



TOGETHER
for a sustainable future

OCCASION

This publication has been made available to the public on the occasion of the 50th anniversary of the United Nations Industrial Development Organisation.



TOGETHER
for a sustainable future

DISCLAIMER

This document has been produced without formal United Nations editing. The designations employed and the presentation of the material in this document do not imply the expression of any opinion whatsoever on the part of the Secretariat of the United Nations Industrial Development Organization (UNIDO) concerning the legal status of any country, territory, city or area or of its authorities, or concerning the delimitation of its frontiers or boundaries, or its economic system or degree of development. Designations such as “developed”, “industrialized” and “developing” are intended for statistical convenience and do not necessarily express a judgment about the stage reached by a particular country or area in the development process. Mention of firm names or commercial products does not constitute an endorsement by UNIDO.

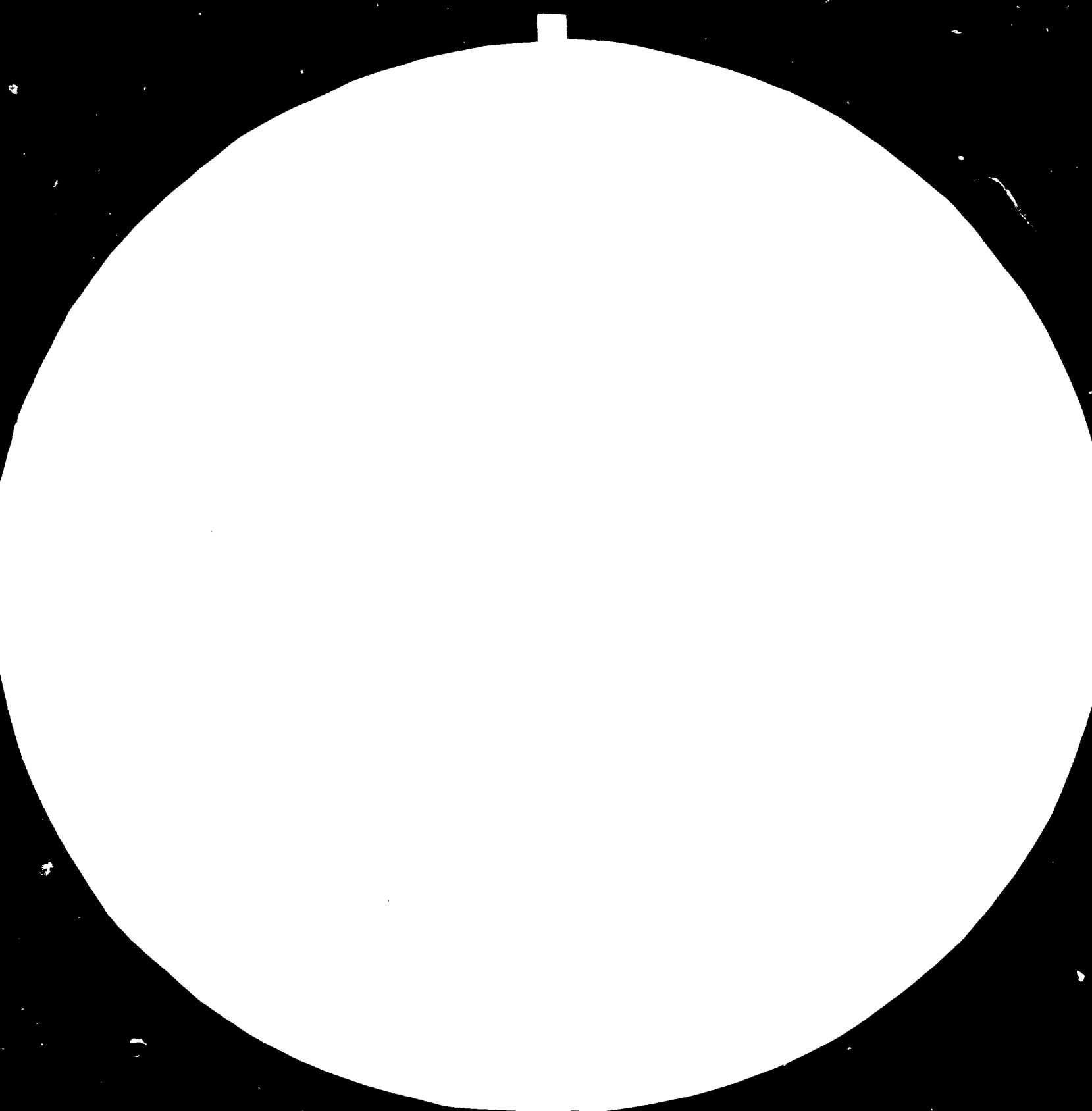
FAIR USE POLICY

Any part of this publication may be quoted and referenced for educational and research purposes without additional permission from UNIDO. However, those who make use of quoting and referencing this publication are requested to follow the Fair Use Policy of giving due credit to UNIDO.

CONTACT

Please contact publications@unido.org for further information concerning UNIDO publications.

For more information about UNIDO, please visit us at www.unido.org





32

36

4



MICROCOPY RESOLUTION TEST CHART

NATIONAL BUREAU OF STANDARDS

STANDARD REFERENCE MATERIAL 1010a

—ANNEX D—100 TEST CHART NBS 1010a

August 1984
English

14097-E

Niger.

EVALUATION

OF THE PRELIMINARY STUDY
OF THE IRON ORE DEPOSITS
AT SAY REPUBLIC OF NIGER

prepared by

RUD HUMBOLDT WEDAG AG

UNIDO PROJECT DP/IAF/79/067

Elaborated by Viktor Sosic

Technical Adviser for Processing of Iron Ore

U N I D O

2946

VIENNA

The views and opinions expressed in this paper are those of the author and do not necessarily reflect the views of the Secretariat of UNIDO.

Received from
Mr. T. Watanabe D-1239

IRON ORE DEPOSITS DOGUEL KAINA AND KOLO.

1. Ore reserves.

The iron ore deposits Doguel kaina and Kolo, close to SAY, are located 30 to 40 km south-east of NIAMEY, Niger.

