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#### UNITED NATIONS INDUSTRIAL DEVELOPMENT ORGANIZATION

#### THE DEVELOPMENT OF A RUBBERSEED PROCESSING TECHNOLOGY FOR THE PRODUCTION OF VEGETABLE OIL AND ANIMAL FEED\*

US/GLO/81/103/21-00

<u>Phase one</u>: Literature review, field studies, laboratory tests and product and process development perspectives

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## Abbreviations

Besides of the common abbreviations symbols and terms the following have been used in this study:

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## Technical abbreviations:

<b>X</b> ▼	=	Acid value
CN	=	Coconut
D	=	Dalton: molecular weight unit
FFA	=	Free fatty acids
GC	=	Gaschromatography
HPLC	=	High pressure liquid chromatography
MM	×	Nolecular weight
MS	=	Nass spectroscopy
NMR	=	Nuclear magnetic resonance
PA	=	Phosphatidic acid
PC	=	Phosphatidyl choline
PE	=	Phosphatidyl ethanolamine
PI	*	Phosphatidyl inositol
RSM	=	Rubberseed meal
RSO	=	Rubberseed oil
SL Rps	=	Sri Lanka Rupies
THF	=	Tetrahydrofurane
TLC	=	Thin layer chromatography
UM	=	Unsaponifiable matter

## Organisations:

CISIR	=	Ceylon Institute of Scientific and Industrial
		Research
RRIM	-	Rubber Research Institute of Malaysia
RRISL	-	Rubber Research Institute of Sri Lanka

I I I I

## Contents

		Lage
Abst	ract	
I	Literature	survey
	1.	Introduction7
	2.	Information from literature
	2.1.	Early papers and reviews
	2.2.	Composition of rubber seed
	2.2.1.	Composition of rubber seed (whole seed). 8
	2.2.2.	Composition of rubber seed kernel 9
	2.2.3.	Composition of rubber seed oil
	2.2.4.	Composition of rubber seed meal12
	2.2.5.	Minor components in rubber seed14
	2.2.5.1.	Hydrogen cyanide14
	2.2.5.2.	Gossypol
	2.2.5.3.	Saponine15
	2.2.5.4.	Tannins
	2.2.5.5.	Volatile inflammable substances15
	2.3.	Processing of rubber seed
	2.4.	Utilization of rubber seed
	2.4.1.	Rubber seed meal as animal feed18
	2.4.2.	Rubber seed meal in human nutrition21
	2.4.3.	Technical utilization of rubber seed22
	3.	Summary
$\rightarrow$	References	
II	Field stud	y in Sri Lanka
		<b>,</b>
	1.	Introduction
	2.	Technical and technological aspects34
	2.1.	Seed availability
	2.2.	Collection of rubber seed
	2.3.	Drying and storage of rubber seed37
	2.4.	Production of oil and cake
	2.5.	Consumption of rubber seed oil
	2.6.	Consumption of rubber seed cake41
	3.	Economic aspects43
	4.	Summary
	References	

4

U

v

.

## III Laboratory Investigation

I.

I.

1.	Introduction
2.	Rubber seed
3.	Rubber seed oil
3.1.	Separation and Refining
3.2.	Investigations of rubber seed oil
3.2.1.	Analytical characterisation of the
	triglycerides
3.2.1.1.	Fatty acid composition
3.2.1.2.	Gel permeation chromatogr. of the oil60
3.2.1.3.	Oxidized fatty acids
3.2.1.4.	Unsaponifiable matter
3.2.2.	Minor constituents of rubber seed oil64
3.2.2.1.	Tocopherols
3.2.2.2.	Polyisoprene
	Phospholipids
3.2.2.3.	Quality assessment
3.3.	Colour stability
3.3.1.	Taste and taste stability?2
3.3.2	Storage tests with crude
3.3.2.1.	rubber seed oil
	Storage tests with refined
3.3.2.2.	rubber seed oil
	Storage tests of a mixture of
3.3.2.3.	rubber seed oil/coconut oil
	rubber seed off/ coconat off
4.	Filtration of rubber seed oil
4.1.	Viscosity
4.2.	Filtration trials
4.3.	Separation of polyisoprene
4.4.	Dilution trials
4.4.1.	Herane as solvent
4,4.2.	Edible oil as solvent
_	and the second
5.	Composition of rubber seed meal
5.1.	
5.2.	Water soluble materials
5.3.	Hydrogen cyanide
5.4.	Aflatoxins
6.	Discussion
6.1.	Preliminary remarks
6.2.	Influence of drying and storing
	on the oil yield
6.3.	Convosition of rubber seed oil
6.4.	Composition of rubber seed meal
6.5.	Technicological aspects
7.	Summary

page

.

¥

۲

## page

1

I.

•

References.		
Recommendati	ions for pilot plant trials	
Appendix 1	Complete references of the literature survey with regard to rubber seed	99
Appendix 2	Contacts during the field study in Sri Lanka	. 165
Appendix 3	Analytical methods	167

•

¥

.

#### Abstract

In this study the composition of rubber seed (Hevea brasiliensis) and the frame work for the setting up of an industrial rubber seed processing technology is described. This report contains all information from a literature review, a field study in Sri Lanka and laboratory investigations carried out at the home laboratory of MATEC.

Until now in most of the rubber producing countries the rubber seeds are waste material. A rough estimate for the amount of seeds worldwide results in about 5 mio tons per year. Utilization of rubber seed is done in few places and very seldom on al economical scale. However, a lot of information about the utilization of rubber seed is already published in the literature.

The composition of the rubber seeds is investigated almost completely. The average total weight of the predried rubber seed is about 4,5 gram. The kernel of the rubber seed is roughly half the weight of the total seed. The kernel contains 40-50 % of a comparably highly unsaturated vegetable oil, 20 % protein and 40-50 % carbohydrates. Because of the fluffy structure of the kernels the best way for the separation of oil from the seeds is milling of the decorticated kernels in a chakku mill.

The unrefined oil is used for the production of alkyd resins for paints or in the production of soap together with coconut oil to obtain a somewhat softer soapbar. Refined oil could be used as an extender for lightly coloured drying oils (linseed oil) and because of its high nutritional value for human consumption. From the toxicological point of view neither the oil nor the real will give insurmountable problems when used for human or animal nutrition, provided that several requirements have been met in the collection and storing of the seed and in the processing steps. The refining of rubber seed oil is somewhat difficult and can be done on an economical scale only if some requirements concerning the selection drying and storage of the seeds are fulfilled.

The rubber seed meal is presently used as fertilizer and also with a certain reluctance as feeding stuff for calves, pigs and broilers. Because of the hard and sharp shell of the rubber seed only dercorticated seeds should be used for animal feed to avoid damage of the intestines. The presence of hydrogen cyanide glycosides in rubber seed requires a special treatment to split the glycosides and sufficient storage of the kernels and the meal to obtain low HCNlevels. It could be shown in this study that a further problem in using rubber seed meal as feeding stuff is the aflatoxin residue caused by moulds. High levels of aflatoxins might cause strong deceases in animal breedings. The only way to avoid such high toxic substances in the meal would be a manual selection of the moulded kernels and a careful obeying of the storage conditions.

In the analytical investigations of this study it was shown that the crude rubber seed oil contains about 1 % of a polyisoprene material with a molecular weight of several hundred thousand Daltons. This material cannot be totally removed in the refining procedure and is responsible for the very low filtration rate of the oil after the bleaching step. It could also be shown by the analysis carried out on rubber seed from Sri Lanka that the oil contains a relatively high amount of phosphatidic acid. High contents of phosphatidic acids may cause emulsification problems in a neutralization step of the oil refining. To avoid this, only oils with a relatively low content of free fatty acids can be refined without problems. As a consequence only oil from fresh seeds

- 5 -

quickly dried at a temperature of 80°C down to a water content of less than 5 % will be suitable raw material which may be processed on an economical scale.

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In view of the above mentioned problems in processing of rubber seed on a pilot plant scale it is recommended to meet the following requirements:

- Seed collection quickly after seed fall,
- immediate drying at 80 °C and storing afterwards,
- decortication by small handrollers and separation of kernels from hulls and moulded ones manually.

suitable places for carrying out these procedures on small scale with simple equipment are at rubber estates.

#### I Literature Survey

#### I 1. Introduction

This literature survey was carried out to compile the published present know how on rubber seed processing technology for the production of vegetable oil and feed. The survey is based on an online databank-recherche, where the following files have been used:

Chemical Abstracts (1967-1985) Food Science and Technology Abstracts (1969 - 1985) Biosis Prereviews (1977 - 1985)

The key words used for the oneline recherche were as follows:

rubber/seed or hevea, nutrition or food or feed or edible, not nutrition or food or feed or edible, process or technology or manufacturing or product. The printouts of the online-recherche are compiled in appendix 1.

To prepare a meport of this literature-review, any online printout was examened with respect to the relevance for the different items of the project. Extended printouts were made from those titles, which seemed to give any contribution to the required information. Original documents were procured of those titles, which seemed to be of higher importance. Some further documents, which have not been found in the online review, but were mentioned in the quotations of the original literature are also included in this report.

In the following pages a compiled information from more than 300 titles of the documents of the online-literature-survey is given.

### I 2. Information from literature

## I 2.1. Barly papers and reviews

Attempts, to utilize rubber seed, are not new at all. The Bibliography No. 10 of the Library of the Rubber Research Institute of Malaya, titled "Bibliography on Rubber seed Oil" covers the literature up to 1970. It started with chemical examinations of Para rubber seed, meal, oil and commercial evaluation done in the Imperial Institute (London) in 1903[1]. Lit.[2] quotes "Rutherford's Planters, Note Book" from 1913 to contain detailed estimates of the costs of collecting, drying and packing of seed, both for Malaya and Ceylon, as well as analyses of seeds and oil. In more recent time the Rubber Research Institute in Sri Lanka has contributed several papers [3,4,5]. Also in other areas, where Hevea is grown, this problem has been considered esp. in view of the oil [6,7,9], but also as feeding stuff [8a].

#### I 2.2. Composition of rubber seed

I 2.2.1. Composition of rubber seed (whole seed)

An example of a rough composition of fresh seed is given in lit. [3]:

kernel	:	41,2 %
shell	:	34,1 %
moisture	:	24,4 %

The moisture may go up as high as 35 %. In four different crops from different plantations the ratio shell : kernel varied between 1:1 and 1:1,7 [7]. For most utilizations of rubber seed mainly the kernel is of importance, so its composition will be of more interest. I 2.2.2. Composition of rubber seed kernel

Some compositions found in the literature are given in Tab.1.

ref. ingr.	[3]	[6]	[9]	[10]	[11]	[1]	[12]	[13]
oil	42,0	48,5	53,6/52,2	31,4	51,2	44,5	42,0	48,0
H <sub>2</sub> 0	5,0	8,5	3,3/ 3,2	6,8	4,3	14,7	5,0	0
cake	53,0							
protein		17,6	30,7/31,1	18,7	18,8		18,2	18,5
carbohy- drates		22,9		30,7			27,2	
crude fiber			1,7/2,2	4,8	1,1		3,7	5,4
ash		2,5	5,3/5,5	1,4	3,4		3,2	3,4
Ca	0,12			0,25			0,11	
P	0,43			0,33			0,43	

Tab. 1 Composition of rubber seed kernels in 2

These figures of course can give only indications about the composition, since starting materials, preparation and methods to determine the composition varied. In all, about 50% oil and 20% protein (moisture free basis) may be seen as relevant figures for the utilization of rubber seed. Similar oil contents of kernels were also reported in lit. [7] and [14].

I 2.2.3. Composition of Rubber seed oil

Rubber seed oil is a highly unsaturated oil. This is due to a relatively high content of linoleic acid and especially linolenic acid in the triglycerides. Some analyses from literature are given in Tab.2.

ref fatty acids	[12]	[15]	[9]	[8]	[6]	[7]	[14]	[17]	[16]	[10]
14:0			0,5/0,9			0 - 0,2	0,2			
16 : 0	10,6	7,5-11,0	8,0/12,7		10,6/ 8,7	9,4-11,4	10,8	17-22	9,6	10,3/10,7
18:0	12,3	8,6-12,0	14,2/14,2	8,3	12,3/10,2	5,8-9,4	12,6	ł	13,4	23,8/23,2
20:0	1,0	0,3- 1,3	1,0/0,6		1,0/1,3	ĺ	)		trace	{
18:1	17,1	17 -30	24,6/24,7	21,9	17,1/20,2	21,4-27,5	28,2	19-22	24,2	47,2/49,2
18:2	35,5	30 -39	33,1/31,6	38,2	35,5/38,4	37.6-41,6	29,3	32-39	17,4	13,1/13,3
18:3	23,5	14 -26	19,9/14,4	24,3	23,5/21,2	14,6-20,1	19,1	21-26	24,9	5,3/4,0
free fatty										
acida <b>X</b>				5,2	5,4	10 -22	ļ			
unsaponifiable										
matter \$			0,8/0,9	0,7		0,6-1,5	r.			

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# Tab. 2 Composition of rubber seed oil (rel. comp. in \$)

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Most authors agree with the fatty acid composition of rubber seed oil given by Hilditch [15]. Variations are due to differences in crops [6,7,17]. Traces of 8:0, 9:0, 11:0, 10:1 and 14:1 fatty acids were found in addition [7]. Somewhat deviating results are given in Lit. [16] in so far, as additionally 9,6 \$ 7,13-Eicosadienoic acid and 1,0% 6,9,12,15-Octadecatetraenoic acid were found in oil from Malaysia. Very recently a rather uncommon composition of an Indian rubber seed oil was published [10] without discussing the deviations from the compositions found normally. The individual glycerides of rubber seed oil were investigated by Gunstone and Padley [18] by argentation thin layer chromatography and lipolysis. As in most seed oils, the distribution of the fatty acids in the individual triglycerides are in a 1.3-random-2-random pattern. More than 50 % of all triglycerides contain at least one linolenic acid. Around 1 % unsaponifiable matter, probably consisting mainly of sterols [8], has been reported [7,8,9]. The content of free fatty acids is highly dependent on the storage conditions of the seed. In oil from fresh or preheated seed less than 0,5 ffa have been found [18a]. The phospholipid content in an oil, obtained by hexane extraction of whole rubber seed was around 1 % [8], it consisted mainly of phosphatidylethanolamine (0,58%), phosphatidylcholine (0,32%) and some phosphatidylserine (0,06%). With respect to the objective of this study the most important fact from the reviewed data is the high content of linolenic acid of roughly 20%. This amount is in between that of linseed oil (30-60%) and considerably higher than in soybean oil (2 - 10%).

- 11 -

I 2.2.4. Composition of rubber seed meal

There are a lot of data about the composition of defatted (mostly expelled) rubber seed meal. Because of different materials and probably also partly because of different methods of analysis the fluctuations are rather broad. The mean values from 10 papers [3,6,10,12,13,19,20,21,22,23] are given in Tab. 3 with calculated standard deviations and extreme values.

#### Tab. 3

Avervage composition of defatted decorticated rubber seed meal

component	mean values (%) + std. dev.	ertreme values
н <sub>2</sub> 0	8,2 ± 2,9	3,4 - 12,5
ether extract or oil	10,6 <u>+</u> 2,7	4,4 - 14,7
crude protein	29,0 ± 4,0	22,9 - 34,3
crude fiber	6,6 <u>+</u> 3,2	2,7 - 13,9
N-free extract or carbohydrates	39,7 ± 4,8	32,0 - 47,3
ash	5,1 ± 1,0	3,0 - 7,0

So roughly the rubber seed cake after pressing out of the oil consists of 30% protein, 10% oil and 40% carbohydrates. No investigations about the nature of the carbohydrates have been found in the literature.

About the contents of Ca and P several authors [10, 19, 20, 22] give data, which result in mean values of  $0.4\% \pm 0.2\%$  for Ca and  $0.6\% \pm 0.1\%$  for P.

In lit. [22] a complete mineral composition is given (mean values of four different samples):

Ca: 0,88 ≸ P : 0,94 ≸ Fe: 147 mg/kg Hg: 0,34 ≸ Cl: 0,18 ≸ Hn: 25 mg/kg K : 1,54 ≸ Zn: 112 mg/kg Wa: 0,21 ≸ Cu: 32 mg/kg

The most important constituent of the meal of course is the protein. Its amino acid composition, as it has been found by several authors, is given in Tab. 4.

	Tab. 4					
Amino acid	composition	of	rubber	seed	rotein	
	(\$ w.r.t.	pro	tein)			

				_			
ref.	[10]	[12]	[13]	[21]	[ 22]	[23]	[24]
Isoleucine	7,10	3,1-4,2	2,71	3,16	3, 38	3,1	3,8
Leucine	3,76	4,8-5,9	3,29	6,10	6,24	6,7	7,1
Lysine	2,35	2,8-4,2	2,60	2,98	3,34	5,4	3,6
Methionine	2,37	1,1-2,2		1,09	1,08	0,7	1,4
Cystine	0,91	1,4-2,0		1,33	1,38		2,9
Phenylalanine	3,04	2,8-3,8		<b>.</b> , <b>85</b>	4,94	3,8	4,8
Threonine	3,26	2,8-3,1	1,79	3,13	3,24	2,8	3,8
Tyrosine	2,24	2,6-2,8		2,69	2,74	2,6	2,6
Tryptophan	2,05	1,2-1,4			1,38	1,3	
Valine	2,13	4,2-6,5	3,56	6,64	5,98	6,4	8,0
Histidine	3,34			1,80	2,03		2,3
Glycine	2,24			3,71	3,85		4,4
Arginine	7,60			9,40	10,24		9,4
Aspartic acid	15,80			10,32	11,25	ļ	11,2
Serine	1,78			4,25	4,86		4,8
Glutamic acid	17,70			14,95	15,87		15,7
Proline	6,15			4,39	4,28		4,4
Alanine	2,62		 	4,80	4,46		4,9

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- 13 -

I 2.2.5. Minor components in rubber seed

These are mainly of interest as far as they may impair the utilisation of rubber seed in human nutrition or animal feed by the existance of hasardous components.

## I 2.2.5.1. Hydrogen Cyanide

Para-rubber-seed contains the cyanogenic glycoside linamarin [25], the same as in manioc [21], which on hydrolysis yields hydrogen cyanide. The highest HCM-contents were found in fresh kernels (up to 0,223 % HCM calculated on a moisture free basis [18a].

Simply on storage the HCN is released by hydrolysis and thus reduced by evaporation (in fresh kernels 94 % of total HCN were bound [13]). This escaping HCN may be a certain toxic danger for the surroundings [4].

Tab. 5

Hydrogen cyanide content of rubber seed kernels [18a]

Period of storage (weeks)	% н <sub>2</sub> 0	HCN-content (ng/kg)
fresh	35,9	770
1	29,0	160
3	12,7	150
4	11,4	110
14	6,5	60-
20	8,1	60

Similar results as shown in Tab. 5 were obtained by Narahari [26]. Fermented products already after one month had only around 2 mg/kg HCN [26,27]. So there are relatively simple methods to remove the HCN. In unfermented, solvent - or mechanically processed meal 55 resp. 60 mg/kg HCN were found [19].

- 14 -

## I 2.2.5.2. Gossypol

Rubber seed meal (decorticated according to analysis) contained 40 - 410 mg/kg (solvent processed) and 100 - 570 mg/kg (mechanically processed) free gossypol. The ranges for total gossypol were 300 - 715 mg/kg and 300 - 800 mg/kg resp. [19]. These figures have to be compared with those of cotton seed meal containing normally 360 - 930 mg/kg free, 9000 - 15000 mg/kg total gossypol.

### I 2.2.5.3. Saponine

1,8 % saponing were found in decorticated rubber seed kernels [28]. That is a similar level as in the meal of the oil containing leguminosea Pentaclethra macrophylla, Mucuma uriens and soybeans. After hydrolysis the sapogening were compared by TLC. The three spots differed in Rf-values slightly from those in soybeans.

### I 2.2.5.4. Tannins

0,4 to 0,5 \$ tannins were analysed in undecorticated rubber seeds [26]. They are located in the shell, since none was found in kernels.

## I 2.2.5.5. Volatile inflammable substances

Thuch substances, probably carbohydrons, have been reported to be present in kernels [4]. They cause a certain risk of fire during drying of seeds in open fired driers as copra kiln. Nothing is reported about the amount of the volatile material present in the seeds.

## I 2.3. Processing of rubber seed

For utilization of rubber seed the seeds have to be collected and processed beforehand. The fresh seeds optimally are collected from plantations every 3rd or ;th day [4,6]. Afterwards they are partially dried by sun [4,6a] or in ovens at 80 - 90°C [7]. This drying procedure to a moisture content of less than 5 % is essential to prevent ensymatic attacks (fat splitting) [3] during further storage of the material.

Starting with dried kernels [18a]  $(5-6\% H_2C)$  the free fatty acids content began to rise after 12 weeks storage (also the H<sub>2</sub>O-content increased somewhat). When the H<sub>2</sub>O-content was kept low [18a] (3-4%) all the time (storage temp. 3C-37°C), the ffa-content did not exceed 1% (in oil) during a storage period of at least 24 weeks. Sterilisation with hot steam improved these results somewhat. After 12 weeks however mould and insect attacks limited storability. Microorganisms on rubber seed have been investigated in Brasilia [29].

Processing normally starts with dehulling. This has been done either manually after cracking the shell [3] or by means of a Kalyan type groundnut decorticator [11]. The latter technique resulted (after recycling) 95% kernels with 5% shells. Seperation of kernels and shells by winnower and scoops was considered to be out of question [6]. In contrast to these more research oriented papers lit. [6a] reports, that 1976-1977 in South India (Tamil Nadu and Kerala) 97 commercial units have processed 12.070 tons of dry kernels. Dehulling here also was mostly done manually, only three mills used machinery and two a combination of machinery and hand labour. Crude oil in a technical scale is obtained by expelling [4]. Adaption of an Anderson 1 expeller to rubber seed kernels has been described [4] (8-10% residual oil in meal). Addition of 10% molasses has facilitated removal of oil [10,6].

Expelling proofed to be very difficult due to jamming of the material inside the expeller chamber [11]. Cold hydrolyc pressing, successful in laboratory scale, gave high oil yield, but could not be adapted to cold crushing in the expeller [11]. According to lit. [5] the expeller cake may be either heat treated and pressed under high pressure to give some more oil, or more usually, it is solvent extracted afterwards.

In South India rubber seed kernels are processed in a rather large scale by groundnut oil millers with the same equipment as for groundnuts, that means rotary machines [6a]. Only a very few expellers were used. About 20 to 30 % molasses was added to the dried kernels resulting in an oil recovery of 30-40 % and cake recovery of 60-75 %.

Detoxification (HCN-removal), apart of the simple storage method, was achieved by fermentation (soaking the meal with tap water 1:3 for 24 hrs.) [26]. Soaking with ash solution or water or roasting (350°, 15 min.) were also applied for detoxification [21]. Without giving figures, roasting was estimated to be the best method [21], but already without special treatment there were no toxic effects to be seen in feeding experiments [21].

Refining of crude rubber seed oil has not been described much in the literature covered in this study. According to lit. [5] it can be refined in a similar manner as linseed oil.

## I 2.4. Utilization of rubber seed

In this chapter the economical views for the utilization of rubber seed. given in several papers, will not be reviewed, because they may depend largely on the special situation of the local area at the time of publication. However, some figures about the availability of seeds will be given. For 1976 in Malaysia a production of 200-300 kg seeds/ha are reported [34]. The expectations for Kernataka, India, 1983 were only 95 kg/ha [7]. A similar figure can be calculated for Sri Lanka 1968 [4]. In still former times (1918, 1927, 1928) between 55 and 130 kg/ha have been found in Malaysia [29a]. The actual seed yield may vary very much [34] due to diseases and weather conditions [2,5a,29b].

Obviously already in 1929 serious attempts have been made to utilize rubber seed. An export of 7.905 tons from Sumatra intended for oil production and plans for a decortication plant in Malaya have been reported [29c]. The reasons why these activities have not been continued, are discussed in lit. [29b].

## I 2.4.1. Rubber seed meal as animal feed

Judging from the literature, utilization of rubber seed as animal feed has aroused much interest. An Indian feed manufacturing company 1977 actually sold already feed containing 10 % RSM [6a]. Mostly the cake, obtained after pressing out much ot the oil, has been used. The worldwide annual potential of RSM has 1983 been estimated to be 1,68 x  $10^6$  t [10].

In none of the reviewed investigations toxic effects due to HCN or cyanogenic components have been found (the HCNcontent in RSM mostly was in the order of 50 mg/kg. Especially in pigs, given up to 30 % RSM (HCN-content (60 mg/kg), no goitrous or anaemic symptoms were found. Neither daily gains nor carcass characteristics were affected by RSM [29d]. However a negative influence on fertility and hatchability of hen eggs was observed [30,31,12], even at a 10%-level [12]. This is probably not due to cyanogenic components. 10% RSM in the fodder of breeding cows also drastically affected the fertility of the herd (cited in lit. [5]).

Layerhens could be fed (without detrimental effect [31]) with up to 20% RSM. Probably due to an imbalance in amino acid composition (shortage in methionine and lysine) higher ratios led to negative influences on the eggs (size, thickness of shell). If additionally lysine and methionine were given, up to 30% RSM could be fed to layers (50 weeks) without negative effects [32]. Egg production decreased however with 40% or 50% RSM in the diet, whereas the quality of the eggs even increased [32]. In lit. [33] it is reported, that up to 20 % RSM substituting coconut meal even increased weight gains of broilers and that at a 25%-level egg production was not affected.

For broilers 20 % [33,12] to 25 % [34] RSM could be used in a basic diet of maize and soybeans meal. Giving additional lysine and methionine, up to 45% RSM were fed to broilers without negative influences [32]. If the basic diet was meat meal and maize, only 10 % RSM could be applied even in the presence of additional methionine [35]. Using fish meal and maize RSM could be rised to 20 % [35]. Pullets however could be fed with 40 % RSM in these diets, showing only slight signs of amino acid imbalance [35].

Chickens were also used to assess the appearent metabolizable energy; 2,80 kcal/g [10] and 2,86 kcal/g [32] have been reported but also 1,79 kcal/g [36]. The true metabolizable energy was even somewhat higher (3,00 kcal/g) [10]. The determined gross protein value was 47,0 [10] (chicken).

Poultry has been fed also whole kernels [21]. No toxic effects were seen up to 50 % kernels in the fodder, which had been pretreated by roasting or soaking with water or ash. Roasted RSM was accepted best by poultry or swine.

Also the rubber seed oil has been added to chicken fodder up to 8 % instead of coconut oil without any obvious drawbacks [37].

For growing swine only 10 % RSM could be included in the fodder. 20 % and especially 30 % resulted in poor weight gain and feed conversion efficiency [38]. Insufficient amino acid balance (lack of lysine and sulfur amino acids) is thought to be responsable. In lit. [5] however much better results are cited.

Growing calves seem to be better adapted for a RSMcontaining diet. 30 % RSM replacing the same amount of cotton seed meal resulted in better results than 15 % or 0 % w.r.t. weight gain/kg feed or weight gain/cost [20]. Maintainance of health was good.

A rather similar investigation is described in lit. [39]. It is concluded that up to 30 % RSM can be incorporated in the fodder for growing calves.

Also in lit. [8a] up to 30 % RSM in fodder for calves and cows were used. The costs for fodder were thus reduced considerably without loss of performance. Similar positive results are reported in the papers [39a, 39b, 39c].

Feeding RSM instead of linseed meal to cows resulted even in 10 % increase of milk production [40]. Goats developed quite normally when fed with 35 % RSM in

- 20 -

their fodder for 3 months [41]. Very limited feeding experiments with sheep indicated a high digestability of RMS [41a].

## I 2.4.2. Rubber seed meal in human nutrition

Only one article has been found, which exactly deals with this topic [42]. It reviews some older papers and gives some intentions for future work. Some other papers about feeding trials with rats, however, will be treated under the above head-line.

Lit. [23] quotes, that rubber seed is used already in the diet of people, living near the plantations. Detoxification may be done similar as with cassava (24 h soaking with water, boiling for half an hour).

Protein efficiency ratio of RSM (PER = gram weight gain/gram protein eaten) was studied in rats at 5, 10 an 20 % protein level. The HCN-content of the RSM was 34 mg/kg. At 5 % protein level the PER was only 0,9 as compared to casein (2,3). This is probably due to low methionine levels. At 20 % protein level (60% RSM in diet) PER was 1,4 (casein 1,6). No toxic effects were observed. The PER of RSM was in about the same order as that of other oil seeds. Former feeding trials with rats had been less satisfactory [43].

Also in lit. [22] RSM was found less good than soybean -, peanut- and casein-protein (10 % protein in basal diet fed to rats). PER for RSM here was even negative (but not for full fat kernels). Responses to amino acid supplementation suggests, that lysine and methionine are the most limiting amino acids in rubber seed protein. The conclusion is, that full fat rubber seed, although inferior to peanuts or soybeans, has some nutritional value, but defatting (by solvents) deteriorates the protein. Lit. [13] on the contrary states, that the raw seed (with around 0,13 % to 0,23 % HCM!) has a low nutritional value and even caused death (rats, 10 % crude protein in the diet). Pretreatment by soaking with water and 1 h cooking reduced the HCN-content to less than 5 % of the original value. Even then the PER was only around 1/3 of that of casein, but close to that of traditional cereals like corn. Limiting amino acid was threenine.

