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## PYRITES, PHOSPHATES AND CHEMICALS LTD INDIA

INVESTIGATIONS TO PRODUCE ELEMENTAL SULHUR FROM AMJHORE PYRITE DEPOSIT

1 SUMMARY

STUDY PHASE II

2	BASIC DATA
3	PROCESS DESIGN
4	PLANT DESIGN
5	OPERATING DATA

ECONOMIC SURVEY

# O OUTOKUMPU ENGINEERING OFK A DIVISION OF OUTOKUMPU OY

### 1. SUMMARY

1.1	Introduction
1.2	Process Selected
1.3	Economic Evaluation
1.4	Conclusions
1.5	Discussion

1.6 Overall Schedule for Plant Supply

1 SUMMARY

1.1 Introduction

The feasibility study reported in this document is the second phase of the work described in the UNIDO Contract No. 82/91 SM.

Additional information has been included based on discussions between PPCL and Outokumpu and on open questions in Final Report of Phase 1 of the subject study.

The purpose of the study is to calculate and present the necessary technical, operational and economical data on a metallurgical plant with utility handling facilities for feasibility evaluation for production of elemental sulphur from Amjhore pyrites.

The techinal design and economical cost estimates are based on a certain process selected by PPCL of the three alternatives which were compared in the Report of Phase I.

The basic data and information for the Phase II study work was collected by Outokumpu engineers before Phase I work during their visit to India in January 1983, and in correspondence from PPCL. The data, in chapter 2, was up-dated in negotiations in Outokumpu office on 22-23th July 1985.

A sample of Amjhore pyrites was analyzed and grinding and flotation tests were made in Finland before the Phase I work of the study.

In this report, Phase II, a specification of offsite facilities prepared by FEDO FACT Engineering India, is attached in Chapter 4. The specification with prices was issued in negotiations in Cutokumpu office on 23th July 1985. Some corrections in the specification were done in the meeting, some checkings and corrections are made by Outokumpu.

With the offsite facilities included, the study now covers the whole plant area.

The annual smelting capacity of the plant is 626 600 t/a (dry basis) pyrite of 39.5 % sulphur. Sulphur production is 228 000 t/a.

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1.2 Process Selected

On the basis of Study Phase I report PPCL has chosen Alternative 1 to be the most suitable alternative. The process is shortly as follows.

The ground pyrite ore and top shale materials are dried and then fed to a flash smelting furnace to be smelted in an atmosphere with excess oxygen.

On the settler part only slag is produced. The slag is tapped and granulated.

Smelting gases are reduced with coal, cooled in waste heat boiler, cleaned in eletrostatic precipitators, catalyzed to convert sulphur compounds of the gas to elemental sulphur (in two stages) and cooled to condensate the sulphur as liquid product. Finally the sulphur is purified from arsenic and prilled to final product.

Separated dusts are mixed with water and thickened. The cake is mixed to granulated slag.



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1.3 Economic evaluation

# 1.3.1 Capital cost

The capital costs are estimated on overall cost basis. Outokumpu's estimate covers the cost of production facilities within the agreed scope and the cost of required off-site facilities are estimated by FEDO.

The price level is according to the first half of the year 1985.

The fixed capital is divided into the indigeneous and foreign portions, as in detail agreed with PPCL. The equipment cost of indigeneous equipment were estimated by FEDO.

The total fixed capital amounts as follows:

TOTAL	Rs 1,576,297,000 (100%)
Off-site facilities (indigeneous)	Rs 107,256,000 (7%)
Indigeneous supplies within Outokumpu's scope	Rs 849,675,000 (54%)
Foreign supplies within Outokumpu's scope	Rs 619,366,000 (39%)

The above fixed investment includes approx. 20 % of duties and taxes:

Custom duty of foreign supplies Rs 249,609,000 Excise duty of indigeneous supplies Rs 44,833,000 Sales tax of indigeneous supplies Rs 17,488,000 Total share of duties and taxes Rs 311,930,000

The working capital amounts to the Rs 79,400,000 covering the necessary inventories and liquid assets.



1.3.2 Financing of the investment

Based on the discussions with PPCL, the initial investment, comprehending fixed capital, interests of the construction period as well as 25% of working capital, will be financed with equity and long term debt.

The share of equity/debt will be 50%/50% and equity will be paid first before the drawing of the loan.

Financing plan of the construction period Rs 1000:

Year	Fixed capital	25% of working capital	interest of debt		Equity nt	Debt
1	102,157			102,157	102,157	-
2	322,710			322,710	322,710	-
3	740,384		22,221	762,605	420,746	341,859
4	364,313		72,858	437,171	-	437,171
5	46,733	19,851	* * *	66,583	-	66,583
Sum	1,576,297	19,851	95,079	1,691,227	845,613	845,613

# 1.3.3 Operating cost

The estimation of operating cost is based on the operating figures received from the process calculations as well as on the experiences on the operation of Outokumpu's Kokkola pyrite smelter. The unit prices of main consumables are evaluated by PPCL.

The summarized estimation results in the following annual operating expenses:

Variable cost:		
- pyrite	Rs/a	218,750,000
- utilities and supplies	**	162,538,000
- fixed cost	**	6,654,000
Total	Rs/a	427,942,000

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1-5

# 1.3.4 Revenues

Elemental sulphur and electric energy will be the products for sale.

Rs 2,573 per ton ex works has been the basic price for sulphur. This price corresponds the present price level for imported sulphur.

With full capacity the sulphur production will be 228,000 tons per annum, which results an annual sales of Rs 586,644,000.

With the nominal capacity there will be an excess power production of 7.5 MWh. With a unit price of Rs 650/MWh the annual power sales will be Rs 36,562,000.

# 1.3.5 Profitability

The Internal Rate of Return of cash flow and  $\epsilon$ quity as well as the pay back period has been used as a character of profitability.

The profitability is calculated for four cases:

Case 1: The plant will operate with the nominal capacity and the costs and revenues are as shown in items 6.1-6.3.

Case 2: As case 1., but the production rate will be 90 %.

Case 3: The revenues are estimated with such a sulphur price that the internal rate of return of cash flow will result in 12%.

Case 4: Calculation of "economic IRR". The investment and operating costs are without duties and taxes. It has been assumed, that the transfer price of pyrite as well as the other operating costs (excluding wages and salaries) contains 5 % of different taxes.

Annual gross margins of the cases, Rs 1000/a:

	Case 1.	Case 2.	Case 3.	Case 4.
Revenues	623,207	560,886	722,936	623,207
./. Operating cost	427,942	394,689	427,942	406,966
Gross margin	195,265	166,197	294,994	216,241

Annual cash flow, internal rate of return and pay back period

The cash flows, presented in appendices 6.1-6.4, give the following results:

	IRR of cash flow		Pay back period
Case 1.	6.5 %	1.1 %	13.3 years
Case 2.	4.7 %	negative	48.5 years
Case 3.	12.0 %	10.8 %	6.4 years
Case 4.	10.5 %	8.8 %	7.2 years

In case 4. the IRR of cash flow of 12 % is resulted with a sulphur price of Rs 3,010.40 per ton.

### Sensitivity analysis

The sensitivity analysis, regarding the most important project variables indicates, that the profitability is very sensitive in respect to the sales price of sulphur as well as to the plant operating cost. The sensitivity analysis is in details shown in section 6.

# 1.4 Conclusions

The results of profitability calculations show, that with the present sulphur price the project is economically not very attractive.

The production process is based on proven technology and it seems to be no technical ways to effect essentially to the investment or operating cost of the plant.

Two very remarkable variables in the cash flow are the sales price of sulphur and the transfer price of pyrite. In case 12 % is an acceptable limit for the IRR of the cash flow, that can be achieved with the present price level, if the ex work price of sulphur will be more than Rs 3,000 per ton or, alternatively, the transfer price of pyrite could be decreased to Rs 210 per ton instead of the present Rs 350 per ton.

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# 1.5 Discussion

In review meeting of Phase I Draft Report between PPCL and Outokumpu on 12 to 16 September 1983 in Espoo, Finland, several questions were raised for discussion.

Most of the questions were answered in Phase I Final Report. To questions that were left open comments and answers are given below.

# 1.5.1 Arsenic Removal

As stated in the final report of Phase I, considerable cost savings can be made if the washing need not be done.

When preparing the Phase II Draft Report, Outokumpu representatives had no information of Indian standards and regulations for allowable arsenic content of sulphur. Thus washing and waste handling equipment are included in the extent.

If, however, the washing in autoclaves is not needed, there will be some savings in capital costs.

Additional cost savings would, of course, be reached in utility and maintenance costs.

### 1.5.2 Slag Removal

Slag tapped from the flash smelter furnace is in this Phase II proposed to be granulated, as in Phase I.

This system is selected because the investement costs are relatively low, and the granulated product is easy to handle i.e. no big vehicles and ladles are needed.

# 1.5.3 Parallel Equipment

Replacing of parallel units with fewer bigger units would save investment cost. However, following respects are to be concerned.

### Multicoil Dryers

When using only one multicoil unit instead of two the equipment size would be so high that there would be a risk in the reliability of the dryer.

In addition, in two unit case, half of the drying capacity can be operated in case of some failure in one unit and thus increase the annual production.

### Electrostatic Precipitators

In case of only one precipitator gas flow into the unit would be appr. 214 000 Nm<sup>3</sup>/h. This flow is rather high to be handled by one precipitator unit due to certain standardization of precipitators.

In addition, in case of two units, reduced production can be continued even if one unit is out of order or being maintained or repaired.

### Cold Catalyzers

All three catalyzers - hot and cold catalyzers- are proposed to be same size. It is estimated that supplying three similar units would not be more expensive than one smaller (hot catalyzer) and one bigger cold catalyzer due to equipment design and manufacturing costs.

Maintenance and operation will also be easier with three similar units.

### Sulphur Condensing Towers

With two parallel condensing towers better pressure control in cold catalyzers - and that way operation control - can be reached.

In addition, start-up from cold stage is easier when having one unit heated first with reduced gas flow and partial sulphur production started with this unit.

#### Liquid Sulphur Cooling Boilers

Necessity of the boilers was discussed between PPCL and Outokumpu in meeting on 12 th to 16 th September, 1983 in Espoo. Outokumpu have reduced the number of boilers from four to three. Still fewer unit system is not reasonable due to the structure of the boilers.

#### Process Air Fans, Process Gas Fans

Process air and process gas fans are recommended to be parallel units, capacity of one being some more than half of the total process flow.

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In case of failure in one fan, reduced production of be continued with the other unit.

With smaller units it is also easier to find cheape equipment in standard models.

## Slag Granulation Equipment

Two unit system is recommended for operational reasons. Four tapping holes and launders are proposed, two per each granulation basin. For operation it is reasonable to have several tapping holes assembled; if there are difficulties with one hole, another can be used. Even if some disturbances occur in granulation equipment or rake classifier the other system can be used and sulphur production continued. Normally only one granulation system is coperation.

## Pumps

Pumps are proposed to be two or three parallel for flexibility and safety in operation.

1.5.4
Grain Size of the Feed Material

## Concentrates

Standard recommendation for sizing of flash smelter concentrates is 100 % minus 16 mesh (1000 microns) and 50-90 % minus 200 mesh (74 microns). Most typica sizing used is 100 % minus 65 mesh (210 microns) and 60-90 % minus 200 mesh.

Coarser ground pyrite 100 % minus 50 mesh (297 microns), 70 % plus 70 mesh (210 microns) and 18 % minus 200 mesh has been tested twice at the pilot plant of Outokumpu in Pori with negative results. Part of the material remained unsmelted, specially the gangue material. The matte and slag did not separate and were nearly impossible to tap. On the bottom of the furnace build-ups were formed causing difficulties in the operation.

## Silica (Top Shale)

Standard recommendation for silica flux for flash smelters is based on normally used natural sand:

100		
100 %	- 4 mesh	(4760 microns)
90 %	- 16 mesh	
80 %		(1000 microns)
50 E	- 28 mesh	(595 microns)



There are references for somewhat coarser flux, e.g. in Outokumpu Harjavalta copper smelter sizing of sand used successfully is:

96 % - 3 mesh (6730 microns) 50 % - 28 mesh (595 microns) 3 % - 150 mesh (105 microns)

Many smelters are using crushed silica with typical sizing of 100 % minus 9-16 mesh (1-2 mm).

Sizing of silica is not as critical as for concentrates. Flux is monthly inert material in the reaction shaft. Slag reactions take place mainly in the settler.

# 1.5.5 Stack Emission of Sulphur Compounds

Using incinerator furnace and gas scrubbing with water and lime stone slurry  $\rm H_2O$  and  $\rm SC_2$ -content of the exhaust gas can be reduced to values none and 0.05 %, respectively.

## 1.5.6 Sulpnur Prilling

In Vienna meeting on 29th November 1984 between PPCL, UNIDO and Outokumpu, PPCL's representatives expressed their desire to prill the sulphur instead of casting. Prilling was even earlier recommended by Outokumpu.

# 1.5.7 Starting of Oxygen Plant 9 MW Motor

In negotiations on May 16th '85 in Outokumpu office a questions was raised of conditions to start the big motor of oxygen plant. As other possibility a steam turbine was proposed.

The electric motor can be started by supplying an additional starting reactor (which is included in equipment) and in the following conditions:

- short circuit capacity of the 110 kV feeder point is minimum 1500 MVA (not known to Outokumpu)
- power plant generator is running on some load
- allowed voltage drop in 11 kV switchgear is at least 9 %.

The disadvantages of using turbine motor refer mainly to possible shortages in steam supply. Oxygen plants technology prefers long operation periods, even with small loads and during short steam shortages. By using an electric motor the operation can be kept on with power from the electric network.

# 1.5.8 Oxygen enrichment

The smelting process is designed to use oxygen enriched process air. Total oxygen percentage is 35 %.

Reason for use of oxygen enrichmet is mainly the smleter gas flow rate. In case of 35 % enrichment the gas flow from smelting is 80 000 m<sup>3</sup>/h and in pure air smelting with the same pyrite feed about 250 000 m<sup>3</sup>/h. Smelting air flows are 81 000 and 240 000 m<sup>3</sup>/h, respectively. Auxiliary fuel oil is needed about 11 t/h in pure air case. Sulphur losses in exhaust gas increase with bigger gas flow.

Gas and air flow rates are in pure air case so enourmous that two parallel smelting and sulphur separation lines should be supplied.

Operation control of smelting is easier in the oxygen enrichment case, especially smelting temperature control, because only smelting air oxygen percentage is to be controlled and no auxiliary oil burner control is needed.

In copper smelting use of oxygen enrichment also decreases formation of build-ups in the flash furnace.

According to Outokumpu's experiences wear of brickwork lining of flash smelting furnace is much lower when using excess oxygen. In Outokumpu's Harjavalta copper smelter the brickwork needs to be repaired only every 4-5 years.

1.5.9

Effluents

The main effluents from the process are as follows

Slag granulate and flue dust

Flash smelter furnace slag is granulated with water and conveyed to a heap.

Smelting flue dust, separated from gas stream in waste heat boiler and electrostatic precipitators, is slurried with water, precipitated in a thickener and the underflow pumped to the scraper conveyor of slag.

From the heap the slag and flue dust waste can be carried off by e.g. front end-loader, used as filling material and covered by soil.

Total amount of slag and flue dust to the heap is about 94 t/h, water amount of which is about 17 t/h.

Main components of the slag are:

Fe 45 % 32 % Al<sub>2</sub>0<sub>3</sub> 6 % 1.6 %

and of the flue dust:

SiO<sub>2</sub> 31 % Fe 22 % AlO<sub>3</sub> 12 % C 10 % S 6 %

Sulphur washing wastes

Effluents from the sulphur autoclave washing water handling are

- filter drum cake
- oveflow water

Filter drum cake formation rate is 370 kg/h of which moisture content is 110 kg/h. Insoluble  $As_2S_3$  is 2 % of solid material, the rest being elemental sulphur and gypsum.

The cake can be carried to a special storage area, built e.g. of concrete.

The overflow water flow rate is 9-10 m<sup>3</sup>/h. Its pH-value is about 3 and As-content 16 mg/l.

If the authorities of India do not allow it to be pumped to drainage, an evaporation pond can be built. The area of the pond should be about 700 m<sup>2</sup>. The bottom should be cf concrete, covered by elemental sulphur.

Dried solid material is every now and then gathered from the bottom of the pond. The pond price is not included in economic evaluation.

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Exhaust gas

The flow rate of exhaust gas out from the stack with the nominal capacity of the plant is 180 000 m $^3/h$  (NTP) and its temperature is 60  $^{\circ}$ C.

Gas analysis is

CO 0.11 % SO 0.05 % H2O 23.6 % CO 17.3 % N2 57.6 %

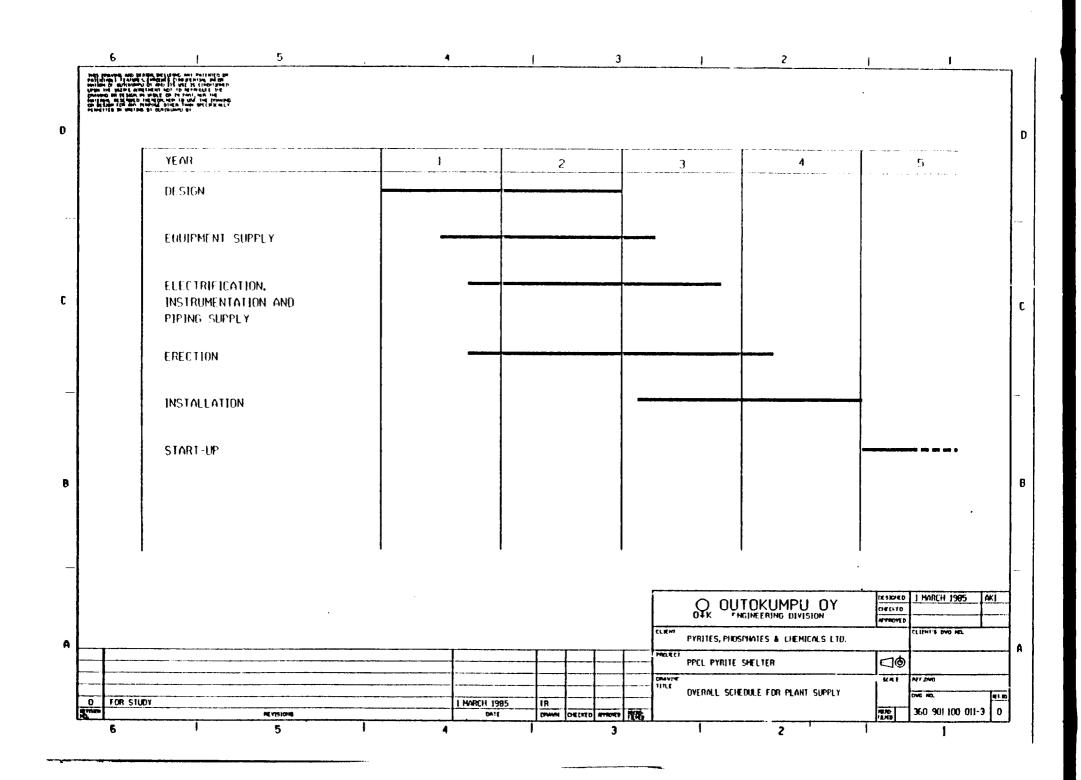
Boiler blow-down steam

Medium flow rate of blow down from the boilers to the blow down tank is about 8 t/h. However, the stream is not constant, it varies according to the need of blow down.

The condensate from the tank (80-90 °C) can be directed to drainage, or it can be used to heating or drying purposes. The use of the water needs however more detailed design.

1.6
Overall Schedule for Plant Supply

Bar Chart Schedule, Dwg No. 360 901 100 011-3 Rev0



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2. BASIC DATA

- Plant Site, Raw Materials, Utilities and Consumables, 2.1 Cost Data
- 2.2 Raw Materials

2.1 Plant site, raw materials, utilities and consumables, transportation, cost data

> See the following attachment: SITE DETAILS OF AMJHORE AREA AND INDIAN COST DATA OF SOME IMPORTANT ITEMS

### SITE DETAILS OF AMJHORE AREA AND INDIAN COST DATA OF SOME IMPORTANT ITEMS

1. LOCATION OF THE : AMJHORE, DISTT. ROHTAS, BIHAR, INDIA

INDUSTRIAL AREA

General Plant Area : Map attached (map/air photograph)

Road and railway net: A metal road exists that leads to the

nearest town and Railway head at Dehrion-Sone, (Eastern Railway) about 35 Kms. away. The Company has its own railway siding facilities at this Railway Station

where 35 wagons can be accommodated.

Electric line

: 440 V-AC, 50 Hz, 3 Ph

net work

Town areas

: Nearest town - Dehri-On-Sone

( 35 Kms. away )

Harbours

: Nearest Harbour : Calcutta

(575 Kms. away)

1.2 Industrial Area

(map, scale approx.

: Map attached

112000)

Ground elevation

: 165 M.S.L.

Road and Railway

: As given at 1.1

connection

supply and water

Connection for water: Tubewell water supply exists and discharge is to the nearest river(about 4 Kms. away)

discharge.

through natural water course.

Connection for electric supply. : The layout of over-head line has been

shown in the map.

Dumping areas

: About 240 hectare around project site.

PLANT CONDITIONS 2.

2.1 Existing services : Transport facilities available. A metal

at the area(if any) road is available at project site.

...2/...

#### 2.2 Steam

Layout of existing system
Diagram of existing system
Connection Points
Steam temperature
Steam pressure

Layout of existing system : Not existing at present.

2.3 Plant air(compressed air) :

Layout of existing system
Connection points
Air pressure
Amount available

Amount available

3 sets of electrical compressors each(2250 cfm, 110 psi) are available and one diesel portable compressor(250 cfm, 100 psi) is available which meet the requirements of mines). There is no surplus capacity.

### MIKE

ER - 8 Atlas Copco(Sweden)
Reciprocating Type Compressors
435 HP each.

2.4 Water(fresh water, cooling water)

Cooling water

Exists for only compressors

Fresh water

Layout of existing system :

Fresh water from tubewell is used. Layout as per map.

Diagram of existing system:

Connection points

Amount available

At present we are getting water from four tubewells, about 2.7 mill. litres per day. This can be further increased to meet the additional requirements.

#### Analysis

a) chloride content in mg/100 gm.

: 0.47

b) sulphate content

: 200 ppm

c) pH

6.5

d) Turbidity : 5 ppm e) Total hardness : 432 : 480 f) Total solid 25°C g) Average water temp.:

: 30°C h) Max. water temp.

### 2.5 Sewage

Locations Capacities : Main open natural drainage channel is connected to Sone River, which is about 4 Kms. away.

## 2.6 Fuel Oil

system

Layout of existing : HSD oil and petrol tank is installed in the project site.

Diagram of existing system

Oil pressure

Connection points

Capacity of storage tanks

: Tank for HSD oil and petrol having 15000 litres capacity each.

#### 2.7 Flectricity

Layout of existing system

: Shown in the map

Diagram of existing system

Voltage, phase and frequency for various efficiency range of motors, lighting and instrumentation.

11 KV transmission lines are existing between the main receiving stations and various sub-stations.

Also existing - 3.3 KV, 3 pH, 50 Hz syncronous induction motors for the compressors.

- plan enclosed.

550 V, 3 ph, 50 Hz squirrel cage/ slipring, induction motors for mining/crusher installations.

440 V, 3 ph, 50 Hz induction motors for surface and workshop installations.

440 V, 3 ph, 50 Hz, 4 wire over-head line for surface lighting.

. . . . . 4/ . . .

#### 2.8 Instrumentation

Information on existing :

system.

Pneumatic equipments other than compressors are not having any

instrumentation.

Pneumatic or electrical:

Sub-station panels and some of the starters are having ammeters and voltmeters only. For domestic consumption single phase energy meters are provided.

2.9 Existing infrastructure at the plant areas.

Road

: Metal road is existing at the project site which connects all the working places.

Railways

: A broad gauge railway facilities exist at about 35 Kms. from the project site at Dehri-on-Sone. There is a proposal to extend the broad gauge railway line from Dehri-on-Sone to project site.

Repairshop

: A good repair & workshop is available. Workshop is provided with Lathe, drilling, grinding, welding machines etc. for the present requirements. However, extra facilities can be provided if required.

Storing house

: A Central store is available in which about Rs.50 lakhs (fifty lakhs) inventory is kept dealing with about 15000 items. Further, house capacity can be provided.

Laboratory

the facilities to analyse Iron, Sulphur, Silica, pH etc. Further facilities can be provided.

Office rooms

: A good office facilities exist having sufficient number of rooms.

3. ENVIRONMENTAL DATA

3.1 Plant elevation from sea level

: 165 M.S.L.

Commence of the second second

...5/...

Soil

Type of soil

: Sandy soil

Soil loading

Natural Design

: 200 kN/m<sup>2</sup> (safe bearing capacity at 2 mtrs.

below the ground level on 600 x 600 mm

plate.

Level of steady soil

Ground water

Water level

: At a depth of about 12 meters from ground level on the eastern side of the project boundary. As we approach towards the hill

the depth of water table increases.

Bed rock

Level

: 12 to 18 meters.

Type of surface

: Lime stone/sand stone.

3.3 Earthquake zone

Probability

: Nil

Intensity in Richter: Not applicable

scale

ATMOSPHERIC DATA

4.1 Monthly air temp.

Average

: 35°C

Max.

: 50°C (during summer)

Min.

: 4°C (during winter)

4.2 Air pressure

Average

: Normal

Max.

: Not available

Min.

4.3 Relative humidity

Average

Max.

: 80% at 40°C during rainy season

(July - August period)

Min.

....6/...

4.4 Rainfall and momentary and daily extremes

Rainfall

: 1691 mm in 1980 1045 mm in 1981

4.5 Wind

Velocity

Average

: 90 Km per hour - maximum

Design

Prevailing direction

: South-West to North-East.

5. TRANSPORT DATA

5.1 Road and railway net

: Main road leading to Debri-On-Some.

5.2 Location of harbours

: Calcutta Port - 575 Km away

5.3 Harbour limitations

: No limitation

5.4 Weight limits

Roads

: No limitation

Railways

: Standard wagendload

4 wheeler - 24 M.T. 6 wheeler - 55 M.T.

5.5 Size limits

Roads

: Maximum width - 5 metre

Railways

DATA FOR PROCESS AND 6. PLANT DESIGN

6.1 Design capacity of the ane Her.

Annual feed of pyrite

: 626,250 M.T.

6.2 Design capacity and design: philosophy of the power plant.

Most of the requirement of complex and complete requirement of smelter will be met through captive power plant.

6.3 Pyrite

Chemical assay Mineralogical analysis Moisture Grain size, screen analysis

: Given separately in the enclosed sheet.

....7/...

sulphur product

6.4 Purity requirement of : Free from arsenic I.S.I. Standard

99.9% 'S'.

: Prilled 6.5 Final form of sulphur

6.6 Storing volumes of raw : Coal - 15 days requirement materials, utilities and products.

Water- One day requirement Full 0il - 10 days requirement.

6.7 Analysis, temperature and availability of water. Sanitary water

> Process water Cooling water

6.8 Analysis and availability: CaCO<sub>3</sub> 80% of lime and limestone Si02 7% - 1.5% R<sub>2</sub>0<sub>3</sub>

6.9 Puels available (fuel oil coal natural gas)

> Type Net heating value Ultimate weight analysis of coal.

6.10 Buildings

: Constructions and materials available.

Pilling Frame of buildings : Not required : Steel frame

the first to the same of the s

Covers and roofing

: Asbestos sheet

6.11 Electrification

Electric power available for the plant

Voltage selection

Feed of main transformer

Distribution voltage

Drive of standard motors

Drive of big motors, over 350 KW

....8/...

Prequency

Failures in electric power feed	:	Month	No. of tripings	Duration of power off
Breaks	:	Oct. '82 Nov. '82 Dec. '82	20 28 10	7 hours 19 hours 2 hours 24 mts.

Fluctuation of : 460 to 380 volts.

voltage

Fluctuation of frequency + %

### 6.12 Instrumentation

Pneumatic or elect- : Pneumatic preferred.
rical system
Voltage and frequency
in control and in feed
of the instrumentation
equipment
Recommendations concerning the manufacturing
of instrumentation

# 6.13 Requirements for environmental protection

Permissible limits of gas emission to the atmosphere.

Sulphur dioxide : 4 Kg./Te. of 100% acid produced

Sulphur trioxide : 0.5 Kg./Te

Carbon monoxide Follow EPA Standards Hydrogen sulphide

7. LOCAL UNIT PRICES FOR CAPITAL COST ESTIMATE

# 7.1 Building and construction work

Unit prices for the following:

52,000

The second state of the second second

- Piling(50 M long, : fs. 23, 000/ per each 660 mm dia)

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	•	Foundation	Rs. 1,350/m
	- concrete mass, ready installed including boarding and steel reinforcements.	Slab Beam Rs. <del>2,250/m</del>	Rs. 1,350/m Rs. 2,800/m Rs. 1,850/m Rs. 2,100/m
	- supporting steel constructions ready installed, painted	Rs. <del>8,000</del> /Te	· 10,000/t
	<ul> <li>walls and roofings of indust- rial buildings</li> </ul>	Rs. 1 <del>00</del> /m <sup>2</sup>	65/m²
	- offices, change rooms	Ps. 1 <del>,200</del> /m <sup>2</sup>	1,500/m2
	- earth excavation	Rs. 15/m <sup>3</sup>	$\frac{11}{m^3}$ $\frac{1}{20}$ $\frac{1}{m^3}$
	- earth filling	Rs. <del>15</del> /m <sup>3</sup>	20/m3
	- rock blasting	Rs. <del>50/</del> m <sup>3</sup>	35/m³
	- asphalt covers	Rs. 100/m <sup>2</sup>	
7.2	Equipment and materials	Materials and manuf.	Transport and erect.
	- Mild steel construction, ready installed	Rs∙	₽s•
	- sheets	20/kg	32/kg
	- profiles	30/kg	3 /2/kg
	- Acid proof steel sheets construction, ready installed	180/kg	3 2/kg
	- Plastics		,
	- pvc		150/kg
	- reinforced plastics	100/kg	50/kg
	- PE	10/kg	V
	- Lead lining, ready installed		
	- sheet lining(3 mm thick)	1100/m <sup>2</sup>	
	- homogenous lining	5000/m <sup>2</sup>	
	- Heat insulation, ready installe inc. covers.		
	- thickness 100 mm	<del>35</del> 0/m <sup>2</sup>	400/m2
	- thickness 200 mm	<del>35</del> 0/m <sup>2</sup> <del>550</del> /m <sup>2</sup>	400/m² 600/m²

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		2	
- Painting (ordinary)	• • •	25/m <sup>2</sup>	
		Rs. $600/m^2$	
- Copper profiles and sheet	5		
Constructions(ready installe	eđ)		
		Materials and manuf.	Transp. and erec. Rs.
- Service platforms, stairs etc.of mild steel	• •	. 15/kg	3 /2/kg
- Tanks, bins etc. of mild steel.	• •	. 20/kg	3 2/kg
- Tanks of acid proof steel	. ••	. 180/kg	n= 11 : ndh
- Tanks of reinforced plast	ics.	. <del>80</del> /kg 1	25/kg 3/1KE
- Gas ducts of mild steel	• •	. 20/kg	V J/KE
Examples of the prices of available equipment, main technical data specified:			
- Pumps			
<ul> <li>type - horizontal, centre</li> <li>fugal.</li> <li>capacity 25 m<sup>3</sup>/hr.</li> </ul>		29,000	_
- pressure 50 MLC	• •	. Rs. 1 <del>8, 310.</del>	<del>00</del> 10%
- material SS 316			
- electric power 10 HB da	rive		
- Belt conveyors			
- type-horizontal, troughthree roll ground converge	eyor	1,000,00	10%
- capacity 200 TPH	•	Rs. <del>345, 00</del>	0.00 Rs. 48,000+00
- width 750 mm			
- length 91.5 M			
- Air and gas fans			
- type-centrifugal blowe	r		1 24
- capacity-10800 NM <sup>3</sup> /hr.	•	Ps.107,000	0.00 10%

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- pressure - 700 mm.wg. - material - casing-MSRL Impeller SS 316 - operating temperature 60°C. - Cranes and hoists Electric hoist - lifting capacity - 2 T. 80,000.00 10% Rs. 40,050,00 - length of bridge - 12 M. Total is. 38 lakhs - Boilers - capacity - 20 TPH - fuel to be used-Fuel oil - pressure - 12 kg./cm<sup>2</sup> - Lorries - type - ordinary 250,000.00 Rs. 200, 000,00 - loading capacity-12 Te. - Fork lift trucks - type - lifting capacity 1,700,000.00 - Front end leaders Rs. 1,011,300.00 - type - Tyre mounted - capacity - 153 m<sup>3</sup> - Electric motors - 75 HP - power - voltage - 415 V fts. 6,000,00 Rs. 60,000.00 - rotating speed-1500 rpm type - synchronous, TEFC squirrel cage

- Ball mills

- diameter - 1.5 M 4, 500, 000.00 150,000.00 - length - 2.4 M Rs. 1,018,000.00 Rs. 100,000.00

- lining material-Rubber

- electric motor- 75 HP

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-	ball	charge	-	り・シ	Te.

-	Drun	fil	ters
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- filter area 67.2 M<sup>2</sup>
- filter cloth-polypropylene
- Rs. 22,50,000.00 (total) - material-Carbon steel

#### Electrification devices 7.3

- Transformers 5....20 MVA: 5 MVA 110kv/11kv, \*\*TRANSFORMER 8.750,000.00 - voltage
- Transformers 500...1500KVA:1000 KVA:11KV/433V, A\*TRANSFORMER B. 1,10,000,00 1,600,000.00
- Cables ( 3 core) 90 - crass section area 120 mm<sup>2</sup> Rs. 76/m
  - insulation PVC (steelwire armoured)
- 200 mm Rs 235/m 100 mm Rs 110/m 500 mm Rs 670/m Rs. 10/kg - Cable racks - Instrumentation Cable Trays Rs.125/m. Material-Al./Anodized Al

#### Piping: cost of materials and 7.4 erection, sizes specified

election, orace absorran	ns.	
- welded steel pipes	15/kg	24/kg 20/kg
- seamless steel pipes	18/kg	20/ leg
- Acid proof steel pipes	1 <del>00</del> /kg	200/49
- Copper pipes	60/k <u>e</u>	, 0
- Plastic pipes	25 <b>-</b> 300/kg	,
- Lead pipes	<del>25</del> /kg	40/kg

20/kg - High pressure pipes

20/kg 25/kg 35/kg - Collars and flanges Carbon-steel

1. The said of the said of

20/kg - T-pieces

- Valves

- Carbon steel, 15-250 NB - Gate (fs. 700-5000) \$5,000

- Globe (Rs. 400-5000) 50,000

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- Pipe bridges and fittings 15 12/kg
- 7.5 Erection and installation work
  - Wages with social cost
    - skilled labour /,800 1000/month helpers /,200 500/month
- 7.6 Taxes and duties of equipment, materials, erection etc.
  - local suppliers & excise duty; 4% S.T.
  - foreign supplies 40% customs duty of CIF prices
  - Engg.commissioning etc. 25%
- 8. LOCAL DATA FOR OPERATING COST ESTIMATE
- 8.1 Unit prices and availability of the following utilities and supplies at the industrial area:

Fresh (potable) water	Cost-Rs.	Unit M <sup>3</sup>
Cooling water	0.50	——— M <sup>3</sup>
Coal	2 <del>00.00</del> 2	50.00 Te
Fuel oil	2 <del>400.00</del> 3,	141.00 Te
Natural gas	-	-
-Electricity	0.65	<del>lewh</del>
Propone (LPG)	<del>3,25</del> 5.	14 kg.
Sulphuric Acid	<del>900.00</del> 1,50	78.00 Te
Lime	600.00	Te
Limestone	20 to 30	Те
HC1 (30% Acid)	330.00	Te
NaOH(Solid-Rayon Grade)	6500.00	Тe
Grinding balls for ball mill	10000.00	Te
Refractory bricks	8.00	brick

- chrome magnesite

- shamotte Not available in India

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Wages and salaries including social 8.2 costs:

343:	Rs.	2 <u>s</u>
Managers	2 <del>, 500</del> /-	3,000/-
Operating Engineers)	<del>2,000/</del> -	2,600/-
Foremen / Skilled labour	1,500/ <b>-</b>	1,800/-
Unskilled labour	1 <del>,000</del> /-	1,200/-

Daily, weekly and annual operating 8.3 time of personnel.

Daily 8 hrs., Weekly 48 hrs. and annual 2400 hrs.

Transportation costs of raw-materials, 8.4 liquids and products:

As. 0.25 to 0.35/ton km. Road freights

Depends on material transported Railway freights and gauge of rail-line.

) Works out to about 2 to ) 3% of F.O.B. cost of Harbour storing costs Harbour stowing costs ) equipment. Harbour duties

DATA FOR ESTIMATION OF REVENUES 9.

> Unit prices of products(ex-works) to be used in profitability calculations:

No valve Iron calcine

appr. 65% - Pe **-** S 0.05% - Cu

Elemental sulphur (solid) 8.1,350/- for fertilizer use and 8.1,500/- for non-fertilizer use.

So\_-bearing process gases for manufacturing of sulphurication.