Oolothic ore occurs in three horizons:

- Upper horizon with iron oolithes "indurées"
Fe-content average 46...51 %
Thickness average 2,20...2,53 m

- Intercalation with ooloth bearing sands and clays
Fe-content average 24...33 %
Thickness average 1,1 m

- Bottom horizon with iron oolithes "tendres"
Fe-content average 43...46 %
Thickness average 2,0...2,9 m

The average overall thickness of the ore horizons amounts to 6,56 m.

1.1 Doguel Kaina.

The total ore reserves in the Doguel kaina area amounts to 1.009 Mt
Average Fe-content 45,73 %

Assuming a cut-off of 35%Fe for Intercalation horizon, the total ore reserves amount to 937 Mt
with an average Fe-content 47,44 %

1.2 Kolo iron ore deposit.

The total ore reserves amount to 207 Mt
with an average Fe-content 40,84 %

Assuming a cut-off of 35% Fe, the total ore reserves amount to	173 Mt
with an average Fe-content	44,67 %

1.3 Advantages of the iron ore deposits Doguel kaina and Kolo.

- Large ore reserves.
- Iron mineral is goethite which is easy reducible.
- Open pit mining.

1.4 Disadvantages of Doguel kaina and Kolo ore deposits.

- Relative high ratio overburden/ore.
- High silicious ore, practically without CaO and MgO.
- Due to impurities in the oolithes, this type of ore is possible to concentrate only up to 54 \pm 1 %Fe.
- Low concentration of iron ore per m², i.e. only about 17 t/m² and therefore it is always necessary a long internal transport from open pit to beneficiation plant which requires high transport cost.

Remote location, i.e. about 900 km from the sea port which excludes any export possibilities.

1.5 By means of an appropriate, simple and cheap beneficiation method concentrated oolothic ore, could be a very cheap raw material for a domestic steel industry.

2. Project Work Plan - PWP.

The detailed PWP has included all necessary works and tests:

- To identify the quality and quantity of the iron ore reserves.
- To asses techno-economically the beneficiation characteristics of the ore, including iron recovery and quality of concentrates.
- To assess techno-economically the pelletization characteri-

stics of the concentrates and direct reduction characteristics of the pellets.

I have to emphasise that the Contractor - HUMBOLDT WEDAG - has carried out this PWP very carefully and exemplary. All above mentioned problems have been successfully solved and optimal possible results have been obtained.

