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ASSISTANCE IN CONSTRUCTION OF PRE-FABRICATED WOODEN HOUSING

SI/BHU/87/801/11-54

BHUTAN

Technical report: Assessment of the boiler plant at the Gedu Wood Manufacturing Corporation*

Prepared for the Government of Bhutan by the United Nations Industrial Development Organization, acting as executing agency for the United Nations Development Programme

Based on the work of M. Wettemann, boiler expert

Backstopping officer: A. V. Bassili, Industrial Management and Rehabilitation Branch

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United Nations Industrial Development Organization Vienna

* This document has not been edited.

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1) INTRODUCTION

As part of its technical assistance programme to Bhutan the United Nations Development Programme has financed, and UNIDO has executed, a project that included, inter alia, assistance to the Gedu Wood Manufacturing Corporation (GWMC) in the field of maintenance of its boiler and the training of their operators. To that effect, Mr. Manfred Wettemann a Boiler Technician, undertook a four week mission to Gedu (Bhutan) from 25th May to 21st June 1989.

EXPERT SERVICE

As the boiler plant has been operated for 3 years and the operators have never been yet trained in its proper operation and maintenance it was decided to provide an expert in boiler maintenance to assess the condition of the boiler, train operators and draw up a preventive maintenance programme.

This technical service (called mission) was split in two parts.

The tasks of the first part of the mission were:

- to bring the boiler plant in proper operation
- to execute the necessary repairs and maintenance works
- to train the operator for basic operation
- to solve the water problem (treatment and dosing)
- to list-up the required spare parts

2) GENERAL INFORMATION

In the Gedu-Wood Complex a wood fired steam boiler plant generates and supplies the required saturated steam for the following consumers:

- 3 veneer dryers

- 1 hot press
- 1 blockboard press
- steam vats
- 3 kiln dryers

The production works in the following shifts:

-	plywood factory:	1st shift: 07.00 - 11.00/12.00 -	16.00
		2nd shift: 16.00 - 20.00/20.45 -	24.30
-	sawmill:	2 shifts as plywood factory	
-	joinery: only	1st shift: 07.00 - 11.00/12.00 -	16.00

- boiler plant: main load: 07.00 - 11.00/12.00 - 20.00/20.45 - 24.30 low load: 11.00 - 12.00, 20.00 - 20.45, 24.30 - 07.00

It works as a closed system, i.e. condensate is pumped back to condensate collecting tank and feed tank. There are losses only as evaporated steam. (approx. 15 %).

The missing water is replaced by treated raw water (make-up water).

The wood waste of the production (sawmill, joinery, plywood and blockboard factory) is used as fuel for the steam boiler.

Refer to the photos 1 and 2 of Annex 12.

TECHNICAL DATA OF THE PLANT

1.0 Fuel Storage and Transport: Wet material: 1 silo for hogged wood waste: 160 m3 net 1 discharge screw: min 3.6 m3/h 1 chain conveyor 1 double flap valve 1 fuel spreader The wet material is spread onto the inclined grate. The fuel passes the drying, the gasification and the burning section

Dry material: 1 silo for chips and dust: 160 m3 net 1 discharge miller: min 1.0 m3/h 1 blow-in fan 1 jet nozzle The dry material is blown into the fire chamber where it burns out while flying.

2.0 Steam Boiler:

-----Gebrüder Weiss Make: 11034 Manufacturer's No. 1985 Year of Manufacture 7,500 kg/hr Permitted steam generation 20 bar Permitted operating pressure 10 - 12 bar Normal operating pressure 102 - 104 oC Feed water temperature Fuel: wet material: chopped shavings, sawdust and chips dry material: sawdust, chips and dust

Boiler type: 3-pass shell boiler with drum type steam space with cooling screen above the furnace (water tubes)

Furnace type: inclined step grate with flat burn-out grate and cooled by primary and secondary combustion air

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3.0 Water Treatment Plant: Raw water quality: according to laboratory analysis: total hardness: 0.16 mval/l = 0.45 degree dH l) 0.23 mval/1 1) m-value: silicate: 8.50 mg/1 4.42 mg/1 phosphate: 3.1 Chemical treatment by: 1 mixed bed ion exchanger capacity: 33 val regeneration by: caustic soda and hydrochloric acid 1 chemical dosing capacity: 0 - 14 1/h chemicals: trisodium phosphate (rest hardness + pH-value) sodium sulphite (rest oxygen) 3.2 Physical treatment by: 1'low-pressure degasifier 1 feed water storage tank: 7,500 1 heating steam pressure: 0.2 bar (operating pressure) degasifaction temperature: 105 oC 4.0 Water Feed Devices: 1 Electrical driven feed water pump for normal operation capacity: 9.5 m3/h 24 bar head: power: 18.5 kW speed: 2920 rpm 1 Diesel engine driven feed pump for emergency operation (power failure) same technical data as the electrical driven feed pump

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1/ Definition from a chemistry text book.

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5.0 Condensate Collecting System:
1 Condensate tank (in boiler house)
 capacity: 5 m3
2 Condensate pumps (1 stand-by)
  capacity: 10 m3/h
             3 bar
  pressure:
             3 kW
  power:
            2900 rpm
  speed:
1 condensate tank (at kiln dryers)
  with sump pump
  capacity: 1 m3
1) The measuring units of the concentration of chemical solutions
   are:
   Mol in mol/kg or mol/l
  '1 mol = molecular mass of the respective chemical compounds
          in gramme (g)
   Val in val/kg or val/l
   1 val = 1 equivalence = 1 mol : valence
   further:
   Gramme in g/kg or g/l: mg/kg, mg/l, 1 ppm = 1 mg/kg
   Hardness: 1 mval/l = 2.8 degree dH = 3.51 degr eH
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1 degree dH = 1,79 degr eH = 1,25 degr fH
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1.1

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- 6 -

3) CONDITION OF EXISTING PLANT (boiler inspection) Checks and findings

The boiler plant has been operating for three years. The first boiler inspection was carried out by the floor engineer Mr. Wensley on 2nd June 1988. His inspection report of 07.06.88 is kept in GWMC.