So2-content appr. 7-9 vol.% o2-content appr. 6-7 vol.%

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#### 10. DATA FOR PROFITABILITY CALCULATIONS 10.1 Tax legislation 6.67 - 10% Straight Line Method Depreciations Area regulations of - A tax holiday of 7 years may be considered for profitability taxation evaluation. Tax free reserve regulapercentages of income tax- 55% + 5% s.c. - 4% purchase tax Other taxes - excise duty 8% 10.2 Capital stock Amount - 50% of total invest. Requirements and limitations of dividends 10.3 Financing terms of investment cost. two Grace period - three years - 11.5% for long term loan and interest 17,5 Pox for short term loan. - 10 years. Pay back period 10.4 Monetary units tobe used and rate of exchange Indian Rupees - 1 US \$ - Rs. 9.5

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# TYPICAL ANALYSIS OF PYRITES

	Percent	
Sulphide Sulphur(S)	38.04	
Sulphate Sulphur(S)	1.41	
Silica (SiO2)	15.28	
Total Iron(Fe)	35.72	
Alumina (Al203)	2.09	
Calcium Oxide (CaO)	Traces	
Magnesium Oxide (MgO)	Traces	
Volatile matter @ 800°C in one hour	31.06	
Arsenic (As)	50 Parts/Million	

\*\*\*\*



2.2 Raw materials

2.2.1 Pyrite ore

> 38.04 % <sup>S</sup>sulphide 1.41 % Ssulphate 8 35.72 % Fe 0.0005 % 0.005 % As 1.0 % С SiO2 15.28 % 2.09 % Al<sub>2</sub>O<sub>3</sub>

80 % - 74 um Grain size Moisture (wet basis) 8 %

2.2.2 Top shale

> 9.2 % Ssulphide 1.6 % Ssulphate 11.2 % Fe 2.6 % С 50.4 % SiO2 A1203 13.2 %

80 % - 74 um Grain size Moisture (wet basis) 8 %

2.2.3 Coal

> 62.5 % Ctot 51.0 %  $c_{fix}$ 20.0 % Volatiles 4.0 % Moisture 25.0 % Ash

23 MJ/kg Net heat of combustion 0-25 mm Grain size

Analysis of ash:

40 % SiO2 10 % Cao 20 % A1203 20 % Fe203



2.	2.	4				
Fu	٦ م		^	i	7	

2.2.4 Fuel oil	Bunker C	C H S N O	85 % 11 % 3.5 % 0.1 % 0.4 %	
	Net heat	of combu	stion	40.5 MJ/kg
2.2.5 Slacked lime	Ca (OH) <sub>2</sub> Balance		90 % 10 %	
2.2.6 Sulphuric acid	H <sub>2</sub> SO4		94 %	
2.2.7 Catalyst mass	A1203 Ca0 Fe Si02		34 % 21 % 7 % 3 %	
2.2.8 Lime stone				
	CaCO3		80 %	

## O OUTOKUMFU ENGINEERING OFK A DIVISION OF OUTOKUMPU OY

3	PROCESS	DESIGN
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3.1	Process Description
3.1.1	
3.1.1.1	Drying of Feed Material
3.1.1.2	Flash Smelting
3.1.1.3	Reduction and Process Gas Handling
3.1.2	Sulphur Plant Area
3.1.2.1	Sulphur Recovery
3.1.2.2	Sulphur Washing
3.1.2.3	Sulphur Prilling
3.1.3	
	Power Plant
3.1.3.2	Coal Plant
3.1.3.3	Oxygen Plant
3.1.3.4	Water Treatment Plant
3.1.3.5	Lime Stone Slurry Preparation Plant
3.1.3.6	Compressed Air Station
3.2	Process Calculations
3.2.1	
	Flash Smelting Area
3.2.2	Sulphur Plant Area
3.3	Process Flow Sheets

Flash Smelter and Sulphur Plant Process Flow Sheet 360 100 901 002-1 Rev 3 Power Plant, Steam Flowsheet 360 100 901 010- 1 Rev 0

PROCESS DESIGN

3.1 Process Description

3.1.1 Flash Smelting Area

3.1.1.1
Drying of Feed Materials

The ground and predried pyrite ore is the starting material of the sulphur production. The grain size of the pyrite is 80 % - 74 um and moisture 8 %.

From the concentrate day bins the pyrite ore and top shale are fed through a screen to drying in steam heated dryers. In the steam dryers wet material is dried by hot steel tubes which are heated from inside by steam at 20 bar.

The moisture content of the dried material is less than 0.2% and the temperature of the exhaust gas is about 100oC. The exhaust gas contains dust, which is separated in the bag filter. The dried material is pneumatically conveyed to the dried charge bin.

### 3.1.1.2 Flash Smelting

The feed material mixture consists of pyrite ore and top shale. The top shale amount is regulated so that all the iron of the pyrite can be slagged. The process air is enriched with technical oxygen. With oxygen enrichment the temperature of the furnace is controlled and with the total oxygen amount the oxidation of sulphur and iron is controlled.

The feed mixture is fed through the roof of the reaction shaft by means of the concentrate burner. Inside the reaction shaft the well distributed pyrite and the top shale particles react with air and oxygen. The retention time for the suspension in the shaft is about 1-2 seconds, in which time the solids are heated up and smelted after many different chemical reactions. As a result of the reactions slag and sulphur containing gas are produced.

In the horizontal settler part slag is separated from gas. The slag is tapped and granulated with water. The produced gas mainly consists of sulphur dioxide, water, carbondioxide and nitrogen.

#### 3.1.1.3 Reduction and Process Gas Handling

After the reaction shaft the gas contains SO2 and therefore reduction of the gas is carried out in th uptake shaft of the flash smelting furnace in order to produce elemental sulphur. The following main reactions take place in reduction:

C + CO2 ---> 2CO

SO2 + 2CO ---> 0.5 S2 + 2CO2

SO2 + 2H2 ---> 0.5 S2 + 2H20

S2 + 2H2 ---> 2H2S

At the same time the oxidic dust components are sul hidized.

In the rear end of the settler part coal dust is burned with oxygen enriched air to raise the temper ture of the smelting gas for the reduction.

The reduction is performed by injecting coal dust (% - 74 um) against the gas flow.

The maximum sulphur production is obtained when the gas after reduction contains a little less SO2 than half of the sum (H2S + H2 + CO + COS).

The reduction is endothermic and the temperature decreases. The temperature after the reduction is 1230 oC.

The reduced process gas together with molten dust i fed into the waste heat boiler, where cooling and solidyfying of dust compounds take place. The boile consists of a radiation chamber and convection section. The gas is cooled to 350oC by the boiler and saturated steam is produced at 70 bar. A minor part of the dust is separated in the boiler and the remaning dust in two electrostatic precipitators workin parallel at a temperature of 360oC.

The dusts from the boiler and electrostatic precipitators are taken out through water seals and fed to thickener.

When the gas is being cooled in the waste heat boiler, many reactions take place between gas components:



2 CO + SG2 ---> 2 CO2 + 1/n Sn

2 CO + S2 ---> 2 COS

2 H2 + SO2 ---> 2H2O + 1/n Sn

2 H2 + S2 ---> 2 H2S

Also sulphur vapour S2 polymerizes to S4, S6 and S8

3.1.2 Sulphur Plant Area

OUTOKUMPU ENGINEERING

### 3.1.2.1 Sulphur Recovery

After the elctrostatic precipitators the cleaned gas is led into the sulphur condensing boiler, where the gas is further cooled down to 150oC and at he same time the elemental sulphur is condensed. The first part of the boiler produces saturated steam at the pressure of 5.5 bar and the second part at the pressure of 1.7 bar.

Part of the condensed sulphur is taken from the bottom of the boiler and the rest is carried over by the gas. These sulphur drops are caught from the gas in the agglomerator and demister.

After the demister the gas is reheated to 430oC in the gas reheater by burning fuel oil with air.

The reheated gas is led into the hot catalyzer where the following main reactions take place:

2 CO + SO2 ---> 1/n Sn + 2 CO2

COS + H2O ---> H2S + CO2

These reactions are exothermic and thus the process gas temperature increases to 480oC. A high alumina cement with Al2O3 as active material is used as catalyst.

The major part of the gas is led after the hot catalyzer into the gas cooling boiler, which produces saturated steam at 5.5 bar. In the boiler, part of the sulphur is condensed. The minor part of the gas is passed by the boiler in order to control the temperature of the gas to 250oC before cold catalyzers.

The main reaction of the cold catalyzers is:



 $SO2 + 2 H2S \longrightarrow 3/n Sn + 2 H20$ 

The reaction is slightly exothermic and increases the temperature of the gas to about 260oC. The same catalyst as in the hot catalyzer is used.

After the cold catalyzers the elemental sulphur is recovered from the gas in sulphur condensing towers. Liquid sulphur is sprayed in the towers, where is meets the process gas counter-currently cooling down the gas to 135oC and condensing sulphur from the gas.

The liquid and condensed sulphur flows from the sulphur condensing towers to the sulphur circulating tank and from there the sulphur is pumped through sulphur cooling boilers back to the sulphur condensing towers. In the suplhur cooling boilers the sulphure temperature drops from 133 °C to 123 °C. The boiler produces saturated steam at he pressure of 1.7 bar.

The recovered sulphur is pumped from the sulphur circulating tank to sulphur washing.

After the condensing towers there is a little sulphur in the gas as drops. These are caught in a demister.

Minor amounts of H<sub>2</sub>O in the gas are converted mainly to SO, by an incinérator, where oil is burned. The gas témperature after the incinerator is 400

Before directing into the stack the gas is still washed with a scrubber-absorption tower system, in scrubber by water and in absorption tower by lime stone slurry. Thus the SO<sub>2</sub>-percentage of the gas is reduced to 0.05 % with no H2S. Temperature of the exhaust gas is 60°.

#### 3.1.2.2 Sulphur Washing

The sulphur produced from the process gas contains arsenic as main impurity. The arsenic is removed from the sulphur in low pressure autoclaves, into which liquid sulphur and lime water suspension are pumped counter-currently. Lime reacts very selectively with arsenic in sulphur forming a water soluble calcium thioarsenate.

The waste liquid from the autoclaves is treated with sulphuric acid in a reactor in order to remove arsenic from the waste liquid. The arsenic precipitate formed is separated in a thickener and in a filter.

#### 3.1.2.3 Sulphur Prilling

The liquid sulphur is fed to a sulphur tank, where the temperature of the sulphur is 125 oC. The sulphur is pumped to prilling nozzles of a prilling tower. The sulphur is sprayed through the nozzles, and air and water are blown to sulphur spray to cool sulphur drops and to slow down falling speed.

From the tower the prilled sulphur is fed to a screen and weighed.

### 3.1.3 Additional Plant Areas

#### 3.1.3.1 Power Plant

Waste heat from flash smelting furnace is recovered by a waste heat boiler which produces saturated high pressure steam of 70 bar.

Main part of the high pressure steam is superheated up to 500 oC in a separate, coal fired superheater. The superheated steam is then used for generation of electric power in a turboalternator. Part of the waste heat boiler steam is reduced to 20 bar and used in the steam dryers.

During shut downs of the smelter the minimum required steam production is ensured by an oil fired auxliary boiler.

The turbine of the turboalternator is of condensing type. The steam flows through the turbine to a condenser, which operates with water cooling. The condensate is returned to the feed water tank.

The steam of 5.5 bar generated in sulphur condensing and gas cooling boilers of the sulphur plant is utilized mainly as heating agent in the feed water tank and in sulphur handling equipment.

The steam of 1.7 bar from sulphur condensing and liquid sulphur cooling boilers is utilized as heating agent for make up water.

The power consumption of the whole area will be about 17.5 MW by full load. The rated power of the turboal-ternator will be 25 MW.

The power generation exceeds the consumption of the plant, and the excess power can be transferred out of the plant area.

3.1.3.2 Coal Plant

> Pulverized coal is used in the flash smelting furnace to increase gas temperature before the uptake shaft and to reduce gases in the uptake. In the superheater boiler coal dust is used for firing.

> Raw coal is charged through a feed funnel to belt conveyors and further to a raw coal bin. From the bin coal is fed to the grinding mill, ground to 70 % minus 200 mesh (0.074 mm) and dried by the warm gas flow, which is mainly preheated air. Pulverized coal is conveyed pneumatically to the dozing bins of flash smelting furnace area and to a storage bin for superheater burner coal. Further to burners it is again transferred pneumatically.

There are two milling units with feed bins in order to ensure continuous feeding of coal dust. Each mill is designed to grind and dry coal successfully at capacity to meet plant requirements.

3.1.3.3 Oxygen Plant Area

> The air separation plant produces oxygen to enrich the flash smelting furnace process air and combustion air and to burn open the furnace tap holes.

> The plant operates according to the low-pressure process with double refrigeration. Drying of the air after cooling as well as simultaneous elimination of the carbon and sulphur dioxides is performed by means of molecular sieves.

The purity of produced oxygen is 95 %.

3.1.3.4 Water Treatment Plant

The water treatment plant and cooling water circulation are included in offsite facilities.

Separate water types needed on the plant area are filtered raw water, demineralized water and semi-soft water.

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#### 3.1.3.5

Lime Stone Slurry Preparation Plant

In the absorption tower the process gas is washed with limestone slurry.

The limestone is ground and screened before mixing with water. The CaCO3 - content of the limestone is 80 %.

#### 3.1.3.6 Compressed Air Station

At the compressed air station pressure air for the needs of the plant is produced in 7 bar abs. pressure.



3.2 Process Calculations

The temperature of the air is supposed to be  $40\,^{\circ}\text{C}$  and its relative humidity  $80\,$  %. The oxygen percentage of the technical oxygen is 95 %.

Note: All gas volumes are at normal state i.e. 1 bar, 0°C.

Boiler pressure figures are absolute values.

3.2.1 Flash Smelting Area

riash smererng med			
Steam Dryer			
Pyrite ore (dry) - moisture (wet basis)		ቲ/h ቄ	83.5 8.0
Top shale (dry) - moisture (wet basis)		t/h %	20.0 8.0
Steam 20 bar, 210°C		t/h	18
Dryer exhaust gas - temperature		m <sup>3</sup> /h	24200 100
Flash Smelting Furnace			
Pyrite Top Shale		t/h t/h	83.5 20.0
Air to reaction shaft Oxygen to reaction shaf - temperature - oxygen enrichment	t	m3/h m3/h °C %	65700 15150 40 35.2
Distribution and leakage air		m <sup>3</sup> /h	2000
Slag		t/h	67.2
Gas after smelting - temperature - analysis	H <sub>2</sub> S CO SO <sub>2</sub> H <sub>2</sub> O CO <sub>2</sub>	3/h CC % % % %	80100 1390 0.2 0.0 0.5 26.7 1.4 4.5 2.7 64.0
	~		

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Coal to settler Combustion air Oxygen - temperature - oxygen enrichment Coal for reduction Injection air Flue dust		t/h m3/h m3/h oC % t/h m3/h t/h	3.2 13700 1800 40 30 17.6 2200
Gas after furnace - temperature - analysis	H <sub>2</sub> s CO COS SO <sub>2</sub> S <sub>2</sub> H <sub>2</sub> O CO <sub>2</sub>	3/h OC 8 8 8 8 8 8	115000 1230 1.2 1.1 5.6 0.2 3.6 7.6 9.3 16.3 55.1
Waste heat boiler			
Flue dust from boiler Steam production - pressure - feed water temperature	e	t/h t/h bar	2.1 111 70 150
Gas after boiler - temperature - analysis	H <sub>2</sub> s CO COS SO <sub>2</sub> S <sub>2</sub> S <sub>8</sub> H <sub>2</sub> O CO <sub>2</sub>	3/h C % % % % % % % % % % % % % % % % % % %	108700 350 0.2 1.7 2.1 1.2 2.2 2.9 10.5 20.2 59.0

# O OUTOKUMPU ENGINEERING O+K A DIVISION OF OUTOKUMPU OY

Electrostatic Precipitators			
Flue dust from precipitators		t/h	8.5
Gas after precipitator -temperature -analysis	H <sub>2</sub> s C0 C0s S0 <sub>2</sub> S <sub>2</sub> ,,s H <sub>2</sub> O C0 <sub>2</sub>	m <sup>3</sup> /h OC % % % % % % % % % % % % % % % % % %	112200 360 0.2 1.5 1.7 1.3 2.3 2.8 12.6 19.7 57.9
3.2.2 Sulphur Plant Area	<i>:</i>		
Sulphur condensing boiler and dem  Sulphur production  Steam production  - pressure  - feed water temperature  Steam production  - pressure  - feed water temperature  Gas after demister	<u>ister</u>	t/h t/h bar oC t/h bar oC  moC	24.1 16.5 5.5 150 7.3 1.7 105
- temperature		°C	150
Gas reheater  Oil Combustion air  Gas after reheater - temperature  Hot catalyzer		t/h m <sup>3</sup> /h m <sup>3</sup> /h o <sub>C</sub>	1.35 15800 126300 426
Gas after catalyzer - temperature - analysis	H <sub>2</sub> S CO COS SO <sub>2</sub> S2,S4,S6 H <sub>2</sub> O CO <sub>2</sub>	m <sup>3</sup> /h OC % % % % % % % % % % % % % % % % % %	125500 480 1.85 0.08 0.10 1.17 0.50 13.0 21.8 61.5

# OTK A DIVISION OF OUTOKUMPU OY

Gas cooling boiler			
Sulphur production Steam production - pressure - feed water temperature		t/h t/h bar °C	1.4 22.7 5.5 150
Gas after boiler - temperature		m <sup>3</sup> /h °C	125100 250
Cold catalyzers			
Gas after catalyzers - temperature - analysis	H <sub>2</sub> S CO COS SO <sub>2</sub> S6,S8 H <sub>2</sub> O CO <sub>2</sub>	m <sup>3</sup> /h o c ዩ ዩ ዩ ዩ ዩ ዩ	124800 259 0.52 0.07 0.08 0.52 0.44 14.4 22.0 62.0
Sulphur condensing towers and dem	nister		
Sulphur production		t/h	4.9
Gas after demister - temperature - analysis	H <sub>2</sub> S CO COS SO <sub>2</sub> S <sub>8</sub> O CO <sub>2</sub> N <sub>2</sub>	3 /h O C ዩ ዩ ዩ ዩ ዩ ዩ	127000 135 0.51 0.07 0.08 0.51 0.01 14.3 21.6 0.4 62.5
Sulphur cooling boilers			
Steam production - pressure - feed water temperature		t/h bar °C	10.4 1.7 105

# O+K A DIVISION OF OUTOKUMPU OY

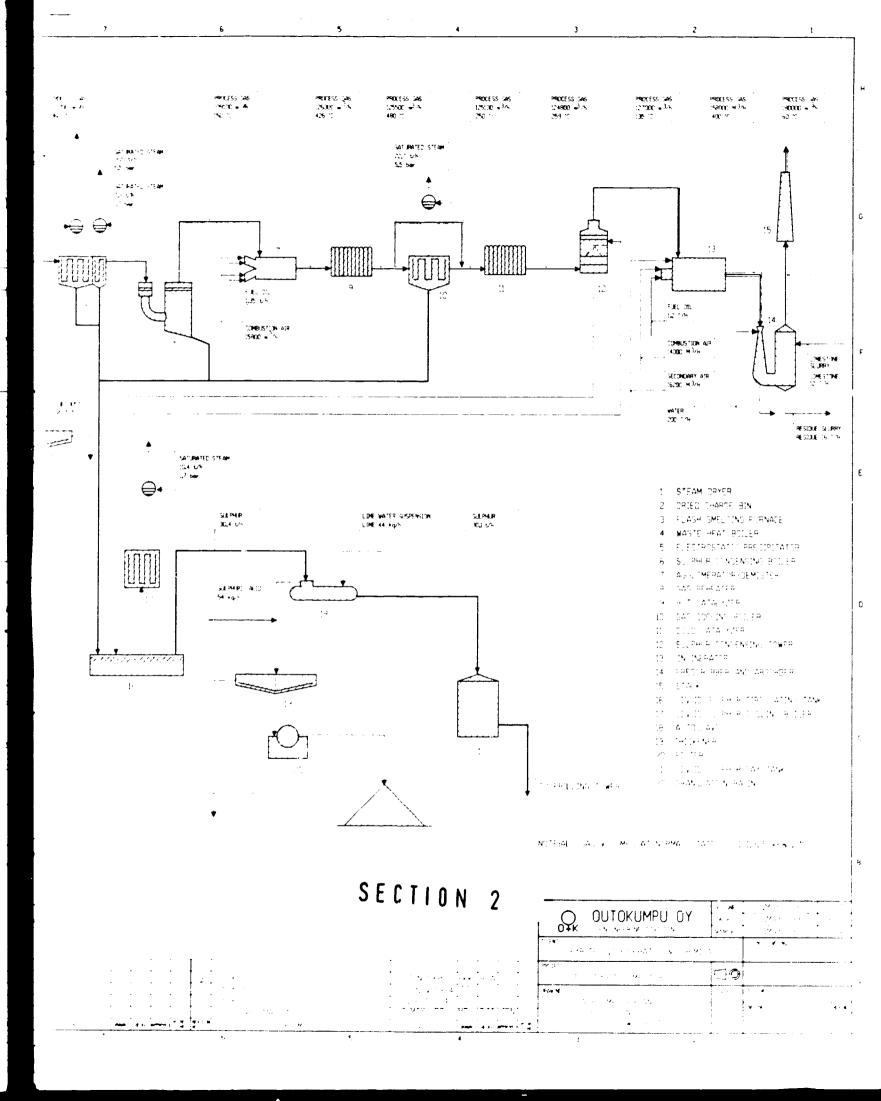
Incinerator			
Oil Combustion air Secondary air		t/h m3/h m3/h	1.2 14000 16200
Gas after incinerator - temperature - analysis	CO SO <sub>2</sub> H <sub>2</sub> O CO <sub>2</sub> O <sub>2</sub> N <sub>2</sub>	m <sup>3</sup> /h oc % % % % %	158000 400 0.13 1.23 13.9 18.5 1.5 64.7
Prescrubber and absorber			
Prescrubber water Limestone (80 % CaCO <sub>3</sub> ) Residue (dry)		t/h t/h t/h	200 12 16
Gas after absorber - temperature - analysis	CO SO <sub>2</sub> H <sub>2</sub> O CO <sub>2</sub> O <sub>2</sub> N <sub>2</sub>	m <sup>3</sup> /h oc % % % %	180000 60 0.11 0.05 23.6 17.3 1.3 57.6

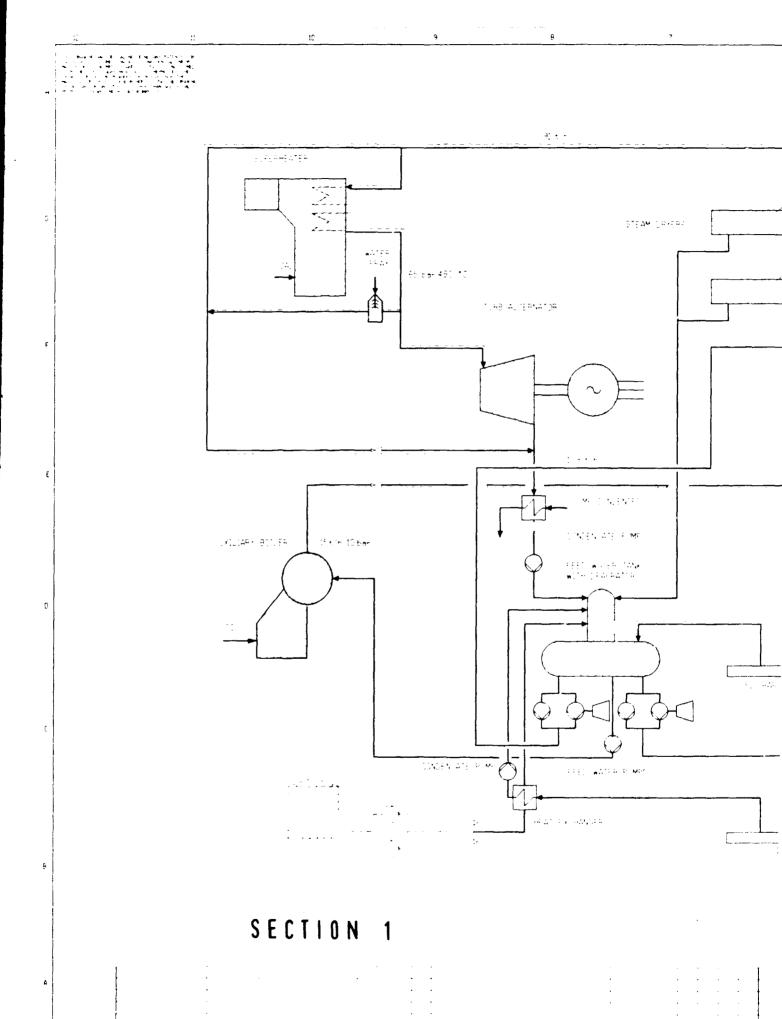


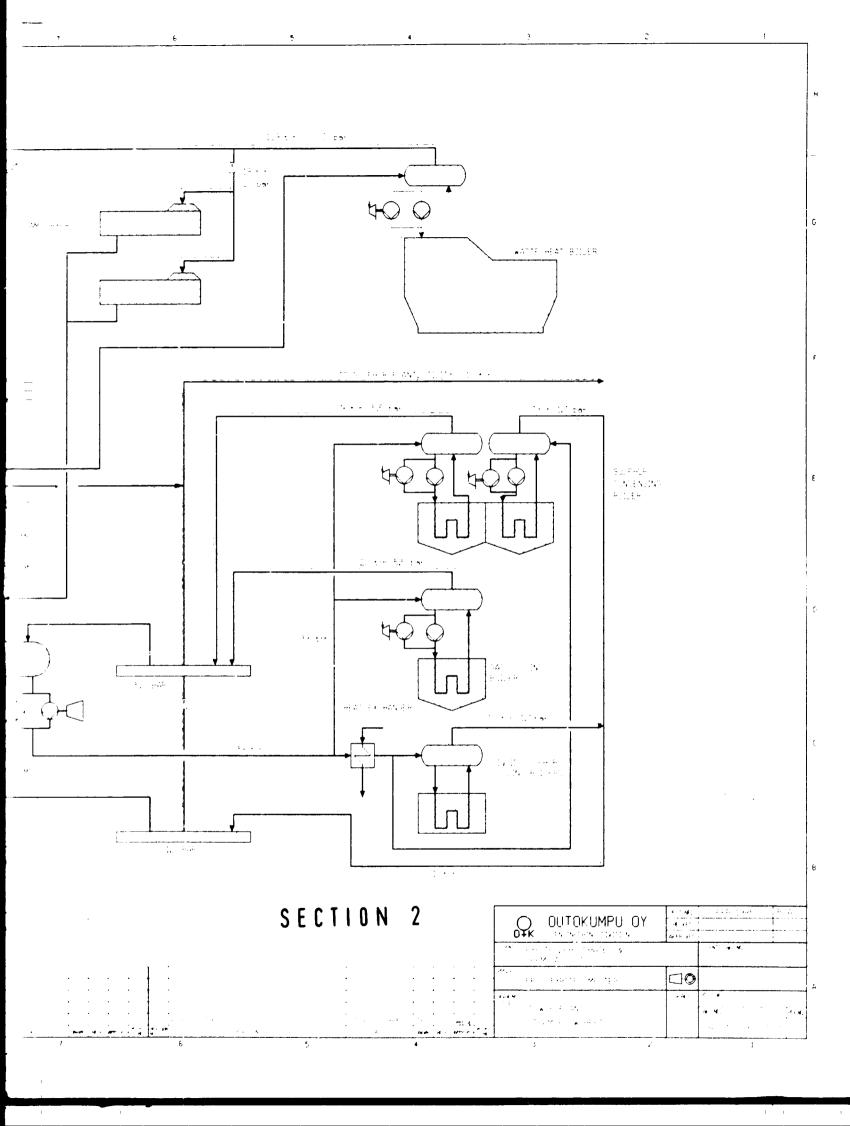
#### MATERIAL BALANCE OF THE FLASH SMELTING FURNACE

	Amount kg	8	S kg/h	8	Fe kg/h	*	SiO <sub>2</sub> kg/h		.1 <sub>2</sub> 0 <sub>3</sub> kg/h	8	C kg/h
In: Pyrite Top Shale Coal	83500 20000 20760		32940 2160 100	35.7 11.2 3.6	2240	15.3 50.4 10.4	12760 10080 2160	13.2		1.0 2.6 64.8	830 520 13450
			35200	······································	32820		25000		5460		14800
Out: Slag Flue dust Furnace o				45.4 22.3		32.3 31.2	21700 3300	6.2	4170 1290		1140 13660
			35200		32820		25000		5460		14800

### SECTION 1







1(2)



# OTK A DIVISION OF OUTOKUMPU OY

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# OUTOKUMPU ENGINEERING

4.	8	Draw	inas
- ·	•	DIGE	

Dwg Title	Dwg	No.			Rev.	No.
Flash Smelter and Sulphur Plant Equipment Diagram	360	100	901	004-9		3
Coal Plant Equipment Diagram	360	100	901	008-1		1
Power Plant Equipment Diagram	360	100	901	009-1		1
Flash Smelter and Sulphur Plant Water Main Flow Diagram	360	100	901	012-1		0
Flash Smelter and Sulphur Plant Site Plan	360	100	902	004-9		2
Flash Smelter and Sulphur Plant Plot Plan	360	100	902	005-1		2
Flash Smelter Area Plant Layout, Plan	360	100	902	006-0		0
Flash Smelter Area Playout Layout Sections A-A and B-B	360	100	902	007-0		1
Sulphur Plant Area Plant Layout, Plan	360	100	902	0-800		1
Sulphur Plant Area Plant Layout Sections C-C, D-D and E-E	360	100	902	009-0		1
Coal Plant and Power Plant Plant Layout Plan and Section	360	100-	902	010-0		1
Flash Smelter and Sulphurm Plant Instrumentation The Most Important Control Loops	360 1	FHS	0001	<b>-</b> 9		0



PLANT DESIGN

4.1 Plant Description

4.1.1 General Site Plan Dwg No. 360 100 902 004-9 Rev. 2 Plot Plan Dwg No. 360 200 902 005-1 Rev. 2

> The plant area is situated in Amjhore at the industrial area of PPCL, about half a kilometer south from the top of Hathini hill, alongside the proposed railway.

> The sulphur smelter plant is a complete unit producing elemental sulphur from ground pyrite ore. The plant includes power station to generate the electric power the whole plant needs from steam that the process produces. Coal needed as well as boiler water are treated in their own handling plants on the plant area.

4.1.2 Flash Smelter Area 200

> Dwg No. 360 100 902 006-0 Rev. 0 Dwg No. 360 100 902 007-0 Rev. 1 Layout Section

4.1.2.1 Dryer and FSF Feed Area 210

> Ground pyrite ore and top shale are transferred to concentrate day bins at the plant area by belt conveyors. The conveyors are not included in the plant scope.

From the day bins the materials are transported by belt feeders and conveyors through a screen to multicoil dryers. After drying in the dryers by steam heated tubes the material is lifted pneumatically to dried charge bin near the flash smelting furnace.

Exhaust gases from the drying plant are purified in a bag filter before blowing to the atmosphere.

4.1.2.2 Flash Smelting Furnace Area 220

> From the dried charge bin the materials are discharged by drag feeders and fed into the flash smelting furnace.

In the flash furnace - which is the heart of the sulphur production - pyrite smelts forming sulphur containing gases and iron and silica rich slag.

In smelting process air and excess oxygen are blown into the reaction shaft.

Slag is tapped from the settler part of the furnace and granulated by water sprays. Granulated slag can be transported e.g. by front end loaders and lorries.

The furnace is protected inside by chrome magnesite and isolation brick lining.

The settler part of the furnace as well as tapping holes are cooled by copper cooling blocks connected to jacket water circulation. Reaction shaft is cooled by spray water flowing down on outer side of the shaft.

The furnace is equipped with emergency damper and stack to be used in cases that for some reason gases cannot be taken into the waste heat boiler and the furnace is still kept hot.

### 4.1.2.3 Process Gas Handling Area 230

Smelting gases are reducted by coal injected into the lower part of the furnace uptake shaft.

From the smelting furnace uptake shaft gases are led to waste heat boiler, where the gases of about 1200oC are cooled to 350oC temperature. The boiler steam, 70 bar, is used for electric power production at power plant. Cooled gases are purified from flue dust by electrostatic precipitators (EP) which are installed two units parallely.

Process gas fans blow the smelting gases to the sulphur revovery area.

For special purposes, e.g. for short preparation work in an electric precipitator or sulphur recovery area simultaneously that the waste heat boiler (WHB) or the other electrostatic precipitator is wanted to keep hot, gases are drafted out of the process by the by-pass ejectors installed between WHB and EP:s and after each EP.

### 4.1.2.4 Flue Dust Handling Area 240

Flue dusts separated in WHB and EP are mixed with water to form slurry, which is conducted by launders to thickener.

### O OUTOKUMPU ENGINEERING

Underflow of the thickener is pumped to slag granulation rake classifiers and that way mixed to slag. The overflow water is used for slag granulation, flue dust slurry mixing and gas cleaning by a scrubber after sulphur recovery.

4.1.3 Sulphur Plant Area 300

Layout Dwg No. 360 100 902 008-0 Rev.l Section Dwg No. 360 100 902 009-0 Rev.l

4.1.3.1 Sulphur Recovery Area 310

Gases blown to sulphur recovery area are first cooled down in a sulphur condensing boiler, where the temperature of gases reduces to 150oC. In the temperature conditions of the boiler elemental sulphur condenses. It is taken out from the boiler bottom. The boiler produces 5.5 bar steam in the front part and 1.7 bar steam in the rear part.

Part of the elemental sulphur in the gas continue as small drops to an agglomerator where the drops grow bigger. The drops are then separated from the gas in demister by gravity.

Gases from demister are now heated up to about 4300C by a gas reheater, where oil combustion gases are mixed to the process gas. The gas reheater has two burners. The reheater is protected by refractory lining. Heavy fuel oil (Bunker C) is used.

Heated gases flow to hot catalyzer unit where additional elemental sulphur forms in the gas mainly from SO2.

Gases are again cooled in a gas cooling boiler where sulphur condenses due to temperature decrease. Gases cool down to 250oC. The boiler generators 5.5 bar abs. steam. The boiler is furnished with a by-pass duct to allow better control of cold catalyzer temperature in special conditions.

Gases flow from cooling boiler to two parallel cold catalyzers, where additional elemental sulphur is formed.

Sulphur is again condensed in sulphur condensing towers by spraying cooled sulphur counter-currently into the gas stream.

Gases from the sulphur condensing towers are blown by two exhaust gas fans through a demister, where the rest of the sulphur drops in the gas are separated.

The minor amounts of  $\rm H_2S$  the gas contains after the condensing towers are converted mainly to  $\rm SO_2$  in an incinerator combusting heavy fuel oil. Gas temperature after the incinerator is 400  $^{\rm O}$ C.

Before blowing into the stack the gases are finally washed in a scrubber-absorption tower system by lime stone slurry to minimize sulphur effluents to the atmosphere.

#### 4.1.3.2 Sulphur Handling Area 320

Elemental sulphur condensed and separated from the gas stream is conducted via pump tanks to a bigger liquid circulating pump tank.

Sulpur separated in the front part of the sulphur recovery area, which contains small amounts of flue dust, is pumped onto a gravity filter before directing into the circulation pump tank.

From the circulation pump tank the sulphur is pumped to agglomerasor/demister unit, via three sulphur cooling boilers to sulphur condensing towers, and to sulphur washing in two autoclaves (the producted sulphur).

In the autoclaves arsenic is washed off from the sulphur by lime stone slurry.

Purified sulphur is again filtered and pumped via measuring tanks to sulphur day tank and further to sulphur prilling tower.

In the prilling tower the liquid sulphur is granulated by spraying it as drops to fall down counter-currently to air stream in the tower.

Granulated sulphur is screened and conveyed to railway waggons by belt conveyors.

Liquid sulphur handling equipment are kept hot by 5.5 bar steam.

### 4.1.3.3 Waste Liquid Handling Area 330

Waste liquid from autoclaves is treated in a reactor where sulphuric acid is added. The arsenic impurity is precipitated and separated from the liquid by a thickener vessel, underflow of which is vacuum filtered to form waste cake.

4.1.4
Additional Plant Areas

4.1.4.1 Coal Plant Area 500

Plan and Section Dwg No. 360 100 902 010-0 Rev. 1

Coal handling equipment is located beside the smelter and power plant, to the west of the power plant.

On the plant raw coal is first stored in bins, then milled, and stored as pulverized. For utilization in flash smelter furnace and steam superheater (at the power plant) the coal is transported pneumatically and injected into the furnaces.

4.1.4.2 Power Plant 600

Plan and Section Dwg No. 360 100 902 010-0 Rev. 1

Separate power station is located beside the smelter area, north of it.

The power plant receives and handles separate steams generated in smelter plant boilers as follows.

- High pressure waste heat boiler steam 70 bar is superheated by coal and used to electric power generation.
- Medium pressure 5.5 bar steam is used for feed water heating in a common feed water tank, located at the power plant.
- Low pressure 1.7 bar steam from sulphur condensing and sulphur cooling boilers is used for heating the boiler feed water.

In power station an auxiliary boiler is installed, using oil as fuel. This boiler is used during shutdown cases to produce steam to keep smelter plant boilers and sulphur handling equipment hot and ready for start-up.

The power plant produces electric power, heating steam and boiler water to be utilized at smelter plant.

4.1.4.3 Oxygen Plant 700

Oxygen Plant 700 Oxygen for enriching the process air is produced in a separate plant, situated north from the other plant area, behind the main railway. Oxygen is conducted to the smelter plant in ducts as gaseous.

The plant is a complete unit comprising all equipment and accessories needed for pure oxygen 95 % production. Production capacity is 650 t/day.

4.1.4.4

Lime Stone Slurry Preparation Area 800 (IN OFFSITE FACILITIES)

Described in Chapter 4.7, Offsite Facilities Para 10, prepared by FEDO FACT, India.

4.1.4.5

Water Treatment Area 900 (IN OFFSITE FACILITIES)

Described in Chapter 4.7, Offsite Facilities, Para 3, prepared by FEDO FACT, India.

4.1.4.6

Compressed Air Station 950

Plant air is produced by two compressors. The capacity of each compressor is 35 Nm  $^{\prime}$ /min. The outlet pressure is 7 bar abs.

Instrument air is produced by drying and filtering the plant air. The capacity of the drying and filtering equipment is 7 Nm /min.