At a lower level (7,4 - 12,4 % RSM in diet) RSM had no influence on weight gain, nitrogen digestibility and carcass composition of rats [24]. There was no difference when autoclaved RSM was used.

# I 2.4.3. Technical utilization of rubber seed

Apart of occasionally remarks that RSM could be used as a fertilizer (which actually has been done in India [6a]), only the oil has been considered for technical utilization. Of course the high content of unsaturated fatty acids may make it useful for substitution of linseed oil in paints. These possibilities and the technical and economical situation in Sri Lanka are reviewed in lit. [5] (1973): Rubber seed oil can substitute 25 % linseed in oil paints. Its drying properties could be improved by reaction with maleic anhydride. Much more important however is its use in alkyd resins (reaction with glycerol and phthalic anhydride). These products were commercially produced in Sri Lanka in 1973. Heating rubber seed oil with sulfur results in the so called factice, a valuable aid for rubber and in mixing processes. Epoxidation leads to products useful to improve some properties of PVC.

In more recent time more papers have been published dealing with industrial use of rubber seed oil. So it has been reported, that the oil can replace 80 % of linseed oil in air-drying medium-oil alkyds [44] directly or after epoxidation [45]. Polymerisation of rubber seed oil with 20 - 45 \$ dicyclopentadiene resulted in a drying oil useful in low quality paints [46,47,48].

Rubber seed oil could be fractionated (solvents) in products with increased iodine value (useful in paints and resins) and products with lower iodine value (useful in soap manufacture) [49].

To utilize rubber seed oil in soaps (or as fatty acids), splitting studies have been performed [50,51]. The unsaturated fatty acids could be converted into stearic acid by electrochemical reduction [52].

Apart from these academic studies it is estimated, that 1976-77 1880 tons of rubber seed oil have been consumed in Tamil Nadu and Kerala (~50 % of the total amount produced in India). This went mainly into the soap industry, only about 100 tons were used for paints [6a]. Sri Lanka exported 420 tons of oil in 1973 [5].

#### I 3. Summary

About utilization of rubber seed quite a lot of work has already been done in different countries. The oldest literature which was found in this study is dated 1903.

Many papers deal with the composition of the seeds. The kernel of rubber seed is roughly half the weight of the total seed. This kernel contains about 40 - 50 % oil, 20 % protein and 40 % carbohydrates.

The rubber seed oil contains around 20 % of linolenic acid, 35 % linoleic acid, ca. 25 % oleic acid and around 10 %

- 23 -

stearic- and palmitic acid each. Of course these figures fluctuate due to different investigations.

The amino acid composition of the protein has been analised several times. Main components are glutamic- and aspartic acid and arginine. The essential amino acids are all present in amounts ranging from ~ 1 % (methionine, tryptophan) till 6 % (leucine).

An important minor component in rubber seed is hydrogen cyanide. In fresh kernels an amount of up to 0.2 % has been reported. It is present as a glycoside. During storage of the kernels for several weeks the HCN-content drops below 100 mg/kg. Small amounts of gossypol (~ 0.1 %), saponins (1.8 %) and volatile inflammable substances have been found in the kernels, ~ 0.5 % tannins are located in the shells.

In processing of rubber seed it is important, to collect the seeds as soon as possible and dry them to moisture contents below 5 %. This limits liberation of free fatty acids and moulding.

The process mostly starts with cracking and manual decortication. In South India (1976 - 1977) about 12000 t kernels have been milled with ground nut equipments (rotary machines). Expellers have been used to press out the oil, but with unsatisfactory results.

Utilization of rubber seed is largely dependent on the availability. The figures about the seed yield vary between 55 kg/ha and 300 kg/ha. It depends largely on weather conditions, plant diseases and clone of the rubber tree. As a worldwide potential 1.7 mio tons (rubber seed meal) have been estimated 1983. Rubber seed meal has been fed to pigs, hens and chickens, cows, calves and goats. It can replace up to 30 % of other feedstuff like linseed meal. Some fertility problems were observed with hens and cows. The HCN-content obviously is not a serious drawback in the utilization of rubber seed meal. Lysine and methionine are the limiting amino acids in rubber seed meal.

Rubber seed oil can replace up to 80 % linseed oil in paints of minor quality. Alkyd resins containing 25 % rubber seed oil instead of linseed oil have been produced on a commercial scale in Sri Lanka. In India 1880 tons of rubber seed oil have been consumed 1976 - 1977, mostly in soaps.

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#### II Field Study in Sri Lanka

#### II 1. Introduction

This part of the report deals with the revealed information during a field study in Sri Lanka which was carried out w.r.t. the technicological and economic situation of the utilization of rubber seed. From the information obtained by the literature study (see Part I) and the statements received from interviews and discussions with research scientists, estate managers, oil millers and production managers of paints and animal feed industries the frame work should be set up for a development of a technology for the production of vegetable oil and animal feed in the countries where rubber production is available. A list of these contacts and the people met for interviews in Sri Lanka is given in appendix 2.

#### II 2. Technical and technological aspects

## II 2.1. Seed availability

This aspect of course is a very basic one, which has been hardly mentioned in the literature. It was learnt that, at least in Sri Lanka, it is a rather recent experience that the seed fall can fail completely in certain years. Taking into account the opinion of experts and estates managers as well as the poor information from the literature [1], the availability of rubber seed depends on a lot of various conditions and may hardly be influenced by agricultural techniques.

Amount and quality of the rubber seed growth depends on the following conditions:

1 1 1

- 1. Weather: The production of seeds from each type of clones varies from year to year according to the weathering conditions. In some years when it rains strongly during the flowering time from March to May the blooms are washed out and no seeds appear in summertime. In such years in these areas nearly no rubber seeds will be obtained. If there is high rainfall during the seedfall time from July to September a lot of seed may become moulded or will rot on the ground within a few days after the fall. In other years, when there is a drought from March to May, the blooms dry up and no seeds will appear in summertime.
- 2. Genetic: The different types of rubber seed trees produce different amounts of seeds. Until now only very few studies have been undertaken to determine the amount of rubber seed w.r.t. the different types of clones.

New types of clones, developed in Malaysia and in the Rubber Research Institute of Sri Lanka, which give high yield in the production of Latex, produce rubber seed which amounts to less than 60 % of some of the older types.

3. Diseases: Phytophthora attacks the seed pods, causing them to rot. Oidium mildew destroys the flowers. Both diseases are largely under control now, but control is only done to protect the trees, not to save the seeds.

Depending on the type of clone and the weather conditions 50-150 seeds can be expected from one tree auring falltime. Assuming that the stand of trees by hectare is about 275-350, depending on planting area, the production of seed/hectare in a year can vary from 12.500-52.500. It has been estimated that 220 seeds will form about 1 kg. Therefore 50-250 kg (200 kg/ha in normal years) of rubber seed can be expected per hectare in one season. A more detailed study about the seed yield/ha depending on site and clone in Sri Lanka is currently under way within the frame work of a doctoral thesis carried out at RRISL [2].

## II 2.2. Collection of rubber seed

Seed collection is a tedious work because the seeds have an earthlike colour and the ground of the rubber plantations is mostly covered with leguminoses so that most of the nuts are hidden. Furthermore, some of the lands where rubber is growing is hilly and rocky - the latter is true especially in Sri Lanka and part of South India - and therefore seed collection cannot be done very effectively.

Thus, only 60 % of the total acres of rubber land in Sri Lanka are suitable for seed collection. In Sri Lanka currently about 250 000 ha are rubber land (increasing). From 150 000 ha (60 %) about 30 000 t seeds could be collected in normal years.

In Sri Lanka as well as in South India most of the seed collection is done by children from pendants of the rubber estates. At present in Sri Lanka the oil millers quote a price for the seed and traders then quote prices to shops situated in the villages. In some years when there was high demand of rubber seed, collection agents organized the seed collection also with adults, but always most of the seed collection was done by children. Using children for the collection is a cheap method but it should be mentioned that payment even for the children might go up with the growing marketing potentiality for the rubber seeds.

As collection centres factory houses of rubber estates or the factory houses of oil millers have been used in some cases. To avoid moulding, rotting or germinating of the seeds they have to be collected fairly fresh. Optimal collecting of the seeds on the same ground has to be repeated at least every 4th day if not more frequently.

# II 2.3. Drying and storage of rubber seed

Before storage, the seed has to be dried (preferably to a moisture content, < 5 %). This is mainly to prevent moulding and rotting. But also lipase activity is reduced and shrinking of the kernel makes decortication easier. Drying has been normally done in the sun at the estates, but drying space and storage capacity sometimes may be limiting factors for the estates.

Oil millers reported about heap storage of undried seeds in their factories for 2-3 months without problems. The accidental moisture content, however, may have been low and also the oil was used for technical purposes only. Drying at 60 -80°C resulted in more oil with less free fatty acids than drying in the sun (RRIM, Annual Report 1975, p. 160). Ovens should be preferred to smoke houses because phenols could diminish the oil yield (private communication Dr. Nadarajah). Storage of dried kernels in polythene bags slows down formation of free fatty acids and prevents mould growth.

## II 2.4. Production of oil and cake

For the production of oil and cake from rubber seeds several methods have been used more or less successful. In Sri Lanka most of the seeds have been milled in copra mills. This however can be done only with undecorticated seeds because the kernels are too fluffy for the relatively wide screws of the copra mills. The throughput is much less than with copra and

- 37 -

the wear of the machinery due to the shells is feared by the millers.

The oil produced is of medium or bad quality and the yield is about 60 % of the total content. The cake contains relatively large particles of the solid shell which might damage the throats and the intestines of cattles and pigs if it is used as animal feed. Therefore most of the rubber seed cakes produced in copra mills are used as manure.

Another technical drawback of milling rubber seeds on the copra expeller is that the seedfall season coincides with the coconut harvest. So the millers are unable to spare adequate capacity for the milling of rubber seeds as the mills are obcupied then with the milling of copra. Therefore Messrs. Lever Brothers developed alternative milling processes. First trials in 1966 and 1967 were done with domorticated rubber seed kernels on a Anderson expeller as well as on a German EP expeller. The latter was an expeller in a pilot plant at CISIR in Colombo. The yield of processed oil in all these experiments was very low, so that more than 35 %, sometimes 50 % of the oil content of the kernels were left as a residue in the cake.

In 1972 an unsophisticated method of milling rubber seed used on the rubber estates by support of Messrs. Lever Brothers was introduced. This process involves crashing the decorticated seeds in a chakku mill, cooking the crashed kernels and finally espelling the oil by means of a manually operated press. With this arrangement an oil yield of ~50 % was obtained. The chakku mills were operated by bulls. It was reported that in South India (Kerala) chakku mills operated by electrical power exist and are being used for the same procedure of utilizing rubber seeds [3].

1 1 1

In many interviews disapproval was expressed mainly about two technical problems in rubber seed processing which seem to be of importance:

- a) If the meal is to be used as feeding stuff, the shell should be either removed or ground very fine. The latter requires special mills and relatively high energy costs. Decortication even in the bigger scale experiments in Sri Lanka (Lever Brothers) has been done by hand so far. But also the rollers for rubber sheets, available at the estates, could be used to crack the shells, followed by a kind of winnowing/sieving. In India a special machinery is in use for this job.
- b) The oil, at least that obtained from copra expellers, contains fines which makes the filtration step in the refining process very time consuming.

### II 2.5. Consumption of rubber seed oil

It is reported in different statements that several trials were done in Sri Lanka to make use of rubber seed oil for the manufacture of laundry or washing soaps. The same is reported for Kerala and Tamil Nadu [4]. The intention to use RSO for the soap production was mainly, to replace parts of the coconut oil to obtain a somewhat softer soapstock. The commercial objective was to have available an oil of an appropriate quality which would not be more expensive than coconut oil.

From all statements it turns out that technically the darkening of the colour of the oil and the presence of unknown particles causes bleaching and filtration problems in the refining process. The filtration time in the bleaching process of RSO is ten-fold as much as that of coconut oil and thus the total process is rather ineffective. If not more

- 39 -

than 10 % of refined RSO is used for the soapstock a fairly well coloured soap is obtained. If RSO is used, only 2 % is acceptable. Darkening during storage of the soap limits the use of RSO for soap manufacture and inquiries made by soap manufacturers show, that washing soap manufactured from RSO is of inferior quality and the consumers in Sri Lanka as well as in Kerala require a higher quality of soap. Nevertheless use is already made of rubber seed oil in a mixture together with coconut oil for the preparation of solid soap bars.

RSO has sometimes been used for paint manufacture. The oil contains about 35 % of linoleic and 25 % of linolenic acid, and therefore was used to replace part of linseed oil as a drying oil in paint industry. Because rubber seed oil does not contain sufficient amounts of linolenic acid it cannot replace linseed oil totally but is used as an extender of linseed oil. Whether unrefined or refined RSO is used in this application could not be established evidentially.

If RSO is used as an extender for linseed oil instead of soybean oil the drying oil may be used for all current paints but not for clear colourless lacquers, because the increasing darkening of the products containing RSO. With the current quality of the RSO no white coloured paints can be prepared. This, however, might be cured by using a better refined oil.

Most of the RSO in Sri Lanka has been used for the manufacture of alkyd resins. Inquiries with the manufacturers of alkyd resins assured, that the properties and the quality of the RSO obtained in the different milling processes is adequate for the production of alkyd resins and that there is lot of know-how at the different paint manufacturers to make use of the RSO. As linseed oil which has to be imported into Sri Lanka is replaced by RSO a saving of foreign currency is obtained. But this is true only if the cost for RSO do not exceed the cost and the import duty of linseed oil or other oils used as extender of drying oils (soybean oil). Therefore, the only limiting factors in this field are the availability of RSO and the costs of the oil in comparison to the costs of linseed or soybean oil.

In the years of large RSO production some of the RSO was exported to European countries (Netherlands, Germany) and was used for the production of oleo chemicals.

Not much emphasis is put on the possible use of RSO as an edible oil until now. The comparatively high amount of unsaturated fatty acids increases the nutritional value of the oil compared to coconut and palmoil. However, the relatively high content of linolenic acid in RSO and a slightly bitter and off-taste which might occur in the present quality of RSO has limited its use in human nutrition especially in a country where coconut oil and palmoil is available all over the year as a common product on a relatively cheap price level.

If - what has to be checked in laboratory trials - a better refined and highly stabilized product could be obtained from a crude RSO, a mixture of RSO and coconut or palmoil may be used as an edible fat with a high nutritional value.

The difficulties which occur in the refining of the oil, especially in the bleaching and filtration steps require further investigations.

## II 2.6. Consumption of "ubber seed cake

The rubber seed cake is used in Sri Lanka in some places as a fertilizer. This is done especially with those cakes com-

- 41 -

ing from oil mills where copra expellers are used to produce the RSO. Large and hard pieces of the shells of the rubber seed give damage problems with cattles, pigs and poultry if this cake is used as animal feed.

In the inquiries with the estates managers and the production managers of the animal feed industry companies, which all showed general interest in making use of the rubber seed cake for animal feed at the cattle or pig farms, a certain reluctance was roticed. Growth inhibition and infertility as well as in some cases high dying rates were told to be found when rubber seed cakes have been used. In contrast to this predominantly negative statements, in many published papers the acceptability of rubber seed cake from decorticated seeds as a component up to 40 % in animal feed is reported. The Veterinary Research Institute of Sri Lanka in Kandy has recently carried out a feeding study for six months with undecorticated rubber seed meal using 16 cattles. Rubber seed cake was used up to 40 % in this feeding trial together with maize and fishmeal. No adverse effect is found in this feeding study so far. Growth of the cattle as well as fertility are reported to be in good order.

The inconsistancy of the statements about the suitability of rubber seed cake for animal feed may find its explanation in the lack of knowledge about the pretreatment and the dietary value of the rubber seed cakes applied. Too big particles of the rubber seed shell or the hydrogen cyanide content of fresh rubber seed kernels as well as the possibility of aflatoxin contamination are factors which might have had adverse effects to the animals. But these obstacles may be overcome from the technical point of view by using correct drying and storage conditions as well as by an adequate milling procedure.

- 42 -

A report from the RRIM [5] says, that rats have been fed with 40 % rubber seed meal in their diet without toxic effects. Broilers and chickens can tolerate up to 15 %. Mould formation can be eliminated by using 0,5 % Luprosil (Ca-propionate).

#### II 3. Economic aspects

In the consideration of economic aspects for the utilisation of rubbe: seed in a developing country like Sri Lanka or India the figures for the profitability of a process will be influenced by several factors. The relatively short period of 3 or 4 months within a year the rubber seed is available, as well as the yearly fluctuating amount of seeds make any economic evaluation very difficult. In this chapter use is made of those cost figures which are based on fairly true facts at present which are revealed in the interviews but which may vary within a rather short period of time. Therefore, all calculated figures should only be taken as an indication of cost.

Currently about 250 000 ha are cultivated in Sri Lanka with Hevea brasiliensis. Because of the hilly structure of the land not more than 60 % are suitable for rubber seed collection. Assuming a yield of 200 kg seeds/ha about 30 000 t seeds (estimates as low as 9-12 000 t have also been given) should be available in a normal year in Sri Lanka. Since Sri Lanka produces about 4 % of the total world production of rubber, a rough estimate for the minimum amount of seeds available worldwide may be in the range of 500 000 to 1 000 000 t.

Milling whole seeds in a copra expeller yields a little more than  $15 \ \%$  oil. In view of the above mentioned 30 000 t seed the potential of RSO by this process in Sri Lanka will be 4 000-5 00C t/year. Milling decorticated kernels in small equipments (chakku-type, man-operated presses) yields 20-25 % oil w.r.t. kernels. This results in 3 000-3 500 t/year. Although the oil yield in this case is less than starting from whole seeds, the advantage of this process is, that a valuable feeding stuff is obtained (s. p.42).

Collection costs of seeds in Sri Lanka are hard to figure out. In the last year with a normal seed fall (1982) 0,3 -0,4 SL Rps/kg have been paid. In 1985 it was expected to be 0,4 to 0,6 SL Rps/kg, but 1985 was a poor seed year, too. It can be assumed that in 1985 if it would have been a year with normal seed fall, about 0,4 SL Rps/kg should have to be paid for collection.

Once the seed has been collected, it has to be dried rather soon. No figures for drying costs were available. Drying costs depend on the local possibilities and weather conditions. In South India 1977 the prices for dried kernels were about 50 % to 100 % higher than for undried kernels. Probably the same relation would apply for drying of seeds in Sri Lanka.

If the seeds are to be milled in existing oil mills, they have to be transported. For 5 t-lots the transportation costs are 15-20 SL Rps/mile in Sri Lanka. Assuming an average distance of 50 miles between the places where most of the oil mills are situated (Colombo) and the growing areas, transportation costs will arise to about 0,2 SL Rps/kg which have to be added, thus the cost for undried seed at the mill will be 600 SL Rps/t.

Decortication, if done by machinery (groundnut decorticators) could not be calculated, because no distinct information about the equipment was available. If decortication is done in the growing areas, the hulls have to be cracked by an inerpensive roller system possibly a rubber sheet former. The cracked shells then have to be separated manually from the kernels. This separation should be less labour intensive than the collection of seed. So we assume the costs for manual decortication at the estates to be not more than 0,2 SL Rps/kg seed. In 1976-77 manual decortication costs amounted to 10-30 % of the costs of undried seeds in South India [6]. As compared to processing of seeds in the oil mills 0,1 SL Rps/kg seed are saved in this case because the shells (ca. 50 % of the whole seed) have not to be transported but could be used locally as fuel or fertilizer.

Milling expenses in small equipment (chakku, handpress) in the growing areas can be assumed roughly from investigations and calculations carried out by Lever Brothers in 1972. At that time processing costs were roughly 40 % of the costs of the kernels. If we calculate the price of 1 kg kernels at present to be 2 SL Rps (2 kg seeds ~ 1 kg kernels; 2 kg seeds take 0.8 SL Rps for collection, 0.8 SL Rps for drying and 0.4 SL Rps for decortication) then the milling expenses will be ~ 0.8 SL Rps/kg kernels.

From these figures the costs for crude oil and cake processed at the growing area can be estimated and is given in the following three examples:

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Costs:
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2 000 SL Rps 1 t kernels 800 " " (in rel.to kernel milling costs costs 1972) additional expenses: (manpower for organisation and supervising, transport costs in the 600 " growing areas) drums and begs for 290 " (in rel.to kernel costs 1972) oil and cake 230 . ( \_ " \_ ) depreciation 20 % transportation of 200 " 1 t to Colombo total costs for 220 kg oil + 700 kg cake (8 % milling loss) 4 120 SL Rps -Selling Prices: cake (3 SL Rps/kg 2 100 SL Rps ~ copra poonac) oil (15 SL  $Rps/kg^{*}$ ) 3 300 " 5 400 " \*\* 1 300 SL Rps **Profit:** \_\_\_\_

<sup>\*)</sup> According to a Sri Lanka paint producer the current rubberseed oil price is about 20 SL Rps/kg. At this price it starts to get too expensive for paint industry but at a price of 15 SL Rps/kg there would be a good demand.

Calculation for processing oil and cake at central milling places without decortication:

#### Example 2:

Costs:

1 t seed	400	SL	Rps
transport	200	Ħ	
milling costs + depreciation	2 250		
	2 850	SL	Rps

 Selling Prices:

 150 kg oil (15 SL Rps/kg) 2 250 SL Rps

 800 kg cake
 250 " "

 Profit:
 - 350 SL Rps (loss)

Here the milling costs cannot be calculated. They must be considerably higher than for copra (~1 500 SL Rps/t CN oil), because the through-put for rubber seed is about only 1/10 of that of copra. Also the stronger wear of the machinery has to be considered.

It was reported by an oil miller that at the current price of rubber seed of 0,6 SL Rps/kg and the current price of RSO (20 SL Rps/kg) production of RSO for Sri Lanka might just be worthwhile, but production for export would be no business. If the oil mills would start with decorticated material (done manually) too, the following result is calculated:

Example 3:

Costs: 1 t kernels 2 200 SL Rps (transport included) milling costs 2 200 \* \* 4 400 \* \* Selling Price: 250 kg oil (15 SL Rps/kg) 3 750 \* \* 700 kg cake (3 SL Rps/kg) 2 100 \* \* 5 850 \* \* Profit: 1 450 \* \*

So also for oil mills decortication is of advantage. It is doubtful, however, whether this is done profitable by machinery, which could be employed for rubber seed only.

If one applies in these 3 examples the production costs only to the oil, a price between 18-19 SL Rps/kg oil can be calculated. So it is obvious, that the profit in case of decortication is mainly from the increased value of the cake.

Also without decortication the cake value probably could be increased by grinding. Thus in example 2 the 800 kg cake could sell for probably 1,50 SL Rps/kg = 1 200 SL Rps. It is not known, however, which costs will arise by this additional grinding step (investment in grinder, energy).

As can be seen from these examples, the profit rises if the endproducts are high priced products. The oil obtained in the examples 1-3 is only crude oil for industrial purposes. To raise the price two possibilities have to be considered seriously:

- To refine the oil to get an edible oil (CN oil sells for ~ 30 SL Rps/kg in Sri Lanka).
- 2. To produce oleo chemicals out of the oil that means hydrolysis and processing of fatty acids and glycerol. The current prices of fatty acids on the world-market are given below (average figures Jan.-Oct. 1985):

palmitic acid	(min.	93	<b>%</b> ):	27	100	SL Rps/t
stearic acid	(min.	92	<b>۶</b> ):	29	400	3
oleic acid	(min.	71	<b>≴</b> ):	24	400	
linoleic acid	(∎in.	64	\$):	30	400	Ħ

Whether manufacture of fatty acids (or other oleochemicals like emulsifiers) is worthwhile, depends on the costs of RSO in relation to the costs of the now used starting material for these products. Certainly it is not favourable to base such a production on RSO alone, but due to demand and availability mixtures with other fats should be used.

### II 4. Summary

From discussions with estate managers and oil millers it appeared that a problem for utilization of rubber seed could be its fluctuating availability. Mainly due to weather conditions seed fall may fail completely in some years. In normal years ~ 200 kg seed/ha are expected. In Sri Lanka occasional collection of seeds has been done by children. The oil millers quoted a price, agents organized the collection in the villages or at the estates. The seeds have been dried in the sun or in snoke houses at the estates to prevent moulding during storage. Since the main seed fall coincides with the coconut season, the oil millers have to store the seeds for 2-3 months until they can be processed in the copra mills.

Using this equipment, only undecorticated seeds could be processed, since kernels are too fluffy for copra expellers. The throughput is low due to filtration problems of the oil. The hard shells increase the wear of the machinery. In 1972 a simple equipment has been used directly at an estate for processing RSO from decorticated seeds. This obviously was similar to a process operating in South India in several places.

Use is already made of RSO in a mixture together with coconut oil for the preparation of solid soap bars. The advantage of this use is 1. the partial replacement of coconut oil which may be used as edible oil of hight quality and 2. a softer soap bar obtained because of the comparatively high amount of unsaturated fatty acids in the oil.

Disadvantages are the yellow colour of the oil and the darkening of the scap during storage if more than 5 % of the coconut oil is replaced by RSO. From the economic point of view the use of RSO for soap preparation instead of coconut oil is only beneficial if the cost for the RSO is below that of the coconut oil.

Further uses are made of RSO as an extender of drying linseed oil in the paint industry. But because of the increasing darkening of products containing RSO it cannot be used for clear colourless lacquers. If imported linseed oil is replaced by RSO, a saving of foreign curency is obtained. But this is true only if the cost of RSO does not exceed the cost and the import duty of linseed oil or other oils (soybean oil) which are used as extender for drying oils.

Quality and properties of the already produced RSO is reported to be satisfactory for the production of alkyd resins. The only limiting factors in this field are the availability of RSO and the costs of the oil in comparison to the costs of linseed or soybean oil. With the current quality of the RSO no white coloured paints can be produced because of the above mentioned darkening of the products. This, however, might be cured by further refining.

Not much emphasis is put on the possible use of RSO as an edible oil for human consumption until now. The comparatively high amount of unsaturated fatty acids increases the nutritional value of the oil compared to coconut and palmoil. However, the content of linolenic acid in the RSO and a slightly bitter taste which occurs in the present quality of RSO has limited its use in human nutrition particularly in countries where coconut oil and palmoil is available all over the year as a common product for a relatively cheap price.

Therefore it has to be examined in laboratory trials whether a better refined and high qual product could be obtained from crude RSO by a refining proceedere which is more adapted to the properties of the RSO.

- 51 -

Rubber seed meal is mainly used as fertilizer. In the attempts to make use of RSM as animal feed unsteady results were obtained. Lack of knowledge of proper pretreatment of rubber seed meal is a possible reason for negative results in feeding trials. As the RSM is reported in the literature to be of good nutritional value, attention should be given in laboratory trials to reveal possible hazard substances in the minor components of the RSM.

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#### III Laboratory investigations

#### III 1. Introduction

A lot of knowledge about rubber seed, its composition and its utilization does exist already. Therefore within the laboratory investigations the work was concentrated on such areas, in which the knowledge was not sufficient for proper utilization. These areas were mainly the questions of refining and whether the oil can be used for human consumption. Another aspect of the laboratory trials was the problem of the minor components in rubber seed, which could hamper its utilization from a practical point of view.

#### III 2. Rubber seed

The starting material for the investigations were rubber seeds (~ 80 kg) which had been collected under the guidance of the Rubber Research Institute at Sri Lanka at the plantations in August 1985. The seeds were collected within 3 or 4 days after seedfall and dried immediately in an air oven with air circulation at 70-80 °C to a water content of below 5 % (about 3 days). The seeds were shipped by air freight to our laboratory in Hamburg within 1 week. After arrival in the laboratory the seeds were stored at 0°C until use.

Because of the bad seed fall in 1985 in Sri Lanka, due to adverse weather conditions only 80 kg seeds could be sent to the Hamburg laboratory at that early date.

#### III 3. Rubber seed oil

## III 3.1. Separation and Refining

To obtain the oil, the crushed kernels were extracted with hot petroleum ether (s. scheme 1). This process was chosen, to get as much oil as possible; it was not chosen as a direct simulation of a technical process. The way, the crude oil has been refined, follows more or less a standard laboratory method, which is designed to simulate the technical process, applied to fats used as edible oil. The method is outlined in scheme 2.

The fat content of the kernels, received from Sri Lanka, was 37 %. This is at the minimum of the range, previously reported in the papers (see part I, chapter 2.2.2., page 9). The reason may be the early harvest date.

The extraction process was carried out after one, two and four months storage of the seed at -  $0^{\circ}C$ . It is interesting to note, that even at this low storage temperature the acid value [1] of the crude oil had increased:

	0ct. 85	Nov. 85	Jan. 86
A V	6.4	13.9	17
oil yield (%)	32	24	25

The water content of the kernels at all three extraction trials was 7.6 %. So even at these low temperatures fat splitting enzymes were active. Lipase activity in these nuts could be demonstrated by a lipase screening test [2] (s. appendix 3, p. 1).

The increase in free fatty acids was also noticeable by the fact, that the crude oil from Nov. 85 emulsified much stron-

ger in the desliming step than the oil from Oct. 85, so that no sludge could be separated. Thus the phospholipids were removed in the following neutralisation/sodium carbonatewater glass-treatment together with the fatty acids. But also here the washing of the oil was difficult because of emulsion formation (yield only 64 % as compared with the yield of 78 % for these two steps with the first oil).