Exactly one year later the 2nd boiler inspection was carried out under the direction of the UNIDO boiler expert.

The whole boiler plant was shut-down for 5 days.

After the cooling down of the furnace and the boiler drum the following findings were made:

Furnace inspection:

The refractory walls were worn normally: only two cracks were found and immediately repaired.

On the right grate side the sliding plates were totally burned out and bent up so that the natural sliding of the fuel was stopped. The damaged plates were replaced by self-made steel plates which after one week again were bent and had to be replaced by used but not too badly worn cast plates. The problem was that there were not enough spare plates. (see photos 3 to 9 in Annex 12).

The step bars and the flat bars were in good condition.

On the walls there were a lot of flue gas ash which could be easily removed.

Drum inspection:

A lot of red sludge and scale covered the inserts of the drum. Particularly the upper part of the smoke tube were covered by thick scales. One big sludge block was stopping a junction point of the cooling section. (see photos 10 and 11 in Annex 12) The loose scales and the sludge were removed very carefully. The covering in the cooling pipes could not be checked. The scale formed up to 2 mm thick plates. The first assumption, that the scales consist of silicate compounds which are very dangerous for the pipes could not be confirmed. As the analyses of the collected samples showed the sludge and the scales consist of the same elements: Iron and calcium phosphate compounds, no silicate and carbon.

The remaining part of scales particularly in the cooling pipes will be removed in future during operation by dosing of trisodium phosphate surplus (1 kg/day for minimum content of 20 mg/l boiler water) and higher blow-down rate.

The rusty surface of some parts indicates that too much oxygen gets into the boiler (during stand-still and operation as residual oxygen). This will be prevented in future by holding the degasifier under steam pressure and by dosing of sodium sulphite.

General Condition:

The boiler plant and the water treatment plant are generally in a good condition and the above mentioned problems can be solved in future.

Design:

The existing plant is correctly designed and suited for the actual local conditions and requirements:

- inclined grate for wet fuel

- saturated steam boiler as 3-pass boiler with cooling screen

- water treatment plant as mixed bed exchanger (silicate)

Operation:

The following instruments and control and regulation equipment had not been set correctly before the expert's arrival in Gedu:

- low level cut-out
- level control
- combustion air dampers
- fuel spreading
- steam pressure control
- uncorrect regeneration
- correct dosing
- stable degasifier steam pressure

The operators did not know how to set the equipment correctly. The main problem was the underpressure control of the combustion chamber. It was not working properly because:

- the air dampers were not set correctly (too big opening angle). the correct setting for full load is shown in photo 13 (Annex 12)
- the existing flue gas channels from the old Indian boilers
 - to the chimney have not been closed (short circuit).

There were often an overheating of the fuel feeding equipment (spreader and double flap valve) and a back fire up to the chain conveyor. (see photo 12 in Annex 12).

The present boiler load is maximum 4 t/h saturated steam according to the calculation and measurements during its operation (condensate return flow, make-up water supply and fuel feeding).

4) REPAIRS AND MAINTENANCE EXECUTED

During the boiler shut down a lot of repairs and maintenance were carried out. These were reported by the boiler foreman and kept in GWMC.

Main works:

- grate repairs: the burnt sliding plates on the left side of the crate were replaced by steel plates
- two safety valves were replaced by a new one
- a new fuel spreader was made of steel
- a new level switch above the double flaps valve was installed
- a new water level indicator glass was installed
- the low level cut out electrode was shortened to the correct length
- electrical feed pump: worn packing material was replaced
- all strainers checked and cleaned
- cleaning of all smoke tubes and collecting pipes
- closing of the flue gas channels of the old Indian boilers by a brick wall
- additional installation: raw water by-pass line

pressure indicator between reducing valves for degasifier blow-down line for level indicator at condensate tank

5) SETTINGS OF SAFETY AND CONTROL EQUIPMENT

The 2 safety valves could not hold the steam pressure above 12 bar. This was due to the broken pressure springs. There was only one spare safety valve, it was installed instead of the 2 old ones. The second one has to be installed immediately after receipt of the new spare spring.

The low level cut out electrode was shortened to the correct length and the switching-off of the plant was checked by setting down of the water level to the minimum level mark (N-W) 1).

The underpressure control of the furnace was the main problem of the operation which was solved mainly by correct setting of the combustion air dampers. The air dampers had been opened too much so that the induced draft fan could not suck enough flue gas to get a negative pressure in the furnace.

The normal water level of the boiler has also been set too low (at the N-W mark). The level was set correctly 50 mm above the N-W mark.

The steam pressure was set to 10 - 12 _ar according to the requirements of the heat consumers.

The heating steam system of the degasifier was set to a proper operating condition without blowing off by the safety value: two reducing values and the flow rates of the condensate and make-up water had to be adjusted correctly to get a stable operating pressure (0.1-0.25 bar). The safety value opens at 0.32 bar.

The water level on the condensate tank and the flow rate were set for better continuous operation.

The combustion air dampers (primary and secondary) were set according to the combustion temperature and the CO2-content in the flue gas.

All the above mentioned settings are established in the setting list given in Annex 8.

1) N-W stands for lowest water level in German (Niedrigst-Wasser).

6) FUEL SUPPLY AND FEEDING

The size of the chips produced is too big. The wet wood waste is badly hogged.

The main reason for this is that the chipper knives are damaged very often by iron and steel parts which pass the chipper.

The chip size is sometimes up to 200 mm. Therefore the material is bulky and causes stops in the double flap valve.

A metal detector before the chipper would be the best investment but it is very costly.

The charging of the chips to the silo centre was improved by a guide plate on the top of the silo: better distribution and discharging (homogeneous material)

The electrical and hydraulic settings of the double flap valve and the fuel spreader were set correcly so that the grate will be covered symmetrically which is very important for correct combustion and the protection of the grate against radiant heat.

