



**TOGETHER**  
*for a sustainable future*

## OCCASION

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**TOGETHER**  
*for a sustainable future*

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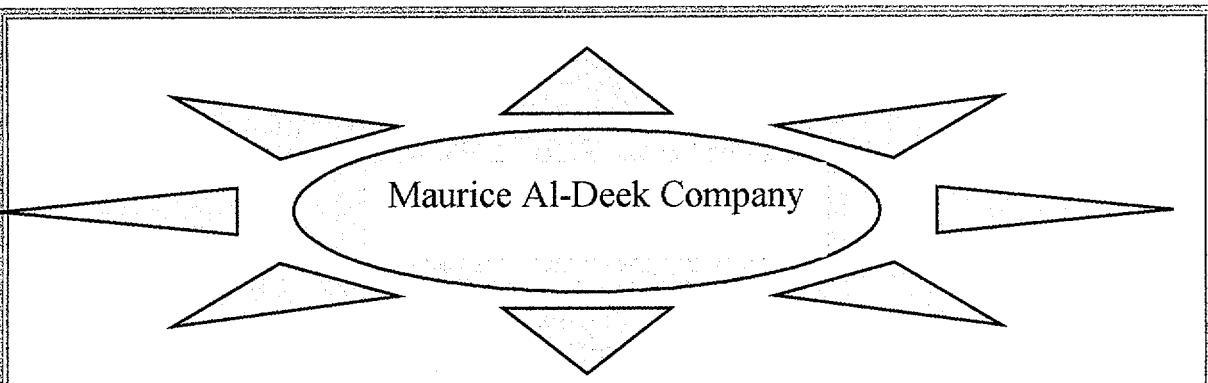
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22239

A sunburst logo consisting of a central oval containing the text "Maurice Al-Deek Company". The oval is surrounded by eight triangular rays pointing outwards.

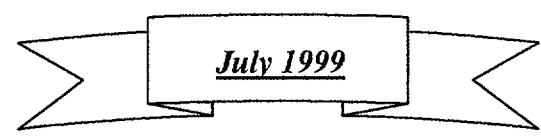
Maurice Al-Deek Company

A thought bubble with a scalloped border and three small circles leading to it from the bottom left.

*UNIDO, Project Number  
MP/JOR/98/89  
Contract Number 99/023*

A large, multi-pointed starburst logo with a double-line border.

*Final Report*

A ribbon-style banner logo with a double-line border.

*July 1999*

To: Mr. V. Koloskov  
Contracts Officer  
General Service Section  
Financial Performance Control Branch  
Field Operation and Administration Division  
UINDO, Vienna, Austria  
Fax: 00 431 26026 6815

Date: 28 July 1999

Subject: **Final Report**

Reference: Contract Number 99/023, Project Number MP/JOR/98/089

Dear Mr. Koloskov

We are Pleased to submit to you here with our Final Report of Contract number 99/023, regarding conversion of Prototypes. In our report you will find the main activities, calculation of prototypes for redesign and redefinition of models and also test result sheets of prototypes that have been tested at our Hot Chamber at our Factory in Amman. It is highly appreciated if you advise us for any further action. We also enclose invoice number 13473 for further action.

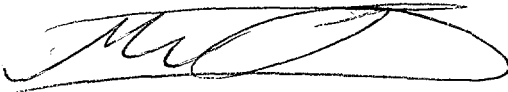
With Regards  
Faithfully Yours

Maurice Al-Deek  
Managing Director

cc. Dr. Malayeri, UNIDO Austria

مؤسسة موريس الديك

مصانع والمصنوعات المعدنية



To: Mr. V. Koloskov  
Contracts Officer  
General Service Section  
Financial Performance Control Branch  
Field Operation and Administration Division  
UINDO, Vienna, Austria  
Fax: 00 431 26026 6815

Date: 28 July 1999

Subject: Invoice 13743, Final Payment

Reference: Contract Number 99/023, Project Number MP/JOR/98/089

The amount of 4,000 four thousand USD, as the final payment of contract 99/023 referring to page 8 paragraph 3.05d) upon approval of final report , payable to :

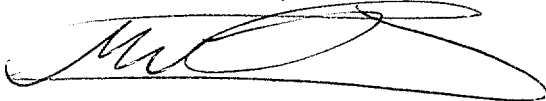
Maurice Al-Deek Co.  
Account Number 41396/8/515  
Arab Bank Plc.  
Abu-Alanda Branch  
P.O. Box 351 Abu Alanda  
Amman - Jordan

Tel: 00 962 6 4161451  
Fax 00 962 6 4162161

Maurice Al-Deek  
Managing Director

مؤسسة موريس الديك

للخدمات والمصنوعات المعدنية



July 1999

UNIDO, Project MP/JOR/98/89

Contract 99/023

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# Maurice Ind. [ Jordan ]



**TestDate:** 99/07/15 15:36  
**TestName:** Energy Consumption

**Report No.:** Spec & Remark  
**ReportDate:** 99/07/16 15:09

### Total Result :

1 - Total Test Time	22 Hours
2 - Working Percent	98 %On
3 - Energy	3.757 kwh
4 - Zoom Time	22:33 Hour
5 - Compr Current	3.02 Amp
6 - Evaprator Mean Temp	3.6 C
7 - Cabin Mean Temp	6.9 C
8 - Crisp Temp	8 C
9 - Compr Temp	64 C
10- Condensor In Temp	67.6 C
11- Condensor Out Temp	21.2 C
12- Condition	31.1 C 38 %H
13- Volt	Max=246 Mean=238 Min=218
14-	
15-	
16-	
17-	

### Product Spec :

1 - File Name	99071515.k36
2 - Test Kind	G Perform.
3 - Product Serial	Prt.mds
4 - Product Name	Show case
5 - Product Model	MDM-200
6 - Product Capacity	3 Stage
7 - Compressor Name	Elc. lux
8 - Compressor Model	R134a
9 - Compressor Power	1/3 Hp
10- Compressor Amper	3 Amp
11- Thermostat No.	3
12- Thermostat Type	Ranco
13-	
14-	

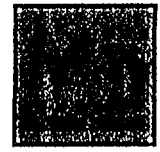
**Technical Manager:** ICRC  
**Lab Chief :** MARIO AL-DEEK  
**Lab Specialist:** ZIAD

### Remark :

Remark1  
Remark2  
Remark3

### Remark :

sign :

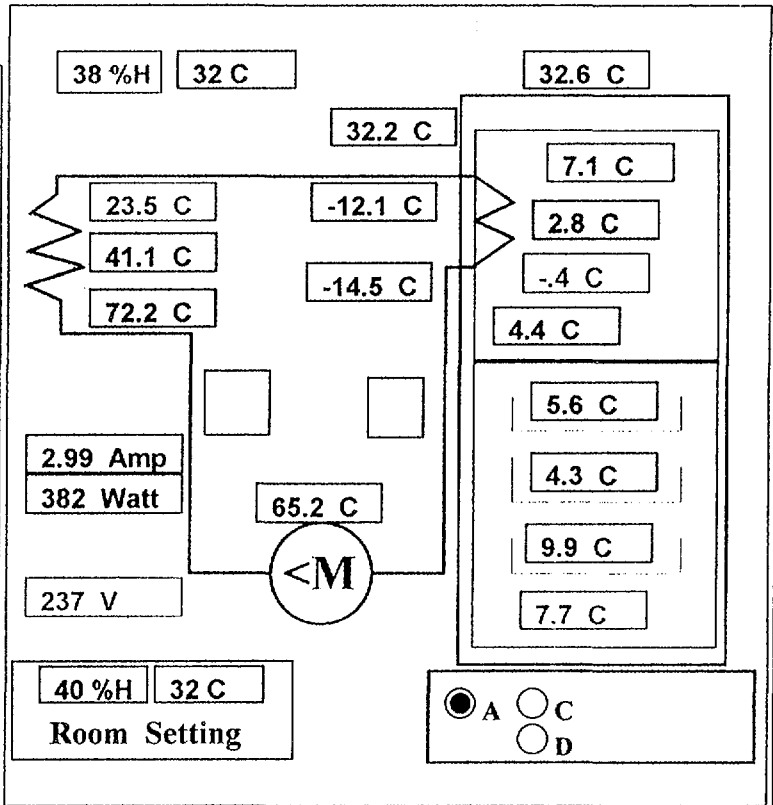


TestDate: 99/07/15 15:36  
PageTestName: Energy Consumption

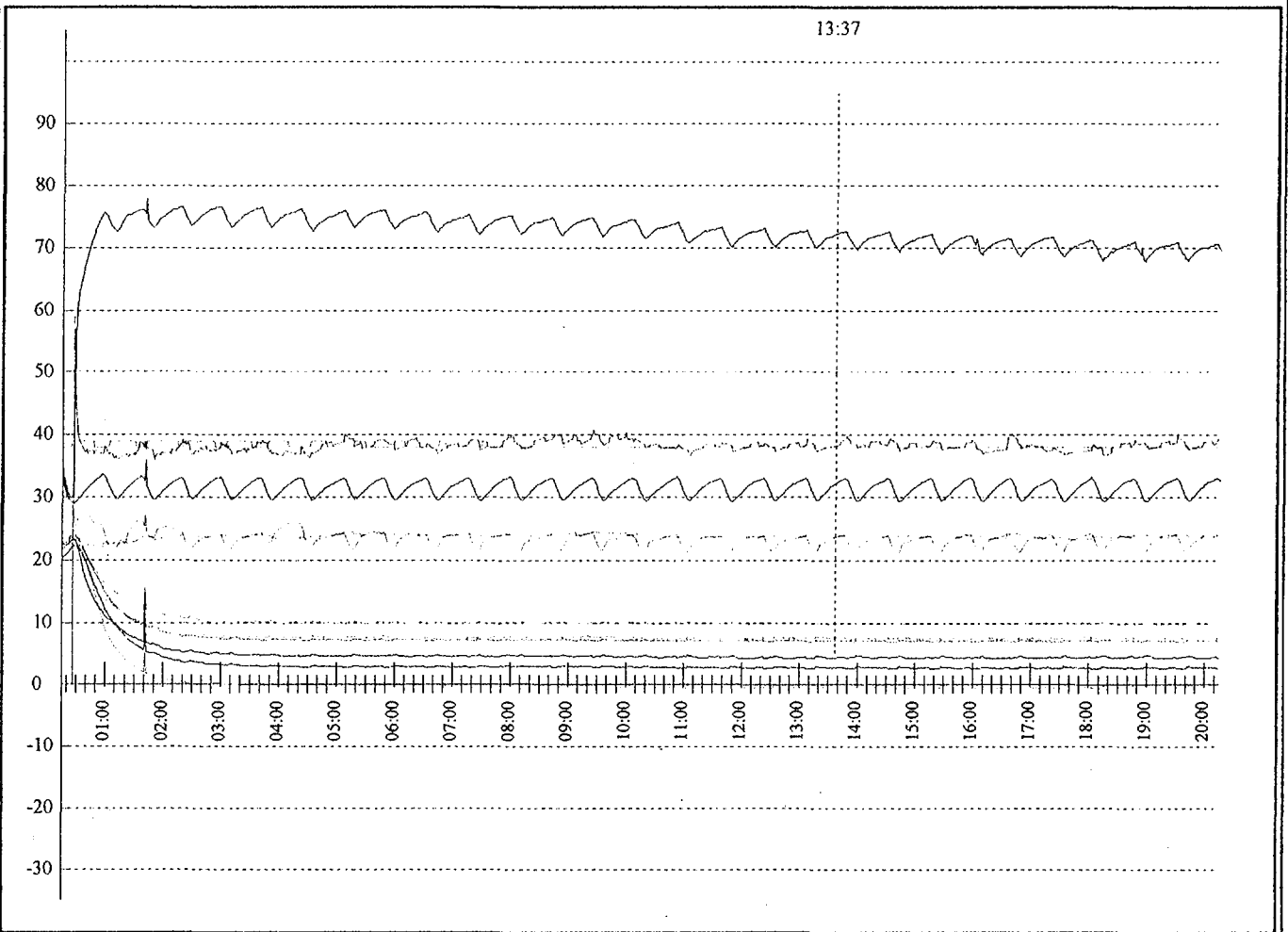
Report No.: ( ) - Page 1  
ReportDate: 99/07/16 15:52

**Page Result :**

- 1 - Page Test Time 20 Hours
- 2 - Working Percent 99 %On
- 3 - Energy (Accord to page) 3.803 kwh
- 4 - Zoom Time 13:37 Hour
- 5 - Compr Current 2.99 Amp
- 6 - Evaprator Mean Temp 3.4 C
- 7 - Cabin Mean Temp 6.6 C
- 8 - Crisp Temp 7.7 C
- 9 - Compr Temp 65.2 C
- 10- Condensor In Temp 72.2 C
- 11- Condensor Out Temp 23.5 C
- 12- Condition 32 C 38 %H
- 13- Volt Max=245 Mean=237 Min=218
- 14-
- 15-
- 16-
- 17-



Industrial Control Research Center HotRoom Ver 5





TestDate: 99/07/15 15:36

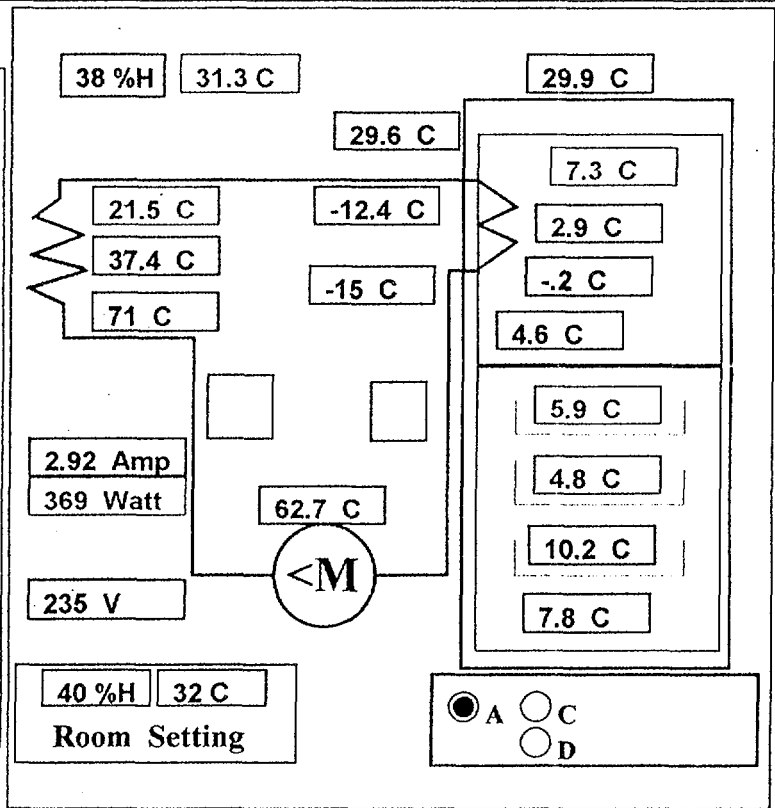
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

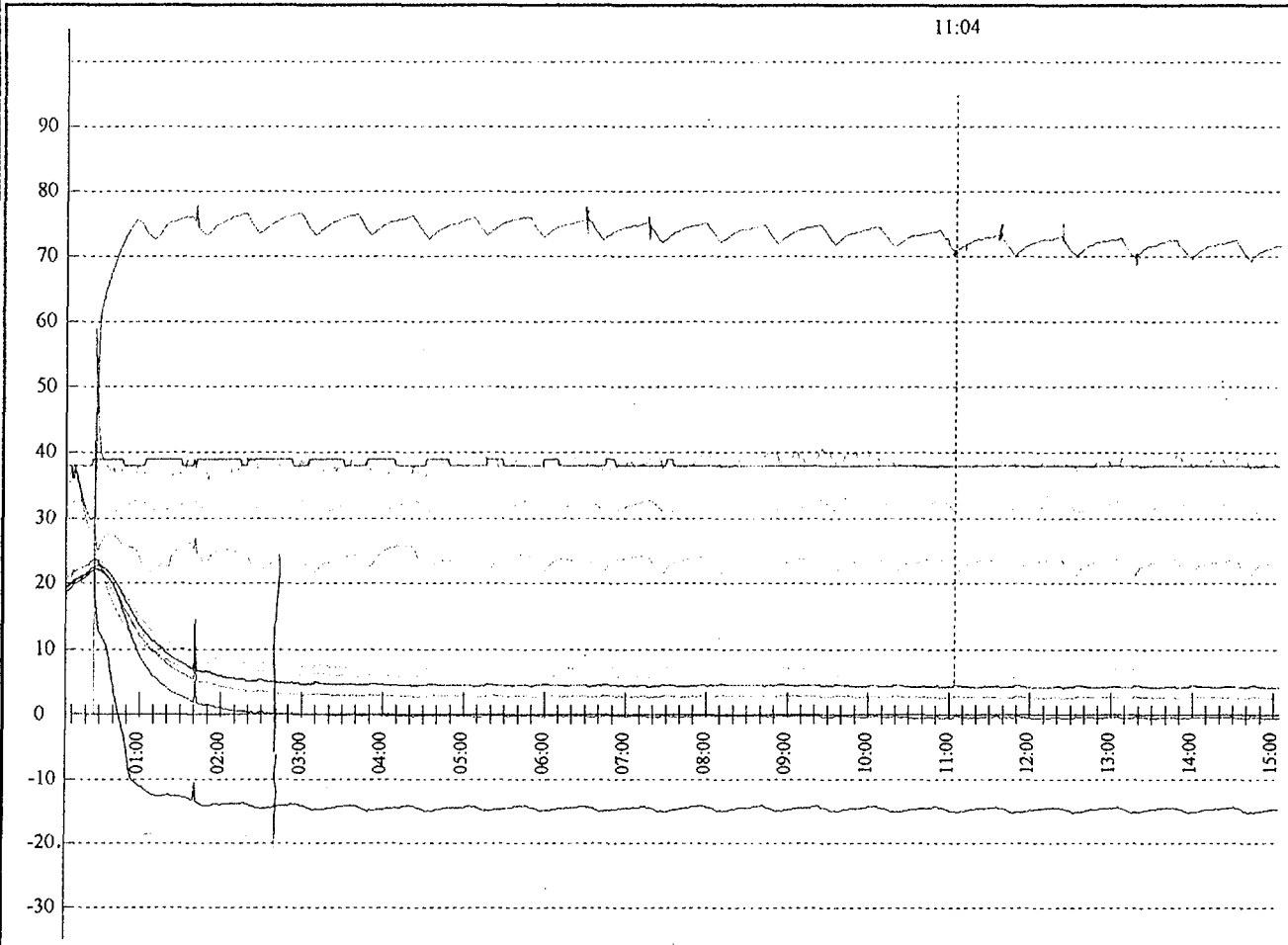
ReportDate: 99/07/16 15:42

### Page Result :

1 - Page Test Time	15 Hours
2 - Working Percent	97 %On
3 - Energy (Accord to page)	3.745 kwh
4 - Zoom Time	11:04 Hour
5 - Compr Current	2.92 Amp
6 - Evaprator Mean Temp	3.6 C
7 - Cabin Mean Temp	6.9 C
8 - Crisp Temp	7.8 C
9 - Compr Temp	62.7 C
10- Condensor In Temp	71 C
11- Condensor Out Temp	21.5 C
12- Condition	31.3 C 38 %H
13- Volt	Max=245 Mean=237 Min=218
14-	
15-	
16-	
17-	



Industrial Control Research Center HotRoom Ver 5







TestDate: 99/07/15 15:36

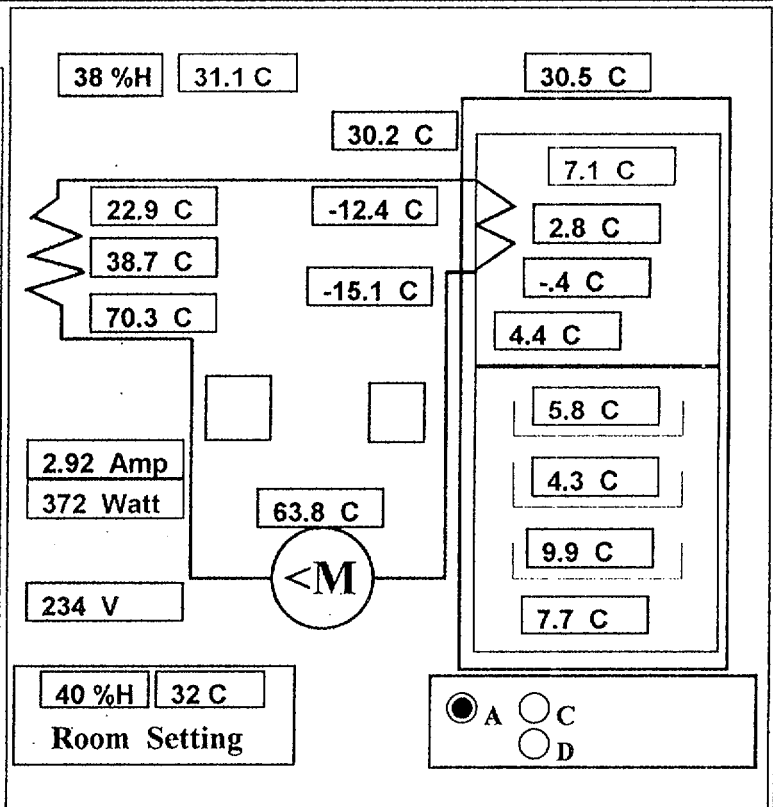
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