2.1 Beneficiation tests.

Crushing, grinding and beneficiation tests have surely proved the following:

- Recoverable Fe is concentrated only in oolithes.
- The emphasis has been put on maximum possible concentration of the iron mineral and 50 pure oolithes from each sample have been manually separated after attrition.
The chemical analyses of the individual oolithes of
 - sample 1 yielded an Fe-content of 54,21 % and
 - sample 2 yielded an Fe-content of 53,40 %
- Quartz grains are mainly smaller than 0,63mm - see B.4.1 !
- Due to very fine impurity inclusions in the structure of oolithes, the fine grinding of oolithes and HIWMS is not giving a higher concentrate quality in comparison with quality of concentrate /-3 + 0,5/mm, i.e. optimal beneficiation results could be obtained only by liberation of oolithes.
- Screen analyses of the crushed oolithic ore are no doubt an approval for the above mentioned statements.

The most characteristic are screen analyses for sample 2, i.e. oolithes tendre - see Annex C-4 and C-6:

Fraction	%W	%Fe	%R	%SiO ₂	%R
+ 5 mm	23,4	41,9	22,9	18,6	24,6
-5 + 3 mm	3,6	42,6	3,5	18,0	3,7
-3 + 2 mm	10,1	<u>50,1</u>	11,8	8,7	5,0
-2 + 1 mm	31,2	<u>50,1</u>	36,6	7,9	14,2
-1 + 0,5 mm	17,5	43,6	17,9	17,2	17,4
-0,5 mm	14,2	21,6	7,2	<u>43,1</u> !!	36,1
Feed	100	42,7	100	17,4	100

Grinding results of sample 2 are a proof that beneficiation of oolitic ore - regardless of feed Fe-content - could be successful only by liberation of oolithes, i.e. by grinding on 100% -3mm, resp. according to screen analyses on -2,5mm, including the attrition/abrading of the matrix on the surface of each oolithe.

The above mentioned statement is valid also for oolitic intercalation horizon, with an Fe-content below cut-off limit of 35 %Fe.

Phosphorus problem.

All attempts to separate or to decrease P-content have failed and therefore in the steel plant a dephosphorization of the pig iron should be provided.

2.2 Crushing-grinding-attrition.

For desintegration of the oolitic ore contractor has used

- hammer crusher,
- hammer mill and
- attrition.

Regardless on the type of ore - indurée or tendre - by this equipment is possible to beneficiate the oolitic ore /-3+0,5/mm practically to the limit, i.e. 53...54%Fe, what is a good result taking into account that a pure goethite - without impurities in the oolithes - has theoretically a content of 62,8 %Fe.

These results have been obtained only by separation of the soft matrix between oolitic grains by crushing/grinding and by abrading of the matrix residue from the oolithe surface during attrition process and by washing the adhering clay particles.

I have no comments concerning above mentioned equipment during beneficiation tests.

Meanwhile taking into account that hammer mill crushing gives considerable quantity of crushed oolithes and that attrition of oolithes is a very important process phase, I recommend for fine grinding - instead of a hammer mill - an autogenous mill with peripheral discharge, as it is KRUPP PERIMILL.

An autogenous PERIMILL closed circuit grinding has many advantages:

- Extremely sharp control of size grinding which should be according to screen analyses decreased on 2,5mm.
- During grinding, the attrition of liberated oolithes is continuously present.
- Dry attrition of oolithe grains is optimal.
- Attrition time is prolonged by recycling of the oversize fraction $\pm 2,5\text{mm}$ to the mill, i.e. closed circuit grinding.
- Wet attrition by a special attrition cell could be shortened to minimum.
- In the material $-2,5\text{mm}$ there will be practically no broken oolithes.
- A PERIMILL will ensure the same liberation conditions for oolithes indurées, oolithes tendres and intercalation, regardless of Fe-content, i.e. cut-off 35 %Fe, taking into account that intercalation consists of iron oolithes bigger than 0,50mm in clayey-sandy matrix.
- No selective mining will be necessary!!

2.3 Desliming.

Contractor has deslimed fraction -0,50mm for HIWMS purposes on $\pm 0,020$ mm.