The following fuel rates were measured: - chips in position A: 17 kg/min = 1020 kg/h (283 kg/m3) - chips in position B: 34 kg/min = 2040 kg/h - dust in position 2 : 4.5 kg/min = 270 kg/h (180 kg/m3)

If in future the hogging of the chips will not be improved the space between the flaps of the double flap valve will be too small.

An improvement is recommended in chapter 11.

7) WATER TREATMENT AND CHEMICAL DOSING

The required make-up water for the boiler plant has never been treated since its commissioning 3 years ago. Pure raw water has been used with its natural content of silicate and hardness.

Silicate can be very dangerous for the boiler as scale because its heat transfer is very, low and for this reason, the covered pipes can be overheated and burst under high pressure. Therefore it is very important to prevent any formation of silicate scales.

The silicate in the raw water can be totally be removed by the existing mixed bed ion exchanger. Any residual silicate in the boiler water can be bound by phosphate which has to be dosed into the feed water. Trisodium phosphate will be used as chemical dosing agent which bind the residual hardness, silicate and increases the pH-value of the water.

The capacity of the mixed bed exchanger is about 33 val which means that approximately 150 m3 raw water can be treated before the exchanger material is exhausted and must be regenerated. The cation resin is regenerated by hydro chloride (HCl) and the anion resin by caustic soda (NaOH). The regeneration has to be performed approximately every two weeks.

As the regeneration has never been done since the commissioning the mixed bed exchanger was use as a filter and a lot of sludge has been collected in the last three years.

During the mission two effective regenerations were performed:

It took a lot of time for cleaning, removal of stops and leakages in the piping to get the plant in proper operation. The suction jets for the chemicals were designed too small, therefore the instruction manual has been revised.

Most of the problems could be solved by cleaning the pipes and changing the procedure (smaller flow rates and longer reaction time). The pollution of the resin by sludge could not be removed in the short time available.

A rough examination of a small sample of the mixed resin showed that the material was not damaged but should be cleaned outside the vessel. This can be done during the expert's second mission to Bhutan.

The water treatment plant was working well after this maintenance. The regeneration can be carried out by the operator (foreman) every two weeks which is not too much work and too complicated.

The result of all this is the best water quality: totally free of hardness and silicate which is a basic requirement to get the boiler free of scales, which means a long life of the boiler plant and less interruptions of production.

The thermal degasifying was working well; only the steam pressure had to be set more stable.

The degasifier has the function to remove the oxygen in the feed water. But there is still a dangerous residual oxygen content which has to be bound. Oxygen is the reason of all corrosion in a boiler plant and the whole steam and condensate piping system. Therefore it is very important to eliminate all oxygen content in the feed water.

An economical way to bind the residual oxygen is chemical binding by a dosing agent. There are 2 main chemicals which bind oxygen: hydrazine (N2H4) and sodium sulphite (Na2SO3). At the time of commissioning sodium sulphite was use. But since more than two years no chemical agent was dosed for oxygen binding. The result can be seen in the boiler drum and in the steam and condensate piping system. Everywhere a lot of oxygen corrosion can be found.

It is very important to dose sodium sulphite for residual oxygen binding and trisodium phosphate for residual hardness and increasing the pH-value. Iron corrodes less if the water it is in contact with has a high pH-value (above 8.5).

For removal of the scales which are still existing in the boiler the dosing rate of the phosphate has to be kept higher than is normally necessary.

The exact dosing rates for the chemicals, the revised instructions for the regeneration and operation of the water treatment plant were recorded in a check list given in Annex 6.

8) TRAINING FOR PROPER OPERATION

The plant runs 24 hours a day (3 shifts) and will be monitored by one operator per shift. In the day shift the foreman and one mechanic are also present.

The foreman is the only man who can speak, read and write the English language.

Therefore he was the only person who received professional training.

The documentation in the plant is not complete: Some important operating/maintenance instruction manuals for the hydraulic unit, centrifugal pumps and water treatment plant are missing. These have to be required and collected from the manufacturer and mailed or handed over personally in the next mission. This was however not a real problem for the correct operation and maintenance.

The responsible foreman was never correctly and sufficient trained during and after the commissioning.

Since the commissioning the operation of the boiler has not been properly done:

- The underpressure control has not worked automatically.
- The steam pressure was controlled by manual switching on/off of the fuel infeed.
- The water level control was set too low.
- The condensate level was controlled manually.
- The main operating work: the fire control for proper combustion conditions have never been done correctly (symmetrically covering of the grate by the fuel, primary and secondary combustion air setting)

During the mission especially the foreman was trained how to operate, to set and to service the plant. A number of instructions were recorded: see the attached check lists (chapter 12).

During the daily round the foreman was advised orally on the correct operation, particularly the correct fire adjustment for partial and full load. He was taught the correct blowing-down of the boiler water, blowing-through of the water level indicators and the recording of operation data.

The operator was advised on water testing and changing of the dosing rate for correct water conditions. The required test kits (listed in chapter 10) were brought by the expert and left at the GMMC.

The regeneration of the mixed bed filter was performed twice with recording of additional instructions to those of the manufacturer. (Annex 10)

3) SPARE PARTS

There are not enough spare parts in store.

The plant has been running since 3 years and it is time now to provide some more spare parts for the future. The boiler plant is the heart of the production and if the plant does not work properly the production also will not work properly.

There are parts which are very important if they are defective the whole plant is in danger and out of control. There are parts (control devices) whose function can be taken over by parts which are manually operated but only for a short time. Further there are very useful parts which are not expensive but should be always in store.

In the spare part lists given in Annex 1 contain all important wear and tear parts of the

- fuel transport equipment
- boiler combustion section
- boiler pressure section
- feed tank and feed pumps
- condensate tank and pumps
- water treatment and dosing plant
- piping system
- electrical control panel

for

- immediate need
- 1 year operation and
- 5 years operation

The make and type and the number of the installed parts are stated in the lists.