ReportDate: 99/07/16 15:39

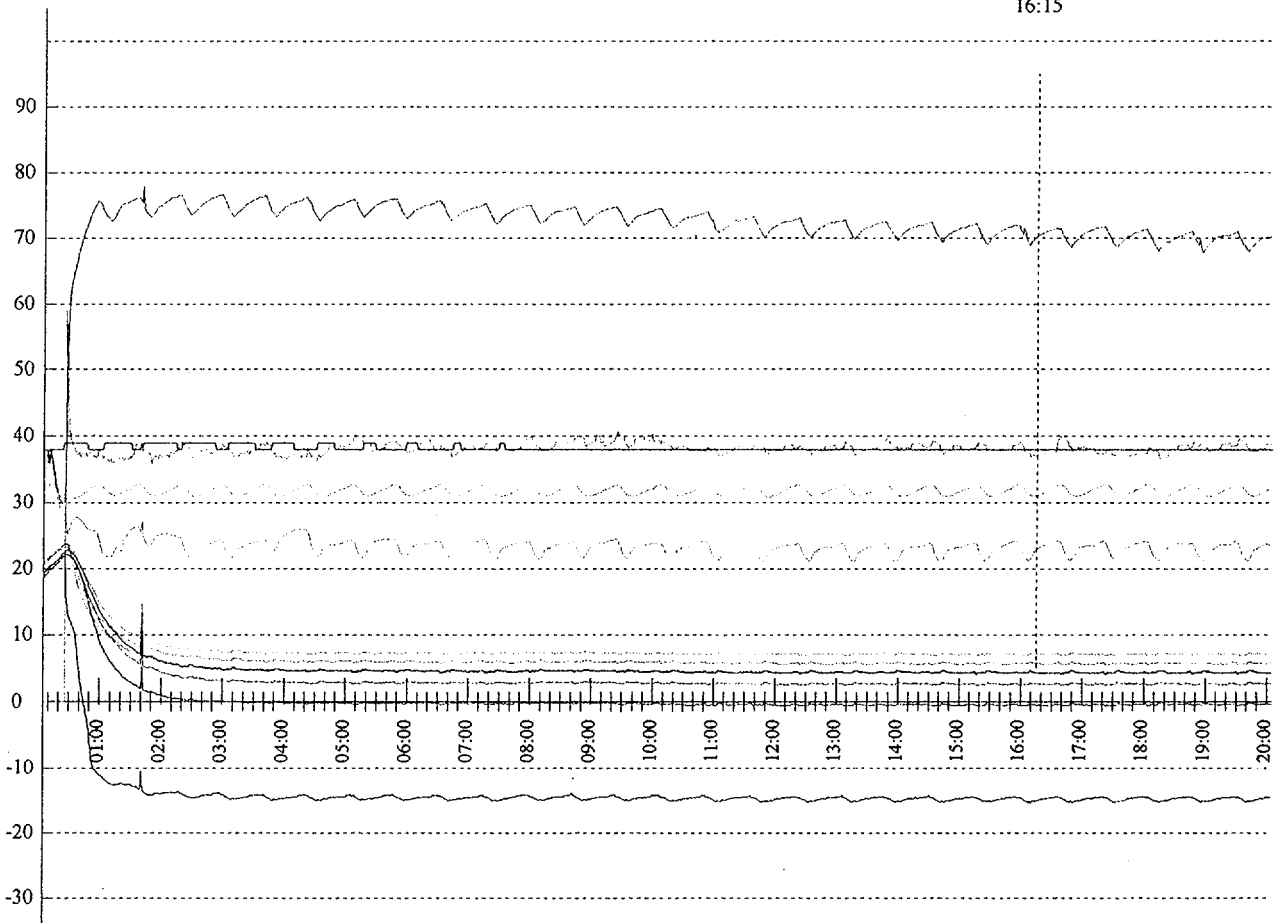
### Page Result :

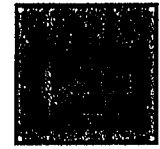
1 - Page Test Time	20 Hours
2 - Working Percent	98 %On
3 - Energy (Accord to page)	3.771 kwh
4 - Zoom Time	16:15 Hour
5 - Compr Current	2.92 Amp
6 - Evaprator Mean Temp	3.4 C
7 - Cabin Mean Temp	6.6 C
8 - Crisp Temp	7.7 C
9 - Compr Temp	63.8 C
10- Condensor In Temp	70.3 C
11- Condensor Out Temp	22.9 C
12- Condition	31.1 C 38 %H
13- Volt	Max=245 Mean=237 Min=218
14-	
15-	
16-	
17-	



Industrial Control Research Center HotRoom Ver.5

16:15





TestDate: 99/07/15 15:36

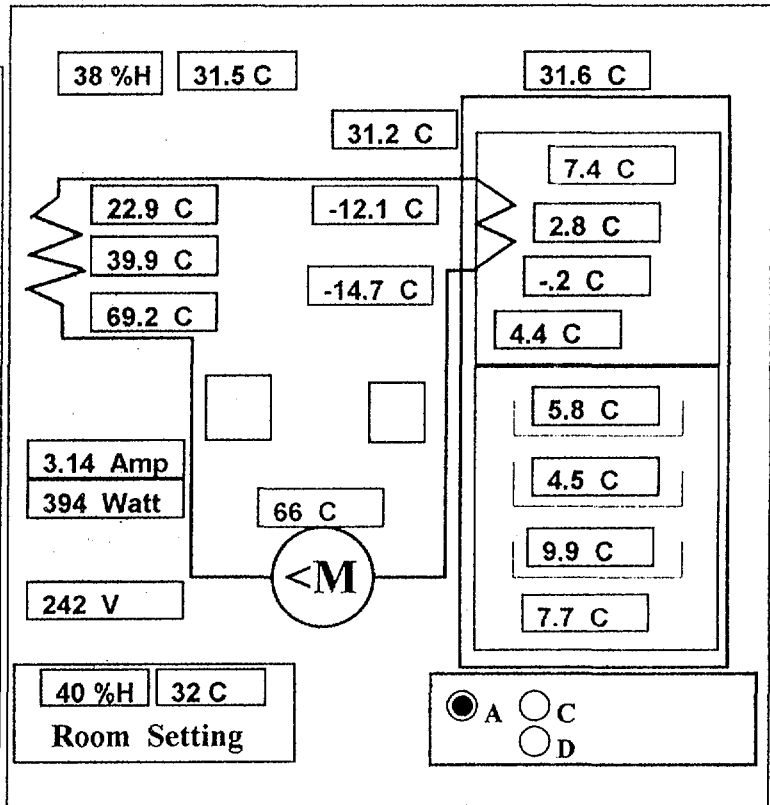
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

ReportDate: 99/07/16 15:30

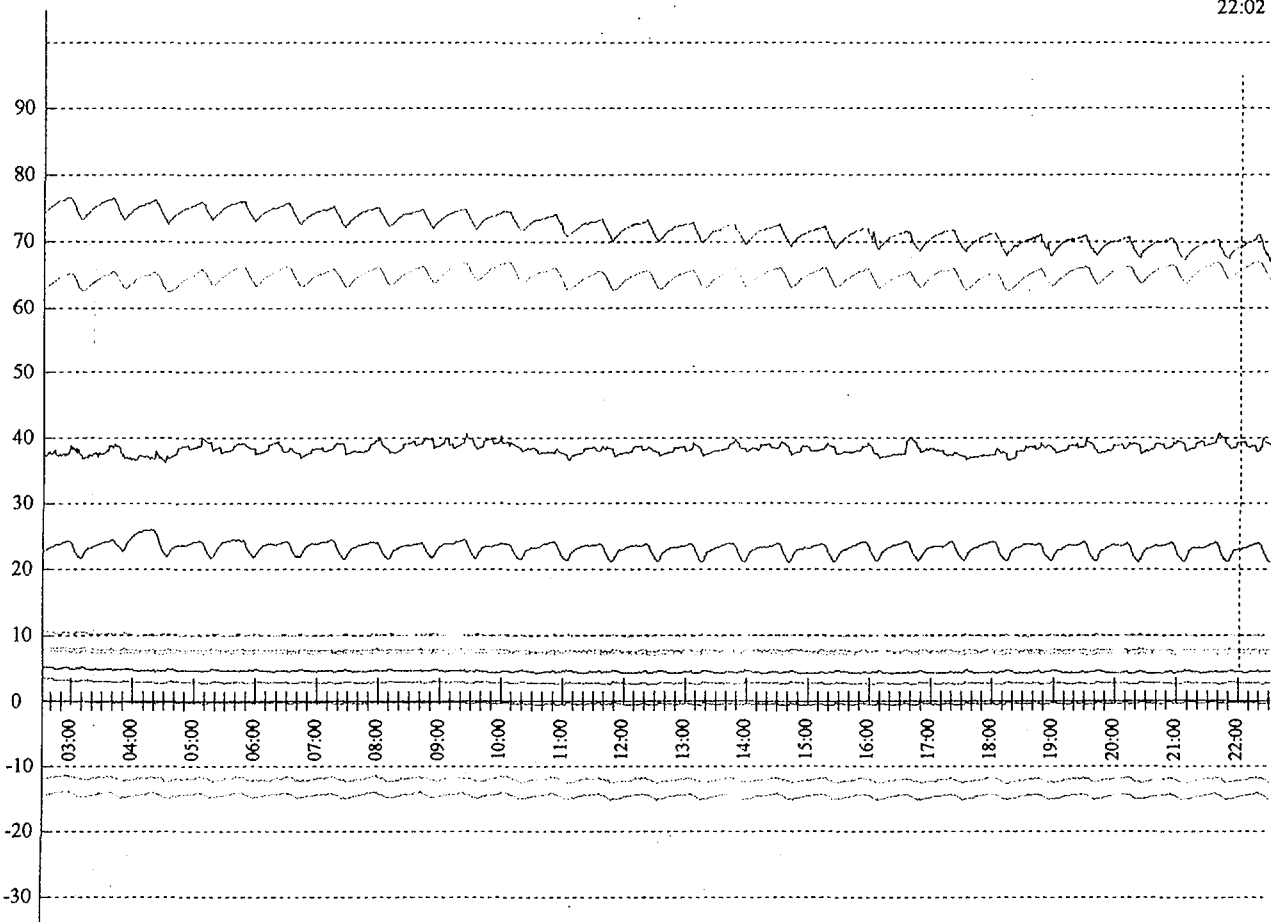
### Page Result :

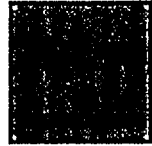
1 - Page Test Time	20 Hours
2 - Working Percent	100 %On
3 - Energy (Accord to page)	3.846 kwh
4 - Zoom Time	22:02 Hour
5 - Compr Current	3.14 Amp
6 - Evaprator Mean Temp	3.6 C
7 - Cabin Mean Temp	6.7 C
8 - Crisp Temp	7.7 C
9 - Compr Temp	66 C
10- Condensor In Temp	69.2 C
11- Condensor Out Temp	22.9 C
12- Condition	31.5 C 38 %H
13- Volt	Max=246 Mean=239 Min=230
14-	
15-	
16-	
17-	



Industrial Control Research Center HotRoom Ver 5

22:02



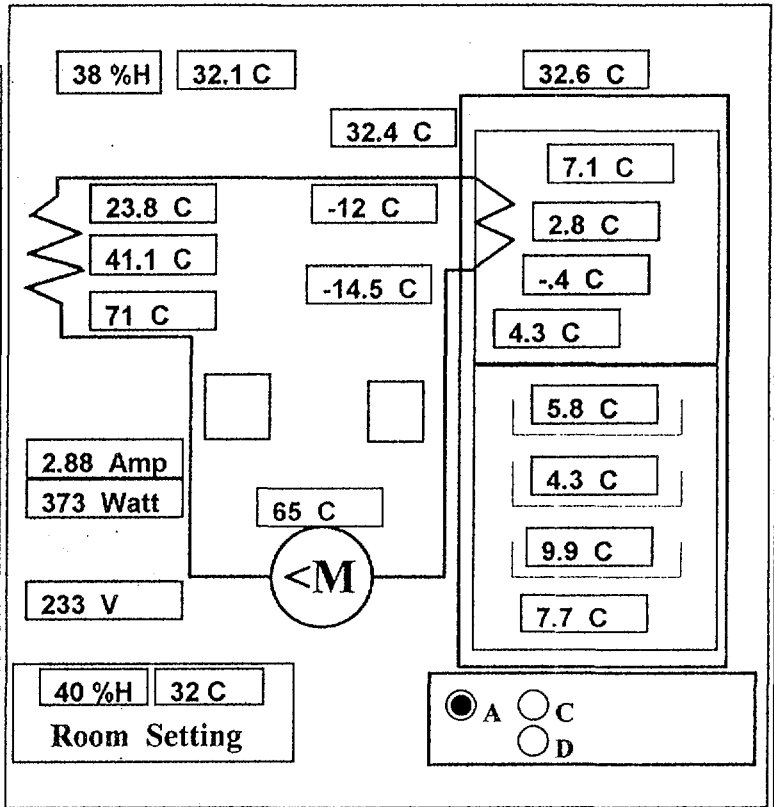


TestDate: 99/07/15 15:36  
PageTestName: Energy Consumption

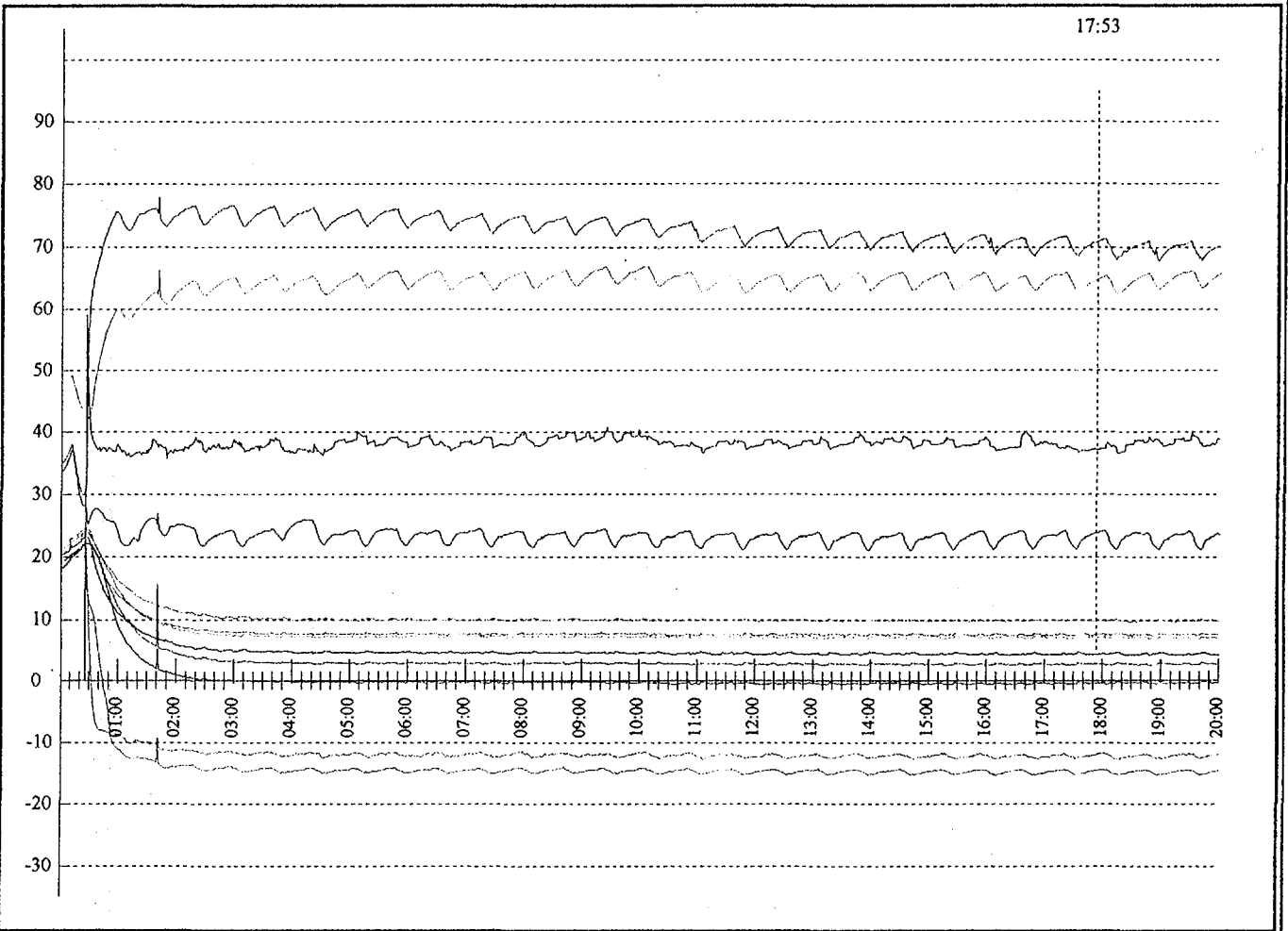
Report No.: ( ) - Page 1  
ReportDate: 99/07/16 15:27

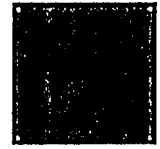
**Page Result :**

- 1 - Page Test Time 20 Hours
- 2 - Working Percent 97 %On
- 3 - Energy (Accord to page) 3.754 kwh
- 4 - Zoom Time 17:54 Hour
- 5 - Compr Current 2.88 Amp
- 6 - Evaprator Mean Temp 3.4 C
- 7 - Cabin Mean Temp 6.6 C
- 8 - Crisp Temp 7.7 C
- 9 - Compr Temp 65 C
- 10- Condensor In Temp 71 C
- 11- Condensor Out Temp 23.8 C
- 12- Condition 32.1 C 38 %H
- 13- Volt Max=245 Mean=237 Min=218
- 14-
- 15-
- 16-
- 17-



Industrial Control Research Center HotRoom Ver 5





TestDate: 99/07/15 15:36

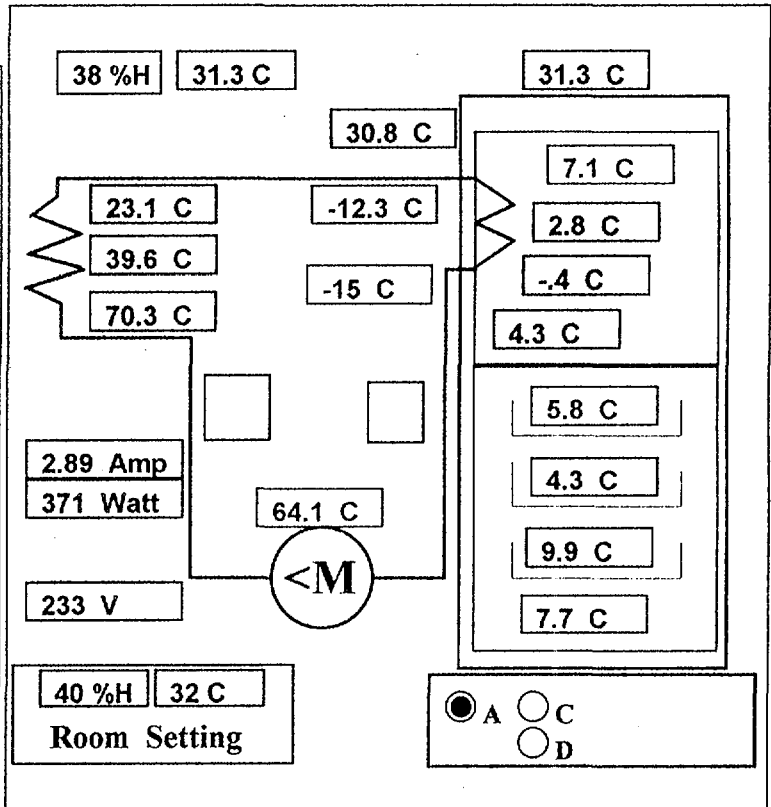
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

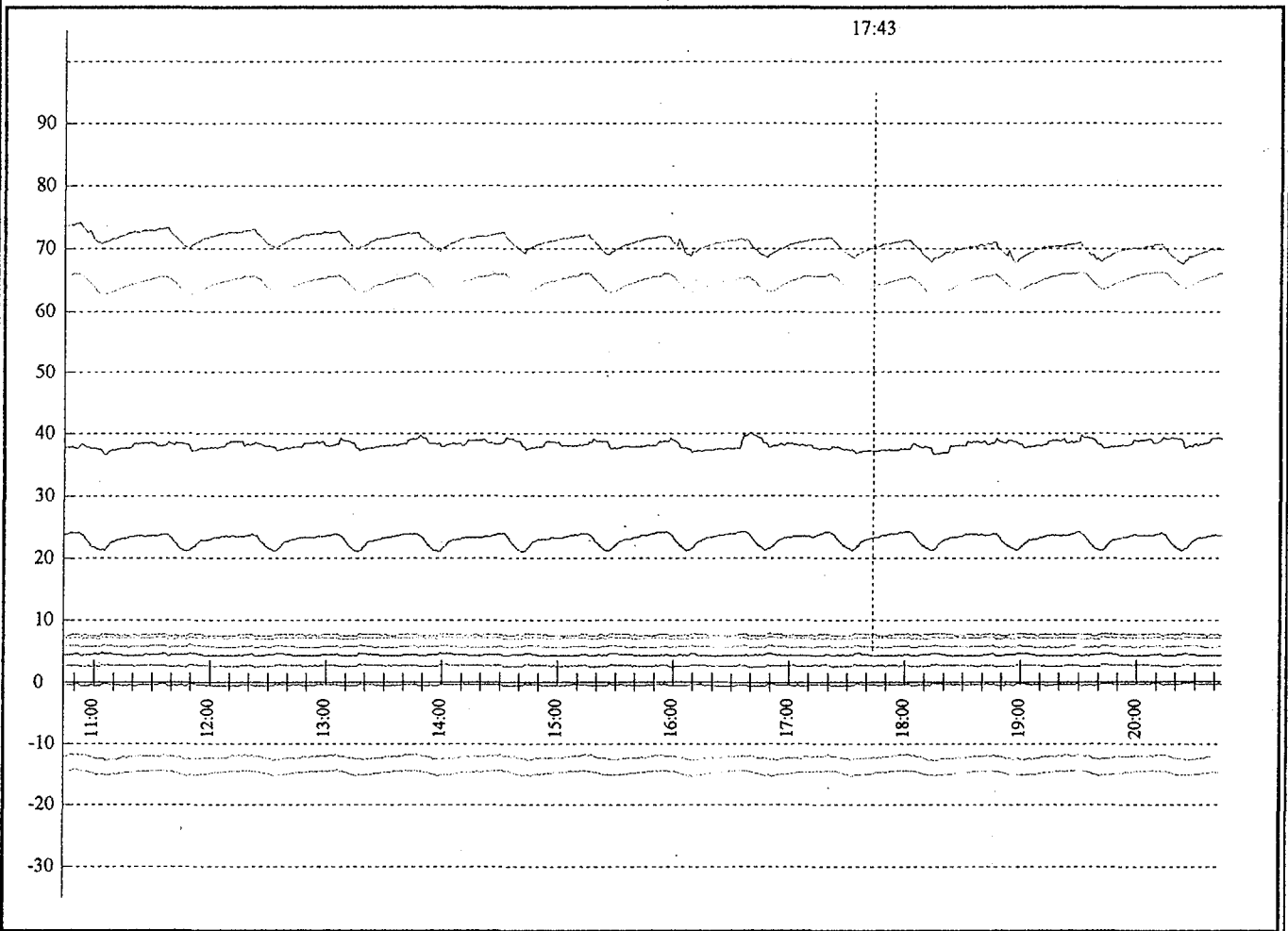
ReportDate: 99/07/16 15:19

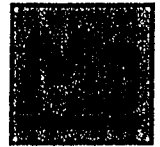
### Page Result :

1 - Page Test Time	10 Hours
2 - Working Percent	100 %On
3 - Energy (Accord to page)	3.877 kwh
4 - Zoom Time	17:43 Hour
5 - Compr Current	2.89 Amp
6 - Evaprator Mean Temp	3.4 C
7 - Cabin Mean Temp	6.6 C
8 - Crisp Temp	7.7 C
9 - Compr Temp	64.1 C
10- Condensor In Temp	70.3 C
11- Condensor Out Temp	23.1 C
12- Condition	31.3 C 38 %H
13- Volt	Max=244 Mean=238 Min=232
14-	
15-	
16-	
17-	