#### OUTOKUMPU ENGINEERING

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4.2 List of Equipment with Main Technical Data

4.2.1 Coding

#### CODE AREA

200	FLASH SMELTER AREA
210	DRYER AND FSF FEED AREA
220	FLASH SMELTER FURNACE AREA
230	FSF PROCESS GAS HANDLING AREA
240	FSF FLUE DUST HANDLING AREA
300	SULPHUR PLANT AREA
310	SULPHUR RECOVERING AREA
320	SULPHUR HANDLING AREA
330	WASTE LIQUID HANDLING AREA
500	COAL PLANT AREA
600	POWER PLANT AREA
700	OXYGEN PLANT AREA
800	LIME STONE SLURRY PREPARATION AREA
900	WATER TREATMENT AREA
950	COMPRESSED AIR STATION

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EQ. GROUP	EQ. TYPE	EQ. CODE
Basins	Granulation basin	108
Bins	Day bin Dried charge bin Feed bin Storage bin	116 117 117 118
Boilers	Steam boiler Superheater Waste heat boiler Boilers, others	122 123 124 129
Burners	Coal dust burner Oil burner Concentrate burner	131 133 435
Casting eq.	Launder	140
Conveyors	Belt conveyor Drag conveyor Pneumatic conveyor Screw conveyor Scraper conveyor Conveyors, others	167 168 170 172 174 179
Dryers	Steam dryer	194
Ducts, gas and dust pipes	Hopper Stack Water lock	202 204 209
Fans	Fan Blower	212 214
Feeders	Air lock feeder Belt feeder Drag feeder	216 218 223
Filter	Drum filter Gravity filter	243 244
Furnaces Heat-transfer eq.	Flash smelting furnace Incinerator Feed water heating/cooling heat exchanger Gas reheater Heat exchanger, others	261 263 280 281 289

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EQ. GROUP	EQ. TYPE	EQ. CODE
Lifting devices	Overhead travelling crane Crane	318
Mills	Mill	325
Pumps	Pump Dosage pump Ejector Slurry pump Vacuum pump Water pump	370 371 372 374 375 376
Screens	Vibrating screen	411
Separating eq.	Bag filter Cyclone Demister Electrostatic precipitator Scrubber	417 419 420 421 423
Special machines and equipment	Agglomerator Hot catalyzer Cold catalyzer Sulphur condensing tower Sulphur prilling tower	431 433 433 464 509
Tanks	Tank Autoclave Feed tank Measuring tank Mixing tank Pump tank Jacket and spray water tank Storage tank Reactor tank	510 511 514 515 516 518 519 519 521
Thickeners	Thickeners	532
Turbines	Steam turbine	556
Valves	Disc valve Emergency valve	562 569

### O OUTOKUMPU ENGINEERING OFK A DIVISION OF OUTOKUMPU OY

4.2.2 Equipment List (In Volume II)

Smelter and Sulphur Plant

Equipment diagram,
Dwg No. 360 100 901 004-9, Rev.3

Coal Plant

Equipment diagram,
Dwg No. 360 100 901 008-1, Rev.1

Power Plant

Equipment diagram,
Dwg No. 360 100 901 009-1, Rev.1

4.3

ELECTRIFICATION

4.3.1

Description of electrification

General principles

Principle of electric power distribution has shown in the main single line diagram. (Appendix 1)

Main transformer station

The main transformer station will be connected to the 110 kV line with open-wire circuit. The station comprises concrete foundations with fire walls of 110/11 kV main transformer and 110 kV switchyard incl. necessary compounds.

The rated power of the main transformer is 40 MVA.

Power plant

An electric room will be built in the power plant for a 11 kV main switchgear. The switchgear comprises 12 cubicles.

The power plant generator will be connected to the 11 kV main switchgear.

The rated power of the generator is about 25 MW.

11 kV auxiliary switchgears

There are three auxiliary switchgears. The switchgears will be located in following buildings:

Smelter Sulphur handling Oxygen plant

The energy will be fed from switch gears by cables to the distribution transformers and high voltage motors (  $\geq$  350 kW ).

The rs are to be placed in ventilated

440 V motor conti

rooms of each department. The energy will be fed from transformers to MCC's by means of bushars.

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Transformers	Following transformers will be required:
	Flash smelting area 3 à 1600 kVA
	Coal handling area 1 à 1600 "
	Sulphur handling area (waste liquid handling) 2 à 1600 "
	Sulphur recovery area 1 à 1600 "
	Oxygen plant 2 à 1600 "
	Power plant 1 à 1000 "
	Off-site facilities $\frac{3}{13}$ a' 1600 " $\frac{3}{13}$ pcs
	The transformers will be placed in separate transformer rooms in the immediate vicinity of motor control centers.
Emergency power	Emergency power needed in the plant will be generated by a diesel-generator. The emergency power unit will be located beside the smelter's electric room. The effect of emergency power unit has been chosen to about 600 kVA. Max. voltage after break-down is generated in 10-30 sec.
Control system	The control of electric motors has been centralized to the control rooms of departments.
Lighting and wel	ding outlets
	Illumination shall provide necessary lighting for the process area. HP-Na lamps and fluorescent tubes will be used.
	Light pillars and masts will be used for area lighting.
	Welding outlets will be located in all necessary working areas.
Power demands	Total installed power is estimated to be 23,4 MW. It can be divided into following parts:
	Flash smelter area 4,5 Sulphur recovery area 1,4 Sulphur handling area 2,0 Oxygen plant 10,0 Coal handling area 1,4 Power plant 1,2 Off-site facilities 2,9 Pinst. 23,4 MW

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Normal running load

Running load at full capacity 17,5 MW

 $\cos y = 0.8$ 

Compensating

Compensating will partly be performed by capacitor banks and partly by power plant generator by which also the regulation of compensation is performed.

Engineering criteria of electrification

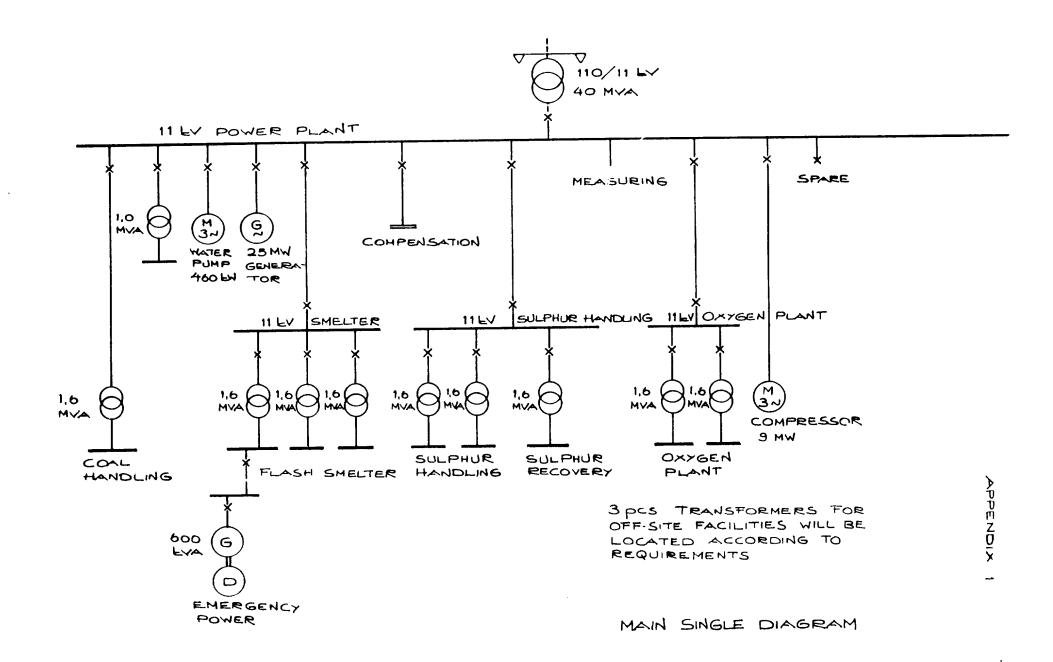
Voltages	Power supply	110	kV	3	ph	50	Hz
	Primary distribution	11	kV	3	ph	50	Hz
	Motors over 350 kW	11	kV	3	ph	50	Hz
	Motors 350 kW and below	440	v	3	ph	50	Hz
	Control (motors)	220	V	1	ph	50	Hz
	Control (HV-distrib.)	110	v	DC	3		

Short circuit capacities

110	kV	3500	MVA	(max.	allowed)
11	kV	500	MVA		
440	V	38	kΑ,	1 s.	

Energy consumption
(estimated operating time 7500 h/year)

Flash smelter	24	000	MWh/a
Sulphur plant	13	000	MWh/a
Power plant with coal handling	10	500	MWh/a
Oxygen plant	66	000	MWh/a
Off-site facilities	<u>17</u>	250	MWh/a
	130	750	MWh/a



#### LIST OF MAIN ELECTRICAL EQUIPMENT

			LIER
	<u>!</u>	FOREIGN	LOCAL
1	Main transformator 110/11 kV, 40 MVA	;	x
2	Power generator 25 MW, 11 kV	x	
3	11 kV switchgears, 4 pcs		x
4	Distribution transformers 1,6 and 1,0 MVA, 10 pcs		x
5	Motor control centers 440 V and relay panels		×
6	Emergency power diesel generator set	×	
7	Frequence converter drives	x	
8	Installation material, cables, cable trays lighting, telecommunication equipment, grounding, power outlets, control boxes etc.	; <b>,</b>	
			x

# OTOKUMPU ENGINEERING

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4.3.2 Motor List

In Volume II

### OUTOKUMPU ENGINEERING

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4.4
INSTRUMENTATION

4.4.1 General Description of Instrumentation

#### CONTENTS

1.0	Design Concepts
2.0	Control Rooms, Control Panels and Operator Work Stations
3.0	Field Mounted Instrumentation, Wiring and Piping
4.0	Power Supplies, Signals and Units of Measurements
5.0	Drawings and Data

1.0 DESIGN CONCEPTS	
1.01	The instrumentation and control system will be designed to provide information and control necessary to operate the plant efficiently, economically and safely with a minimum of personnel.
1.02	The controls shall be implemented using industry standard instruments and control systems. Use of custom designed or proprietary control systems shall be avoided to the extent possible.
1.03	Major instrumentation and controls shall be standardized in all plant areas of the project.
	The following factors shall be given special consideration.
	The number of operators required to operate the plant.
	The availability and the location of vendor service and parts supply centers.
	The amount of flexibility demanded by plant operations and optimum cost per unit of production for fuel, power, additives and labor.
	The maximum recovery of a high purity product and controlled pollutant levels in plant effluents.
1.04	Electronic type instruments shall be generally used. Use of pneumatic instruments shall be avoided, except for control valves, certain local control loops, and special applications where the pneumatic instrumentation has a definitive advantage over the electrical instrumentation.
1.05	The control room instrumentation shall be based on a modern distributed digital control system (DCS). In addition a computer system for optimization, high level controls, data acquisation, reporting and process management shall be included in the project plan.
1.06	ISA symbols shall be used on preparing of Piping Instrumentation Diagrams (P & ID).
1.07	DIN standards and metric units shall be used on instrumentation design.

2.0 CONTROL ROOMS, CO	NTROL PANELS AND OPERATOR WORK STATIONS
2.01	A central control room (CCR) with control panels and operator work stations will be provided. The control room shall be the point of control for operating and/or monitoring the process and will contain the necessary instrumentation and controls to operate the process.
2.02	Colour TV-display units and Operator Work Station (OWS) with dynamic keyboard shall be used for DCS.
2.03	A free standing control panel with semigraphic diagram on the top part shall be provided for CCR. The vertical section of the panel shall include complementary analog instruments. The sloping console section shall include start-stop push buttons for motors, selector switches, ammeters etc.
2.04	There will also be a Relay Room (RR) near CCR for auxiliary equipment and electronic cabins of DCS.
2.05	The CCR and the Relay Room shall be pressurized with filtered air to exlude dust and noxious gases (SO2 and H2S) and shall be air conditioned to maintain suitable constant temperature and humidity.
2.06	There will also be a control room for elementary sulphur plant. One sub OWS of DCS shall be located there. Certain operations of the sulphur plant will be controlled from this control room. A conventional control panel like that at CCR, shall be provided there, too.
2.07	The other plant of the area (Power Plant, Oxygen Plant and Coal Powder Plant) shall have their own control systems. However, the operations of these plants are depending on each other because their processes shall be connected together. That is why adequate information transmission between them shall be absolutely necessary. Information connections between the plants will be defined on Basic Engineering.



### 3.0

FIELD MOUNTED INS	STRUMENTATION, WIRING AND PIPING
3.01	Field Mounted transmitters shall be two (2) wire type wherever possible. For certain special applications, where two (2) wire transmitters are not available, four (4) wire transmitters may be used.
3.02	Enclosures for field mounted instruments shall be DIN IP54 dust tight and water tight construction. Classification for hazardous application location, if required, shall be specified on the data sheets.
3.03	Instruments located outdoors and subject to severe ambient conditions including moisture, freezing and corrosion, shall be protected either by heating and/or shall be installed in weatherproof housing or shelters. The use of protective housing, or enclosures shall not inhibit the functioning of the instrument or detract from the ability to perform routine service.
3.04	All automatic control valves shall be provided with isolating block and bypass valves, unless dupliction of equipment and lines allows control valve replacement without shutting down the process. Control valves which are not provided with isolating block valves and bypass shall be supplied with a manual handwheel or other means for hand operation.
3.05	Instrument signals and alarm wiring shall be designed with twisted pair cable with aluminum mylar electrostatic shielding, a bare copper drain wire and overall PVC jacket. The cable shall be suitable and approved for installation in cable trays.
3.06	Multipair cables shall generally be used to connect the field junction box to the control panel. The cable characteristics shall be same as above except each pair of conductors shall be individually shielded and have a bare copper drain wire.
3.07	The primary instrument connection shall be the responsibility of piping section. These connections will include process block valves, thermowell or probe couplings and flanges.
3.08	The instrument process piping material including tube, valves and fittings shall be 316 stainless steel.
3.09	The tubing runs for pneumatic transmission signals, and connections between filter-regulators and instruments, shall be made with 6 mm outside diameter 316 stainless steel tubing with 1.0 mm wall thickness.
3.10	Tube fittings for pneumatic system shall be 316 stainless steel compression type.



4 ^			

4.0 POWER SUPPLIES, S	SIGNALS AND UNITS OF MEASUREMENT
4.01	The electrical supply for instruments will be 220 V, 50 Hz.
4.02	An uninterruptible power supply (UPS) providing 220 V/50 Hz shall be provided as the source of power to the Distributed Control System (DCS). The UPS shall provide a bumpless, fully synchronized 220 V/50 Hz power to DCS for a minimum period of 60 minutes in case of a power failure of primary source.
4.03	Supply of power to all instruments regardless of their location shall be design responsibility of instrument section. The supply of power to field instruments shall originate from the appropriate control panel. The instruments in the same loop shall be powered from the same source of power.
4.04	Pneumatic instruments shall operate from instrument air supply of 140 kPa gage pressure and shall yield a control signal over a range of 20 to 100 kPa gage pressure. Under special circumstances other signal ranges, and air supply pressures may be specified.
4.05	The piping section will supply a nominal 600 kPa gauge pressure dried and filtered instrument air supply source.
4.06	The main instrument air header design shall be the responsibility of the piping section and shall be shown on the area piping drawings.
4.07	The following transmission signal levels shall be used:

- 4-20 mA DC Analog Signals - 24 V DC - 24 V DC Alarm Signals Counters Solenoid Valves - 220 V, 50 Hz
ON-OFF Controls - 220 V, 50 Hz
Status Signals - 220 V, 50 Hz
Interlocks - 220 V, 50 Hz 4.08

The following SI metric engineering units shall be used on instrumentation:

- Kilopascal gauge pressure (kPa gauge) (a) Pressure
  - Megapascal gauge pressure (MPa gauge)
- (b) Vacuum - Pascal Vacuum (Pa vacuum)
  - Kilopascal Vacuum (kPa vacuum)
- (c) Temperature Degrees centigrade (C)
- 0-100 percent (d) Level
- (e) Flow - 0-100 percent linear

Water, volume - Liter per second (L/s)

Process liquids

volume - Liter per second (L/s)

Process additives (liquids),

volume - Liters per hour (L/h)

Process additives

(solids), mass - Metric tons per hour (tph)

Process solids

- Metric tons per hour (tph) mass

(f) Angular

- Revolutions per minute (rpm) speed

0-100 percent

(g) Linear

- Meter per second (m/s) velocity

- Kilogram per cubic meter (kg/m<sup>3</sup>) (h) Density
- (i) Electrical

- Ampere (A) current

- 0-150 Percent

(k) Acidity,

Alkalinity - pH Unit

(1) Oxidation

Reduction

Potential - millivolts (orp mV)

5.0 DRAWINGS AND DATA

5.01

A set of basic engineering drawings and data shall be prepared for major instrumentation and control systems. The drawings and data shall be sufficient to allow a qualified engineering company to perform detail engineering. The basic engineering drawings and data shall include the following:

- General Specification for Instrumentation Design
- Instrument Index
- Piping and Instrumentation Diagrams (P & ID)
- P & ID Symbols and Legends, Instrumentation
- Preliminary Instrument Data Sheets
- Control Panel Specifications
- Control Panel Layouts
- Preliminary lay-out for Central Control Room and Relay Room
- Space reservations for local control rooms and desks
- General specifications for Distributed
   Control System and Computer System
- Block Diagrams for DCS and Computer
- General specification for main control functions and operation
- General Specification for Instrumentation Installation

5.02

A complete set of detail engineering drawings and data shall be prepared for all instrumentation and control systems. The drawings and design data shall be detailed to allow a qualified contractor to submit bids for the procurement of installation material and completion of the work with a minimum of field engineering at the jobsite. The detail engineering drawings and data shall include the following:

- Updated Basic Engineering Drawings and Data
- Loop Diagrams
- Wiring Diagrams

### O OUTOKUMPU ENGINEERING O+K A DIVISION OF OUTOKUMPU OY

Cable Schedules
 Cable Tray Layouts
 Plot Plant of Field Instruments and Junction Boxes
 Installation Details and Bills of Material
 Drawings of Process Couplings and Tappings
 Vendors Drawings and Data for engineering, maintenance, construction and record purposes
 Drawings of Auxiliary Voltages Supply system
 Drawings of Installation Racks and Auxiliary

Equipment Cabins

4.4.2 Preliminary Loop Number Schedule for Instrumentation

Instrument code letter identifications have been designated in accordance with the standard of Instrument Society of America. In addition following symbols have been used to decine operation/location of the instruments:

- / Distributed Control System connection
- O A local instrument
- θ An analog instrument at Control room
- X An interlock or special service

A tag number of an instrument shall consist of five digit numbers. The first two digits represent the plant area in which the sensing or primary is located, followed by a three digit sequential number. The plant area numbers are:

- 00 GENERAL AREA, UTILITIES
- 01 MATERIAL DAY BINS AND FEEDING EQUIPMENT
- 02 DRYING AND DRYED CHARGE BINS
- 03 FLASH SMELTING FURNACE
- 04 GAS COOLING AND DEDUSTING
- 05 SULPHUR PLANT, GAS LINE
- 06 SULPHUR HANDLING EQUIPMENT

Attached are 16 sheets of Loop Number Schedules.

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71 - 03 123	ARC TEMP OF FLASH SHE	LTING FERNACE		_/_	<u> </u>	<u> </u>	<u> </u>	ļ	<b></b>	ļ	ļ				
71 - 03/24	TAKE -UP SHAFT OF FSF				<u> </u>	<u> </u>	<u> </u>				<u> </u>				
TJR- 03.125	TAKE-UP SHAFT OF FSF	<u>_</u>			6	_									
IDIA - 03126	PRESSUE WOOD OF TAKE UP:	CHAFT THPOAT				L				/					
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	15 PARRYING AIR FLOW BUL		ll	4	_						<u> </u>				
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111A 02302	JACKET WATER TANK								/	1					
F4: 12303	MAKE - DE WATER														
PAL - 02 304	PRITIATI COOKING WATE	R								/					
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-145 - 03306	JACKET WATER			/						1	$\times$			•	
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11 03314	FR MARY CANLING WATER AT SOLE	T OF HEAT EXCH.					<u>L.</u>	<u> </u>	<u> </u>	<u> </u>		L			
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Loop No	Service			D C	R C C	inte	₽ E	Set	S	Alarm	<u>=</u>			Notes		
	CAFFYING GAS FLOW			 4												<del></del>
	CAKETING GAS		<del> </del>	 						<u> </u>	-	<b>├</b>	P-038			
	CAPPYING GAS		<del></del>	 7				<del> </del>	-	ļ		<del>├</del> ─┼	T COET			
	L'OTARY SCALE COAL INJECT ROTARY SCALE COAL INJECT		<del> </del>	 /		<del>-</del>			1	-		┞─┼	CLAVE CO			
	ESTARY SCALE COAL INJECTO		1	<del>'</del> /	$\dashv$	7		<del>                                     </del>	7	<del>                                     </del>	<del> </del>	<del>                                     </del>	SLAVE CO			
	ENTARY SCALE COAL INJECT		† <u> </u>	 7					1		-	$\vdash$	SLAVE CO.			
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	TOKUMPU OY	Client		Pro	ject								Designed	Checked	Approved
	INEERING DIVISION SPOO FINLAND	PPCLIA						27E H-4 <b>A</b> ,		A 11)	Ŋ		144 E4	<del> </del>	
Drawing INST	RUMENT LOOP NO SCHEDULE	Drawing No.	163 011			_					9.0		Rev. No	III	
Area 04 WASTE	HEAT BOILER EL STATIC PRECIP	Function		ation	Recording	grati	Hand control	point	roi	E	locki				
Loop No	Service			i di	Reco.	In te	Ē	Set	Control	Alar	Inter			Notes	
	STEATA FLOW			/		/									
	FEED WATER FLOW					/									
	CILCULATION WATER				ļ	ļ		1	ļ	1	×				
	DRUM LEVEL					L	1_	1	1	1	L				
<del></del>	STEAM FRESSORE OF DE			/_	<b>!</b>	_		<del> </del>	1	A A D A C C C C C C C C C C C C C C C C					
	PPESSURE DROP OF FONCES			/	ļ	<u> </u>	<u> </u>	<u> </u>	ļ	14				· · · · · · · · · · · · · · · · · · ·	
	SAS PRESSURE INSIDE TH			/_	<b></b>	<u> </u>	1_	<u> </u>	1	1	ļ		SLAVE 101	TILE OF 4	1cA-031.
	FEED WATER BY FASS YAL	νE			L	ļ	1	<del> </del>	<del>  </del>	↓	<b> </b>				
	MAIN STEAM: VALVE				<b> </b>	ļ	1/	<del> </del>	<del> </del>	<b>↓</b>	<u> </u>		_		
	START-UP STEATA VALVE	-			<u> </u>	<b> </b>	1	╁	<b> </b>	<del>ل</del> _	ļ		<b>_</b>		····
	FEED WATER PRESSURE				<u> </u>	├	<del> </del>	<del> </del>	<b> </b>	14	<u> </u>				
	FEED WATER TEMPERAT	OKE		/_	├	<del> </del>	<del> </del>	∔	-	1	<del> </del>			<del></del>	
	DUDA LEVEL				<b> </b>	↓	↓_	<del> </del>	<del> </del>	14	X				·
	ENILER WATER CONDUCTIVE			/_			↓	↓		14	ļ				<del></del>
	CONTINUE BLOW-OUT OF THE D.			/	<b> </b>		╁	<del> </del>	<b> </b>	<del> </del>	ļ				
	GAS TELLE OF RADIATION PART				<b>├</b> —			╂	<del> </del>	<del>  _</del>	├				
	GAS TEMP. AT BOILER OUTLE				-	-	╁-	-	<del> </del>			<del>  </del>	<del></del>	<del></del>	
	GAS TEMP AT BOILTK OUT LI				0		+	-	<b></b>	<b>├</b> -					
	DRAG CONVEYOR OF FLUE					├	<del>  _</del>	- <del> </del>	<del> </del>	1/	<del> </del> :		<del>-</del>		
	DISC VALVE AT INLET OF EL.				<del> </del>	├	1	<del> </del>	<b></b> -	<b>↓</b>	<del> </del>	<del>                                     </del>			
	DISC VALVE AT LIET OF ELS	TATIC PRECIP.			<u> </u>	├	1		<del> </del>	╂	-				
1 04/122	HY-PASS EJECTOR		<del></del>			<del> </del>	/	╂	<del> </del>	-	-	<del>                                     </del>	<del></del>		
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Drawing INST	TRUMENT LOOP NO SCHEDULE	Drawing No. 360 FHO 16	ェーショー <u></u>			e e	control				وَ		Rev. No Instr. digg	fam. No.	
Area NA ELECTI	POSTATIC PRECIPITATIONS	Function		Indication	Recording	Intergration	60	Set-point	ē	E	8 8		listi. didg	14111 110	
Loop No	Service			In de	Rec 0	late	Hand	Set	Control	Alar	Inter			Notes	
77 - 04201	ECONDARY CUREENT OF PRECIPIT	TATOR PELD 1		1									·		<del></del>
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	SECONDARY CHERENT OF PUTCIFI			1			1								
VI - 04204	SECONDALY WATAGE OF HEELT	ITATOR PIELD 1		1		Τ	1								
	SECONDARY VOLTAGE OF HERIDI			1/											
	SECONDARY VOLTAGE OF PRECIP			/										•	
	SECONDARY VOLTAGE CONTRIL						1								
	SECONDARY VOLTAGE CONTROL						/		$\prod$						
HC - 04201	SECONDARY VOLTAGE CONTROL	FIELD 3					/								
XI - 04 210	SPARK RATE FIELDA			1/			T							· · · · · · · · · · · · · · · · · · ·	
VI - 04211	SPARK RAIE FIELD2			/											
XI - 042.12	SPARK RATE FIELD 3			_/											
TA - 04213	TOP PART OF THE PRECIPITAT	OR.		1						1/			AT/At AL	AFMING FO	P FIFE DET
7/4 - 0421,	TOP PART OF THE PRECIPITAT	OR		1			Τ			/					FIRE DETECT
	TOP PART OF THE PRECIPITAT			7	(	1	T			1					THEY DETRE
-A - 04216	BOTTOM HART OF THE PERCIPITA	170K		1/						1				#	
T/A - 04217	BOTTOIN PART OF THE +KECIPITA	TOK		1					Ĭ	1				·	
JE - 8125.4	ENTTOM LART OF THE PHECIPI	TATOR			e					/					
XA Minais	MALFINCTION OF THE PRECIP	177170 R								1					
F/Q - 0/1220	HEATING STEAM FOR ISOLAT	ORS		1		/									
SAL - 01,221	DLAG CONVEYOR OF FIVE DUS	iT .								1					
SAL MIZZZ	DRAG CONVEYOR OF FLUE DU	ST		1						1					
	PRESSURE AT OUTLET OF THE									/					
	TEXID, AT GUTLET OF THE !			1	$\Theta$										
11. 04225	FY BASS EJECTOR														
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	L				<u> </u>	<u> </u>	Щ.	ــــــــــــــــــــــــــــــــــــــ	<u></u>	<u> </u>	L				

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Drawing INC	TRUMENT LOOP NO CONFOUNC	Drawing No.				~//			-71 (	, , 				Rev. No	+	+
	TRUMENT LOOP NO SCHEDULE		F40 163 N	) 1	_	_	6	control	+			5	-	Instr. dia	aram No	<del></del>
Area Say EVEY	TPOSTATIC PFECIPITATORS	Function			Indication	Recording	Intergratio	C 0 L	point	ē	٤	Locking				
Loop No	Service				Indic	Reco	Inter	Hand	Set-1	Control	Alarm	Inter			Notes	
II- 04231	SECONDARY CURRENT OF FRECIPIT	ATOK FIELD 1			.1											<del></del>
	SECONDARY CUERENT OF EXECIPIT,				1											
77 - 04233	SECONDARY SORRENT OF FRECIPITA	TOK FIELD 3			/											
	SECONDARY VOLTAGE OF PRECIPITA				/											
VI - 04235	SECONDARY VOLTAGE OF PRECIPITA	TOR FIELD 2			/											
VI - 04236	SECONDARY VOLTAGE OF MECIPITY	TOR FIELD 3			/										•	
	SECONDARY VOLTAGE CONILOL F							1								
	SECONDARY YOUTHGE CONTROL F							/								
	LECONDARY VOLTAGE CONTROL F							/								
	SPARK RATE FIELD 1				1											
.1 - 04241	SPARK RATE FIELD 2				/											
.1 - 04242	SPARK RATE FIELD 3				1											
TIA - 04243	TOP PART OF THE PRECIPITAT	0R			/						1			AT/At ALAH	MING FOR	FIRE DETECT
-11 - 04244	TOP PART OF THE PRECIPIT	ATOK			/						1	-			1.	
JP - 70.125.6	TOP PART OF THE PRECIPIT	ATOR			1	0					7				/-	
71A = DH146	BOTTOM PART OF THE PRECIPIT	FATOR			/						/				·· / · · · ·	
FA - 04247	BATTOM PART OF THE PRECIPIT	ATO R									/				1	
7UF - 03,125.7	POTTOKI HART OF THE PRECIPIO	FATOR			1	$\mathfrak{D}$					/				и	
XA - 04249	CONTMON MALFUNCTION AZARM	OF THE PRECIP									_					
FIQ- 04250	HEATING STEAM FOR ISOLAT	OKS			/		1								_	
SAL - 04251	DRAG CONVEYOR OF FLUE DU	ST									/					
SAL - 04:52	DRAG CONVEYOR OF FLUE DU	s T									/					
PIA 04253	PRESSURE AT OUTLET OF THE P	PECIPITATOR			/						1					
111 - 03.125.8	ETAP. AT OUTLET OF THE PI	PECIPITATOR				Θ										
-16 04255	BY-PASS EJECTOR															
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	RUMENT LOOP NO SCHEDULE	Drawing No. こらり / Function	THO 163 00	f	6	g.	ation	control	int			ocking		Rev. No Instr. dia	gram No	
Loop No	FSS JAS FAMS Service				Indication	Recording	Intergration	Hand c	Set-point	Control	Alarm	Interloc			Notes	
11AH - 74301	POWER OF PROCESS GAS	FAN			Ħ	α	=	-	01	3	1	=	-			
	VIER ATION				╀	<del> </del>	<del>                                     </del>	<del> </del>	<del> </del>	<del>                                     </del>	/			<del></del>	•	
	WINDING OF MOTOR								<b>†</b>		1	1			·	
	MOTOR & FAN BEARING										1					<del></del>
	SPEED OF PROCESS GAS A	AN			1										· · · · · · · · · · · · · · · · · · ·	
1144 - 04306	POWER OF PROCESS GAS F.	AN			/						/				•	
NAH - 0/1307	VIBRATION										/					
	WINDING OF MOTOR										1					
TAH - 04.303	MOTOR & FAN BEARING	?									/					
	SPEED OF PROCESS GAS F		· · · · · · · · · · · · · · · · · · ·		/	L	ļ	<u> </u>	<u> </u>	<u> </u>	<u> </u>					·
TJK -02.125.9	PROCESS GAS TEMP AT OUTLET O	F THE FANS			ļ	0	ļ		<b> </b>	<u> </u>	ļ					
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,	ESPOO FINLAND	INDIA	105	a guttatos	FLANT		CMA	
Drawing title	INSTRUMENT LOOP NO SCHEDULE	Drawing No. 365 FHS 163 501		lont		бu	Rev. No	
Are 05	SULPHOR PLANT, GAS LINE	Function	ation	grafi grafi		l ock i		-
Loop No	Service			Puph	) Juog	Alar Inter	Notes	
F.	NS 101 MOCESS GAS AT IMPET OF SOLFWOR G	OF SULPHUR COMORINGING BOILER	L_			╀		
1.1	05 102							
7.JR -	051031		Θ					
	05104 FLEO WAIER FOR 5.5 EAR BOY	EDILER	/					
FIA -	OSING STEAM OF S.SBAR BOILER		/	/				
FIAS -	يد	OF SEBAR POILER	/			メヽ	•	
11CA -	05107 DRUNG LEVEL OF 55 1.AR BYLER	2 E R			/			
1 273	OSMO STEAM HITSSURE OF SSBAR BOILER	BB112FR	/		/			
F1 -	05160 FEED WATER FOR 17BAR BULER	1.ER	//					
F10 -	05/110 STEAM OF 178AR BOILER							
F/AS - 1	05111 CIRCULATION WATER OF 17BAR	18 BOILER	/		_	X   X		
-	05112 DEUM LEVEL OF 17BAR B	BOILER						
PIC -	OSTIS STEAM FRESSORE OF 1+BAR BOILCR	BOILCR	\					
171 - (	OSTILL THOUSE AND PPESSURE AT OUTLET	7 OF THE BOLCE						
$i \in I_{(\frac{1}{2})}$	05115 TEAND AT SUTLET OF SUDMY C	COND. BOLLE						
118 - 0	11		(0)				•	
0 - 1 <u>a</u>	05.116 PROCESS GAS PESS AT OUTET OF	AT OUTLET OF AKSLOTIERATOR	\					
77 - 0	US. 117 PENCESS GAS IN COUTLET OF DEA	DEMISTER-AGGINA						
17, 0	05.118		/					
V - 4/2	1 - H -		Œ					
V - 2H	65.119 EV-PASS VALVE OF DEMISTER-AGGINEPATOR	SGLOWERATOR						
AICR - C	OS 120 PENCESS CAS CHAINTOGRAPH FOR SO, 185, COS	502 112 605	/ 0				MASTER CHITRE FOR COAL	ו יועבכדיטו
1.1 - 0	05. 121 PROCESS GAS PRESS AT CONUTY OF GAS FAIN	F GAS FAN						
[ ]	05 122 PROCESS GAS TEMP ATTINIET OF GR REHEAT	F GKS REHEAT	/					
- 37: - 0	05.103.4		Φ					
710 - 0	05.123 PRICESS ANS TELID. AT COUNT OF GAS REHILATER	. REHEATER .	/			X	WASTER CONIRR. OF FUEL ATAMOUN	WOMEN 2
JR - A	N5103.5		Θ					
1717	OS DA TOCESS SAS PIESS, AT MEET OF HOT CATALYRER	OT CATALYZER	_					

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E	SPOO FINLAND	101DIA			SUL	PH	UL	P	LAF	17_			2011		
Drawing INS	TRUMENT LOOP NO SCHEDULE	Drawing No. 369 FHD	162 001			ation	control				5 0		Rev. No Instr. diag	Sam No	
Area 05 50%	FAUR PLATIT GAS LIVIE	Function		Indication	guip	Intergratio	Con	point	Control	E	nterlocking		, matri didg	· (),,,	
Loop No	Service			a di di	Reco	Inter	Hand	Set-	Cont	Alarm	Inter			Notes	
17 05 125	LLOCESS GAS PRESS AT OUTLET	F HAT CATALYEED		1											
711A - 05126	PRICESS SAS TEAD AT AUTLET OF	HOT CATALYZER		1						/					
					$\Theta$										
PI - 05127	PLOCESS GAS PRESS AT OUTLET OF	GAS COOL ENKER		/											
	PROCESS GAS TEMP AT OUTLET OF								/					_	
TUR - 05.103.7					$\Theta$										
1 - 05123	FEED WATER FOR GAS COOLIN	G BOILER													
=/Q - <b>0</b> 5/30	STEATH OF GAS CANITYS	BYLER		1		1									
MAS - 00131	CIRCULATION WATER OF GAS	COOL NG EVER		/						/	×				
LICA - 05132	DEUL OF GAS COULT	NG BAILER		1					/	1					
	STEAM PRESSURE OF GAS COS								/						
FICE - 05134	FUEL OIL OF THE GAS REHEAT	TER EURNER 1				/					<u> </u>	_	SLAVE CON	TRE OF TIC	105.12
EFIC - 15135	COMBUSTION AIR FOR PEACATE	ER EURNER 1		_ /		L									
<i>TT - 051</i> 36	TEMP OF COMBUSTION AIR			l									T. GORRE	SC770AL FO.	1º FLOUS
PT - 05137	FRESS, OF COMBUSTION AIR												F CORRECT	STONI TO	( 17. 10g
F16 V 05/38	FUEL OIL OF THE GAS REHEATER B	URNER 2		/					/				SLAVE OF	HIR OF TI	c . 55 12.
FFIC 05 133	COMBUSTION AIR BUNNER	2							/						
	TETTE OF COLLEUSTION AIR												T. COPRE	C710N 7	17.17.18
-7 - 05/41	HAESS, OF COLLEGETION A	IR.											P-COKRE	CT1011 10	1 FLOW
MA - 05142	PROCESS GAS PLESS AT DUTLET OF	OND CHALYPERY													
"IA - 05143	TYNCESS GAS TEMP. AT OUTLET OF	OLD CATALYZER 1								/					
JR - 05 112.8	en e				$\odot$										
MA - 02.144	HADCESS GAS PRESS, AT MILET Y COLD I	CATALYZER Z		1											· · · · · · · · · · · · · · · · · · ·
	PRINCESS MAS TEMP AT OWNET OF COLD :	ATALYTER Z		/						/					
JR - 05103.3					Φ			]	]						
	PROJESS GAS HESS AT DITLET OF COND	. TOWER 1						/					MASIER 4	DITTEK. OF S	1c -DS17
TIA - 05147	HONOFES GAS TEMP. AT 100 LET OF CONN	D. TOWER 1					[	]	_	/					
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	INEERING DIVISION	PACL			FLA	$\leq H$	51	2 E. C.	iΣt	? #	NO	149 84		
ES.	SPOO FINLAND	INDIA			501	p 4.	11/	11	19.11	7		SOM	1	
Drawing INST	RUMENT LOOP NO SCHEDULE	Drawing No.					-					Rev. No		
		≥60 F Function	HO 163 171	<sub>6</sub>	5	ation	Hand control	point			king g	Instr. dia	ram No	
<del></del>	HOR FUNDT, GAS LIVE		· · · · · · · · · · · · · · · · · · ·	ication	Recording	6.1	٦	8	Control	E	E			<del></del>
Loop No	Service			Indi	a G	Ĕ	Hand	Set-	ပီ	Alar	e la		Notes	
12h 05148	PLYESS GAS PRESS. AT DUTILT OF C	OND. TOWER 2		/				/				MATER COI	VIPPOF SI	C-0511
74 - 05140	FFOCESS GASTEMPLATO LLET OF G	OND. TOWER 2				<u> </u>	L.	<u> </u>	<u></u>	/				
JE 65 1211	4				$\Theta$				<u> </u>					
1 - 05150	PROCESS GAS PRESS AT MOTLET OF EX	GAS FAN			ļ	<u> </u>			<u> </u>					
7 - 15151	PROCESS GAS TEAP AT OUTLET OF EX	GAS FA!		/	<u> </u>									
- <b>05</b> /52	HENESS GAS PRESS AT OUTLET OF DE	MISTER			<u> </u>	L		L	<u> </u>			<u> </u>		
1 - 05153	LPOLESS BAS TEAP AT OUTLET OF D	EMISTER			<b> </b>					<u> </u>				
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4.5 Civil Works

4.5.1 Description of Buildings

Buildings on the plant

- Office and control building, electrical rooms included
  - size L x B x H is<sub>3</sub>19 x 18 x 15 m
    i.e. about 5500 m<sup>3</sup>
  - number of floors 3
  - material of floors is concrete
  - outer and inner walls of bricks
  - mechanically ventilated
- Smelter building
  - size L  $x_3$ B x H is 35 x 24 x 38 m i.e. about
  - steel construction with steel or asbestos roofing
  - flash smelter furnace foundation as well as tapping floor are of concrete, other floors of steel structure.
- Power plant
  - size L x B x H is 36 x 25 x 18 m
    i.e. about 16 200 m
  - main part of the building is the steel framed and steel or asbestos plate roofed turbine generator aisle.