Parallel to the increase in free fatty acids during storage of the seeds, the oil yield under the rather simple extraction conditions decreased. Whether this will occur also under more practical conditions cannot be decided as yet. Scheme 1

Crude RSO from rubber seed

15.10 kg seeds

1) cracking of the shell in a mechanic plate/press
7.10 kg shells

(47.0 %)
(47.0 %)
(5.4 %)

7.19 kg good kernels (47.6 %)

after mixing with 1 kg dry ice ground in a Stefan-Cutter stirred with 35 1 hexane and refluxed for 1 h, filtrated over a Seitz-filter (KO) extraction repeated in the same manner with 20 1 hexane each

combined hexane extracts

evaporated at normal pressure, vacuum applied towards the end

2.27 kg crude RSO (32.0 %) (15 % w.r.t. seed)

Scheme 2

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#### Refining of crude RSO

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## 1200 g crude RSO

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1200 g	Crude RSO
1	desliming
	addition of 1.2 g 50 % aqueous solution of
	citric acid at 70°C, stirring for 10 min.
	After cooling to $25^{\circ}$ C addition of 18 g H <sub>2</sub> O
	and stirring for 60 min. Then the oil was
	heated up to 60 <sup>0</sup> C within 20 min while stirr-
	ing and cooled down over night without stirr-
	ing.
66 g sludge	Centrifugation
↓	
drying 1082 g	deslimed oil (90 %)
1023 g	used for
	tralization
•	in N <sub>2</sub> -atmosphere heated up to 95 <sup>0</sup> C, addition
56 g dry sludge	of 220 ml 0.8 N NaOH, stirred for 5 min,
	settled at 60 <sup>0</sup> C. After drainage of the aque-
	ous phase the oil was washed 3 times with 100
	ml of hot saturated NaCl-solution, afterwards
	with 100 ml 0.1 N NaOH.
	Soda water glass treatment
	to the oil 3 % of 20 % Na <sub>2</sub> CO <sub>3</sub> -solution
	and 1.6 % of sodium silicate (water glass)
	were added and for 20 min life steam was
	injected. Afterwards the oil was washed with
	hot water 15 times until it was free of soap
	(pH neutral).
	Drying was done at 105 <sup>0</sup> C at 1 mbar for 30
	min.
۷	

## 894 g neutralized oil (87 %)

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bleaching
stirred under N<sub>2</sub> with 18 g Tonsil ACCFF at
105°C/1 mbar for 20 min.
filtration<sup>*)</sup>
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284 g bleached oil (28 %)

deodorisation deodorised for 3 h at 230<sup>0</sup>C with 40 % H<sub>2</sub>0 (33 ml H<sub>2</sub>0/h) in a laboratory deodorisation equipment.

241 g deodorized oil (85 %) overall yield: 19 %

A second refining trial was carried out. Starting from 1000 g crude oil a similar overall yield was obtained. Again the highest loss was in the bleaching step.

<sup>\*)</sup> Filtration proved to be very difficult. Even the hot oil containing additional filter aid (Kristall Theorit, Seitz) was running only very slowly through a suction filter. The filter paper had to be changed very frequently and this explains the high losses of oil during this step.

III 3.2. Investigations of the rubber seed oil

III 3.2.1. Analytical characterisation of the triglycerides

III 3.2.1.1. Fatty acid composition

Glycerides: The composition of the fatty acids in the triglycerides of RSO is well known from the literature. A GLC analysis of the fatty acid composition (s. appendix 3, p. 1) of the oils used in this investigation is given below.

	RSO		
fatty acid	neutralized	fully refined	
14:0	0.1	0.1	
16:0	8.9	8.8	
18:0	8.4	8.8	
20:0	0.4		
18:1c	23.4	23.5	
18:2cc	39.2	39.1	
18:3000	18.8	16.8	
18:3 isomers	0.9	1.4	
	<u>Σ</u> 99.2	Σ 99 <b>.</b> 4	

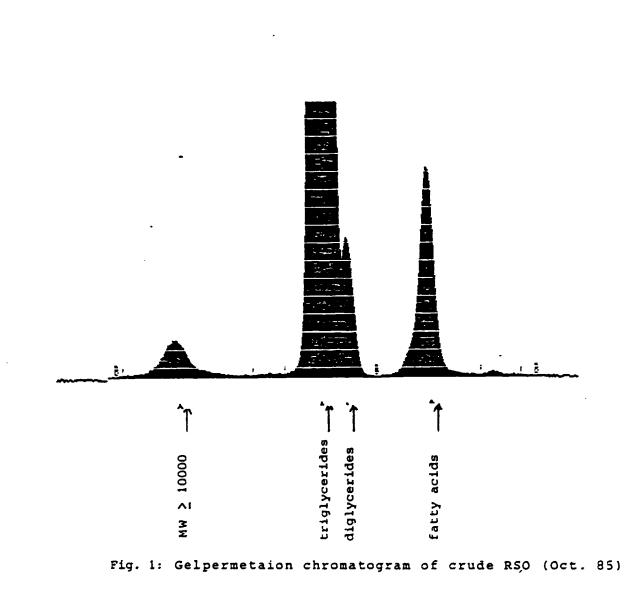
GLC-composition of RSO (fatty acid methylesters, area-%)

These compositions are well within the range, which is given in literature. In the fully refined oil obviously some isomerization of the 18:2ccc-fatty acid has taken place, either during the bleaching process (acid bleaching earth) or during the deodorization. III 3.2.1.2. Gelpermeation chromatography of the oil

GPC (s. appendix 3, p. 2) of the intact oil separates the constituents according to their molecular weights. The GPC diagrams of crude RSO and fully refined RSO are shown in fig. 1 and 2. The area %, which is roughly weight %, is shown in the following table. The fractions are coor'inated to the different types of lipids [3].

GPC-compositions of RSO (area %)			
oil from extraction			
October 1985		January 1986	
crude RSO	refined RSO	crude RSO	
3.7 %	0.3 %	7.1 %	
1.8	1.9	1.7	
93.1	95.9	90.1	
0.1	0.6	./.	
./.	./.	./.	
1.3	1.2	1.1	
	0 0ctober crude RSO 3.7 \$ 1.8 93.1 0.1 ./.	oil from extrac           October 1985           crude RSO         refined RSO           3.7 %         0.3 %           1.8         1.9           93.1         95.9           0.1         0.6           ./.         ./.	

The fraction with the lowest molecular weight contains fatty acids, monoglycerides and sterols. Mostly this fraction consists of fatty acids in case of crude RSO, what is evident in comparison to the refined RSO. In refined RSO hardly any free fatty acids should be present. The remaining 0.3 % thus is the upper limit for monoglycerides and sterols in crude RSO, since both components are hardly removed in the refining procedure. This assumption leaves 3.4 % free fatty acids in crude RSO which agrees well with the acid value of 6.4 (see p. 54, = 3.2 % free fatty acids).



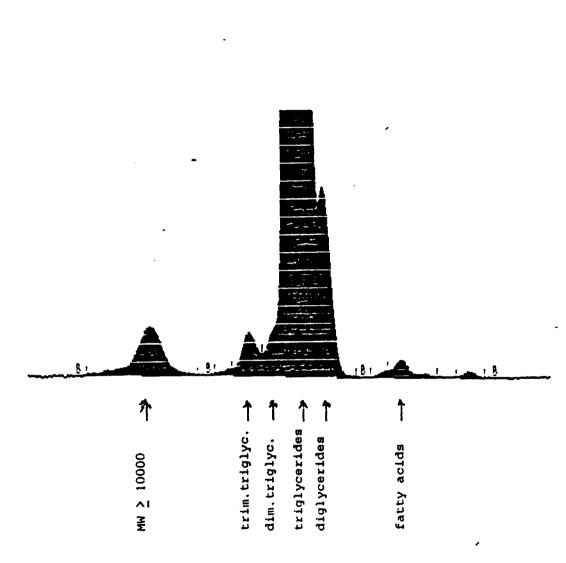


Fig. 2: Gelpermeation chromatogram of fully refined RSO

Diglyceride and triglyceride contents are a little bit higher in refined RSO than in crude RSO due to the fact, that free fatty acids have been removed.

The low content of dimeric triglycerides of 0.1 % or less in crude RSO is expected in the fresh extracted oil, where not much damage in the triglyceride molecules is caused by heat. A somewhat higher content after refining was found. That is due to the heat treatment in the deodorization step, where triglycerides containing hydroperoxy - or epoxy fatty acids are dimerised. Mevertheless the value of 0.6 % dimeric triglycerides is quite normal in refined oils.

The most interesting feature of the GPC-diagrams of the RSO is the substance with a rather high molecular weight of >10 000 D. The exact molecular weight of this fraction could not be determined by the column used in this experiment. Investigations concerning the nature of this substance are given in 3.2.2.2.

## III 3.2.1.3. Oxidized fatty acids

From the GPC-results of monomeric triglycerides it is not possible to differentiate between those triglycerides containing oxidised or normal fatty acids. The composition of the normal fatty acids may be seen from GLC of the methylesters, but the methylesters of oxidised fatty acids normally are not assessed by GLC.

Applying a method to fatty acid methylesters, which is described for polar lipids (s. appendix 3, p. 3) 91.3 % unpolar esters (w.r.t. total ester content) [4], were found in the crude RSO extracted October 1985. In the fully refined RSO the proportion of these esters was 95.7 %. These figures show, that in RSO from fresh kernels most of the fatty acids in the triglycerides are not oxidized. The fact that in the

- 63 -

fully refined oil the proportion of intact fatty acids is higher than in the crude oil, indicates, that the ox \_ised fatty acids are enriched in constituents of the crude oil, which are removed during refining (phospholipids, free fatty acids). The figures are well in accordance with the results known for other vegetable oils.

# III 3.2.1.4. Unsaponifiable matter

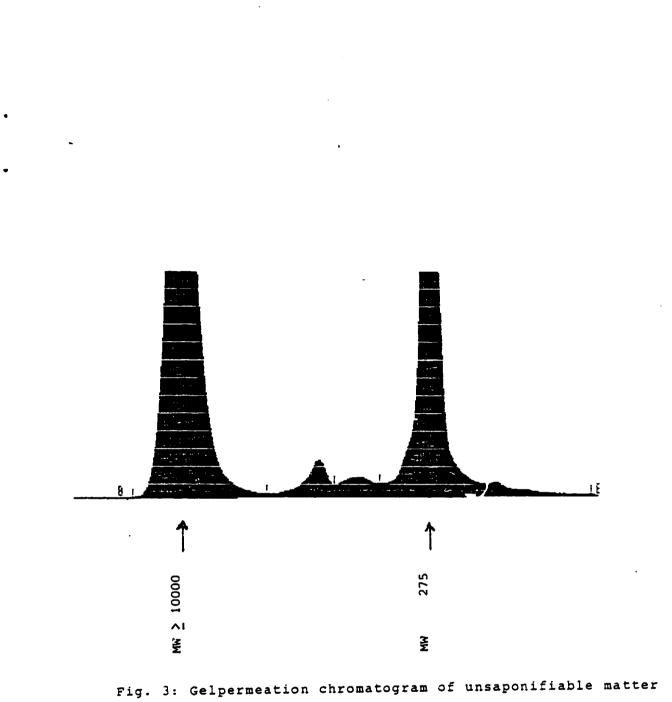
The amount of UM [5] in crude RSO was found between 1.1 % and 1.3 %. From the GPC analyses of this material about 57 % were determined as high molecular material, the remaining rest showed molecular weights around 300 D (see fig. 3). Thus the high molecular material is enriched in the UM.

In TLC two spots in the range of sterols were visible, which could not be identified satisfactorily, but by comparison with literature data are probably not one of the more common phytosterols like e.g. stigmasterol or sitosterol.

In refined RSO only between 0,3 - 0,4 % UM was found. In this UM only 20 % had a high molecular weight of > 10000 D. Since according to GPC the content of this polymer material shows a similarly high molecular weight in crude and refined oil, the considerable differences of the UM in both oils cannot be explained without further sophisticated investigations.

# III 3.2.2. Minor constituents of rubber seed oil

In view of a possible use of RSO for human consumption, it was interesting to look for minor components in this oil, which could influence this utilization. For instance the content of a natural antioxidant is of high importance for



of crude RSO

the taste keepability of such a highly unsaturated oil.

## III 3.2.2.1. Tocopherols

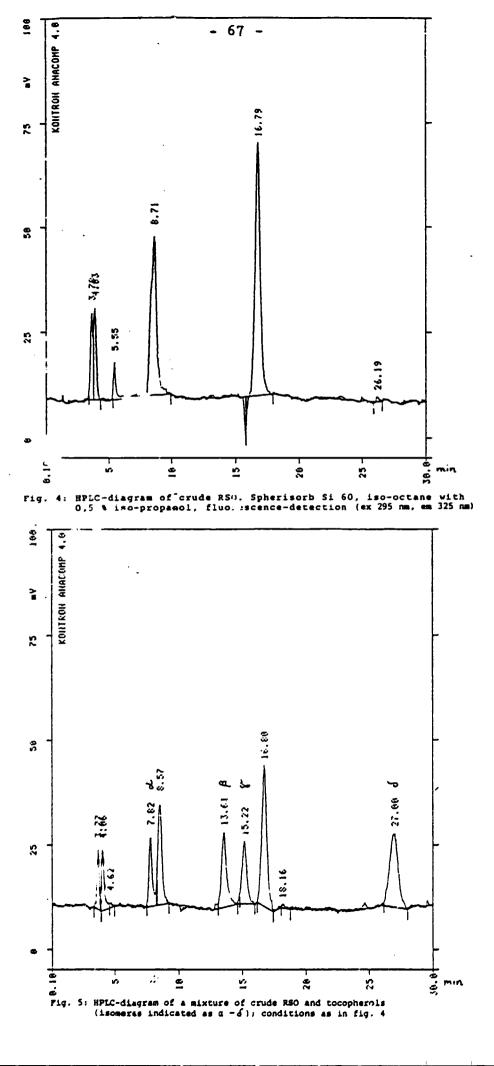
A HPLC-diagram of crude rubber seed oil (method see appendix 3, p. 3) is shown in fig. 4. By cochromatography of a mixture of tocopherols  $(\alpha - \delta)$  and rubber seed oil it was demonstrated, that rubber seed oil does not contain tocopherols (fig. 5). Two main signals in RSO with a 10 % larger retention time than the neighbouring  $\alpha$ - and  $\gamma$ -tocopherols were obtained. It is assumed, that these signals belong to tocotrienols. Tocotrienols and their esters are reported to be present in latex of Hevea brasiliensis [6,7,8].

## III 3.2.2.2. Polyisoprene

One of the most interesting minor component which was found in RSO during this investigation is the high molecular weight material, which was detected in the GPC-diagram (s. III 3.2.1.2, p. 64). It was present in the oil in amounts of ~ 1 \$. The assumption could be made, that this component does not contain oligomeric triglycerides or phospholipid micelles, since it is enriched in the unsaponifiable material of the oil.

To get some material for identification purposes the following procedure was applied:

- 1) Preparation of unsaponifiable material from crude RSO
- 2) Gelpermeation chromatography on preparative scale: 5 mg of the UM were separated on a polystyrene column, using tetrahydrofurane as eluent (s. appendix 3, p. 2). The first fraction was trapped and evaporated.



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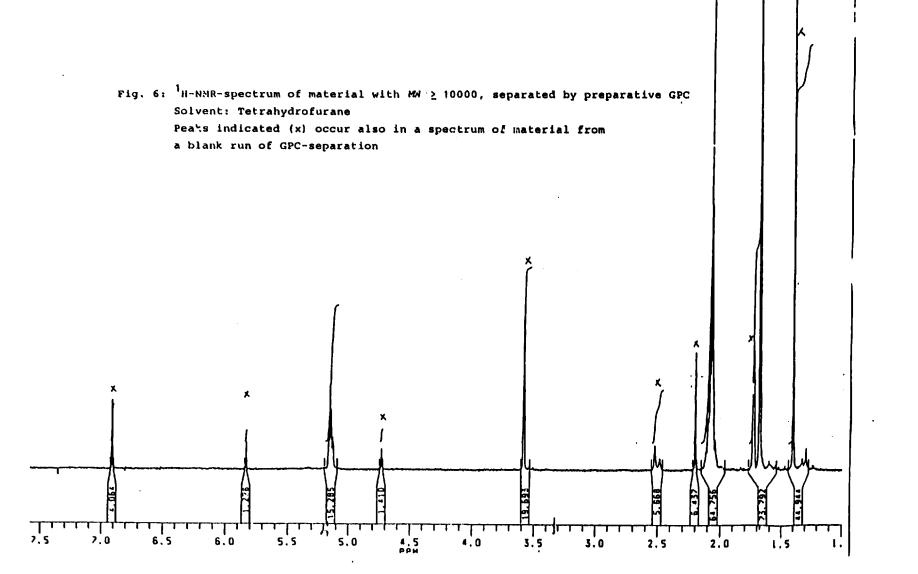
The <sup>1</sup>H-NMR-spectrum (400 MHz) of this material in deuterated THF is shown in fig. 6. The signals indicated by x appear also in a spectrum of the blank material. They derive from impurities in the THF, used for fractionation and from the solvent used for the NMR-spectrum. The remaining three signals of the polymer have the characteristical chemical shifts for CH-protons,  $CH_2$ -protons and  $CH_3$ -protons with the relative intensities of 1 : 4 : 3.

This pattern is characteristic for isoprene increments

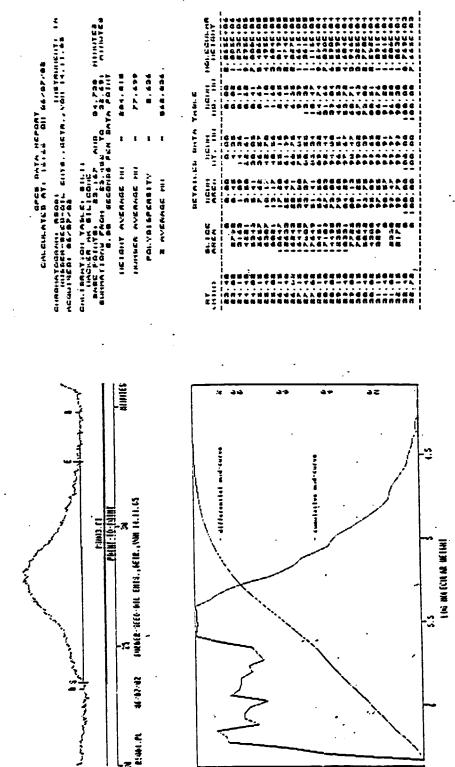
$$- CH_2 - CH = C - CH_2 - CH_$$

in trans- and cis-1,4-polyisoprene. Whether the configuration at the double bond is cis or trans could not be decided from the NMR-spectrum. Most probably it is cis, because Hevea brasiliensis produces cis-1,4-polyisoprene anyway in form of latex.

A further GPC-investigation was carried out, to get a more exact value for the molecular weight of this polyisoprene. Using a column set suitable for discriminating between much higher molecular weights than the set used for characterization of the RSO, molecular weights of several hundred thousand Daltons were found. The molecular weight distribution (volume-weight) is given in fig. 7. For polyisoprere in latex molecular weights of 200000 - 400000 D [9] or degrees of polymerisation of 8000 to 30000 [10] ~ 5,4  $\cdot$  10<sup>5</sup> to 2  $\cdot$  10<sup>6</sup>D are reported. So the molecular weights of the polyisoprene molecules in RSO are about the same as those in latex.



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Fig. 7: Molecular weight distribution of polylsoprene in RSO

-70 -

### 3.2.2.3. Phospholipids

The crude oil, obtained Oct. 1985, had 260 ppm phosphorous. Applying a commonly used converting factor of 25, this results in 0.65 % phospholipds in this oil. In a TLC of this crude oil the main phospholipid to be seen is phosphatidic acid.

The relative phospholipid composition was assessed in the sludge, obtained from this oil (1-dimensional TLC and phosphorus determination in the spots of the phospholipids [11], see appendix 3, p. 3).

Phospholipid composition relative to total phospholipids assessed:

phosphatidic acid (PA):	46 烯
phosphatidyl inositol (PI):	22 🖇
phosphatidyl choline (PC):	24 🖇
phosphatidyl ethanolamine (PE):	8 %

No other phospholipid of significance could be detected. These 4 phospholipids analysed in the sludge account only for 22 % of the total phospholipids, present in the crude oil. So the major part of the phospholi .ds remained in the "deslimed" oil and probably adds to the emulsion problems in the neutralization step. However, they are removed together with the soaps.

III 3.3. Quality assessment

III 3.3.1. Colour stability

The colour stability of RSO, exposed to air and daylight, was investigated (s. appendix 3, p. 4):

storage time (weeks)	iodine colour crude RSO ; refined RSO		
0	40+	3+	
1	40-	3-	
2 1/2	25	2	
5	20	turbid	
7	most material was polymerised the remaining oils were only slightly yellow coloured		

During storage under these conditions, the colour was reduced in both oils. This is a normal behaviour with oils containing carotenoids as the main colouring matter. Carotenoids are oxidised by lipid-hydroperoxides, formed in the first autoxidation step of unsaturated fatty acids. This is in contrast to the statement that soap, containing 5 - 10 % RSO, gets a darker colour during storage (s. II 2.5., p. 40).

### III 3.3.2. Taste and taste stability

Crude RSO as obtained after hexane extraction was a brownish clear somewhat sticky oil. A fresh sample with a relatively low acid value (6.4) had a mild pleasant nutty taste with only slightly soapy and bitter notes. The soapy and bitter taste was more pronounced in the sample with an acid value of 17.

The fully refined sample of RSO was almost colourless, the nutty flavour had disappeared, the taste was rather neutral.

III 3.3.2.1. Storage test with crude rubber seed oil

The acceptable taste of a fresh oil does not guarantee, that the taste will keep during longer storage. Especially the high proportion of linolenic acid in the triglycerides of RSO is vulnerable to the attack of oxygene, resulting in a bad taste. So it was of interest to see how long the taste of the oils will remain stable, and whether this can be influenced by an antioxidant.

Storage tests were done in half filled bottles under air and in darkness. To simulate the conditions in tropical countries storage temperature was  $30^{\circ}$ C. The taste was assessed by an experienced taste panel at intervals of 2 - 4 weeks. Main emphasis in the judgement was put on detecting taste deterioration. Taste intensity, as is often assessed, was not so important here, because the crude RSO started already at a relatively high level.

The results of the organoleptic judgements are compiled in Tab. 1. Crude BSO get a slightly seedy odor after 1 month which changed into a burnt note after 2 months. Taste deterioration became noticeable after 2 months. The soapy and bitter taste had increased, the oil now caused some irritation in the throat. A "burnt" taste was first noticed after 2  $\frac{1}{2}$  months are ecame stronger and stronger to the end of the test peri (p-6 months). At the end also a sour taste was perfered. Surprisingly no "varnish" taste was observed, as wid have been expected because of the similarity of the triglycerides to linseed oil.

The crude RSO was rendered acceptable under these test conditions roughly up to 2 months. Addition of 1000 ppm synthetic  $\alpha$ -tocopherol did not improve the taste stability of crude RSO, the kind and speed with which off-tastes developed were about the same as without tocopherol.

- 73 -

Tab. 1

### Organoleptic judgement of rubber seed oil

all oils stored at 30 °C in total darkness

storage time	crude RSO	refined RSO	Mixture of 80 % refi with	ned CN
[weeks]			20 % crude RSO	20 🗯 refined RSO
initial	slightly scapy, bitter [a]	tasteless [a]	nutty, bitter [a]	tasteless [a]
2	slightly seedy [a]	slightly ranzid [a]	nutty, bitter [a]	tasteless [a]
4	slightly seedy [a]	slightly ranzid [a]	nutty, bitter [a]	tasteless [a]
8	slightly seedy [a]	slightly ranzid [a]	nutty, bitter [a]	tasteless [a]
10	slightly seedy little "burnt" [a]	slightly ranzid [a]	nutty, bitter [a]	tasteless [a]
15	" " stronger "burnt" [a]	faint taste of cod liver [a]	slightly soapy [a]	slightly ranzid [a]
20	throat irritating "burnt" taste [na]	faint taste of cod liver [a]	slightly throat irritating [a]	slightly ranzid [a]
25	strong sourish [na]	faint taste of cod liver [a]	slightly throat irritating [a]	<pre>slightly ranzid [a] + slightly sourish [a]</pre>

- 74 -

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[a] = acceptable taste

[na] = non acceptable taste

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III 3.3.2.2. Storage test with refined rubber seed oil The refined RSO started with almost no taste. After 12 days a very slight rancid smell occurred, which probably derived only from the thin oil layer at the ground stopper. It did not increase on further storage and was not noticed in the taste. The latter became slightly seedy after 1 month and did not change much until after 3 ½ months a faint taste of cod liver oil occurred. But up to the end of the test period (5 months) the taste of the refined RSO was still acceptable.

When 1000 ppm a-tocopherol was added to refined RSO, this oily and seedy taste was not observed. After almost 2 months a musty taste was firstly perceived, which only slightly increased until the end of the test period (5 months). So in this case the antioxidant had a positive effect; with crude RSO this effect probably is overuled by the more intensive basic taste of the oil itself

## III 3.3.2.3. Storage testy of a mixture of rubber seed oil/ coconut oil

In a third test row the taste stability of a mixture of 20 % crude RSO and 80 % refined coconut oil was checked. Under the same test conditions as mentioned above, the taste of the mixture (which was nutty at the beginning) got slightly soapy and irritating to the throat after 3  $\frac{1}{2}$  months. After 5 months a slightly "burnt" taste was perceived in addition, but the mixture still was acceptable.

The mixture with 20 % refined RSO was quite neutral in taste at the beginning. A very slight rancid odour after  $3\frac{1}{2}$ months did hardly increase until 5 months. At the end a slightly sourish note was perceived in addition. Some problems occured during refining of RSO, particularly in the bleaching step when bleaching earth has to be filtered off. It took more than 20 hours to filter off = 1 kg RSO and severe losses of oil were observed, even at temperatures around  $70^{\circ}$ C and with a high rate of changing the filters.

To illustrate the problem, the filtration speed of RSO was compared with that of soybean oil:

2 ml oil of each kind were filtered through a Büchner funnel (diameter 1 cm) equipped with a paper filter ("Schwarzband", Schleicher u. Schüll). Then vacuum was applied and the time assessed, necessary for the oil to run through. Whereas the soybean oil passed the filter within 5 sec the RSO (neutralized, dried, clear oil) took 6-10 min.

### III 4.1. Viscosity

In principle the slow filtration of RSO could be caused by a high viscosity. In comparison with soybean oil the RSO seems to be somewhat more sticky.

Measurement of the viscosities with a Rotovisko-apparatus resulted in the following viscosity figures:

	Viscosities 25 <sup>0</sup> C	(in mPa's) at 1 80°C	:
RSO	78.2	12.2	
soybean oil	42.2	9.0	

The viscosity differences would merely explain a factor 2-3 in filtration speed at ambient temperature. At higher temperatures hardly any difference in the viscosity was recognised. Therefore other reasons must be responsible for slow filtering rates in refining experiments, which are carried out at temperatures of 70 - 100°C

### III 4.2. Filtration trials

In the following experiments the influence of RSO on the filter material was investigated. Using a glass filter (Glasfritte D 4, maximum of pore diameter 16  $\mu$ m) soybean and RSO re-filtered in the sequence as given below:

1) soybean oil 4 ml: 1 min filtration time 2) . 4 ml: 1 3) 2 ml: 1/2 -4) RSO 2 ml: 1 1/5 " 2 ml; 1 <sup>1</sup>/<sub>2</sub> " \*) 5) 11 -6) Ħ 4 ml: 9 Ħ 7) soybean oil 2 ml: 5 8) filter washed with acetone 9) soybean oil 2 ml: 3 min **11** -

This experiment shows the following:

- 1. The filtering rate of RSO is at least 3fold at the beginning of the process.
- 2. The filtering time increased also for soybean oil, after RSO had passed the filter.
- 3. If the RSO is prefiltered (No. 5), the filter properties obviously are not changed by this oil.

<sup>\*)</sup> The oil in this experiment had been filtered through a glass filter before

4. The material that clogs the filter, cannot be washed out by acetone.

From these results it is concluded, that the filter picks up some material from the RSO, which partly blocks the pores and cannot be removed by polar solvents.

Another glassfilter D 4 (14  $\mu$ m Ø) was completely blocked for soybean oil and even acetone, after filtration of 4 ml RSO.

Instead of paper also glass fiber sheets of different porosity were tested (samples delivered by Lehmann & Voss & Co., Hamburg)

1. AFS -  $3\frac{1}{4}$ , dustfilter, big pores 2. Lydair grade 251, medium density 3. " 220, highest density

	filter times for 2 ml oil with filter type			
oil	1 1	2	3	
soybean oil	3 sec	3 sec	11 sec	
crude RSO	8 sec	9 sec	1 <sup>1</sup> / <sub>2</sub> min	

On addition of bleaching earth Tonsil ACCFF only filters 2 and 3 retained the bleaching earth. The filter times, however, increased to several minutes, because now the filter cake blocked the filtration.

# III 4.3. Separation of polyisoprene

Because of the insufficient results of the filtration experiments with different filter types further trials were carried out to remove polyisoprene, using a technique which

- 78 -

is based on an adsorption chromatography column [12].

Triglycerides and more polar constituents are adsorbed to silica gel from hexane solution. More unpolar molecules like carbohydrons (or very large molecules or micelles which do not fit into the pores of the SiO<sub>2</sub>) are washed out.