The responsible persons of the GMMC (foreman, floor engineer and manager) have to find out the source of supply and where they can get the parts from. (locally made, purchased in India or overseas)

Recommendation:

All the spare parts for the boiler plant shall be stored in a separate cabin in the boiler house and sorted according to the above listed sections.

10) TOOLS, OPERATING FACILITIES, ADDITIONAL INSTRUMENTS

The existing tool box in the boiler house does not contain the correct and complete range of necessary tools for immediate action. Sometimes it took too long to get the right size of spanners for immediate repair during operation. This has to be improved.

The following chemicals will be used in the plant:

- Hydrochloric acid HCl for regeneration of cation exchanger resin
- Caustic soda NaOH for regeneration of anion exchanger resin
- trisodium phosphate for binding of residual hardness and increasing of pH-value of the feed and boiler water
- sodium sulphite for binding of residual oxygen in the feed water

The regameration chemicals in store HCl and NaOH are sufficient for operating for the next 10 years.

Trisodium phosphate (Na3PO4) is only available for the next 5 months and Sodium sulphite (Na2SO3) was not available in the plant and has to be provided immediately. Both chemicals can be purchased in India.

The consumption of the chemicals is as follows:

- HC1 31/33% - NaOH 45% - Na3P04	::	9 ltr/2 weeks = 225 ltr/yr (in store: 2.400 ltr) 8 ltr/2 weeks = 200 ltr/yr (in store: 2.200 ltr) (July + Aug): 25 kg/month (in store: 120 kg) (later): 0.5 kg/day = 12.5 kg/month = 150 kg/yr
- Na2SO3	:	0.1 kg/day = 2.5 kg/month = 30 kg/yr

Water Test Kits:

In order to make the necessary water analyses the following test kits are minimal required:

- pH-value test kit (feed and boiler water)

- phosphate test kit (boiler water)
- silicate test kit (make-up water)
- sulphite test kit (feed water)

The first 3 test kits were brought and left by the expert. The sulphite test kit was sent by him by air parcel end of July.

The test kits needed for the next 3-4 months are available (depending on the consumption of the reagents and how often the water will be tested)

Additional water test instruments and reagents were handed over:

- Density meter for boiler water
- Thermometer 0 100 oC
- Erlenmeyer flask 200 ml
- Measuring glass
- Automatic brown burette (for titration)
- Filter papers
- 1 ltr test hydrochloric acid 0.1 mol/l (p/m-value)
- Phenolphalein solution (p-value)
- Methyl orange solution (m-value)
- Oxygen test kit
- Residual hardness test kit

1 chemical filling pump (hand-pump) has to be provided: (filling-up of the storage tank of the regeneration agents)

11) RECOMMENDATIONS

Additional installations in future

- 1) Water treatment plant:
 - 1 flow meter (counter) DN 20 in feed pipe: (for checking of the operation and recording of the consumption)
- 2) Dosing plant.

1 Manual/Automatic-switch in the panel: (for start-up phase and normal operation)

3) Feed pump:

2 stop valves DN 15 in the minimum flow pipe (for repairs and maintenance)

4) Condensate tank:

2 stop valves DN 20 PN 10 at the level indicator (maintenance)

1 flow meter (counter) DN 50 between pumps and feed tank

(for checking of the operation and recording of the consum.)

- 5) Boiler:
 - 1 flow meter (counter) DN 50 between feed pumps and boiler (for checking of the operation and recording of the consum.)

6) Fuel supply

2 operating-hour counters for chips and dust (for recording of the consumption and its balancing) Spare parts

The spare parts listed for immediate need should be bought at once.

The spare parts listed for one year operation should be provided as soon as possible.

General Training

The boiler foreman Leki Dorji should be sent for a general training for boiler operation to Canada or the United Kingdom. The special training will be provided locally during the next mission.

Changing of the installation

One of the main problems of the plant are the fuel stops in the double flap valve and on the inclined grate:

The stops in the double flap valve can be remedied by enlarging the cross section of the duct (in the direction to the silo).

The stops of the fuel slides on the change of the refractory grate and step grate will be improved by providing of a fire concrete beam instead of the special slide plates for which no spares exist.

12) CHECK LISTS

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The following lists were compiled and handed over to the operator of the boiler plant:

- check list for operating data (Annex 2)
- check list for start-up of the boiler plant (Annex 3)
- check list for operation (daily checks) (Annex 4)
- check list for shut-down of the boiler plant (Annex 5)
- check list for chemical dosing (Annex 6)
- check list for weekly checks (Annex 7)
- setting list (Annex 8) ·
- maintenance list (Annex 9)
- check list for regeneration of water treatment plant (Annex 10)
- reference list for monthly boiler plant report (Annex 11)

13) FURTHER ACTION (2nd phase of mission)

The task of the first phase of the mission was:

- to bring the boiler plant to a proper operation

- to execute the necessary repairs and maintenance works

- to train the operator on its basic operation

to solve the water problem (treatment and dosing)

- to list the required spare parts

The task of the second phase of the mission should be:

- further operating training (checkings and reporting)

- improvements on the grate (concrete beam)

- improvements of fuel discharging and feeding

- checking and cleaning of the exchanger resin (water treatment)

- checking of boiler water and scale formation

- additional installations (listed in chapter 11)

- provision and storage of spare parts

- improvements of the steam and condensate piping system

- completion of the operating and maintenance instruction manual (of the manufacturers'

It is anticipated that the second phase of the mission will take place in November 1989.