Industrial Control Research Center HotRoom Ver. 5





TestDate: 99/07/15 15:36

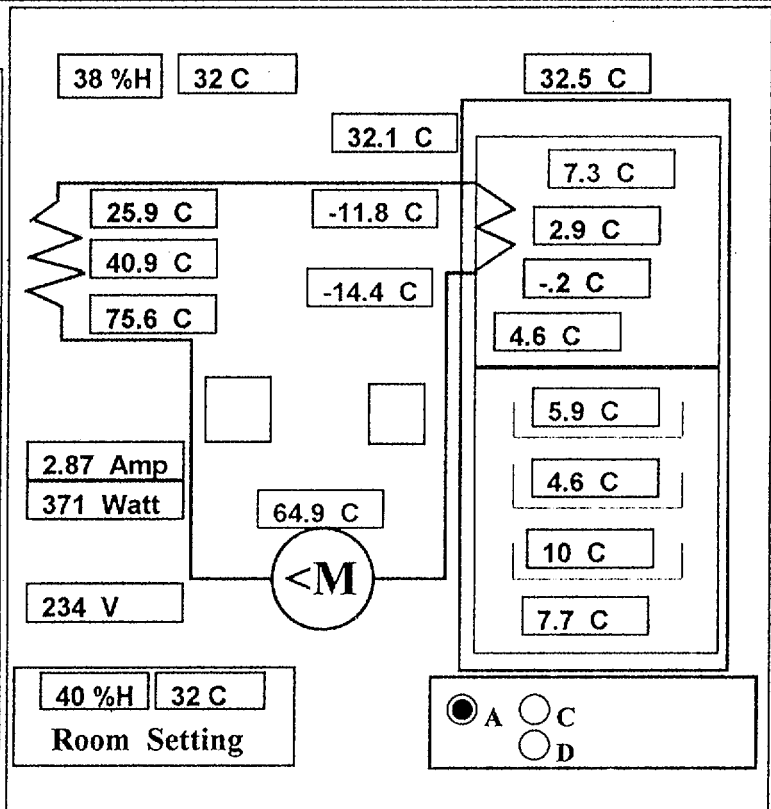
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

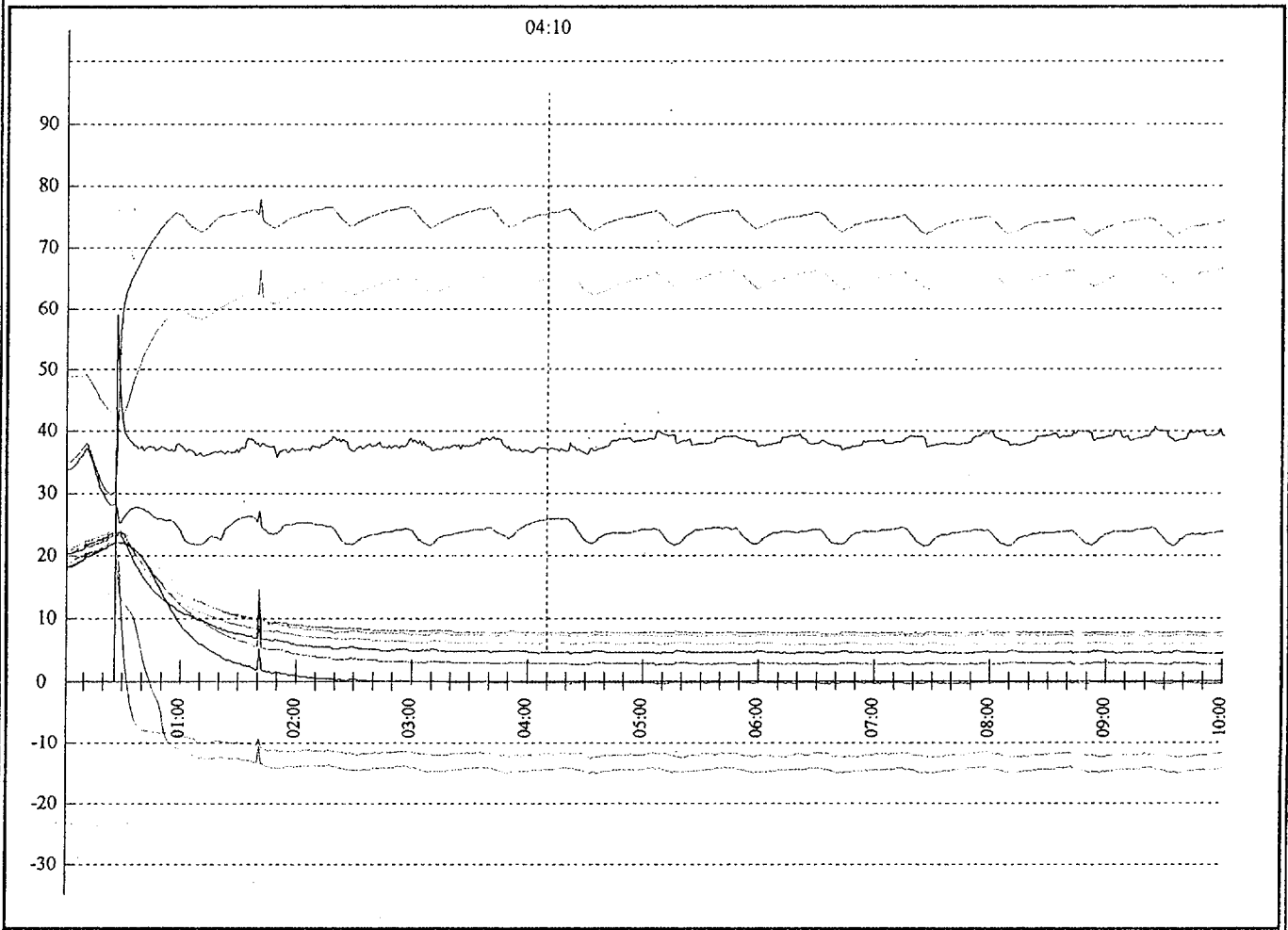
ReportDate: 99/07/16 15:16

### Page Result :

- 1 - Page Test Time            10 Hours
- 2 - Working Percent        95 %On
- 3 - Energy (Accord to page) 3.639 kwh
- 4 - Zoom Time              4:10 Hour
- 5 - Compr Current         2.87 Amp
- 6 - Evaprator Mean Temp   3.6 C
- 7 - Cabin Mean Temp      6.8 C
- 8 - Crisp Temp            7.7 C
- 9 - Compr Temp            64.9 C
- 10- Condensor In Temp    75.6 C
- 11- Condensor Out Temp   25.9 C
- 12- Condition             32 C 38 %H
- 13- Volt    Max=245 Mean=237 Min=218
- 14-
- 15-
- 16-
- 17-



Industrial Control Research Center HotRoom Ver 5



# Maurice Ind. [ Jordan ]



**TestDate:** 99/07/15 15:36  
**TestName:** Energy Consumption

**Report No.:** Spec & Remark  
**ReportDate:** 99/07/16 15:02

### Total Result :

1 - Total Test Time	22 Hours
2 - Working Percent	68 %On
3 - Energy	2.468 kwh
4 - Zoom Time	22:33 Hour
5 - Compr Current	3.51 Amp
6 - Evaprator Mean Temp	-5.7 C
7 - Cabin Mean Temp	-2.8 C
8 - Crisp Temp	-5.5 C
9 - Compr Temp	51 C
10- Condensor In Temp	59.8 C
11- Condensor Out Temp	32.4 C
12- Condition	31.1 C 38 %H
13- Volt	Max=246 Mean=238 Min=218
14-	
15-	
16-	
17-	

### Product Spec :

1 - File Name	99071515.k36
2 - Test Kind	G Perform.
3 - Product Serial	Prt-mdcf2
4 - Product Name	Chest Free
5 - Product Model	MDCF-125
6 - Product Capacity	1250 lit
7 - Compressor Name	Elec.lux
8 - Compressor Model	R134a
9 - Compressor Power	1/4 Hp
10- Compressor Amper	
11- Thermostat No.	3
12- Thermostat Type	Ranco
13-	
14-	

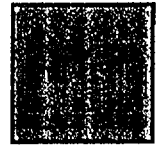
**Technical Manager:** ICRC  
**Lab Chief :** MARIO AL-DEEK  
**Lab Specialist:** ZIAD

### Remark :

Remark1  
Remark2  
Remark3

**Remark :**

sign :



TestDate: 99/07/15 15:36

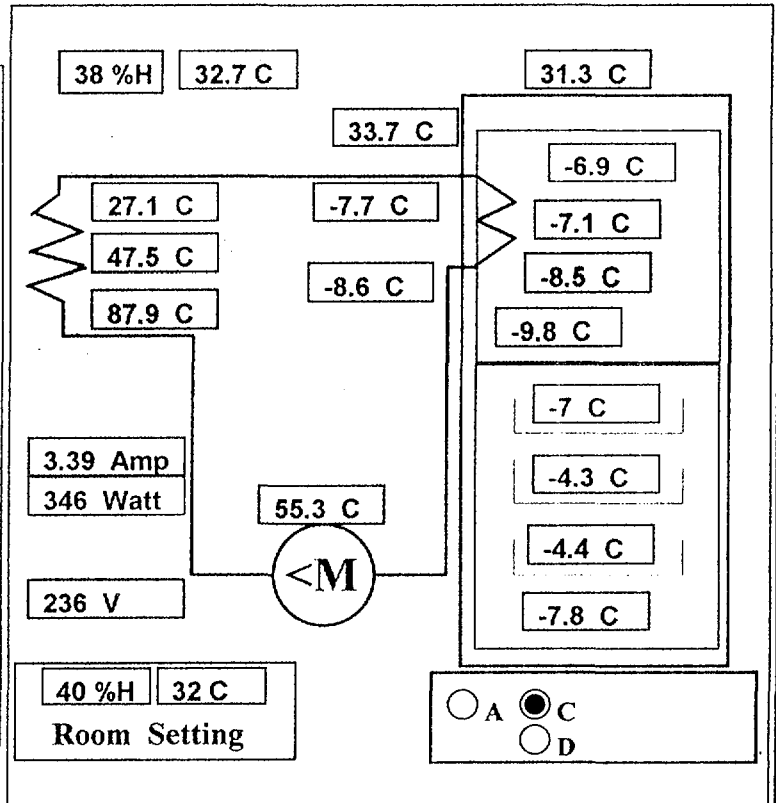
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

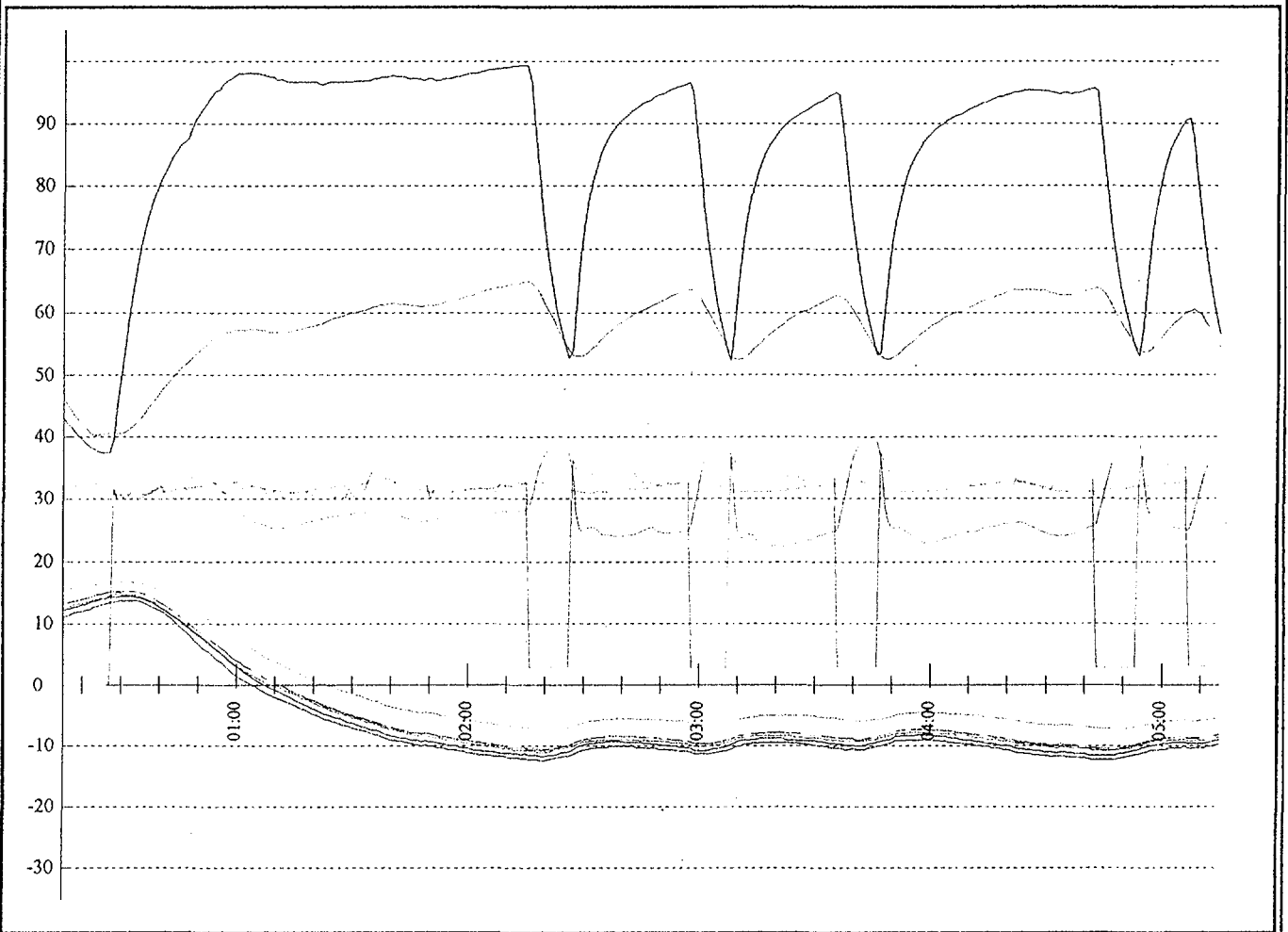
ReportDate: 99/07/16 14:30

### Page Result :

- |                             |                          |
|-----------------------------|--------------------------|
| 1 - Page Test Time          | 5 Hours                  |
| 2 - Working Percent         | 78 %On                   |
| 3 - Energy (Accord to page) | 2.337 kwh                |
| 4 - Zoom Time               | 13:05 Hour               |
| 5 - Compr Current           | 3.39 Amp                 |
| 6 - Evaprator Mean Temp     | -8 C                     |
| 7 - Cabin Mean Temp         | -5.2 C                   |
| 8 - Crisp Temp              | -7.8 C                   |
| 9 - Compr Temp              | 55.3 C                   |
| 10- Condensor In Temp       | 87.9 C                   |
| 11- Condensor Out Temp      | 27.1 C                   |
| 12- Condition               | 32.7 C 38 %H             |
| 13- Volt                    | Max=245 Mean=234 Min=218 |
| 14-                         |                          |
| 15-                         |                          |
| 16-                         |                          |
| 17-                         |                          |



Industrial Control Research Center HotRoom Ver 5





TestDate: 99/07/15 15:36

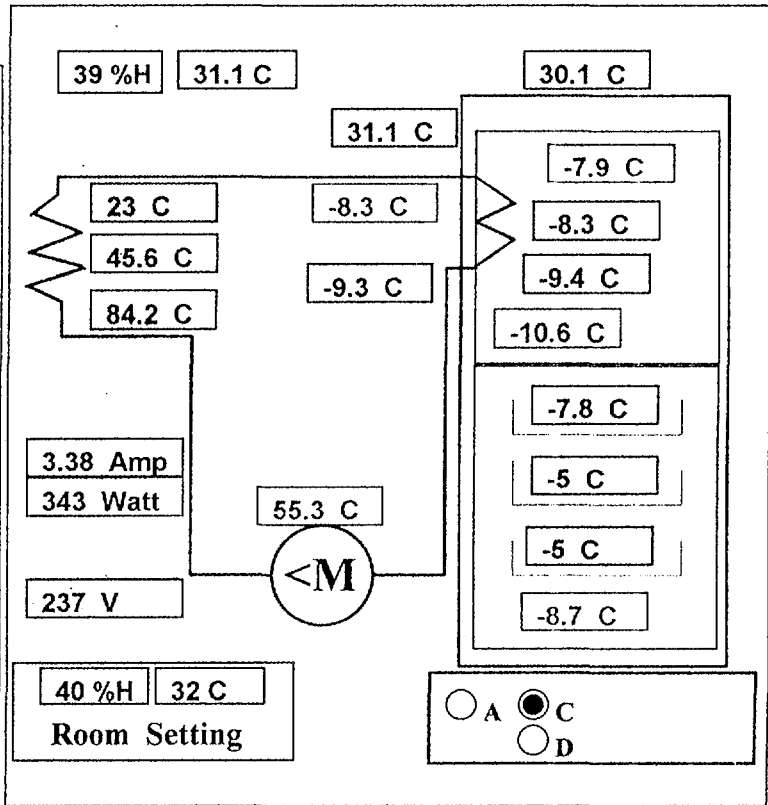
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

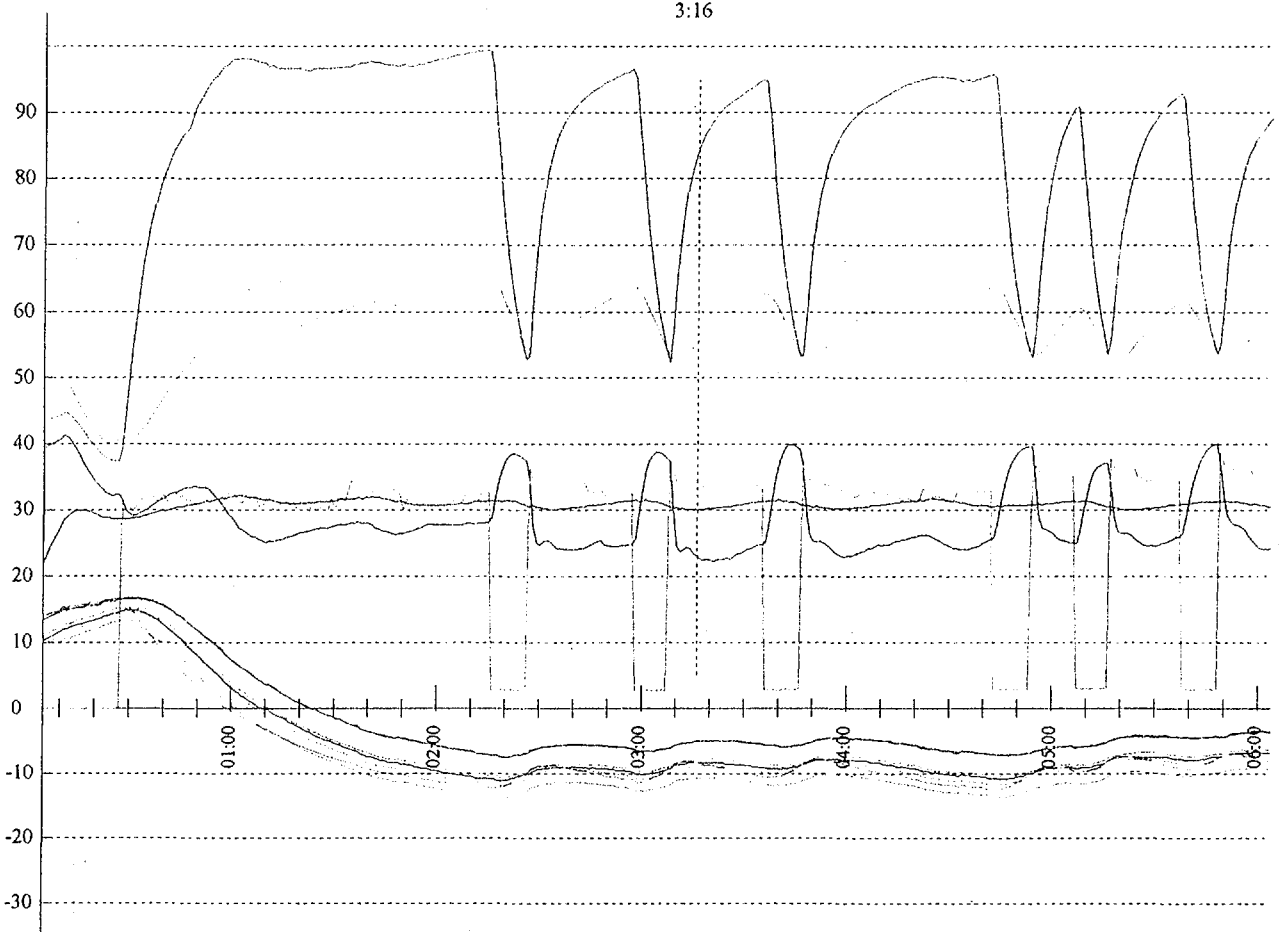
ReportDate: 99/07/16 14:55

### Page Result :

- 1 - Page Test Time 6 Hours
- 2 - Working Percent 76 %On
- 3 - Energy (Accord to page) 2.348 kwh
- 4 - Zoom Time 3:16 Hour
- 5 - Compr Current 3.38 Amp
- 6 - Evaprator Mean Temp -9 C
- 7 - Cabin Mean Temp -5.9 C
- 8 - Crisp Temp -8.7 C
- 9 - Compr Temp 55.3 C
- 10- Condensor In Temp 84.2 C
- 11- Condensor Out Temp 23 C
- 12- Condition 31.1 C 39 %H
- 13- Volt Max=245 Mean=235 Min=218
- 14-
- 15-
- 16-
- 17-

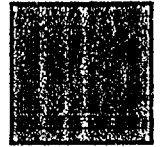


3:16





# Maurice Ind. [ Jordan ]

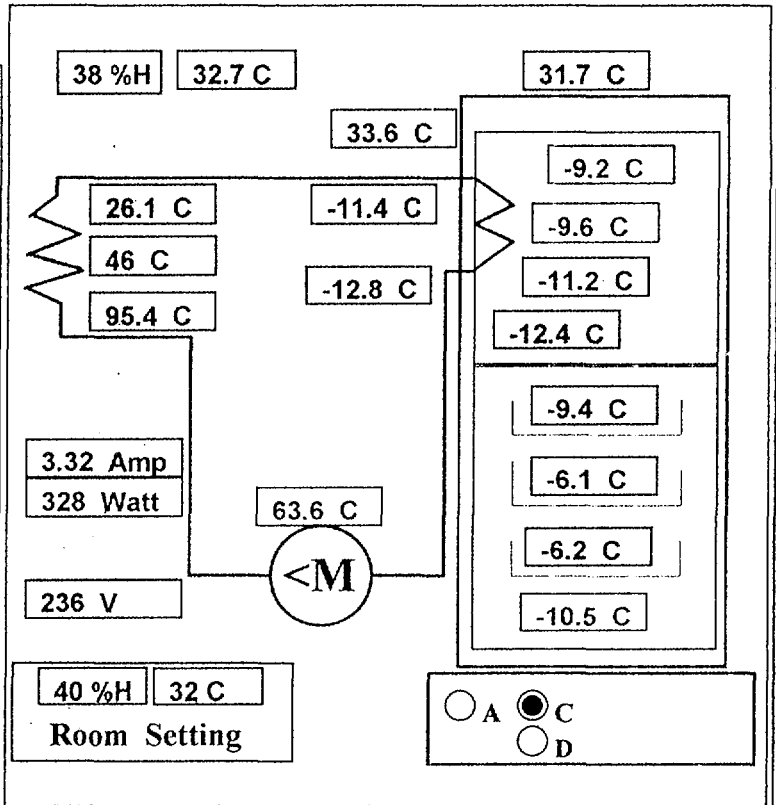


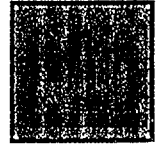
TestDate: 99/07/15 15:36  
PageTestName: Energy Consumption