Blution scheme:

500 g	SiO <sub>2</sub> (Merck, activated at 160 <sup>0</sup> C, 12h)
in he	Xane
d2 g crude RSO in 400 ml hexane	1) 6 1 hexane, 0.5 g liquid, MW < 380
82 g crude RSO	2) 1.5 l hexane, 1.5 g brownish wax, 50 % phospholipids
	3) 4 l hexane, 19 g triglyceride
	4) 8.5 1 hexane : ether = 87 : 13, 137 g triglycerides + fatty acids
	5) 3.5 1 ether, 7 g fatty acids, diglycerides

By this procedure the polyisoprene content of the RSO (fraction 4) has been reduced from 1.1 % to 0.4 %. The polyisoprene is concentrated in fraction 2 (although this contains also phospholipids,  $P = 2.0 \% \approx 50 \%$  phospholipids). This oil (fraction 4) was filtered over glass fiber filter (see below) in corparison to the starting oil:

	filtering t	ime (2 ml oil)
oil	grade 251	grade 220
crude RSO	9 sec	1 1/2 min
Si02-treated RSO	6 sec	5 min
-		

In case of the denser filter even longer filter times with the purified oil were obtained.

Some further experiments were carried out in order to reduce the filtration time of RSO: By treatment of the oil with different adsorbents in order to adsorb the polyisoprene particles ( -5 %, 10 min at  $50^{\circ}$ C). The following adsorbents were vsed:

> Charcoal of different particle size Kieselgel (Merck 7729, <0,08 mm) Celite (filter aid) Polyethylene (BASF, Lupolen 5270 Z) Rubber (powdered tube)

None of them, when the treated RSO was filtered through paper (Schwarzband), gave a better filtration rate.

III 4.4. Dilution trials

III 4.4.1. Hexane as solvent

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Small amounts of hexane reduce the viscosity very much and at the same time may dissolve some of the polyisoprene.

filtering times of crude RSO containing 0   5   10   20   30   50 % herane					
6-10 min	2-3 min	1 <sup>1</sup> / <sub>2</sub> 2 min	1 1/2 min	1/2 min	10 sec

(2 ml oil, Schwarzband)

So relatively small amounts of hexane seems to improve the filtration rate.

The same filtration times as with 30-50 % hexane could be obtained with crude RSO at  $70-90^{\circ}C$  (30-20 sec), but it was found that the high starting rate will soon be reduced because of blocking of the filter.

III 4.4.2. Oil as solvent

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As a more appropriate solvent vegetable oils in mixtures of RSO were investigated. With mixtures of crude RSO and soybean oil = 1 : 1 no better filtration rates were obtained.

A mixture of 20 % crude RSO and 80 % coconut oil, however, showed the same filtratiion speed as coconut oil (at 50 - $55^{\circ}$ C). Therefore, with 1 kg of a mixture of 80 % refined coconut oil and 20 % crude RSO a refining experiment was carried out on a somewnat larger scale.

The oil mixture was:

- 1) neutralized. Some emulsion problems were noticeable,
- 2) bleached with 1 % Tonsil ACCFF. After addition of filter aid Seitz Kristall Theorit the fat mixture filtered in quite a normal manner.

It remains to be checked on a pilot plan scale, whether is a practical , way to overcome the filter problems wi RSO.

#### III 5. Composition of Rubber seed Meal

The RSMs of the three extractions (see III 3.1, page 54) were stored at  $-20^{\circ}$ C prior to analysis. After drying at  $120^{\circ}$ C until constant weight, a water content of 8,8, 9,2 and 9.1 % was found for three extracted samples.

### III 5.1. Residual oil content

The rubber seed meal of the first extraction was subjected to a further two hour extraction with diethylether. By this extraction an amount of 6,2 % soluble material was obtained.

A GPC-analysis of the ether extract showed that the composition of this residual oil is rather similar to the extracted crude RSO obtained as described on page 60.

constituent	area 🖇
triglycerides	89.4
diglycerides	1.5
monoglycerides .	0.3
fatty acids	4.9
dimeric triglycerides	1.3
trimeric "	1.0
MW > 10000	0.6

III 5.2. Water soluble materials

From the ether extracted meal the following results were obtained after further extraction with water:

Water soluble material:33.5 % (w.r.t. RSM)Ash in"6.5 \%Mater soluble protein :7.1 %Clulated from nitrogen content (Kjeldahl)(F = 6.25)water soluble carbohy tratesare calculated from these figures33.5 % - (6.5 % + 7.1 %)= 19.9 \%

The water soluble carbohydrates [13] were analysed by TLC. 2 spots (s. fig. 8) were seen, indicating a mixture of a disaccharide and a monosaccharide. Higher carbohydrates e. g. trisaccharides or tetrasaccharides could not be detected.

The total raw protein was calculated from the total nitrogen content determined by the Kjeldahl method using the convertion factor 6,25 %. A total raw in content of 30 % was determined in the three meal sam, ...

In the following table the main components of the investigated RSM is compared to the average values found in literature.

constituent	results found		
	own investig.	lit.	
	<del>%</del>	%	
H <sub>2</sub> 0	9.1	6	
lipid	6.2	11	
sol.carbohydr.	19.9	40	
total protein	30.0	29	
ash	6.5	5	
fibre	8.0	7	
Σ	<79,4 %	100 \$	

Only in the soluble carbohydrates our results differed from the literature values. By microscopical inspection of the RSM, besides of cell fragments, a lot of almost spheric\_1 particles (diameter ~ 5-10  $\mu$ m) were found. Their colour darkened on addition of diluted iodine solution. This confirms the assumption, that these particles consist of starch, which is a water insoluble carbohydrate and therefore has not been assessed together with the soluble carbohydrates. Its amount was determined in the range of 15 - 20 \$.

- 83 -

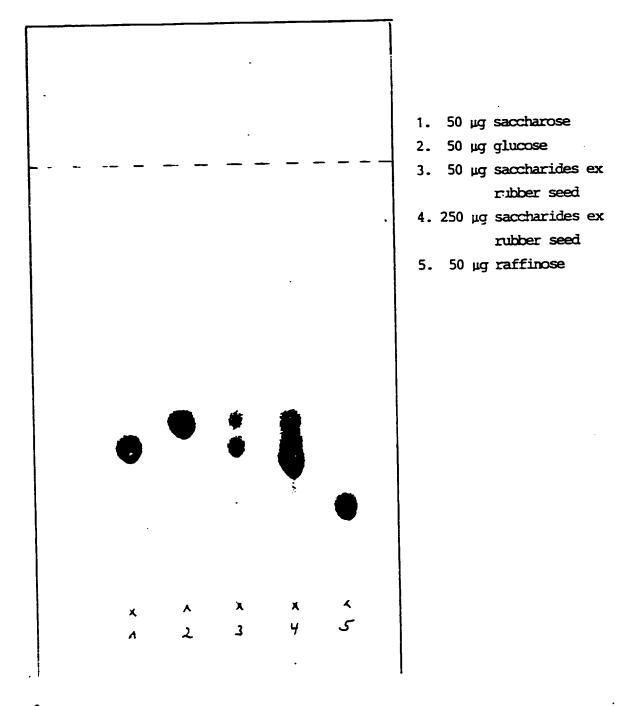


Fig. 8: TLC of rubberseed carbohydrates Silica gel, n-butanol : formic acid :  $H_2 0 = 33$  : 50 : 1 diphenylamin/anilin/phospnoric acid Starch is a normal constituent of for y seeds. It is quite astonishing that in analyses of rubber seed or RSM, reported in the literature, starch never has been mentioned. Presumably in those materials the starch had been converted already into soluble carbohydrates by enzymes. The material investigated was from the beginning of the seed fall period, has been collected immediately and was stored cold. Thus the starch cleaving enzymes may not have had much chance for attack. It should, however, be mentioned that starch could be seen in the seeds even after 5 months at room temperature.

#### III 5.3. Hydrogen cyanide

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The content of hydrogen cyanide in the RSM obtained by hexane extraction of freshly crushed kernels was assessed after 3 months storage of the RSM at  $-20^{\circ}$ C. To liberate the HCN from its glycosidic molety, the RSM was acidified and the HCN was steam-destilled and assessed via colour formation with picric acid [14].

The amount of 140 mg HCN/kg was remarkably low for a material whic<sup>+</sup> had been stored so carefully. But still this content was about 2-3 times higher than reported for RSM stored at normal conditions. Therefore the assessment was repeated with a RSM sample kept for 6 months at room temperature (darkness). An amount of 95 mg HCN/kg was found which shows, that the HCN-content can be reduced by a simple storage procedure. A much lower HCN-content of 20 mg HCN/kg was obtained after heating the RSM with Hydrochlorid acid and steam for 10 min. at 100 °C.

# III 5.4. Aflatoxins

Aflatoxins are formed by certain mould varieties (e.g. Aspergillas flavus, Aspergillus niger) which grow on fat containing seeds in warm climates.

In preparing the kernels for production of oil and meal 10 % dark seeds, which could possibly contain mould, were selected out beforehand. In two batches of the selected material the aflatoxin content were determined [15].

		Selected batch		
		Nr. 1	Nr. 2	
aflatorin	B <sub>1</sub> :	1.85 mg/kg	1.70 mg/kg	
n	B <sub>2</sub> :	0.10 "	0.03 mg/kg	
W	G <sub>1</sub> :	4.25 "	7.10 mg/kg	
π	G <sub>2</sub> :	0.16 "	0.35 mg/kg	
Σ	:	6.36 mg/kg	9.18 mg/kg	

Calculated on the total amount of kernels the amount of aflatoxins is at least 0.65 mg/kg and might go up to 1 mg/kg in the total meal if no selection of the moulded kernels is provided. The aflatoxin content of those kernels which were free of moulded material by manual selection showed sufficiently low figures given below:

aflatorin	<sup>B</sup> 1		0,002	mg/kg
aflatorin	<sup>B</sup> 2	۲	0,001	mg/kg
aflatoxin	G <sub>1</sub>		0,002	mg/kg
aflatorin	G <sub>2</sub>	\$	0,001	mg/kg

- 86 -

### III 6. Discussion

In this chapter several important aspects with regard to the composition and the possible utilization of rubber seed is discussed in view of the laboratory work.

## III 6.1. Preliminary remarks

It was already known from the literature and was revealed during the field study that the quality of the oil and the meal would be strongly dependent on the freshness of the seeds. Because of the circumstances that compelled us to carry out the laboratory trials within the time schedule of the project and to meet the above mentioned requirements the whole rubber seed used in this laboratory work was collected in the beginning of the seed fall and, as a consequence, may not be a representative product in all aspects. Consequences may be seen with respect to the content of starch, phosphatidic acid and lipase in the seeds. Therefore slight differences in the behaviour of the oil and the meal during the technical production from this seed compared to materials from later seed fall might be possible. But this will not change any of the main statements in the following liscussion.

# III 6.2. Influence of drying and storing on the oil yield

Although the seeds used for the laboratory trials were dried down to a water content of less than 5 % it was found as mentioned in chapter I.3.1 that there was a significant lipase activity which leads to a fat splitting even when the seeds were stored at 0°C. In the literature [I, 18a] it has been reported that kernels with 3-4 %  $H_20$  could be stored for 24 weeks at 30-37°C without substantial increase in free fatty acid content of the oil. According to another paper [I, 3] less than 5 % H<sub>2</sub>0 in whole nuts should be present, to prevent ensymatic attack. Obviously in this investigation it was ascertained, that the hydrolysis was not stopped by low temperature at this water content. Probably it is also important, whether in the predrying step of the nuts such a high temperature is reached, that the lipolytic ensyme is killed. This means that drying conditions with temperatures > 80°C have to be applied in the drying equipment irrespectively whether this is done by solar heated air or in a fire heated drying oven.

As a possible consequence of the enzymatic fat splitting the oil yield in the extraction process is reduced significantly. On a period of four months the oil yield was diminished from 32 to 25 % while the acid value were going up from 6 to 17. A similar observation, however, on a much lower level of acid values has been made by the Rubber Research Institute of Malaysia (private communication of Mr. Nadarajah). The figures obtained in that unpublished study were as follows:

Property	Period of storage (months) 0   2   4   6   8   10					
% moisture	3.16	2.78	4.07	4.21	3.86	5.07
% oll yield	39.5	39.4	40.0	37.2	31.7	29.3
% free fatty acids in the oil	0.65	0.98	1.12	1.14	1.40	1.86

A similar behaviour is not reported for other oil seeds like linseed and rapeseed, apart from the always occurring small oil yield losses during long storage.

### III 6.3. Composition of RSO

The composition the extracted RSO investigated in this study did not show much differences for the triglyceride and fatty acid content in comparison to other highly unsaturated vegetable bils. This is in accordance with the literature. Fairly new results which have not been reported in previous papers were obtained by the analysis of the unsaponifiable matter and the minor constituent. The most surprising result was obtained in the GPC analysis of the oil. The crude RSO contains about 1 % of a polyisoprene material with a molecular weight of several hundred thousand Daltons. Because of the very good oil solubility of such materials this component could only be reduced partly in a refined procedure. Several attempts failed to remove this polymere material from the oil by applying different absorption materials. The technological problem caused by this material is discussed later (s. III 6.5, p. 92).

As a refined and even a crude RSO has an acceptable taste and does not contain high levels of harmful components the oil may be used for human consumption. In this case the toxicological aspect of the existing polyisoprene in the oil is of importance. The polyisoprene as a very inert material lacking any functional groups may be seen without hesitation with respect to the toxicity. The influence of such a material on the human body, however, if applied over a long period of time cannot be predicted as absolutely safe. Most likely the polyisoprene will pass the intestines without any resorption or metabolisation. Polymeric olefines for instance with a molecular weight of 800 thousand Dalton in a 90 days toxicity test with rats did not show any harmful effects [16, 17].

However, to run no risk more long term toxicological data should precede the marketing of RSO for human consumption. Long term toxicity studies are very expensive. The cost for a long term study with two species will be in the order of several thousand Dollars. In view of these immense costs it should be pointed out clearly that such a study could be carried out only if a serious attempt is made to marketing RSO as an edible oil.

- 89 -

## III 6.4. Composition of rubber seed meal

As the protein and carbohydrate content of the rubber seed meel is of really good nutrional value for the use in animal feeds in this study emphasis was laid on the minor components which could cause toxic effects on the animals as described in several papers. As the gossypol content of the rubber seed meal was found to be equal or lower in comparison to linseed or soya meal only the hydrogen cyanide or a possible mould toxin content may have adverse effects in using RSM as animal feed.

The content of hydrogen cyanide in the form of a glycoside will be quite high in the seeds direct after seed fall. 140 mg/kg was found in the meal when they arrived at the laboratory after drying. In the literature contents of 2000 mg/kg is reported. Encymatically splitting of the glycoside in the presence of water during storage reduces the hydrogen cyanide content rather quickly. Under the same condition the lipase activity will split the triglycerides, and therefore cause bad yield of a low quality oil. If the pre-dried seeds with a low water content are stored, encymatic splitting fails and therefore the hydrogen cyanide release may be somewhat lower. But even in this case hydrogen cyanide content may come down to 10 mg/kg in the meal during the storage or will be lowered to a value of 1 mg/kg by a short steam treatment.

The lethal dosis of hydrogen cyanide for pigs is reported to be the same as for men (1 mg HCN/kg body weight). Assuming that 1/10 of the lethal dosis will not do any harm to the animal then a fifty kg animal may take up not more than 5 mg HCN with one meal. If the HCN content of the RSM contains 10 mg HCN/kg, not more than half a kg RSM could be consumed

- 90 -

by the pig per feeding. This calculation shows that the HCMcontent could be a limiting factor in the utilization of RSM as feeding stuff, if the storage of the seeds and the meal is not optimized. Optimization of this process has to be done on pilot plant scale.

A much more limiting factor for the usage of RSM as feeding stuff comes from mould toxins, especially aflatoxin. In chapter III, 5.4, p. 86 the results for the aflatoxin contents of the comparable freshly collected and dried seeds used in the study demonstrate the uneasy situation of the RSM. A limiting maximum content of 50  $\mu$ g/kg aflatoxin in animal feeding stuffs is recommended by WHO and introduced in most countries over the world. Amounts of about 1 mg aflatoxin per kg foodstuffs as determined in this study are very dangerous to young animals especially calfs and have been shown to cause death i animal husbandry. Because any treatment of the seeds or the meal to remove aflatoxin content is too expensive (most suitavie method is ammonia treatment at 120 °C of several minutes), the only possibility to avoid these problems of animal feeding is the manual selection of the moulded mostly dark appearing ker-. nels.

Another way to minimize the problems with HCN and aflatoxins will be the limitation of RSM to 25 % in the total feeding stuff. This is in accordance with what has already been reported in the literature.

- 91 -

# III 6.5. Technological aspects

While with the exception of the optimizing procedure mentioned in III 6.4, p. 90 no problems occur with the technical preparation of rubber seed meal, some difficulties in the processing of the RSO particularly the production of a high quality oil have been revealed in this study.

In chapter III, 3.2.2.3 a relatively high phosphor lipid content with a high amount of phosphatidic acid was determined in a crude RSO. The latter cannot easily be removed from the oil by the desliming step, and therefore may cause problems by emulsification of the oil containing high amounts of FFA during the refining step. The only possibilities to remove the phosphatidic acid drastically would be an adsorption column cleaning or ultrafiltration of the oil. Both processes would be far too expensive for processing refined RSO. Therefore the best way to avoid this problem in the neutralization step as mentioned in chapter 3.1, is quickly drying of the fresh collected seeds at temperatures of 80°C to kill the lipolytic enzymes.

A further problem in the raffination of RSO is a low filtering rate, obviously caused by the content of polyisoprenes which are clogging the filter. On page 80 uselessness of filter aids is described. Solvent solution of the oil may be a suitable method, but because the solv.nt has to be removed after filtration by an evaporation process this is an expensive process. A more practical attempt to overcome the filtering problem would be the mixing of RSO with other vegetable oils before the raffination. The feasibility of this procedure has to be proved on pilot plant scale experiments.

As a consequence of the above outlined difficulties in the raffination of RSO careful considerations are required for a set up of pilot plant trials in order to develop a RSO processing with the aim to obtain a high quality oil on a low cost level.

#### III 7. Summary

Hubber seeds grown 1985, freshly collected and dried is an air oven at  $70-80^{\circ}$ C in Sri Lanka, were investigated in the NATEC laboratory (Hamburg) with regard to the composition and technical aspects.

After manual decortification the oil was extracted from the crushed seed with petroleum ether. The acid value in the crude oil increased during storage of the predried seeds  $(H_20 \text{ in kernels } 7,6 \text{ })$  at  $0^{\circ}$ C for several months because of lipase activity. The crude oil was refined via a standard laboratory method including desliming, neutralization, water glass-treatment, bleaching and deodorization.

The oil composition was comparable to other unsaturated vegetable oils with regard to the fatty and the oxidized and dimerisized triglycerides or  $p^{-1}$  and diglycerides. Gel permeation chromatograph 2C) indicated a high molecular material (~ 1 % of the  $r^{-1}$ ) which was separated by preparative GPC and identified as 1,4rolyisoprene by <sup>1</sup>H-NMR. The molecular weight of this material was about 500 000 D which is comparable to that of polyisoprene in latex.

Tocopherols a natural antioxidants were absent in the oil. HPLC analysis of the oil revealed the existence of tocotrienols which have also been found in latex. Phospholipids in the oil were mainly phosphatidic acid, in lesser amounts also phosphatidyl-choline, -inositol and -ethanolamine.

The crude oil had a brown-yellow colour (iodine colour 40) and a pleasant nutty taste. It could be refined into an slightly yellow (iodine colour 3) oil which was almost tasteless. The colours of both oils were reduced by storage at daylight under air. In view of the linolenic acid content of 18 % the taste stability of the crude and refined RSO were quite acceptable for several months. Additional tocopherols gave a somewhat increasing stability. 20 % crude or refined rubber seed oil in coconut oil were acceptable w. r. t. taste up to 5 months.

Technically filtration of rubber seed oil is a somewhat difficult problem. Obviously the polyisoprene clogs the filter. It was not possible, to remove this polymer by adsorbents or to overcome the difficulties by using other filter material or filtering aids. Addition of 50 % hexane improved the filtration considerably. Also mixtures of 20 % rubber seed oil and 80 % coconut oil were filtered in quite a normal manner, but it has to be checked in pilot plant trials, whether this holds also in technical scale.

In rubber seed meal some 15 - 20 % starch were detected, which has not been reported in other papers before. The water soluble carbohydrates consist only of mono- und disaccharides, no tri- or tetrasaccharides, which may cause digestion problems, were detected.

The content of toxic hydrogen cyanide of 95 - 140 mg/kg meal was in the known range. In the moulded and rotten part of the kernels, which has been separated before processing, an alarmingly high amount of aflatoxins has been found. Recalculated on the total amount of kernels the aflatoxin content was at least 0,65 mg/kg.

The results of the laboratory investigations are discussed in view of the technical and economical aspects of the utilization of rubber seed, and the key points are lined out which have to be taken into consideration the the set up of pilot plant trials the further progress of this project.

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### Recommendations for pilot plant trials

In view of the already available experiences in the utilisation of rubberseeds and taking into account the problems outlined in the study for the production of RSO of high quality and RSM to be used as animal feeding stuff the following route for the set up of pilot plant trials for the oil and meal production is recommended:

- Collection of seeds to be done by people at the states (children and dependants) organized by the superintendents or their estates managers.
- 2) Drying of the seeds is to be done on the estates in the smoke-houses or by solar energy equipments. The latter has to be built at the estates.
- 3) Decortication of the seed is to be done on the estates on a rubber-mill or on a groundnut decorticator. The latter has to be installed, selection of kernels from the hulls is done manually.
- 4) Milling of the kernels in a chakku mill together with molassis or in an electrical groundmill. Both milling systems have to be installed at the estates. Organisation of this work to be done by the estates superintendents and estate managers.
- 5) Trensport of the raw oil and cake to the cil and feed consuming companies.

6) Refining of the oil should be done in small batches of about 500 kg, the cake should be mixed with other materials to obtain finished animal feed products and stored for several weeks before given to the animals.

As there is a relatively high demand of cheap oil in the paint industry for the preparation of alkyd resins the oil should be shipped from the estates directly to the paint factory. The oil may be used in a refined or unrefined state for the preparation of the finished products.

In this route the low transport costs, the relatively low costs for the investment of the simple machinery for decortication and milling leads to a process which is based on a very profitable system. From the economical point of view it may be worthwhile to do the seed collection, drying, decortication and milling at one estate in an area of several estates so that the machinery equipments have to be installed only at one place.

Interest for this model was mentioned by the general estate manager of the Sri Lanka States Corporation 111. By this model on the one hand with a fairly simple technology a comparable high priced raw material could be produced in a not industrial area. On the other hand only products of improved quality not containing waste-weight materials like moisture or shells have to be transported to the refineries and factories in the industrial area where more sophisticated technologies for the preparation of final products have to be applied.

- 98 -

### Appendix 1

### Complete References of the Literature Survey with regard to Rubberseed

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This literature retrieval contains citations on

#### RUBBER/SEED OR HEVEA

and

NUTRITION OR FOOD OR FEED OR EDIBLE ( Part 1 ) and NOT (NUTRITION OR FOOD OR FEED OR EDIBLE) ( Part 2 )

Taken into consideration are records retrieved under these key words from the databases

311:Chemical Abstracts Search - 1982-1985
310:Chemical Abstracts Search - 1980-1981
320:Chemical Abstracts Search - 1977-1979
309:Chemical Abstracts Search - 1972-1976
308:Chemical Abstracts Search - 1967-1971
51:FSTA ( FOOD SCIENCE & TECHNOLOGY ABSTRACTS ) - 1969-1985

Sequence of records is chronological, latest records named first. Owing to retrieval in different databases double entries may occur.

Record # 1

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Ord.no. : 311:02077786 CA-No. : 102(9)77786t Source : Journal *Titel :* Plant tissues as indicators of soil nutrient availability for Hevea: glasshouse evaluations Author : Yew, F. K.; Pushparajah, E. Location: Malay. Journal : J. Rubber Res. Inst. Malays. Date : 1984 ,32(3 )171-81 Coden JRRIAN ISSN : 0035-953X Language: English Record # 2 Ord.no. : 311:01089481 CA-No. : 101(11)89481g Source : Journal reliminary study on levels of rubber seed meal for broiler rations Titel Author : Sripongpun, S.; Pralomkarn, W.; Chandumpai, A. Location: Fac. Sci., Prince Songkla Univ., Thailand Journal : Warasan Songkhla Nakkharin : 1983 ,5 (2)131-5 Date Coden ; WSNAEV Language: Thai Record # 3 Ord.no. : 311:01071537 CA-No. : 101(9)71537v Source : Journal Titel : Evaluation of some chemical and nutritional characteristics of rubber tree seed (Hevea brasiliensis) *Author :* Selle, Celia Margarita; Gonzalez de Mejia, Elvira; Elias, Luiz G.; Bressani, Ricardo Location: Univ. Valle Guatemala, Guatemala, Guatemala Jeurnal : Arch. Latinoam. Nutr. Date *2* 1983 ,33 (4 )884-901 Coden : ALANEH ISSN : 0004-0622 Language: Spanish

Record # 4 Ord.no. : 311:01005766 CA-No. : 101(1)5766t Source : Journal Titel Chemical composition and nutritional value of para-rubber seed and its products for chickens Author : Narahari, D.; Kothandaraman, P. Location: Dep. Poultry Sci., Madras Vet. Coll., Madras, 600007, India Journal : Anim. Feed Sci. Technol. Date **: 1984 ,10 (4)257-67** Coden : AFSTDH ISSN : 0377-8401 Language: English Record # 5 Ord.no. : 311:00066745 CA-No. : 100(9)66745m Source : Journal Titel The influence of processing and storage on hydrogen cyanide and tannin contents of para-rubber seed and its products Author : Narahari, D.; Kothandaraman, P. Location: Dep. Poult. Sci., Madras Vet. Coll., Madras, 600007, India Journal : Anim. Feed Sci. Technol. Date : 1983 ,9 (4)319-23 Coden # AFSTDH ISSN : 0377-8401 Language: English Record # 6 Ord.no. : 311:00033693 CA-No. : 100(5)33693q Source : Journal Titel : Study on the zinc status in rubber growing soils and its effects on rubber trees in China Author : Wang, Guohong Location: Rubber Cultiv. Res. Inst., Acad. Trop. Crops South China, Peop. Rep. China Journal : Turang Xuebao Date : 1983 ,20 (3 )313-21 : TJHPAE Coden ISSN : 0564-3929 Language: Chinese Record # 7 Ord.no. : 311:00021985 CA-No. : 100(3)21985y Source : Konferenz-Bericht Titel : Legume cover crops as a source of nitrogen in plantation crops in the tropics Author : Pushparajah, E. Location: Rubber Res. Inst. Malaysia, Kuala Lumpur, Malay. Journal : Trans. Int. Congr. Soil Sci., 12th Date *i* 1982 ,2,)189-97 Coden : SOPPAH Language: English Publish : Ind. Soc. Soil Sci., New Delhi, India

Record # 8 Ord.no. : 311:00004937 CA-No. : 100(1)4937s Source : Journal : The saponin content of some Nigerian oil seeds Titel Author : Achinewhu, S. C. Location: Dep. Food Sci. Technol., Rivers State Univ. Sci. Technol., Port Harcourt, Nigeria Journal : Qual. Plant. - Plant Foods Hum. Nutr. Date : 1983 ,33(1)3-9 Coden : QLPLAN ISSN : 0377-3205 Language: English Record # 9 Ord.no. : 311:99157269 CA-No. : 99(19)157269m Source : Konferenz-Bericht : Nitrogen cycle in rubber (Hevea) cultivation Titel Autnor : Pushparajah, E. Location: Soils Crop Manage. Div., Rubber Res. Inst. Malaysia, Kuala Lumpur, 16-03, Malay. Journal : Nitrogen Cycling South-East Asian Wet Monsoonal Ecosyst., Proc. Reg. Workshop Editor : Wetselaar, Robbert (Ed)^ Simpson, Jeffrey R. (Ed)<sup>^</sup> Rosswall, Thomas (Ed) Date : 1981 )101-8 Coden : 500SAY Language: English ; 790000 Date Publish : Aust. Acad. Sci., Canberra, Australia Record # 10 Ord.no. : 311:99052404 CA-No. : 99(7)52404y Source : Journal Titel : Evaluation of the suitability of the methods for assessment of nutrients of Datmara soils with respect to rubber plant Author : Anam, K.; Didar-Ul-Alam; Rahman, Shafiqur; Huq, S. M. Inamul Location: Dep. Soil Sci., Univ. Dhaka, Dhaka, Bangladesh Journal : Dhaka Univ. Stud., Part & : 1982 ,30 (2 )181-9 . Date Coden # DUBSDX Language: English Record # 11 Ord.no. : 311:99004337 CA-No. : 99(1)4337g Source : Journal Frelative efficacy of some antifeedants and deterrents against insect Titel pests of stored rice Author : Devi, D. Ambika; Mohandas, N. Location: Div. Entomol., Coll. Agric., Trivandrum, 695 522, India Journal : Entomon Date // 1982 .7 (3 )261-4 / ENTODS Coden ISSN : 0377-9335 Language: English

Record # 12 Ord.no. : 311:98159194 CA-No. : 98(19)159194a Source : Journal : Finding of .alpha.-, .beta.- and .gamma.-dehydrotocopherol in wheat germ Titel oil by HPLC and GC/MS - a contribution to tocopherol analysis Author : Mueller-Mulot, W.; Rohrer, G.; Oesterhelt, G.; Schmidt, K.; Allemann, L.; Maurer, R. Location: Kontrollabteil., Hoffmann-La Roche A.-G., Grenzach-Wyhlen, Switz. Journal : Fette, Seifen, Anstrichm. Date **: 1983 ,85** (2)66-72 *Coden* : FSASAX ISSN : 0015-038X Language: German Record # 13 Ord.no. : 311:97161710 CA-No. : 97(19)161710z Source : Journal Titei : Commercial experience in the use of leaf analysis for diagnosing nutritional requirement of Hevea Author : Kow, Chang Ah; Hai, Teoh Cheng Location: Harrisons and Crosfield Prang Besar Res. Stn., Selangor, Malay. Journal : Proc. Rubber Res. Inst. Malays. Plant. Conf. Date : 1982)220-31 Coden : PMPCDT ISSN : 0126-9054 Language: English Date : 810000 Record # 14 Ord.no. : 311:97161595 CA-No. : 97(19)161595r Source : Journal Titel Capability and management of alluvial soils under Hevea in Peninsular Malaysia Author : Daud, Noordin Wan; Pushparajah, E. Location: Rubber Res. Inst. Malaysia, Malay. Journal : Proc. Rubber Res. Inst. Malays. Plant. Conf. Date : 1982)174-202 Coden : PMPCDT : 0126-9054 ISSN *Language:* English Date *:* 810000 Record # 15 Ord.no. : 311:97161572 CA-No. : 97(19)1615721 Source : Journal Titel > Nitrogenous fertilizers for Hevea cultivation Author : Pushparajah, E.; Huat, Tan Keh; Lock, Chin Siew Location: Rubber Res. Inst. Malaysia, Malay. Journal : Proc. Rubber Res. Inst. Malays. Plant. Conf. Date : 1982)203-19 Coden : PMPCDT ISSN : 0126-9054 Language: English Data / 810000

Record # 16 Ord.no. : 311:97022603 CA-Mo. : 97(3)22603d *Source :* Journal Titel : Effect of rubber seed oil on the development and regression of experimental atherosclerosis of the aorta in rabbits Author : Liu, Chaoran; Tang, Chaocai; Yang, Liang; Chen, Guozhen Location: Kunming Med. Coll., Kunming, Peop. Rep. China Journal : Zhonghua Xinxueguanbing Zazhi Date : 1982 ,9(1 )54-7 Coden CHHCDF Language: Chinese Record # 17 Ord.no. : 311:96033588 CA-No. : 96(5)33588h Source : Journal Titel : Gossypol in rubber seed meal -Author : Abdullah, Abdul Salam; Hutagalung, R. I. Location: Fac. Vet. Med. Anim. Sci., Univ. Pertanian Malaysia, Serdang, Malay. Journal : Pertanika Date *:* 1981 ,4 (1 )96-8 PERTDY Coden ISSN : 0126-6128 Language: English Record # 18 Ord.nc. : 311:96019162 CA-No. : 96(3)19162h *Source :* Journal Titel : Ultrastructure of mineral deficient leaves of Hevea. III. Quantitative considerations Author : Binte Hamzah, Samsidar; Gomez, J. B. Location: Rubber Res. Inst. Malaysia, Kuala Lumpur, Malay. Journal : J. Rubber Res. Inst. Malays. : 1981 ,29(1 )15-23 Date Coden : JRRIAN ISSN : 0035-953X Language: English Record # 19 Ord.no. : 311:96005596 CA-No. : 96(1)5596r Source : Journal Titel Ultrastructure of mineral deficient leaves of Hevea. II. Effects of micronutrient deficiencies Author : Hamzah, Samsidar Bte; Gomez, J. B. Location: Rubber Res. Inst. Malaysia, Kuala Lumpur, Lumpur, Malay. Journal : J. Rubber Res. Inst. Malays. Date **28**(1)17-25 Coden 🔮 JRRIAN ISSN ; 0035-953X Language: English Record # 20 Ord.no. : 310:95041360 CA-No. : 95(5)41360x Source : Journal Titel # Some aspects of the mineral nutrition of young havea trees in Ivory

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- 115 -

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IIIIIIIII

I.