The floor is on the ground level made of concrete, as turbine generator foundations, too.

Necessary steel gratings and supports are included.

- the auxiliary part (about 2600 m<sup>3</sup> of total) consists of control and electrical rooms and offices.
  The walls of this part are built of bricks, floors are made of concrete.
- Compressed air station (compressor room)
  - size is about L  $\times$  B  $\times$  H = 12  $\times$  10  $\times$  6 m i.e. 720 m<sup>3</sup>
  - constructed of bricks for better noise absorption
  - concrete floor on the ground

### OUTOK

#### OUTOKUMPU ENGINEERING

A DIVISION OF OUTOKUMPU OY

- 5. Oxygen plant
  - area reservation for the plant is 40 x 30 m, concrete floored
  - the main part of process equipment is unprotected, only some critical items such as the compressor with motor are protected.
  - the office part on one side, approx. 1000 m<sup>3</sup>, is built of bricks. It includes control room, offices and other necessary covered rooms.
  - the total building volume of the oxygen plant is approx. 2500 m
- 6. Demineralized water plant
  - size B x L x H is 7 x 20 x 8 m i.e. 1120 m<sup>3</sup>
    steel frame construction with asbestos roofing
- 7. Lime stone slurry preparation plant
  - size L x B x H is 15 x 15 x 8 m i.e. about 1800 m<sup>3</sup>
  - steel frame construction with asbestos roofing
- 8. Lime storage
  - size appr. 5 x 5 x5 m i.e.  $125 \text{ m}^3$
  - steel frame construction with asbestos roofing
- 9. Power receiving station

Electrical equipment is located in the power plant house or unprotected on field.

10. Other

In addition, rainroofs are built e.g. above concentrate and top shale day bins as well as coal mills.

Pipe racks are covered, too.

Excavation

The ground on plant site will be levelled to the ground floor level of buildings before starting building works.

#### Foundations

Foundations will be made of concrete by casting on site. Machine and equipment foundations will be built separate from building frame foundations.

Big equipment foundations include roughly the following items:

- Concentrate and top shale day bins, multicoil steam dryers, flash smelting furnace, waste heat boiler, electrostatic precipitators, slag granulation basins and dust slurry thickener on flash smelter area
- Sulphur condensing, gas cooling boilers, hot and cold catalyzers, agglomerator/demister unit, sulphur condensing towers, incinerator, absorbtion tower, sulphur day tank and sulphur cooling tower on sulphur plant area
- Raw coal and pulverized dried coal bins and mills on coal plant area
- Superheater, turboalternator and auxiliary boiler in power plant
- Compressor with drive in oxygen plant
- Compressors with drives in compressed air station

#### Frame structures

The building frames are of steel consisting of supporting columns, beams and purlin structures on which the roofings will be fixed.

Steel supporting structures of machines and equipment are connected to the building or are independent steel structures.

The frame structures will be prefabricated in so big parts as possible for transportation and treatment. Frame columns will be erected onto foundations with cast anchor bolts.

Steel intermediate platforms, service platforms, stairs, equipment foundations, etc. will be erected before or after machine installations as necessary.

Generally approved tolerance requirements and instructions will be followed in manufacture and installation. Connections to be made on work site are mainly bolted connections; only truss diagonals and other steel parts which must be exactly installed will be fixed on site by welding.

All steel structures will be sand-blasted for rust removal and after that painted in accordance with a program to be prepared separately. Only the necessary finishing will be performed on installation site. All steel structures to be made on site will also be painted.

Walls

External walls will be of plastic coated, corrugated steel sheet or asbestos sheet fixed onto steel wall purlins with screws. The walls of offices can also be made of bricks.

The lower part of walls in the flash smelter building can be open.

Partition walls will mainly be of bricks.

Roof slabs

Roofs will be of plastic coated corrugated steel sheet which is fixed onto steel roof purlins with screws. Roofs in office and storage buildings can also be made of double corrugated asbestos cement sheet fixed onto purlins.

Rain water will be led from rain water gutters on eaves into rain water drains on the ground inside or outside the building.

Platforms

Part of platforms, like tapping platform of flash smelter, floors of control room, electric and office rooms will be of reinforced concrete platforms built on steel beams.

Other platforms will be of steel grating or steel plate built on steel frame.

Stairs will be steel framed. Steps of hot-dipped galvanized steel grating. Railings of painted steel pipes. Small outer stairs can also be made of reinforced concrete.

Outer windows in plant buildings will mainly be of colourless, plastic sheet, made according to the profile of wall corrugated sheet. Inner windows of polished plate glass. Office areas will be provided with double glass windows.

Outer doors in buildings and inner doors in plant and electric rooms will be manual steel doors. Inner doors in office rooms are wooden flush panel doors.

The floors resting on the ground will be made of concrete on a compact gravel layer. The surfaces will be finished in connection with the casting considering floor slopes.

The floors in offices and control room will be covered with asbestos vinyl tiles, and the floors in toilets with ceramic tiles. The floors in electric rooms will be painted.

Plasterworks and other finishings

The bottom of flash furnace overflow pond under the furnace and part of smelter tapping platforms will be covered with refractory bricks.

The walls in offices, wash rooms, control and electric rooms will be painted; wash rooms, etc. can also be covered with tiles. Other walls will generally be untreated.

Stairs

Windows

Doors

Floors

e

Ventilation

Natural ventilation will be used as general ventilation in the plant buildings. Compensation air will be taken through louvres provided with blocking device installed in walls, or the lower part of walls will be open (smelter building). The exhaust will be made by means of exhaust units on the roof. These exhaust units will be provided with wind protection and rain shelter.

The office and cotrol room building will be provided with mechanical ventilation. These areas will be kept in over-pressure compared to surrounding areas. Electric rooms will also be provided with mechanical ventilation and will be kept in over-pressure. Inlet air will be filtered.

Out-door tanks

The cooling water pump tanks will be made of water tight concrete.

4.5.2 Quantities of Concrete, Structural Steel, Coatings, Maintenance Platforms, etc.

In the following material quantities needed in plant erection are estimated.

The equipment areas and buildings the estimation covers are as follows:

- all the process plant area including drying plant, flash smelter, sulphur recovery and handling areas as well as gas purifying area
- office and control building
- oxygen plantpower plant
- compressed air station
- belt conveyors
- pipe racks

The following concrete equipment is not included, because it is concerned process equipment and included in the equipment list:

- concentrate and top shale day birs
- thickener, dia 30 m
- water tanks
- sulphur prilling tower
- slag granulation basins
  - main stack

#### Material amounts needed

_	concrete	6	900	m3
_	structural steel	1	500	t
_	building coatings	8	500	m2
_	brick walls	2	900	m2
	excavation		600	
_	filling		700	
_	maintenance platforms		600	
_	steel stairs	_		m
_	SCEET SCUITS			

4.6 WATER SUPPLY

Water supply to the plant is described in Chapter 4.7, Offsite Facilities, Faras 2 to 5, by FEDO FACT, and in the attached Water Main Flow Diagram No. 360 100 901 012-1.

Main flows and services are as follows (flow numbers refer to the diagram):

#### Flow no Description

- Filtered raw water from the river Sone at 2 km distance.
- 2. Filtered raw water from the surface water tank to different handling plants and consumption points.
- 3. Semi soft water, i.e. ion exchanged and part lly chemically treated water, to cooling circulation water system as make-up water.
- 4. Cooling circulation water (secondary cooling) to be used for:
  - secondary cooling of flash smelter furnace jacket cooling water circulation
  - oxygen plant cooling
  - turbine steam condenser and 1.7 bar boiler feed water cooler at power plant
  - make-up water for flash smelting furnace reaction shaft spray cooling
  - compressor cooling at compressed air station
  - sealing water for pumps all over the plant
- 5. Refur of the cooling water of item 4, above
- 6. Filtered raw water to overflow pump tank item 240-518-0100 in smelter
- 7. Filtered raw water return from:
  - smelter thickener, item 240-532-0100, overflow
  - sulphur plant absorption tower circulation

- 8. Tailing pond overflow circulation to absorption tower lime stone slurry mixing tank and scrubber inlet pipe in sulphur plant.
- Demineralized water to
  - power plant feed water tank
     smelter FSF jacket cooling (primary circulation) as make-up water
- 10. Blow-down water from boilers
- 11. Scrubber outlet water from sulphur plant to lime stone slurry preparation plant
- 12. Lime stone slurry to absorption tower in sulphur plant (5-6 % of solids)
- 13. Potable water to different consuming points

728000

### SULPHUR RECOVERY PLANT - 221250 TPA (OUTOKUMPU PROCESS)

#### OFFSITE FACILITIES

#### 1. LAND, LAND DEVELOPMENT ROADS AND DRAINS

The area required for the plant is about 10 hectres (25 acres). A barbed wire fencing is proposed around the plot. Eventhough land is almost a level ground, some development works are required to make it suitable for installation of the proposed plant. Further about 3 k.m. length of roads with drains are provided in the plant area.

#### 2. Water Supply System

It is proposed to draw necessary quantities of water (500 M<sup>3</sup>/hr.) for the plant from the nearby river - Sone river - which is about 2 k.m. away from the plant site. The facility will comprise of an intake well on the river bed, sand filtration system and pumps at the intake point. The water will be piped . (two lines - one sandby -) to the surface storage tank (10,000 M<sup>3</sup> capacity - about one days requirement) at the plant site. Water will be pumped to DM Water Plant, Water Softening Plant and other consuming points from the above surface tank.

#### 3. D.M. Water Plant

20 Tonnes per hour of D.M. water is required in the plant. A D.M. Plant of 480 M<sup>3</sup>/day is proposed. The D.M. plant consists of an activated carbon filter, ammonia exchanger, carbon exchanger and a mixed bed unit. There is a D.M. water storage of 200 M<sup>3</sup> in the D.M. Plant along with two numbers (1 + 1) D.M. Water pumps of required capacity for supply of D.M. water to the deaerators of the boilers. The plant is enclosed in an asbestos roofed building of 7 M x 20 M area.

#### 4. Water Softening Plant

A water softening plant is proposed to supply semisoft water. This is for make up of cooling tower besses losses (3% of Cooling Water circulation), gland leaks, evaporation losses in flash furnace area etc. The total requirement of semisoft water is estimated as 270 M<sup>3</sup>/hr. The plant consists of a sodium base exchange softener and associated facilities for regeneration along with a pump and a standby to supply semisoft water to cooling tower basins and to overhead water tank.

#### 5. Cooling Tower System

The requirement of circulating cooling water is 7900 M<sup>3</sup>/hr. A 10°C rise is expected for the return hot water. Cold water will be of 31°C which is the lowest attainable cooling water temperature in the plant location during summer months. A cooling tower station consisting of 4 cells is proposed. Cold water will be supplied to the consumer points by cold well pump (4+1). Hot well pumps (4+1) will be used for supplying hot water at the top of the cooling towers. Cooling water will be semi soft water and make up requirement will be met by the water softening plant. Distribution headers (1000 mm-diameter) are provided for supply/return of cooling water upto the individual consuming plants.

## 6. Fuel Oil Supply

The requirement of fuel oil is as follows :

- Light fuel oil : 1.30 TPD
- Heavy fuel oil : 40.00 TPD (LSHS)

each have

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Separate storage tanks of 10 days requirement each have been provided for both light fuel oil and heavy fuel oil (LSHS). The storage tank of light fuel is of 2.8 M dia and 3 metres height, while the tank for LSHS is  $\frac{9.5}{0.5}$  M dia and 9 M height. Steam heating coils

have been provided for LSHS tanks. Pumps for the unloading/supply of fuel oil are provided with the respective storages. (2+1) for heavy fuel oil and (1+1) for light fuel oil.

## 7. Sulphuric Acid Storage Tank

The requirement of sulphuric acid is 1.28 tonnes/day. A storage tank of 3 M diameter and 3.5 M height is proposed which will meet one month's requirement (40 tonnes). Pumps (1+1) have been provided for unloading sulphuric acid from tankers to the storage tank as well as to supply to the plant.

## 8. Pyrites Supply

No provision has been envisaged for storage, handling etc. of pyrites upto supply to theplant. The cost of storage, handling, supply to the plant is assumed to be covered in the transfer price of pyrites. No cost has been given for supply of teh Shale

Outokumpu 9.

Smeller 578 206 Coal Supply The requirement of coal is 550 TPD (478 TPD in smaller The coal will be plant and 72 TPD in power plant). stored in an open yard, with fencing 70 H x 38 H (located near the railway siding) which will be sufficient to store coal of 15 days' requirement. Coal is transported to A wagon tippler cum conveyor site by rail wagons. system is provided for transferzing the coal to the Coal will be delivered to the coal feed storage yard. hopper of the battery limit plant by means of a pay loader.

### 10. Lime Stone Storage and Slurry preparation

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The daily requirement of lime stone is 225 tonnes and it is to be supplied in the slurry form to the plant. One day's open storage is envisaged for lime stone; 150 M<sup>2</sup> per area is provided in this regard. Lime stone will be transported from the nearby quarry (about 100 M eway) to the storage yard by means of dumpers. A front end loader will transfer the lime stone from the storage to a jaw crusher. From the jaw crusher, the material will be transferred by means of conveyors to a hammer mill and from there to wet grinding mill. The ground lime stone slurry from the mill will be fed to the mixing tank where further water will be added to make up the required consistency. The slurry will be pumped from the mixing tank to lime stone slurry feed pipe in the battery limits by means of the lime stone A lime stone grinding and slurry slurry pumps (1+1). preparation section is housed a 8 M high building 15 M x 15 M area.

#### 11. Lime Storage

Lime powder (1.1 tonnes per day) is to be supplied at the battery limit. 10 days' storage of bagged lime is envisaged. A building of 25 M<sup>2</sup> area with asbestos roofing is proposed for storing the lime.

#### 12. Power Receiving Station

It is assumed that the power will be made available at 110 KV by Bihar State Electricity Board at the power receiving station in the plant area. The power receiving sub-station will consist of the following equipment items :

- 110 KV Switchgear
- 40 MVA, 110/11KV Transformer
- 12 panel, 11 KV Board
- Capacitor banks for power factor unprovement
- Cabling, earthing, lighting of the substation
- battery and battery changer

provision will be there for exporting the captive power to the main grid of the electricity board. The substation will be housed in a RCC building of appropriate size.

Ontolen mil. 13.

## Sulphur Storage

228 000 The yearly production of sulphur is 221250 tonnes at 100% rated capacity of the plant. It is proposed to have a storage of about 1 month's production for the The product will be stored in open product sulphur. with a retaining wall around an area of 100 M x 50 M with concrete flooring has been provided for this purpose. 2 Conveyors of 40 M length have been provided in the battery limit plant for transporting product sulphur It is assumed that these outside the prilling section. conveyors can transport sulphur to the storage. another 80 M long conveyor is provided in the battery limit plant to transport sulphur upto the railway siding. This conveyor will be able to transfer the sulphur from Hence no additional storage to railway wagons. conveyors have been provided at sulphur storage area,

#### 14. Workshop

A well maintained repairshop is shorts already available at PPCL Amjhore, hence only a lumpsum provision has to be made towards some extra machines/facilities to the existing workshop.

## 15. Chemical Laboratory

It is assumed that the existing laboratory can be expanded to cater the needs of the sulphur plants also. Additional provision is made for this expansion.

#### 16. Wash and Change

Change rooms are provided in different areas of the plant for wash and change of operating personnel.

## 17. Material Handling - Pay Loaders

A total of 4 Payloaders have been provided for handling of lime stone, coal and product sulphur in the respective storage areas.

## 18. Transport Vehicles

2 Cars, and one Jeep have been provided. Requirement of transport trucks is expected to meet from the existing pool of trucks evailable in the mixing plant.

#### 19. Pire Fighting Equipment

A fire engine and associated accessories have been provided Fire hydrant points are provided at the critical areas like coal and sulphur storages and boiler plant.

## 20. Township

A total of 40 dwellings of everage 70 M<sup>2</sup> area have been additionally provided in the existing PPCL Township at Amphore for catering to the proposed sulphur plant.

Addition to FEDO-specification for offsite facilities

#### 21. Tailing Ponds

Two pieces of tailing ponds, each 200 x 225 x 3 m, are built on the plant site. The ponds are excavated in the ground and the surface is tightened with clay.

The two ponds can be utilized either separately or in series, depending e.g. on the annual season (rains) or need for emptying.

केवट इंजिनियरिय एष्ट विचाइन ओगनिसेषन FACT ENGINEERING AND DESIGN ORGANISATION Corrections agreed Ontokument in meeting in Ontokument office on 22-2: the July 85 office on 22-2: the July 85 petween PPCL/FEDO/Outokumpu

## Sulphur Recovery Plant for M/s PPCL - Off-site Facilities - Outokumpu's Process

#### Off-site Facilities

		(B. lakhs)
	<pre>1. Land, land development, )   rolds and drains )</pre>	15.00
	2. Water Supply System	153.02
	3. D.M. Water Plant	23.00
	4. Water Softening Plant	21.03
	5. Cooling tower system	<del>223.91</del> 173.91
	6. Puel oil supply system	9.47
	7. Sulphur(Acid Storage and Handling	1.40
	8. Pyrites supply system	-
	9. Coal supply system	55.00
	10. Limestone storage and slurry preparation	60.09
	11. Lime storage	0.50
	12. Power receiving station	154.22
	13. Sulphur storage	7.00
	14. Max Workshop	10.00
	15. Chemical laboratory	15.00
	16. Wash and change	2.00
	17. Material handling - pay-loaders	83.01
	18. Transport vehicles	5.00
	19. Fire fighting equipment	25.00
	20. Township	50.04
A.	TOTAL UPTO (1-20)	<del>913.69</del> 843.69
в.	ENGG., PROCUREMENT, PROJECT MANAGEMENT ) • 10% AND SITE MANAGEMENT )	91.37 86.37
c.	CONTINGENCIES • 5%	20:48 50 25 SS
	GRAND TOTAL (A+B+C)	1050.74 1055 3
	Tailing pond	75.00 1072.56
	Ex. D. (included in 2600e) 58.26 21.06	

## Operating Personnel (Off-sites)

Sl.	Particulars	No. of Persons	Remarks
<u> </u>		at relative	Nemal Va
1.	Water Supply System	4	(at river side)
2.	Water treatment, DM Plant, ) Cooling Tower etc. )	8	
3.	F. end loaders	24	(pay-loader)
4.	Wagon tippler operators	4	
5.	Slurry preparation section operators	8	
6.	Dumper operators	4	
7.	Electricians (Sub-station operation)	4	
8.	Sulphur storage area operator	CB 4	(Accommitting of sulphur export)
9.	General drivers	12	
10.	Off-site facilities	4	
	Total:	<del>-</del> 76	
		<del></del>	
	Maintenance Pe	ersonnel (Total for	main plant of Cossilier
1.	<b>Eitter</b> s	16	
2.	Riggers	16	
3.	Helpers	48	
4.	Machinists	8	
5.	Leadsmen	3	
6.	Electricians	8	
	Total:	99	

SULFUR RECOVERY	PROJECT	FROM AMTHORE	PYRITES (PPCL
Morse poure of			
	No	HP/unit	I Total HP
(" ) Lad oil pumps	2	50	5.0
(2) 4. fuel oil pumps	3	7.5	7.5
(3) lime stone conveyor		80	8.0
(4) Cooling town for	4	100 0	400.0
(5) tot well purios	4+1	200.0	800 0
(6) Cold well pumps	4+1	450 C	1800 0
(7) DN water pumps	1+1	<u>5 0</u>	5.0
(8) fellered water purplie)	1+1	200.0	200 0
(9) Softe 10 water puris	1+ 1	50 0	50 0
(10) Sufferer first fring	1+1	1.0	/ 0
(11) end prinding mell	<i>1</i>	200.0	200.0
(12) Juin Water fring at	a+1	3e0 0	200.0
(13) Van ouwher town out )		ಸಿ00 ೦	200 0
Story from the	POTAL		3876.5

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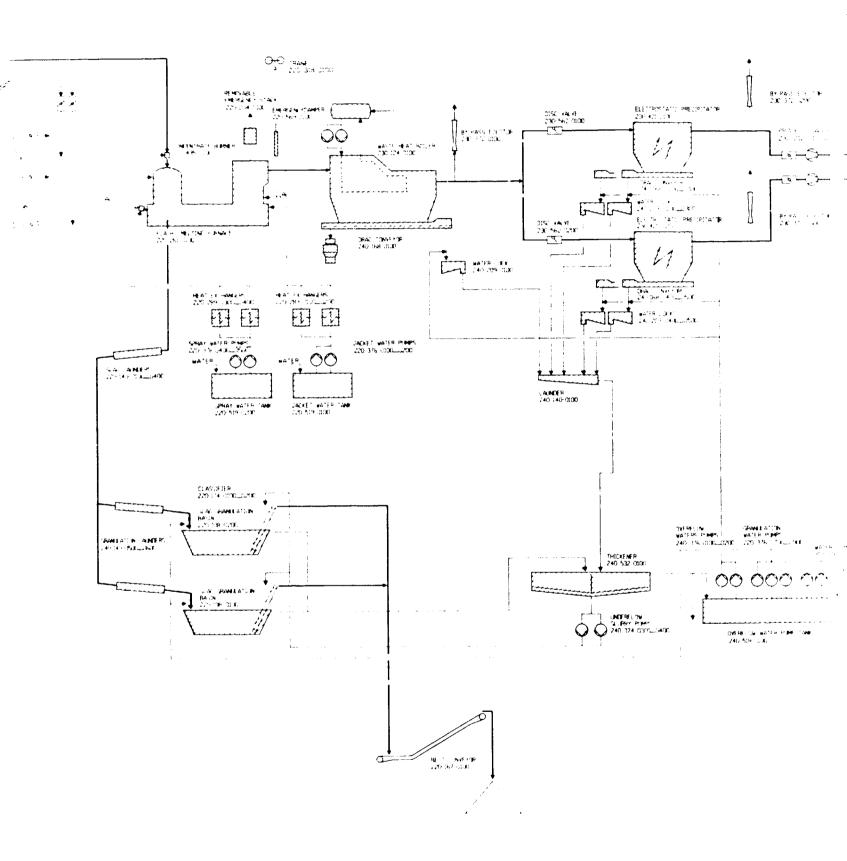
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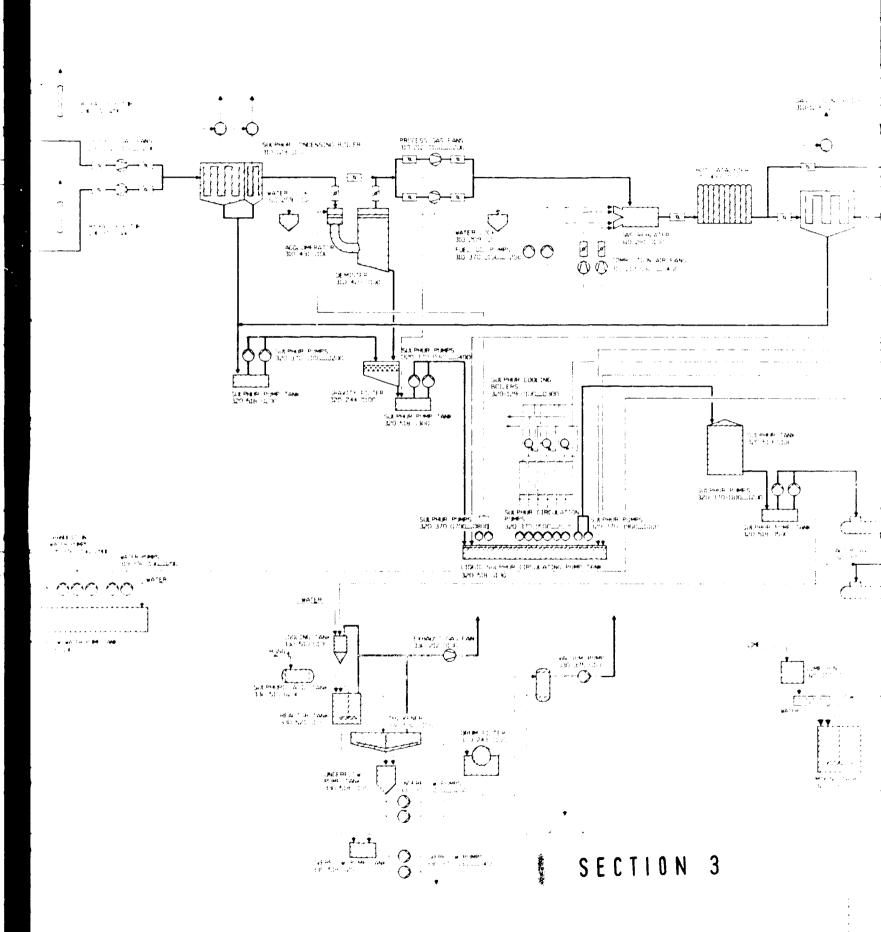
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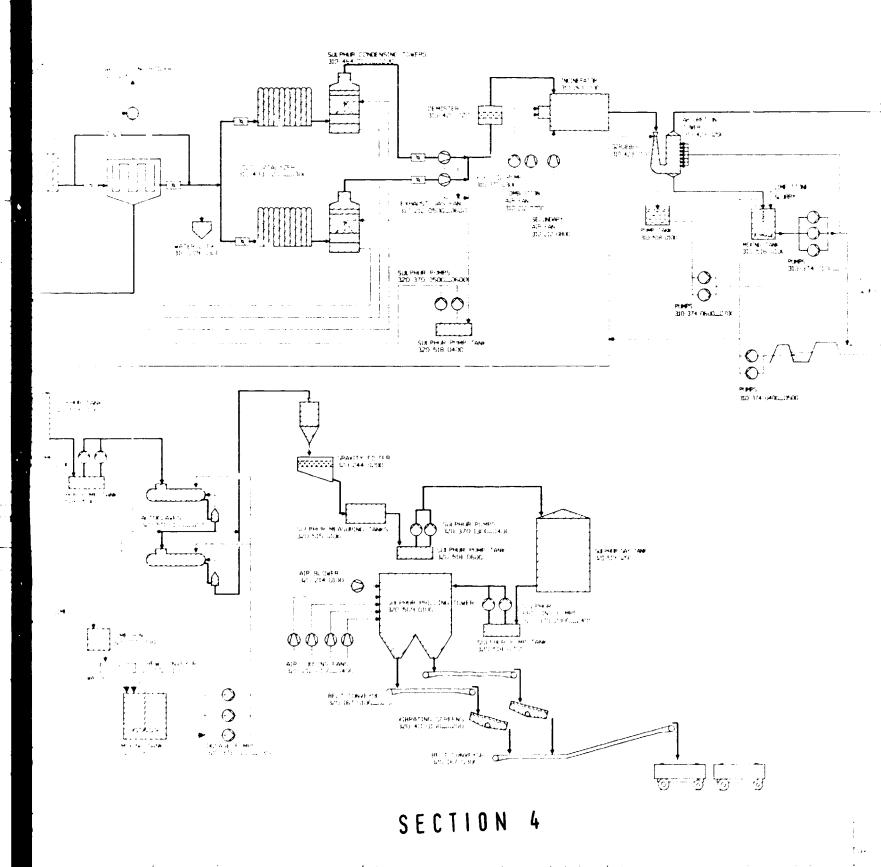
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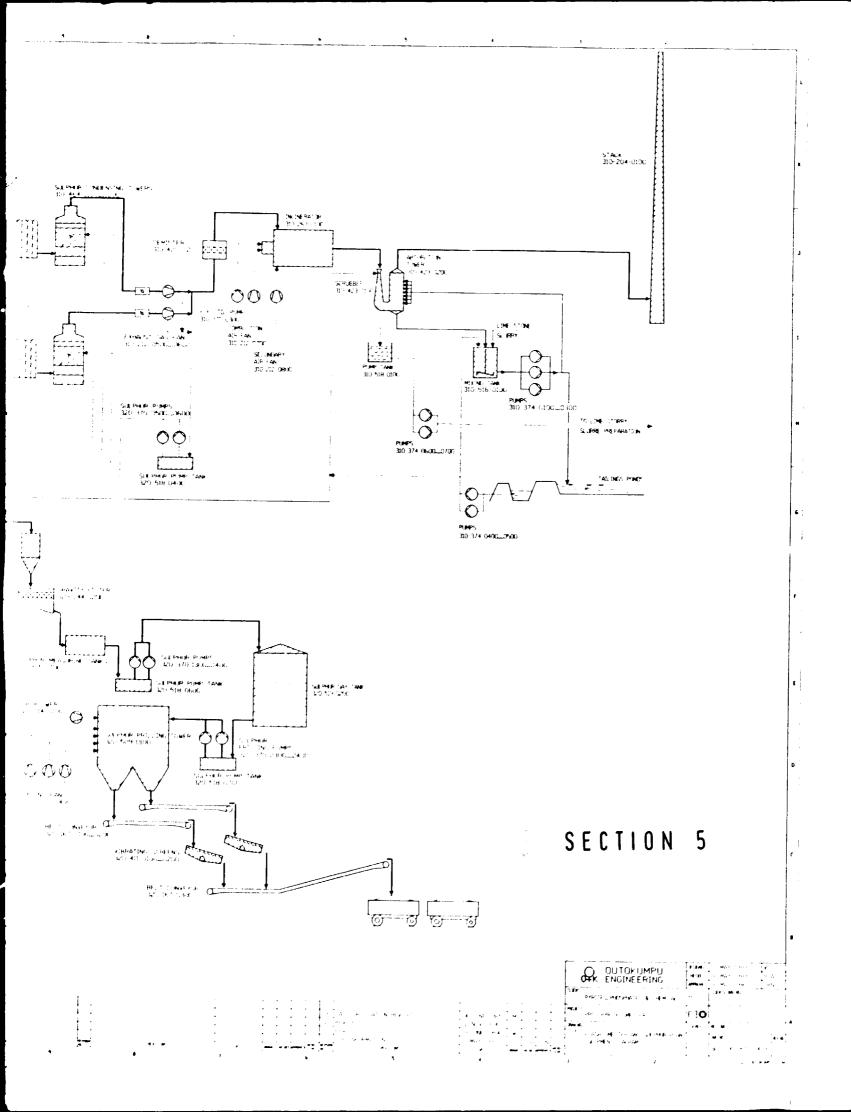
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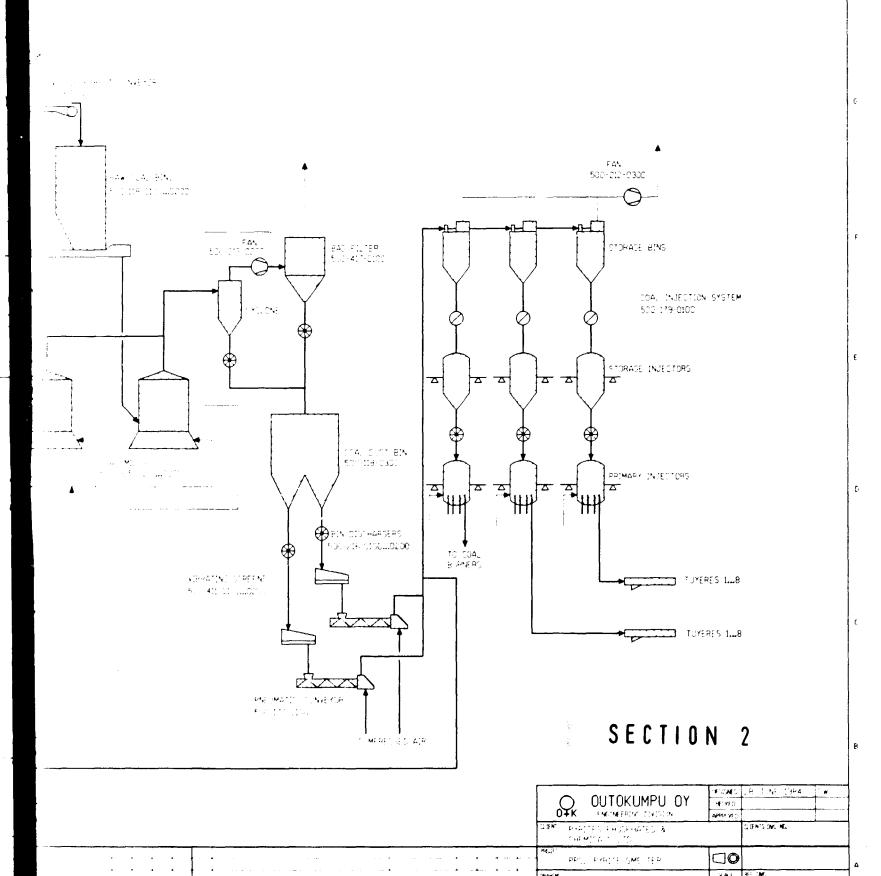
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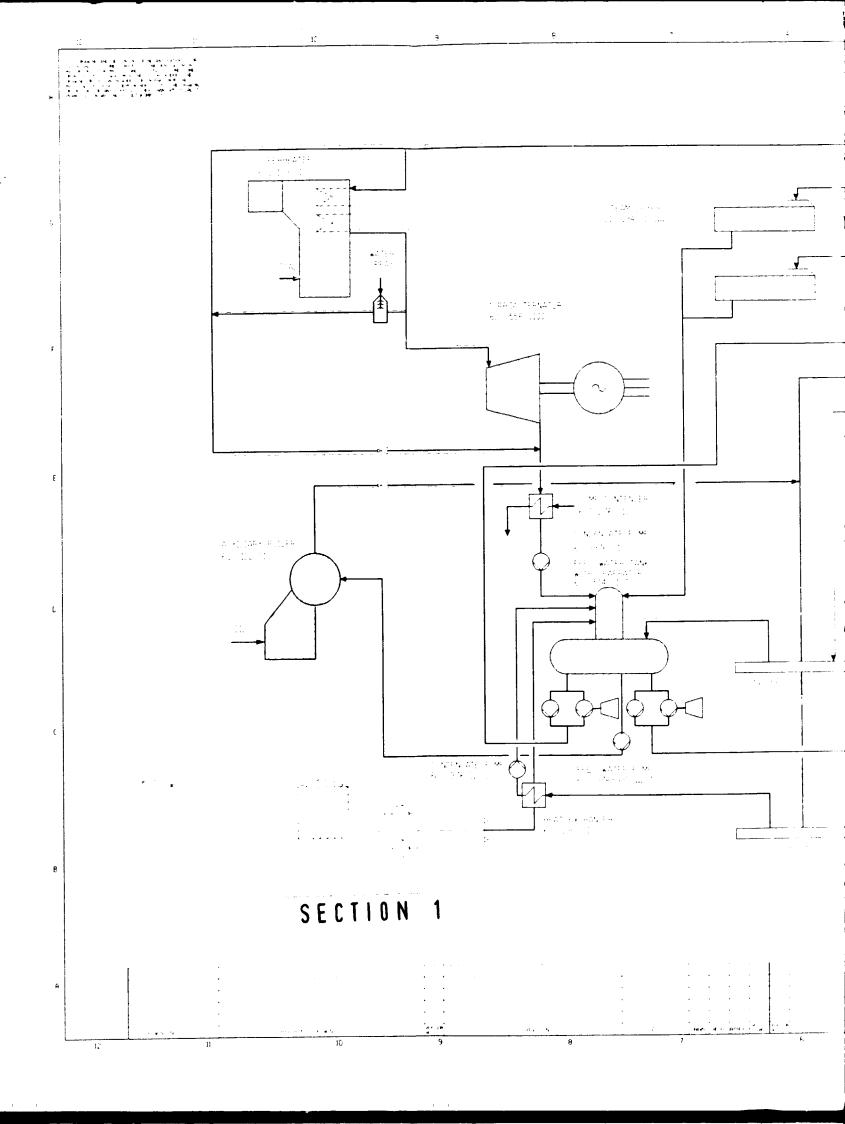
eff. Hibbéb 86.1 CONVEYOR 600-L67-0100 e 2 202,012 REVERSIBLE BELT CONVEYOR 535-167-0200 RAW COAL BINS 530 119 0100...0200 DRAD FEEDERS EDL 223-0100...0200 AIR E FAN 500-010-0104 010 808N68 500-138-00 1 | noal | Mil. | | | 500 | 305 | 0000 | | noon 0 500-212-0400 PREHEATER 500-281-0100 TOTAL PURMERS OF LUFERHEATER CTORAGE BIN 500 119-0400 VENZTA D  $S^{*}=41^{*}\ldots\ldots$ SECTION 1 COMPRESSED AIR PNE JMATES SONVEYOR 500 170 6206 .... 12 10