- 24 -ANNEX 1 GEDU-WOOD MANUFACTURING CORPORATION/BHUTAN - BOILER PLANT LIST OF SPARE PARTS ******************* 5 y 1) inst. immed. ly mfr/type 1.0 FUEL Transport Equipment 1.1 Chips discharge equipment (Screw-type) refer to WEISS Spare Parts Catalogue of AS 2/55/RS/7,5MI315 and PIV-list EL-51.001 GB (enclosed in operating + maintenance manual) 1 Weiss 315165 1 - freewheel clutch 1 - anti reversing lock Weiss 315164 . 1 1.2 Dust discharge equipment (Miller-type) refer to WEISS Spare Parts Catalogue of AF 8/55/R.G.5.5.MI (enclosed in operating + maintenance manual) 2.0 BOILER - Combustion Section 2.1 Fuel feeding 1 1 2 Vickers System -- hydraulic cylinder 22728/1 HRZ-CX for flaps 1 1 -Vickers System . - hydraulic cylinder 22728/2 HRZ-CX for spreader 3 3 - repair kit 2 6 • - bearings for flaps • 1 E+H/FTM 230 1 - level switch = manufacturer 1) mfr inst. = installed immed. - immediate need = for 1 year operation 1 y = for 5 years operation 5 y

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		mfr/type	inst.	immed.	1у	5 y 1)
2.2	Hydraulic unit	GL-Hydraulik Ser.No. 5007	1	-	-	-
	consists of:					
	- hydraulic pump	11]/min	1	-	-	?
	- electric motor	2.2 kW/1450 rpm	1	-	-	1
	- filter	Mann/W962	ī	-	1	•
	- solenoid valve	MS43P06CF31A1D3	3	-	-	2
	- solenoid valve	MS42P06AF01A1D3	ĩ	-	-	1
	- coil for valve	_ N _	7	-	3	2
	- manometer	Wika/0-160/63	4	-	ī	ĩ
						-

2.3 Furnace (Combustion chamber)

	- refractory material	clay		25 kg		
			•	25 KY	05 1	_
	.	castable retrac	tory		25 K	g
	- refractory brick (ash door protection	300x400x120 mm)	1	-	-	1
	- adapter fire bars	Weiss CSL9198	20) will be	repl	aced
	- sliding plates	Weiss CSL9197	8) by fire	conc	rete
	- step grate bars	Weiss 1000 mm	20	-	8	12
	- step grate bars	Weiss 800 mm	40	-	16	24
	- support bars	Weiss 80x980mm	6	-	_	6
	- rear support har	Weiss 900 mm	2	-	-	2
	- centre support bar	Weiss 900 mm	2	-	-	2
	- fire bar	Weiss 600 mm	48	-	_	48
	- side fire har	Waiss 600 mm	40 6	-	_	
	- side angle har	Weiss 600 am	6	-	_	6
	- fire watch glacs	Weiss 000 mm	4	-	2	2
	- The watch glass	NE133	4	-	۲	۲.
2.4	Combustion air fan					
	- bearings	ball type	2	-	-	2
	- V-helts		2	-	3	-
	- electric motor	7.5 kW/2910	ĩ	-	-	1
			-			-
2.5	Dust fan					
	- bearings	ball type	2	-	-	2
	- V-belts	• •	3	-	3	-
	- electric notor	7.5 kW/2860	ī	-	-	1
			-			-

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	mfr/type	inst.	immed.	1у	5 y 1)
2.6 ID-fan					
- bearings	antifrig.	2 4	-	2 4	-
- flow monitor	DWF U/B	1	-	1	-
- electric motor	45 kW/1465	1	-	-	1
2.7 Control equipment					
- servo motor:	Aris/WAN 6	1	in ste	ore	
 combustion 	1xPtRh-Pt	1	1N ST	ore	

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3.0 BOILER - Pressure Section

thermometer

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		mfr/type	inst.	immed.	1 y	5 y 1)
	- autom. non return	Schröter/	2	spare	parts	
	valve	DN32PN40	-	in sto	ore	-
	- electric motor	18.5 kW/2965	1	-	-	1
	- Diesel motor:	Hatz/2M40L	1	-	-	-
	- maintenance set	Hatz 00987102	-	-	1	-
	- emergency set	Hatz 00987202	-	-	1	-
	- gasket set for cylinder head	Hatz 00992200	-	-	1	-
5.0	Feed Water Tank					
	- level indicator	12 v 1 24 m	1	1	_	1
	alace with seal	1C × 1•C+ #	1	1	-	•
	rings					
	- exhaust steam valve	R1/2#	1	_	1	1
	- level switch	S010-F04 1	1	-	-	1
	- temperaturer	Sarco/412T3	1	•	-	1
	controller	Jui CO/ 41210	•			•
	- reducing valve	Sarco/DP17S	1	-	-	1
	· · · · · · · · · · · · · · · · · · ·	DN25 PN25	-			-
	 pressure spring (yellow) 	_ " _	1	-	1	-
6.0	Condensate Pumps	DIA/SN 32-160	2	(1 sta	and-by)	
	- packing material	part no 46.1	1	-	1	-
	- shaft sleeves	part no 52	1	-	1	-
	- set of seal rings	part no 40	1	-	1	-
	- ball bearings	part no 32.1	2	-	2	-
	- felt ring	part no 50.7	2	-	2	-
	- electric motor	3 kW/2895	1	(1 sta	and-by)	
7.0	Condensate Tank					
	- water level indicat.	Taema/NA7-45	1	in sta	re	
	- magnetic switch	Igema/M410	2	1	1	-
			-	-	-	
8.0	Water Treatment Plant	Hager + Elsässer				
	- circulating pump	Grundfos/UP25-45N	1	in sto	ore	
	- air compressor	Alof/DT3.6	1	-	-	1
	- flow meter	GEMÜ/07/17	1	in sto	ore	