Meanwhile screen analyses of the fraction -0,50mm have showed that desliming on $\pm 0,10$ mm^{x)} will give practically the same or even better technological results: See Annex C-13!

<u>Fraction</u>	<u>%W</u>	<u>%Fe</u>	<u>%R</u>	<u>%SiO₂</u>	<u>%R</u>
-0,50 \pm 0,30 mm	11,2	34,1	9,2	27,9	17,1
-0,30 \pm 0,10 mm	11,0	22,2	5,9	41,1	25,1
-0,10 \pm 0,063 mm	2,4	<u>16,5</u>	1,0	<u>45,7</u> !!	6,1
-0,063 mm	2,3	<u>18,1</u>	1,0	<u>34,9</u> !!	4,5

These results are based on a material which was crushed by force by a hammer mill, i.e. the crushing which gives a considerable quantity of crushed oolites in the fraction -0,50mm.

Meanwhile PERIMILL will give practically no broken oolites!!
x) or even 0,150 mm!!

2.4 Attrition.

Attrition is a very important process phase. By attrition

- clayay matrix between oolites should be separated and
- clayay oolithe surface shells should be abraded, taking into account that each oolithe has a barren shell of some tenth microns thickness which seems to be of the same hardness as oolites themselves.
- Attrition of the soft clayay matrix represents no problem, meanwhile attrition of the oolithe shells demands more time and optimal attrition conditions, the conditions which occur only during autogenous grinding.

Conditions of attrition of the fraction -3mm were probably not optimal, concerning the pulp density:

	g/dm^3	dm^3 solid	dm^3 water	Ratio s/w
Sample 1	1100	0,415	0,585	65/35
Sample 2	1500	0,490	0,510	72/28

Taking into account relatively low spec. density of the oolithes - with a bulk density of 1,92 - attrition conditions were acceptable for sample 2, but not for sample 1.

Attrition is namely successful when ratio s/w is about 70/30 to 75/25, depending upon the volume concentration.

2.5 HIWMS.

The only successful process for the beneficiation of deslimed fraction -0,50mm is HI Wet Magnetic Separation.

Oolitic ore crushed by a hammer mill has always a higher percentage of broken oolithes in the fraction -0,5mm. But oolitic ore milled by a PERIMILL contains practically no broken oolithes.

The fraction -0,10mm is practically pure matrix material, i.e. clayey material which should be deslimed without any deterioration of Fe recovery.

In this case HIWMS will operate under much better conditions!

Dewatering of of any concentrate +0,10mm represents no problem.

Fraction for HIWMS.

All beneficiation tests have been elaborated on the basis of two main fractions:

/-3 + 0,5/mm and fraction -0,50mm.

Taking into account data - se page B 16 1 - that quartz grains are mainly in the fraction -0,63mm, I recommend the following fractions:

- fraction $-2,5 + 0,6$ /mm and
- fraction $-0,60$ mm, the fraction which should be deslimed on $\pm 0,10$ mm.

Material $-0,5 + 0,1$ /mm is still a very convenient one for HUMBOLDT JONES HIWMS process.

3. Conception for the exploitation of the iron ore deposits.

All critical remarks about C.6.1 - Treatability of the differend ore horizons - are correct taking into account the proposed beneficiation scheme, i.e. crushing by a hammer mill.

By an autogenous mill with peripheral discharge, desintegration of oolites will be optimal,

- practically without broken oolites in the fraction $+0,6$ mm,
- without broken oolithe particles in the fraction $-0,60$ mm
- and with an attrition under optimal conditions.

Evenmore, by introducing a PERIMILL close circuit grinding, the beneficiation conditions of all iron ore horizons, including intercalation, will be equaled, regardless of the Fe-content.

No selective exploitation will be necessary and all three iron ore horizons could be exploited at once.

The quantity of the fraction $-0,60$ mm will be strongly increased:

- partly due to the decreasing of upper size from 3 to 2,5mm,
- partly due to the screen size increasing from 0,5 to 0,6mm and
- mainly due to a strong attrition action during the autogenous milling in closed circuit by a PERIMILL.

By first desliming on $\pm 0,10$ mm, attrition conditions will be strongly improved.