Report No.: ( ) - Page 1  
ReportDate: 99/07/16 14:46

## Page Result :

- 1 - Page Test Time 10 Hours
- 2 - Working Percent 70 %On
- 3 - Energy (Accord to page) 2.413 kwh
- 4 - Zoom Time 4:24 Hour
- 5 - Compr Current 3.32 Amp
- 6 - Evaprator Mean Temp -10.6 C
- 7 - Cabin Mean Temp -7.2 C
- 8 - Crisp Temp -10.5 C
- 9 - Compr Temp 63.6 C
- 10- Condensor In Temp 95.4 C
- 11- Condensor Out Temp 26.1 C
- 12- Condition 32.7 C 38 %H
- 13- Volt Max=245 Mean=237 Min=218
- 14-
- 15-
- 16-
- 17-



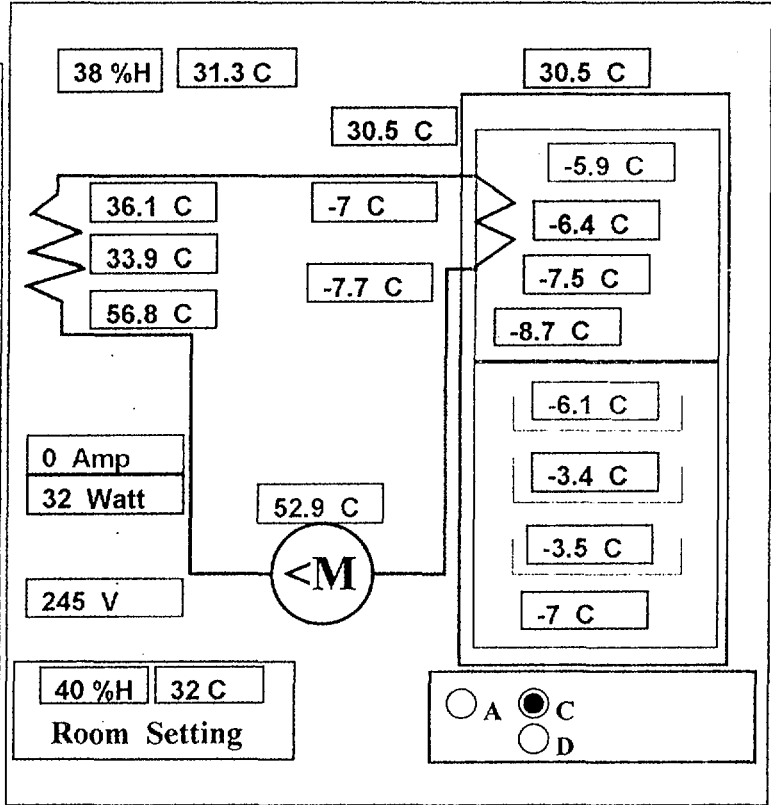


TestDate: 99/07/15 15:36  
PageTestName: Energy Consumption

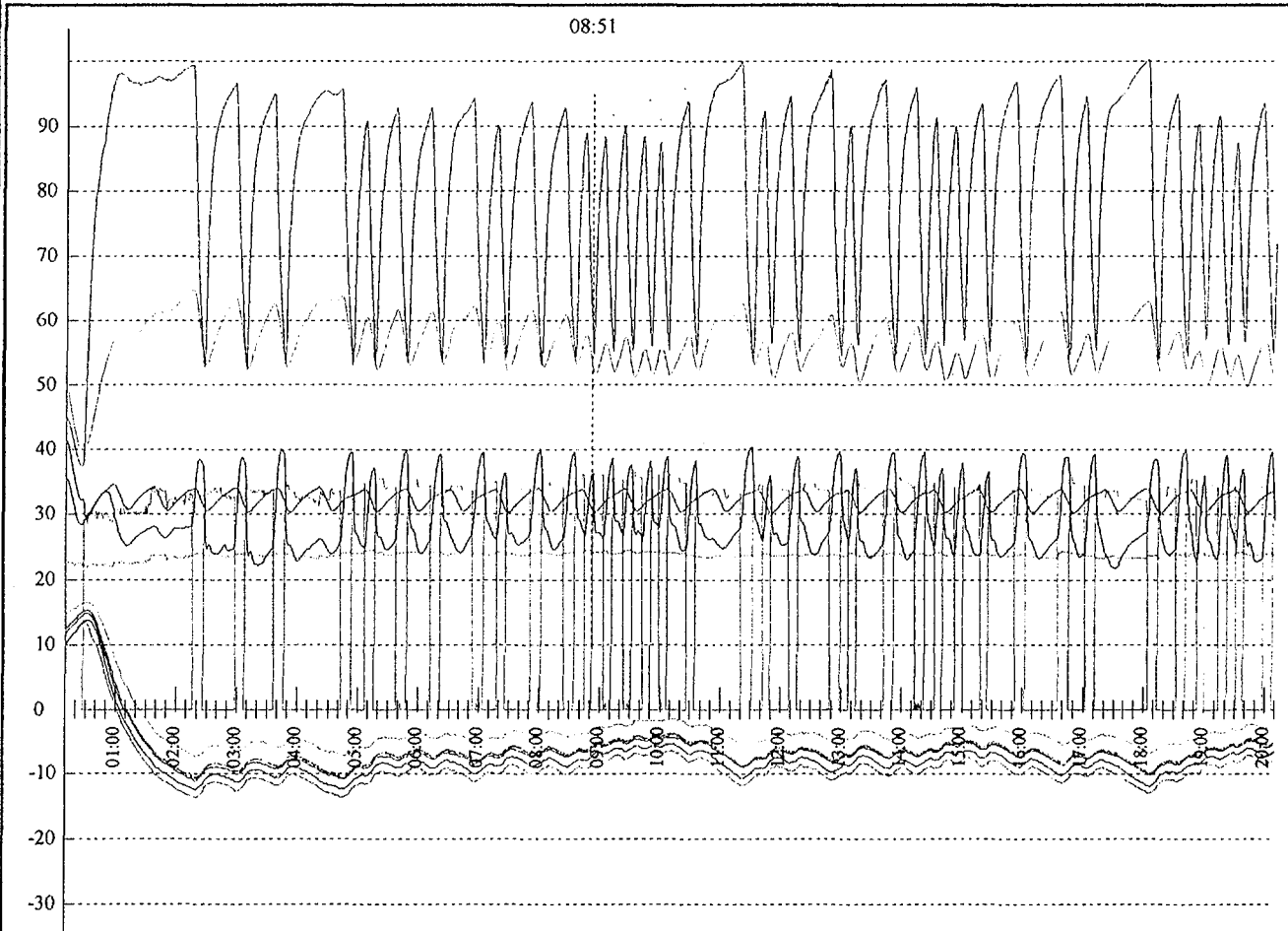
Report No.: ( ) - Page 1  
ReportDate: 99/07/16 14:38

**Page Result :**

- 1 - Page Test Time 20 Hours
- 2 - Working Percent 69 %On
- 3 - Energy (Accord to page) 2.492 kwh
- 4 - Zoom Time 8:52 Hour
- 5 - Compr Current 00 Amp
- 6 - Evaprator Mean Temp -7.1 C
- 7 - Cabin Mean Temp -4.3 C
- 8 - Crisp Temp -7 C
- 9 - Compr Temp 52.9 C
- 10- Condensor In Temp 56.8 C
- 11- Condensor Out Temp 36.1 C
- 12- Condition 31.3 C 38 %H
- 13- Volt Max=245 Mean=237 Min=218
- 14-
- 15-
- 16-
- 17-



Industrial Control Research Center HotRoom Ver 5





TestDate: 99/07/15 15:36

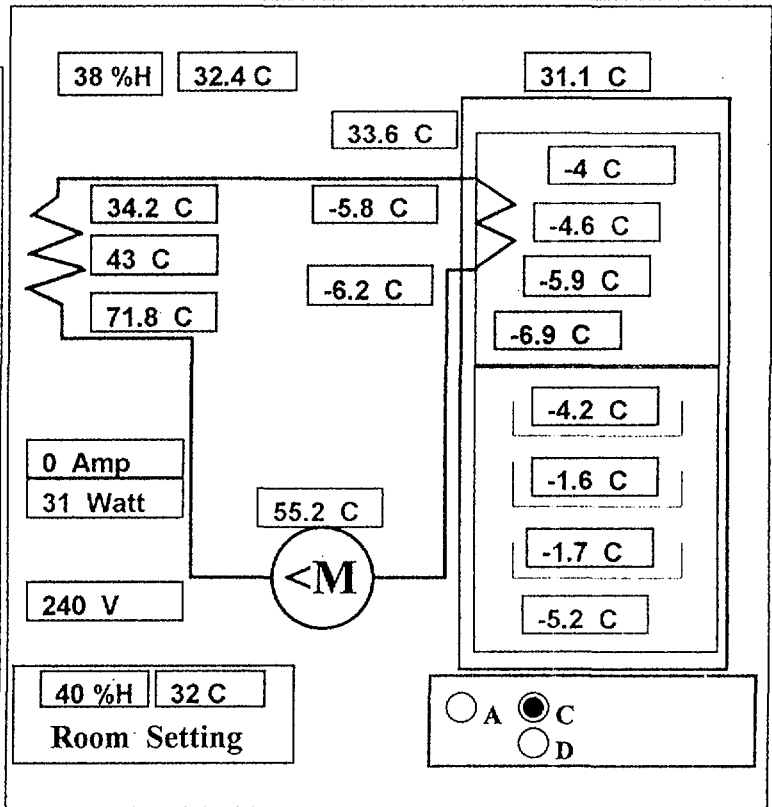
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

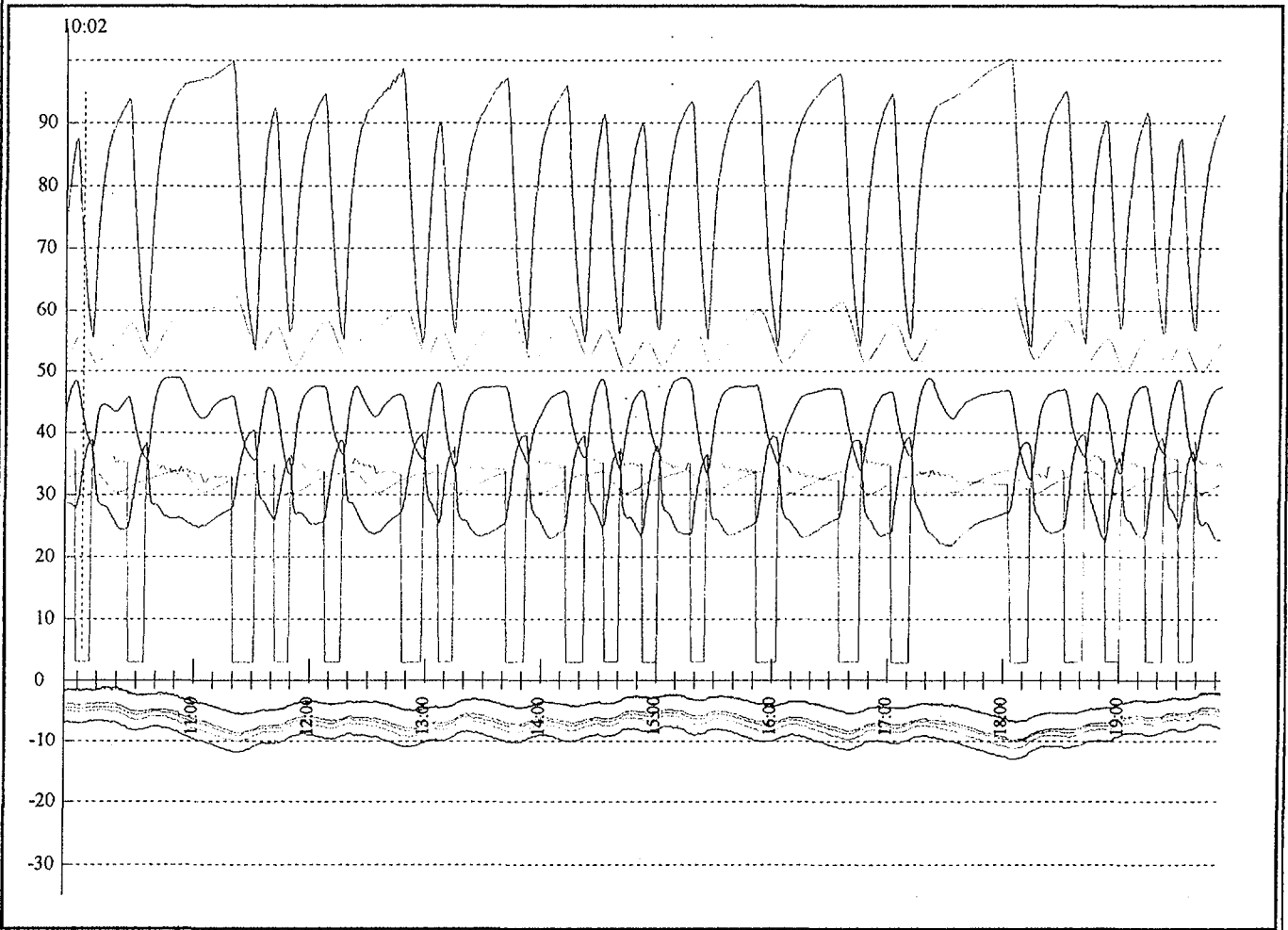
ReportDate: 99/07/16 14:49

### Page Result :

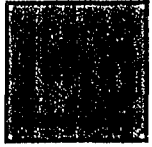
- 1 - Page Test Time 10 Hours
- 2 - Working Percent 69 %On
- 3 - Energy (Accord to page) 2.563 kwh
- 4 - Zoom Time 10:02 Hour
- 5 - Compr Current 00 Amp
- 6 - Evaprator Mean Temp -5.3 C
- 7 - Cabin Mean Temp -2.5 C
- 8 - Crisp Temp -5.2 C
- 9 - Compr Temp 55.2 C
- 10- Condensor In Temp 71.8 C
- 11- Condensor Out Temp 34.2 C
- 12- Condition 32.4 C 38 %H
- 13- Volt Max=244 Mean=238 Min=232
- 14-
- 15-
- 16-
- 17-



Industrial Control Research Center HotRoom Ver 5



# Maurice Ind. [ Jordan ]



TestDate: 99/07/15 15:36

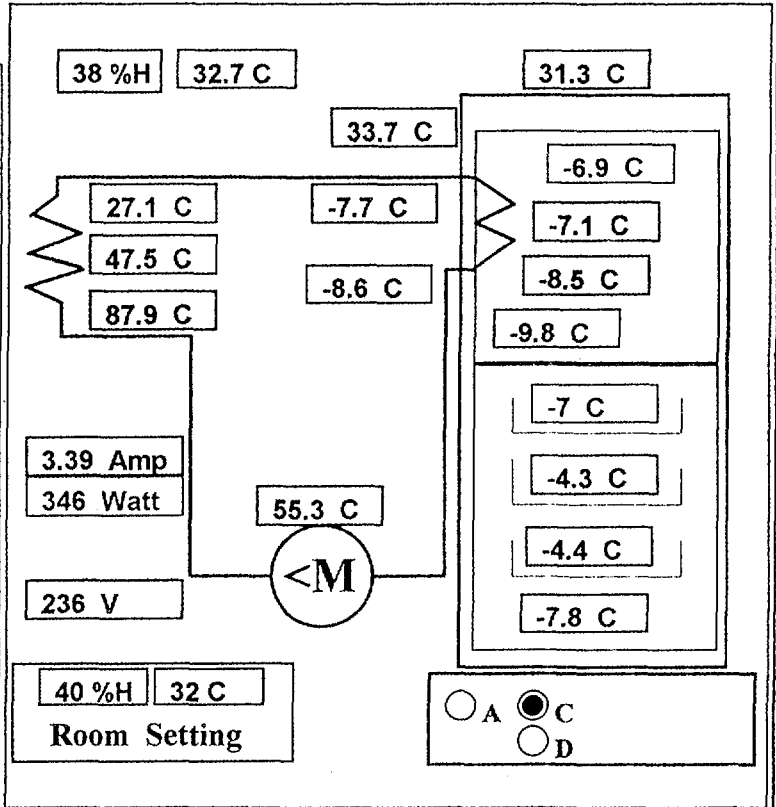
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

ReportDate: 99/07/16 14:32

## Page Result :

- 1 - Page Test Time 20 Hours
- 2 - Working Percent 70 %On
- 3 - Energy (Accord to page) 2.507 kwh
- 4 - Zoom Time 13:05 Hour
- 5 - Compr Current 3.39 Amp
- 6 - Evaprator Mean Temp -8 C
- 7 - Cabin Mean Temp -5.2 C
- 8 - Crisp Temp -7.8 C
- 9 - Compr Temp 55.3 C
- 10- Condensor In Temp 87.9 C
- 11- Condensor Out Temp 27.1 C
- 12- Condition 32.7 C 38 %H
- 13- Volt Max=245 Mean=237 Min=218
- 14-
- 15-
- 16-
- 17-



Industrial Control Research Center HotRoom Ver 5





TestDate: 99/07/15 15:36

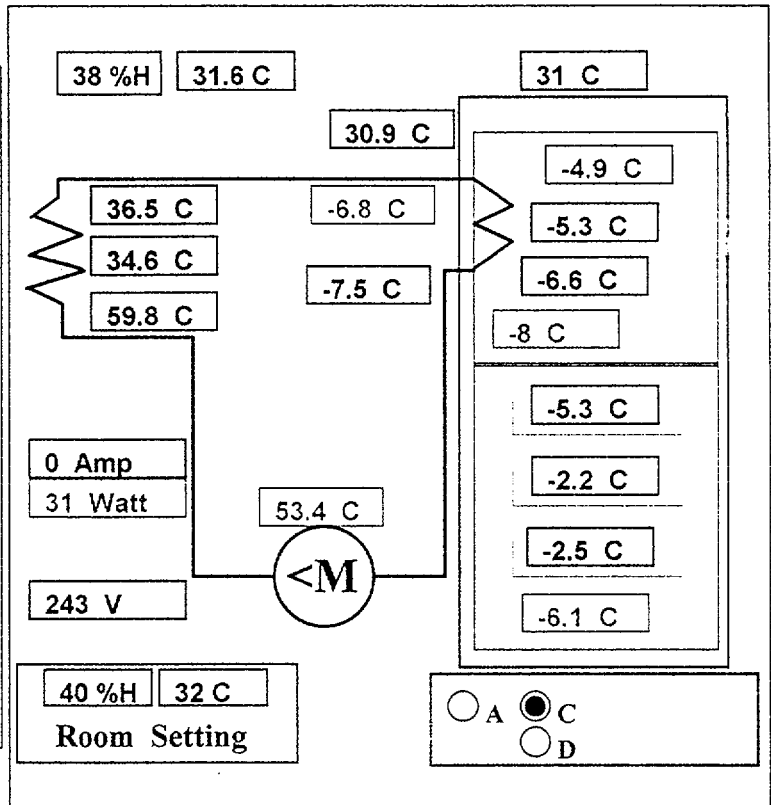
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

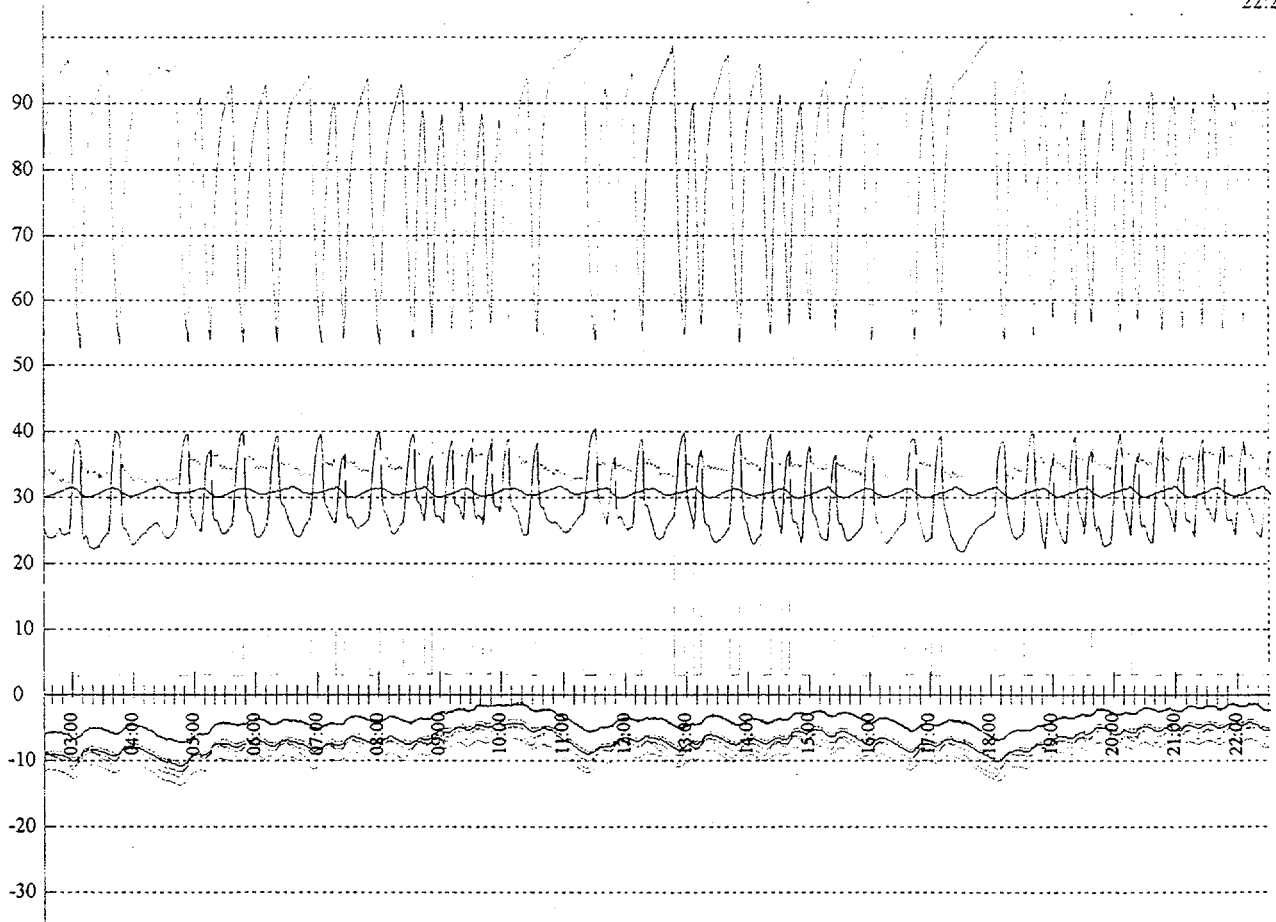
ReportDate: 99/07/16 14:58

### Page Result :

- 1 - Page Test Time 20 Hours
- 2 - Working Percent 67 %On
- 3 - Energy (Accord to page) 2.527 kwh
- 4 - Zoom Time 22:30 Hour
- 5 - Compr Current 00 Amp
- 6 - Evaprator Mean Temp -6.2 C
- 7 - Cabin Mean Temp -3.3 C
- 8 - Crisp Temp -6.1 C
- 9 - Compr Temp 53.4 C
- 10- Condensor In Temp 59.8 C
- 11- Condensor Out Temp 36.5 C
- 12- Condition 31.6 C 38 %H
- 13- Volt Max=246 Mean=239 Min=230
- 14-
- 15-
- 16-
- 17-