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mfr/type inst. immed.	1 y 5	iy 1)
- conductivity meter E+H/LzW1 1 -	1	-
with electrode XG 0.1		
- deaerator R3/4" 1 -	-	1
- throttle valve DN 20 4 -	-	2
- throttle valve DN 15 12 -	-	4
- medium membrane for DN 20 4	2	-
- medium membrane for DN 15 12 -	4	3
- ball valve UN 15 11 -	1	-
- solenoid valve UN 25 1 - 12/4 -	5/2	-
- 0-ring sets for UN 15/20 12/4 $-$	-	1
- ball valve with UN 15 2 -		-
grate indicator DVG applicator DN 15/20 for repair -	10/10	-
$= p_{V_{i}} = sockets \qquad \qquad b_{V_{i}} = sockets \qquad \qquad b_$	2/2 m	-
- PVC-pipe DN 15/20 for repair -	10/10	-
- Pri-denus DN 15/20 for repair -	5/5	-
- PVC-alue for repair -	1 tin	
- Prograe		
9.0 Dosing Plant		
membrane num Alldos/M241-12 1 -	1	-
- electric motor Siemens/1LP3053 1 -	1	-
- pressure relief V85 PVC/HF1 DN5 1 -	1	-
valve 9 bar		
10. Piping System		
- stop valves DN 20 PN 10 - 2	-	-
for condensate tank		-
- stop valves DN 15 PN 40 - 2	-	-
for feed pumps	2	-
- stop valves UN 40 PN 25/40 5	L	
for boiler blow down	-	1
- Stop valves UN 52 PN 25/40 4	1	-
- reducing value yellow	2	-
springs biow	1	•
- manometer valves 1/2 "	3	-
\sim valve nacking DN 20 - 150 -	1 set	-
material	-	
- flange bolts 4 D DN 20 - 150 -	1 s e t	-

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11. Electrical and Control Equipment (installed in control panel)

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	mfr/type	inst.	immed.	1у	5 y 1)
- low level cutout relav	Gestra NRS1-3	1	-	-	1
- level control relay	Gestra NRR2-1	1	-	1	-
- temperature indicator	Jume OR Bt-96	1	-	-	1
 ring balance controller 	Rixen rix-o-tact	1	-	-	1
- presetting relay	Weiss 312901	1	-	-	1
- progra mme r 4.35K6 - timer	SchleicherKS5198	1	•	1	-
1 30K10 A 36K7	K1 0323/4 0323/5	2	_	1	-
- stand still monitor	ifm A 300/AZ 33-B	1	-	•	-
- crite relays		6	-	1	1
	TDE 11 ATL D	6	-	1	1
- time relay 7 25K5		1	-	-	1
2 01KA 7 01KA	Dold 57 20	2	-	-	ī
- control relays	Klöckner Möller	6			•
- concron relays	Nil R22/timer	11/10	•	-	2/2
	Dil R31/timer	6/1	-	-	1/1
	DIL R40/timer	6/2	-	-	1/1
- contactors	Klöckner Möller	0,2			-, -
(2.01K1.K2.K3)	DIL 2M+11DIL M	3/3	-	-	1/1
	DIL OM/11DIL M	3/1	-	-	1/1
	DIL OOAM/	12/	-	-	2
	11DIL/11DLL M	4/3			1/1
	DIL OAM/	2/	-	-	1
	11DLL M/22DIL	1/1	-	-	1/1
- bi-metal relays	Klöckner Möller				
•	Z00-0.4	2	-	-	1
	-4.0	1	-	-	1
	-1.0	1	-	-	1
	-6.0	1	-	-	1
	-10	3	•	-	1
	-16	4	-	-	2
	Z1-40 (24-40A)	1	-	•	1
	Z4-100 (70-100Å)	1	-	•	1

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	mfr/type	inst.	immed.	1 y	5 y 1)
- D-fuses for E27	2 A	7	-	-	3
-	4 A	4	-	-	2
_	10 A	5	-	-	2
-	16 A	3	-	-	1
-	20 A	6	-	-	3
- D-fuces for E33	35 A	12	-	-	3
NU-fuce links	63 A	3	-	-	3
- nn-iuse links	160 4	3	-	-	3
- main switch	Klöckner Möller	1	-	-	1
- control transformer (0.30 T1)	ismet CSTU 1000/2000VA Nr 596/31/5J	1	-	-	1
- switches	Kraus+Naimer/BG1	0			_
- manual/automatic	A 212	4	-	-	2
- on/off	A 202	7	-	-	2
- +/-	D-F 643	2	-	-	1

1) mfr = manufacturer inst. = installed immed. = immediate need 1 y = for 1 year operation 5 y = for 5 years operation

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ANNEX 2							
CHECK LIST FOR OPERATING DATA							
Steam pressure	**	bar		10 -	12		
Load (pos.or contr.valve)		ada an	5 - 10				
Combustion temperature			0.0 - 1.2 600 - 000				
She as temperature		ر د	300 - 500				
Fuel chine / dust			above 250 chins				
Feed tank level (mark)		- -	above blue mark				
Feed tank pressure		bar					
Feed tank temerature		oC	100				
Cond. tank temperature		oC		70 -	90		
Cond. tank level	(mark)	%		betw.	the level s	witches	
Make-up water su	ylqu	1/h		1000	- 1500		
Pos. of chips di	isch.	A-E		A - B	3		
Pos. of dust dis	sch.	1-10		1 - 3	3		
Blow-off		7	•	5			
Water tests: (a	according	to the i	nstruc	tion	of the kits)	day	
Make-up water	conductiv	itv	ມS/cm	1	0.2	1	
·····	S102	-			0.3	3/2	
	pH-value		•••		5 - 8	7	
Feed water	pH-value				7 - 9.5	1	
	sulphite		mg/1		0.2 - 0.3	1	
	conductiv	ity	μŠ/cπ	1	0.03	1	
	resid. ha	rdness	odH		0.02	7	
Boiler water	pH-value				10 - 11	1	
	phos-cont	ent	m g/1		10-20/5-10	1	
	conductiv	ity	μS/ca	1	below 50	1	
	SiO2		m g/1		below 30	7	
	resid. ha	rdness	odH		0.1	7	
	p-value		mval/	' 1	1 - 5	3	
	sulphite		m g/1		max. 20	7	
Condensate	conductiv	ity	µS/ca	9	0.3	7	
	pH-value				7	7	
<pre>p-value test: 1) fill the test glass to 100 ml mark 2) add 3 drops p-reagent (Phenolphtalein) 3) titration by 0.1 m HCl till red colour</pre>							