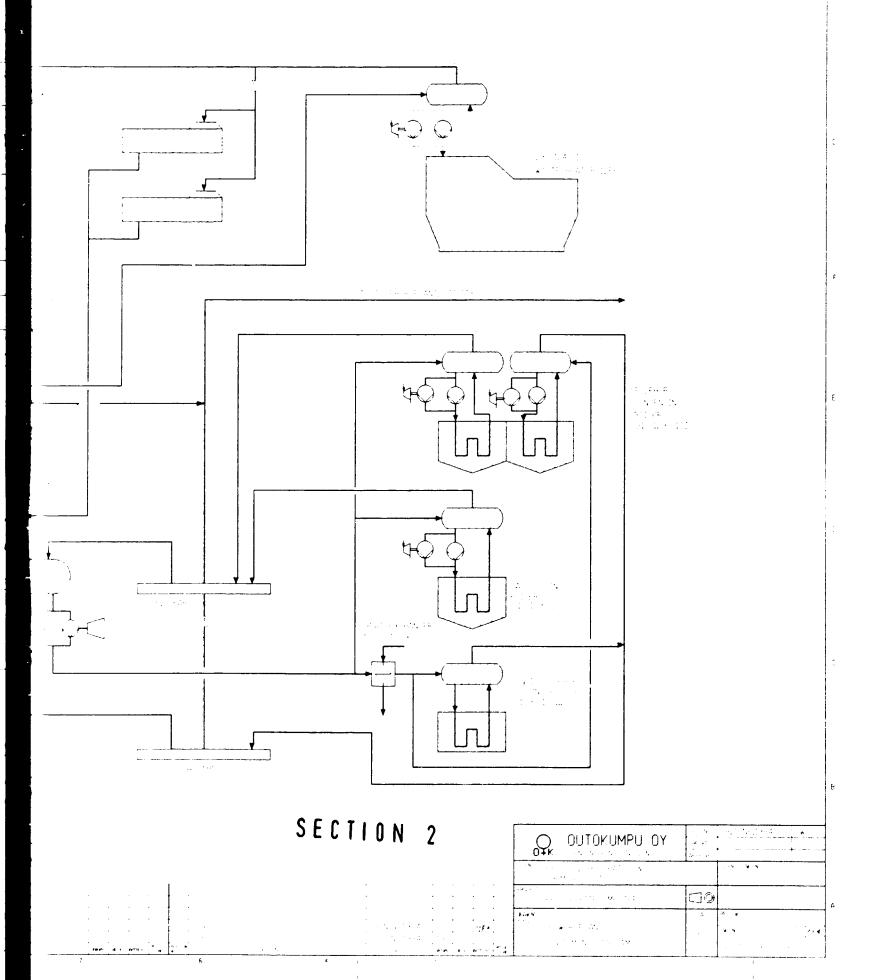


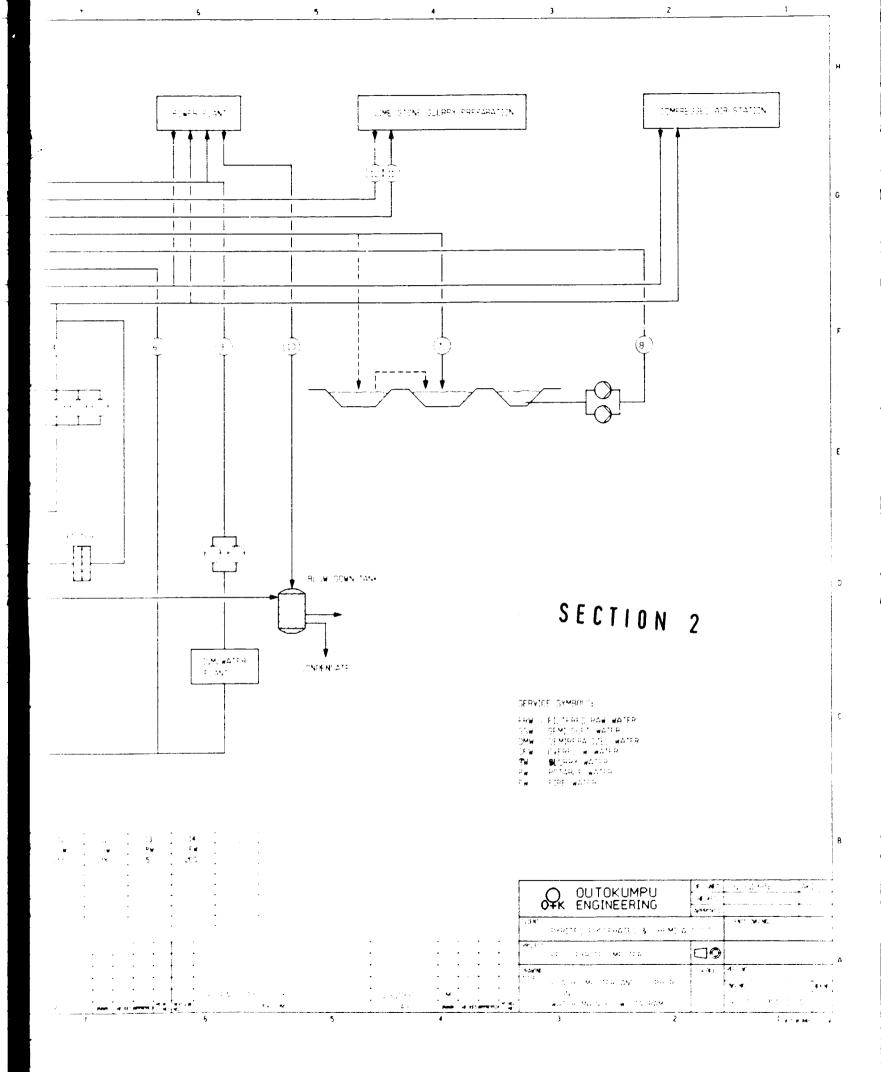
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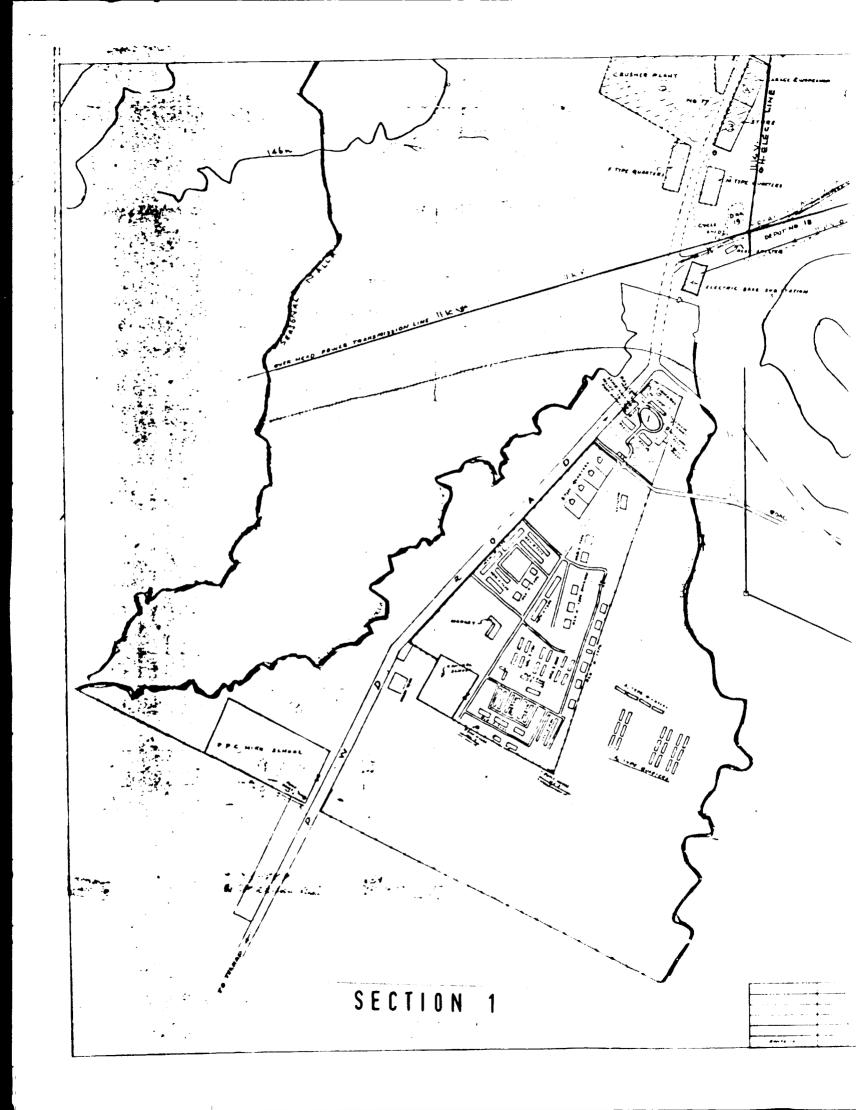
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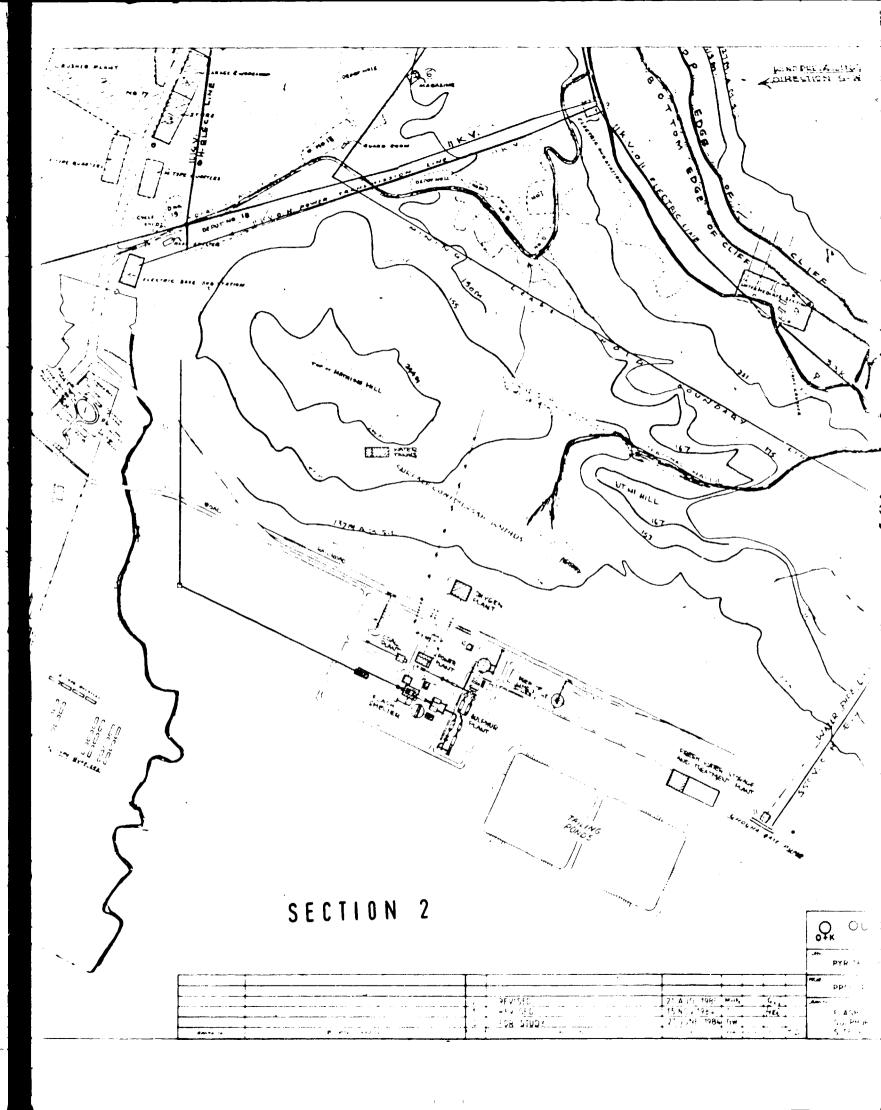
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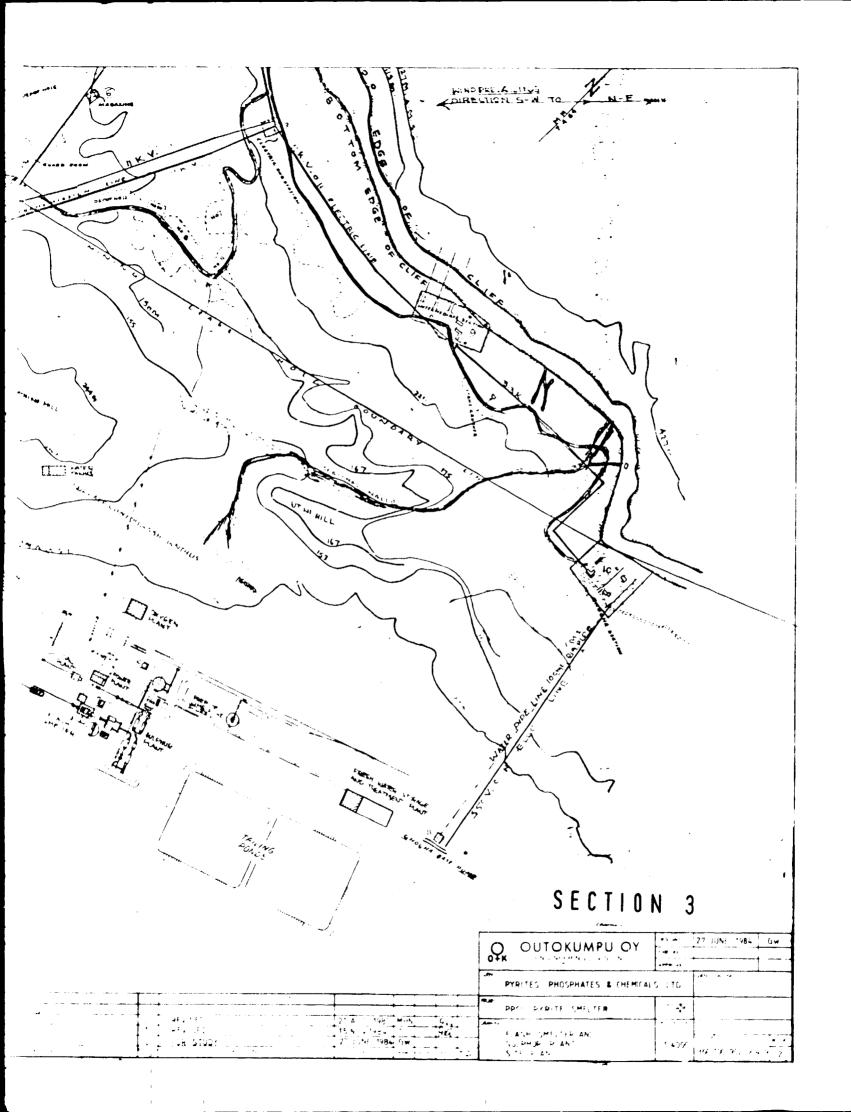


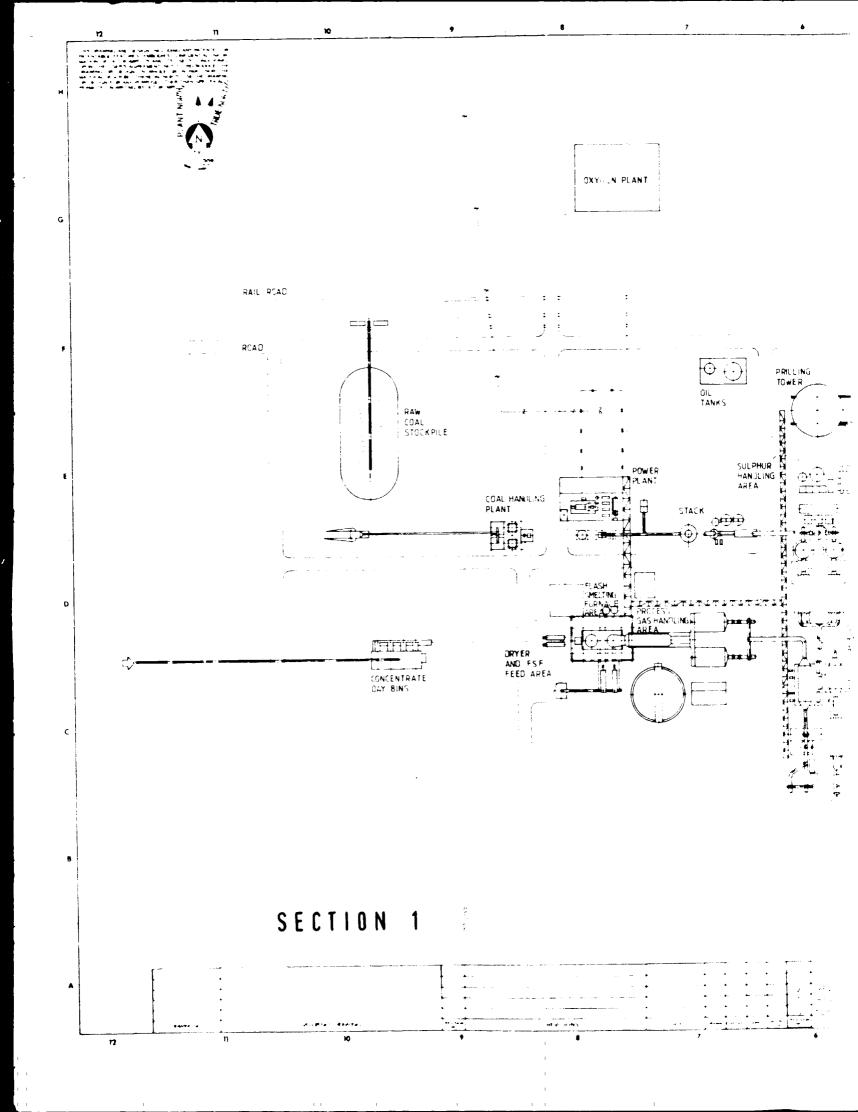


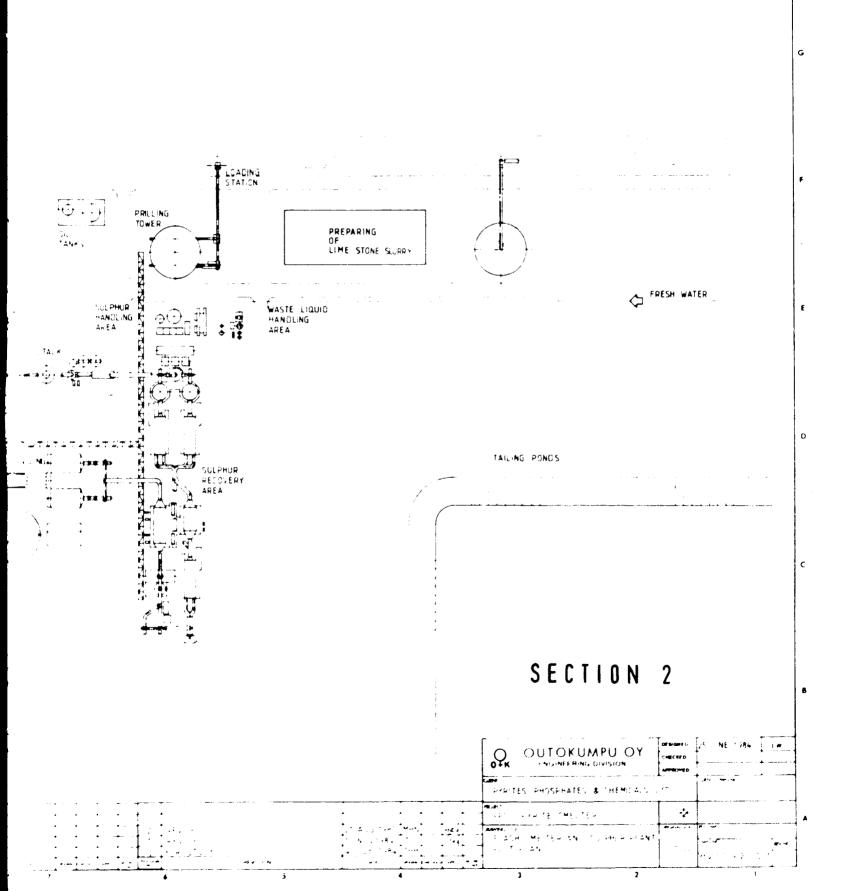


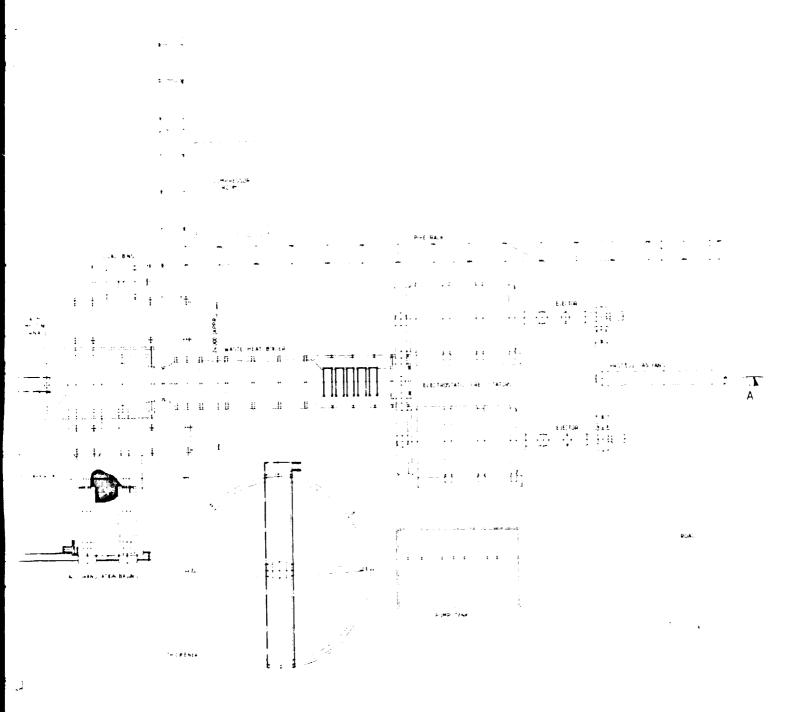




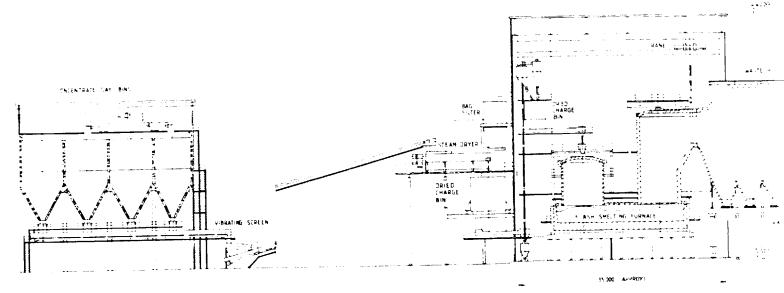




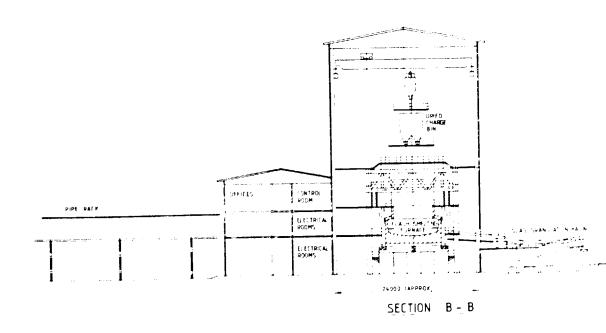




SECTION 2



SECTION A - A



SECTION 1

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ELECTROSTATIC PRECEPTATORS

ELECTROSTATIC PRECEPTATORS

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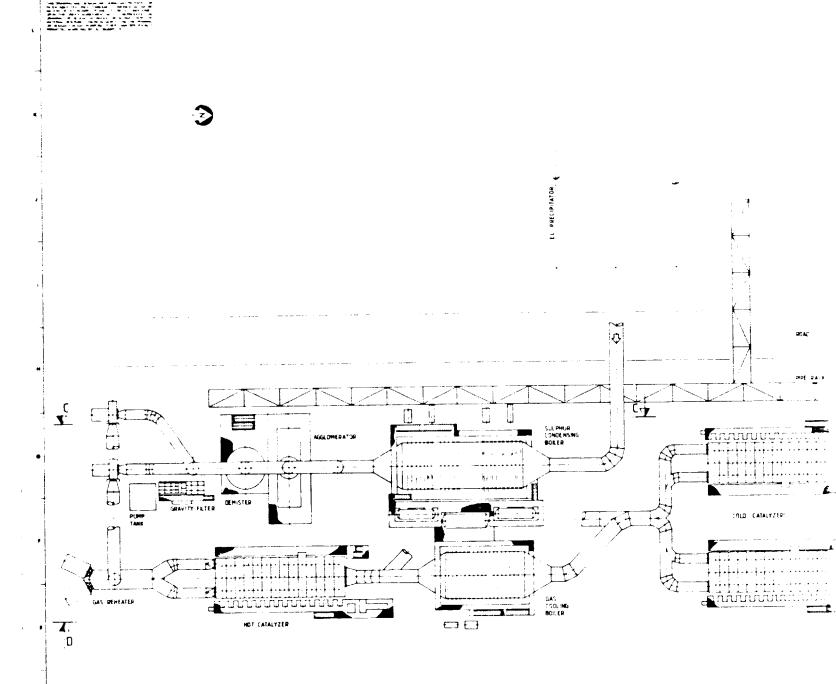
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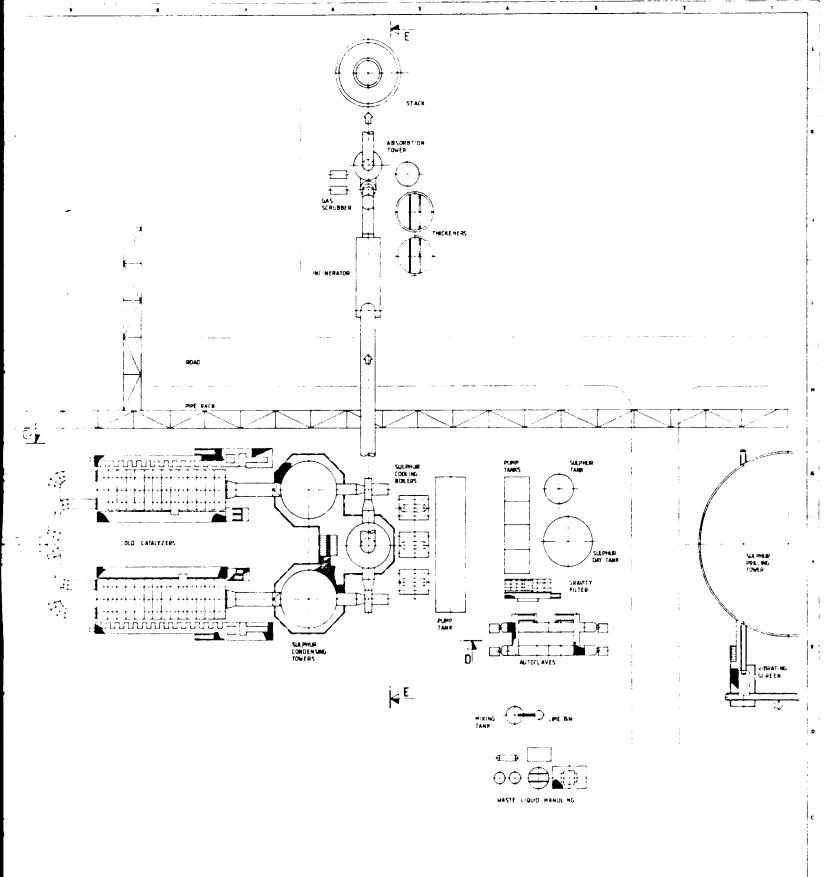
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SECTION 2

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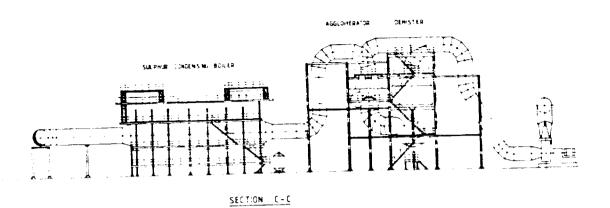
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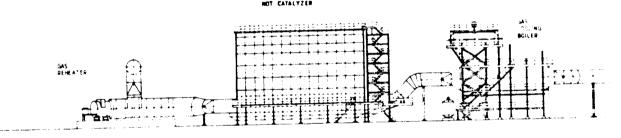




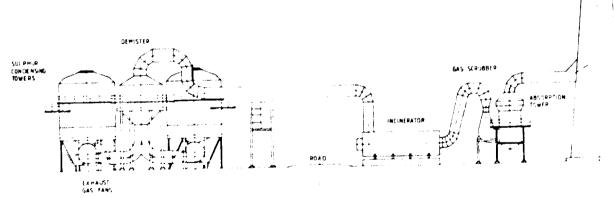
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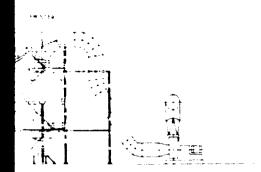


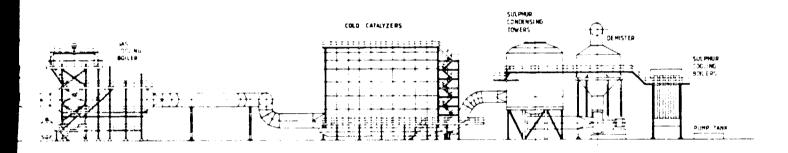


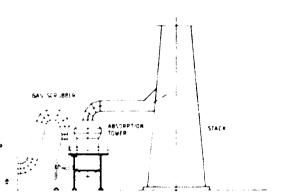
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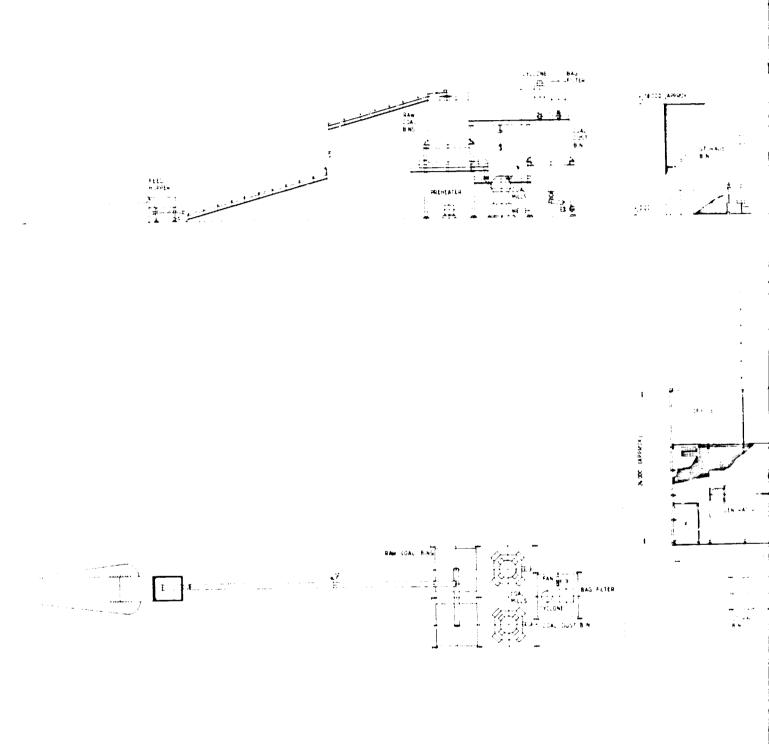
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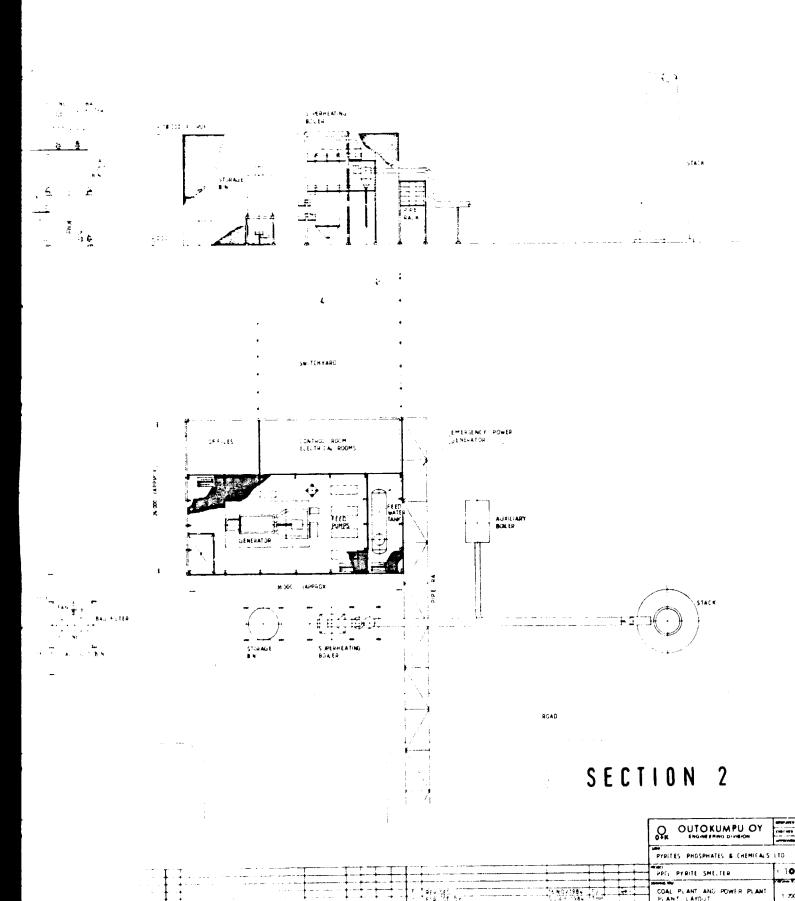


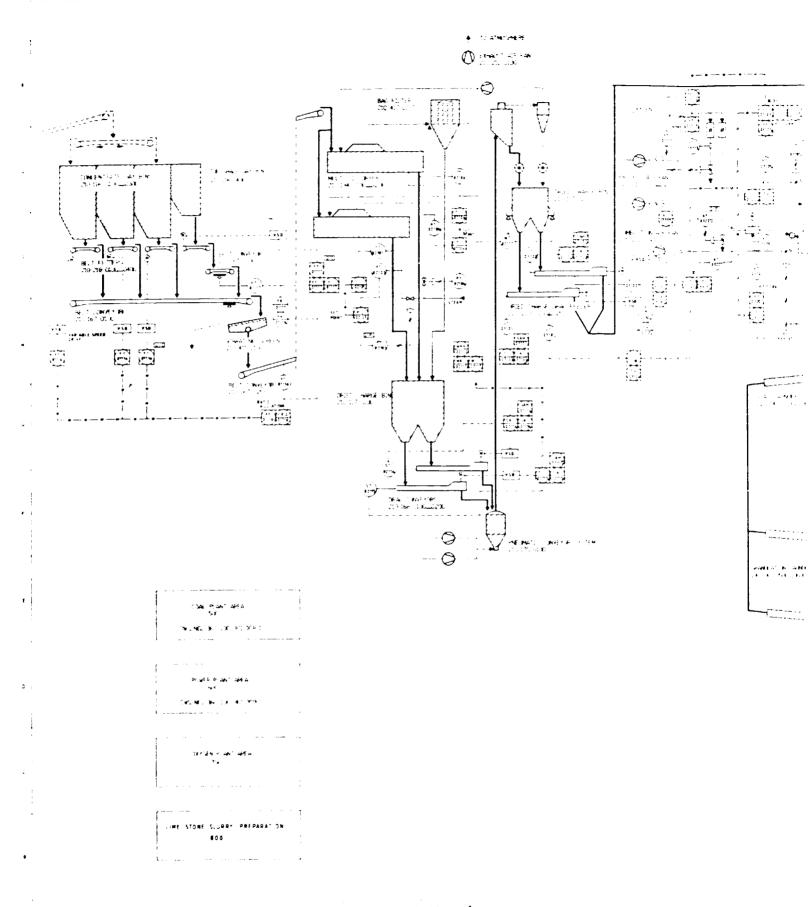


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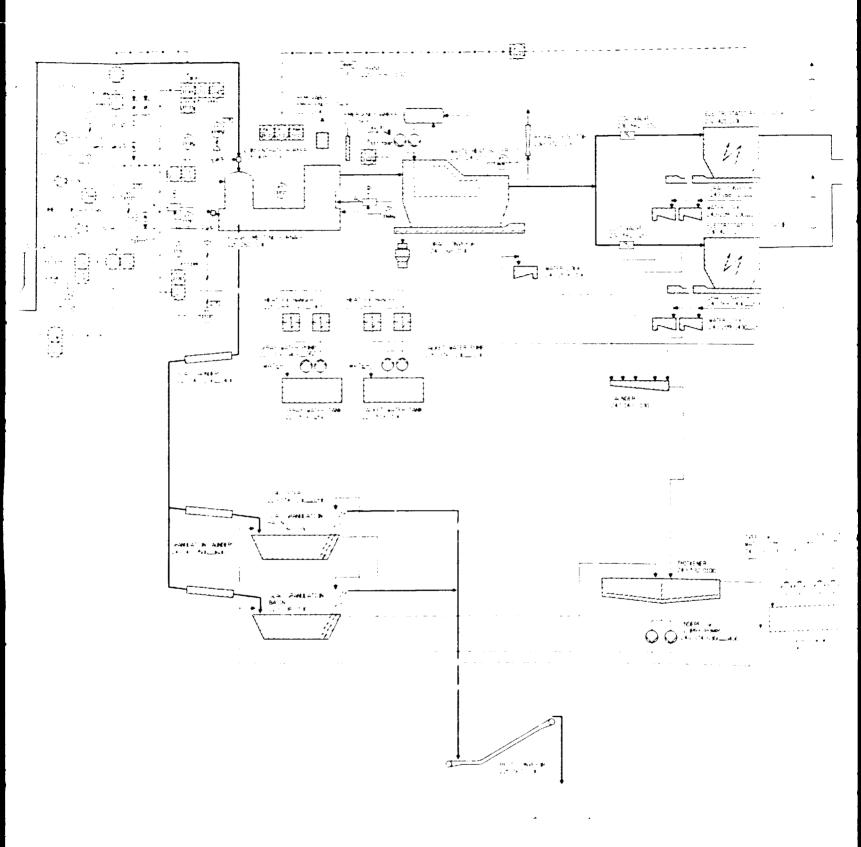