22:29



# Maurice Ind. [ Jordan ]



**TestDate:** 99/07/15 15:36  
**TestName:** Energy Consumption

**Report No.:** Spec & Remark  
**ReportDate:** 99/07/16 15:35

### Total Result :

1 - Total Test Time	22 Hours
2 - Working Percent	33 %On
3 - Energy	0.277 kwh
4 - Zoom Time	22:33 Hour
5 - Compr Current	00 Amp
6 - Evaprator Mean Temp	11.5 C
7 - Cabin Mean Temp	29.2 C
8 - Crisp Temp	29.4 C
9 - Compr Temp	28.1 C
10- Condensor In Temp	28.4 C
11- Condensor Out Temp	27.8 C
12- Condition	31.1 C 38 %H
13- Volt	Max=246 Mean=238 Min=218
14-	
15-	
16-	
17-	

### Product Spec :

1 - File Name	99071515.k38
2 - Test Kind	G Perform.
3 - Product Serial	Prt.mdwc/4
4 - Product Name	Water Cool
5 - Product Model	MDWC-100
6 - Product Capacity	100 L/H
7 - Compressor Name	Elect.lux
8 - Compressor Model	134 a
9 - Compressor Power	1/5 Hp
10- Compressor Amper	
11- Thermostat No.	3
12- Thermostat Type	Ranco
13-	
14-	

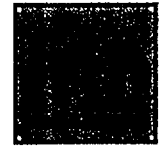
**Technical Manager:** ICRC  
**Lab Chief :** MARIO AL-DEEK  
**Lab Specialist:** ZIAD

### Remark :

Remark1  
Remark2  
Remark3

### Remark :

sign :



TestDate: 99/07/15 15:36

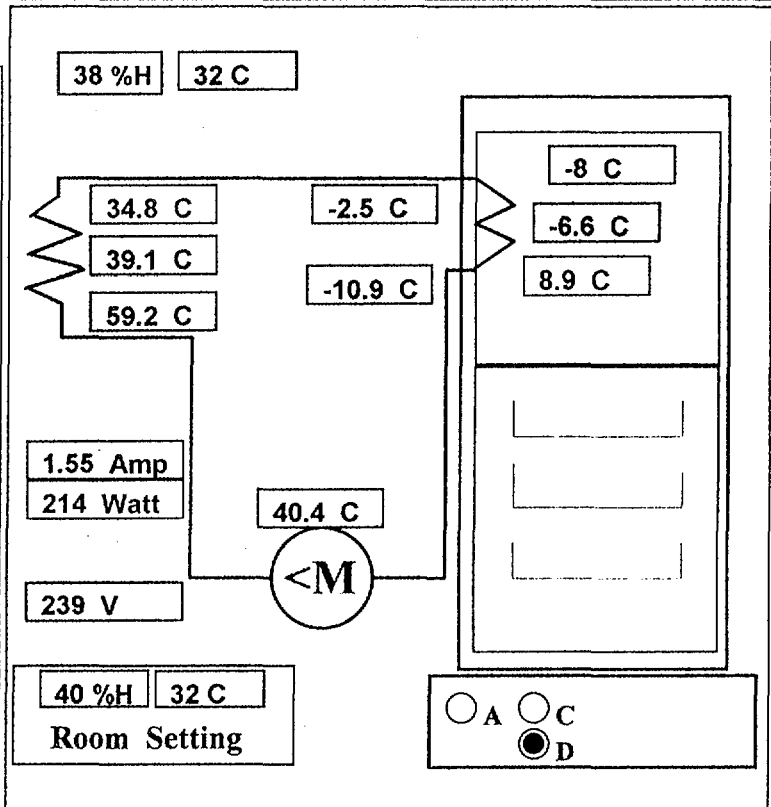
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

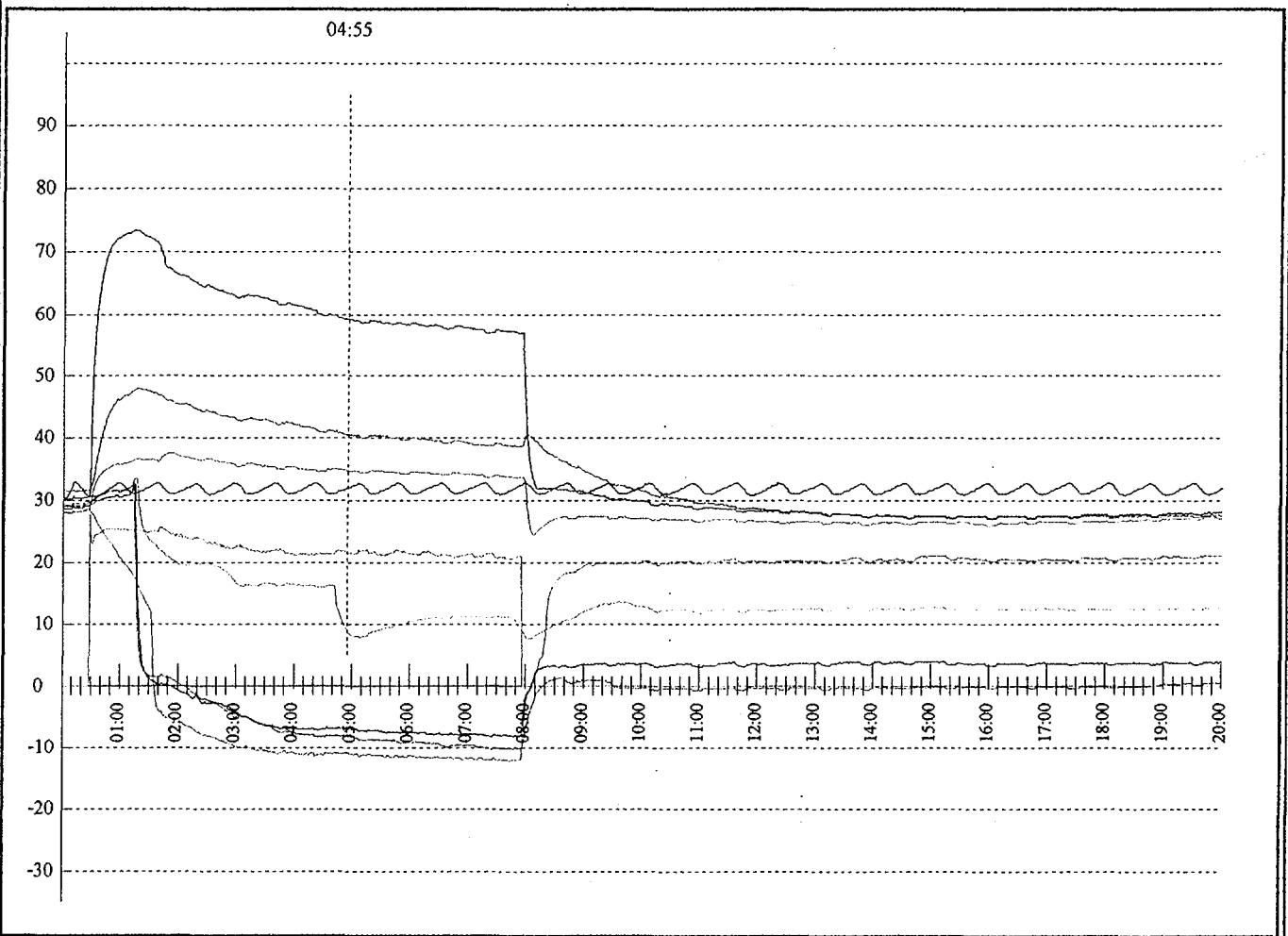
ReportDate: 99/07/16 15:49

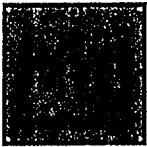
### Page Result :

- 1 - Page Test Time            20 Hours
- 2 - Working Percent         37 %On
- 3 - Energy (Accord to page) 0.312 kwh
- 4 - Zoom Time                4:55 Hour
- 5 - Compr Current            1.55 Amp
- 6 - Evaprator Mean Temp    6.3 C
- 7 - Cabin Mean Temp        30.4 C
- 8 - Crisp Temp              30 C
- 9 - Compr Temp              40.4 C
- 10- Condensor In Temp      59.2 C
- 11- Condensor Out Temp    34.8 C
- 12- Condition                32 C 38 %H
- 13- Volt    Max=245 Mean=237 Min=218
- 14-
- 15-
- 16-
- 17-



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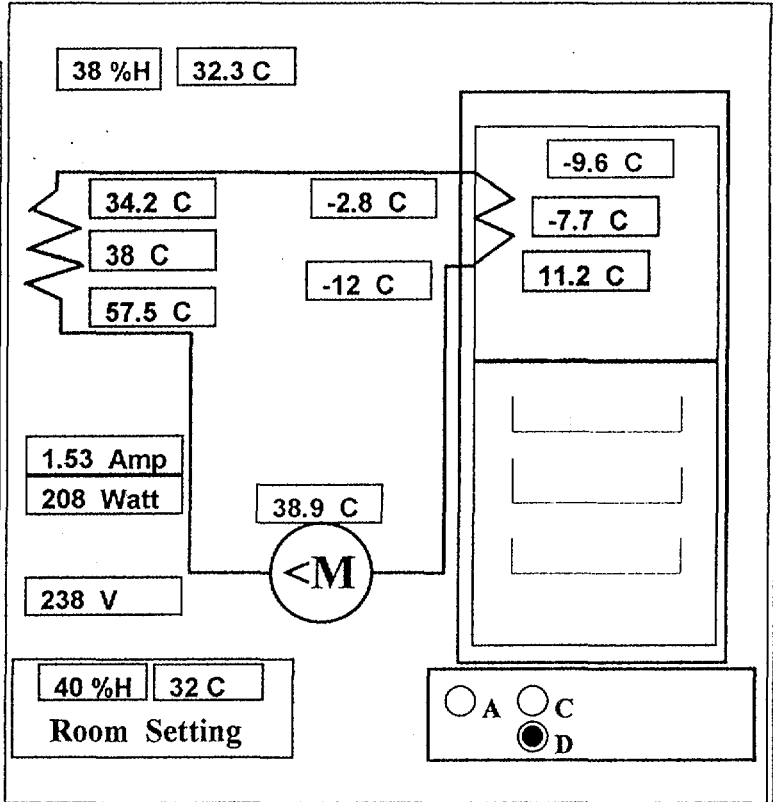


TestDate: 99/07/15 15:36  
PageTestName: Energy Consumption

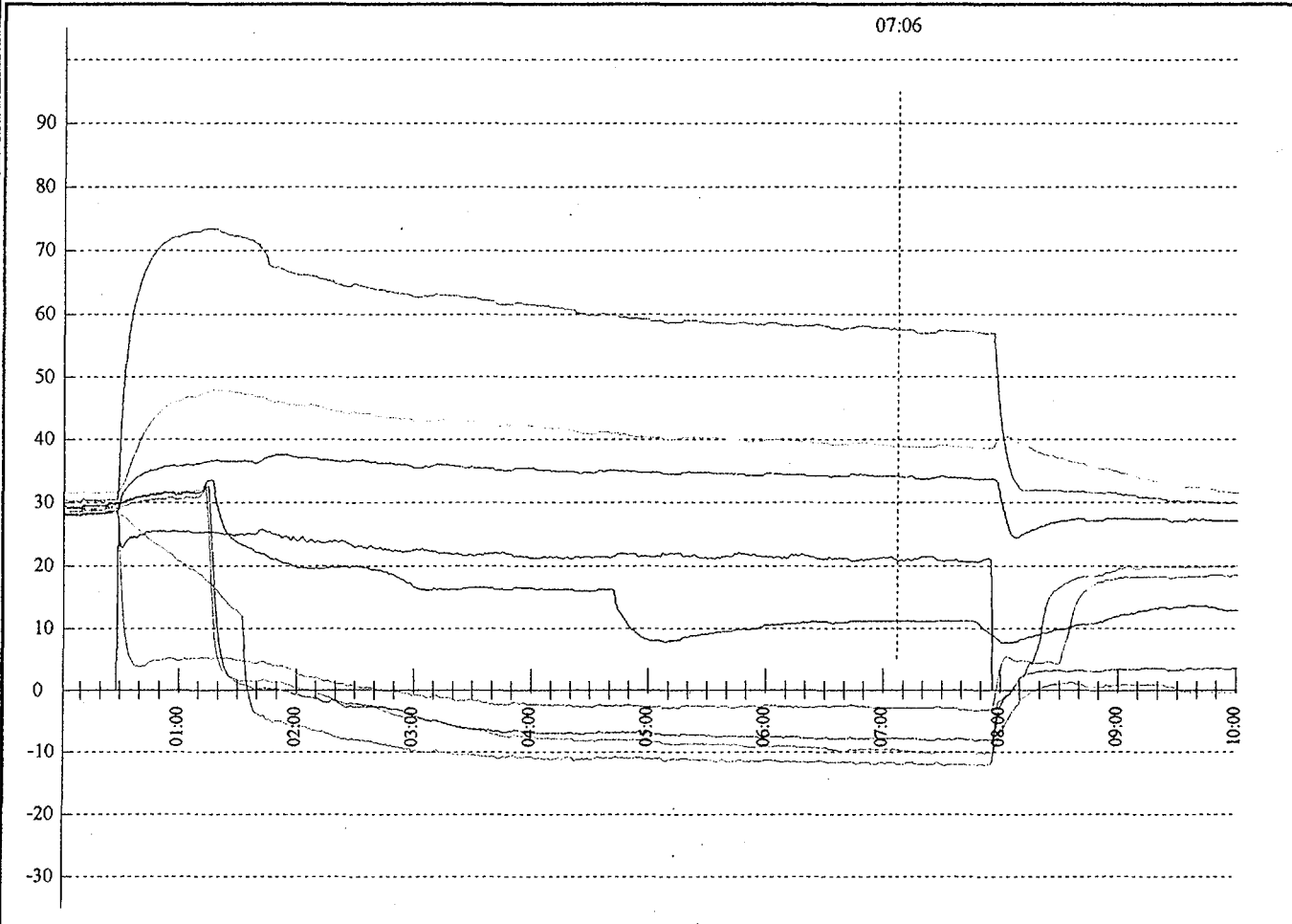
Report No.: ( ) - Page 1  
ReportDate: 99/07/16 15:23

**Page Result :**

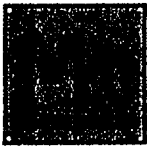
- 1 - Page Test Time 10 Hours
- 2 - Working Percent 74 %On
- 3 - Energy (Accord to page) 0.626 kwh
- 4 - Zoom Time 7:07 Hour
- 5 - Compr Current 1.53 Amp
- 6 - Evaprator Mean Temp 6 C
- 7 - Cabin Mean Temp 30 C
- 8 - Crisp Temp 29.7 C
- 9 - Compr Temp 38.9 C
- 10- Condensor In Temp 57.5 C
- 11- Condensor Out Temp 34.2 C
- 12- Condition 32.3 C 38 %H
- 13- Volt Max=245 Mean=237 Min=218
- 14-
- 15-
- 16-
- 17-



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TestDate: 99/07/15 15:36

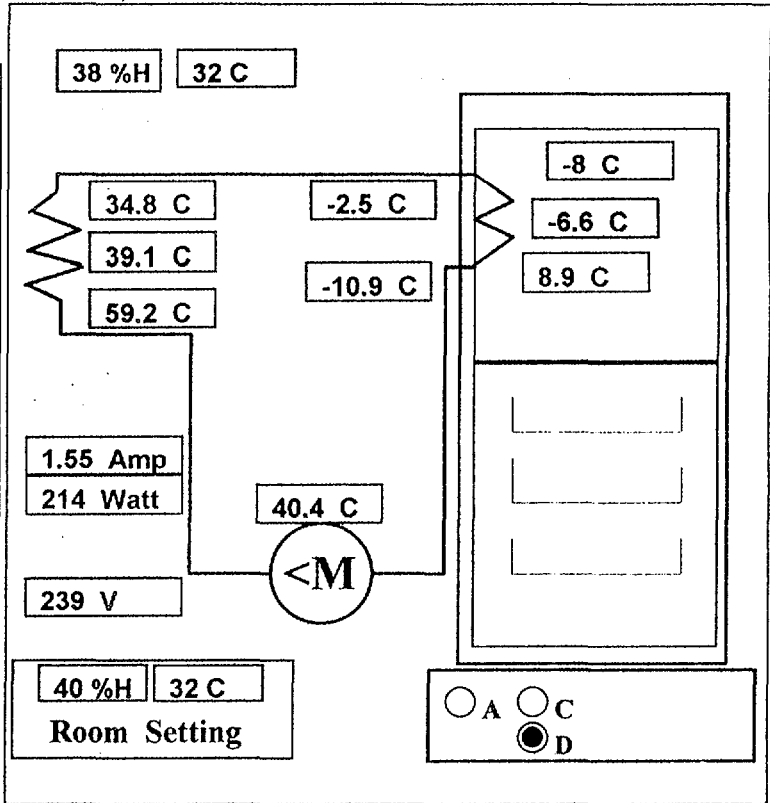
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

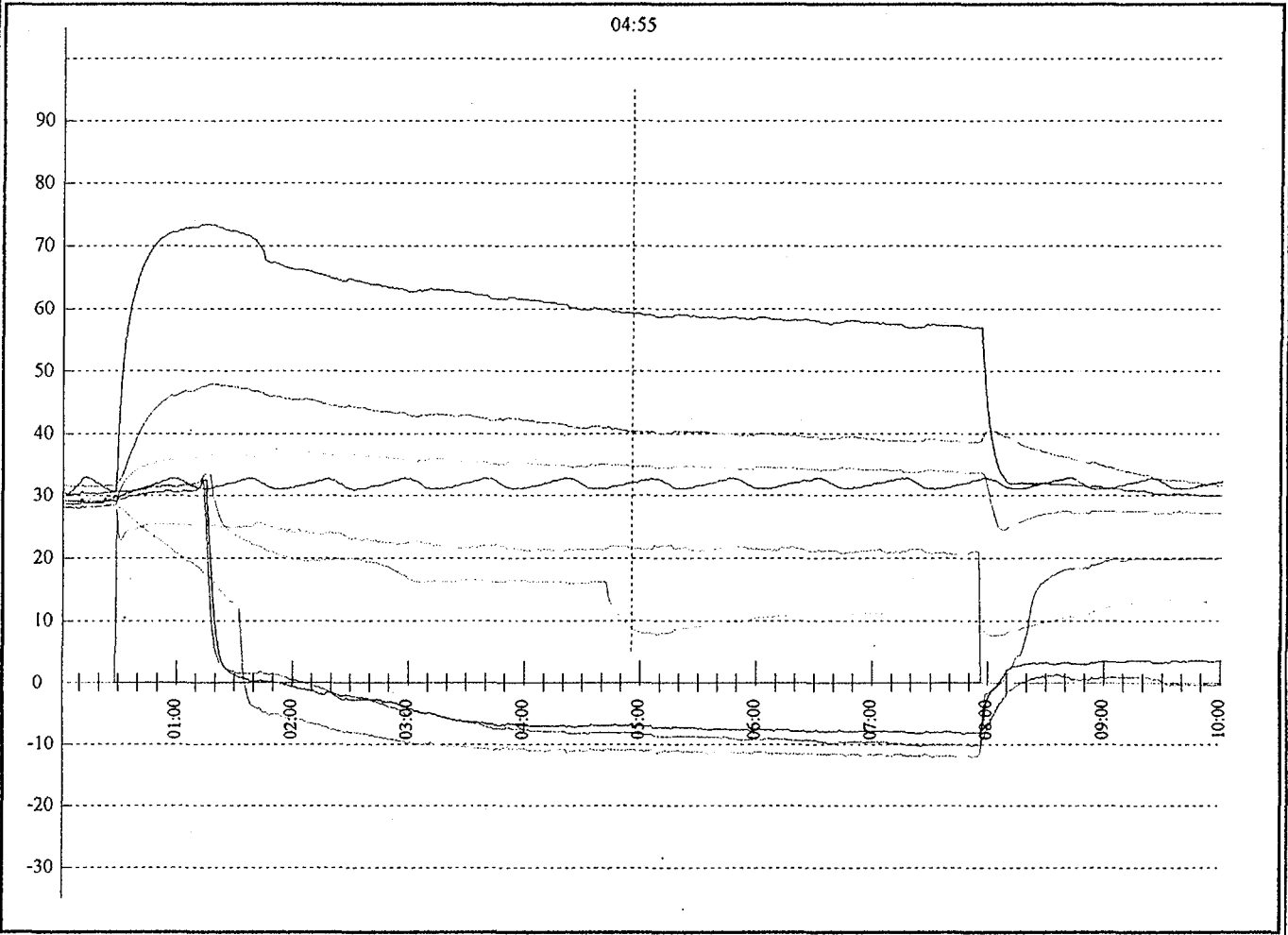
ReportDate: 99/07/16 15:47

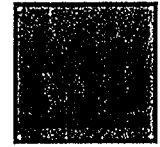
**Page Result :**

- 1 - Page Test Time 10 Hours
- 2 - Working Percent 74 %On
- 3 - Energy (Accord to page) 0.626 kwh
- 4 - Zoom Time 4:55 Hour
- 5 - Compr Current 1.55 Amp
- 6 - Evaprator Mean Temp 6.3 C
- 7 - Cabin Mean Temp 30.4 C
- 8 - Crisp Temp 30 C
- 9 - Compr Temp 40.4 C
- 10- Condensor In Temp 59.2 C
- 11- Condensor Out Temp 34.8 C
- 12- Condition 32 C 38 %H
- 13- Volt Max=245 Mean=237 Min=218
- 14-
- 15-
- 16-
- 17-