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Ord.no. to Recs. # 1-72 Ord.no. to Recs. # 73-85 3/9/1 Chloride-ion stimulation of the tonoplast proton-translocating ATPase from Hevea brasiliensis (rubber tree) latex. A dual mechanism 3/9/2 Manufacture of rubber seed oil-modified alkyd resins 3/9/3 Recent advances in the study of tonoplast ATPases from fungi and higher plants 3/9/4 Factors influencing responses to ethephon 3/9/5 Relationships between yield and clonal physiological characteristics of latex from Hevea brasiliensis 3/9/6 Purification and characterization of hevain, a serine protease from Hevea brasiliensis 3/9/7 Canopy photosynthesis in rubber (Hevea brasiliensis) : characteristics of leaves in relation to light interception 3/9/8

A preliminary investigation into the relationship between latex

invertase and latex vessel plugging in Hevea brasiliensis 3/9/9 Characterization of cell sap of Hevea and its influence on cessation of latex flow 3/9/10 Endogenous ethylene in Hevea bark tissues 3/9/11 Carbohydrate status of exploited Hevea. III. Nonstructural carbohydrates in the bark 3/9/12 Evidence for a glutathione reductase activity in the cytosol from the latex of Hevea brasiliensis 3/9/13 Study of the pulping of mixtures of log residues from plywood manufacture in Amazonas State, Brazil 3/9/14 Fractionation of Hevea brasiliensis latex on Ficoll density gradients 3/9/15 Role of the lutoidic tonoplast in the control of the cytosolic homeostasis within the laticiferous cells of Hevea 3/9/16 Role of the lutoidic tonoplast in the senescence and degeneration of the laticifers of Hevea brasiliensis 3/9/17 Comparison of Hevea tonoplast adenosine-triphosphatase from freshly isolated vacuoles and lyophilized tonoplast vesicles 3/9/18 Glutathione S-transferase from Hevea brasiliensis 3/9/19 Physiological regulation of phosphoenolpyruvate carboxylase from a non-chlorophyllian system : the Hevea latex 3/9/20 Control of pink disease of Hevea using tridemorph in ammoniated latex 3/9/21 Sensitivity of tonoplast-bound adenosine triphosphatase from Hevea to inhibitors 3/9/22 Plant growth regulator use in natural rubber (Hevea brasiliensis) 3/9/23 Improved alkyds with epoxidized rubberseed oil 3/9/24 Rubber seed oil - the untapped potential source in Karnataka, India 3/9/25 Effect of cyanide on Microcyclus ulei cultures 3/9/26 A thermogravimetric study of the catalytic decomposition of nonedible vegetable oils 3/9/27 An alkaline protease inhibitor from Hevea brasiliensis latex 3/9/28 A simplified boron diffusion treatment for rubber wood 3/9/29 A model of the vacuolar system : latex lutoids of Hevea brasiliensis. (Report on 15 years of research done in the Ivory Coast and in France) 3/9/30 Chemical defoliation of rubber tree in Bahia State

3/9/31

the peroxidative degradation of organelle membrane and for the early, as well as in situ, congulation of the latex of Hevea brasiliensis 3/9/32 Transtonoplastic proton efflux coupled to electron transport (the NADH-cytochrome c oxidoreductase? functions in the membrane of the vacuole lysosomes from the latex of Hevea brasiliensis 3/9/33 Increase in Hevea production by ethylene 3/9/34 Use of logs left over from plywood manufacture in the pulp and paper industry of Amazonas State, Brazil 3/9/35 Carbohydrate status of exploited Hevea. II. Effect of microtapping on the carbohydrate content of latex 3/9/36 Guayule (Parthenium argentatum A. Gray) : an alternative to hevea (Hevea brasiliensis). (H.B. & K.) Muell. Aug 3/9/37 The suitability of rubberwood (Hevea brasiliensis Muell Agr.) for particleboard manufacturing 3/9/38 The lysozyme of Hevea brasiliensis latex : isolation, purification, enzyme kinetics and a partial amino acid sequence 3/9/39 Formulation and use of fungicides in mineral oils for rubber leaf disease control 3/9/40 Hydroxymethylglutaryl CoA reductase (NADPH) in the latex of Hevea brasiliensis 3/9/41 Laboratory investigations on fungicides and biological agents to control three diseases of rubber and oil palm and their potential applications 3/9/42 Cardanol-based polymer. III. Insulating varnish from Vietnamese materials 3/9/43 Mastication and grean strength of Hevea rubber 3/9/44 Production of antifungal compounds in Hevea pods in response to infection by Phytophthora meadii 3/9/45 Evidence for an electrogenic adenosine triphosphatase in Hevea tonoplast vesicles 3/9/46 Pulping characteristics of waste lors from plywood manufacture in Amazonas State (Brazil) 3/9/47 Sucrose synthetase in the latex of Hevea brasiliensis Muell. Arg 3/9/48 The occurrence of 3-hydroxy-3-methylglutaryl CoA reductase (NADPH) in the latex of regularly-tapped Hevea brasiliensis 3/9/49 Processing of hevea latex 3/9/50 Mycelial biomass and laccase activity in Hevea roots infected by Rigidoporus lignosus 3/9/51 Physiological and anatomical investigations on long-term ethephon-stimulated trees

3/9/52

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I.

A comparative rheological investigation of natural and synthetic cis-1,4 polyisoprenes and their carbon black compounds 3/9/53 Release of bud dormancy in budded stumps and maxi stumps using growth substances 3/9/54 Enzymes of Hevea brasiliensis latex. Adenylate kinase, sulfate adenyly<sup>1+</sup>nusterase (ATP-sulfurylase) and thiosulfate sulfurtransferase (rhodanese). 3/9/35 Carbohydrate status of exploited Hevea. I. The effect of different exploitation systems on the concentration of the major soluble carbohydrates in latex 3/9/56 Multielement determination of trace elements in plant samples by inductively coupled plasma emission spectroscopy : r econcentration and elimination of alkaline earth metal interferences 3/9/57 Triclopyr, a new arboricide for rubber 3/9/58 RRIM trials on stimulation of young rubber 3/9/59 Energization of solute transport and accumulation at the tonoplast in Hevea later 3/9/60 A plant vacuolar system : the lutoids from Hevea brasiliensis latex 3/9/61 A comparative study of stress-induced crystallization of quayule, hevea, and synthetic polyisoprenes 3/9/62 Initial physiological changes in Hevea latex and latex flow characteristics associated with intensive tapping 3/9/63 3-Hydroxy-3-methylglutaryl CoA reductase of Hevea latex : the occurrence of heat-stable activator in the C-serum 3/9/64 Land-disposal of rubber effluent : soil-plant system as a pollutant remover 3/9/65 Biosynthesis of rubber in Hevea brasiliensis 3/9/66 Energization of solute transport and accumulation in the Hevea latex vacuole 3/9/67 Arrhenius plot characteristics of membrane-bound 3-hydroxy-3-methylglutaryi coenzyme A reductase from the latex of Hevea brasiliensis 3/9/68 Characterization of a magnesium-dependent proton translocating ATPase on Hevea latex tonoplast 3/9/69 Some factors influencing tack properties of monoclonal latexes 3/9/70 Physiological activators of invertase from Hevea brasiliensis latex 3/9/71 Penetration of sawed green wood by liquid preservatives 3/9/72 The proton gradient across the vacuolysosomal membrane of lutoids from the latex of Hevea brasiliensis. I. Further evidence for a proton-translocating ATPase on the vacuolysosomal membrane of intact lutoide

3/9/73 Gumwood veneer in plywood manufacture 3/9/74 Further evidence for the proton pumping work of tonoplast ATPase from Hevea latex vacuole 3/9/75 Conversion of linoleic and latex furanoid acid to fish C18 dimethyl furanoid isomers 3/9/76 Fungicide 3/9/77 Proton and carbon-13 NMR spectroscopy of nonadrides 3/9/78 Fatty acids. Part XX1V. Fatty acid composition and the characterization of a novel dioxo C18-fatty acid in the latex of Hevea brasiliensis 3/9/79 Presence of a malic enzyme in Hevea brasiliensis latex 3/9/80 Long-term Ethephon stimulation. 1. Effects of continuous Ethephon stimulation with half-spiral alternate daily tapping 3/9/81 Quebrachitol synthesis in Hevea brasiliensis 3/9/82 The electrochemical proton gradient and its influence on citrate uptake in tonoplast vesicles of Hevea brasiliensis 3/9/83 Viscosity stabilizers and antioxidants for natural rubber latex 3/9/84 The protonmotive potential difference across the vacuo-lysosomal membrane of Hevea brasiliensis (rubber tree) and its modification by a membrane-bound adenosine triphosphatase 3/9/85 Automated determination of sulfur in Hevea and associated cover plants Ord.no. to Recs. # 1-57 92124855 93240925 95169872 92123254 93240909 95129373 92105735 95117337 93240893 92105734 93235272 95099367 92105687 93221705 95092204 92090998 93216564 95082682 92017818 93216519 95082642 92007626 93216518 95082613 92007624 93162534 95063932 93151402 95045105 93144510 95044971 93110805 94193457 93065226 94176775 93063415 94158073 93041764 94156640 93040774 94140920 93020653 94079063 93020652 94042508 93004104 94031830 92210081 94031829 92194500 94031828 92177638 94031827 92165485 94027547 92165311 94027376

1/9/1

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Seeded emulsion polymerization of water-soluble and nonsoluble vinyl monomers 1/9/2 .alpha.-Mannosidase in a plant vacuolar system : lutoids from Hevea brasiliensis latex 1/9/3 Treatment of rubber trees 1/9/4 Utilization of rubber seed oil and karinnotta oil for the preparation of air-drying oil-modified alkyd resins 1/9/5 Asulam based mixtures for weed control in tropical plantation crops 1/9/6 Pulping of rubber tree wastes 1/9/7 Chemi-thermomechanical pulping of Para rubber waste wood 1/9/8 Preservative treatment of rubber wood (Hevea brasiliensis) by pressure impregnation - chemical and biological evaluations 1/9/9 Some studies on fungal deterioration of rubber wood (Hevea brasiliensis) 1/9/10 Electrochemical reduction of rubber seed oil to stearic acid 1/9/11 Preservative treatment of rubber wood (Hevea brasiliensis) by pressure impregnation - chemical and biological evaluations 1/9/12 Long chain branching in natural hevea rubber - determination by gel permeation chromatography 1/9/13 Rubber-seed oil for paint 1/9/14 New early Hevea selection criteria : description and first results 1/9/15 Synthesis of a fish C2O furanoid fatty acid from the lipid extract of the latex of the rubber plant (Hevea brasiliensis) 1/9/16 Use of papain treatment of NR latex to produce superior-quality rubbers 1/9/17 A neutral cytoplasmic phosphatase from the latex of Hevea brasiliensis 1/9/18 Detection of the fungicides thiophanate-methyl, benomyl and triadimefon in rubber tree extracts 1/9/19 Factors influencing the colloidal stability of fresh clonal Hevea latices as determined by the Aerosol OT test 1/9/20 Enzyme deproteinization of Hevea latex. III. Clonal suitability for papain treatment 1/9/21 Enzyme deproteinization of Hevea latex. II. The use of papain in RSS manufacture 1/9/22 Suitability of hundred \_2ries clones for crepe manufacture. Part I 1/9/23 A comparison of abscission of rubber (Hevea brasiliensis) leaves infected with Microcyclus ulei with leaf abscission induced by ethylene treatment, deblading and senescence

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1/9/24 Distribution of proteins between the fractions of Hevea latex separated by ultracentrifugation 1/9/25 Carbon-13 nuclear magnetic resonance spectra of natural rubber latex 1/9/26 Effect of potassium fatty-acid soaps upon heat sensitivity of natural rubber latex containing zinc ammine ions 1/9/27 Effect of storage on the properties of high-ammonia-preserved Hevea latex concentrate 1/9/28 In vitro germination of pollen and pollen tube growth of Hevea brasiliensis in the presence of calcium and boron 1/9/29 The pH of Hevea latex, its effect on production and the elements of its regulation 1/9/30 Use of indolebutyric acid on budded stumps to aid earlier root initiation and growth 1/9/31 Movement of benomyl, thiophanate methyl, and mancozeb on leaves of Hevea brasiliensis and their fungicidal action on Microcyclus ulei 1/9/32 A new formulation for controlling black stripe 1/9/33 Chemical control of rhododendron dieback caused by Phytophthora heveae 1/9/34 Microbial deterioration and preservation of Hevea latex 1/9/35 Protection of Hevea flowers and seeds for maximizing seed production and utilization 1/9/36 Factors associated with development of partial dryness (of latex trees) 1/9/37 Neutron-activation analysis of plant materials 1/9/38 Modification of pH of latex cytoplasm by ethylene 1/9/39 The relationship of phenols and oxidative enzymes with the resistance of Hevea to South American leaf blight 1/9/40 Automated determination of boron in Hevea plant materials 1/9/41 Ethylene formation in excised Hevea bark disks 1/9/42 Stimulation of lateral root production and bud-break with growth regulators in Hevea budded stumps 1/9/43 Some evidence about the occurrence of a magnesium-ATP-dependent proton pump in a plant vacuo-lysosomal compartment 1/9/44 pH variations between the vacuolar and cytoplasmic compartments in the latex of Hevea brasiliensis. Seasonal influences and action of hormonal treatments (ethrel, generator of ethylene). Effects on latex yield and formation of dry zones on tapping cuts 1/9/45 The biochemistry of three natural products of Hevea brasiliensis and

their utilization potential

1/9/46 Fusion of protoplasts of Hevea brasiliensis (Muell. Arg.) and Hevea pauciflora (Muell. Arg.). Establishment of technique 1/9/47 Wood quality aspects of tropical hardwoods used for pulp and paper 1/9/48 Production of drying oil for paint from rubber-seed oil 1/9/49 Polyisoprene 1/9/50 Chemical weeding in Hevea culture 1/9/51 Induction and control of flowering in Hevea 1/9/52 Variations in stimulation response in yield of a Hevea clone. 1. Component variance model 1/9/53 Chemical weeding in Hevea culture 1/9/54 Regulation of indoleacetic acid oxidase activities in Hevea leaves by naturally occurring phenolics 1/9/55 Purification and study of phosphoenolpyruvate carboxylase from Hevea brasiliensis latex 1/9/56 Natural rubbers as renevable resources 1/9/57 Chemistry and structure of natural rubbers Ord.no. to Recs. # 1-72 Ord.no. to Recs. # 73-96 

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37112956 87093811 87097155 87054269 87050150 87035941 87002440 87002399 87002334 86191052 86186077 86186020 86184567 85084519 86074859 86036504 86012619 1/9/1 Use of oil of rubber granules for producing electrically-insulating oleoresinous varnishes 1/9/2 Phenolic compounds from the latex of Hevea brasiliensis :aglycons 1/9/3 Rubber seed oil. Analysis and possible applications 1/9/4 Paraquat, vegetable oils, copper and other elements as stimulants of latex production 1/9/5 Enzyme deproteinization of Hevea latex. I. Preparation and properties of DPNR and viscosity stabilized DPNR 1/9/6 Relationship between leaf age and some carbon dioxide exchange characteristics of four Hevea brasiliensis Muell, Arg. clones 1/9/7 Some influences of ethrel stimulation on properties of natural rubber and latex 1/9/8 Use of thin-layer chromatography in the analysis of fatty acids in rubber seed oil 1/9/9 Drying of zeolites 1/9/10 Carbohydrate composition of some floral species of Amazonia (Brazil) 1/9/11 Sucrose content in latex of native rubber trees stimulated with Ethrel 1/9/12 Effects of compounding variations on the properties of quayule rubber 1/9/13 Partial purification and properties of glutathione-S-aryltransferase in latex of Hevea brasiliensis 1/9/14 Efficacy test of several fungicides against moldy rot 1/9/15 A review of chemical weed control in rubber plants and legumes 1/9/16 The spontaneous coagulation of hevea latex 1/9/17 Tissue culture of Hevea brasiliensis Muell. Arg 1/9/13

Structure and properties of a 2-chloroethylphosphonic acid (ethephon) metabolite from Hevea brasiliensis bark 1/9/19 Evaluation of some herbicides against weeds in the rubber planting strip 1/9/20 Efficacy trial of Cepha-10-LS and Flots-100-SCO latex stimulants on rubber trees 1/9/21 The prospect of Ethrel application on rubber in Indonesia 1/9/22 Surface study on the rubber particles in pretreated Hevea latex system 1/9/23 Factors affecting alkali sorption into some wood species 1/9/24 Chronological development, after stimulation, of some characteristics of Hevea brasiliensis latex 1/9/25 Metabolism of 2-chloroethylphosphonic acid (Ethephon) in suspension cultures of Hevea brasiliensis 1/9/26 Distribution and concentration of major soluble carbohydrates in Hevea latex, the effects of ethephon stimulation and the possible role of these carbohydrates in latex flow 1/9/27 Sea water desalinization system 1/9/28 Enzyme treatment of Hevea latex to obtain superior quality rubber 1/9/29 Properties and potential of rubber seed oil 1/9/30 Extraction of rubber or rubberlike substances from fibrous plant materials 1/9/31 The occurrence of a furanoid fatty acid in Hevea brasiliensis latex 1/9/32 Demonstration of latex coagulants in bark extracts of Hevea and their possible role in latex flow 1/9/33 A model of an isolated intact vacuolar structure : lutoids from Hevea brasiliensis latex. II. Characteristics of the lutoid membrane 1/9/34 A model of an isolated intact vacuolar structure : Lutoids from Hevea brasiliensis latex. I. Accumulation and penetration of citrate and L-lysine in lutoids 1/9/35 Production of articles of elastic hard rubber using modified natural rubber. Part II 1/9/36 Effect of storage on the properties of high ammonia-preserved Hevea latex concentrate 1/9/37 Control of South American leaf blight (Microcyclus ulei (P. Henn.) V. Arx.) in rubber tree nursery with several fungicides 1/9/38 Study on yield, sucrose level of latex and other important characteristics of Hevea brasiliensis Muell. Arg. III. As influenced by microtapping system 1/9/39 Study of yield, sucrose level of latex and other important

characteristics of Hevea brasiliensis Muell. Arg. I. As influenced by clone 1/9/40 Study on yield, sucrose level of latex and other important characteristics of Hevea brasiliensis Muell Arg. II. As influenced by tapping system 1/9/41 Performance of ethephon and Ethad on smallholdings (of rubber trees) 1/9/42 Responses of Hevea to stimulation 1/9/43 Preservative treatment of poplar, beech and rubber wood 1/9/44 Electrophoresis and demonstration of enzymic activities in Hevea brasiliensis latex 1/9/45 Stimulation methods and practices (and rubber trees) 1/9/46 Hard flexible materials based on natural rubber. Part I. Blends of natural rubber with Heveaplus MG49 1/9/47 Investigations on new fungicidal systems for control of bark rot on Hevea brasiliensis 1/9/48 The thermal oxidation of Guayule and Hevea rubbers by dynamic differential scanning calorimetry 1/9/49 Contribution to the study of premature flowering of hevea 1/9/50 Evaluation of fungicides for control of South American leaf blight of Hevea brasiliensis 1/9/51 Report on the results of chemical weed control experiments the rubber plantations in south India 1/9/52 Hard flexible materials based on blends of natural rubber with Heveaplus MG 49 1/9/53 Report on large scale stimulation experiments 1/9/54 Ethrel stimulation of Hevea under conditions in Sri Lanka 1/9/55 Practical aspects of the use of Ethrel in association with periodic tapping of rubber 1/9/56 Study of the latex coagulation mechanism in Hevea brasiliensis (Kunth) Mull. Arg. II. Enzymic systems implicated in the process. I. Phenol oxidases 1/9/57 Fungicides for controlling tapping panel diseases 1/9/58 Effect of chilling temperature on plant metabolism of Hevea brasiliensis 1/9/59 Protein biosynthesis of latex, factor of hevea production 1/9/60 Water vapor and carbon dioxide diffusion resistances of four Hevea brasiliensis clonal seedlings 1/9/61 Ecophysiology of tropical crops. Rubber

1/9/62

Stimulation of rubber yield from Hevea brasiliensis 1/9/63 Oil plants of Zaire. III. Botanical families producing oils of relatively high nonsaturation 1/9/54 Ethylene production by Hevea brasiliensis tissues treated with latex yield-stimulatory compounds 1/9/65 The role of lipids and proteins in the mechanism of latex vessel plugging in Hevea brasiliensis 1/9/56 A spray-on natural rubber latex formulation for controlling pink disease 1/9/67 Plant growth regulator composition, especially for rubber plants 1/9/68 Effect of nematicides in an immature rubber planting 1/9/69 Use of pre-emergence herbicides during est blishment of leguminous cover crops 1/9/70 Use of Roundup (glyphosate) for lalang control prior to planting oil palm and rubber 1/9/71 Effects of repeated treatments of hevea by 2-chloroethylphosphonic acid on latex polyribosomes 1/9/72 Low-volume spray of an oil-based systemic fungicide for controlling Oidium secondary leaf fall 1/9/73 Ribosomes in the lutoid fraction (=lysosomal compartment) from Hevea brasiliensis Kunth. (Mull.-Arg.) latex 1/9/74 Plant crops as a source of fuel and hydrocarbon-like materials 1/9/75 Membrane ATPase of lysosomal vacuoles : Heveabrasiliensis latex lutoids 1/9/75 Some factors affecting yield response to stimulation with 2-chloroethylphosphonic acid 1/9/77 Protein and enzyme variation in some Hevea cultivars 1/9/78 Phospholipid composition of the membrane of lutoios from Hevea brasiliensis latex 1/9/79 Roundup for weed control in mature rubber planting strips dominated by Ottochloa nodosa and Paspalum conjugatum 1/9/80 Kinetics of the effect of 2-chloroethylphosphonic acid on Hevea brasiliensis latex polyribosomes 1/9/81 Lipids of Hevea brasiliensis and Euphorbia coerulescens 1/9/82 Microbiological degradation of Hevea latex and its control 1/9/83 Heveaplus MG latex - preparation from latex concentrate 1/9/84 Hydrocarbons via photosynthesis 1/9/85 Diverse properties in citrate, malate, and succinate by lubbids from

٠

- 128 -

latex, Hevea brasiliensis 1/9/86 Absorption of citrate by the lutoids of latex and rubber production by Hevea 1/9/87 Study of a membrane ATPase of lysosomal vacuoles : lutoids from Hevea brasiliensis latex 1/9/88 Problems posed concerning the existence of ribonucleic acids in plant lysosomal compartments 1/9/89 Study of coagulation mechanism of Hevea brasiliensis (Kunth) Muell. Arg. latex. I. Factors acting on coagulation 1/9/90 Study of two peroxidases extracted from Hevea root tissues, either healthy or contaminated by Leptoporus lignosus (K1.) Heim 1/9/91 Absorption of amino acids by lutoids from the latex of Hevea brasiliensis 1/9/92 Composition and method for stimulating the yield of rubber from Hevea Brasiliensis 1/9/93 Cultivation in vitro of callus tissue derived from anthers of Hevea brasiliensis (Muell Arg.) 1/9/94 Examination of hybrid rubber seed oils 1/9/95 Variations of polyribosomes from Hevea latex caused by ethrel and other treatments enhancing latex flow 1/9/96 A study on the comparative effect of some pre-emergence weedicides on the control of weeds in rubber plantations Ord.no. to Recs. # 1-72 

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Ord.no. to Recs. # 73-107 78098758 75101396 76100857 78098210 78093640 76086822 78093466 76082191 76082123 78084525 78071544 75082122 78068622 76082032 76073411 78059535 78053924 75070031 78044787 76043997 76001266 78040385 78012595 77155385 77149653 77148992 77123020 77122925 77122915 77103021 77102960 77063659 77021083 76155192 76151114 1/9/1 Control of carbohydrate metabolism by ethylene in latex vessels of Hevea brasiliensis Muel. Arg. in relation to rubber production 1/9/2 Seasonal changes in the effectiveness of ethrel, 2,4-D and NAA in the stimulation of latex flow in Hevea brasiliensis mull. arg 1/9/3 Extracting rubber latex 1/9/4 Method of modifying plant growth 1/9/5 Laccase and peroxydase activities in Hevea roots infected by the white wood rotting fungus Leptoporus lignosus 1/9/6 Lysozymes : major components of the sedimentable phase of Hevea brasiliensis latex 1/9/7 'Coagulase' from the fractionation of C-serum of Hevea latex 1/9/8 Role of growth promotor and growth inhibitor in foliar senescence and abscission of Hevea brasiliensis Muell. Arg 1/9/9 Responses of clones and seedlings to stimulation in large-scale variety trials 1/9/10 Alternative crumbling agent for Hevencrumb manufacture 1/9/11 Dunlop Ethrel trials 1/9/12 Metabolism of ethephon (2-chloroethylphosphonic acid) and related compounds in Hevea brasiliensis 1/9/13 Morphogenesis in callus cultures of Hevea brasiliensis 1/9/14 The effects of agitated liquid medium on in vitro cultures of Hevea brasiliensis