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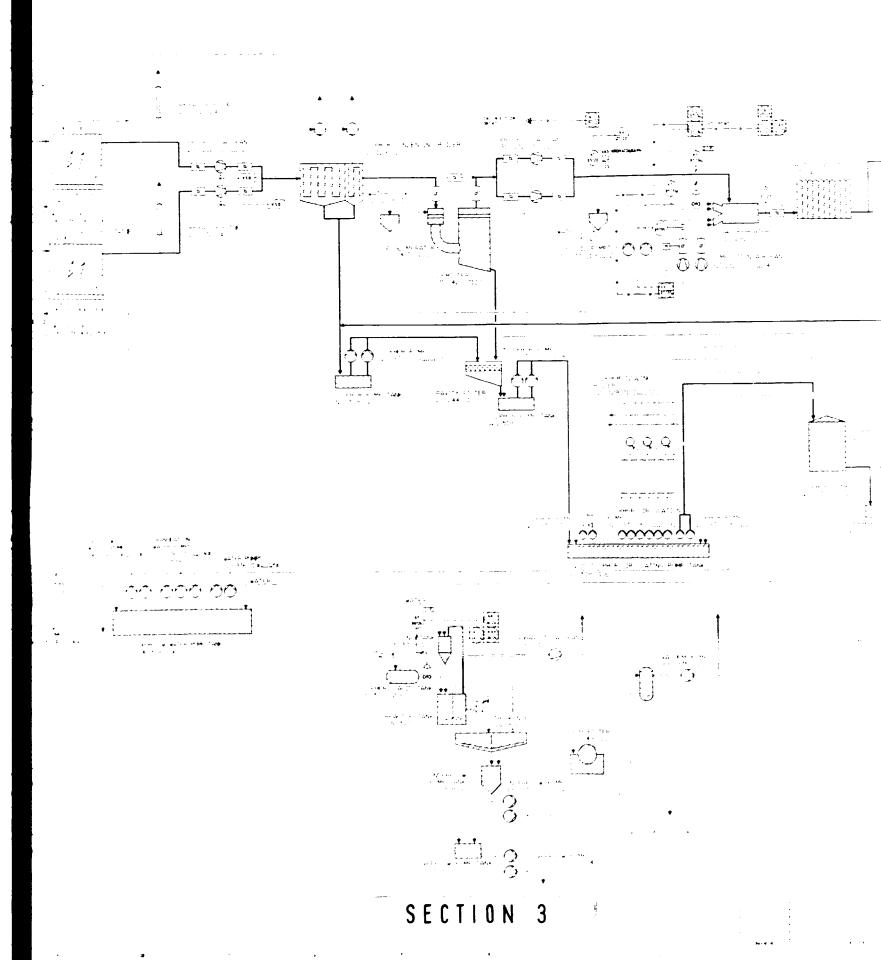


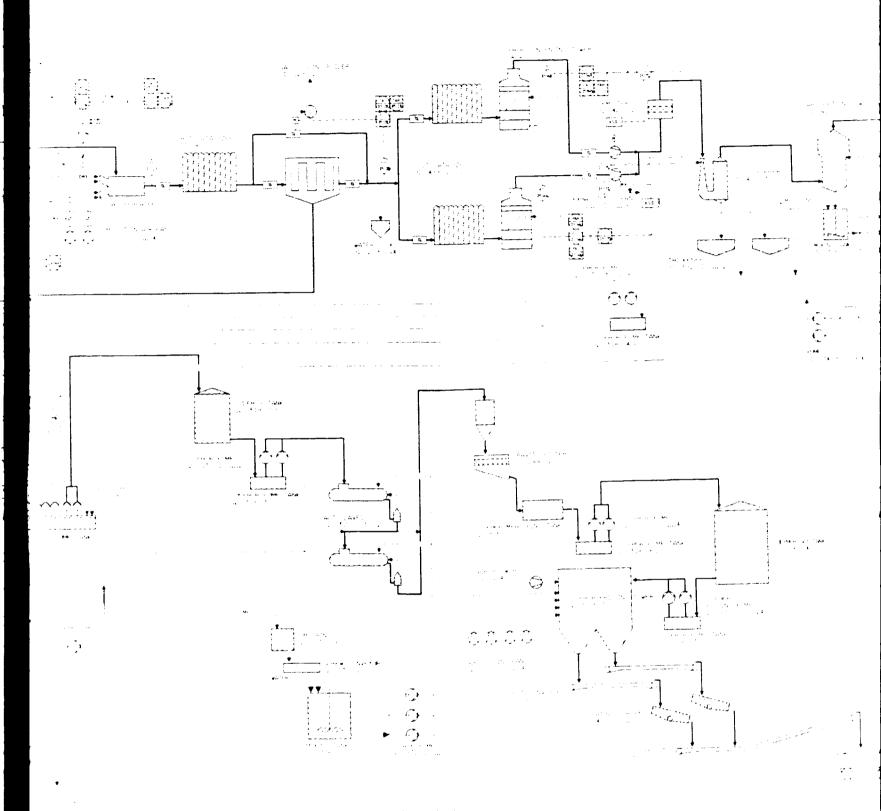


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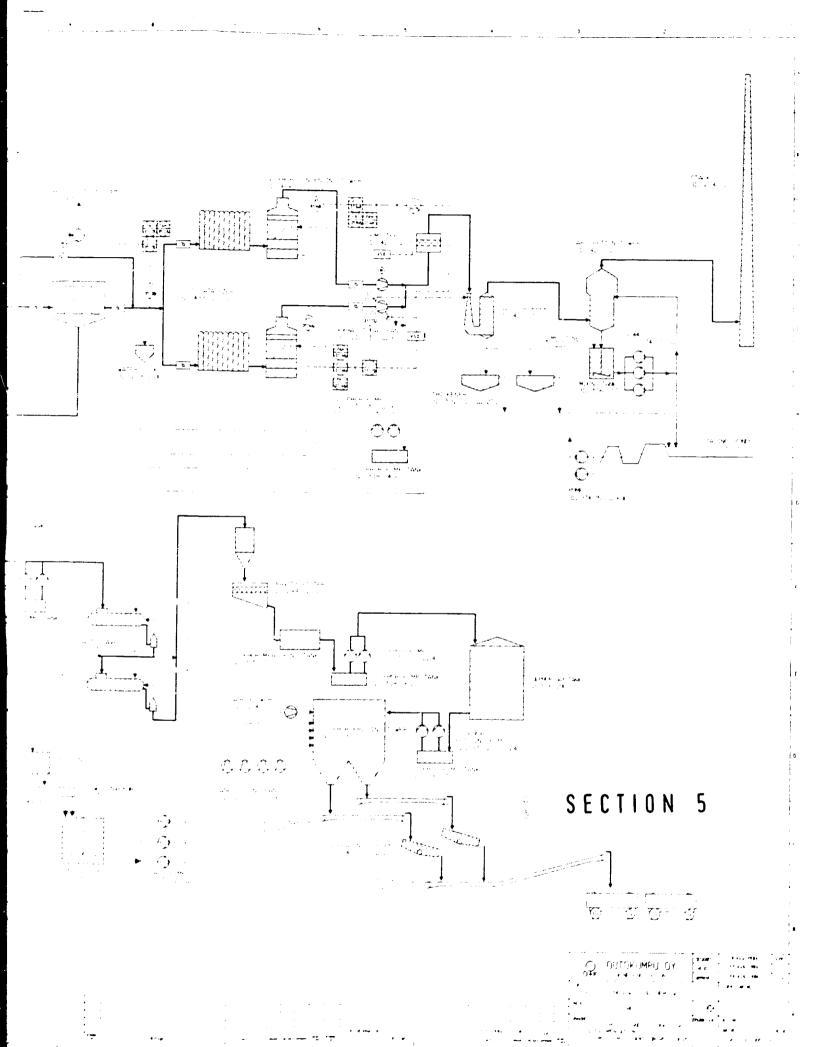


SECTION 2





SECTION 4



5 OPERATING DATA

- 5.1 Supervision and Labour Requirements
- 5.2 Requirements of Utilities and Consumables

5

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### O OUTOKUMPU ENGINEERING

5				
OPERATING DATA				
5.1				
Supervision and	Labour Requirements	3		
	Supervision and loperation are pre- laboratory persor evaluation because local situation.	sented belonel are not	w. Maint	tenance an
5.1.1				
Total Personnel	Plant manager Engineers Foremen Crew		1 6 27 70	
	TOTAL	2	04	
5.1.2 General Supervis:	ion			
	Technical manager Chief metallurgis Metallurgist	t	1 1 1	
	TOTAL		3	
_			3	
_			3	
_		Day shift		TOTAL
5.1.3 Smelter and Sulph	nur Plant Engineers	Day shift		_
_	nur Plant Engineers General foremen	1 1	Shift	TOTAL 1 1
_	nur Plant Engineers	_		1 1 11
_	nur Plant Engineers General foremen Foremen	1 1 3	Shift 8	1 1 11 13
Smelter and Sulph	nur Plant Engineers General foremen	1 1	Shift	1 1 11
Smelter and Sulph	nur Plant Engineers General foremen Foremen	1 1 3	Shift 8	1 1 11 13
Smelter and Sulph	Engineers General foremen Foremen Operating crew	1 1 3	Shift 8	1 1 11 13 88
Smelter and Sulph	Engineers General foremen Foremen Operating crew	1 1 3	Shift 8	1 1 11 13

Operating crew 8 44

# OTK A DIVISION OF OUTOKUMPU OY

_	-	_	_	_	
A D	IVISIO	N OF	ουτοκι	JMPU	OY

5.1.5 Oxygen Plant		Day shif	it Shift	TOTAL	
	Foremen	1		1	
	Operating crew	2	8	10	
5 1 <i>C</i>	operacing crew	2	0	10	
5.1.6 Material Transfer	(whole area)	Day shif	ft Shift	TOTAL	
	General foreman Foremen	1	4	1 5 6	
	Crew	8	12	20	
Note: 5.2 Requirement of Ut	Operating personn are described in ilities and Consum	Chapter 4	.7 by FEDO	fsite facilit	ies
5.2.1 Flash Smelting Ar	ea				
	Coal Electric energy Steam 20 bar, sat Filtered raw wate		t/a MWh/a t/a	158 000 24 000 150 000	
	(process water) Demineralized wat Refractory bricks Mortar for bricks	er	m3/a m3/a t/a t/a	160 000 30 000 300 25	
	Oxygen lances kg/a Tapping clay kg/a		8 000 6 000		
5.2.2 Sulphur Plant Are	Light fuel oil		t/a	400	
	Heavy fuel oil (B Electric energy Steam 5.5 bar, sa Filtered raw wate Lime Lime stone Sulphuric acid Catalyte mass Glass wool	turated	t/a MWh/a t/a m3/a t/a t/a t/a t/a t/a t/a m3	19 000 13 000 90 000 975 000 330 90 000 400 900 500	

### O+K A DIVISION OF OUTOKUMPU OY

5.2.3					
Power	Plant	Area	incl.	Coal	Plant

Operation time 7500 + 500 h/a

Coal	t/a	24	000
Heavy fuel oil	t/a	2	300
Electric energy	MWjh/a	10	500
Demineralized water	m3/a m3/a	112	000
Filtered raw water	m <sup>3</sup> /a	16	000

5.2.4 Oxygen Plant Area

Electric	energy	<b>MW</b> h/a	66	000
Filtered	raw water	m³/a	15	000

#### ECONOMIC SERVEY

- 3.1 Estimation of investment cost
- 8.2 Estimation of operating cost
- 5.3 Estimation of revenues
- 8.4 Profitability calculations

6

E. ECONOMIC SURVEY

C.: ESTIMATION OF CAPITAL COST

6.1.1 Basis of capital cost estimate

> Outokumpu Oy has evaluated the investment cost of the project within the agreed scope. Additionally, in order to get a view of the overall investment and profitability, Outokumpu's estimate is supplemented with the cost of off-site facilities.

The costs of off-site facilities are estimated by FEDO.

Scope of Outokumpu's estimates

The estimates cover the cost of required process facilities within the scope of work but infrastructures such as workshop, laboratory, site works, etc. are excluded from the scope.

The following areas are included in the estimates:

- pyrite drving
- flash smelting
- flash smelting furnace gas and dust handling
- elemental sulphur line
- sulphur purification and prilling
- oxygen plant
- coal handling
- auxiliary boiler and superheater
- turbine generator plant
- boiler feed water plant
  - compressed air plant

Terminal points of Outokumpu's estimates

The estimates are limited within the following terminal points

Pyrite: inlet to the dryer feed bins

Coal: inlet to the feed hopper

Bunker C oil: inlet to the day tame

Light fuel oil: inlet to the day tank

Slag and dust: outlet from belt conveyor of slag

granulation

lime: inlet to the lime feed bin

Limestone slurry: inlet to the feed pipe

Tailing of exhaust gas scrubber: outlet from the tailing pumps

Sulphur: outlet from the belt conveyors of priling tower

Process water: inlet to the plant area

Demineralized semisoft water: inlet to the plant

Secondary cooling water: inlet to the plant area outlet from the plant area

Electric energy: inlet/outlet at the main switchgear

Sulphuric acid: inlet to the feed tank

Tail gases: outlet from the main stack

Arsenic waster outlet from the arum filter

Scope of FEDO's estimates

FEDO has estimated the investment of the required off-site facilities:

- Land, land development, roads and drains
- Water supply system
- Demineralized water plant
- Water softening plant
- Cooling tower system
- Fuel oil supply

### O OUTOKUMPU ENGINEERING

- Sulhuric acid storage
- Pyrites supply
- Coal supply
- lime stone storage and slurry preparation
- Lime storage
- Power receiving station
- Sulphur storage
- Workshop
- Wash and change rooms
- Pay loaders
- Transport vehicles
- Fire fightning equipment
- Township facilities

Taxes and duties

Supplies of indigeneous origin:

An excise duty of 12% and a sales tax of 4% is added to the equipment cost of indigeneous origin. The value of excise duty is calculated on the basis of "Ex Work" price before transportation cost. The sales tax is calculated after adding the excise duty to the "Ex Work" price.

The freight, insurance and erection cost as well as the cost of buildings and civil work have been free on duties and taxes.

Custom duty of foreign supplies

A custom duty of 40% is added to the FOB cost of foreign equipment supplies and 25% for the forlegn engineering and commissioning work.

Price level

The estimates are based on the equipment cost of the first half of the year 1985.

The foreign supplies are estimated according to the European price level, based of Outokumpu's files from prevoius projects as well as on the contact to the equipment manufactures.

The Indian supplies are estimated according to Indian price level based on the cost estimates of FEDO and the information on unit prices received from PPCL.

When converting the foreign currencies to the Indian Rupees, the following rates of exchange have been used:

RS 1 = Finnish Marks 0.50

RS 1 = United States Dollars 0.077

RS 1 = Great Britain Pounds 0.064

#### Foreign Indian supplies

The fixed capital costs are divided into foreign and Indian portions.

The division of process equipment into foreign and Indian portions was in details discussed by PPCL and Outokumpu in the meeting in April 1984. This division is shown in the equipment lists.

Concerning the other items of fixed capital, Outokumpu has made the following assumptions:

- The basic and detail engineering will be partly foreign and partly Indian.
- Commissioning, supervision and training will be partly foreign, partly Indian.
- The process piping, process gas ducting, electrification and building constructions are of Indian origin. The investment is estimated according to the Indian price level as far as there has been available information of the local unit prices.
- 30 % of instrumentation and automation is assumed to be of Indian origin and 70 % European, the price level is according to the European conditions.

#### Working capital

The working capital includes the inventories of raw material, process and products as well as accounts payable and accounts receivable inventories.

A storage of one month in average is reserved for raw materials and supplies. A production of one month is calculated for process and product inventories.

The accounts receivable have been calculated according to one months production and accounts payable according to the purchases of one month.

6.1.2 Fixed capital, Rs 1000

Items	Basic pr FOR/FOR	ice	Freight A: Insurance:		s and dur
	Indian Supplies	Foreign supplies	:	Excise duty for Indian supplies 12 %	duty for foreign supplies 45 % (2)
Licence fee		5000	:		127
Basic engineering	2400	20200	:		<b>5</b> 0f
Detail engineering	9600	60600	:		151/
Commissioning, supervision of erection and start up, training of staff	7500	52800	:		132(
Equipment, foreign -smeiter -sulphur plant -power plant and coal treatmen -oxygen plant	n t	154960 64327 64363 124000	3216 : 3218 :	•	697: 2894 2896 5580
Equipment, Indian -air and gas ducting -others	16630 1 <b>7</b> 5703		931 : 9839 :		
Electrification	27788		1556 :	3335	
Piping and ducting	70000		3 <b>92</b> 0 :	8400	
Instrumerriation and automation	6706	22563	1504 :	805	1015
Spare parts	12751	21059	1691 :	1530	947
Erection and installation	104337		:		
Building constructions	46454		:		
Subtotal	<b>479</b> 869	589872	39824 :	37149	23772
Miscellaneous, 5 %	23993	29494	: 1991 :	: : 1857	1188
TOTAL COST INSIDE OUTOKUMPE'S SCOPE	503863	619366	41815 : :	39007	<b>2496</b> 0
OFF SITE FACILITIES, TURN KEY		(incl. fre		5826	
OVERALL INVESTMET	603187				24960

Overall investment witout duties and taxes

603187 619366 41815

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SECTION 1

	Freight A		s and duti	es	Cost	t at site	
ут. 1 ms	instrance	Excise duty for Indian supplies 12 %	Custom duty for foreign supplies 45 % (25%	Sales tax of Indian supplies ) 4 %	Indian <b>s</b> upplies	foreign supplies	Total
5000		:	1250		1250	5000	6250
6200		:	5050	96	7546	20200	27746
6600		; ;	15150	384	25134	60600	85734
2800		; ; ;	13200	300	21000	52800	73800
.4960	7748	: : :	69732		77480	154960	232440
4327 - 4363	$\frac{3216}{3218}$	: :	28947 28963		32164 32182	64327 64363	96491 96545
4000	6200	:	55800		62000	124000	186000
	931 9839	1996 21084		745 7871	: 20302 : 214498		20302 214498
	1556	3335		1245	33924		33924
	3920	: <b>840</b> 0		3136	85456		85456
2563	1504	: : 805	10153	300	19468	22563	42031
1059	1691	1530	9477	571	26020	21059	47080
		:			104337		104337
		:			46454		46454
9872	39824	37149	237723	14649	809214	589872	1399086
9494	1991	1857	11886	732	40461	29494	69954
9366	<b>;181</b> 5	39007	249609	15382	849675	619366	1469041
. fre	·	: 5826		2106			107256
93 <b>66</b>	41815	: 44833	249609	17488	: 956931	619366	1576297

3366 41815

603187 661181 1264368

SECTION 2

6.1.3 Working capital

Inventories: - Pyrite storage, one month, 52,000 t - Supplies, one month - Process and product inventories,	Rs 18,200,000 Rs 12,451,000	
variable operating cost of one month	Rs 31,774,000	
Accounts receivable, sales of one month ./.Accounts payable, operating cost of	Rs 51,934,000	
one month without wages and salaries	<u> Bs34,958,000</u>	
Total working capital	Rs 79,400,600	

5.1.4 Annual breakdown of the investment cost

The investment is annually divided into project years assuming that the implementation time will be four years.

Project	Years	Fixed capital Rs 1000	Working capital Rs 1000
1		102,157	
2		322,710	
3		710,384	
4		364,314	
4 5		46,733	37,548
6		<del>-</del>	39,814
7			2,038
Total		1,578,298	79,400

The breakdown of annual investment cost is shown in the table on the next page.

#### ANNUAL BREAK DOWN OF INVESTMENT COST Rs 1000

YEARS	1	2	3	4	5	TOTAL
iscence tee	6250					6250
mast engineering	27746					2774 b
Detail engineering	42867	42867				85734
<pre>/wmissioning, supervision of //rection and start up, training of stuff</pre>		1476	18450	29520	24354	73800
Equipment, foreign -smelter -sulphur plant -power plant and coal treatment oxygen plant		58110 24123 24136 46500	134815 55965 55996 107880	34866 14474 14482 27900	4649 1930 1931 3720	232440 96491 96545 186000
Equipment, Indian sair and gas ducting others		5076 53625	11775 124409	3045 321 <b>7</b> 5	406 4290	20302 214498
Electrification		3392	23747	6106	678	33924
Fiping and ducting		8546	59819	15382	1709	85456
instrumentation and automation		4203	29422	7566	841	42031
Spare parts				47080		47080
erection and installation			31301	73036		104337
Building costructions		4645	20904	20904		46454
subtotal	76863	276699	674483	326536	44508	1399088
Miscellaneous, 5 %	3843	13835	33724	16327	2225	69954
TOTAL COST INSIDE OUTOKUMPU'S SCOPE	80706	290533	708207	342862	46733	1469042
OFF-SITE FACILITIES, TURN KEY	21451	32177	32177	21451		107256
OVERALL INVESTMET	102157	322710	740384	264214	46733	1550000
OVERALL INVESTMENT WITHOUT DUTIES AND TAXES	85700	252543	583320	305842	36963	1264368

6.1.5

Financing of the investment

The financing plan is based on the discussions with the representatives of PPCI.

The initial investment will be financed with long term loan and equity. The other financing, required to balance the cash flow, will be supplied with short term loans.

The interests of the construction period as well as the 25 % of working capital will be calculated to the initial investment.

The portions of equity-long term loans will be 50 %/50 %. The equity will be paid totally first before drawing the loan.

The interest of the long term loans will be 13 %per annum, grace period two years and pay back time ten years.

The interest of short term loans will be 17.5 %.

It is assumed that the payment of the pay back and interests of long term loans will be at the end of the year.

The unnual financing schedule is shown on the next page.

FINANCING PLAN, Rs 1000

Year	-	21	27	<del>-</del>	ζ-	Total
Investment cost without interests 25% of working capital Interests of long term loan % 13	102157	322710	740384	364314	46733 19850	1576298 19850
fotal investment to be financed with equity long term loan	102157	322710	762605	437172	66583	1691227
long term loans drawing commission	<b>c</b> c	0 0	341859 341859	437172	66583 845613	845613 845613
Equator goda	291201	322710	120246	Ć	c	845613

ESTIMATION OF OPERATING COST

6.2.1 Basis of operating cost estimates

Scope and extent of estimates:

The operating cost are estimated according to the same scope and within the same terminal points as the investment cost litem 6.1.1.

Additionally, the operating cost of off-site facilities are separately estimated by FEDO.

The consumption figures of utilities and supplies are based on the process and plant design. The estimation of the amount of operating personnel as well as maintenance cost is based on the experience from Outokumpu's Kokkola pyrite smelter.

A miscellaneous cost of 5 % is estimated to cover the unspesified operating cost such as administration, purchasing, insurances and miscellaneous supplies.

Unit prices used in the estimates

The unit prices are partly based on the information received from PPCL partly on the European conditions.

- Wages and salaries including social cost:

	- managers	Нs	3,000	mont.
	- operating engineers	**	2,500	**
	- foremen	**	2,500	••
	- skilled tabour	**	1,800	••
	- helpers	••	1,200	••
-	Buncer C oil	Rs	0,1,1	ton
	light fuel oil	••	3,500	••
	coal	**	250	••
-	lime	**	600	••
	irmestone		3 ()	
_	refractory bricks	••	8,000	**
	mortar for bricks	••	5,000	**
	cast refractory		6,000	**
	exygen lances for	**	: ()	$\mathbf{h}_B$
	tapping			
-	tapping clay		2.000	T () [] (

### OUTOKUMPU ENGINEERING

OTK A DIVISION OF OUTOKUMPU OY

-	sulphuric acid	**	1,500	••
_	glass woo!	••	700	m.
-	fresh water	••	_	*1
	cooling water	**	_	••
	catalyze mass	••	5,500	••

The water supply cost is included in the power. chemicals etc. costs.

6.2.2 Haw muterials

> The transfer price of pyrite suiphur content 38% is Rs 350 ton.

No transfer price has been used for top shale.

Total pyrite feed per annum will be 625,000 tons which corresponds to an annual cost of Rs 218,750,000.

6.2.3 Annual operating cost

6.2.3.1 Variable cost

<u>Raw\_materials</u>

Rs 218,750,000

<u>Utilities\_and\_supplies</u>

Smelter:

	Annual consumption	Unit Price Rs	Annual cost Rs 1000/a	
*Coa}	158,000 t	250	39,500	
*Electric energy	24,000 MWh	produced in	the power plant	
*hefractory bricks	300 t	8000	2,400	
*Mortar for bricks	25 t	6000	150	
*Onygen lances	8,000 t	$ar{i}_i$	4 0	
*Tappang clay	6,000 t	2	1.2	
*Light fuel oil	400 t	3500	1,400	

## O+K A DIVISION OF OUTOKUMPU OY 6-12

	Annual consumption		Annual cost Rs 1000 a
Sulphur plant:			
*Heavy fuel oil Bunker C: *Electric energy *lime *Lime stone *Sulphuric acid *Catalyte mass *Glass wool		3141 produced in 600 30 1500 5500 700	the power plant 198 2,700 360 4,950
Power plant and coal treatment:			
*Coal *Heavy fuel oil * Electric energy	24,000 t 2,300 t 10,500 MWh	3141	30,000 7,224 the power plant
Oxygen plant			
*Electric energy	66,000 MWh	produced in	the power plant
Off-site facilities: *Slag/dust dumping *Electric energy	583,500 t 17,250 MWh		5,835 the power plant
Subtotal of utilities and s Miscellaneous 5 % Total utilities and supplie			Rs 154,798,000 a 7,740,000 a Rs 162,538,000 a
Total variable operating co	osts	į	Rs 381,288,000 a
6.2.3.2 Fixed operating cost		,	ks 10007a
Mages and salaries, main pi - plant manager (1) - engineers (6) - toremen (27) - operating crew (170)	Rs 3000 mo " 2500 " " 2500 "		36 186 810 3.672
Wages and salaries, off sit		nth	1,642
Wages and salaries, mainter - foremen (10 - skilled workers (5): - helpers (48)	mance   Es   2500/mo 	nth.	306 1,102 
Total wages and salaries			8,443

Spare parts and maintenance materials 36,000 subtotal 44,443 General and miscellaneous cost 5% 2,221 Total fixed operating cost Rs 46,654,000 a 

Variable operating cost with different capacities:

In the cash flow calculation the production rate of the first operating year is assumed to be 50 %. Also a cash flow with a capacity of 90 % is calculated.

The consumption of utilities does not directly follow the capacity rate. It is estimated that with a capacity of 50 % the utility cost will be 65 % of the cost of full production and with a capacity of 90 % the cost will be 93 % respectively.

b.3 ESTIMATION OF REVENUES

> Elemental sulphur and electric energy will be the products for sale.

Hs 2573 per ton has been the basic price of sulphur in the profitability calculations.

With the nominal capacity the electric power generation will be 7.5 MW higher than the consumption and this share is assumed to be sold. A price of hs 650/MWh is used as a sales price of electric energy.

The sales revenues with the nominal capacity:

\*Sulphur 228,000 t/a, Rs 2573/t, Rs 586,644,000 a \*Fl.energy 56,250 MWh/a, Rs 650/MWh, Rs 36,562,500 a

Total revenues

Rs 623,206,500 a

6.4 Prefirmbility calculations

6.4.1 General

The Internal Rate of Return of cash flow and equity as well as the pay back period has been used as a character of profitability.

In the estimation of annual cash flow the following bases have been used:

Income taxes:

No income taxes have been considered.

Calculation period:

Construction period: 4 years Operational period 15 years 19 years

Start-up of production:

The production rate of the first operating vear will be 50 %.

Salvage value of the investment: 5 % of fixed capital

Financing expenses:

The financing terms are as specified in item 6.1.5.

Calculation of pay back period:

The pay back period is calculated with a simplified method of dividing the total investment with the annual profit. The profit is sales revenues minus operating expenses and average interests of loams.

The profitability is calculated for four cases:

Case l: The plant will operate with the nominal capacity after the fifth project year, and the costs and revenues are as shown in items 6.1-6.3.

 $Sase_2$ : As case 1., but the production rate will be 90 %.

Case 3: The revenues are estimated with such a sulphur price that the internal rate of return of cash flow will result in 12 %.

Case 4: Calculation of "economic IRR". The investment and operating costs are without duties and taxes, it has been assumed, that the transfer price of pyrite as well as the other operating costs excluding wages and salaries, contains 5 % different taxes.

6.4.2Annual cash flow, internal rate of return and pay back period

> The cash flows, presented in appendices 6.1-6.4. give the following results:

	IRR of cash flow	IRR of equity	Pay back period
Case 1.	6.5 %	1.1 %	13.3 years
Case 2.	4.7 %	negative	48.5 years
Case 3.	12.0 %	10.8 %	6.4 years
Case 4.	10.5 %	8.8 %	7.2 years

In case 4, the IRR of cash flow of 12 % is resulted with a sulphur price of ks 3,010.40 per ton.

6.4.3 Sensitivity analysis

> The sensitivity analysis regarding the most important project variables indicates the following internal rate of return of cash flow:

	IRR of cash flow	IRR of equity
Fixed_investment:		
Rs 1,000,000,000	12.1 %	11.2 %
Rs 1,250,000,000	9.3 %	7.0 %
Rs 1,566,347,000	6.5 %	1.1 %
Fs 1,750,000,000	5.2%	-8-3-%
Fs 2,000,000,000	::.7 °	negative

	IRR of cash flow	IRR of equity
Frice of sulphur:		
Rs 2,573 per ton	6.5 %	1.1 %
" 2,600 "	6.9 %	2.4 %
" 2,700 "	¥.3 %	5.3 %
" 2.800 "	9.6 %	7.4 %
" 2.900 "	10.8 %	8.8 %
" 3.000 "	11.9 %	10.8 %
" 3.100 "	13.0 %	12.4 %
" 3.200 "	14.1 %	13.8 %
" 3.300 "	15.2 %	15.2 %
" 3.400 "	16.1 %	16.5 %
" 3.500 "	17.1 %	17.8 %
Total operating cost:		
Hs 350,000,000 a	11.4 %	10.2 %
Rs 400,000,000 a	8.2 %	5.3 %
ks 427,942,000 /a	6.5 %	1.1 %
Rs 445,000,000 a	5.4 %	-6.9 %

The results of the sensitivity analysis are graphically presented in appendices  $6.5 \cdot 6.7$  The test of Ash Flore, has come

der word sulphur 85 2,575 per ton

Production capacity 50 % during the 5th year and 100 % late.

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Visibilità dell'estare holdete.	102157	322710	420746	()	0	i .

INTERNAL RATE OF RETURN OF CASH FLOW (BEFORE FINANCING) INTIDNAL RATE OF RETURN OF EQUITY 1.1%

NET PROFIT FOR CALCULATION OF PAY BACK TIME.

623207 sales revenue per annum Production cost per annum 427942 Average interest per annum 76354

SECTION 1

118911 PAY BACK TIME 13.3 YEARS FROM THE START UP

or entitled % later on

<del>.</del>	٠,	7	;	4	10	i I	, , ,	13	i 1	
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· 4501	84561	84561	84561	84561	84561	84561	84561	84561	84561	
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, A. J. C.	38270	47326	51179	53467	54085	52714	48972	12 103	32467	
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BEFORE FINANCING EXPENDED: 6.5%

SECTION 2

THE START UP

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SECTION 3

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Series of Sulphur Rs 2, 75 per ton-

Production capacity 50 % during the 5th year and 90 % lates.

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Note that the property					287160	5413.4
e speraturi ost					215025	v 1200 (y ta
e e en et per et per terret et le c					17910	1:00
and the contract of the contract of					16664	Fritois I
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entre transfer of the control of the					375 (8	32250
se speat cost without interests	102157	322710	740384	364314	16733	
to the transfer of the second	102157	322710	740381	364314	10881	125176
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rt term looms tender tund) = tve end of vest terms	() () ()	() () ()	() ()	() ()	180232 180231 18770	08107 278580 40430
essa, two requerements	102157	3227+0	420746	()		
the analysis for whare holders	102157	322710	420716	()	()	t.

INTERNAL RATE OF RETURN OF CASH FLOW BEFORE FINANCING.
INTERNAL RATE OF RETURN OF EQUITY NEGATIVE

NET PROFIT FOR CALCULATION OF PAY BACK LIMES.

Sales revenue per annum 560886 Production cost per annum 394689 Average interest per annum 433724

SECTION 1

PAY BACK TIME 48.5 YEARS FROM THE START IF

	Later on
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	100.5	18035	348035	348035	348035	348035	348035	348035	348035	3.4900
	1 11 1						44.751	46654	46654	<b>.</b>
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	1 70 1 (1 0 1   0 1 03 (3) 7	591930 81561 87944	507368 21561 76961	422807 81561 65958	338246 81561 54965	253684 (41561 43972	169123 84561 32979	81561 81561 21986	6 84561 10333	
	031 57 278 589 30 529	62089 340478 54151	60163 400641 64848	59654 460295 75332	59048 519343 85718	58325 577667 95988	57463 635130 106120	56436 691567 116086	55213 746779 125855	70% 20%
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BE FINANCING EXPENCES: 4.7

SECTION 2

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348035	348035	348035	348035	348035	348035	348035	348035	. (803.)	
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SECTION 3

PROJECT CASH FLOW, Rs 1000

Price of sulphur Rs 3,010.40 per ton

Production capacity 50 % during the 5th year and 100 % late

. 0.41	ı	1.1		ı	5	P <sub>if</sub>
Sect of exemp					332869	694333
A driver to operating cost					215025	381288
change in product inventories					17919	10850
auxed a ending cost					46654	16654
Atomo mengan	()	0	0	0	89109	280251
working capital					41357	43963
anvestment cost without interests	102157	322710	740384	364314	46733	
Annual cash flow before timencing cost	102157	322710	740381	361314	1019	236283
one term forms drawing bund drawe end of very pay from	0	<b>()</b>	340857 340857	137033 777890	68660 761895 84655	677240 84686
interest \$ 13	0	U	22156	72719	105589	99046
don't term foans tamee cumulative end of year interest \$17.5	() ()	0 0 0	() () ()	() () ()	132125 132125 11561	32285 99840 20297
rquity requirements	102157	322710	421683	0		
Available for share holders	102157	322710	421683	U	()	()

INTERNAL RATE OF RETURN OF CASH FLOW (BEFORE FINANCING INTERNAL RATE OF RETURN OF EQUITY 10.8%

NET PROFIT FOR CALCULATION OF PAY BACK TIME:
Sales revenue for addim 722036

Sales revenue per annum 722936 Production cost per annum 427942 Average interest per annum 13086

PAY BACK TIME

245908 6.4 YEARS FROM THE STARL UP

SECTION

#### sear and 100 % later on

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		722936	722956	722936	722936	<b>7</b> 22936	722936	722936	7229%
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B BEFORE FINANCING EXPENCES 12.0%

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SECIION 2

245908 ⊙M THE START UP

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. 10 \$ 10 + 4	. 16 \$ 1816 \$	244444	2544 <b>535</b> 44	20 <b>9 3</b> 0404 5	, 4444£	41000	• •	
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### § SECTION 3

SHOUFET CASH FLOW, Rs 1000 (CALCULATION OF ECONOMIC INTERNAL RATE OF RETURN)

The investment and operating costs are witouth duties and to

Price of sulphur Rs 2,573 per ton

Production capacity 50 % during the 5th year and 100 % late

ir or	i	2	3	-1	5	6
Not revenue					287160	598764
. irrable operating cost					204273	362223
change in product inventories					17023	13162
rixed operating cost					44743	44713
caross margin	()	0	0	0	55167	204960.
working capital					36461	38850
Investment cost without interests	85700	252543	583320	305842	36963	
Annual cash flow before	85700	252543	583320	-305842	18257	166110
cong term loans  drawing  cumulative end of year;  pay back	0	0 0	259474 259474 16866	363180 622654 57338	56300 611059 67895 84605	543163 67895 79438
Interest  Intere	0	0	0	0 1	125432 125433	3478 128911
interest	0	0	0	0	10975	22256
Equity requirements	н <b>57</b> 00	252543	340712	. 0		
Available for share holders	85700	252543	340712	0	0	()

INTERNAL RATE OF RETURN OF CASH FLOW (BEFORE FINANCES INTERNAL RATE OF RETURN OF EQUITY 8.8%

SECTION 1

NET PROFIT FOR CALCULATION OF PAY BACK TIME:
Sales revenue per annum 623207
Production cost per annum 406966
Average interest per annum 40858

175383

PAY BACK TIME 7.2 YEARS FROM THE START BP

fURN: touth duties and taxes

year and 100 % later on

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	17023	13162			44743	44743	44743	44743	44743	441
	14743	44743	44743	44743	44740			216241	216241	216.
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r 4.7	18257	166110	214204	216241	216241	216241	216241	210241		
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FLOW BEFORE FINANCING EXPENCES) 10.5% Y 8.8%

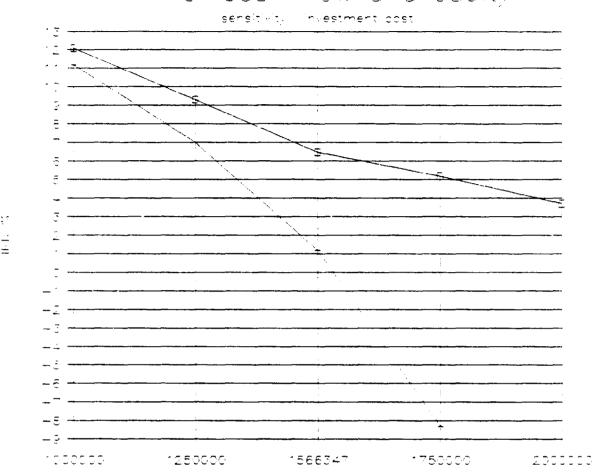
SECTION 2

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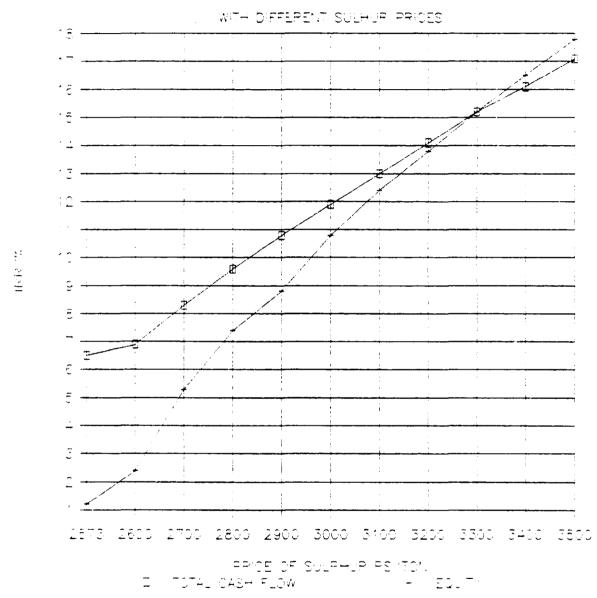
SECTION 3