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TestDate: 99/07/15 15:36

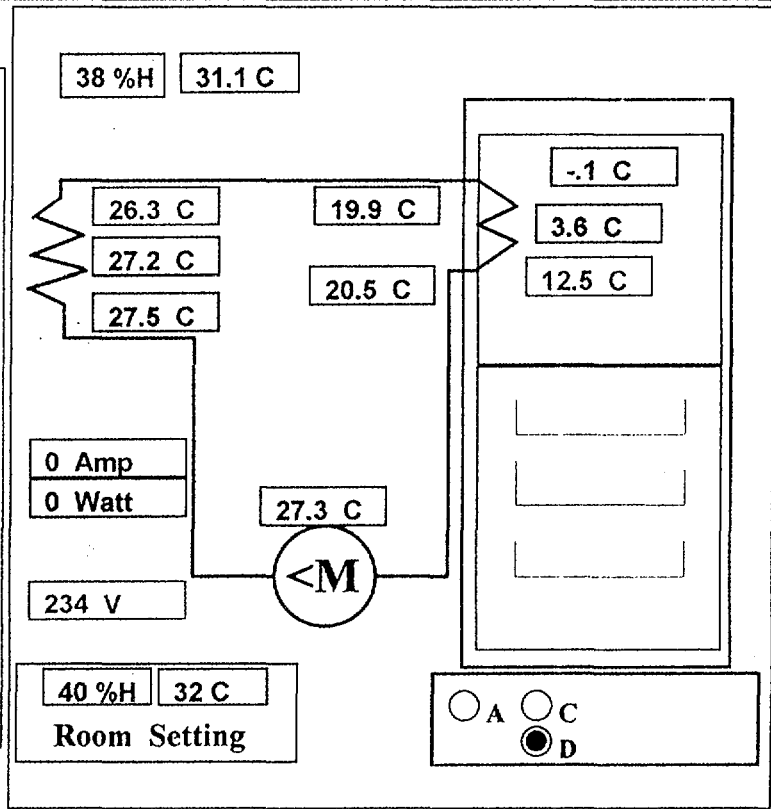
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

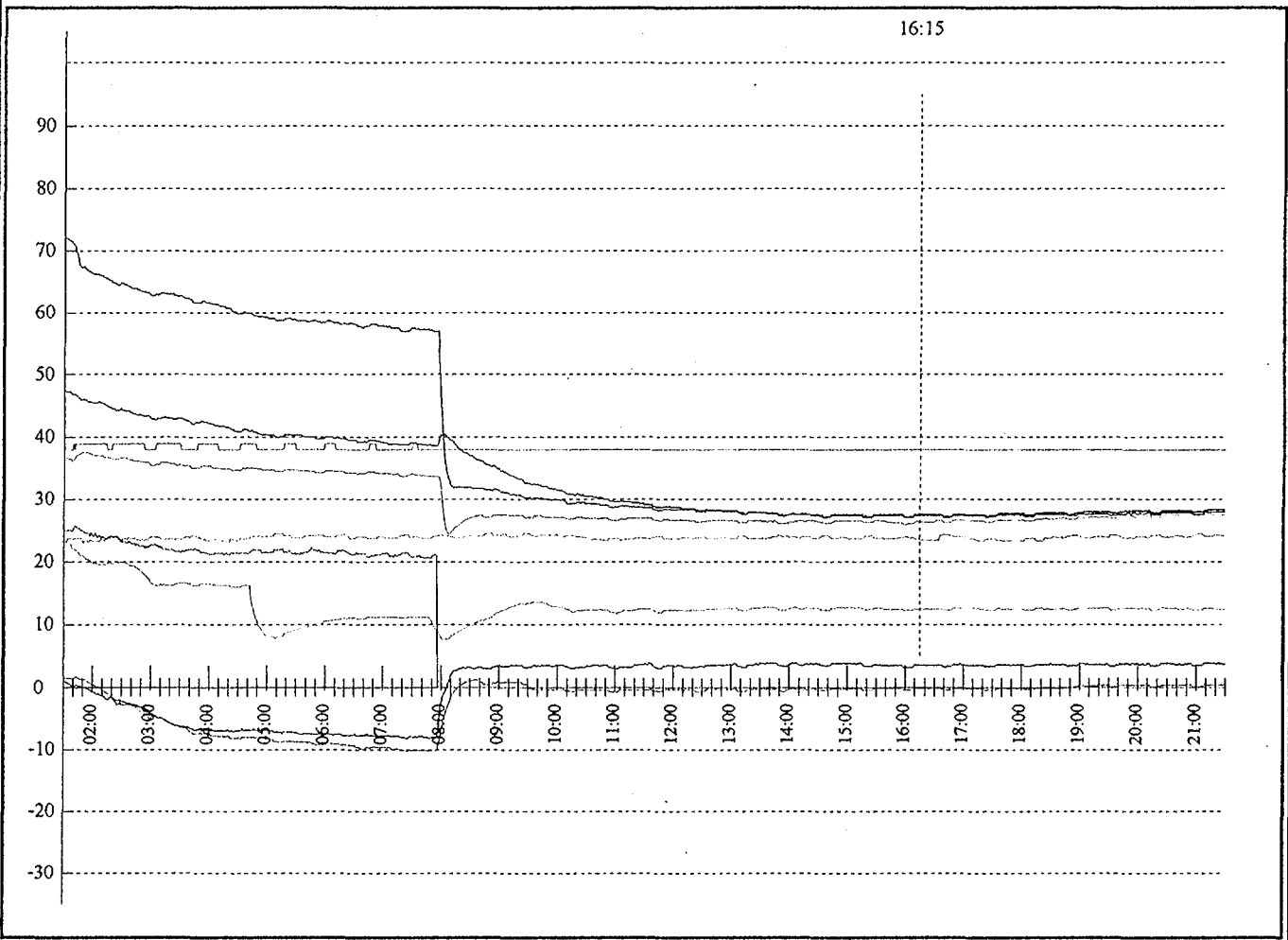
ReportDate: 99/07/16 15:55

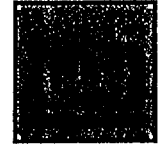
### Page Result :

- 1 - Page Test Time 20 Hours
- 2 - Working Percent 32 %On
- 3 - Energy (Accord to page) 0.239 kwh
- 4 - Zoom Time 16:15 Hour
- 5 - Compr Current 00 Amp
- 6 - Evaprator Mean Temp 11 C
- 7 - Cabin Mean Temp 28.7 C
- 8 - Crisp Temp 28.8 C
- 9 - Compr Temp 27.3 C
- 10- Condensor In Temp 27.5 C
- 11- Condensor Out Temp 26.3 C
- 12- Condition 31.1 C 38 %H
- 13- Volt Max=245 Mean=238 Min=229
- 14-
- 15-
- 16-
- 17-



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TestDate: 99/07/15 15:36

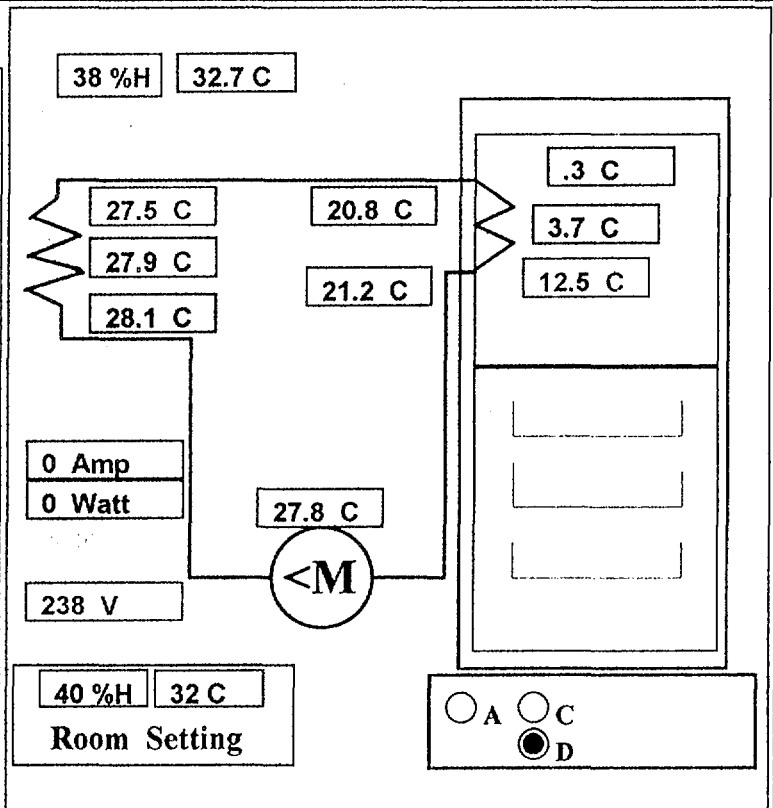
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

ReportDate: 99/07/16 15:57

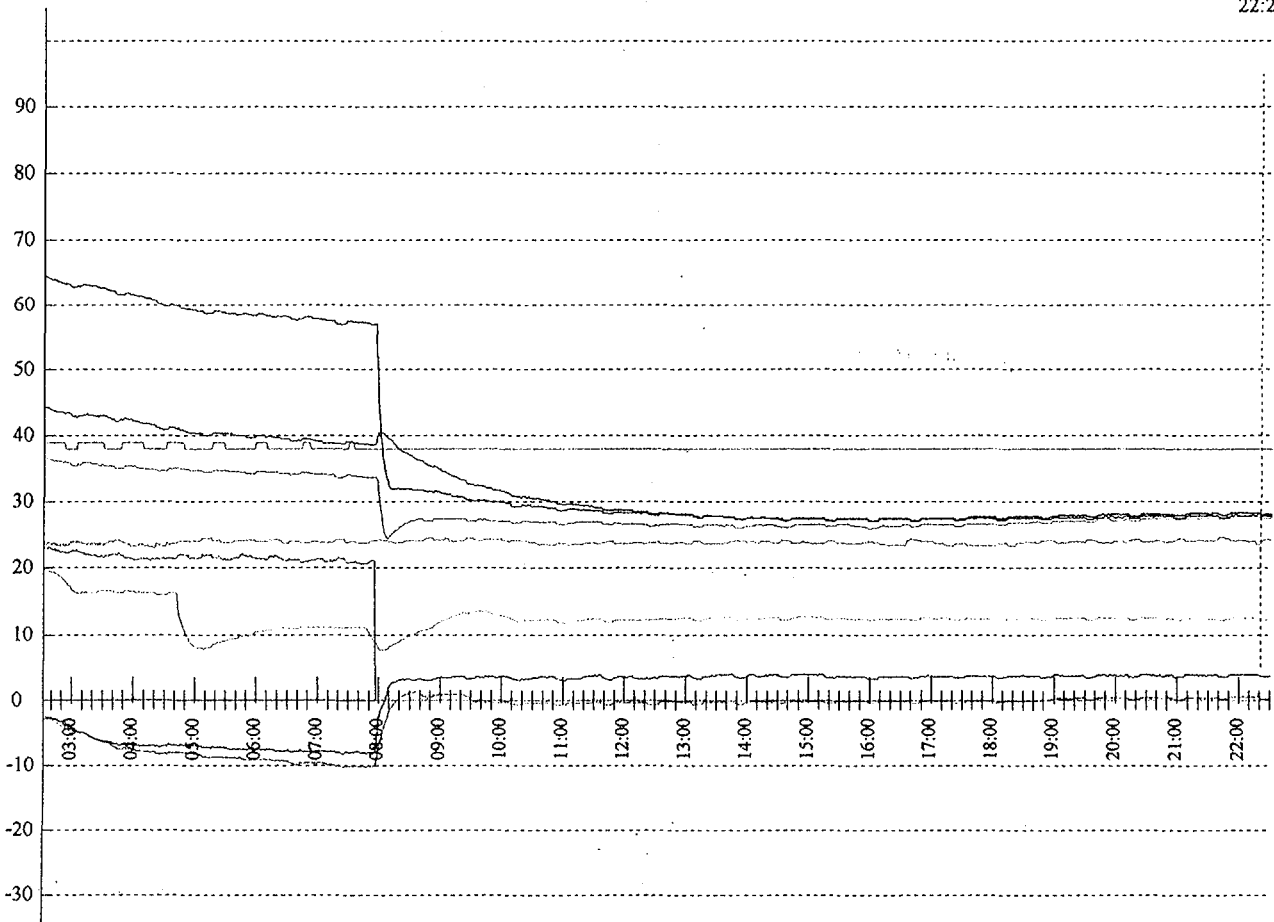
### Page Result :

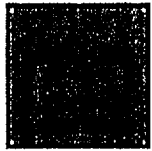
1 - Page Test Time	20 Hours
2 - Working Percent	26 %On
3 - Energy (Accord to page)	0.18 kwh
4 - Zoom Time	22:21 Hour
5 - Compr Current	00 Amp
6 - Evaprator Mean Temp	11.2 C
7 - Cabin Mean Temp	29 C
8 - Crisp Temp	29.1 C
9 - Compr Temp	27.8 C
10- Condensor In Temp	28.1 C
11- Condensor Out Temp	27.5 C
12- Condition	32.7 C 38 %H
13- Volt	Max=246 Mean=239 Min=230
14-	
15-	
16-	
17-	



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22:21





TestDate: 99/07/15 15:36

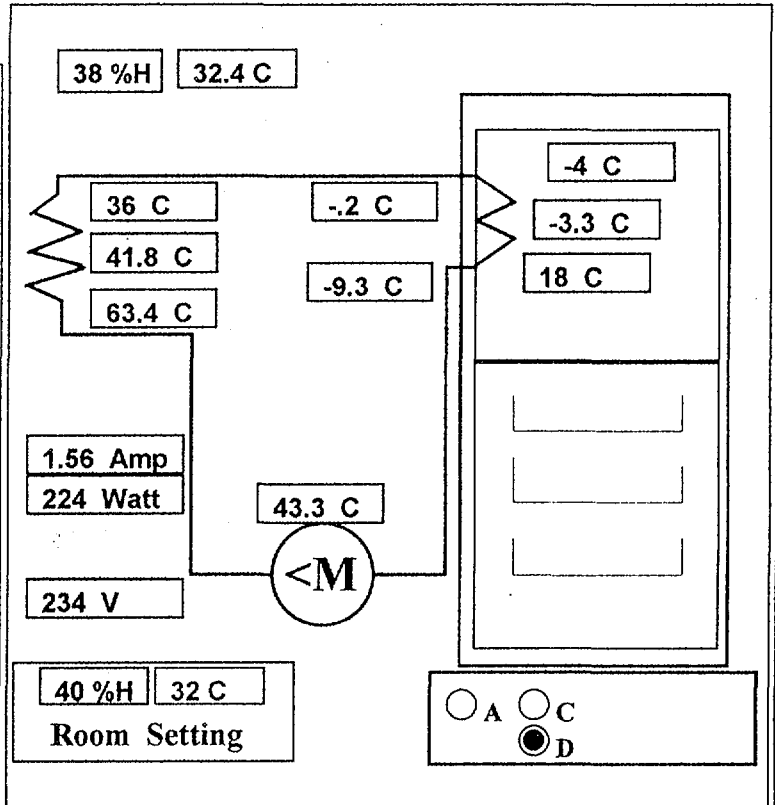
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

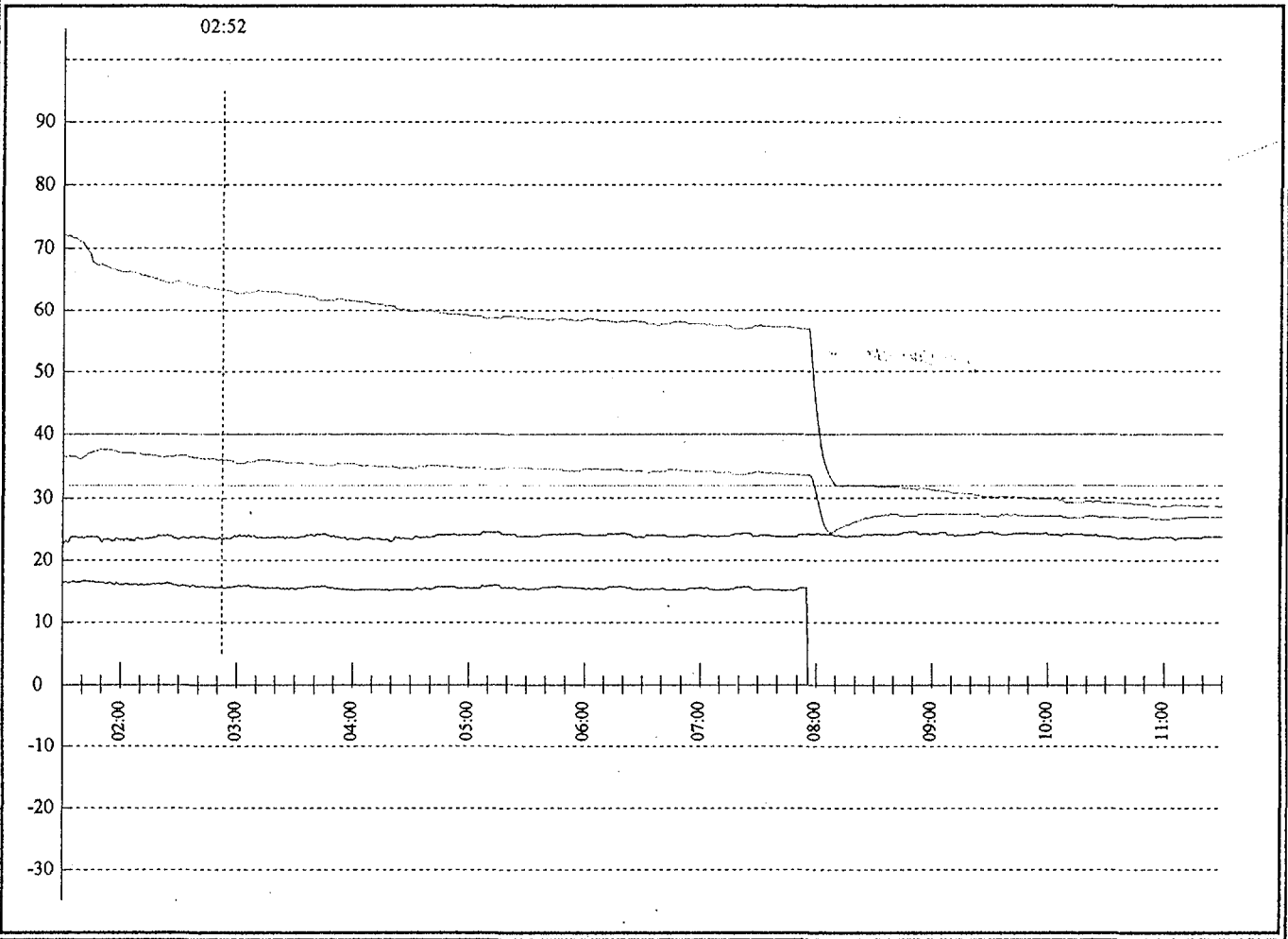
ReportDate: 99/07/16 16:00

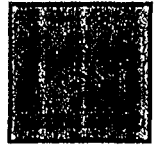
**Page Result :**

- 1 - Page Test Time 10 Hours
- 2 - Working Percent 64 %On
- 3 - Energy (Accord to page) 0.479 kwh
- 4 - Zoom Time 2:53 Hour
- 5 - Compr Current 1.56 Amp
- 6 - Evaprator Mean Temp 10.6 C
- 7 - Cabin Mean Temp 31 C
- 8 - Crisp Temp 30.5 C
- 9 - Compr Temp 43.3 C
- 10- Condensor In Temp 63.4 C
- 11- Condensor Out Temp 36 C
- 12- Condition 32.4 C 38 %H
- 13- Volt Max=245 Mean=239 Min=229
- 14-
- 15-
- 16-
- 17-



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TestDate: 99/07/15 15:36

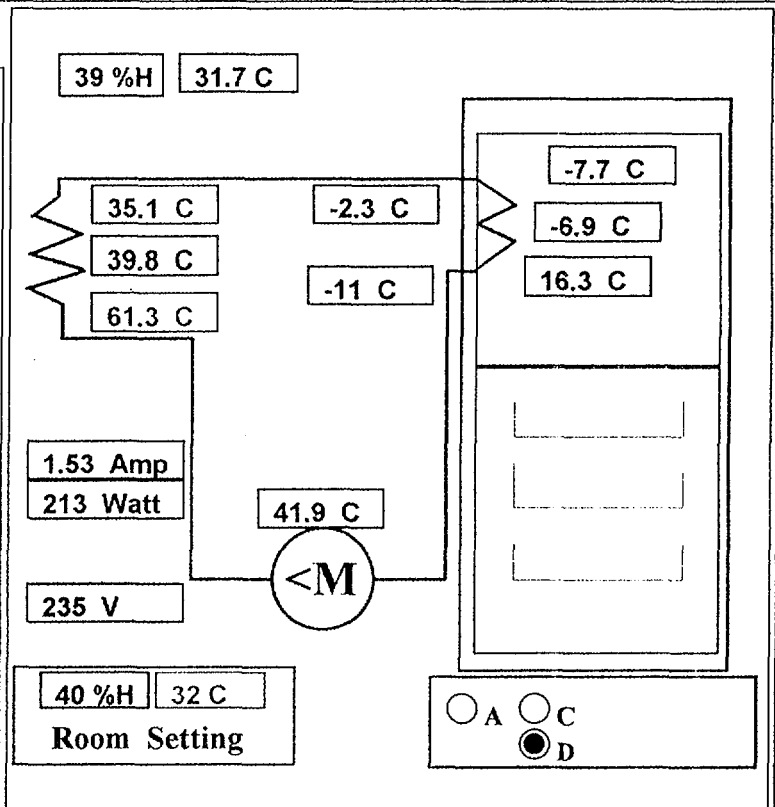
Report No.: ( ) - Page 1

PageTestName: Energy Consumption

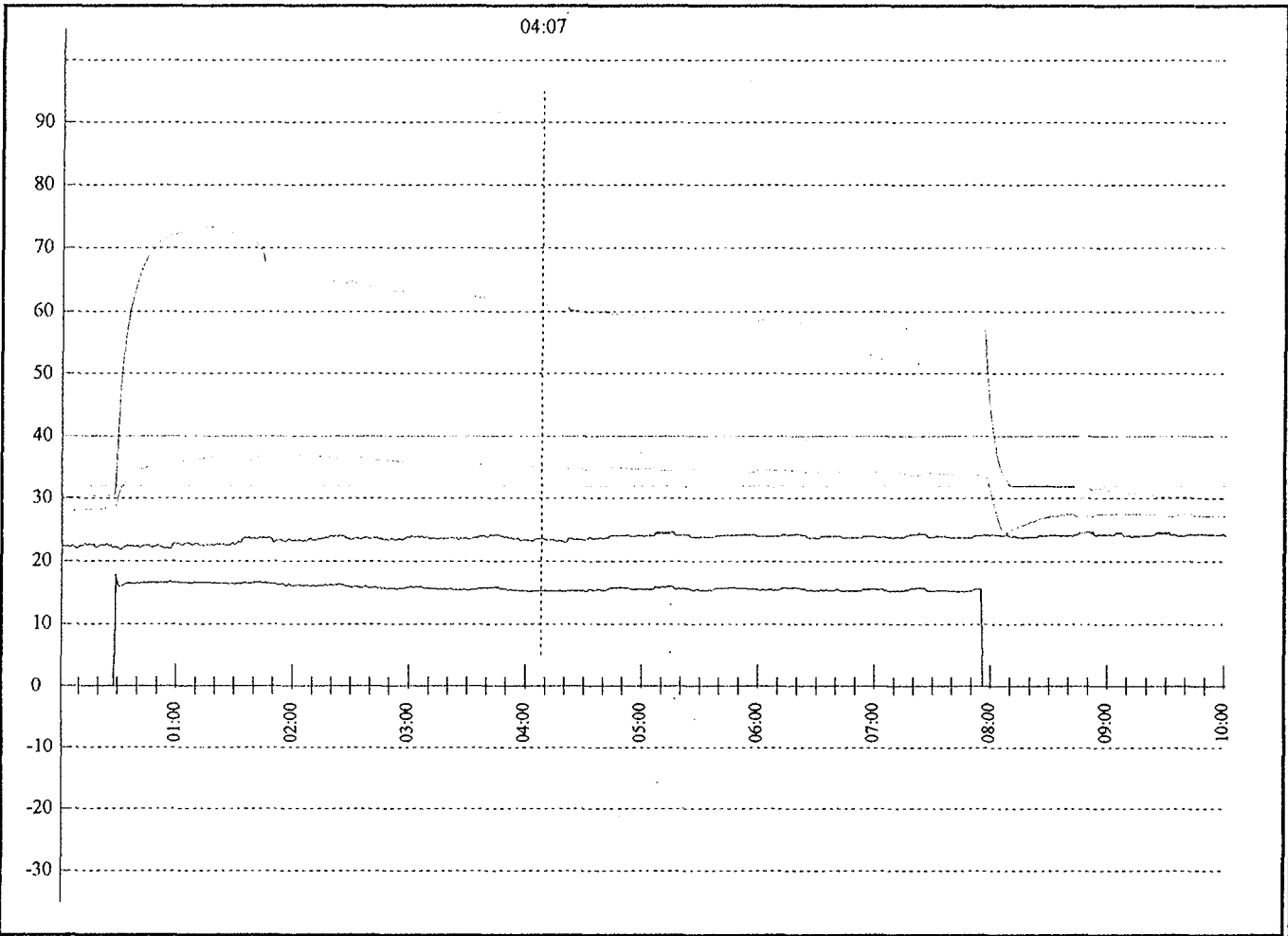
ReportDate: 99/07/16 16:02

### Page Result :

1 - Page Test Time	10 Hours
2 - Working Percent	74 %On
3 - Energy (Accord to page)	0.626 kwh
4 - Zoom Time	4:08 Hour
5 - Compr Current	1.53 Amp
6 - Evaprator Mean Temp	8.2 C
7 - Cabin Mean Temp	30.6 C
8 - Crisp Temp	30.2 C
9 - Compr Temp	41.9 C
10- Condensor In Temp	61.3 C
11- Condensor Out Temp	35.1 C
12- Condition	31.7 C 39 %H
13- Volt	Max=245 Mean=237 Min=218
14-	
15-	
16-	
17-	



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## General

This Report has been prepared. Based on the UNIDO TOR and relevant contrat between UNIDO and Maurice Al-Deek Co. to convert five prototype models into R134a refrigerant circuit system.