1/9/15 Proceedings of the R.R.I.M. Planters' Conference 1973, Kuala Lumpur 1/9/15 Physiological studies on the abscission of leaves of rubber (Hevea brasiliensis) caused by Phytophthora palaivora and on its inhibition by synthetic growth regulators 1/9/17 Studies on some anticoagulants and preservatives of Hevea latex 1/9/18 Coagulation of Hevea latex with surfactant and salt. II. Batch-wise commercial processing 1/9/19 Methane fermentation of rubber (Hevea brasiliensis) latex effluent 1/9/20 The proteins of Hevea brasiliensis latex. Part 6. Hevamine : a crystalline basic protein from Hevea brasiliensis latex--1/9/21 Studies of Indian rubberseed and rubberseed oil. II. Processing 1/9/22 Method of preparing paper-making material 1/9/23 Solvent fractionation of Indian rubber seed oil 1/9/24 Efficiency of paraquat as a weed control chemical for rubber nurseries 1/9/25 Technical feasibility of para-rubber (Hevea brasiliensis Muell.-Arg.) for particleboard manufacture 1/9/26 Modifications of citrate transport and intraparticulate pH by ATP in lutoids of Hevea brasiliensis latex 1/9/27 Resins from epoxy oils for surface coating 1/9/28 Control of blue-stain on rubber (Hevea brasiliensis) wood during the boron diffusion treatment 1/9/29 Proteolytic action of papain on proteins in Hevea latex 1/9/30 Novel method of stabilizing Hevea latex 1/9/31 Latex flow studies. IX. Effects of application of yield stimulants on rheology of Hevea latex and on concentrations of charged components in its serums 1/9/32 Organic silicon compounds 1/9/33 Plant standard for the analysis of leaves 1/9/34 Characterization of a membrane ATPase in the presence of an acid phosphatase in the latex lutoids of Hevea brasiliensis 1/9/35 Electron transport in the memorane of lutoids from the latex of Hevea brasiliensis 1/9/36 Mechanism of citrate accumulation in the lutoids of Hevea brasiliensis latex 1/9/37 Occurrence of ribonucleic acid in the lutoid fraction (lysosomal compartment) from Hevea brasiliensis latex (77:38)

Purification and study of the lutoidic sold phosphatase of the Heves brasiliensis latex 1/9/37 Occurrence of ribonucleic acid in the lutoid fraction (lysoscmal compartment) from Hevea brasiliensis latex 1/9/40 Model for the mechanism of stimulation of latex flow in Hevea brasiliensis by ethylene 1/9/41 Control of RNA level and of RNA ratios in the latex of Hevea brasiliensis. Effect of latex tapping and of growth regulators 1/9/42 Yield stimulants for Hevea brasiliensis 1/9/43 Free amino acids of Hevea brasiliensis latex 1/9/44 Effect of 2-chloroethylphosphonic acid (Ethrel) on Hevea brasiliensis latex polysomes. 1/9/45 Stem galls of Hevea brasiliensis 1/9/46 Mixed cooring of rubberwood and bamboo by the sulfate process 1/9/47 Problems of applying growth regulators to selected agricultural crops of the tropics and subtropics. Literature survey 1/9/48 Activity of latex invertase and latex production in Hevea brasiliensis 1/9/49 Structure of hemicellulose isolated from rubber wood 1/9/50 Characteristics of amino acid incorporation by latex polysomes from Hevea brasiliensis 1/9/51 Rubber coagulation by enzymes of Hevea brasiliensis latex 1/9/52 2 -Nucleotidase, a new enzyme of Hevea brasiliensis latex 1/9/53 Changes in bacteria-free filtrate of Hevea latex C-serum from partially dry trees 1/9/54 Assessment of some molecular parameters of mevalonate kinase from plant and animal sources 1/9/55 Latex flow stimulation by phosphonates 1/9/56 Composition for stimulating latex yield of rubber plants 1/9/57 Regulation of invertase activity in the latex of Hevea brasiliensis. Effects of growth regulators, bark wounding, and latex tapping 1/9/58 Rubber, gutta percha, and chicle 1/9/59 Decomposition of 2-chloroethylphosphonic acid in stems and leaves of Hevea brasiliensis 1/9/60 Level and distribution pattern of latex sucrose along the trunk of Hevea brasiliensis as affected by the sink region induced by latex tapping 1/9/61 Autom ted coloridetric determination of magnetium in follage of

Hevea and other tropical crops 1/9/52 Role of malonyl-coanzyme A in isopramoid biosynthesis 1/9/63 Sucrose-mobilizing effect of auxias in Hevea brasiliensis. Dependence on metabolic activity of the treated tissue 1/9/64 Gelling properties of Havea latex serum 1/9/65 Stimulation of Hevea brasiliensis by ethylene compositions 1/9/56 Paper-making pulp from a waste rubber wood 1/9/67 Effect of hormone stimulation of production on the sucrose content of Hevea brasiliensis latex 1/9/68 Natural latex 1/9/69 Study of sodium alizarin-3-sulfonate for the determination of aluminum in leaves of Hevea brasiliensis 1/9/70 Black thread disease, control measures, and yield stimulation in Hevea brasiliensis in Liberia 1/9/71 Antifungal preparation for the control of brown bast in Hevea species 1/9/72 Control of black thread (Phytophthora palmivora) in Hevea brasiliensis with Difolatan 1/9/73 Ethylene treatment of Hevea brasiliensis 1/9/74 Reaction kinetics of polymer substituents. Neighboring substituent effects in pairing reactions 1/9/75 Organosilicon plant growth regulators 1/9/75 Difolatan, a promising fungicide for control of the tapping pane. disease, Black Thread, in Hevea brasiliensis 1/9/77 Organosilicon compounds 1/9/78 Fungal products. IV. Structure of heveadride, a new nonadride from Helminthosporium heveae 1/9/79 Glyceraldehyde 3-phosphate dehydrogenase of Hevea brasiliensis latex. Comparison with its phosphorylating homolog 1/9/80 Preservation of Hevea latex 1 / 7/81 Chemical defcliation of Hevea brasiliensis for avoiding secondary leaf fall 1/9/82 Chemical treatment in the extraction of rubber latex from Hevea brasiliensis 1/9/83 Output, composition, and metabolic activity of Hevea latex in relation to tapping intensity and the onset of brown bast 1/9/84 Ethrel-induced increase of latex production in Hevea brasiliensis twooet trees

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1/9/85 Improvement of wood by impregnation with monomers and curing by heat catalyst 1/9/86 Compartmentalization of different oxidoreductases (peroxidase, 0-diphenol oxidase, and malate dehydrogenase) in the latex of Hevea brasiliensis 1/9/87 Inhibition of plant mevalonate kinase preparations by prenyl pyrophosphates 1/9/83 Stimulation of rubber yield in Hevea brasiliensis 1/9/39 Improvement in vegetative multiplication of the hevea. Effect of growth substances on chizogenesis 1/9/90 Weed control under Hevea in Ceylon with herbicide mixtures based on MSMA (monosodium acid methane arsonate) 1/9/91 Preparation of Heveacrumb from first fraction coagulum 1/9/92 Naturally occurring antioxidants in Hevea brasiliensis latex 1/9/93 Pulping of para rubber tree 1/9/94 Naturally occurring antioxidants in Hevea brasiliensis latex 1/9/95 Manufacture of dark factice from rubber seed oil 1/9/96 Demonstration of functional polysomes in Hevea brasiliensis latex 1/9/97 Measurements of fiber dimensions and analysis of the chemical composition of Taiwan hardwoods 1/9/98 Coagulation of Hevea latex with surfactant and salt. I. Development of the process and its effect on raw rubber properties 1/9/99 Improvements to assisted biological coagulation of Hevea latex 1/9/100 Haloparaffin stimulation of the rubber yield in Hevea brasiliensis 1/9/101 Novel stimulants and procedures in the exploitation of Hevea. III. Comparison of alternative methods of applying stimulants 1/9/102 Novel stimulants and procedures in the exploitation of Hevea. II. Pilot trial using (2-chloroethyl)-phosphonic acid(ethephon) and acetylene with various tapping systems 1/9/103 Novel stimulants and procedures in the exploitation of Hevea. I. Introductory review 1/9/104 Seasonal variations in some properties of Hevea brasiliensis latex 1/9/105 Physiological aspects of the exploitation of rubber trees 1/9/106 Photosynthesis and latex production of three Hevea brasiliensis clones 1/9/107 Enzymes forming isopentenyl pyrophosphate from 5-phosphomevalonate (mevalonate 5-phosphate) in the latex of Hevea brasiliensis

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Ord.no. to Recs. # 1-72
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74039228
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74030974
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74020362
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Ord.no. to Recs. # 73-139
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68079356
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68079280
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68075767
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68075733
                   57011617
 1/9/1
  Structure of heveaflavone
 1/9/2
 Flavonoids of some Euphorbiaceous plants
 1/9/3
  Splitting of Indian vegetable oils. VIII.
                                                Unusual oils of
commerical importance
 1/9/4
 Mathematical expressions for the flow of Hevea brasiliensis latex
 1/9/5
  Cyclization of matural rubber (Hevea). II
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1/9/5 Rubber transferase from Hevea brasiliensis 1/9/7 Ubiguinones of Hevea brasiliensis 1/9/8 Role of lutoids in the flow of latex in Hevea brasiliensis. II. Development of lutoid hydrolases and of some properties of latex during tapping 1/9/7 Particularities of glycolysis and its regulation within the latex of Hevea brasiliensis 1/9/10 Protoplasts of comycete fungi 1/9/11 Relationship between latex yield of Hevea and rubber biosynthesis in vitro 1/9/12 Stimulation of Hevea brasiliensia rubber production 1/9/13 Cellulase in latex and its possible significance in cell differentiation 1/9/14 Hevea latex enzymes detected by zymogram technique after starch gel electrophoresis 1/9/15 Spectrographic determination of calcium in latex of natural subber (Hevea brasiliensis) 1/9/16 Catalyst for stereospecific polymerization of butadiene 1/9/17 Effect of hydroxylamine hydrochloride on micro-organisms in Hevea latex 1/9/18 Control of Gloeosporium leaf disease of Hevea in Ceylon 1/9/19 Purification and identification of a substance from the rubber tree (Hevea brasiliensis) involved in resistance to the fungus Dothidella ulai 1/9/20 Biosynthesis of tocochromanols 1/9/21 Role of lutoids in the flow of latex in Hevea brasiliensis. I. Development of lutoid hydrolases and some properties of the latex during the tapping of virgin trees 1/9/22 Hydrolysis of semidrying oils. II. Splitting studies on rubber seed oil 1/9/23 Inhibition of Hevea brasiliensis latex NADP-phosphatase and interference with isoprene anabolism 1/9/24 Electron microscopical studies of latex vessel system of Hevea brasiliensis 1/9/25 Electrophysiological phenomena in Hevea brasiliensis 1/9/26 Physiology of Hevea (latex flow) 1/9/27 Changes in organomineral composition and respiratory activity of Hevea latex associated with intensive tapping 119124

Nucleic acids in latex and production of tubber in Hevea brasiliensis 1/9/29 Substrate and metabolism of carbon dioxide formation in Hevea latex in vitro 1/9/30 Carbohydrate metabolism in Hevea latex---availability and utilization of substrates 1/9/31 Regulation of glycolysis in latex of Hevea brasiliensis 1/9/32 Composition of latex serum and 'bottom fraction' particles 1/9/33 Processing of Hevea latex into natural rubber 1/9/34 Rubber seed 1/9/35 Properties of Hevea brasiliensis latex 1/9/35 Hormone stimulation of production in Hevea brasiliensis 1/9/37 Continuous coagulation of Hevea latex 1/9/38 Influence of light on paraquat activity in the tropics 1/9/39 Biochemical study of the lutoids in the latex of Hevea brasiliensis. Differences and analogy with lysosomes 1/9/40 NADP phosphatase in Hevea brasiliensis latex 1/9/41 Cellulase in Hevea latex 1/9/42 Pulping of rubber (tree) wood 1/9/43 Identification of glyceraldehyde-3-phosphate dehydrogenase in the latex of Hevea brasiliensis 1/9/44 Unsaturated natural or synthetic rubbers resistant to degradation 1/9/45 Isolation of .gamma.-tocotrienol dimers from Hevea latex 1/9/46 Determination of dry rubber content of hevea brasiliensis by latex film dialysis 1/9/47 Characteristics of pyruvate kinase of the latex of Hevea brasiliensis 1/9/48 Kinetics of reduced nicotinamide adenine dinucleotide (NADH) accumulation. Regulation of glycolysis in Hevea brasiliensis latex 1/9/49 Cyclisation of cis-polyisoprene (natural hevea rubber) 1/9/50 Effects of minerals introduced directly into the wood and of acetylene applied to the back of Hevea 1/9/51 Gas chromatographic determination of the pyrolytic products of cyclized natural pale Crepe (hevea) rubber 1/9/52 Cellulase in latex and its possible significance in cell differentiation 1/9/53

•

Anatomical and chesical characteristics of Indian Services with special reference to their suitability for pulp. III 1/ 7/ 54 Choice of fungicides for low-volume sprays 1/9/55 Biosynthesis of rubber from latex 1/9/55 Stimulatory effects of 2,4;dichlorophenoxyacetic acid and of 1-maphthaleneacetic acid on sucrose level, invertase activity, and sucrose utilization in the latex of Hevea brasiliensis 1/9/57 Cyclization of cis-polyisoprene (natural Hevea rubber) 1/9/58 Viscosity-stabilized heveacrumb 1/9/59 Heveacrumb Process 1/9/60 Heveaflavone - a new biflavonoid from Hevea braseliensis 1/9/61 Ethylene, a new agent stimulating latex production in Hevea brasiliensis 1/9/62 Stimulation of Hevea brasiliensis latex production by application of growth substances at a certain distance from the cut 1/9/63 Role of malonyl-coenzyme A in isoprenois biosynthesis 1/9/54 Determination of hydrogen sulfide in Hevea latex and concentrates 1/9/65 Latex flow studies. VI. Effects of high pressure gradients on flow of fresh Hevea latex in narrow-bore capillaries 1/9/66 Latex flow studies. V. Rheology of fresh Hevea latex flow in capillaries. 1/9/67 Determination of rubber in Hevea species 1/9/68 Evaluation of fungicides for the control of Helminthosporium heveae on Hevea rubber in Malaysia. II. Field tests 1/9/69 Evaluation of fungicides for the control of Helminthosporium heveae on Hevea rubber in Malaysia. I. Laboratory assessment 1/9/70 Stimulation of latex flow in Hevea brasiliensis by 4-amino-3,5,6-trichloropicolinic acid and 2-chloroethanephosphonic acid 1/9/71 Structure of cell walls of phycomycetes 1/9/72 Utilization of ethanol as a carbon source by Phytophthona heveae 1/9/73 Growth of Phytophthora heveae on media containing L-glutamine and urea 1/9/74 In vitro effect of certain inorganic ions and organic compounds on the stability of certain lutoids in hevea latex 1/9/75 Structure of sulfur vulcanizates of SBR and Hevea rubber 110/74

Wie in Actualone to Control Acid Continuants in Hevel (Ster Systems

containing yeasts and bacteria 1/9/77 Latex flow studies. III. Electrostatic considerations in the colloidal stability of fresh Hevea latex 1/9/78 Latex flow studies. II. Influence of lutoids on the stability and flow of Hevea latex 1/9/79 Latex flow studies. I. Electron microscopy of Hevea brasiliensis in the region of the tapping cut . /9/80 Uptake of ergothioneine from the soil into the latex of Hevea brasiliensis 1/9/81 Effects of plant growth regulators and other compounds on flow of latex in Hevea brasiliensis 1/9/82 Metabolic pathways in Hevea brasiliensis latex, dehydrogenase lacate, and aldoiase 1/9/83 Planting and production of natural rubber and latex 1/9/84 Differentiation of cis-trans configurations of trialkylethylene isomers by infrared spectroscopy 1/9/85 Some characteristics of pyrophosphomevalonate decarboxylase from Hevea brasiliensis latex 1/9/85 Effect of ATP on the metabolism of pyruvate in Hevea brasiliansis latex 1/9/87 Formation of .DELTA.3-isopentenyl monophosphate and pyrophosphate in the latex of Hevea brasiliensis 1/9/88 Utilization of L-asparagine by two species of Phytophthora 1/9/39 Inhibition of ATP by malate, alcohol, and lactate dehydrogenases in Hevea brasiliensis latex 1/9/90 Radiochemical process for the in situ determination of metabolic activity of the latex of Hevea brasiliensis 1/9/91 Anaerboic respiration in latex of Hevea brasiliensis substrate and limiting factors 1/9/92 Photosensitizing activity of some organic compounds on degradation of natural rubber (Hevea) in solution in the pressence of visible light 1/9/93 Structura' elucidation of cyclized rubbers by chemical degradation 1/9/94 Unsaturation in depolymerized rubber 1/9/95 Pentose cycle in Hevea brasiliensis latex 1/9/96 Lysosomal character of lutoids in Hevea brasiliensis latex 1/9/97 L-Alanine, an allosteric inhibitor of lactic dehydrogenase in Hevea brasiliensis latex. Effect of pH 1/9/98

Ergothioneine and hercynine in Hevea brasiliensis latex

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1/9/99 Determination of osmolarity of small latex samples by vapor-pressure osmometer 1/9/100 Anaerobic respiration in latex of Hevea brasiliensis. Substrate and limiting factors 1/9/101 Carbohydrate catabolism in Hevea brasiliensis latex 1/9/102 Effects of tapping, wounding, and growth regulators on turgor pressure in Hevea brasiliensis 1/9/103 Cellulose 1/9/104 Kinetic studies of the cyclization of natural (Hevea) rubber 1/9/105 Use of chemical weed killers in the cultivation of young heveas planted in tertiary sands on the Ivory Coast 1/9/105 Presence of both hexokinase and fructokinase in Hevea brasiliensis latex 1/9/107 Plastic bonded copper foil 1/9/108 Determination of castor oil in heveacrumb rubber by thin-layer chromatography 1/9/109 New form of natural rubber 1/9/110 Coper fungicides. I. Biological eficacy of copper spray deposits containing various stickers 1/9/111 Chemical composition of hyphal wall of phycomycetes 1/9/112 Plastochromanol 1/9/113 Stimulation of Hevea by chlorophenoxyacetic acids and its influence on the drained area 1/9/114 Incorporation of methionine-14C into chromanols and guinones by Hevea brasiliensis latex 1/9/115 Newsprint from Hevea brasiliensis wood 1/9/115 ATP, an allosteric inhibitor of lactic dehydrogenase in Hevea brasiliensis latex 1/9/117 Determination of the microstructure of the 1,4-and the 3,4-polyisoprenes by pyrolysis and gas chromatography 1/9/118 Biological coagulation of Hevea latex using waste carbohydrate substrates 1/9/119 Study of the productivity and some properties of latex from different parts of the Hevea trunk 1/9/120 The plurality of long chain isoprenoid alcohols (polyprenois) from natural sources 1/9/121 Studies on tissue culture of Hevea brasiliensis. I. Role of osmotic concentration, carbohydrates, and pH values in induction of

callus growth in plumule tissues from Hevea seedlings 1/9/122 Particle aggregation following dilution of Hevea latex :a possible mechanism for the closure of latex vessels after tapping 1/9/123 Physiological changes in Hevea brasiliensis tapping panels during the induction of dryness by interruption of phloem transport. II. Changes in bark 1/9/124 Physiological changes in Hevea brasiliensis tapping panels during the induction of dryness by interruption of phloem transport. I. Changes in latex 1/9/125 Planting and production of raw rubber and latex 1/9/125 Glyceride studies. VI. The component glycerides of rubber seed oil Hevea brasiliensis 1/9/127 Preliminary physiological studies on the promotion of latex flow by plant growth regulators 1/9/128 Stimulation of latex flow in Hevea brasiliensis 1/9/129 Molecular interpretation of the .gamma.-transition in poly-ethylene and related compounds. 1/9/130 Metabolism of quebrachitol and other carbohydrates by Hevea latex bacteria 1/9/131 Breakdown of amino acids by Hevea latex bacteria 1/9/132 Accuracy and precision in routine leaf analyses 1/9/133 White root disease of Hevea brasiliensis collar protectant dressings 1/9/134 Certain modifications of Hevea rubber and their use in pressure sensitive adhesives. II. Use of maleic anhydride-modified and phenol-modified rubbers in pressure-sensitive adhesives 1/9/135 The new look of natural rubber. I 1/9/136 Chemical ground pulp from Hevea wood 1/9/137 Taraxerol from rubber leaves 1/9/138 Certain modifications of Hevea rubber and their use in pressure-sensitive adhesives. I. Modification of Hevea rubber with maleic anhydride and phenols 1/9/139 Identification and separation of isoprenoid alcohols

File 51:FSTA - 69-85/May 1/5/1 272547 85-02-n0054 A comparison of the stability of oils from Brazil nut, Para rubber and passion fruit seeds. 1/6/2 262694 84-08-n0409 (Finding of ALPHA -, BETA - and GAMMA -dehydrotocopherol in wheat germ oil by HPLC and GC/MS - a contribution to tocopherol analysis.) Zur Auffindung von ALPHA -, BETA - und GAMMA -Dehydrotocopherol in Weizenkeimoel mittels HPLC und GC/MS - ein Beitrag zur Analytik der Tocopherole. 1/6/3 019988 70-08-L0523 GAS CHROMATOGRAPHY OF TRIMETHYLSILYL SUGARS AT VARIOUS TEMPERATURES.

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80008094		27067491
80008083	78056374	27057490
79058560	78054700	27057489
79058559	78046778	27063575
79054400	78042976	27054350
79043893	78035478	27019724
79043882	78033031	26074873
79040571	78927421	26058145
79040570	78022606	26048751
79040569	78014714	26026514
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28069450	77091692	74086838
28059445	77091688	76075366
28069422	77091226	76067914
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28012564	77072576	76036917
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78090458	27081759	76029116
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76018419	75010553	74039396
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75090977	75003156	74027573
75090884	75003149	74027518
75090763	25039918	74016945
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75080305	25032498	74005719
75072494	25029827	74002973
75072486	25019294	73057027
75071955	24067432	73039036
75067677	24964484	73035182
75067487	24042389	73031502
75064725	24027556	73020373
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	74083242	73002783
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75048217	74078412	23013948
75041785	74078411	23012037
75041780	74075018	22063123
75033959	74076017	22060942
75029105	74075086	22002060
75026966	74870203	72083559
75021295	74068523	72073543
Ord.no. to	Recs. # 145-170	
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71080837 71074265 71055525 71045235 71043342 71038389 71033319 71031214 71631213 71027032 71007322 71005581 71005540 71003798 21055437 21041171 1/9/1 79085750 A NOTE ON THE WORKING QUALITY AND FINISH ADAPTABILITY OF RUBBERWOOD HEVEA-BRASILIENSIS Descriptors :WORKABILITY FINISH 1/9/2 79081883 EFFECTS OF DIFFERENT MANAGEMENT SYSTEMS ON THE PHYSICAL PROPERTIES OF A CLAY YELLOW LATOSOL OF THE STATE OF AMAZOMAS BRAZIL Descriptors : HEVEA-SPP PUERARIA-PHASEOLOIDES TILLAGE NO-TILL VEGETATIVE COVER FLOCCULATION AGGREGATE STABILITY TILTH ~?T 1/6/1 1/5/1 79085750 A NOTE ON THE WORKING QUALITY AND FINISH ADAPTABILITY OF RUBBERWOOD HEVEA-BRASILIENSIS ?T 1/6/ALL 1/6/1 79085750 A NOTE ON THE WORKING QUALITY AND FINISH ADAPTABILITY OF RUBBERWOOD HEVEA-BRASILIENSIS 1/6/2 79031883 EFFECTS OF DIFFERENT MANAGEMENT SYSTEMS ON THE PHYSICAL PROPERTIES OF A CLAY YELLOW LATOSOL OF THE STATE OF AMAZONAS BRAZIL 1/6/3 79077104 INFLUENCE OF STOCK PREPARATION AND PLANTING TECHNIQUES ON VEGETATIVE DEVELOPMENT OF RUBBER HEVEA-BRASILIENSIS CLONE FX-2251 1/6/4 79077094 CORRELATIONS AMONG 9 CHARACTERS OF RUBBER TREE HEVEA-SPP CLONES AT PORTO-VELHO CONDITIONS RONDONIA STATE BRAZIL 1/6/5 79077083 OF AND USE ANATOMICAL AND PHYSIOLOGICAL **QUANTIFICATION** CHARACTERISTICS OF LEAVES IN THE DETERMINATION OF HYDRIC EFFICIENCY IN CLONES OF HEVEA-SPP 1/6/6 79058560 EFFECT OF LIME AND NITROGEN PHOSPHORUS POTASSIUM FERTILIZERS ON RUBBER HEVEA YIELD IN SOUTHERN BAHIA BRAZIL

1/5/7

79058559 EFFECTS OF NITROGEN PHOSPHORUS AND POTASSIUM ADDITION ON GROWTH OF RUBBER TREE HEVEA-BRASILIENSIS IN SOUTHERN BAHIA BRAZIL 1/6/8 79054400 REMOVAL OF IRON AND ALUMINUM INTERFERENCES IN BORGN DETERMINATION FROM SOIL EXTRACTS 1/5/9 79843893 EFFECT OF HUMIDITY AND TEMPERATURE ON THE DEVELOPMENT OF SOUTH AMERICAN LEAF BLIGHT MICROCYCLUS-ULEI OF HEVEA-BRASILIENSIS 478740 77043382 LEAF BLIGHT OF FICUS-PUMILA CAUSED BY A BASIDICMYCETE 1/6/11 79040571 PLANT TISSUES AS INDICATORS OF SOIL NUTRIENT AVAILABILITY FOR HEVEA GLASSHOUSE EVALUATIONS 1/6/12 79040570 ENDOMYCORRHIZAL FUNGI IN SOILS UNDER RUBBER HEVEA 1/5/13 79040569 COMPARATIVE STUDY OF PHOTOSYNTHESIS IN SEVERAL HEVEA-BRASILIENSIS CLONES AND HEVEA SPECIES UNDER TROPICAL FIELD CONDITIONS 1/5/14 79003988 RELATIONSHIPS BETWEEN YIELD AND CLONAL PHYSIOLOGICAL CHARACTERISTICS OF LATEX FROM HEVEA-BRASILIENSIS 1/6/15 28069450 SOME PROPERTIES OF THE HEVEA TONOPLAST ATPASE 1/6/16 28069445 CHARACTERIZATION OF TONOPLAST PROTON-TRANSLOCATING ATPASE FROM HEVEA LATEX-PRODUCING CELLS A COMPARATIVE STUDY 1/6/17 28057422 THE CONTROL OF THE CYTOSOLIC HOMEOSTASIS BY TONCPLAST AND VACUOLES IN THE LATEX-PRODUCING CELLS FROM HEVEA-BRASILIENSIS 1/6/18 28069421 ETHYLENE STIMULATION OF THE ATP-DEPENDENT TRANSTONOPLASTIC PROTON FLUXES IN HEVEA LATEX-PRODUCING CELLS 1/6/19 28069337 CITRATE TRANSPORT BY HEVEA TONOPLAST VESICLES ENERGIZATION OF TRANSLOCATOR AND MECHANISM OF ITS FUNCTION AS A PROTON ANTIPORTER 1/6/20 28012564 RUBBER HEVEA 1/6/21 28009182 NEW CROPS FOR ARID LANDS 1/6/22 28006818 PHYTOPHTHORA-SPP IN CHINA 1/6/23 78090458 WOODY BIOMASS OF FOREST STANDS 1/6/24

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78082488 AVIAN COMMUNITY STRUCTURE IN 2 MODIFIED MALAYSIAN MASITATS 1/5/25 78078733 SPECIES MATING TYPES AND PATHOGENICITY OF PHYTOPHTHORA DISTRIBUTED IN CITRUS ORCHARDS IN TAIWAN 1/6/25 78078554 PHYTOFHTHORA-SPP FROM RUBBER TREE HEVEA-BRASILIENSIS PLANTATIONS IN YUNNAN PROVINCE OF CHINA 1/6/27 78070854 PURIFICATION AND CHARACTERIZATION OF HEVAIN A SERINE PROTEASE FROM HEVEA-BRASILIENSIS 1/6/28 78065895 MORPHOGENETIC STUDY OF THE CROWN SHAPE OF WIND SUSCEPTIBLE AND RESISTANT CLONES OF HEVEA-BRASILIENSIS 1/6/29 78056374 ZERO GRAZED PASTURE UNDER IMMATURE HEVEA RUBBER PRODUCTIVITY OF SOME GRASSES AND GRASS LEGUME MIXTURES AND THEIR COMPETITION WITH HEVEA 1/6/30 78054700 FRACTIONATION OF HEVEA-BRASILIENSIS LATEX ON FICOLL DENSITY GRADIENTS 1/6/31 78045778 EVIDENCE FOR GLUTATHIONE REDUCTASE EC-1.6.4.2 ACTIVITY IN THE CYTOSOL FROM THE LATEX OF HEVEA-BRASILIENSIS 1/6/32 78042976 THE SAPONINS CONTENT OF SOME NIGERIAN OIL SEEDS 1/6/33 78035478 GENETIC AND PHENOTYPIC CORRELATIONS BETWEEN SOME QUANTITATIVE TRAITS IN JUVENILE CLONAL RUBBER TREES HEVEA-SPP 1/6/34 78033031 TAXONOMY OF PHYTOPHTHORA-SP ISOLATED FROM RUBBER HEVEA-BRASILIENSIS IN SRI-LANKA 1/6/35 78027421 A BASIS FOR SELECTING HEVEA CLONES STABLE TO UNPREDICTABLE AGRO CLIMATIC VARIABILITY 1/6/36 78022506