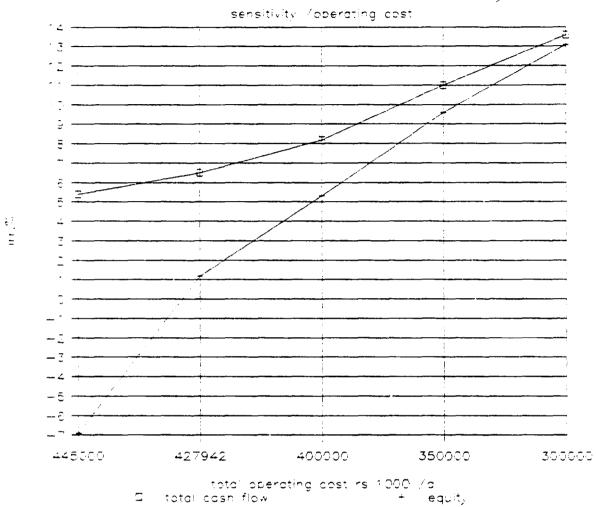


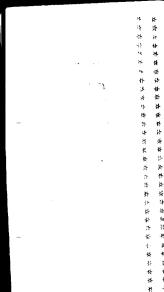
fived investment

## PP OF CASH FLOW AND EQUITY



## irr of cash flow and equity







4.2.2

Equipment List (In Volume II)

Smelter and Sulphur Plant

Equipment diagram, Dwg No. 360 100 901 004-9, Rev.3

Coal Plant

Equipment diagram,
Dwg No. 360 100 901 008-1, Rev.1

Power Plant

Equipment diagram,
Dwg No. 360 100 901 009-1, Rev.1

CUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTEK

DATE:85-08-28 PAGE NO: 1
DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
DUTOKUMPU NG :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NG:
FEVISION:5 DATE:22.08.85

200----0

EUUIPMENT TYPE

FLASH SMELTER AREA

210----0

EQUIPMENT TYPE

DRYER AND FSF FEED AREA

210-116-0100

EQUIPMENT TYPE

CONCENTRATE DAY BIN

CAPACITY

1100 T

VOLUME MATERIAL (TOTAL) 60C M3

CONCRETE AFPROX. 250 M3

MANUFAC TUPER

LOCAL

210-116-0200

EQUIPMENT TYPE

CENCENTRATE CAY BIN

CAPACITY

1100 T

VOLUME MATERIAL (TCTAL) 60G M3

CONCRETE APPROX. 250 M3

MANUF ACTUREF

LOCAL

210-116-0300

EQUIPMENT TYPE

CONCENTRATE DAY BIN

CAPACITY

1100 T

VCLUME MATERIAL (TCTAL) 60C M3

CONCRETE APPROX. 250 M3

MANUFACTURER

OUTOKUMPU CY/ENGINEERING DIVISION
PROJECT :PPCL PYFITE SMELTER

DATE: 85-08-28 PAGE NO: DEPARTMENT: PROJECT

CLIENT :PPCL
DOCUMENT: EQUIPMENT LIST (ATNB)
OUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

210-116-0400

EQUIPMENT TYPE

DAY BIN

SERVICE

TOP SHALE CAY BIN

CAPACITY

600 T

VOLUME MATERIAL (TOTAL) 30C M3

CONCRETE A FPROX. 180 M3

MANUFAC TURER

LCCAL

210-117-0100

EQUIPMENT TYPE

DRIED CHARGE BIN

VCLUME MATERIAL WEIGHT (TOTAL) 350 M3

STEEL

APPRICA-60 T (INCL-STEEL SUPPORTS)

MANUFACTURER

LCCAL

210-117-0200

EQUIPMENT TYPE

DRIED CHARGE BIN

VCLUME

WEIGHT

MAT ER TAL

(TCTAL) 50 M3 STEEL

APPECX.20 T (INCL.SUPPORTS)

MANUFACTURER

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE ND: 3 DEPARTMENT : PROJECT

CLIENT :PPCL DOCUMENT: EQUIPMENT LIST (ATNB) QUTCKUMPU NO :360 100 900 001 ALT1 **DESIGN** : AK I

CLIENT NO :

REVISION :5 DATE :22.08.85

210-167-0100

EQUIPMENT TYPE

BELT CONVEYOR

CAPACITY

140 T/H

MAIN DIMENSIONS

LENGTH 33000 MM 1000 MM WIDTH INCLANATION: HORIZONTAL

WEIGHT

APPRCX. 5 I

INCLUDING

BELT SCALE

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\* 210-167-0100-M1\*\*\* 4 BELT CONVEYOR

MANUFACTURER

LOCAL

210-167-0200

EQUIPMENT TYPE

BELT CONVEYOR

CAPACITY

140 T/H

MAIN DIMENSIONS

75000 MM LENGTH WIDTH 1000 MM IN" ANATION: 14 DEGREES

WEIGHT

AP 0X. 12 T

MOTOR NO./RATING (KW) - MOTOR TITLE

\*\*\* \_10-167-0200-M1\*\*\* 11 BELT CONVEYOR

MANUFACTURER

OUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 4
DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
GUTOKUMPU NG :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

210-167-0300

FOUTPMENT TYPE

BELT CONVEYOR

SERVICE

FOR TOP SHALE

CAPACITY

40 T/H

MAIN DIMENSIONS

LENGTH 700C PM
INCLANATION: HORIZONTAL

BELT WIDTH WEIGHT

650 MM APPRCX. 1 T

INCLUDING

BELT SCALE

MCTOR NC./RATING (KW) MOTOR TITLE

\*\*\*210-167-0300-M1 \*\*\* 3.0 \*\*\*

BELT CONVEYOR

MANUFACTUFER

LOCAL

210-168-0130

EQUIPMENT TYPE

DRAG CONVEYOR

CAPACITY

80 T/H

MAIN DIMENSIONS

LENGTH 5000 MM WIDTH 800 MM

WEIGHT

APPROX. 7 T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*210-168-0100-M1 \*\*\* 7.5
DRAG CONVEYOR

MANUFACTURER

DUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: 5 DEPARTMENT : PROJECT

CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

OUT OKUMPU NO :360 100 900 001 ALT1

:4KI DESIGN

CLIENT NO :

REVISION :5 DATE :22.08.85

210-168-0200

EQUIPMENT TYPE

DRAG CONVEYOR

CAPACITY

80 T/H

MAIN DIMENSIONS

LENGTH SOOD MM WIDTH 800 MM

WEIGHT

APPRCX. 7 T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*210-168-0200-M1 \*\*\* 7.5 DRAG CONVEYOR

MANUFACTURER

**FOREIGN** 

210-170-0100

EQUIPMENT TYPE

PNEUMATIC CONVEYOR SYSTEM

SERVICE

FOR DRIED CHARGE

CAPACITY WEIGHT

150 T/H APPREX. 20 T

MOTOR NO. / RATING (KW)

\*\*\*210-170-0100-M1 \*\*\* 132 \*\*\* AIR BLOWER

MOTOR TITLE

\*\*\*210-170-0100-M2 \*\*\* 132 \*\*\* AIR BLOWER STAND BY

\*\*\*210-170-0100-M3 \*\*\* 1,1 \*\*\*

AIR LCCK

\*\*\*210-170-0100-M4 \*\*\* 1,1

AIR LOCK

\*\*\*210-170-0100-M5 \*\*\* 5 \*\*\*

RETURN AIR FAN

MANUFAC TURER

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: DEPARTMENT : PROJECT

CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB) DUTOKUMPU NO :360 100 900 001 ALT1

DESIGN :AKI CLIENT NG :

REVISION :5 DATE :22.08.85

210-194-0100

EQUIPMENT TYPE

MULTICOIL DRYER

TYPE

STEAM DRYER

CAPACITY PRESSURE MATERIAL WEIGHT

70 T/H (STEAM) 20 BAR AISI 316 APPRCX. 30 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\* 210-194-0100-M1\*\*\* 160 \*\*\* MULTICOIL DRYEF

M ANUFACTUFER

**FOREIGN** 

210-194-0200

EQUIPMENT TYPE

MULTICGIL CRYER

TYPE

STEAM DRYER

CAPACITY PRESSURE MATERIAL WEIGHT

70 T/H (STEAM) 20 BAR AISI 316 APPRCX. 30 T

MOTER NO./RATING (KW) MOTOR TITLE

\*\*\*210-194-0200-M1 \*\*\* 160

MULTICOIL DRYER

MANUFAC TUFEL

OUT OKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 7
DEPARTMENT:PROJECT

CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

DUTCKUMPU NO :360 100 900 001 ALT1

DES IGN : AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

210-212-0100

ECUIPMENT TYPE

EXHAUST AIR FAN

SERVICE

EXHAUST AIR FAN FOR BAG FILTER

CAPACITY MATERIAL WEIGHT 30000 NM3/F AISI 316 APPRCX. 1,5 T

MOTOR NO./FATING (KW)

MOTOR TITLE

\*\*\*210-212-0100-M1 \*\*\* 45 \*\*\*

EXHAUST AIR FAN

MANUFACTURER

FOREIGN

210-218-0100

EQUIPMENT TYPE

BELT FEEDER FOR CONCENTRATE

CAPACITY

25-120 T/H

BELT LENGTH BELT WIDTH BELT INCLINE

WEI GHT

V ...

12000 M 1200 MM NCNE APPECX. 7 I

MOTOR NO./RATING (KW)

MOTOR TITLE

\*\*\* 210-218-0100-M1\*\*\* 7.5 \*\*\*

BELT FEEDER

MANUFACTURER

OUTOKUMPU GY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 8
DEPARTMENT :PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
OUTOKUMPU NO :360 100 930 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

210-218-0200

EQUIPMENT TYPE

BELT FEEDER FOR CONCENTRATE

CAPACITY

25-120 T/H

BELT LENGTH
BELT WIDTH
BELT INCLINE
WEIGHT

12000 M 1200 MM NCNE APPRCX. 7 T

MOTOR NO./RATING (KW)

\*\*\* 210-216-0200-M1\*\*\* 7,5 \*\*\*
BELT FEEDEF

MANUF AC TUFER

LOCAL

210-218-0300

EQUIPMENT TYPE

BELT FEEDER FOR CONCENTRATE

CAPACITY

25-120 T/H

BELT LENGTH BELT WIDTH BELT INCLINE WEIGHT

12000 M 1200 MM NONE APPREX. 7 T

MCTOR NO./RATIES (KW) MCTOR TITLE

\*\*\* 210-218-0300-M1\*\*\* 7,5 \*\*\*
BELT FEEDER

MANUFAC TURER

DUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 9
DEPARTMENT:PROJECT

CLIENT :PPCL
DCCUMENT:EQUIPMENT LIST (ATNB)
DUTCKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

210-218-0400

EQUIPMENT TYPE

BELT FEEDER

SERVICE

BELT FEEDER FOR TOP SHALE

CAPACITY

4-40 T/H

BELT LENGTH BELT WIDTH BELT INCLINE WEIGHT

8000 MM 800 MM NGNE APPRGX. 5 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*210-218-0400-M1 \*\*\* 3,0 \*\*\*

BELT FEEDER

MANUFAC TUPER

LOCAL

210-411-0100

EQUIPMENT TYPE

VIBRATING SCREEN

CAPACITY

140 T/H

FRACTION

25 MM

MATERIAL WEIGHT

CARBON STEEL APPROX. 2 T

MOTOR NG./RATING (KW) MOTOR TITLE

\*\*\*210-411-0100-M1 \*\*\* 15 \*\* VIBRATING SCREEN

LOCAL

MANUFAC TURER

CUTOKUMPU CY/ENGINEERING DIVISION PROJECT :PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 10 DEPARTMENT:PROJECT

CLIENT :PPCL
DCCUMENT:EQUIPMENT LIST (ATNB)
DUTGKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NG:
REVISION :5 DATE :22.08.85

210-417-0100

EQUIPMENT TYPE

BAG FILTER

CAPACITY

30000 NM3/H

TEMPERATURE

110 C

WEIGHT MATERIAL APPFEX. 5 T

HOUSING: AI SI 316, BAGS: POLYACRYLVITR.

MANUF ACTUR ER

FOREIGN

220---0

EQUIPMENT TYPE

FLASH SMELTING FURNACE AREA

220-108-0100

EQUIPMENT TYPE

GRANULATION BASIN

SERVICE

FOF SLAG

**DIMENSIONS** 

MATERIAL

L X W X H : 11 X 3 X 2 M

CCNCRETE . E STIMATED VOLUME: 40 M3

MANUFACTURER

LGCAL

220-108-0200

EQUIPMENT TYPE

GRANULATION BASIN

SERVICE

FOR SLAG

DIMENSIONS

MATERIAL

L X W X H : 11 X 3 X 2 M

CONCRETE . E STIMATED VOLUME: 40 M3

MANUF ACTUR ER

BUTOKUMPU GYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: 11 DEPARTMENT : PROJECT

CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB) DUTOKUMPU NO :360 100 900 001 ALT1

DESIGN :4KI CLIENT NO :

**REVISION :5 DATE :22.08.85** 

220-131-0100

EQUIPMENT TYPE

CCAL DUST BURNER

CAPACITY

WEIGHT

0,3- 1 T/H APPROX. 1 T

LCCAL

MANUFAC TUPER

220-131-0200

EQUIPMENT TYPE

COAL DUST EURNER

CAPACITY

WEIGHT

0,3- 1 T/H

APPRCX. 1 T

MANUFAC TURER

LOCAL

220-131-0300

EQUIPMENT TYPE

COAL DUST BURNER

CAPACITY

WEIGHT

0,3- 1 T/H APPECX. 1 T

MANUFAC TURER

LOCAL

220-131-0400

EGUIPMENT TYPE

CCAL DUST BURNER

CAPACITY

WEIGHT

0,3- 1 T/H APPRCX. 1 T

MANUFACTURER

LCCAL

220-131-0500

EQUIPMENT TYPE

COAL DUST BURNER

CAPACITY

WEIGHT

0,3- 1 T/H APPRCX. 1 T

MANUFACTURER

OUTOKUMPU CYZENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE: 85-08-28 PAGE NO: 12 DEPARTMENT: PROJECT

CLIENT :PPCL
DDCUMENT:EQUIPMENT LIST (ATNB)
GUTOKUMPU ND :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

220-131-0600

EQUIPMENT TYPE CCAL DUST BURNER

CAPACITY 0.3-1 T/H WEIGHT APPF CX. 1 T

MANUFACTURER LOCAL

220-133-0100

EQUIPMENT TYPE AUXILIARY BURNER

SERVICE START UP BLRNER

CAPACITY 150-600 KG/H FUEL LIGHT CIL WEIGHT APPRCX. 1 T

MANUFACTURER LOCAL

220-133-0200

220-140-0100

EQUIPMENT TYPE . AUXILIARY BURNER

SERVICE STAFT UP BURNER

CAPACITY 150-600 KG/H
FUEL LIGHT GIL
WEIGHT APPRCX. 1 T

MANUFACTURER LGCAL

EQUIPMENT TYPE SLAG LAUNDER WITH COVERS

DIMENSIONS LENGTH 12000 MM

MATERIAL CCPPER WEIGHT APPRCX.11 T

MANUFACTURER FCREIGN

OUTOKUMPU GY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE: 85-08-28 PAGE NO: 13

DEPARTMENT : PROJECT

CLIENT :PPCL
DCCUMENT:EQUIPMENT LIST (ATNB)
DUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

220-140-0200

EQUIPMENT TYPE

SLAG LAUNDER WITH COVERS

DIMENSIONS

LENGTH 12000 MM

MATERIAL WEIGHT COPPER

APPRCX.11 T

MANUFACTURER

FOREIGN

220-140-0300

EQUIPMENT TYPE

SLAG LAUNDER WITH COVERS

DIMENSIONS

LENGTH 120 CO MM

MATERIAL WEIGHT CCPPER

APPRCX.11 T

MANUFACTURER

FOREIGN

220-140-0400

EQUIPMENT TYPE

SLAG LAUNDER WITH COVERS

DIMENSIONS

LENGTH 120 CO MM

MATERIAL

COPPER

WEIGHT

APPRCX.11 T

MANUFACTURER

OUT DRUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: 14 DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

GUTOKUMPU NO :360 100 900 001 ALT1 CLIENT NO :

DESIGN :AKI REVISION :5 DATE :22.08.85

220-140-0500

220-140-0600

220-167-0100

EQUIPMENT TYPE GRANULATION LAUNDER

DIMENSIONS LENGTH 3500 MM

MATERIAL STEEL WEIGHT APPROX. 1.5 T

MANUFAC TURER LOCAL

EQUIPMENT TYPE GRANULATION LAUNDER

DIMENSIONS LENGTH 350C MM

MATERIAL STEEL WEIGHT APPROX. 1.5 T

MANUFACTUR ER LOCAL

EQUIPMENT TYPE BELT CONVEYOR

SERVICE FOR SLAG

CAPACITY 100 T/H

MAIN DIMENSIONS LENGTH 350CO MM WIDTH 650 MM

BELT INCLINE 10 DEGREES WEIGHT APPFCX. 3 T

MOTOR NO. / FATING (KW) \*\*\*220-167-0100-M1 \*\*\*11 MOTOR TITLE BELT CONVEYOR

MANUFACTUP ER LOCAL OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 15 DEPARTMENT:PROJECT

CLIENT :PPCL
DCCUMENT:EQUIPMENT LIST (ATNB)
GUTDKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

220-174-0100

EQUIPMENT TYPE

RAKE CLASSIFIER

TYPE SERVICE SCRAPER DEWATERING CONVEYOR FOR SLAG

CAPACITY

100 T/H

MAIN DIMENSIONS

L:11000 MM B:2000 MM

#EI GHT

APPRGX. 25 T

MOTOR NO./RATING (KW) MCTOR TITLE

\*\*\*220 -174-0100-M1 \*\*\* 11
RAKE CLASSIFIER

**FOREIGN** 

M AN UF AC TUR ER

220-174-0200

EQUIPMENT TYPE

RAKE CLASSIFIER

TYPE SERVICE SCRAPER DEWATERING CONVEYOR FOR SLAG

CAPACITY

100 T/H

MAIN DIMENSIONS

L: 11000 MM, B:2000 MM

WEIGHT

APPROX. 25 T

MCTCR NO. /FATING (KW)

\*\*\*220-174-0200-M1 \*\*\* 11

MOTOR TITLE

RAKE CLASSIFIER

MANUFACTURER

BUTCKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: 16 DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

OUT CKUMPU NO :360 100 900 001 ALT1

DES IGN :AKI CLIENT NO :

REVISION :5 DATE :22.08.85

220-198-0100

EQUIPMENT TYPE

GAS DUCTWORK

SERVICE

PROCESS AND COMBUSTION

AIR DUCTING

INCLUDING

DIMENSIONS

MATERIAL WEIGHT

TCTAL LENGTH: 150 M. WALL THICKNESS: 4 AND 6 MM.DIAM: 700 AND 1600 MM MILD STEEL 21 T TOTAL (SUPPORTS NOT INCL.)

LOCAL

MANUFACTURER

OUTOKUMPU GY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 17 DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
DUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :

FEV ISION :5 DATE :22.08.85

220-198-0200

EQUIPMENT TYPE

GAS DUCTWORK

SERVICE

GXYGEN DUCTING FOR SMELTER PLANT.

INCLUDING

SUCISUAMIC

MATERIAL WEIGHT

TOTAL LENGTH: 250 M. WALL THICKNESS: 4 MM. DIAM: 700 MM STAINLESS STEEL

18 T TOTAL (SUPPORTS EXCLUDED)

MANUFACTURER

LOCAL

220-212-0100

ECUIPMENT TYPE

TYPE

CAPACITY
PRESSURE
TEMPERATURE
WEIGHT

PROCESS AIF FAN

CENTRI-UGAL

40000 NM3/F 10 KPA 35 C APPRCX. 2,5 T

MOTOR NO./RATING (KW) MOTOR TITLE

MANUFACTURER

\*\*\* 220-212-0100-M1\*\*\* 160 \*\*\*
PROCESS AIR FAN

DUTOKUMPU GYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 18
DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
GUTGKUMPU ND :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22-08-85

220-212-0200

EQUIPMENT TYPE

PROCESS AIR FAN

TYPE

CAPACITY
PRESSURE
TEMPERATURE

CENTRIFUGAL

10 KPA 35 C

WEIGHT

APPRCX. 2,5 T

MOTOR NO./RATING (KW)
MCTOR TITLE

MANUFACTURER

\*\*\* 220-212-0200-M1\*\*\* 160 \*\*\*

PROCESS AIR FAN

LOCAL

220-212-0300

EQUIPMENT TYPE

COMBUSTION AIR FAN

TYPE

CAPACITY
PRESSURE
TEMPERATURE
WEIGHT

CENTRIFUGAL

20000 NM3/H 9 KPA 35 C APPREX. 2 T

MOTOR NO./RATING (KW) MOTOR TITLE

M ANUF AC TUP ER

\*\*\*220-212-0300-M1\*\*\* 110 \*\*\*

COMBUSTION AIR FAN

LOCAL

220-223-0100

EQUIPMENT TYPE

DRIED CHARGE DRAG FEEDER

7-70 T/H

MAIN DIMENSIONS

LENGTH 10 COO MM WIDTH EOO MM APPRCX. 8 T

WEIGHT

CAPACITY

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\* 220-223-0100-M1 \*\*\* 11 DRAG FEEDER

MANUFACTUFER

BUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 19 DEPARTMENT : PROJECT

CLIENT :PPCL

DECUMENT: EQUIPMENT LIST (ATNB) OUTOKUMPU NO :360 100 900 001 ALT1

DESIGN

:AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

220-223-0200

ECUIPMENT TYPE

MAIN DIMENSIONS

DRIED CHARGE DRAG FEEDER

CAPACITY

WEIGHT

7-70 T/H

LENGTH 10000 MM

h I DT H MM 0 03

APPROX. 8 T

MCTOR NG. / FATING (KW)

MOTOR TITLE

\*\*\*220-223-0200-M1 \*\*\* 11

DRAG FEEDER

**MANUFACTURER** 

**FSREIGN** 

220-261-0100

ECUIPMENT TYPE

FLASH SMELTING FURNACE

SERVICE

FOR PYRITE

CAPACITY **SUCTIONAL NIAM** 

REACTION SHAFT D=6.5 M H=7.0 M

SETTLER L=22 M

UPTAKESHAFT D=6.0 M H=15 M

SLAG HOLES 4

BURNER CPENINGS

NO. OF TAP HOLES

SETTLER

120 T/H

6 FOR COAL

MANUFACTUR ER

LGCAL/FORE IGN

REMARKS

STEEL CONSTRUCTION 950 T (LOCAL) BASIC BRICKS 1200 T (FOREIGN) NON BASIC BRICKS 370T (LOCAL) COOLING ELEMENTS 110 T (FOREIGN)

SPRINGS 5 T (FOREIGN)

DUTCKUMPU CY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 20 DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
DUTOKUMPU NG :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NC : REVISION :5 DATE :22.08.85

220-289-0100

EQUIPMENT TYPE

JACKET WATER HEAT EXCHANGER

CAPACITY
TEMPERATURE FANGE
WEIGHT

700 M3/H
mATER IN:50 DEG.C. OUT:40 DEG.C.
APPRCX. 5 T

MANUF ACTUR ER

LCCAL

220-289-0200

EQUIPMENT TYPE

JACKET WATER HEAT EXCHANGER

SERVICE

STAND BY

CAPACITY TEMPERATURE FANGE WEIGHT 700 M3/H
hATEF IN:50 DEG.C. DUT:40 DEG.C.
APPRCX. 5 T

MANUFACTURER

LGCAL

220-289-0300

EQUIPMENT TYPE

SPRAY WATER HEAT EXCHANGER

CAPACITY
TEMPERATURE RANGE
WEIGHT

300 M3/H WATER IN:50 DEG.C. GUT:40 DEG.C. APPRCX.2.5 T

MANUFAC TUFER

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 21 DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
GUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

220-289-0400

ECUIPMENT TYPE

SPRAY WATER HEAT EXCHANGER

SERVICE

STAND BY

CAPACITY
TEMPERATURE RANGE
WEIGHT

300 M3/H WATER IN:50 DEG.C. DUT:40 DEG.C. APPRCX. 2,5 T

MANUFACTUFER

LOCAL

220-318-0100

EQUIPMENT TYPE

CVERHEAD TRAVELLING CRANE

LIFTING CAPACITY LIFTING HEIGHT SPAN WEIGHT

34 M 24 M

10 T

APPRCX. 20 T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*220-318-0100-M1 \*\*\* 11 \*\*\*

CVERHEAD TRAVELLING CRANE

\*\*\*220-318-0100-M2 \*\*\* 2,2 \*\*\*

OVERHEAD TRAVELLING CRANE

\*\*\*220-318-0100-M3 \*\*\* 1,1 \*\*\*

OVERHEAD TRAVELLING CRANE

MANUFACTURER

LOCAL

220-376-0100

EQUIPMENT TYPE

JACKET WATER PUMP

CAPACITY PRESSURE WEIGHT 700 M3/H 650 KPA APPRCX. 3 T

MCTOR NO./RATING (KW) MCTOR TITLE

\*\*\*220-376-0100-Mi \*\*\*200 \*\*\*

JACKET WATER PUMP

MANUFAC TURER

LCCAL

1 1

OUTOKUMPU BY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 22 DEPARTMENT:PROJECT

CLIENT :PPCL

DCCUMENT: EQUIPMENT LIST (ATNB)
GUTGKUMPU NG :360 100 900 001 ALT1

DESIGN : AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

220-376-0200

EQUIPMENT TYPE

JACKET WATER PUMP

SERVICE

STAND BY

CAPACITY PRESSURE WEIGHT 700 M3/H 650 KPA APPF CX. 3 T

MOTOR NG./RATING (KW) MCTOR TITLE

\*\*\*220-376-0200-M1 \*\*\*200
JACKET WATER PUMP

JACKET WATER PUT

MANUFACTURER

LOCAL

220-376-0400

EQUIPMENT TYPE

SPRAY WATER PUMP

CAPACITY PRESSURE WEIGHT 300 M3/H 600 KPA APPRCX. 2 T

MOTOR NC./RATING (KW) MOTOR TITLE

\*\*\*220-376-0400-M1 \*\*\* 90 SPFAY WATER PUMP

MANUFACTUR ER

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 23 DEPARTMENT:PROJECT

CLIENT :PPCL
DSCUMENT:EQUIPMENT LIST (ATNB)
OUTDKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :

FEVISION :5 DATE :22.08.85

223-376-0500

EQUIPMENT TYPE

SPRAY WATER PUMP

SERVICE

STAND BY

CAPACITY PRESSURE WEIGHT

300 M3/H 600 KPA APPRCX. 2 T

MCTOR NO./FATING (KW) MOTOR TITLE

\*\*\*220-376-0500-M1 \*\*\* 90 \*\*\*
SPRAY WATER PUMP

MANUF AC TUP ER

LOCAL

220-376-0700

EQUIPMENT TYPE

GRANULATION WATER PUMP

CAPACITY PRESSURE WEIGHT

600 M3/H 350 KPA APPFOX. 2.5 T

MGTOR NO./FATING (KW) MOTOR TITLE

\*\*\*220-376-0700-M1 \*\*\* 90 \*\*\*
GRANULATION WATER PUMP

M AN UF AC TUF ER

LUCAL

220-376-0800

EQUIPMENT TYPE

GFANULATION MATER PUMP

CAPACITY PRESSUFE WEIGHT

600 M3/H 350 KPA APPRGX. 2,5 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*220-376-0800-M1 \*\*\* 90 \*\*\*
GRANULATION WATER PUMP

1 1 1

M AN UF AC TUKER

DUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 24 DEPARTMENT:PROJECT

CLIENT :PPCL
DCCUMENT:EQUIPMENT LIST (ATNB)
DUTDKUMPU NC :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

220-376-0900

EQUIPMENT TYPE

GRANULATION WATER PUMP

SERVICE

STAND BY

CAPACITY PRESSURE WEIGHT

600 M3/H 350 KPA APPRCX. 2.5

MGTOR NO./RATING (Kw) MOTOR TITLE

\*\*\*220-376-0900-M1 \*\*\* 90 \*\*\*
GRANULATION WATER PUMP

MANUFACTURER

LCCAL

220-435-0100

EQUIPMENT TYPE

CONCENTRATE BURNER

CAPACITY
MAIN DIMENSIONS

120 T/H

WEIGHT

APPRCX. 5 T

MANUF ACTUFER

FOREIGN

220-519-0100

EQUIPMENT TYPE

JACKET WATER TANK

VCLUME MATERIAL 400 M3 CCNCRETE 100 M3 STEEL COVER

MANUFACTURER

OUT OKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 25 DEPARTMENT :PROJECT

CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)
CUTOKUMPU NO :360 130 900 001 ALTI

DESIGN :AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

225-519-0200

EQUIPMENT TYPE

SPRAY WATER TANK

VCLUME MATERIAL 300 M3 CCNCRETE 8C M3 STEEL COVER

MANUFACTURER

LECAL

220-519-0300

EQUIPMENT TYPE

CIL TANK

SERVICE

FCR HEAVY FUEL OIL

VOLUME DIMENSIONS

700 M3

DIAM: 9,5M .HIGHT:10.0 M

MATERIAL

MILD STEEL

MANUFACTURER

LOCAL

REMARKS

SUPPLIED WITH STEAM HEATING PIPES

220-519-0400

EQUIPMENT TYPE

OIL TANK

SERVICE

FOR LIGHT FUEL DIL

VCLUME DIMENSIONS

18 M3 DIAM:2,8M,F1GHT:3 M

MATERIAL

MILD STEEL

MANUFACTURER

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 26 DEPARTMENT:PROJECT

CLIENT : PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)
BUTOKUMPU ND :360 100 900 001 ALT1

DESIGN

: AK I

CLIENT NO :

REVISION :5

DATE :22.08.85

220-569-0100

EQUIPMENT TYPE

EMERGENCY DAMPER BETWEEN FSF-WHB

MAIN DIMENSIONS

TEMPERATURE WEIGHT

WATER IN:30 DEG.C. GUT:60 DEG.C.

APPROX. 6 T

MANUFAC TUFER

LCCAL

6 X 5 M

REMARKS

WATER FLOW: 100 M3/H WATER PRESSURE: 4 BAR

230----0

EQUIPMENT TYPE

PROCESS GAS HANDLING AREA

230-124-0100

EQUIPMENT TYPE

WASTE HEAT BOILER

C TYPE SERVICE

WEIGHT

FCRCED CIRCULATION

FCR FLASH SMELTING FURNACE

CAPACITY
PRESSURE
GAS FLOW

SATURATED STEAM 140 T/H

70 BAR 130000 NM3/H

TEMPERATURE

INLET 1250 C

CUTLET

350 C

ου

APPRCX. BCILER: 600 T SUPPORTS: 350 T

MANUFAC TURER

1 111

**FCREIGN** 

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NG: 27 DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
DUTGKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

230-198-0100

EQUIPMENT TYPE

GAS DUCTWOFK

SEFVICE

PROCESS GAS DUCTING FOR

AREA 230

**DIMENSIONS** 

TOTAL LENGTH:175 M DIAM:1800, 2000,2200 MM, WALL THICKNESS:8 MM

MILD STEEL

MATERIAL WEIGHT

71 T (TOTAL, SUPPORTS NOT INCLUDED)

M ANUF ACTURER

LGCAL

230-212-0100

EQUIPMENT TYPE

PROCESS GAS FAN

CAPACITY
PRESSURE
TEMPERATURE

70000 NM3/H 4 KPA 360 C

WEIGHT

APPROX. 10 T

MOTOR NO. / PATING (KW)

\*\*\*230-212-0100-M1 \*\*\* 250 \*\*\*
PROCESS GAS FAN

MOTOR TITLE

MANUFACTURER

FOREIGN

REMARKS

INVERTER REGULATED

DUTOKUMPU DY/ENGINEERING DIVISION PROJECT :PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 28
DEPARTMENT:PROJECT

CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

DUTOKUMPU ND :360 100 900 001 ALT1

DESIGN :AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

230-212-0200

EQJIPMENT TYPE

CAPACITY
PRESSURE
TEMPERATURE
WEIGHT

PROCESS GAS FAN

70000 NM3/H 4 KPA 360 C APPEGX. 10 T

MOTOR NO./RATING (KW)

MOTOR TITLE

M AN UF ACTURER

REMARKS

\*\*\*230-220-0200-M1 \*\*\* 250 \*\*\*

PROCESS GAS FAN

FOREIGN

INVERTER REGULATED

230-372-0100

EQUIPMENT TYPE

**EJECTOR** 

SERVICE

CE BY-PASS EJECTOR BETWEEN WHB AND EP.

C AP ACITY
MATERIAL

GAS FLOW 6C 000 NM3/H STAINLESS STEEL

WEIGHT INCLUDING

APPRCX. 1.5 T INLET VALVES

M AN UF AC TURER

1 1

FUREIGN

REMARKS

 $I = I \qquad \quad I = -I = -I$ 

SUCTION: 1 KPA

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT :PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 29
DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
JUTOKUMPU NO :360 100 900 GO1 ALT1
DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

230-372-0200

EQUIPMENT TYPE

EJECTOR

SERVICE

BY-BASS EJECTOR AFTER EP.

C AP ACITY MATERIAL

GAS FLOW: 20 000 NM3/H STAINLESS STEEL

WEIGHT INCLUDING

APPEOX. 0.5 T INLET VALVE

MANUFACTURER

FOREIGN

REMARKS

SUCTION: 1 KPA

230-372-0300

EQUIPMENT TYPE

EJECTOR

SERVICE

BY-BASS . TOR AFTER EP.

CAPACITY MATERIAL

GAS FLOW: 2 JOO NM3/H STAINLESS SIEEL

WEIGHT INCLUDING

APPRCX. 0,5 T INLET VALVE

M AN UF AC TUR ER

FOREIGN

REMARKS

SUCTION: 1 KPA

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE: 85-08-28 PAGE NO: 30 DEPARTMENT: PROJECT

CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

OUT CKUMPU NO :360 100 900 001 ALT1

DESIGN : AKI

CLIENT NO :

FEVISION :5 DATE :22.08.85

230-376-0100

EQUIPMENT TYPE

MATER PUMP

SERVICE

WHB CIRCULATION WATER PUMP

CAPACITY HEAD WEIGHT 1100 M3/H 40 M

MCTOR NO./RATING (KW)

APPRCX. 2 T

MOTOR TITLE

\*\*\*230-376-0100-M1 \*\*\* 200 \*\*\*
WHB CIRCULATION WATER PUMP

MANUFAC TURER

FORE IGN

230-376-0200

EQUIPMENT TYPE

MATER PUMP

TYPE SERVICE TURBINE DRIVE WATER PUMP WHB CIRCULATION WATER PUMP

FUR EMERGENCY

CAPACITY HEAD WEIGHT

1100 M3/H

40 M

APPRCX. 1,5 T

MANUF ACTUR ER

FOREIGN

SUTCKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: 31

DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

DUTOKUMPU NO :360 100 900 001 ALT1

:AKI

CLIENT NO :

DATE :22.08.85 REVISION :5

230-421-0100

**EQUIPMENT TYPE** 

ELECTROSTATIC PRECIPITATOR

TYPE

SERVICE

FCR WHB

CAPACITY TEMPERATURE

WEIGHT

70000 NM3/H

360

APPRCX. PRECIPITATOR 370 T

SUPPORTS 50 T

MOTOR NO. / RATING (KW)

MOTOR TITLE

\*\*\* SEVERAL, TOTAL \*\*\* 90

\*\*\*

MANUFACTUR ER

FOREIGN

230-421-0200

EQUIPMENT TYPE

ELECTROSTATIC PRECIPITATOR

TYPE

SERVICE

FOR WHB

CAPACITY

TEMPERATURE

₩EI GHT

70000 NM 3/H

360

APPROX. PRECIPITATOR 370 T

SUFPERTS 50 T

MOTOR NO. / RATING (KW)

MOTOR TITLE

\*\*\* SEVERAL. TOTAL \*\*\* 90

MANUFACTURER

230-562-0100

EQUIPMENT TYPE

DISC VALVE

SERVICE

FOR EP.

**FCREIGN** 

MAIN DIMENSIONS

WEIGHT

DIAMETER: 2 M APPRCX. 1 T

MANUFAC TUPER

DUTOKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 32 DEPARTMENT : PROJECT

CLIENT : PPCL DOCUMENT: EQUIPMENT LIST (ATNB) GUTOKUMPU NO :360 100 900 001 ALT1 :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

230-562-0200

EQUIPMENT TYPE

DISC VALVE

SERVICE

FCR EP.