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ANNEX 3				
CHECK LIST FOR START-UP OF THE BOILER PLANT				
Start-up:				
 Close the make-up water supply with the ball valve. Fill-up the boiler to low level cut-out Switch off the feed pump Put dry wood material on the burn-out grate Close the combustion air dampers Switch on the induced draft fan Feed-in the chips by switching on/off the combustion air fan After covering 30 % of the grate with chips make fire from the bottom (maybe without induced draft fan) Open slowly the combustion air dampers according to the fire formation and temperature rise Feed-in chips according to the fire formation Blow-down (boiler water) according to maximum water level (150 mm above N-W mark) Supply the first steam to feed tank do not change the settings of the reducing valves do not feed make-up water to feed tank till steam pressure is minimum 0.1 bar and water temperature is minimum 90 oC Do not worry about the low level, use condensate Supply steam to consumers (factory) from 3 bar onwards (very slowly) Set-up fire for steam pressure up to 10-12 bar please note that the grate should be covered by chips symmetrically Air damper setting: normal load: upper 40 - 50 mm lower 30 - 40 mm 				
The above mentioned preconditions after week end are not necessary. Points 1, 3, 11, and 12 are not relevant in this case.				

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		ANNEX 4					
CHECK LIST FOR OPERATION (daily checks)							
1	Fire Control:	the grate should be symmetrically covered by chips regulated by Relay 4.36-K7 and hydraulic speed					
2	Combustion air dampers	S:					
	primary setting:	day load: upper: lower: night load: upper + lower	40 - 50 mm 30 - 40 mm : 20 - 30 mm				
	secondary setting:	burn-out grate: chamber air:	pos. 2 - 3 pos. 2 - 3				
3	Check burn-out grate:	maximum material height: 200 mm ash removal at night shift					
4	Fuel supply:	discharge screw: chain conveyor: symm double flap valve: fuel spreader: symm hydraulic unit: oii	position etrical feeding clogging etrical covering level + leakage				
5	Underpressure control:	: 0.6 - 1.2 mbar if induced draft fan st position of flue gas da not fully op en	opped: 0.1 mbar mper:				
6	Combustion air :	if higher than 1000 oC th damper has to be opened b it is below 500 oC to be	e chamber air y 1 step and if closed by 1 step				
7	Boiler drum:						
	Steam pressure setting	gs: chips 11 - 12 bar dust 10 - 11 bar					
	Water level indicator:	: normal: 50 mm above cleaning by blowing-	N-W mark through				
	Proper operation of co	ontrol valve: normal posit	ion: 5 - 10 mm				
8	Blow-down valves:	daily at 11.00 - 12.00 h check water level during	blowing-down				

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- 34 check leakages (hot pipe) drum valve: 3 x 5 sec 3 x 3 sec each other valves: check the water level: Condensate tank: 9 The automatic switching on/off of the pumps to be checked often. Sometimes there is a problem with the water movement in the tank and the automatic level control does not work. Then operate manually for one charge. discharge time: approximately 5 min daily blow-through the level indicator (cleaning) 10 Feed water tank normal: at blue mark water level: daily blow-through (cleaning) normal: 0.2 bar boiling pressure: check vent valve reducing valve setting: only the 2nd one very slowly temperature: normal 190 oC after boiling: check whether the temperature regulator is fully in the pipe 11 Dosing tank daily fill up by make-up water (treated water) daily add: trisodium phosphate: 1/0.5 kg 100 g (according to the required sulphite sodium sulphite: content) according to the required pH-value (Annex 2) NaOH: normal 35 % set the flow rate: according to daily filling of 70 - 90 1 12 Water treatment plant: feed pressure: 3.5-4.5 bar (raw water pump) normal: 1.000 - 1.500 1/h flow rate: 1.800 1/h max.: 400 1/h min.: check the packing leakage 13 Feed pump: check the bearing temperature of: 14 Bearings: - feed pumps max. 80 oC - induced draft fan - combustion fan

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ANNEX 5

CHECK-LIST FOR SHUT-DOWN OF THE BOILER PLANT

WEEKEND - SHUT-DOWN

- 1 The last shift shall store dry material for the next start-up.
- 2 Further more the last shift shall fill-up the condensate tank by setting higher the level switches (or manually).
- 3 At about 24.00 h, 30 minutes before factory closing, bring fire and steam pressure slowly down.
- 4 Switch off the fire when steam pressure is about at 5 bar and only low fire is on.
- 5 Close the main gate valve to the factory.
- 6 Close the main air dampers: leave only the lower damper a finger wide open.
- 7 Switch off the induced draft fan.
- 8 Switch off the feed pump.
- 9 Close to slightly open the steam value before the reducing values of the feed tank.
- 10 Close the ball valy: of the water treatment plant.
- 11 Switch off the main switch.
- 12 Before leaving of the plant check whether the fire is out or very low.

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ANNEX 6

CHECK-LIST FOR CHEMICAL DOSING

The following chemicals can be mixed with one another

1 Trisodium phosphate Na3PO4

for binding residual hardness (SiO2), for removing the existing scales in the boiler and for increasing of the pH-value

for the 1st stage (July and August): 1 000 g / day for the 2nd stage (after August): 500 g / day

the phosphate-content (P205) in the boiler water should be:

for the 1st stage (July and August):10 - 20 mg/lfor the 2nd stage (after August);5 - 10 mg/l

2 Sodium sulphite Na2SO3

for reduction of oxygen and increasing of the pH-value start with: 100 g / day = 80 ml / day surplus in feed water: 0.2 - 0.3 mg/l in boiler water: max. 20 - 30 mg/l

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ANNEX 7

CHECK-LIST FOR WEEKLY CHECKS

The following have to be checked every week:

1	the functioning of safety valves:	by hand lifting
2	the functioning of low level cut-out:	during start-up procedure
3	the functioning of the pressure limiter:	during low load time (lunch time) by opaning the air dampers and operation of induced draft fan
4	the condition of the grate:	particular the sliding plates
5	the production of ash:	ash removal
6	the pollution grate of the smoke tubes:	cleaning?