According to these scheme improvements the following concentrate could be produced:

Fe concentrate	with 53...55 %Fe,	in ignited state	62±1 %Fe
with approx.	2 % P_2O_5	"	2,3 % P_2O_5
with approx.	less than 4 % SiO_2	"	4,5 % SiO_2

Such a concentrate could be a very good raw material for local consumption - Niger and north Nigeria -but due to low basicity and mine remote location, any export possibilities are excluded, taking into account that river Niger is not navigable between Niamey and the river mouth.

4. Pelletizing and Direct Reduction process.

I have no remarks on the pelletizing tests.

Contractor has proved that high quality acid pellets could be produced.

Pellets with a basicity 0,8 could not be produced.

Meanwhile the problem of pelletizing should be treated in connection with the chosen reduction process.

Among the many DR processes, contractor has chosen and recommended KR process, the process which has many advantages, although until now - August 1984 - no industrial KR plant has been put in operation.

But for the chosen KR process pelletizing is not at all necessary. KORF Engineering claimed that by KR process the following iron ores could be used:

- pellets,
- natural pellets -25mm and
- sinter !!

In our case the concentrate /-2,5 +0,1/mm represents an excellent sinter material and even self-fluxing sinter is not excluded.

Therefore there is no need for the following proposed expensive phases:

- fine grinding of Fe concentrate and
- pelletizing of such a ground Fe concentrate.

The proposed metallurgical KR process - which produces pig iron - enables use of Fe concentrates with over 0,20 %P, taking into account that a dephosphorization process should be provided in the steel plant.

5. Conclusions and proposed scheme.

5.1 Exploitation of iron ore deposits.

Oolitic iron ore will be exploited by ripping. A CAT D8H with one-teeth hydraulic ripper will be probably sufficient strong, since oolitic ore is strongly bedded.

Ore produced by ripping has practically no boulders!

5.2 Crushing.

Ore should be crushed by a primary single-toggle crusher 1000 x 800mm.

Recommended discharge setting 250mm.

Crushed ore will be stocked on a small open pile.

5.3 Grinding.

Crushed ore -250mm is a feed for an autogenous KRUPP PERIMILL, with peripheral openings 5mm, probably without grinding balls.

The mill will work in closed circuit with a screen $\pm 2,50$ mm.

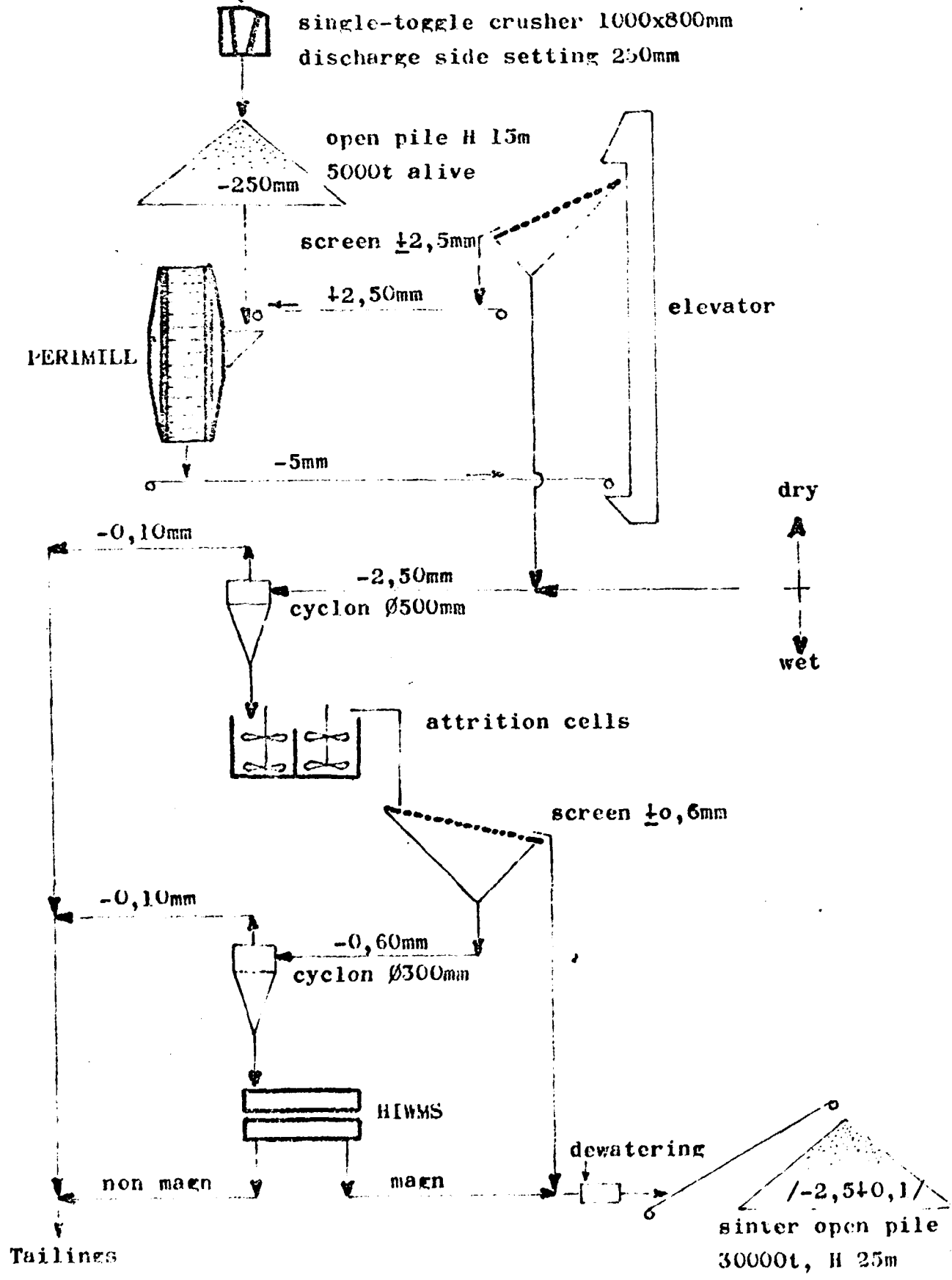
Oversize $\pm 2,5$ mm will return to the mill.

