) and as such, he is really able to understand R and D work. I have talked with him after his becoming the Director. He fully supports the project and is quite conscious that it constitutes a very important venture in terms of product to be produced (carbon fiber) and in terms of creating a team of innovative people with autonomy to keep on working with this or other fibers and materials in the future. (2) He is quite aware of the need to keep on adding highly qualified personnel to the team, to keep the present personnel in the project and also to continue improving it. He is also conscious about the leadership problem, the need to complete the physical facilities and about the language problem.
- b) The problem of leadership, which I discussed in the previous PER and letters, is in the way of being solved via the permanence of Dr Nagabusharam at CTA. In this aspect, Brig Piva and Chel Kessel are undertaking all efforts to make this possible. I want to insist that we should also do our utmost to help in this process(3). I think the presence of Dr Nagabusharam, using him as master, is absolutely essential to form a national leader.

⁽¹⁾ The comments partly refer to my previous comments to last PER, please refer to them.

⁽²⁾ By this I do not mean that we did not have such a strong backing from Brig. Menezes, who was an extremely able man too and who gave full support to our project.

⁽³⁾ I think we will have to keep investing in sending him to congresses (CONT).



2-

- c) The process of maturation of the team continues on going, the processes and technologies to produce the carbon fiber and precursor at beach scale and plot plant are being developed. The necessary equipment is being put into place and in operation. Supposing that we successfully complete all that process, the introduction of all that at the industrial scale will become important. In this sence, the CTA is taking the right steps too, namely:
 - i- the contract between CTA and CCPENE which would include the financial help from the latter in the final stages of development of the technology at the CTA and the responsability of COPENE for the work which is being carried out at FISIBA (4) COPENE will inject the necessary money to complete the work at pilot scale there and to install the subsequent industrial production.
 - ii- Cel Kessel is already negotiating with a company, the technology for the production of oxidized P/N (at rate of 5 tow/menth), which is very important in terms of stabilizing part of the production cycle.
 - iii- Mitzui has been initiating the production of preong using imported carbon fiber. This is very important, tince they will open the market for carbon fiber (at EXBRAGE and others). Subsequently, once the local production of carbon fiber attains the right quality, it will be only a matter of substituing the imported carbon fiber by the national one.

^{(3) (}COMT.) outside Brazil in such a way that he does not feel that he is getting out of the "jet set" in his area of expertise.

⁽⁴⁾ FISJBA is a comparatively quite small company when compared with the mother company, COPEME, besides that, FISIBA is going through a bad financial situation.

3-

- d) At CTA, Dr Nagabushanam continues to be an extremely important part in the continuing maturation of the team. His presence is escential in the completion of the whole process in which we are involved.
- e) In terms of actions required , I would add:
 - i- To complete as soon as possible the process (be it with the Sta Clara company in Brazil or any other) to make the production possible and put into operation the stabilization furnace at the appropriate capacity (1 - 3 Tons/year). Unit reponsable: CTA with UNICO's help.
 - ii- Even if it may appear a sideline matter, the team has to become more proficient in English as to extract the most out of the consultants and scientific and technical literature in general.