SENSITIVITY OF TONOPLAST BOUND ATPASE FROM HEVEA-BRASILIENSIS TO INHIBITORS 1/6/37 78014714

CHEMICAL COMPOSITION AND NUTRITIONAL VALUE OF PARA RUBBER HEVEA-BRASILIENSIS SEED AND ITS PRODUCTS FOR CHICKENS 1/6/38 78014457

GLUTATHIONE S TRANSFERASE EC-2.5.1.18 FROM HEVEA-BRA CONSISTED 1/6/39

77091692

GENETIC PARAMETERS IN RUBBER TREES HEVEA-SPP UNDER NURSERY SEEDLING CONDITIONS

1/6/40

77091588 YIELD RESPONSE OF RUBBER HEVEA-BRABILIENSIS TO FEFTILIZERS ON AN ULTISOL IN NIGERIA 1/5/41 77091225 PAPER INDUSTRY STUDY OF THE MIXTURE OF LEFTOVER ROLLS BY PLYWCOD FACTORIES IN THE STATE OF AMAZONAS BRAZIL 176742 77075349 RHIZOBIUM INOCULATION OF CALOPOGONIUM-CAERULEUM 1/5/43 77073121 NOTES FROM THE HERBARIUM 1 1/6/44 77072576 THE INFLUENCE OF PROCESSING AND STORAGE ON HYDROGEN CYANIDE AND TANNIN CONTENTS OF PARA RUBBER HEVEA-BRASILIENSIS SEED AND ITS PRODUCTS 175745 77062529 THE KINETICS OF THE INFECTION OF HEVEA-BRASILIENSIS PLANTS BY RIGIDOPORUS-LIGNOSUS 175/45 77022566 0F INCLULATION YOUNG PLANTS QF HEVEA-BRASILIENSIS RY RIGIDOPORUS-LIGNOSUS AND PHELLINUS-NOXIUS 1/6/47 27081757 REGIONAL ASIAN COLLABORATION IN PLANT QUARANTINE 1/6/48 27068244 EVALUATION OF POTENTIAL FEED INGREDIENTS OF TROPICAL ORIGIN IN POULTRY DIETS 1/5/49 27058170 THE PATTERN OF LATEX FLOW FROM RUBBER TREE HEVEA-BRASILIENSIS IN RELATION TO WATER STRESS 1/5/50 27067538 ROLE OF THE LUTOIDIC TONOPLAST IN THE SENESCENCE AND DEGENERATION OF THE LATICIFERS OF HEVEA-BRAGILIENSIS 1/5/51 27067505 COMPARISON OF HEVEA-BRASILIENSIS TONOPLAST ATPASE FROM FRESHLY ISOLATED VACUOLES AND LYOPHILIZED TONOPLAST VESICLES 1/6/52 27067491 ISOLATION PURIFICATION AND SUBUNIT STRUCTURE OF PROTON TRANSLOCATING ATPASE FROM HEVEA LATEX 1/6/53 27057490 EFFECT OF CHEORIDE ON TONOPLAST BOUND ATFASE FROM HEVEA LATEX 1/6/54 27067489 EFFECT OF NIGERICIN ON TONOPLAST BOUND ATPASE FROM HEVEA LATEX 1/6/55 27063575 ROLE OF THE LUTOIDIC TONOPLAST IN THE CONTROL OF THE CYTOSOLIC HOMEOSTASIS WITHIN THE LATICIFEROUS CELLS OF HEVEA-BRASILIENSIS 1/6/56 27054350

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FATTERN OF LATEX FLOW DURING TAPPING OF A RUBBER TREE THE HEVEA-BRASILIENSIS 1/6/57 27019724 PHYSIOLOGICAL REGULATION OF PHOSPHOENOL PYRUVATE CARBOXYLASE EC-4.1.1.31 FROM A NONCHLOROPHYLLIAN SYSTEM THE HEVEA-BRASILIENSIS LATEX 1/5/58 26074873 CHARACTERIZATION OF TONOPLAST ATPASE AND THE VACUOLAR PROTON PUMP OF HEVEA LATEX 1/6/59 26058145 THE IMPORTANCE OF LEGUME COVER CROP ESTABLISHMENT FOR CULTIVATION OF RUBBER HEVEA-BRASILIENSIS IN MALAYSIA 175760 26048751 DEVELOPMENT OF MIXED TREE AND FOOD CROP SYSTEMS IN THE HUMID TROPICS A RESPONSE TO POPULATION PRESSURE AND DE FORESTATION 1/6/61 26026514 ASSOCIATION 0F FUSARIUM-SOLANI WITH ROOT LESIONS OF RUBBER HEVEA-BRASILIENSIS SHOWING LEAF WILT IN SRI-LANKA 1/6/62 76090935 AN ENDOGENOUS NADPH DEPENDENT ENZYMATIC ACTIVITY RESPONSIBLE FOR THE PER OXIDATIVE DEGRADATION OF ORGANELLE MEMBRANE AND FOR THE EARLY AS WELL AS IN-SITU COAGULATION OF THE LATEX OF HEVEA-BRASILIENSIS 1/6/63 76086838 RELATIVE EFFICACY OF SOME ANTI FEEDANTS AND DETERRENTS AGAINST INSECT PESTS OF STORED PADDY 1/5/64 76075366 LABORATORY INVESTIGATIONS ON FUNGICIDES AND BIOLOGICAL AGENTS TO CONTROL 3 DISEASES OF RUBBER HEVEA-BRASILIENSIS AND OIL PALM AND THEIR POTENTIAL APPLICATIONS 1/6/65 76067914 EVIDENCE FOR AN ELECTROGENIC ATPASE IN HEVEA TONOPLAST VESICLES 1/5/66 76067758 SYSTEM TO EVALUATE OF THE INCIDENCE OF THE TARGET SPOT A. THANATEPHORUS-CUCUMERIS IN RUBBER TREE HEVEA-SPP 1/6/67 76044827 A TRANS TONOPLASTIC PROTON EFFLUX COUPLED TO ELECTRON TRANSPORT THE NADH CYTOCHROME C OXIDO REDUCTASE IN THE MEMBRANE OF THE VACUO LYSOSOMES FROM THE LATEX OF HEVEA-BRASILIENSIS/s 1/6/68 76036917 AN ALKALINE PROTEASE INHIBITOR FROM HEVEA-BRASILIENSIS LATEX 1/6/69 76033848 PREDICTION OF GENETIC GAIN FOR SOME RUBBER TREE CHARACTERS UTILIZING 3 DIFFERENT SCHEMES OF SELECTIONS 1/6/70 76029274 3 HYDROXY-3-METHYL GLUTARYL COENZYME A REDUCTASE EC-1.1.1.34 OF HEVEA-BRASILIENSIS LATEX THE OCCURRENCE OF A HEAT STABLE ACTIVATOR IN

THE C SERUN/V

475771 76029115 OCCURRENCE OF FUNGI IN RUBBER HEVEA-BRASILIENSIS SEEDS 1/6/72 76029078 CHEMICAL DEFOLIATION OF HEVEA-SPP BY THERMAL FOGGING 1/6/73 76021547 HOST PARASITE INTERACTIONS BETWEEN HEVEA-BRASILIENSIS AND THE ROOT ROTTING FUNGI PHELLINUS-NOXIUS AND RIGIDOPORUS-LIGNOSUS COMPARATIVE PHYSIO PATHOLOGICAL STUDY 1/6/74 76021527 ULTRASTRUCTURAL STUDIES OF PHLOEM DEGRADATION OF HEVEA-BRASILIENSIS ROOTS INFECTED WITH RIGIDOPORUS-LIGNOSUS 1/6/75 76018419 THE BIOLOGICAL EFFECTS OF THE COMMUNITY STRUCTURE OF 1 ARTIFICIAL RUBBER HEVEA-BRASILIENSIS FOREST WITH THE STUDIES OF THE VARIATION REGULARITY OF SOME ECOLOGICAL FACTORS 1/6/76 76013656 HYDROXYMETHYL GLUTARYL COENZYME A REDUCTASE NADPH EC-1.1.1.34 IN THE LATEX OF HEVEA-BRASILIENSIS 1/6/77 75090977 IN-VITRO MICRO CUTTING OF HEVEA-BRASILIENSIS PLANTS 1/6/78 75090884 ON THE LYSOZYME AND COMPONENTS OF MICRO HELICES OF STUDIES HEVEA-BRASILIENSIS LATEX 1/6/79 75090763 FUNGAL BIOMASS AND LACCASE ACTIVITY IN RUBBER TREE ROOTS INFECTED BY RIGDOPORUS-LIGNOSUS 1/5/80 75088042 PHYSIOLOGICAL AND ANATOMICAL INVESTIGATIONS ON LONG-TERM ETHEPHON STIMULATED TREES 1/6/81 75080305 SUCROSE SYNTHETASE EC-2.4.1.13 IN THE LATEX OF HEVEA-BRASILIENSIS 1/6/82 75072494 EFFECTS OF DIFFERENT SPACINGS ON THE ALLOMETRIC GROWTH OF RUBBER HEVEA-SPP NURSERY SEEDLINGS 1/5/83 75072486 EFFICIENCY OF MENDES EARLY TAPPING TEST IN RELATION TO HAMAKER MORRIS MANN IN RUBBER TREE HEVEA-SPP SELECTION 1/6/84 75071955 PRESERVATIVE TREATMENT OF RUBBER WOOD HEVEA-BRASILIENSIS BY PRESSURE IMPREGNATION CHEMICAL AND BIOLOGICAL EVALUATIONS 1/6/85 75067677 ARRHENIUS PLOT CHARACTERISTICS OF MEMBRANE BOUND 3 HYDROXY-3-METHYL COENZYME REDUCTASE EC-1.1.1.34 FROM THE LATEX OF GLUTARYL A HEVEA-BRASILIENSIS/s 1/6/86

75067487

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STUDIEB ON THE PLANT WEMATORES IN SOUTH RUJIAN CHINA C. THE SPECIES OF RHABDITIDA 1/6/87 75064725 CHARACTERIZATION OF LEAF AREA INDEX AND CANOPY LIGHT PENETRATION OF HEVEA-BRASILIENSIS BY HEMISPHERICAL PHOTOGRAPHY 1/6/88 75064147 OF. **RUBBER** SOME STUDIES 0N FUNGAL DETERIORATION 4000 HEVEA-BRASILIENSIS 1/6/89 75049244 ORGANOGENESIS IN THE APICAL MERISTEM OF HEVEA-SP 1/5/90 75048217 EVALUATION OF DAMAGE CAUSED BY CATERPILLAR ERINNYIS-ELLO IN HEVEA STOCK NURSERY 1/6/91 75041786 ASSESSMENT OF THE PERFORMANCE OF RUBBER CLONES HEVEA-SPP UTILIZING THE SELECTION INDEX METHOD 1/5/92 75041780 EXPERIMENTAL AND ECOLOGICAL STUDIES ON THE RUBBER HEVEA-BRASILIENSIS TEA CAMELLIA-SINENSIS-VAR-ASSAMICA ARTIFICIAL COMMUNITY 1/6/93 75033959 FINE ROOTS IN MIXED PLANTATIONS OF HEVEA HEVEA-BRASILIENSIS AND CACAO THEOBROMA-CACAO 1/6/94 75027105 INTERSPECIFIC CROSSES IN THE GENUS HEVEA A PRELIMINARY PROGENY TEST OF SOUTH AMERICAN LEAF BLIGHT RESISTANT DWARF HYBRIDS 1/6/95 75026966 STUDIES ON THE PLANT NEMATODES IN SOUTH FUJIAN CHINA 1. THE SPECIES OF TYLENCHIDA 1/5/95 75021295 PHYSIOLOGICAL ACTIVATORS OF INVERTASE FROM HEVEA-BRASILIENSIS LATEX 1/5/97 75018288 REPEATABILITY OF COEFFICIENT AND EFFICIENCY OF MICRO TAPPING TEET IN SEEDLINGS OF RUBBER TREE HEVEA-SP 1/5/98 75010554 PHYSIOLOGICAL CHANGES IN HEVEA LATEX AND LATEX FLOW INITIAL CHARACTERISTICS ASSOCIATED WITH INTENSIVE TAPPING 1/6/99 75010553 CARBOHYDRATE STATUS OF EXPLOITED HEVEA 1. THE EFFECT OF DIFFERENT EXPLOITATION SYSTEMS ON THE CONCENTRATION OF THE MAJOP SOLUBLE CARBOHYDRATES IN LATEX 1/6/100 75006126 IN-VITRO POLLEN GERMINATION OF HEVEA-CAMARGOANA 1/6/101 75003156 RECENT ADV. NCES IN ANTHER CULTURE OF HEVEA-BRASILIENSIS

1/6/102

.

75003149 EFFECT OF HERBICIDE ETHIDIMURON ON RUBBER HEVEA-EFF BEEILINGE IN DIFFERENT GROWTH STAGES 1/5/103 25037718 PHOTOSYNTHESIS STOMATAL CONDUCTANCE AND LEAF WATER POTENTIAL DURING WATER STRESS SITUATIONS IN YOUNG RUBBER TREES HEVEA-BRABILIENSIE UNDER TROFICAL CONDITIONS 1/5/104 25832499 ENERGIZATION OF SOLUTE TRANSPORT AND ACCUMULATION AT THE TONOPLAST IN HEVEA-BRASILIENSIS LATEX 1/6/105 25032498 A PLANT VACUOLAR SYSTEM THE LUTOIDS FROM HEVEA-BRASILIENSIS LATEX 1/6/106 25029827 A NEW REPORT OF DIEBACK DISEASE ON HEVEA-BRASILIENSIS FROM TRIPURA INDIA 1/6/107 25019294 NEW COMBINATIONS OF YEAST FUNGI OF THE GENUS CRYPTOCOCCUS 1/5/108 24067432 ENZYMES OF HEVEA-BRASILIENSIS LATEX ADENYLATE KINASE EC-2.7.4.3 SULFATE ADENYL TRANSFERASE ATP SULFURYLASE EC-2.7.7.4 AND THIO SULFATE SULFUR TRANSFERASE RHODANESE EC-2.8.1.1/ 1/5/107 24064684 RELEASE OF BUD DORMANCY IN BUDDED STUMPS AND MAXI STUMPS USING GROWTH SUBSTANCES 1/5/110 24342389 THONNINGIA-BANGUINEA A NEW PARASITE ON RUBBER HEVEA-PEASILIENSIB SCOLE 1/6/111 2-027422 NITROGEN CYCLE IN RUBBER HEVEA-BR FUNGI OF THE GENUS CRYPTOCOCCUS 1/6/108 24067432 ENZYMES OF HEVEA-BRASILIENSIS LATEX ADENYLATE KINASE EC-2.7.4.3 SULFATE ADENYL TRANSFERASE ATP SULFURYLASE EC-2.7.7.4 AND THIO SULFATE SULFUR TRANSFERASE RHODANEER EC-2.8.1.1/ 1/5/109 24064684 RELEASE OF BUD DORMANCY IN BUDDED STUMPS AND MAXI STUMPS USING GROWTH SUBSTANCES 1/5/110 24042389 THONNINGIA-SANGUINEA A NEW PARASITE ON RUBBER HEVEA-BRASILIENSIS ROOTS 1/5/111 24027556 NITROGEN CYCLE IN RUBBER HEVEA-BROF RUBBER HEVEA-BRASILIENSIS IN NIGERIA 1/6/117 74076017 MODIFICATION OF CROWN DEVELOPMENT OF HEVEA-BRASILIENSIS BY CULTURAL PRACTICES 1. PRUNING 176/118

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EFFECTS OF SHADE COVER AND AVAILABILITY OF MIDGE BREEDING SITES IN POLLINATING MIDGE POPULATIONS AND FRUIT BET IN 2 CORDA THEORYCHA-CACAG FARMS 1/5/119 74670203 EFFECT OF RUBBER SEED OIL ON THE DEVELOPMENT AND REGRESSION OF EXPERIMENTAL ATHERO SCLEROSIS OF THE AORTA IN RAPBITS 1/5/120 74068523 EVALUATION OF RUBBER CLONES HEVEA-BRASILIENSIS DERIVED FROM THE 1ST HAND POLLINATION PROGRAM AT THE RUBBER RESEARCH INSTITUTE OF NIGERIA 1/6/121 74044153 PROTON NMR AND CARBON-13 MMR EPECTROSCOPY OF THE NONADRIDES 1/6/122 74042427 PROTON GRADIENT ACROSS THE VACUO LYSOSOMAL MEMBRANE OF LUTOIDS THE FROM THE LATEX OF HEVEA-BRASILIENSIS 1. FURTHER EVIDENCE FOR A PROTON TRANSLOCATING ATPASE ON THE VACUO LYSOSOMAL MEMBRANE OF INTACT LUTOIDS/o 1/5/123 74039395 PRELIMINARY RESULTS OF RUBBER TREE HEVEA-SP CLONES REHAVIOR IN THE ECOLOGICAL CONDITIONS OF MANAUS BRAZIL 1/6/124 74032069 HEVEA CLONES BEHAVIOR AT THE EDGE OF THE TAPAJOS RIVER BRAZIL 1/6/125 74027573 FURTHER EVIDENCE FOR THE PROTON PUMPING WORK OF TONOPLAST ATPASE FROM HEVEA LATEX VACUOME 1/6/126 74007518 EVALUATION OF 7 HEVEA CLONES IN RELATION TO THE RESISTANCE AGAINST SOUTH AMERICAN LEAF BLIGHT MICROCYCLUS-ULEI 1/6/127 74016945 SCREENING OF PRESERVATIVES AGAINST SAP STAIN AND MOLD FUNGI FROM TROPICAL HARDWOODS LABORATORY TESTS AGAINST ISOLATES FROM 1. RUBBERWOOD HEVEA-BRASILIENSIS 1/5/128 74005973 THE ELECTROCHEMICAL PROTON GRADIENT AND ITS INFLUENCE ON CITRATE UPTAKE IN TONOPLAST VESICLES OF HEVEA-BRASILIENSIS 1/6/129 74005719 ULTRASTRUCTURE OF MINERAL DEFICIENT LEAVES OF HEVEA 3. QUANTITATIVE CONSIDERATIONS 1/6/130 74002973 VIABILITY TEST ON HEVEA SEEDS BY THE TETRAZOLIUM METHOD 1/5/131 73057027 THE EFFECT OF MOISTURE AND TEMPERATURE ON THE ULTRASTRUCTURE AND VIABILITY OF SEEDS OF HEVEA-BRASILIENSIS 1/6/132 73039036 PLOIDY IN THE PROCESS OF ANTHER CULTURE OF HEVEA-BRASILIENSIS/ 1/6/133 73025182 THE PROTONMOTIVE POTENTIAL DIFFEPENCE ACROSS THE VACUO LYSOSOMAL

MEMBRANE OF MEVEA-BRASILIENSIB RUBBER TREE NACITE MODIFICATION BY A MEMBRANE BOUND ATPAGE 1/6/134 73031502 PRESERVATIVE TREATMENT OF RUBBER WOOD HEVEA-BRASILIENSIS BY PRESSURE IMPREGNATION CHEMICAL AND BIOLOGICAL EVALUATIONS 1/6/135 73020373 LATICIFEROUS ÛF SPECIES OF THE FRIMARY SYSTEM OF ONTOGENY. HEVEA-BRASILIENSIS AN ULTRASTRUCTURAL AND CYTOCHEMICAL STUDY 1/6/136 73002783 EARLY EXPLOITATION OF HEVEA RUBBER TREES SY PUNCTURE AND SHORT-OUT TAPPINGS 1/5/137 23035194 NUTRIENT CHARACTERIZATION OF SOME TROPICAL FEEDSTUFFS 1/5/133 23013948 IN-VITRO PROPAGATION OF LATEX PRODUCING PLANTS 1/5/139 23012037 CONVERSION OF LINOLEIC-ACID AND LATEX FURANCID ACID TO FISH 18 CARBON DI METHYL FURANOID ISOMERS 1/5/140 22063123 GOSSYPOL IN RUBBER SEED MEAL 1/5/141 22060942 EFFECTS OF PLANTING DENSITY ON YIELD GROWTH CROWN FORMS AND OTHER TREE CHARACTERISTICS IN HEVEA-BRASILIENSIS 1/6/142 22862668 POPULATION PRESSURE AND LAND USE CHANGE FROM TREE CROPS TO SAWAH IN NORTHWESTERN KALIMANTAN INDONESIA 1/6/143 72083559 THANATEPHORUS-CUCUMERIS FELLICULARIA-FILAMENTOSA ON RUBBER SEEDLINGS GROWING IN NURSERIES IN FELIXLANDIA MINAS-GERAIS PRAZIL 1/5/144 72073543 ASPECTS OF ECOLOGIC ANATOMY OF THE LEAVES OF HEVEA-BRASILIENSIS 1757145 72073522 INDUCED FLOWERING IN YOUNG HEVEA BUDDINGS 1/6/146 72073521 VARIATIONS IN LEAF MORPHOLOGY AND ANATOMY BETWEEN CLONES OF HEVEA 1/6/147 72062103 PATHOGENICITY OF SOME PHYTOPHTHORA-PALMIVORA ISOLATES ON DIFFERENT HOSTS 1/6/148 72059492 POSSIBILITIES OF EARLY SELECTION IN HEVEA-BRASILIENSIS 1/6/149 72054954 ETIOLOGY OF RHODODENDRON-MAXIMUM DIEBACK CAUSED BY 4 SPECIES OF PHYTOPHTHORA 1.3.120

CHEMICAL 20NTRIL := RHODODENDEDA 0153404 140351 3.1 PHYTOPHTHOPA-HEVEAE 1.4/151 72046351 OCCURRENCE OF REACTION WOOD IN BRANCHES OF DICOTYLEDONS AND ITS POLE IN TREE ARCHITECTURE 1/6/152 71033415 HISTOLOGICAL ASPECTS OF BROWN BAST DISEASE IN HEVEA-BRASILIENSIS 1/6/153 71080837 RUBBER PARTICLE STABILITY AS FACTORS STABILITY AND LUTOID INFLUENCING YIELD DURING DROUGHT IN RUBBER HEVEA-BRASILIENSIS 175/154 71074265 TUCKERELLA-ORNATA A MITE NEW FOR BRAZIL AND OTHER TETRANYCHOIDEA ACARI FROM THE STATE OF PARA 1/6/155 71065525 THE CONDUCTING PHLOEM IN RELATION WITH THE EXPROPRIATION OF LATEX IN HEVEA-BRASILIENSIS 1/6/155 71045285 FACTORS INFLUENCING THE COLLOIDAL STABILITY OF FRESH CLONAL HEVEA LATICES AS DETERMINED BY THE AEROSOL OT TEST 1/6/157 71043842 ISOLATION AND CHARACTERIZATION OF MICRO HELICES FROM LUTOIDS OF HEVEA LATEX 1/6/158 71038389 FUSION OF PROTOPLASTS OF HEVEA-BRASILIENSIS AND HEVEA-PAUCIFLORA ELABORATION OF TECHNIQUE 1/8/157 71033819 DISTRIBUTION OF PROTEINS BETWEEN THE FRACTIONS OF HEVEA-LATEX SEPARATED BY ULTRA CENTRIFUGATION 1/6/16071031214 IBOLATION OF HEVEA PROTOPLASTS 1/6/161 71031213 SOIL MOISTURE USE AND GROWTH OF YOUNG HEVEA-BRASILIENSIS AS DETERMINED FROM LYSIMETER STUDIES 1/6/152 71027032 CYTOPLASMIC PHOSPHATASE FROM THE LATEX OF NEUTRAL A HEVEA-BRASILIENSIS 1/6/163 71007322 EFFECT OF FEEDING PUBBER BEED CAKE TO GROWING CALVES ON DRY MATTER AND NUTRIENTS UTILIZATION 1/6/164 71005651 AUTOMATED DETERMINATION OF SULFUR IN HEVEA AND ASSOCIATED COVER PLANTS 1/6/165 71005640 ULTRASTRUCTURE OF MINERAL DEFICIENT LEAVES OF HEVEA 2. EFFECTS OF MICRO NUTRIENT DEFICIENCIES

2

L o lip

71003798 FUNCTIONAL ORGANIZATION OF THE BARK OF HEVEA-BRASILIENSIS RUBBER TREE A STRUCTURAL AND HISTO ENZYMOLOGICAL STUDY 1/5/167 21055437 THE NIGERIAN MOIST FORESTS AN ARGUMENT FOR BASIC SYSTEMATIC RESEARCH 1/6/168 21041171 PLANT PARASITIC FUNGI OF GORAKHPUR INDIA 23 1/6/169 21008788 ETIOLOGY AND CONTROL OF RHODODENDRON DIEBACK CAUSED BY PHYTOPHTHORA-SPP 1/6/170 20012216 COMMONWEALTH MYCOLOGICAL INSTITUTE DESCRIPTIONS OF PATHOGENIC FUNGI AND BACTERIA

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File E5:813818 Proviews - 0977 orm. 0983 (Capr. 819818 1980) 17571 70032049 FUNGAL FLORA OF A RUBBER PLANTATION SOIL IN RELATION TO CERTAIN EDAPHIC FACTORS 1/3/2 70074193 A COMPARISON OF A2SCISSION OF RUSSER HEVEA-BRASILIENSIE LEAVES WITH MICROCYCLUS-BLEI WITH LEAF ABBCIEBICN INCOCO BY INFECTED ETHYLENE TREATMENT DE BLADING AND SENESCENCE 1/5/3 70071417 THE STUDIES ON EC0 PHYSIOLOGICAL INDICES OF RUBBER TREES HEVEA-BRASILIENSIS AT CHILLING TEMPERATURE 1/5/4 70062053 RUBBER SEED MEAL AS A PROTEIN SUPPLEMENT IN GROWING SWINE RATIONS 1/6/5 70053527 THE RELATIONSHIP OF PHENOLS AND OXIDATIVE ENZYMES WITH THE RESISTANCE OF HEVEA-BRASILIENSIS TO SOUTH AMERICAN LEAF BLIGHT 1/5/5 70050942 THE USE OF SELECTION INDEX IN RUBBER TREES 1/5/7 70049778 PRINCIPAL INDICATOR GROUPS IN THE FLORA OF ADVENTITIOUS PLANTS FROM HEVEA CULTURE AT THE EXPERIMENTAL STATION OF ANGUEDEJOU IVORY-COAST 1/6/8 70046731 MODIFICATION OF PH OF LATEX HEVEA-BRASILIENSIS CYTOPLASM BY ETHYLENE 1/5/9 70043912 VEGETATIVE GROWTH OF RUBBER TREE HEVEA-SP CLONES 175/10 70043911 FLUCTUATIONS OF REST AND ACTIVITY PERIODS IN THE INTERMITTENT GROWTH OF RUBBER TREE NURSERY SEEDLINGS 1/6/11 70043908 SEED GRAFTING OF HEVEA 1. POTENTIAL VIABILITY PRELIMINARY RESULTS 1/5/1270038004 CELLS LATEX VESSELS IN SECONDARY FHLOEM OF TANNIN AND HEVEA-BRASILIENSIS 1/6/13 70029382 STUDIES ON THE SUCCESSION OF PHYLLOPLANE MICRO FLORA OF DEVELOPING LEAVES OF HEVEA PUBBER 1.5/14 70029315 DIPLOPOD STUDY MYRIAPOD POPULATIONS FROM A COMPARATIVE ÛF HYGROPHILOUS FOREST AND FROM A HEVEA PLANTATION IN LOWER IVORY-COAST 1/6/15 70025223 EFFECT OF POTASSIUM AND ALUMINUM TREATMENTS ON GROWTH AND NUTRIENT UPTAKE OF RUBBER HEVEA SEEDLINGS AND ON SOILS 1/6/16 70019393 THE DEVELOPMENT OF PHOTOSCUPETIC PATE WITH LEVE AGE 11

HEVEA-BRASILIENSIS CLONAL SEEDLINGS ETHYLENE FORMATION IN EXCISED HEVEA BARK DISCS REGULATION OF IAA OXIDASE ACTIVITIES IN HEVEA-BRASILIENSIS LEAVES BY NATURALLY OCCURRING PHENOLICS INDUCTION AND CONTROL OF FLOWERING IN HEVEA-BRASILIENSIS VARIATIONS IN STIMULATION RESPONSE IN YIELD OF A HEVEA-BRASILIENSIS CLONE 1 COMPONENT VARIANCE MODEL EFFECTS OF INTERSTOCK ON GROWTH OF HEVEA HORMONAL REGULATION OF SEXUAL REPRODUCTION IN PHYTOPHTHORA ULTRASTRUCTURE OF MINERAL DEFICIENT LEAVES OF HEVEA 1. EFFECTS OF MACRO NUTRIENT DEFICIENCIES

1/5/24 70009470

1/6/17 70019316

1/5/18 70019159

1/5/19 70015468

1/6/20 70015467

1/6/21 70015455

1/6/22 70012402

1/6/23 70012154

A BIOMETRICAL APPROACH TO STUDY CROWN TRUNK RELATIONSHIPS TN HEVEA-SPRUCEANA 1/6/25

70009469

COPPER ZINC MANGANESE IRON AND ALUMINUM CONTENTS OF SOILS COMMONLY USED FOR HEVEA-BRASILIENSIS CULTIVATION 1. DISTRIBUTION WITHIN SOIL PROFILES 1/6/25