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ANNEX 8

SETTING LIST

1.0 Safety equipment ------20 bar 1.1 Safety valves: at N-W mark (red mark) 1.2 Low level cut-out: = 770 mm from flange top edge 15 bar 1.3 Pressure limit switch: 2.0 Control equipment -----2.1 Pressure controller for chips: 11 - 12 bar . 2.2 Pressure controller for dust: 10 - 11 bar 0.8 mbar (set in special relay) 2.3 Underpressure control: 50 mm above N-W mark 2.4 Water level control: 3.0 Monitoring equipment _____ 500 oC 3.1 Combustion air temperature switch: min. max. 1.000 oC (and indicator) interlocked to dust feeding 3.2 Flow monitor for induced 0.3 mbar draft fan: by construction 600 mm 3.3 Fuel level monitor: above filling flap 4.46-F10 (in panel) 3.4 Stand-still monitor: limit switch 4.65-S7 (panel) 3.5 Flow monitor dust fan:

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4.0 Other settings 4.1 Fuel spreader: by timer 4.36-k7 12/12 sec by hydraulic speed 3.0/3.0 (setting) 4.2 Combustion air dampers: day load night load stand-still main dampers: upper mm 40 - 50 20 - 30 0 lower mm 30 - 40 20 - 30 10 - 15 secondary dampers: flat grate 2/3 1 1 fire box 2/3 1 0 4.3 Feed tank 0.2 bar steam pressure: at make-up water flow of 1.5 m3/h only set by 2nd reducing valve after boiling temp.: 100 oC 4.4 Water treatment plant normal flow rate: 1.000 - 1.500 1/h flow rate: 1.800 1/h max. min. flow rate: 400 1/h 4.5 Raw water pressure: 3.5 - 4.5 bar 4.6 Dosing flow rate: normal: 35 % which meet a daily supply of 70 - 90 1 4.7 Condensate discharge rate: between upper and lower level switch: approximately 5 min.

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ANNEX 9 _____

MAINTENANCE LIST _____

1.0 During operation _____

- daily blowing-through of the water level indicators:

2 indicators at boiler 1 indicator at reed tank 1 indicator at condensate tank

- daily blowing-down of boiler water

daily checking of feed pump packing
daily checking of bearings

- (feed pump, induced draft fan, air fan)
- daily checking of leakages of valve packings
- daily checking of flange connections
- daily checking of correct settings of control equipment
- daily checks that no water drops onto electrical equipment
- daily blowing-out of the manometer valves

2.0 During shut-down

- weekly checking and correction of V-belt tension for induced draft fan and air fan
- weekly checking of grate wear and immediate repair, (enough cooling air)
- checking of wear of chain conveyor and repair
- checking of pollution of smoke tubes and if necessary cleaning of them
- removal of ash: step grate and flat grate

CHECK LIST FOR REGENERATION OF WATER TREATMENT PLANT Preparation: if regeneration is done during normal operation time: ----- - fill-up the concensate tank - keep the feed tank at normal level (otherwise dosing plant does not operate) Regeneration: 1 switch-off the circulating pump and close the ball valve after the pump (2) + (3) + (4)1) 2 back rinsing: 25 min - 750 400 1/h 3 sucking of NaOH and HC1 concurrently: (5) + (6) 30 min - 300 400 1/h transport water 9 1 NaOH: position: 35 o) mark tank using ruler 10 1 HCl : position: 45 o) for flow rate checking 4 slowly washing: (7) = (5.1)30 min - 350 1/h 5 settling: (8) it takes more time than 10 min! 50 mm above resin level do not forget to close valve 8! 6 mixing: (9) 20 min automatically 7 venting of nozzle bottom: (10) 8 filling-up: use valve 1 and not via 6 + 6.1 900 1/h 9 quick washing: (13) till conductivity lower than 1 uS/cm (30 min - 1.300 l/h)Checking of water: SiO2 - test: lower 0.3 mg/l

1) Numbers in bracket relate to diagram supplied by the manufacturer.

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ANNEX 10

ANNEX 11

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POWER PLANT REPORT MONTH:.... 1) PROCESS-DATA Operating time: 1. from .../.... hr to .../.... hr 2. from .../.... hr to .../.... hr 3. from .../.... hr to .../.... hr 4. from .../.... hr to .../.... hr 5. from .../.... hr to .../.... hr Interruptions: 1. from ... /..... hr to ... /..... hr 2. from .../.... hr to .../.... hr 3. from .../.... hr to .../.... hr No Consumptions weekly:/..../..../..../..../ t Saw-dust t Chips/..../..../..../..../..... **b**3 Make-up water Operating facilities monthly: 1 Chemicals: HC1: kg NaOH: kg Kg Sulfite Phosphate: 1 Lubricant: Lubeoil: kg Grease: kg Regeneration of Watertreatment plant executed:..... Capacity between two regenerations: m3 Production veekly: No/..../...../...../ t Steam production:/..../..../..../..../...../ t Condensate flow · • • • • • • / • • • • • / • • • • • / • • • • • / • • • • • • Waterquality (average value): mval/1 hardness: Rav-water: micro S/cm conductivity: Make-up water: pH-value: pH-value: Feed water: mg/1. Hydrazine: pH-value: Boiler water: mval/1 p-/m-value: P205: mg/1. Be density: mg/1. hydrazine:

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1. GEDU-WOOD COMPLEX



2. Boiler Plant with Silos and chimney

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1. 19MB-CODINA (194MIC) Hometalot (1955) 1955-1

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EL COMELIE EL ANNO 2007 EL PRESENTE ANNO 2007 L'ADRE



7. Secondary Cohamper air nozzies



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12. Overheated (burned fuel feeding equipment (double flap valve and spreader)



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13. COMBUSTION AIR DAMPERS correct setting for full load