5.4 Desliming.

Undersize material -2,50mm should be deslimed in front of attrition by cyclons: \emptyset about 500mm, pressure about 0,5 bar.

IRON ORE DEPOSITS S A Y - N I G E R

BENEFICIATION SCHEME



41a

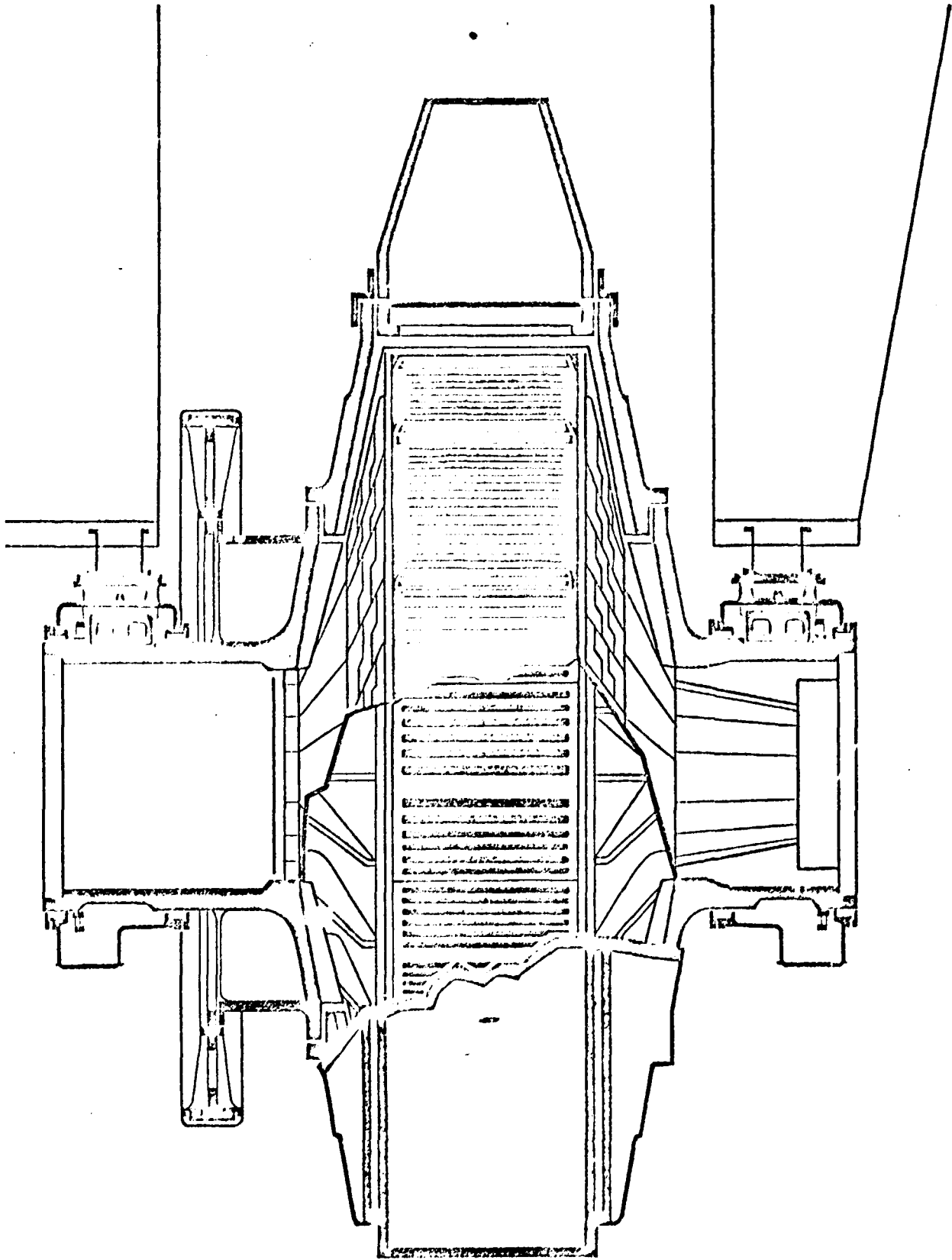


FIG. 1

2 1 0 9 8 7 6 5 4 3 2 1

FIG. 2

5.5 Attrition of material $-2,5 \pm 0,1$ /mm.

Attrition time by an attrition double blade cell will be maximum about 5 min.

5.6 Screening on $\pm 0,6$ mm.

Oversize $\pm 0,60$ mm will be dewatered.

Undersize $-0,6 \pm 0,1$ /mm is feed for HIWMS.

5.7 Desliming of fraction $-0,60$ mm.

Fraction -060 mm should be deslimed in front of HIWMS.

5.8 HIWMS.

Fraction $-0,60$ mm will be separated by HIWMS and concentrate will be dewatered together with the concentrate $\pm 0,60$ mm.

5.9 Sintering.

Limestone or dolomitised limestone will be added to the Fe concentrate and a self-fluxing sinter will be obtained.

5.10 KR process.

KR process produces a pig iron with phosphorus.

A dephosphorization process - LDAC - in the steel plant will produce Thomas slag - a fertilizer - for local consumption.

5.11 Slag.

Due to high Al_2O_3 content in Fe concentrate, a specific slag with high alumina will be produced with the following analyses:

SiO_2	about	34 ± 4 %	Al_2O_3	about	18 ± 2 % !!
CaO	about	38 ± 3 %	MgO	about	6 ± 1 %

Such a slag - with high alumina content - is today produced

only by some iron work plants like:

- Appleby Frodingham, Great Britain,
- Iron Works Skopje, Yugoslavia and
- some Australian iron works.

Appleby Frodingham is selling this slag

- partly as CALUMITE for glass industry and
- partly is grinding this slag and the product is a valuable cement, marketed as CEMSAVE.

By adding 20...30% hydrated lime, this cement is used for the construction of water dams.

6. Remark.

Krupp Industrie and Stahlbau, Rheinhausen, FRG, dispose of a pilot plant with a PERIMILL $\phi 1,9\text{m} \times 0,9\text{m}$, which is working in closed circuit with a screen $\pm 2\text{ mm}$.

Designing of the mill demands in any case a pilot plant grinding test, the test which will prove that a PERIMILL is an ideal device for desintegration of soft oolitic ore,

- without crushing the oolithes and
- that optimal results concerning quality and Fe recovery could be obtained by an autogenous grinding.

Ljubljana, 18th August 1984

Vilijam S. ...