70009468

STIMULATION OF LATERAL ROOT PRODUCTION AND BUD BREAK WITH GROWTH REGULATORS IN HEVEA BUDDED STUMPS 1/6/27

70009467

HERITABILITIES OF & BIOMETRICAL CHARACTERS OF SINGLE PAIR MATING FAMILIES IN HEVEA-BRASILIENSIS 1/5/28

70009466

DAILY VARIATIONS IN YIELD AND DRY RUBBER CONTENT IN 4 HEVEA CLONES 1/6/29

70009462

HEVEA RUBBER PAST AND FUTURE 1/6/30

70009461

COMPARATIVE ANATOMY BETWEEN DI PLOID AND POLY PLOID LEAVES OF THE HYBRID HEVEA-BRASILIENSIS-X-HEVEA-BENTHAMIANA 1/6/31

69075183

PROPERTIES AND GEOMORPHIC RELATIONSHIPS OF SOME SOILS OF LIBERIA 1/6/32

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69057945 VARIATION IN STIMULATION RESPONSE IN YIELD OF A HEVEA CLONE 2. A REGRESSION MODEL

1/6/33 69057944

EFFECTS OF BUD TYPES ON EARLY SCEDY GROWTH OF HEVEN 1/8/34 37035375 MICROSCOPE STUDIES OF ODGONIAL WALL AND ELEMENTAL ELECTRON COMPOSITION OF COGONIA IN PHYTOPHTHOPA 175735 59034468 CONTACT URTICARIA TO FUEEER 1/5/35 59033046 0F HEVEA-BRASILIENSIS LEAVES T0 -INFECTION REACTION WITH MICROCYCLUS-ULEI 1/5/37 69032979 OCCURRENCE OF CRINULA-CALICIIFORMIS IN THE AMAZON REGION BRAZIL REGION 1/3/38 69016643 CLONAL VARIABILITY FOR STOMATAL CHARACTERS AND ITS APPLICATION IN HEVEA-BRASILIENSIS BREEDING AND SELECTION 1/6/39 19049933 AN EASY SYNTHESIS OF MUCO INOSITOL 1/6/40 19039935 DIFFERENCES IN STOMATAL DENSITY DIMENSION AND CONDUCTANCES TO WATER VAPOR DIFFUSION IN 7 HEVEA SPECIES 176741 19039665 POLY ISOPRENE 1/5/42 18056024 RELATIONSHIP BETWEEN LEAF AGE AND SOME CARBON DI DAICE EXCHANGE CHARACTERISTICS OF 4 HEVEA-BRASILIENSIS CLONES 176743 18047193 PLANTS AND DRUGS OF STOMATOLOGICAL INTEREST 1/5/44 18037854 THE NATURE OF AMPHIGYNY IN PHYTOPHTHORA 1/6/45 16039154 RHODODENDRON DIEBACK CAUSED BY PHYTOPHTHORA-HEVEAE 1/5/45 18031474 MOVEMENT AND TADPOLE ARBOREAL CARRYING BEHAVIOR 0F DENDROBATES-PUMILIO DENDROBATIDAE IN NORTHEASTERN COSTA-RICA 1/6/47 18028745 HISTOLOGICAL AND BICCHEMICAL STUDIES ON SOUTH AMERICAN LEAF BLIGHT MICROCYCLUS-ULEI OF HEVEA-SPP 1/6/48 18018855 PHENOLIC COMPOUNDS OF THE LATEX OF HEVEA-BRASILIENSIS AGLYCONES/ 1/6/49 18018727 ON THE OCCURRENCE AND EFFECT OF NEMATODE INFESTATION IN RUBBER HEVEA-BRASILIENSIS PLANTATIONS IN INDIA 1/6/50 1.363 3975 RETROLEUM FLANTATIONS FOR FUEL AND MATERIALS

1/6/51 66053425 PHOTOSYNTHETIC RATES AND DIFFUSION RESISTANCES 0F 7 HEVEA-BRASILIENSIS CLONES 1/6/52 68056604 THE OCCURRENCE OF A FURANOID FATTY-ACID IN HEVEA-BRASILIENSIS LATEX 1/6/53 66050547 PHOTOSYNTHESIS AND DIFFUSION RESISTANCE TO CARBON DI OXIDE IN HEVEA-BRASILIENSIS CLONES 1/6/54 58043931 METABOLISM OF 2 CHLOROETHYL PHOSPHONIC-ACID ETHEPHON IN SUSPENSION CULTURES OF HEVEA-BRASILIENSIS/ 1/6/55 68037453 A PROCESS OF OBTAINING POLLEN PLANTS OF HEVEA-BRASILIENSIS 1/6/56 68031053 MATING TYPES OF PHYTOPHTHORA-PALMIVORA PHYTOPHTHORA-NICOTIANAE-VAR--PARASITICA AND PHYTOPHTHORA-BOTRYOSA IN THAILAND 1/6/57 68006531 RESPONSE OF SOYBEAN TO DOLOMITIC LIME RATES AND PHOSPHORUS SOURCES ON MALAYSIAN SOILS 1/6/58 58005181 EFFECT ÛF HILLING TEMPERATURE ON PLANT METABOLISM 0F HEVEA-BRASILIENSIS 1/6/59 68002908 ESTIMATES 0F PARENTAL COMBINING ABILITIES IN RUPBER HEVEA-BRASILIENSIS BASED ON YOUNG SEEDLING PROGENY 1/5/60 57059581 STRUCTURE AND PROPERTIES OF A 2 CHLOROETHYL PHOSPHONIC-ACID ETHEPHON METABOLITE FROM HEVEA-BRASILIENSIS BARK 1/6/51 67057133 DEVELOPMENT OF LEAF BLADE CLASS CONCEPT FOR THE CHARACTERIZATION OF HEVEA-BRASILIENSIS LEAF AGE 1/6/62 67067132 DISTRIBUTION AND CONCENTRATION OF MAJOR SOLUBLE CARBOHYDRATES IN HEVEA LATEX THE EFFECTS OF ETHEPHON STIMULATION AND THE POSSIBLE ROLE OF THESE CARBOHYDRATES IN LATEX FLOW 1/6/63 67054224 NET PHOTOSYNTHESIS OF 4 HEVEA-BRASILIENSIS CLONAL COMPARATIVE SEEDLINGS 1/6/64 57049890 MEDICINAL PLANTS IN THE PAST TODAY AND TOMORROW 1/5/65 67039388 A NEW INFRAGENERIC CLASSIFICATION OF HEVEA PART 1 HISTORICAL CONSIDERATIONS ON INFRAGENERIC CLASSIFICATIONS 1/6/66 67035115 DEMONSTRATION OF LATEX COAGULANTS IN BARK EXTRACTS OF HEVEA AND

THEIR POSSIBLE ROLE IN LATEX FLOW 1/5/57 67035114 RESIDUAL EFFECT OF APPLIED PHOSPHATES ON PERFORMANCE OF HEVEA-BRASILIENSIS AND PUERARIA-PHASEOLOIDES 1/5/68 67033641 FURTHER STUDIES ON THE OCCURRENCE AND DISTRIBUTION OF MICRO HELICES IN CLONES OF HEVEA 1/6/69 67028319 2 INDICES TO QUANTIFY LATEX FLOW CHARACTERISTICS IN HEVEA-BRASILIENSIS 1/6/70 67026532 A NEW CANKER DISEASE OF AVOCADO CAUSED BY PHYTOPHTHORA-HEVEAC NEW-RECORD 1/6/71 57017843 EVALUATION OF FUNGICIDES FOR CONTROL OF SOUTH AMERICAN LEAF BLIGHT OF HEVEA-BRASILIENSIS 475772 67015526 ASSESSMENT OF PARENTAL PERFORMANCE FOR YIELD IN HEVEA BREEDING 1/6/73 67015132 INVESTIGATIONS ON INDIGENOUS SUBSTITUTES FOR IMPORTED HORNBEAM CARPINUS-SP FOR MAKING COTTON LOOM SHUTTLES 1/6/74 57005113 LEAF BLIGHT OF HEVEA-BRASILIENSIS CULTURE OF SOUTH AMERICAN MICROCYCLUS-ULEI 1/6/75 57004369 HEVEA-BRASILIENSIS SEEDS FOR HUMAN NUTRITION 1/6/75 17046476 THE LUTOIDS OF HEVEA-BRASILIENSIS LATEX 1/6/77 17014688 RHODODENDRON DIEBACK CAUSED BY PHYTOPHTHORA-HEVEAE 1/6/78 16055711 INTERNATIONAL UNION OF FURE AND APPLIED CHEMISTRY REPORTS ON PESTICIDES PART 4 TERMINAL RESIDUES OF ORGANO PHOSPHORUS PESTICIDES 1/6/79 16026597 ECO PHYSIOLOGICAL ASPECTS OF HIGH DENSITY PLANTING RELATED TO HEVEA-BRASILIENSIS LATEX PRODUCTION 1/6/80 16016639 THE INFLUENCE OF RAINFALL ON YIELD OF RUBBER HEVEA-BRASILIENSIS/ 1/6/81 16015698 RUBBER 1/6/82 16007405 A MODEL OF INTACT ISOLATED VACUOLAR STRUCTURE LUTOIDS FROM LATEX OF HEVEA-BRASILIENSIS PART 2 CHARACTERISTICS OF THE LUTOID MEMBRANE/ 1/6/83 16007404

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A MODEL OF INTAUT INIGATES LACELLAS ETFLITURE LETVILS FROM LATES OF HEVEA-BRASILIENSIS FART : ATTUMULATION AND FENETRATION OF TITRATE AND L LYSINE IN THE LUTDIDS 1/5/3-16000317 PRODUCTION AND STORAGE OF RECALCITRANT SEEDS IN THE TROPICS 1/5/85 STUDIES ON APICULTURE IN SRI-LANKA PART 1 CHARACTERISTICS OF SCME 36051262 HONEYS 1/6/85 55045031 EDIBLE PLANTS NATIVE TO NORTHWESTERN AMAZONIA 4/6/87 VAPOR AND CARBON DI OXIDE DIFFUSION RESISTANCES OF 4 55035452 WATER HEVEA-BRASILIENSIS CLONAL SEEDLINGS 1/6/88 66021322 THE ROLE OF LIPIDS AND PROTEINS IN THE MECHANISM OF LATEX VESSEL PLUGGING IN HEVEA-BRASILIENSIS 1/5/89 RIBOSOMES IN THE LUTOID FRACTION EQUALS LYSOSOMAL COMPARTMENT FROM 55019870 HEVEA-BRASILIENSIS LATEX 1/5/90 66003412 NEMATODES FROM THE AMAZON REGION BRAZIL PART 1 PARASITIC AND FREE LIVING NEMATODES ASSOCIATED WITH THE RUBBER TREE HEVEA-BRASILIENSIS AND WITH THE GUARANA PAULLINIA-CUPANA-VAR-SORBILIS 1/5/91 ETHYLENE PRODUCTION BY HEVEA-BRASILIENSIS TISSUES TREATED WITH LATEX 65073156 YIELD STIMULATORY COMPOUNDS 4/6/92 DISPERSAL OF BASIDIO SPORES OF 65061013 PRODUCTION GERMINATION AND GANODERMA-PSEUDOFERREUM ON HEVEA 1/6/93 THE ETIOLOGY OF BARK CRACKING DISEASE OF HEVEA-BRASILIENSIS 45054884 1/5/94 ATPASE OF LYSOBOMAL VACUOLES LUTGIDE FROM LATEX 45029487 \_\_)≓ MEMBRANE HEVEA-BRASILIENSIS 1/6/95 55025504 MICROBIOLOGICAL DEGRADATION OF HEVEA LATEX AND ITS CONTROL 1/5/96 SOME RHIZOMIICOLOUS AND FOLLICOLOUS FUNGI OF GINGER FROM INDIA PART 65005635 2 1/6/97 ESTIMATES OF GENERAL COMBINING ABILITY IN HEVEA BREEDING AT THE 65001948 RUBBER RESEARCH INSTITUTE OF MALAYSIA PART 1 PHASES II AND IIIA 1/6/98 65001947 LATEX FLOW STUDIES PART 10 DISTRIBUTION OF METALLIC IONS BETWEEN PHASES OF HEVEN LATEX AND THE EFFECTS OF YIELD STIMULATION ON THIS 01177228U710ft

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65001946 FACTORS AFFECTING YIELD RESPONSE TO STIMULATION WITH 2 SOME CHLOROETHYL PHOSPHONIC-ACID 1/5/100 65001945 PROTEIN AND ENZYME VARIATION IN SOME HEVEA CULTIVARS 1/5/101 15047040 REPEATED OF HEVEA BY 2 CHLOROETHYL EFFECTS 0F TREATMENTS PHC3PHONIC-ACID ON LATEX POLY RIBOSOMES 1/5/102 15043506 0F FLUORESCENT LABELING METHODS IN MORPHOLOGICAL AND USE HISTOCHEMICAL STUDIES OF LATEX IN-SITU 1/6/103 15037217 IMPROVEMENT OF GROWTH RATES OF PLANT CELL CULTURES 1/5/104 15007635 AERIAL SPRAYING AGAINST SOUTH AMER. V LEAF BLIGHT OF RUBBER 1/6/105 15005377 THE ODYSSEY OF THE CUL TED RUBBER TREE 1/6/106 78024810 LACCASE AND PEROXIDASE ACTIVITY IN ROOTS OF HEVEA INFECTED WITH WHITE WOOD ROT FUNGUS LEPTC PORUS-LIGNOSUS/ 1/6/107 78022588 2 NEW NEMATODES ON RUBBER 1/6/108 78022585 PERICONIA-HEVEAE LEAF LLIGHT ON RUBBER 1/5/109 78019585 VARIATIONS OF POLY RIEOSOMES FROM HEVEA-BRASILIENSIS LATEX BY ETHREL AND OTHER TREATMENTS INCREASING LATEX FLOW 1/6/110 78007319 LIPIDS OF HEVEA-BRASILIENSIS AND EUPHORBIA-COERULESCENS 1/6/111 64059353 ACTION KINETICS OF 2 CHLOROETHYL PHOSPHONIC-ACID ON THE POLY RIBOSUMES OF THE LATEX OF HEVEA-BRASILIENSIS 1.1/112 64056900 EFFECT OF VARIOUS COVERS ON SOLL FERTILITY UNDER HEVEA-BRASILIENSIS AND ON GROWTH OF THE TREE 1/6/113 64050278 ROOT DEVELOPMENT OF HEVEA-BRASILIENSIS IN RELATION TO CLONES FEEDER AND ENVIRONMENT 1/6/114 64047263 ATPASE 0F MEMBRANOUS LYSOSOMAL VACUOLES LUTOIDS FROM HEVEA-BRASILIENSIS LATEX 1/6/115 64045063 INFLUENCE OF INITIAL RATE OF LATEX FLOW ROWS OF LATEX VESSELS AND PLUGGING INDEX ON THE YIELD OF THE PROGENIES OF HEVEA-BRASILIENSIS

DERIVED FROM CROSSES INVOLVING TUIR-I AS THE FEMALE PARENTY 1/6/116 54043515 SCME PROBLEMS ABOUT THE OCCUPRENCE OF ANA IN THE PLANT LYEOSOMAL COMPARTMENT 1/5/117 54041211 DIFFERENT ABSORPTIVE PROPERTIES OF CITPATE MALATE AND SUCCIMATE BY THE LUTOIDS OF LATEX OF HEVEA-BRASILIENSIS 1/6/118 64040333 BIOLOGICAL EVALUATION OF PARA RUBBER SEEDS HEVEA-BRASILIENSIS 1/5/119 64035121 AMINO-ACIDS BY LUTCIDS FROM THE LATEX OF ABSORPTION ÛF HEVEA-BRASILIENSIS 1/6/120 64020752 GROWTH OF NURSERY ROOTSTOCK SEEDLINGS OF HEVEA-BRASILIENSIS CULTIVAR TJIR 1 PART 2 1/5/121 64020751 SOME METHODS FOR DETERMINING LEAF AREAS IN HEVEA 1/6/122 64014546 ABSORPTION OF CITRATE BY THE LUTOIDS OF LATEX AND RUBBER PRODUCTION BY HEVEA-BRASILIENSIS 1/6/123 64000775 COMPARATIVE ENZYME PATTERNS IN CRYPTOCOCCUS-LAURENTII AND ITS TAXONOMIC VARIETIES 1/6/124 63037609 GUAYULE A RUBBER PRODUCING SHRUB FOR ARID AND SEMI ARID REGIONS 1/6/125 63032835 CONTROL OF CARBOHYDRATE METABOLISM BY ETHYLENE IN LATEX VESSELS OF HEVEA-BRASILIENSIS IN RELATION TO RUBBER PRODUCTION 1/6/126 63029015 MATING TYPES OF PHYTOPHTHORA-PALMIVORA IN MALAYSIA 1/6/127 63022955 OF HEVEA-BRASILIENSIS CLONES ΤÛ ASSESSING SUSCEPTIBILITY MICROCYCLUS-ULEI 1/5/128 63022902 SOUTH AMERICAN LEAF BLIGHT OF HEVEA-BRASILIENSIS SPORE DISPERSAL OF MICROCYCLUS-ULEI 1/6/129 53020672 DRAINAGE AREA OF THE BARK AND SOIL MOISTURE CONTENT AS FACTORS INFLUENCING LATEX FLOW IN HEVEA-BRASILIENSIS 1/6/130 63007089 COMPOSITION OF THE MEMBRANE OF LUTOIDS FROM LIPID PHOSPHO HEVEA-BRASILIENSIS LATEX 1/6/131 63001930 PHOTOSYNTHESIS AS A PESCURCE FOR ENERGY AND MATERIALS 1 6 132

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NATEC Institut für naturwissenschaftlichtechnische Dienste GmbH

Dr. G.C. Schmerse ;

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## Appendix 2 - Contacts during the field study in Sri Lanka

Rubber plantations:

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Elpitiya State plantation, Alpitiya, Sri Lanka

Igalkanda Estate, Elpitiya, Sri Lanka

Usk Valley State Plantation, Baduraliya, Latpandura, Sri Lanka

Dalkeith State Plantation, Baduraliya, Latpandura, Sri Lanka

Yatadola State Plantation, Matugama, Sri Lanka

Clyde State Plantation Tebuwana, Sri Lanka

Sri Lanka State Plantation Crop. 111 Ceylon Planters, Provident Sciety

Authorities:

Ministry of Rural Industrial Development Dr. V. Ramanathan Colombo (Additional Scretz

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Mr. P.S. de Silva (Superintendent)

Mr. D.H. Ariyaratne (Superintendent)

Mr. N. Ratwatta (Superintendent)

Mr. A.H.V. Perera (Superintendent)

Mr. A.H.N. Wlikala (Superintendent)

Mr. M.R.C. Peiris (Chairman)

Additional Scretary) Bandula S. de Silva (Director)

Dr. G.H.P. Ganegodu (Veterinary Research Institute) **Research Institutes:** \_\_\_\_\_ Rubber Research Institute of Sri Lanka Mr. S.W. Karunaratne Acting Director (Head of Rubber Chemistry & Technology Department) Dr. Mendes Ceylon Institute of Scientific and Industrial Research (CISIR) Dr. C. Wijesundera (Head of Section Oils & Fats) N. Nadarajah (Rubber Consultant) Formerly Head of Rubber Chemistry & Technology Department, RRISL Industries: \_\_\_\_\_\_ Ceylon Oils & Fats Corp. oil mill, Mr. D.S.Kalansuriya (Chairman) fats, soaps, chemicals oil mill Adamjee Lumanjee & Sons Ltd. Mr. Adamjee Lukmanjee (Director) oil mill Sedawatte Mills Mrs. Amari Deraniyagala (Director) Lever Brothers Ltd. oils, soaps Mr. A. Mangold (Chairman) Dr. I. Ismail (acting Technical Director) paints, soaps British Ceylon Corporation Mr. Jerry Perera (Production Manager) Paints & Gen. Industries Ltd. paints, soaps Mr. M.D.S. Perera (Director) paints, soaps, oils Lankem Ceylon Limited Mr. A.C. Gunasinghe (Managing Director)

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Appendix 3 - Analytical methods

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(Literature References see III, page 95, 96)

1. Acid Value [1]: Some 3 - 10 g oil is weighed to the nearest 10 mg into a 200 ml Erlenmeyer flask, dissolved in 50 ml ethanol : ether = 1 : 1 (v/v, titrated before against phenolphthalein with 0.1 N KOH) and titrated with 0.1 N KOH (phenolphthalein as indicator).

Calculation:  $AV[mg KOH/g] = \frac{56,1 \cdot ml 0,1 N KOH \cdot 0,1}{weight of oil [g]}$ 

2. Lipase screening test [2]: Principle: An aqueous suspension of the test material reacts for some hours with test kits containing esters and pH-indicators. The acids liberated cause a colour shift in the solutions which is compared with a colour scale.

With rubber seeds: 10 mg in 90  $\mu$ l H<sub>2</sub>O cleave in 4 h at 37°C:

5nmol 2-naphthyl-butyrate 5nmol 2-naphthyl-caprylate 5nmol 2-naphthyl-myristate

3. Fatty acid composition of oil: 200 mg oil is converted into fatty acid methylesters by mixing with 2 ml methanolic NaOCH<sub>3</sub>(0,25 N). After 5 - 10 min the mixture is extracted with 1 ml iso-octane and 2 ml methanol. 1 - 2  $\mu$ l of the iso-octane-phase is injected into a gaschromatograph. Gaschromatographic conditions:

column: Sil 88, 25 m, fused silica capillary temperatures: injector: 250°C column: 160 - 220°C, 2°/min detector: FID, 300°C 1

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The integrated areas of the individual fatty acid methylesters are calculated as % of the total area of all peaks.

4. Gel permeation chromatography [3]: The oils are separated on polystyrene columns. Tetrahydrofurane is used as solvent. The eluted substances are detected by a differential refractometer.

Column set for oil analysis: 3 Ultrastyragel columns with 500, 200 and 100 Å pore diameter (Waters), 1 Microgel column, 100 Å pore diameter (Chrompak).

Column set for molecular weight determination of polyisoprene: 3 Ultrastyragel columns with 100, 500 and  $10^4$  Å pore diameters, 1 micro-Styragel column  $10^3$  Å, 1 Microgel column  $10^6$  Å.

Flow rate: 1 ml/min, temp. 38°?

Calibration is done with "ol ,tyrene of known molecular weights.

Preparative GPC: Column 500 x 25 mm, Prep Gel 10  $\mu$ m, 50 Å pore diameter (Latek GmbH). 5 mg unsaponifiable from RSO, injected in 1,9 ml, were separated with THF (p.a., Merck) at a flow rate of 5 ml/min. When the high molecular material appeared, 6,5 ml were collected and evaporated. A blank run was performed without UM and 6,5 ml THF collected after the same time.

- 168 -

- 5. Assessment of polar fatty acids [4]: Fatty acids, obtained from the assessment of the UM of RSO, were esterified with methanol/BF<sub>3</sub>. Ca. 1 g of these methylesters were dissolved in 10 ml petroleum ether : ethyl ether = 87 : 13 (v/v) and given on a column of 10 g SiO<sub>2</sub> (activated at 160°C) in this solvent. Elution with 60 ml of this solvent and evaporation gave the amount of unpolar fatty acid methylester. The difference to 100 % is calculated as amount of polar fatty acid methylester.
  - 6. Unsaponifiable matter [5]: 5 g fat is hydrolized by heating with 50 ml 2 N ethanolic KOH (reflux, 1 h). The cooled solution is diluted with 50 ml H<sub>2</sub>0 and then extracted with 100 ml petroleum ether (3 times). The combined petroleum ether extracts are washed with 40 ml H<sub>2</sub>0 and 40 ml ethanol : H<sub>2</sub>0 = 1 : 1, dried with Na<sub>2</sub>SO<sub>4</sub> and evaporated. The residue is dried at  $103^{\circ}$ C to constant weight.
  - HPLC-Method for assessment of tocopherols: 20 μl of the oil were injected into the following HPLC-system:

column: Spherisorb Si 60 (Kontron), 250 x 4,5 mm solvent: Iso-octane with 0,5 % isopropanol flow rate: 1 ml/min detector: Fluorescence, Ex. 295 nm, Em. 325 nm

synthetic tocopherols are used as test substances

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8. Assessment of phospholipids [11]: The phospholipids are separated on a TLC-plate (SiO<sub>2</sub>) using the solvent mixture chloroform : acetone : methanol : acetic acid :  $H_2O$  = 10 : 4 : 2 : 2 : 1. The amount of phospholipid per spot should be equivalent to 0,1 - 3 µg P. After staining with  $J_2$ -vapor the spots are scraped off and transferred into 10 ml centrifuge-tubes (precleaned with  $H_2SO_4$  K\_2CrO\_4). 0,7 ml 70 % perchloric acid is added (saturated with ammonium molybdate) and then the tube is heated at 160°C for 1 h. After cooling 4,3 ml of a freshly prepared mixture of 2 parts 1 % ammonium molybdate solution and 3 parts of a 2 % ascorbic acid solution are added and heated at 50°C for 1 h. The centrifuged mixture then is measured in 1 cm cuvettes at 820 nm against water. The value is corrected for a blank, containing SiO<sub>2</sub> of a similar size as the spots, but free of phospholipids. Equilibration is done with KH<sub>2</sub>PO<sub>4</sub> spotted on TLC-plates and treated in the same way as the phospholipids.

- 9. Colour stability of RSO: The oil was put in a Petri disk (1 cm layer) and stored at day light (Nov. - Dec. 1985, window to the North side) for several weeks. At certain intervals the iodine colour was assessed in a colorimeter (Hellige-Colorimeter).
- 10.  $H_2O$ -determination in RSM: About 1 g sample is dried at  $120^{\circ}C$  to constant weight. The loss is calculated as water.
- 11. Fat content in RSM: 5 g samples are extracted in a Soxhlet apparatus with petroleum ether or ether for 2 h. After evaporation of the solvent the residue is calculated as fat.

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12. Soluble carbohydrates [13]: 5 g of the finely ground RSM is mixed in a mortar with 12 ml of a 1 % HgCl<sub>2</sub>-solution. After dilution with water to 200 ml, the mixture is heated to 50°C for 20 min. At room temperature 5 ml phosphoric acid (20 ml

85 % H<sub>3</sub>PO<sub>4</sub> diluted to 1 1) is added, which is afterwards neutralised by a saturated aqueous solution of Ba(OH)<sub>2</sub>. Then the slightly alkaline mixture is filled up to 250 ml with water and filtered. 50 ml (~ 1 g RSM) are evaporated in a platinum vessel and dried at 103 - 105°C (weight a). After weighing, the residue is ashed at 800°C (weight b). In a separate sample of the water solution the N-content is assessed by the Kjeldal method.

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Calculation: \$ soluble carbohydrates = (weight a - weight b) • 100 - \$ H • 6,25

13. Hydrogen cyanide in RSM [14]: 10 g RSM, 40 ml H<sub>2</sub>O and 5 ml 5 % trichloroacetic acid were given in a 250 ml 2-necked flask equipped with an air cooler connected with a 10 ml flask. This small flask contained 3 ml H<sub>2</sub>O and 1 ml 5 % Na<sub>2</sub>CO<sub>3</sub>-solution and was cooled with ice. A constant stream of N<sub>2</sub> is blown through the apparatus while the contents of the 250 ml flask is boild for 15 - 20 min.

The content of the small flask then is transferred into a 10 ml measuring flask containing 2 ml of a 1 % picric acid solution in water and filled up to 10 ml. After 3 min in a water bath of  $100^{\circ}$ C and 1 h at room temperature the adsorbance was measured (1 cm, 500 nm) against a blank, coniaining 1 ml 5 % Na<sub>2</sub>CO<sub>3</sub>, 2 ml picric acid solution and 7 ml H<sub>2</sub>O. A calibration curv<sup>-</sup> was obtained with KCN.

14. Aflatoxins [15]: 50 g ground sample, mixed with 5 g Hyflosupercel is defatted by shaking with 150 ml petroleum ether. After filtering and washing with 2 x 50 ml petroleum ether the residue is air dried and extracted in a Soxhlet with chloroform : methanol = 90 : 10 (3 h). The solution is evaporated, the residue dissolved in 100 ml petroleum ether : methanol = 1:1-mixture and transferred to a separation fun-

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nel. After addition of 5 - 10 ml H_2^0 the aqueous methanolic
layer is washed with 50 ml petroleum ether and diluted with
70 ml water. This liquid is extracted 4 times with 25 ml
chloroform, the combined chloroform solutions are evaporated
and the residue dissolved in 2,00 ml chloroform.
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2 - 20  $\mu$ l of this solution is spotted on a 20 x 20 cm TLCplate (Macherey u. Nagel, Sil-G/25-HR) and developed in 2 directions with

1) Ether : methanol : H<sub>2</sub>0 = 94 : 4,5 : 1,5 (saturation)
2) Chloroform : aceton : methanol = 90 : 10 : 2 (without saturation)

The dried plate is quantitatively assessed with a TLC-scanner (e.g. Spectrodensitometer Model SD 3000, Schoeffel Instr. Corp.), fluorescence mode (Ex 365 nm, Em 435 nm). Standard curves are obtained with pure aflatoxins.