Considering all elements and technical services in the UNIDO,s TOR. And fulfill the entire project requirement in Maurice Al-Deek Co to phase out CFC-12.

The project will phase out the use of CFC-12 for the production of commercial refrigerator at Maurice Al-Deek Co. The implementation of this project will enable Maurice Al-Deek Co. to convert R12 commercial refrigerator system of its products into Ozone friendly R134a refrigerant System.

Based on Montreal and Jordan agreement, R134a refrigerant was selected as suitable Ozone friendly Refrigerant replacement and an alternative for R12 refrigerant and also Cyclopentane as a substitute for R11.

This change to the cooling system requires significant modification and improvement of cooling system. Due to the enhanced physical and chemical properties of the new refrigerant the main components of the cooling circuits must be replaced or adjusted as a consequence of substitution of R12 into R134a.

This report contencs, calculation of prototypes for determination of cooling capacity of each prototypes and also selecting compatible compressor for substituting R12 compressor with R134a compressor, because this is the first step for making prototype. It is indeed a difficult job to find precise compressor capacity to much the installed R12 compressor in the Jordanian market.

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The technical data will help us to calculate required refrigeration load that should be produced by the compressor and evaporators. For making prototypes our policy is to keep the existing size of condenser and evaporator and perform minor changes as required in cooling circuit, we think that minor adjustment will be required in refrigerant weight charge and probably in length of capillary tube.

In this report we will give some detailed technical data in different tables for each prototype model and then we calculate the refrigeration load calculation for each prototype.

### Company Background

Maurice Al-Deek Establishment for Refrigeration & Metal Industries was founded in March 1980, the factory started with 500 sq. meters of premises and four workers to manufacture commercial refrigerators. The company proceeded to expand its activities and increase to production rate and models to cover also Chest Freezers and Water Coolers.

In 1983 the company extended the existing facility from 500-sq. meters to 2500 sq. meters, the total staff also increased to 25 persons. The production of different commercial refrigerators also increased to furnishing restaurants, bakeries and supermarkets with all their needs of commercial refrigerators, freezers, stands, shelves, tables And show cases.

In 1985 the company opened its first show room in the center of Amman and in 1986 the OMS Low Pressure Foam Dispensing machine was installed at the factory, and at the same time the company's staff was

increased to 40 persons. Production of sandwich panels for making cold rooms and building hangers and making pharmaceutical factories with insulated tanks and doors were started at this time.

At present, the factory produces various models of Commercial

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refrigerators, water coolers, freezers, cold rooms with different capacities and upon request models. 70 staff are working for the company as engineer, technicians, and workers in different production lines and two equipped service cars.

### **Aim of the Project**

The aim of the immediate project is to;

Design, calculate and drafting for model redefinition.

Testing two prototypes for functionality and performance criteria.

Redesign the cooling units of the all models so that they could run on the new Ozone friendly R134a instead of the ODP active CFC12.

### **Scope of the Contract**

A study will be made for 5 models of commercial refrigerators made by Maurice Al-Deek Co. to specify;

Dimensional specification;

Type and thickness of insulation

Refrigeration unit component details

Working performance

Energy consumption

Selection of HFC 134a compatible components

Redesign of the refrigeration circuit as necessary

Specifying necessary changes in the cooling system if required

Preparation of the trial equipment one prototype per model

Testing of two prototypes for functionality and performance

Evaluation of the test results

### **Supply of the Material**

Following components and material been used to make prototypes as necessary.

R134a Compressors R134a Refrigerant

Refrigerant Accumulators



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Specially designed filter drier  
Specially designed evaporator and condenser

Some necessary modification of the side panels as required with the new design criteria  
Consumable material as required

### **Activities**

In this report we will give some detailed technical data in different tables for each prototype model and then we calculate the refrigeration load calculation for each prototype.

The prototypes were tested under designated ambient temperature mostly at + 32 C, the test performance revealed that no significant changes is necessary for refrigeration system circuit, because the original size of evaporator and condensers are much bigger than cooling requirements.

The adjustment will be applied to the mainly to the amount of refrigerant charge and length of capillary tube.

Each prototypes should under go for performance test at the following test criteria.

Pull down test at + 32 C

Continuos run Test at = 32 C ambient temperature

Cyclic run test at + 32 C ambient temperature.

The test condition was selected in accordance with appropriate ISO test standards.

All prototypes were tested at existing hot chamber in our facilities in Awajan Amman

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the test results sheet will be provided after necessary performance test evaluation and perform necessary modification.

Before making prototypes we conducted a training course to train the six companies to make their own prototypes and also make them familiar with the new technology.

The following topics were thought during the theatrical training course.

An orientation to UNIDO CFC phase out project.

Montreal Protocol

Ozone Layer and CFC side effect to Ozone layer

Familiarization with new R134a Refrigerant, application, safety precaution, use and maintenance.

Familiarization with the new vacuum and charging equipment, vacuum pump and charging board.

Recovery and recycling of R12 refrigerant, and also R134a.

Alternative for R11 and R12.

Some explanation about R141b blowing agent,

Selection of refrigeration components to be replaced with R12 refrigeration system.

Calculation and redesign of prototypes

Performance test

Test results Evaluation.

Refrigeration system adjustment.

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The material as sample for making prototypes were supplied mainly from local market, due to the limitation for purchasing R134a compressor from local market we had to contact several manufacturers to find out the technical specification for appropriate compressor.

The prices for material specially R134a and R141b blended polyol are much higher than R12 and R11, for instance the price for one kg of R11 blended polyol is about 3.21 US\$ and the price for R141b blended polyol is 3.92 US \$ it means 0,71 US \$ more.

We also invested a lot of money to make our hot chamber, we hope that UNIDO will help us to purchase PC computer and relevant heat and cooling system measuring devices. Such as data loggers electronic control panels PC software and temperature sensors. Having our hot chamber operation is an importance for completion of conversion project of the prototypes, therefore we urge to construct and complete the hot chamber as soon as possible.

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**Refrigeration Load Calculation for different type of  
Water Coolers**

Water cooler cabinet usually consist of a sheet metal housing built around a steel framework, inside this sheet housing there is usually a condensing unit, located near the floor, and above this is the water-cooling mechanism. The latter is the only part insulated (foamed plastic) from the room. The insulation is usually specially formed and between one and one half inches and two inches thick. These cabinets are made in such a way that one or more sides may be easily removed to gain access to the interior. The basin of the water cooler is generally made of porcelain-coated cast iron, porcelaicoated - steel, or stainless steel. Heat exchangers are frequently used on water coolers. These make use of the low temperature of waste water and the suction line to pre-cool the fresh water line to the evaporator coil.

Self-cooler are of two types,

1- □ Bottle Type.

2- □ Tap water type

The bottle cooler usually uses a 20 to 25 liter bottle of water inverted on the top of the cabinet. Overflow and drain water are stored in a container built the cabinet. These coolers use air-cooled condensing units exclusively. They are used where water and drains are not available or where available the plumbing insulation may be expensive.

Water cooler using a plumbing supply and drain connection, must be installed according the relevant approved standards. The plumbing should be concealed, a hand shutoff valve should be installed in the fresh water line. Drain pipe at least 1 1/2 inches in diameter provided, and rubber opening must be above the drain in such a way as to eliminate the chance for accidental siphoning of the drain water back into the fresh water system. The tap water models use variety of evaporator coil wrapped around the water-cooling tank.

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Temperatures of the cooling water are variable depending on the persons who are drinking the water. We consider 10 C for the temperature of drinking water, while our inlet temperature is considered 24 C.

In large business establishment, in office buildings, or in factories, multiple water cooler, instead of individual ones, are popular. These

coolers have one large condensing unit supplying many bubbles and these may be of many different types.

Water cooler is a device that usually is used in the public area to supply cold drinking water to the customers and different people. The appliance is mainly used in

the Airports, Railways Station, Coach Terminals, Banks, Offices, Parks, and etc. therefore, it is hard to specify an standard for cold water consumption during the day from the water cooler.

We consider three refrigeration load components that should be taken into our consideration.

Heat gain by heat transmission from, main water storage tank wall insulation.

Heat removed from water entering to the water tank at the initial refrigeration system operating condition, (water stored in storage tank during the night, with normal ambient temperature) which is divided by 24 hrs.

Heat removed from Drinking Water flow that are consumed during designated operating hours " $\dot{M}$ "

The problem of determining the refrigeration load of a water-cooled installation is basically a specific heat and heat leakage problem combination. The water is cooled to temperature which vary upward from about 4 degree centigrade , and the amount heat removed from

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the water to cool it to a predetermined temperature is simple specific heat problem. The water, being maintained at these low temperature,

results in a heat leakage from room into the water, and this part involves the heat leakage portion of installation.

$Q_1 = m C \Delta T$ , Where:

$Q_1$  Total heat removed from total drinking water tank volume capacity (lit.) during specific period, related to compressor cooling capacity power in Watts, at initial compressor start up, and early in the morning. When the water temperature is 30 C.

$m$  total weight of water in the water cooler storage tank in Kg. Considering that one litter of water at 24 C is equal to approximately one Kg.

$C$  Specific heat factor of water in Kcal/Kg °C

$\Delta T$  Temperature difference ( $T_i - T_c$ ), where,  $T_i$  is inlet water temperature, and  $T_c$  is final cooled water.

$$Q_2 = \dot{M} C \Delta T$$

$Q_2$  Total heat removed from total drinking water flow (lit.) during specific period, 16 hours. In Kcal.

$\dot{M}$  total weight of water flow during 16 hours. in Kg.

$C$  Specific heat factor of water in Kcal/Kg °C

$T$  Temperature difference ( $T_i - T_c$ ), where,  $T_i$  is inlet water temperature, and  $T_c$  is final cooled water temperature.

$$Q_3 = UA \Delta T$$

Where:

$Q_3$  Total Leak, gained through side wall of drinking water storage tank by conduction in Kcal..

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- U Heat Resistance Coefficient Factor in Kcal/Sq. mt. C  
A Total Area which heat is transmitted by. In Sq. Mt.  
 $\Delta T$  Temperature difference ( $T_a - T_c$ ), where,  $T$  is ambient temperature, and  $T_c$  is final cooled water temperature.

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Upright Show Case Model MSD-200 Technical Specification	
Show Case Upright Refrigerator	Type of Product
2000 x 800 x 2000 mm	Overall Dimension
40 mm	Wall Thickness
P.U. Foam R11	Type of Foam
35 - 40 Kg/ cu mt.	Foam Density
100 ISO, 100 Polyol, 35 R11	Foam Mixing Ratio %
1800 lit.	Net Internal Volume
Hermetic, Air Cooled	Type of Compressor
1173 Watts at -15 C	Compressor Cooling Capacity
Fin and Tube	Type of Condenser
4, four rows	Size of Condenser
Fin and Tube	Type of Evaporator
R12	Type of Refrigerant
R12, = 650 Gr.	Refrigerant Charge
30 Gr.	Filter Drier Size
220/50	Power Source
- 15 °C	Designated Inside Evaporator Temperature
5 °C	Designated Inside Ref. Temperature
Standard 32 °C	Designated Operating Condition



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**Refrigeration Load Calculation**  
**Upright Refrigerator Showcase Model MDS- 200**

a) Transmission load calculation

Refrigerator Compartment	Dimension Cm.	Area (sq.mt.)	Insulation Thickness	Temp. Difference
Side Walls	2 x (120x55) + 2x(80x40)	1.96	40mm	27 c
Back Panel	200x160	3.2	40mm	27 c
Top Surface	80x200	1.6	40mm	27 c
Lower Panel	40x200	0.8	40mm	27 c
Bottom Surface	80x200	1.6	40mm	37 c
Door	120x270	3.24	15mm air	27 c

Insulation Type: Pu Foam with R141b blowing agent.

Thermal Conductivity for Foam = 0.0180 W/ mt. ° C

Thermal Conductivity for Air at -12 at 1 atm. =0.02367 W/mt. ° C

Temperature Difference Refrigerator Compartment:

$$\Delta T = 32 - (+5) = 27 \text{ }^\circ\text{C}$$

Ambient Temperature = 32 °C

Refrigerator Air Temperature = +5 °C

Calculation , Heat Leak For Refrigerator Compartment.

$$Q_{TL} = Q_{SW} + Q_{Back\ Panel} + Q_{door} + Q_{Bottom} + Q_{Top} + Q_{lowe\ Panel}$$

$$Q = U A (T_a - T_r)$$

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$$U = \frac{1}{X_1 / K_1}$$

Where :

U = Heat Resistance Coefficient Factor,  $K_1$  = Foam Thermal Conductivity

Due to the short thickness of cabinet out side panel ( 0.6 mm ) and plastic inner liner ( 1.5 mm ) heat resistance of these materials have been considered negligible.

Therefore:

$$Q_{\text{SideWalls}} = [ U A ( T_a - T_r ) ]$$

$T_a$  = Ambient Temperature

$T_r$  = refrigerator air Temperature

$$U = 1 / ( 0.040 / 0.0180 ) = 0.45 \text{ W/ sq.m } ^\circ\text{C}$$

$$A = 1.96 \text{ Sq. Mt.,}$$

$$T_a = 32 \text{ } ^\circ\text{C}$$

$$T_r = + 5 \text{ } ^\circ\text{C}$$

therefore

$$Q_{\text{SideWalls}} = 0.45 \times 1.96 \times 27 = 24 \text{ Watts}$$

$$Q_{\text{SideWalls}} = 24 \text{ Watts}$$

$$Q_{\text{Door glass}} = [ U A ( T_a - T_r ) ]$$

$$U = 1 / ( 0.015 / 0.024 ) = 1.6 \text{ W/ sq.m } ^\circ\text{C}$$

$$T_a - T_r = 27$$

$$A = 3.24$$

$$Q_{\text{door}} = 1.6 \times 3.24 \times 27 = 140 \text{ Watts}$$

$$Q_{\text{door}} = 140 \text{ Watts}$$

$$Q_{\text{Back panel}} = [ U A ( T_a - T_r ) ]$$

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$$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C,}$$
$$T_a - T_r = 27$$
$$A = 3.2$$

$$Q_{\text{Back panel}} = 0.45 \times 3.2 \times 27 = 39 \text{ Watts}$$

$$Q_{\text{Back panel}} = 39 \text{ Watts}$$

$$Q_{\text{lower panel}} = [U A (T_a - T_r)]$$

$$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C,}$$
$$T_a - T_r = 27$$
$$A = 0.8$$

$$Q_{\text{lower panel}} = 0.45 \times 0.8 \times 27 = 9.7 \text{ Watts}$$

$$Q_{\text{lower panel}} = 9.7 \text{ Watts}$$

$$Q_{\text{Top}} = [U A (T_a - T_r)]$$

$$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C,}$$
$$T_a - T_r = 27$$
$$A = 1.6$$

$$Q_{\text{Top}} = 0.45 \times 1.6 \times 27 = 19 \text{ Watts}$$

$$Q_{\text{Top}} = 19 \text{ Watts}$$

$$Q_{\text{Bottom}} = [U A (T_a - T_r)]$$

$$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C,}$$
$$T_a - T_r = 37$$
$$A = 1.6$$

$$Q_{\text{Bottom Surface}} = 0.45 \times 1.6 \times 37 = 27 \text{ Watts}$$

$$Q_{\text{Bottom Surface}} = 27 \text{ Watts}$$

$$\text{Total Refrigerator Heat Leak} = 24 + 140 + 19 + 27 + 9.7 + 39 = 258.7 \text{ W}$$

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**Product Load**

A product placed in a refrigerator at a temperature higher than the storage temperature will lose heat until it reaches the storage temperature. The quantity of heat to be removed may be calculated from knowledge of the product, including its state upon entering the refrigerator, its final state, its weight, specific heat above and below freezing point, its freezing temperature and latent heat. When a definite weight of product is cooled from one state and temperature to another state and temperature, some or all of the following calculations must be made:

Heat removal from initial temperature to some lower temperature above freezing.

$$Q = mc(T_1 - T_2)$$

Heat removal from initial temperature to freezing point of product.

$$Q = mc(T_i - T_f)$$

Heat removal to freeze product.

$$Q = mh_{if}$$

Heat removal from freezing point to final temperature below freezing.

$$Q = mc(T_f - T_3)$$

Where

- Q = heat removed, Kj
- M = weight of product, kg
- C = specific heat of product above freezing point, Kj/Kg. K
- T<sub>1</sub> = initial temp. C
- T<sub>2</sub> = lower temperature above freezing, C
- T<sub>f</sub> = freezing temperature of product, C

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$H_f$  = latent heat of fusion, kj per kg

Since this product is mainly used for storing fresh Lamb meet and beef above freezing point at +5 C, we consider 800 Kg of milk products to be stored in this refrigerator therefore we calculate as follow,

$$Q = mc(T_1 - T_2)$$

$$M = 800 \text{ kg}$$

$$C = 0.87 \text{ Btu}/(\text{lb})\text{F deg} = 0.67 \times 4.184 = 3.7 \text{ j/g K}$$

$$T_1 = 25 \text{ C}$$

$$T_2 = 5 \text{ C}$$

$$Q = 800000 \times 3.7 \times (25 - 5) = 59200000 \text{ jul} / 86400 = 685 \text{ Watt}$$

Internal Load

Electric Fan 2x10 = 20 Watt

Florescent Lamp = 20 watt

Door Opening

Refrigerator Internal Volume 1800 lit.

Number of air change as per ASHREA standard = 70 per day

Heat removed per cubic meter of air 75000 j

Air Change load =  $1.8 \times 70 \times 75000 / 86400 = 109 \text{ Watt}$

$$Q_{\text{Total}} = Q_{\text{heat leak}} + Q_{\text{product load}} + Q_{\text{internal load}} + Q_{\text{air change}}$$

$$Q_{\text{Total}} = 685 + 258.7 + 20 + 20 + 109 = 1092.7 = 1093$$

Considering 10 % of Q total for safety factor

$$Q_{\text{Grand Total}} = 1093 + 10\%(109) = 1202 \text{ watts}$$

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With respect to the above calculation we have to select a compressor of R134a with cooling capacity of approximately 1202 watt at -15 degree centigrade evaporating temperature. We select a compressor to match with Electrolux model S34TY

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Meat Show Case Model MDR-160 Technical Specification	
Show Case	Type of Product
1600 x 800 x 2000 mm	Overall Dimension
40 mm	Wall Thickness
P.U. Foam R11	Type of Foam
30 - 40 Kg/ cu m	Foam Density
100 ISO, 100 Polyol, 35 R11	Foam Mixing Ratio %
1200 lit.	Net Internal Volume
Electrolux S26TY, Hermetic, Air Cooled	Type of Compressor
772 Watts	Compressor Cooling Capacity
Fin and Tube	Type of Condenser
3, rows	Size of Condenser
Fin and Tube = 15 meter	Type of Evaporator
R12	Type of Refrigerant
R12, = 600 Gr.	Refrigerant Charge
30 Gr.	Filter Drier Size
220/50	Power Source
- 15 °C	Designated Inside Evaporator Temperature
5 °C	Designated Inside Ref. Temperature
Standard 32 °C	Designated Operating Condition

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**Refrigeration Load Calculation**  
**Upright Refrigerator Showcase Model MDR-160**

a) Transmission load calculation

Refrigerator Compartment	Dimension Cm.	Area (sq.mt.)	Insulation Thickness	Temp. Difference
Side Walls	2 x (80x200)	3.2	40mm	27 c
Back Panel	160x200	3.2	40mm	27 c
Bottom	80x200	1.6	40mm	27 C
Top	80x200	1.6	40mm	37 c
Doors	160x200	3.2	40mm	27 c

Insulation Type: Pu Foam with R141b blowing agent.  
 Thermal Conductivity for Foam = 0.0180 W/ mt. ° C  
 Temperature Difference Refrigerator Compartment:  
 $\Delta T = 32 - (+5) = 27 \text{ }^\circ\text{C}$   
 Ambient Temperature = 32 °C  
 Refrigerator Air Temperature = +5 °C

Calculation :

Heat Leak For Refrigerator Compartment.

$$Q_{TL} = Q_{SW} + Q_{Back\ Panel} + Q_{door} + Q_{Bottom} + Q_{top}$$

$$Q = U A (T_a - T_r)$$

$$U = \frac{1}{X_1 / K_1}$$

Where :

U = Heat Resistance Coefficient Factor

K<sub>1</sub> = Foam Thermal Conductivity



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Due to the short thickness of cabinet out side panel ( 0.6 mm ) and plastic inner liner ( 1.5 mm ) heat resistance of these materials have been considered negligible.

Therefore:

$$Q_{\text{SideWalls}} = [ U A ( T_a - T_r ) ]$$

$T_a$  = Ambient Temperature 32

$T_r$  = refrigerator air Temperature 5

$$U = 1 / ( 0.040 / 0.0180 ) = 0.45 \text{ W/ sq.m } ^\circ\text{C}$$

$A = 3.2 \text{ Sq. Mt.}$ ,

$T_a = 32 \text{ } ^\circ\text{C}$

$T_r = + 5 \text{ } ^\circ\text{C}$

therefore

$$Q_{\text{SideWalls}} = 0.45 \times 3.2 \times 27 = 39 \text{ Watts}$$

$$Q_{\text{SideWalls}} = 39 \text{ Watts}$$

$$Q_{\text{doors}} = [ U A ( T_a - T_r ) ]$$

$$U = 1 / [( 0.040 / 0.018 ) ] = 0.45 \text{ W/ sq.m } ^\circ\text{C}$$

$T_a - T_r = 27$

$A = 3.2$

$$Q_{\text{doors}} = 0.45 \times 3.2 \times 27 = 39 \text{ Watts}$$

$$Q_{\text{doors}} = 39 \text{ Watts}$$

$$Q_{\text{top}} = [ U A ( T_a - T_r ) ]$$

$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C}$ ,

$T_a - T_r = 37$

$A = 1.6$

$$Q_{\text{top}} = 0.45 \times 1.6 \times 37 = 26.6 \text{ Watts}$$

$$Q_{\text{top}} = 26.6 \text{ Watts}$$

$$4 - Q_{\text{back panel}} = [ U A ( T_a - T_r ) ]$$

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$$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C,}$$

$$T_a - T_r = 27$$

$$A = 3.2$$

$$Q_{\text{back panel}} = 0.45 \times 3.2 \times 27 = 39 \text{ Watts}$$

$$Q_{\text{back panel}} = 39 \text{ Watts}$$

$$5 - Q_{\text{Bottom}} = [U A (T_a - T_r)]$$

$$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C,}$$

$$T_a - T_r = 27$$

$$A = 1.6$$

$$Q_{\text{Bottom Surface}} = 0.45 \times 1.6 \times 27 = 19.4 \text{ Watt}$$

$$Q_{\text{Bottom Surface}} = 19.4 \text{ Watts}$$

$$\text{Total Refrigerator Heat Leak} = 39 + 39 + 26.6 + 19.4 + 39 = 163 \text{ W}$$

### Product Load

A product placed in a refrigerator at a temperature higher than the storage temperature will lose heat until it reaches the storage temperature. The quantity of heat to be removed may be calculated from knowledge of the product, including its state upon entering the refrigerator, its final state, its weight,

specific heat above and below freezing point, its freezing temperature and latent heat.

When a definite weight of product is cooled from one state and temperature to another state and temperature, some or all of the following calculations must be made:

Heat removal from initial temperature to some lower temperature above freezing.

$$Q = mc(T_1 - T_2)$$

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Heat removal from initial temperature to freezing point of product.

$$Q = mc(T_i - T_f)$$

Heat removal to freeze product.

$$Q = m h_{if}$$

Heat removal from freezing point to final temperature below freezing.

$$Q = mc(T_f - T_3)$$

Where

Q = heat removed, Kj

M = weight of product, kg

C = specific heat of product above freezing point, Kj/Kg. K

T<sub>1</sub> = initial temp. C

T<sub>2</sub> = lower temperature above freezing, C

T<sub>f</sub> = freezing temperature of product, C

H<sub>if</sub> = latent heat of fusion, kj per kg

Since this product is mainly used for storing fresh Lamb meet and beef above

freezing point at +5 C, we consider 600 Kg of meet to be stored in this refrigerator therefore we calculate as follow,

$$Q = mc(T_1 - T_2)$$

M = 600 kg

C = 0.67 Btu/(lb)F deg = 0.67 x 4.184 = 2.8 j/g K

T<sub>1</sub> = 25 C

T<sub>2</sub> = 5 C

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$$Q = 600000 \times 2.8 \times (25-5) = 33600000 \text{ jul} / 86400 = 389 \text{ Watt}$$

Internal Load

Motor Fan 16 Watt

Door Opening

Refrigerator Internal Volume 1200 lit.

Number of air change as per ASHREA standard = 70 per day

Heat removed per cubic meter of air 75000 j

$$\text{Air Change load} = 1.2 \times 70 \times 75000 / 86400 = 72.9 \text{ Watt}$$

$$Q_{\text{Total}} = Q_{\text{heat leak}} + Q_{\text{product load}} + Q_{\text{internal load}} + Q_{\text{air change}}$$

$$Q_{\text{Total}} = 163 + 389 + 16 + 73 = 641$$

Considering 20 % of Q total for safety factor

$$Q_{\text{Grand Total}} = 641 + 20\%(128) = \underline{769} \text{ watts}$$

With respect to the above calculation we have to select a compressor of R134a with cooling capacity of approximately 769watt at -15 degree centigrade evaporating

temperature. We should select a compressor to be compatible with Electrolux compressor model S26TY.

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Show Case Model MDM-200 Technical Specification	
Show Case Upright Refrigerator	Type of Product
2000 x 800 x 1100 mm	Overall Dimension
40 mm	Wall Thickness
P.U. Foam R11	Type of Foam
30 - 40 Kg/m	Foam Density
100 ISO, 100 Polyol, 35 R11	Foam Mixing Ratio %
600 lit.	Net Internal Volume
Electrolux Model P12TX	Type of Compressor
458 Watts	Compressor Cooling Capacity
Fin and Tube	Type of Condenser
3 rows	Size of Condenser
Fin and Tube 4 lines	Type of Evaporator
R12	Type of Refrigerant
R12, = 750 Gr.	Refrigerant Charge
30 Gr.	Filter Drier Size
220/50	Power Source
- 15 °C	Designated Inside Evaporator Temperature
5 °C	Designated Inside Ref. Temperature
Standard 32 °C	Designated Operating Condition

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**Refrigeration Load Calculation**  
**Upright Refrigerator Showcase Model MDM-200**

a) Transmission load calculation

Refrigerator Compartment	Dimension Cm.	Area (sq.mt.)	Insulation Thickness	Temp. Difference
Side Walls	2 x (110x80) - [(70x30)/2]	1.55	40mm	27 c
Lower Front panel	40x200	0.8	40mm	27 c
Back Panel	200 x 110	2.2	40mm	27 c
Top Surface	50 x 200	1	40mm	27 c
Bottom Surface	80 x 200	1.6	40mm	37 c
Front Glass	200 x 60	1.2	15mm air	27 c

Insulation Type: Pu Foam with R141b blowing agent.

Thermal Conductivity for Foam = 0.0180 W/ mt. ° C

Thermal Conductivity for Air at - 12 C = 0.0237 W/ mt. ° C

Temperature Difference Refrigerator Compartment:

$$\Delta T = 32 - (+5) = 27 \text{ } ^\circ \text{C}$$

Ambient Temperature = 32 °C

Refrigerator Air Temperature = +5 °C

Calculation :

Heat Leak For Refrigerator Compartment.

$$Q_{TL} = Q_{SW} + Q_{Back\ Panel} + Q_{lower\ panel} + Q_{Bottom} + Q_{top} + Q_{front\ glass}$$

$$Q = U A (T_a - T_r)$$

$$U = \frac{1}{\sum X_i / K_i}$$

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Where :

U = Heat Resistance Coefficient Factor

$K_1$  = Foam Thermal Conductivity

Note : Due to the short thickness of cabinet out side panel ( 0.6 mm ) and plastic inner liner ( 1.5 mm ) heat resistance of these materials have been considered negligible.

Therefore:

$$Q_{\text{SideWalls}} = [ U A ( T_a - T_r ) ]$$

$T_a$  = Ambient Temperature

$T_r$  = refrigerator air Temperature

$$U = 1 / ( 0.040 / 0.0180 ) = 0.45 \text{ W/ sq.m } ^\circ\text{C}$$

$$A = 1.55 \text{ Sq. Mt.,}$$

$$T_a = 32 \text{ } ^\circ\text{C}$$

$$T_r = +5 \text{ } ^\circ\text{C}$$

therefore

$$Q_{\text{SideWalls}} = 0.45 \times 1.55 \times 27 = 19 \text{ Watts}$$

$$Q_{\text{SideWalls}} = 19 \text{ Watts}$$

$$Q_{\text{front glass}} = [ U A ( T_a - T_r ) ]$$

$$U = 1 / ( 0.015 / 0.0237 ) = 1.6 \text{ W/ sq.m } ^\circ\text{C}$$

$$T_a - T_r = 27$$

$$A = 1.2$$

$$Q_{\text{front glass}} = 1.6 \times 1.2 \times 27 = 52 \text{ Watts}$$

$$Q_{\text{front glass}} = 52 \text{ Watts}$$

$$Q_{\text{Back panel}} = [ U A ( T_a - T_r ) ]$$

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$$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C,}$$

$$T_a - T_r = 27$$

$$A = 2.2$$

$$Q_{\text{Back panel}} = 0.45 \times 2.2 \times 27 = 27 \text{ Watts}$$

$$Q_{\text{Back panel}} = 27 \text{ Watts}$$

$$Q_{\text{Top}} = [U A (T_a - T_r)]$$

$$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C,}$$

$$T_a - T_r = 27$$

$$A = 1$$

$$Q_{\text{Top}} = 0.45 \times 1 \times 27 = 12 \text{ Watts}$$

$$Q_{\text{Top}} = 12 \text{ Watts}$$

$$Q_{\text{Bottom}} = [U A (T_a - T_r)]$$

$$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C,}$$

$$T_a - T_r = 37$$

$$A = 1.6$$

$$Q_{\text{Bottom Surface}} = 0.45 \times 1.6 \times 37 = 27 \text{ Watts}$$

$$Q_{\text{Bottom Surface}} = 27 \text{ Watts}$$

$$Q_{\text{lower panel}} = [U A (T_a - T_r)]$$

$$U = 0.45 \text{ w/sq. Mt. } ^\circ\text{C,}$$

$$T_a - T_r = 27$$

$$A = 0.8$$

$$Q_{\text{lower panel}} = 0.45 \times 0.8 \times 27 = 10 \text{ Watts}$$

Total Refrigerator Heat Leak =

$$19+27+12+27+52+10=147 \text{ Watt}$$



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**Product Load**

A product placed in a refrigerator at a temperature higher than the storage temperature will lose heat until it reaches the storage temperature. The quantity of heat to be removed may be calculated from knowledge of the product, including its state upon entering the refrigerator, its final state, its weight, specific heat above and below freezing point, its freezing temperature and latent heat. When a definite weight of product is cooled from one state and temperature to

another state and temperature, some or all of the following calculations must be made:

Heat removal from initial temperature to some lower temperature above freezing.

$$Q = mc(T_1 - T_2)$$

Heat removal from initial temperature to freezing point of product.

$$Q = mc(T_i - T_f)$$

Heat removal to freeze product.

$$Q = mh_{if}$$

Heat removal from freezing point to final temperature below freezing.

$$Q = mc(T_f - T_3)$$

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Where

Q = heat removed, Kj

M = weight of product, kg

C = specific heat of product above freezing point, Kj/Kg. K

T<sub>1</sub> = initial temp. C

T<sub>2</sub> = lower temperature above freezing, C

T<sub>f</sub> = freezing temperature of product, C

H<sub>if</sub> = latent heat of fusion, kj per kg

Since this product is mainly used for storing fresh Lamb meet and beef above freezing point at +5 C, we consider 300 Kg of meet to be stored in this refrigerator therefore we calculate as follow,

$$Q = mc(T_1 - T_2)$$

M = 300 kg

C = 0.67 Btu/(lb)F deg = 0.67 x 4.184 = 2.8 j/g K

T<sub>1</sub> = 25 C

T<sub>2</sub> = 5 C

Q = 300000x2.8x (25-5) = 11200000 jul/86400 = 194 Watt

Internal Load

Florescent Lamp = 20 watt

Door Opening

Refrigerator Internal Volume 600 lit.

Number of air change as per ASHREA standard = 70 per day

Heat removed per cubic meter of air 75000 j

Air Change load = 6x70x75000/86400 = 36 Watt

$$Q_{\text{Total}} = Q_{\text{heat leak}} + Q_{\text{product load}} + Q_{\text{internal load}} + Q_{\text{air change}}$$

$$Q_{\text{Total}} = 147 + 194 + 20 + 36 = 397$$

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Considering 10 % of Q total for safety factor

$$Q_{\text{Grand Total}} = 397 + 10\%(40) = 437 \text{ watts}$$

With respect to the above calculation we have to select a compressor of R134a with cooling capacity of approximately 437 watt at -15 degree centigrade evaporating temperature. The suitable compressor should compatible with compressor Electrolux model P12TX .

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Chest Freezer Model MDCF-125 Technical Specification	
Chest Freezer	Type of Product
1250 x 650 x 860 mm	Overall Dimension
50 mm	Wall Thickness
P.U. Foam R11	Type of Foam
35 - 40 Kg/m	Foam Density
100 ISO, 100 Polyol, 35 R11	Foam Mixing Ratio %
500 lit.	Net Internal Volume
Electrolux model P12FW	Type of Compressor
235 Watts	Compressor Cooling Capacity
Wire on Tube	Type of Condenser
Tube in Body	Type of Evaporator
R12	Type of Refrigerant
R12, = 300 Gr.	Refrigerant Charge
15 Gr.	Filter Drier Size
220/50	Power Source
- 18 °C	Designated Inside Evaporator Temperature
5 °C	Designated Inside Ref. Temperature
Standard 32 °C	Designated Operating Condition

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**Chest Freezer Model MDCF-125****a) Transmission Load Calculation****Dimension**

	Dimension Cm.	Area (sq. mt.)	Insulation Thickness mm
Side Walls	2 x (65x86)	1.12	50
Front & Back Panel	2 x (125x86)	2.14	50
Chest Door	125 x 65	0.81	50
Bottom Floor	125 x 65	0.81	50

Insulation Type: Pu Foam R141b expanded blowing PU foam

R141b Foam Thermal Conductivity: 0.018 W /mt.C

Temperature Difference: ( $\Delta T$ ) = 32 - (-25) = 57 C

Ambient Temperature = 32 C

Freezer Air Temperature = - 25 C

Calculation :

$$Q_{TL} = Q_{side\ Walls} + Q_{Bottom} + Q_{Top}$$

$$Q = U A ( T_a - T_f )$$

$$U = \frac{1}{X_1 / K_1 + X_2 / K_2 + \dots}$$

Where :

U = Heat Resistance Coefficient Factor

K<sub>1</sub> = Foam Thermal ConductivityX<sub>1</sub> = Foam Thickness

Note : Due to the short thickness of cabinet out side panel ( 0.6 mm ) and plastic inner liner ( 1.5 mm ) heat resistance of these materials have been considered negligible. Therefore:

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$$Q_{\text{SideWalls}} = [U A (T_a - T_f)]$$

$T_a$  = Ambient Temperature

$T_f$  = Freezer air Temperature

$$U = 1 / (0.05/0.018) = 0.36 \text{ W/ sq.m C}$$

$$A = 1.12 \text{ Sq. Mt.}$$

$$T_a = 32 \text{ C}$$

$$T_f = -25 \text{ C}$$

$$Q_{\text{SideWalls}} = 0.36 \times 1.12 \times 57 = 23 \text{ Watts}$$

$$Q_{\text{SideWalls}} = 23 \text{ Watts}$$

$$Q_{\text{Front Wall}} = [U A (T_a - T_f)]$$

$T_a$  = Ambient Temperature

$T_f$  = Freezer air Temperature

$$U = 1 / (0.050/0.018) = 0.36 \text{ W/ sq.m C}$$

$$A = 1.07 \text{ Sq. Mt.}$$

$$T_a = 32 \text{ C}$$

$$T_f = -25 \text{ C}$$

$$Q_{\text{Front Wall}} = 0.36 \times 1.07 \times 57 = 22 \text{ Watts}$$

$$Q_{\text{Front Wall}} = 22 \text{ Watts}$$

$$Q_{\text{Back panel}} = [U A (T_a - T_f)]$$

$T_a$  = Ambient Temperature

$T_f$  = Freezer air Temperature

$$U = 1 / (0.050/0.018) = 0.36 \text{ W/ sq.m C}$$

$$A = 1.07 \text{ Sq. Mt.}$$

$$T_a = 42 \text{ C}$$

$$T_f = -25 \text{ C}$$

$$Q_{\text{back panel}} = 0.36 \times 1.07 \times 57 = 22 \text{ Watts}$$

$$Q_{\text{Top}} = [U A (T_a - T_f)]$$

$T_a$  = Ambient Temperature

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$T_f$  = Freezer air Temperature

$$U = 1 / ( 0.050/0.018 ) = 0.36 \text{ W/ sq.m C}$$

$$A = 0.81 \text{ Sq. Mt.}$$

$$T_a = 32 \text{ C}$$

$$T_f = - 25 \text{ C}$$

$$Q_{\text{Top}} = 0.36 \times 0.81 \times 57 = 17 \text{ Watts}$$

$$Q_{\text{Top}} = 17 \text{ Watts}$$

$$Q_{\text{Bottom}} = [ U A ( T_a - T_f ) ]$$

$T_a$  = Ambient Temperature

$T_f$  = Freezer air Temperature

$$U = 1 / ( 0.050/ 0.018 ) = 0.36 \text{ W/ sq.m C}$$

$$A = 0.81 \text{ Sq. Mt.}$$

$$T_a = 42 \text{ C}$$

$$T_f = - 25 \text{ C}$$

$$Q_{\text{Bottom}} = 0.36 \times 0.81 \times 67 = 19 \text{ Watts}$$

Total Heat Leaks;

$$Q_{\text{TL}} = 23 + 26 + 22 + 19 + 17 = 107 \text{ watts}$$

$$Q_{\text{Total Heat Leaks}} = 107 \text{ Watts}$$

$$\text{Ice Making Capacity} = 5_{\text{kg}} \times 1 \times (15 - 0) \times 1.163 = 87 \text{ Watts}$$

c) Heat gain through infiltration;

We consider 10% safety factor for door opening and infiltration

$$\text{Heat gain by infiltration} = 0.1 \times ( \text{total heat leaks} )$$

$$\text{Heat gain by infiltration} = 0.1 \times ( 87 ) = 9 \text{ Watts}$$

Total Cooling Capacity Required is calculated as follows;

$$Q_{\text{Grand Total}} = Q_{\text{Heat Leaks}} + Q_{\text{Ice Making}} + Q_{\text{Infiltration}}$$

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$$Q_{\text{Grand Total}} = 107 + 87 + 9 = 203 \text{ Watts}$$

$$Q_{\text{Grand Total}} = 203 \text{ Watts}$$

The suitable R134a compressor should be compatible with cooling capacity of 203 watt. A compressor compatible with Electrolux model P12Fw should be selected.



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### Model MDWC-100

$$Q_1 = m C \Delta T, \text{ Where:}$$

$Q_1$  Total heat removed from total drinking water tank volume capacity (lit.) during specific period, related to compressor cooling capacity power in Watts, at initial compressor start up, and early in the morning. When the water temperature is 24 C.

$m$  total weight of original water in the water cooler storage tank in Kg. Considering that one litter of water at 24 C is equal to approximately one Kg.

$$M = 100 \text{ liter} = 100 \text{ Kg.}$$

$C$  Specific heat factor of water in Kcal/Kg °C = 1

$\Delta T$  Temperature difference ( $T_i - T_c$ ), where,  $T_i$  is inlet water temperature, and  $T_c$  is final cooled water.

$$T_i = 24 \text{ }^\circ\text{C} \text{ and } T_c = 10 \text{ }^\circ\text{C}$$

$$T_i - T_c = 24 - 10 = 14 \text{ }^\circ\text{C}$$

$$Q_1 = m C \Delta T = 100 \times 1 \times 14 = 1400 \text{ Kcal} = 1400 \times 1.163 = 1628 \text{ Watts/24 hrs}$$

$$Q_1 = 1628 / 24 \text{ water cooler operating time per day} = 69 \text{ Watts}$$

$$Q_1 = 69 \text{ Watts}$$

$$Q_2 = \dot{M} C \Delta T$$

$Q_2$  Total heat removed from total drinking water flow (lit.) during specific period, 16 hours. In Kcal.

$\dot{M}$  total weight of water flow during 16 hours. in Kg. =  $H \times N \times M$  where:

$H$  = Total Water Cooler Usage Time (Hours) = 16

$N$  = Number of Glass of Drinking Water per Hour = 30

$M$  = Kg weight of water in one Glass of Water = 0.2 Kg

$$\dot{M} = 16 \times 30 \times 0.2 = 96 \text{ lit.} + 20\% \text{ Waste Water} = 96$$

$C$  Specific heat factor of water in Kcal/Kg °C = 1

$\Delta T$  Temperature d( $T_i - T_c$ ), where,  $T_i$  is inlet water temperature, and  $T_c$  is final cooled water temperature.

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Ti = 24 °C and T = 10 °C and Ti - Tc = 24-10 = 14 °C

Q2 = m C ΔT = 96 x 1 x 14 = 1344 Kcal = 1344 x 1.163 = 1563 Watts/16 hrs

Q2 = 1563/12.8 compressor operating time per day = 122 Watts

**Q2 = 122 Watts**

Q3 = UA ΔT, Where:

Q3 Total Leak, gained through side wall of drinking water storage tank by conduction in Kcal.

U Heat Resistance Coefficient Factor in Kcal/Sq. mt. C

U = 1 / (0.05 / 0.018) = 0.36 Watt / m² . °C

A Total Area which heat is transmitted by. In Sq. Mt.

A = {(30 x 3.14 x 50) + [(2 x 30 x 30 x 3.13) / 4]} = 0.6123 Sq. Mt.

ΔT Temperature difference (Ta - Tc), where, T is ambient temperature, and Tc is final cooled water temperature.

Ta = 30 °C and Tc = 10 °C

Ta - Tc = 30-10 = 20 °C

Q3 = UA ΔT = 0.36 x 0.6123 x 20 = 4.4 Watts

**Q3 = 4.4 Watts**

**Qt = Q1 + Q2 + Q3 = 69 + 122 + 4.4 = 195 Watts**

Suitable compressor to be selected should have at least 195 watt cooling-capacity and must be compatible with compressor model Electrolux L76AV.