MAIN DIMENSIONS HEIGHT

DIAMETER = 2 M APPRCX. 1 I

MANUFAC TUFER

LOCAL

240----0

EQUIPMENT TYPE

FLUE DUST HANDLING AREA

240-140-0100

EQUIPMENT TYPE

LAUNDER

TYPE SERVICE

FOR FLUE DUST

DIMENSIONS

L:40000 MM W:500 MM

DEPTH: 500 PM

MATERIAL

CONCRETE 7 M3, STEEL COVERS

MANUFAC TURER

LCCAL

1 1 1

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE: 85-08-28 PAGE NO: 3: DEPARTMENT: PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
OUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NG: REVISION:5 DATE:22.08.85

240-168-0100

EQUIPMENT TYPE

DRAG CONVEYOR FOR WHB DUST

TYPE CAPACITY

WITH SCREEN

15 T/H

MAIN DIMENSIONS

LENGTH 40 COO MM

WEIGHT

APPROX. 22T

MOTOR NO./FATING (KW)
MOTOR TITLE

\*\*\*240-168-0100-M1 \*\*\* 5,5 \*\*\*
DFAG CONVEYOR FOR WHB DUST

MANUFACTURER

FCREIGN

240-168-0200

EQUIPMENT TYPE

DRAG CONVEYOR FOR EP DUST

CAPACITY

5 T/H

MAIN DIMENSIONS

LENGTH 20000 MM WIDTH 500 MM

WEIGHT

APPREX. 7 I

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*240-168-0200-M1 \*\*\* 3
DRAG CONVEYOR FOR EP DUST

\*\*\*

MANUFACTURER

FOREIGN

240-168-0300

EQUIPMENT TYPE

DRAG CONVEYOR FOR EP DUST

CAPACITY

5 T/H

MAIN DIMENSIONS

LENGTH 20 COO MM WIDTH 500 MM

WEIGHT

APPRCX. 7 T

MOTOR NO./FATING (KW)
MOTOR TITLE

\*\*\*240-168-0300-M1 \*\*\* 3
DRAG CONVEYOR FOR EP DUST

MANUFACTURER

FOREIGN

DUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 34 DEPARTMENT:PROJECT

CLIENT :PPCL
DCCUMENT:EQUIPMENT LIST (ATNB)
DUTCKUMPU NC :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

249-168-0400

EQUIPMENT TYPE

DRAG CONVEYOR FOR EP DUST

CAP ACITY

5 T/H

MAIN DIMENSIONS

LENGTH 20COO MM WIDTH 500 MM

WEIGHT

APPRCX. 7 T

MOTOR NC./FATING (KW) MOTOR TITLE

\*\*\*240-168-0400-M1 \*\*\* 3
DRAG CONVEYOR FOR EP DUST

MANUFACTURER

FOREIGN

240-168-0500

EQUIPMENT TYPE

DRAG CONVEYOR FOR EP DUST

CAPACITY

5 T/H

MAIN DIMENSIONS

LENGTH 20 CO 0 MM WIDTH 50 0 MM

WEIGHT

APPECX. 7 T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*240-168-0500-M1 \*\*\* 3
DRAG CONVEYOR FOR EP DUST

MANUF AC TUP ER

**FORE IGN** 

240-209-0100

EQUIPMENT TYPE

WATER LOCK

TYPE SERVICE WITH WATER NOZZLES FOR WHB DUST

VOLUME WEIGHT 1 M3

APPRCX. 0.5 T

MATERIAL

STAINLESS STEEL

MANUFAC TUPER

DUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 35 DEPARTMENT:PROJECT

CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)
GUTOKUMPU NO :360 100 900 001 ALTI

DESIGN :AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

240-209-0200

EQUIPMENT TYPE

MATER LOCK

TYPE SERVICE WITH WATER NOZZLES FOR EP DUST

VGLUME WEIGHT 1 M3 APPRCX. 0.5 T

MATERIAL

STAINLESS STEEL

MANUFACTURER

LCCAL

240-209-0300

EQUIPMENT TYPE

WATER LOCK

TYPE SERVICE WITH WATER NOZZLES FOR EP DUST

VOLUME WEIGHT 1 M3

APPRCX. 0,5 T

MATERIAL

STAINLESS STEEL

MANUF ACTUR ER

LCCAL

240-209-0400

EQUIPMENT TYPE

WATER LOCK

TYPE SERVICE WITH WATER NGZZLES FOR EP DUST

VCL UME WEIGHT 1 M3

APPRCX. 0,5 T

MATERIAL

STAINLESS STEEL

MANUFAC TURER

LGCAL

GUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYPITE SMELTER

DATE:85-08-28 PAGE NO: 36 DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
DUTDKUMPU NC :360 '00 900 001 ALT1
DESIGN :AKI

CLIENT NG:
REVISION:5 DATE:22.08.85

WATER LOCK

240-209-0500

240-374-0300

EQUIPMENT TYPE

TYPE WITH WATER NOZZLES SERVICE FCR EP DUST

VCLUME 1 M3
WEIGHT APPRCX. 0.5 T

MATERIAL STAINLESS STEEL

M ANUFACTURER LCCAL

EQUIPMENT TYPE SLURRY PUMF

I

SERVICE UNDERFLOW SLURRY PUMP

CAPACITY 25 M3/H HEAD 20 M

MATERIAL STEEL WITH RUBBER LINING

WEIGHT APPRCX. 0.8 T

MANUFACTURER FGRE IGN

GUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 37 DEPARTMENT : PROJECT

CLIENT :PPCL DOCUMENT: EQUIPMENT LIST (ATNB) DUT DKUMPU NO :360 100 900 001 ALT1 :AKI DES IGN

CLIENT NO : REVISION :5 DATE :22.08.85

240-374-0400

EQUIPMENT TYPE

SLURRY PUMF

SERVICE

UNDERFLOW SLURRY PUMP.STAND-BY

CAPACITY HEAD

25 M3/H 20 M

MATERIAL

STEEL WITH RUBBER LINING

WEIGHT

MOTOR NO./FATING (KW) MOTOR TITLE

MANUFACTURER

APPRCX. O.E T

\*\*\*240-374-0400-M1 \*\*\* 7.5 \*\*\* SLURRY PUMF

**FCREIGN** 

240-376-0100

EQUIPMENT TYPE

HATER PUMP

SERVICE

CVERFLOW WATER FOR FLUE DUST SLURRY

CAPACITY HEAD WEIGHT

MOTOR NO. / FATING (KW) MOTOR TITLE

1.1.1

MANUFACTURER

130 M3/H 15 M APPROX. 0,5 T

\*\*\*240-376-0100-M1 \*\*\* 15 MATER PUMP

LCCAL

1 1

OUTGKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 38 DEPARTMENT:PROJECT

CLIENT :PPCL
DGCUMENT: EQUIPMENT LIST (ATNB)
DUTCKUMPU NG :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO:
REVISION :5 DATE:22.08.85

240-376-0200

EQUIPMENT TYPE

WATER PUMP

SERVICE

GVERFLOW FCR FLUE DUST SLURRY STAND-BY

CAPACITY HEAD WEIGHT

130 M3/H 15 M APPRGX. 0.5 T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*240-376-0200-M1 \*\*\* 15 \*\*\*
WATER PUMP

MANUFAC TUPER

LOCAL

240-518-0100

EQUIPMENT TYPE

PUMP TANK

SERVICE

CVERFLOW WATER PUMP TANK

V CLUME MATERIAL

500 M3 CCNCRETE WALLS.STEEL COVER CCNCRETE VCLUME ABOUT 100 M3

MANUF ACTURER

OUTOKUMPJ GY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 39 DEPARTMENT:PROJECT

CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

OUTOKUMPU NO :360 100 900 001 ALT1

DESIGN :AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

240-532-0100

EQUIPMENT TYPE

THICKENER

DIMENSIONS

DIAMETER 20000 MM

MATERIAL

CONCRETE, APPROX. 370 M3

MOTOR NO. /FATING (KW)

MOTOR TITLE

\*\*\*240-532-0100-M1 \*\*\* 3 \*\*

THICKENER

\*\*\*240-532-0100-M2 \*\*\* 3 \*\*\*

THICKENER

\*\*\*240-532-0100-M3 \*\*\* 0,5 \*\*\*

THICKENER

MANUFACTURER

LCCAL

300----0

EQUIPMENT TYPE

SULPHUR PLANT AREA

310----0

EQJIPMENT TYPE

SULPHUR RECOVERING AREA

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 40 DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
GUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO:
REVISION :5 DATE :22.08.85

310-129-0100

EQUIPMENT TYPE

CAPACITY

PRESSURE

GAS FLOW TEMPERATURE

VOLUME MAIN DIMENSIONS

MATER TAL

WEIGHT

MOTOR NO./RATING (KW) MOTOR TITLE

MANUF ACTUFER

REMARKS

SULPHUR CONDENSING BOILER

SATURATED STEAM 19 T/H (HIGH PRESS) SATURATED STEAM 8 T/H (LOW PRESS.)

5,5 BAR 1,7 BAR

125000 NM3/H

INLET 360 C GUTLET 150 C

HEAT TRANSFER AREA 2650 / 2650 M2 L X W X H 24 X 7 X 4 M STEEL

APPRCX. BOILER 155 T SUPPORTS 145 T

LOCAL

CIRCULATION PUMPS(ELECTRICAL AND TURBINE DRIVEN ARE INCLUDED)

DUTCKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: 41 DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: EQUIPMENT LIST (ATNB) OUTOKUMPU NO :360 100 900 001 ALT1

DESIGN : 4KI CLIENT NO :

REVISION :5 DATE :22.08.85

310-129-0200

EQUIPMENT TYPE

GAS COOLING BOILER

CAPAC ITY

SATURATED STEAM 26 T/H

PRESSURE

5,5 BAR

GAS FLOW TEMPERATURE 130000 NM3/H INLET 480 C CUTLET 250 C

VOLUME MAIN DIMENSIONS

MATERIAL

HEAT TRANSFER AREA 2950 M2

LXNXH 15 X 7 X 4 M STEEL

WEIGHT

APPRCX. BOILER 180 T

SUPPORTS 160 T

MCTOR NO./RATING (KW) MOTOR TITLE

**\*\*\*310-129-0200** \*\*\* 110 \*\*\*

CIRCULATION WATER PUMP

MANUFAC TUPER

LCCAL

REMARKS

CIRCULATION PUMPS (ELECTRIC AND TURBINE DRIVEN) ARE INCLUDED

310-198-0100

EQUIPMENT TYPE

GAS DUCT

MANUFAC TURER

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NG: 42 DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: EQUIPMENT LIST (ATNB) OUTOKUMPU NO :360 100 900 001 ALT1

: AK I DES IGN

CLIENT NO :

REVISION :5 DATE :22.08.85

310-198-0200

EQUIPMENT TYPE

GAS DUCT

SERVICE

PROCESS GAS DUCTINGS FOR AREA 310

DIMENSIONS

MATERIAL WEIGHT

LENGTH: 80 M TOT-DIAM-2M AND 2.2M

STAINLESS STEEL WALL THICKNESS 8 MM 36 T (TOTAL, SUPPOFTS EXCLUDED)

MANUFACTUFER

LUCAL

310-204-0100

EQUIPMENT TYPE

STACK

SERVICE

FCR SULPHUR LINE AND POWER PLANT

HEIGHT

MATERIAL

150 M

CENCRETE . 2800 M3

MANUFACTURER

LCCAL

3 10-2 09-01 00

EQUIPMENT TYPE

WATER LOCK

VICL UM E

WEIGHT

5 M3

APPROX. 5 T

MATER IAL

BODY OF MILD STEEL , LINED WITH

STAINLESS STEEL

MANUF ACTURER

LUCAL

GUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 43
DEPARTMENT:PROJECT

CLIENT :PPCL
DCCUMENT:EQUIPMENT LIST (ATNB)
DUTOKUMPU NG :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22-08-85

310-209-0200

EQUIPMENT TYPE

WATER LOCK

VOLUME WEIGHT 5 M3 APPRCX. 5 T

MATERIAL

BCDY OF MILD STEEL LINED WITH

STAINLESS STEEL

MANUFACTURER

LOCAL

310-209-0300

EQUIPMENT TYPE

WATER LOCK

VCLUME WEIGHT 5 M3

APPEGX. 5 T

MAT ER IAL

BODY OF MILD STEEL, LINED WITH

STAINLESS STEEL

MANUFACTURER

LCCAL

310-212-0100

EQUIPMENT TYPE

PROCESS GAS FAN

CAPACITY
PRESSURE
TEMPERATURE
WEIGHT

70000 NM3/H 4 KPA 170 C APPREX. 10 T

MOTOR NG./RATING (KW) MOTOR TITLE

\*\*\*310-212-0100-M1 \*\*\* 160 \*\*\*
PFOCESS GAS FAN

MANUF ACTURER

FOREIGN

REMARKS

INVERTER REGULATED

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 44
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CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)
DUTOKUMPU NG :360 100 900 001 ALT1

DESIGN : AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

310-212-0200

EQUIPMENT TYPE

PROCESS GAS FAN

CAPACITY
PRESSURE
TEMPERATURE
WEIGHT

70000 NM3/H 4 KPA 170 C APPFGX. 10 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*310-212-0200-M1 \*\*\* 160 \*\*\*
PROCESS GAS FAN

\*\*\*310-212-0300-M1 \*\*\* 132 \*\*\*

MANUFACTUR ER

**FORE IGN** 

REMARKS

INVERTER REGULATED

310-212-0300

EQUIPMENT TYPE

COMBUSTION AIR FAN

TYPE SERVICE CENTRIFUGAL FOR GAS REFEATER

CAPACITY
PRESSURE
TEMPERATURE
WEIGHT

18000 NM3/H 17 KPA 35 C APPF DX. 2.5 T

MOTER NO./FATING (KW) MCTOR TITLE

COMBUSTION AIR FAN

M ANUF AC TUR ER

OUTOKUMPU OY/ENGINEEFING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: 45 DEPARTMENT : PROJECT

CLIENT :PPCL DCCUMENT: EQUIPMENT LIST (ATNB) DUT OKUMPU NG :360 100 900 001 ALTI : AKI DESIGN

CLIENT NO : REVISION :5 DATE :22.08.85

310-212-0400

EQUIPMENT TYPE

SERVICE

COMBUSTION AIR FAN

FOR GAS REFEATER STAND-BY

CAPACITY PRESSURE TEMPERATURE WEIGHT

18000 NM3/H 17 KPA 35 C APPRCX. 2,5 T

MOTOR NO./RATING (KW) MOTOR TITLE

MANUF ACTURER

\*\*\*310-212-0400-M1 \*\*\* 132 \*\*\*

COMBUSTION AIR FAN

310-212-0500

EQUIPMENT TYPE

SERVICE

FAN

LOCAL

EXHAUST GAS FAN

CAPACITY PRESSURE TEMPERATURE WEIGHT

75000 NM3/H 4.0 KPA 140 C APPRGX. 10 T

MOTOR NO./FATING (KW) MOTOR TITLE

MANUFACTURER

REMARKS

\*\*\*310-212-0500-M1 \*\*\* 160 \*\*\*

EXHAUST GAS FAN

FCREIGN

INVERTER REGULATED

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 46
DEPARTMENT:PROJECT

CLIENT :PPCL
DGCUMENT:EQUIPMENT LIST (ATNB)
CUT CKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT ND:
REVISION:5 DATE:22.08.85

310-212-0600

EQUIPMENT TYPE

ICIN' I I F C

SERVICE EXHAUST GAS FAN

CAPACITY 75000 NM3/H
PRESSURE 4.0 KPA
TEMPERATURE 140 C
WEIGHT APPRICX- 10 T

FAN

MOTOR NO./RATING (KW) \*\*\*310-212-0600-M1 \*\*\* 160 \*\*\*
MOTOR TITLE EXHAUST GAS FAN

MANUFACTURER FOREIGN

REMARKS INVERTER REGULATED

310-212-0700

EQUIPMENT TYPE COMBUSTION AIR FAN

SERVICE FOR INCINERATOR

CAPACITY

PRESSURE

TEMPERATURE

16000 NM3/F

10 KPA

35 C

MOTOR NO./FATING (KW) \*\*\*310-212-0700-M1 \*\*\* 75 \*\*\*
MOTOR TITLE COMBUSTION AIR FAN

MANUFACTURER LOCAL

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYSITE SMELTER

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DOCUMENT: EQUIPMENT LIST (ATNB)
OUTGKUMPU NG :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO:
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310-213-0800

EQUIPMENT TYPE

SECONDARY AIR FAN

SERVICE

FOR INCINE FATOR

CAPACITY
PRESSURE
TEMPERATURE

19000 NM3/F 10 KPA 35 C

MOTOR NO./RATING (KW) MCTOR TITLE

\*\*\*310-213-0800-M1 \*\*\* 90 \*\*\* SECONDARY AIR FAN

MANUF ACTURER

LGCAL

310-263-0100

EQUIPMENT TYPE

INCINERATOR

SEPVICE

FOR PROCESS GAS H2S COMBUSTION

C AP ACITY DIMENSIONS INLET:145000 NM3/H CUT:180000 NM3/H D:4M L:13M

MANUFACTURER

LCCAL

REMARKS

INCLUDING: BRICKLINING
FUEL: HEAVY FUEL DIL
FUEL CONSUMPTION: 1,4 T/H
TEMP:INLET/OUTLET 130/400 C

OUT OKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT : PPCL

DECUMENT: EQUIPMENT LIST (ATNB) DUTOKUMPU NC :360 100 900 001 ALT1 : AK I

CLIENT NO :

REVISION :5 DATE :22.08.85

DES IGN

310-281-0100

ECUIPMENT TYPE

GAS FEHEATER

SERVICE

FOR HOT CATALYZER

CAPACITY

GAS INLET 125000 NM3/H CUTLET 143000 NM3/H

INLET/OUTLET 150/430 C

TEN PERATURE FUEL

CONSUMPTION DIMENSIONS

CIL 1-5 T/H

D = 3 M L = 10 M

WEIGHT INCLUDING

APPFOX. 71 T DUCT, BRICKLINING

MANUFACTURER

LOCAL

310-370-0130

EQUIPMENT TYPE

FUEL DIL PLMP

TYPE SERVICE

FOR GAS REHEATER

CAPACITY WEIGHT

1.7 M3/H APPFGX.0.3 T

MCTOR NO./RATING (KW) MOTOR TITLE

\*\*\*310-370-0100-M1 \*\*\* 3 FUEL CIL PUMP

MANUF ACTURER

LCCAL

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT : PPCL

DCCUMENT: EQUIPMENT LIST (ATNB) DUTOKUMPU NO :360 100 900 001 ALTI

**DESIGN** 

:AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

310-370-0200

EQUIPMENT TYPE

FUEL GIL PUMP

SERVICE

FCR GAS REFEATER, STAND-BY

CAPACITY WEIGHT

1.7 M3/H APPRCX. 0.2 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*310-370-0200-M1 \*\*\* 3 FUEL GIL PLMP

MANUF AC TUR ER

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

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CLIENT :PPCL
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OUTCKUMPU NC :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NG :

REVISION :5 DATE :22.08.85

310-370-0300

EQUIPMENT TYPE

FUEL CIL PLMP

SEFVICE

FOR INCINERATOR

CAPACITY WEIGHT 1.7 M3/H APPRCX. 0,2 T

MCTOR NO./RATING (KW) MCTOR TITLE

\*\*\*310-370-0300-M1 \*\*\* 3 \*\*\*
FUEL DIL PLMP

MANUF ACTURER

LOCAL

310-374-0100

EQUIPMENT TYPE

SLURRY PUMP

SERVICE

FCF ABSORBIICN TOWER (LIME STONE SLURRY)

\*\*\*310-374-0100-M1\*\*\* 90 \*\*\*

CAPACITY

600 M3/H

PRESSURE

300 KPA

WEIGHT

APPECX. 0,5 T

MOTOR NO./RATING (KW)

1 1 1 1

APPECAS UPS 1

MCTCR TITLE

SLURRY PUMP

MANUFACTURER

LCCAL

QUICKUMPU GY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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CLIENT : PPCL DOCUMENT: EQUIPMENT LIST (ATNB) DUTCKUMPU NO :360 100 900 001 ALT1 DESIGN : AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

310-374-0200

EQUIPMENT TYPE

SLURRY PUMP

H

SERVICE

FOR ABSORBTION TOWER (LIME STONE SLURRY)

CAPACITY PRESSURE WEIGHT

800 M3/H 300 KPA APPREX. 0.5 T

MOTER NO. / FATING (KW) MOTOR TILLE

\*\*\*310-374-0200-M1 \*\*\* 90 \*\*\*

SLURRY PUMP

MANUF 4C TURER

LOCAL

310-374-0300

EQUIPMENT TYPE

SLURRY PUMP

TYPE SERVICE FOR ABSORBTION TOWER FOR ABSORBTION POWER(STAND-BY) (LIME STONE SLURRY)

CAPACITY PRESSURE WEIGHT

800 M3/H 300 KPA APPRCX. 0,5 T

MOTOR NG. /RATING (KW) MOTOR TITLE

1

\*\*\*310-374-0300-M1 \*\*\* 90 SLURRY PUMP

1 11

LCCAL

MANUFACTURER

DUTCKUMPU DY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

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CLIENT : PPCL DOCUMENT: EQUIPMENT LIST (ATNB) OUT OK UMPU NO :360 100 900 001 ALT1 DES IGN : AK I

CLIENI NG : REVISION :5 DATE :22.08.85

\*\*\*

310-374-0400

EQUIPMENT TYPE

WATER PUMP

SERVICE

FOR TAILING POND OVERFLOW

CAPACITY

250 M3/H

PRESSURE

300 KPA

WEIGHT

APPRIX. 0.5 T

MOTOR NO./RATING (KW)

\*\*\*310-370-0400-M1 \*\*\* 30

MOTOR TITLE

MATER PUMP

MANUFACTURER

LGCAL

310-374-0500

EQUIPMENT TYPE

MATER PUMP

SERVICE

FOR TAILING POND OVERFLOW

(STAND-BY)

CAPACITY

250 M3/H

PRESSURE

300 KPA

WEIGHT

APPEDX. 0.5 T

MOTOR NO. / FATING (KW)

1

MOTOR TITLE

\*\*\*310-370-0500-M1 \*\*\* 30 WATER PUMP

MANUF AC TURER

LCCAL

DUTOKUMPU GY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
DUTDKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22-08-85

310-374-0600

EQUIPMENT TYPE

MATER PUMP

SERVICE

FOR SCRUBBER OUTLETWATER

CAPACITY PRESSURE WEIGHT 300 M3/H 300 KPA APPRCX. 1.C T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*310-370-0600-M1 \*\*\* 30 \*\*\*

WATER PUMP

MANUFACTURER

LOCAL

310-374-0700

EQUIPMENT TYPE

MATER PUMP

SERVICE

FOR SCRUBBER OUTLETWATER

(STAND-BY)

CAPACITY PRESSURE WEIGHT 300 M3/H 300 KPA APPROX. 1.0 T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*310-370-0700-M1 \*\*\* 30

MATER PUMP

MANUFAC TURER

DUTDKUMPU CY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

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CLIENT :PPCL
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OUTOKUMPU NC :360 100 900 GO1 ALT1
DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

310-376-0100

EQUIPMENT TYPE

MATER PUMP

SERVICE

FOF GAS SCRUBBER

CAPACITY PRESSURE WEIGHT 50 M3/H 600 KPA APPRCX. 0.5 T

MCTOR NO./FATING (KW) MCTOR TITLE

\*\*\*310-376-0100-M1 \*\*\* 15 \*\*\*

WATER PUMP

MANUFAC TURER

LCCAL

310-376-0200

EQUIPMENT TYPE

WATER PUMP

CERVICE

FOR GAS SCRUBBER(STAND-BY)

CAPACITY PRESSURE WEIGHT 50 M3/H 600 KPA APPRCX. 0,5 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*310-376-0200-M1 \*\*\* 15 \*\*\*
WATER PUMP

MANUFAC TUR ER

LCCAL

OUTOKUMPU GY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT :PPCL
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DUTCKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO:
REVISION:5 DATE:22.08.85

310-420-0100

EQUIPMENT TYPE

CAPACITY 125000 NM3/H

DIMENSIONS

TEMPERATURE

MAT ER IAL

WEIGHT

MANUFACTURER

310-420-0200

EQUIPMENT TYPE

CAPACITY TEMPERATURE

DIMENSIONS

MATERIAL

WEIGHT

MANUFACTURER

DEMISTER

125000 NM 3/H 150 C

DIAMETER 7000 MM, HEIGHT 12000 MM DEMISTER BED: HEIGHT 150 MM CARBON STEEL, BED OF ACIDPROOF STEEL

APPRGX. 52 T (SUPPGRTS INCL.)

LCCAL

DEMISTER

143000 NM3/H 135 C

DIAMETER 7000 MM, HEIGHT 8000 MM DEMISTER BED : HEIGHT 150 MM BED MATERIAL : ACID PROOF STEEL

APPROX. 30 T (SUPPORTS INCL.)

LCCAL

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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OUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NG :

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310-423-0100

EQUIPMENT TYPE

SCRUEBER

SER VICE

FOF PROCESS GAS CLEANING

CAPACITY
GAS TEMPERATURE

180000 NM3/H INLET 400 C GUTLET 50 C

MAIN DIMENSIONS

DIAMETER 2500 MM HEIGHT 10000 MM

MATERIAL

STAINLESS AND ACID PROOF STEEL

WEIGHT

APPROX. 27 T

MANUFACTURER

LOCAL

310-423-0200

EQUIPMENT TYPE

ABSCRBTION TOWER

CAPACITY

200 000 NM3/H

GAS TEMPERATURE

60 DEG.

MAIN DIMENSIONS

DIAM: 4800 MM, HEIGHT: 12000 MM

MATERIAL CONSTRUCTION

BCDY:CARBON STEEL LINING:ACIC PROOF STEEL

WEIGHT

APPRCX. 18C T

MANUFAC TUR ER

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT :PPCL
DCCUMENT:EQUIPMENT LIST (ATNB)
OUTCKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

310-431-0100

EQUIPMENT TYPE

CAPACITY TEMPERATURE

DIMENSIONS

MAT ERIAL

WEIGHT

MANUF ACTURER

310-433-0100

EQUIPMENT TYPE

CAPACITY TEMPERATURE

NO.OF CELLS VOLUME DIMENSIONS

MATERIAL WEIGHT

MANUFACTURER

AGGLOMERAT CR

125 000 NM3/H 150 C

DIAMETER 3700 MM
HEIGHT APPR. 2000 MM
AGGLOMERATOR BED: HEIGHT 100 MM
BED: ACIDPROF STEEL, BODY: CARB. STEEL

APPREX. 25 T

LOCAL

HOT CATALYZER

143000 NM3/H 480 C

14
EFFICIENT MASS VOLUME 730 M3
MAIN DIM. L X W X H :
22 X 8,5 X 15 M
CELL : 1 X 8 X 6.5 M

STAINLESS STEEL APPROX. 30C T

FCREIGN

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
GUTGKUMPU NC :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO:
REVISION:5 DATE:22.08.85

310-433-0200

EQUIPMENT TYPE

COLD CATALYZER
75000 NM3/F
250 C (INLET)

CAPACITY TEMPERATURE

NO.OF CELLS VOLUME DIMENSIONS

14
EFFICIENT MASS VOLUME 730 M3
MAIN DIM. L X W X H :
22 X 8,5 X 15 M
CELL : 1 X 8 X 6,5 M

MATERIAL WEIGHT

STEEL APPRCX. 30C T

MANUFACTURER

LCCAL

310-433-0300

EQUIPMENT TYPE

COLD CATALYZER

CAPACITY TEMPERATURE

75000 NM3/F 250 C (INLET)

NG. OF CELLS VOLUME DIMENSIONS

14
EFFICIENT MASS VOLUME 730 M3
MAIN DIM. L X W X H :
22 X 8,5 X 15 M
CELL : 1 X 8 X 6,5 M

MATERIAL WEIGHT

STEEL APPROX. 300 T

MANUFACTURER

LCCAL

OUTCKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT : PPCL DOCUMENT: EQUIPMENT LIST (ATNB) DUTOKUMPU NO :360 100 900 001 ALT1 DESIGN : AK I

CLIENT NO : REVISION :5 DATE :22.08.85

310-464-0100

EQUIPMENT TYPE

CAPACITY

SULPHUR FLCW : 650 T/H

SULPHUR CONDENSING TOWER

GAS FLOW TEMPERATURE 75000 NM3/F INLET 260 C **CUTLET 135 C** 

**DIMENSIONS** 

DIAMETER 9000 MM HEIGHT 120CO MM

MATERIAL

STEEL

WEIGHT

APPRCX. 26C T

M ANUF ACTUPER

**FCREIGN** 

310-464-0200

EQUIPMENT TYPE

SULPHUR CONDENSING TOWER

CAPACITY

SULPHUR FLEW : 650 T/H

GAS FLOW TEMPERATURE 75000 NM3/F INLET 260 C **DUTLET 135 C** 

**DIMENSIONS** 

DIAMETER 9000 MM HEIGHT 120 CO MM

MATERIAL

STEEL

WEIGHT

APPROX. 260 T .

MANUFACTURER

FOREIGN

DUTOKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 60 DEPARTMENT:PROJECT

CLIENT :PPCL
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OUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :
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310-516-0100

EQUIPMENT TYPE

SERVICE

MIXING TANK

FOR ABSORBTION TOWER

CAPACITY MATERIAL WEIGHT 100 M3/H CARBEN STEEL APPEGX. 10 T

MCTOR NO./RATING (KW) MCTOR TITLE

M AN UF AC TUR ER

\*\*\*310-516-0100-M1 \*\*\* 37 \*\*\*
MIXING TANK

LCCAL

310-518-0100

EQUIPMENT TYPE

SERVICE

PUMP TANK

FOR SCRUBBER OUTLET WATER

CAPACITY WEIGHT MATERIAL 100 M3 APPRCX. 10 T MILD STEEL

MANUFACTURER

LCCAL

320----0

EQUIPMENT TYPE

SULPHUR HANDLING AFEA

OUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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OUTOKUMPU NO :360 100 900 001 ALT1

: AK I DESIGN

CLIENT NO : REVISION :5 DATE :22.08.85

320-117-0100

EQUIPMENT TYPE

BIN

SERVICE

LIME BIN

VOLUME MATERIAL WEIGHT

5 M3 STEEL APPRCX. 1 T

MANUFACTURER

LOCAL

320-129-0100

EQUIPMENT TYPE

SU! PHUR COCLING BCILER

TYPE

NATURAL CIPCULATION

CAPACITY

SATURATED STEAM 3,5 T/H

PRESSURE

1.7 BAR

GAS FLOW TEMPERATURE CIRCULATING SULPHUR FLOW 860 T/H INLET 133 C

OUTLET 123 C

VOLUME

HEAT TRANSFER AREA 650 M2

WEIGHT

APPRCX. 35 T

MANUFACTURER

FOREIGN

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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DESIGN :AKI

CLIENT NG:
REVISION :5 DATE:22.08.85

320-129-0200

EQUIPMENT TYPE

SULPHUR COCLING BOILER

TYPE

NATURAL CIRCULATION

CAPACITY

SATURATED STEAM 3.5 T/H

PRESSUE E

1,7 BAR

GAS FLOW TEMPERATURE CIRCULATING SULPHUR FLOW 860 T/H INLET 133 C

CUTLET 123 C

VCLUME

HEAT TRANSFER AREA 650 M2

WEIGHT

APPROX. 35 T

MANUFACTURER

**FOREIGN** 

320-129-0300

EQUIPMENT TYPE

SULPHUR COCLING BOILER

TYPE

NATURAL CIRCULATION

CAPACITY

SATURATED STEAM 3.5 T/H

PFESSURE

1,7 BAR

GAS FLOW TEMPERATURE CIRCULATING SULPHUR FLOW 860 T/H INLET 133 C

GUTLET 123 C

VOL UME

HEAT TRANSFER AREA 650 M2

WEIGHT

APPRCX. 35 T

MANUFAC TUPER

FOREIGN

GUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NG: 63
DEPARTMENT:PROJECT

CLIENT :PPCL
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OUTCKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

320-167-0100

**EQUIPMENT TYPE** 

ECUIPMENT TYPE BELT CONVEYOR

SERVICE FOR PRILLING TOWER

CAPACITY 150 T/H

MM 000 CM HTQUE HTQUE NIAM 600 CM HTQUE HT

BELT INCLINE HGRIZONTAL WEIGHT APPRIX. 5 T

MOTOR NO./FATING (KH) \*\*\*3 20-167-0100-M1 \*\*\* 5,5 \*\*\*

BELT CONVEYOR

MCTOR TITLE BELT CONVEYOR

MANUFACTURER LOCAL

320-167-0200

SERVICE FOR PRILLING TOWER

CAPACITY 150 T/H

MAIN DIMENSIONS LENGTH 40 COO MM WIDTH 650 MM

BELT INCLINE HORIZONTAL WEIGHT APPR CX. 5 T

MOTOR NC./RATING (KW) +++320-167-0200-M1 +++ 5,5 +++

MOTOR TITLE BELT CONVEYOR

MANUFACTURER LGCAL

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

DUTOKUMPU NO :360 100 900 001 ALTI

DESIGN : AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

320-167-0300

**EQUIPMENT TYPE** 

BELT CONVEYOR

SERVICE

FOR PRILLED SULPHUR

CAPACITY

150 T/H

MAIN DIMENSIONS

LENGTH 80 COO MM WIDTH 650 MM

BELT INCLINE

**WEIGHT** 

6 DEGREES
APPROX. 8 T

INCLUDING

BELT SCALE

MOTOR NO. / RATING (KW)

MOTOR TITLE

\*\*\*3 20-167-0 300-M1 \*\*\* 11 \*\*\*

BELT CONVEYOR

MANUFACTUFER

LOCAL

320-172-0100

EQUIPMENT TYPE

SCREW CONVEYOR

SERVICE

FOR LIME

CAPACITY

0-200 KG/H

MAIN DIMENSIONS

LENGTH: 40 00 MM

WEIGHT

APPROX. 0,5 T

MOTOR NO. / FATING (KW)

MCTOR TITLE

\*\*\*320-172-0100-M1 \*\*\* 0,75 \*\*\*

SCREW CONVEYOR

MANUFAC TURER

BUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB) DUTOKUMPU NO :360 100 900 001 ALT1

:AKI DESIGN

CLIENT NO :

REVISION :5 DATE :22.08.85

320-212-0100

EQUIPMENT TYPE

TYPE SERVICE AIR COOLING FAN

AXIAL FAN

FOR PRILLING TOWER

CAPACITY PRESSURE TEMPERATURE WEIGHT

75000 NM3/H 350 PA 35 C APPEDX.0.5 T

MOTOR NO./FATING (KW) MOTOR TITLE

M ANUF AC TUR ER

\*\*\*320-212-0100-M1\*\*\* 15 \*\*\* AIR COOLING FAN

LOCAL

320-212-0200

EQUIPMENT TYPE

TYPE SERVICE AIR CODLING FAN

AXIAL FAN FOR PRILLING TOWER

CAPACITY PRESSURE TEMPERATURE WEIGHT

75000 NM3/F 350 PA 35 C APPRCX.0.5 T

MOTOR NO./RATING (KW) MOTOR TITLE

MANUFAC TURER

\*\*\* 320-212-0200-M1\*\*\* AIR COOLING FAN

LCCAL

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 66 DEPARTMENT : PROJECT

CLIENT :PPCL DOCUMENT: EQUIPMENT LIST (ATNB) OUT CKUMPU NC :360 100 900 001 ALT1 **DESIGN** :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

320-212-0300

EQUIPMENT TYPE

AIR COOLING FAN

TYPE SERVICE

AXIAL FAN FOR PRILLING TOWER

CAPACITY PRESSURE TEMPERATURE WEIGHT

75000 NM3/F 350 PA 35 C APPROX.0.5 T

MOTOR NO. / FATING (KW) MOTOR TITLE

\*\*\* 320-212-0300-M1\*\*\* 15 \*\*\* AIR COOLING FAN

MANUFACTURER

LOCAL

320-212-0400

EQUIPMENT TYPE

AIR COOLING FAN

TYPE SERVICE

AXIAL FAN FOR PFILLING TOWER

CAPACITY PRESSURE TEMPERATURE WEIGHT

75000 NM3/H 350 PA 35 C APPRCX.0,5 T

MCTOR NO. / RATING (KW) MOTOR TITLE

\*\*\* 320-212-0400-M1\*\*\* 15 \*\*\* AIR COOLING FAN

MANUFAC TURER

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 67 DEPARTMENT : PROJECT

CLIENT : PPCL DOCUMENT: EQUIPMENT LIST (ATNB) QUTOKUMPJ NO :360 100 900 001 ALT1 :AKI DESIGN

CLIENT NO : REVISION :5 DATE :22.08.85

320-214-0100

**EQUIPMENT TYPE** 

AIR BLOWER

TYPE SERVICE CENTRIFUGAL FOR PRILLING TOWER

CAPACITY **PRESSURE** TEMPERATURE WEIGHT

2000 NM3/F 10 KPA 35 C APPFOX. 0,4 T

MCTOR NO./RATING (KW) MOTOR TITLE

\*\*\*320-214-0100-M1 \*\*\* 11 \*\*\*

AIR BLOWER

M ANUFACTURER

LCCAL

320-244-0100

EQUIPMENT TYPE

GRAVITY FILTER

TYPE SERVICE GLASS WOOL FILTER . FOR SULPHUF

VOLUME **DIMENSIONS** 

10 M3 LX b X H: 8 X 2 X 0,65 M

WEIGHT MATERIAL APPF CX. CON CRETE 8 M3. STEEL 4 T CONCRETE, STEEL COVER STEAM HEATING PIPES

MANUFAC TURER

LOCAL

REMARKS

CUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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320-244-0200

EQUIPMENT TYPE

GRAVITY FILTER

TYPE SERVICE GLASS WOOL FILTER(STEAM HEATED) FOR SULPHUR

VCLUME DIMENSIONS

10 M3 LXWXH: 8 X 2 X 0,65 M

WEIGHT MATERIAL APPROX.CONCRETE 8 M3.STEEL 4 T CONCRETE

STEAM HEATING PIPES

MANUFACTURER

LOCAL

PEMARKS

STEAM HEATED

320-370-0100

EQUIPMENT TYPE

PUMP

I

TYPE SERVICE

SULPHUR PUPP FROM PUMP TANK TO GRAVITY FILTER

CAPACITY HEAD WEIGHT

25 M3/H 25 M APPROX. D.5 T

MOTER NO. / FATING (KW)

MCTOR TITLE

\*\*\*320-370-0100-M1 \*\*\* 11 SULPHUR PUPP

\*\*\*

MANUFAC TUPER

FOREIGN

REMARKS

GUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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CLIENT NO:
REVISION :5 DATE :22.08.85

320-370-0200

EQUIPMENT TYPE

PUMP

1

TYPE SERVICE SULPHUR PUMP ( STAND BY )
FROM PUMP TANK TO GRAVITY FILTER

CAPACITY HEAD WEIGHT 25 M3/H 25 M APPRCX. 0.5 T

MOTOR NO./FATING (Km) MOTOR TITLE

\*\*\*320-370-0200-M1 \*\*\* 11 \*\*\*

SULPHUR PUMP

MANUFACTURER

FOREIGN

REMARKS

STEAM HEATED

320-370-0300

EQUIPMENT TYPE

PUMP

TYPE SERVICE SULPHUR PUMP FROM PUMP TANK TO CIRCULATION TANK

CAPACITY HEAD WEIGHT 50 M3/H 25 M

APPROX. 0.7 T

WEIGHT

\*\*\*320-370-0300-M1 \*\*\* 18,5 \*\*\*

SUL PHUR PU MP

MOTOR TITLE

MCTOR NO. /RATING (KW)

FCREIGN

REMARKS

OUT OKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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CLIENT NG : REVISION :5 DATE :22.08.85

320-370-0400

EQUIPMENT TYPE

PUMP

TYPE SERVICE

SULPHUR PUPP ( STAND BY ) FROM PUMP TANK TO CIRCULATION TANK

CAPACITY HEAD WEIGHT

50 M3/H 25 M APPROX. 0,7 T

MOTOR NO. / RATING (KW) MCTOR TITLE

\*\*\*320-370-0400-M1 \*\*\* 18,5 \*\*\*

SULPHUR PUMP

MANUFACTURER

**FOREIGN** 

REMARKS

STEAM HEATED

320-370-0500

EQUIPMENT TYPE

PUMP

TYPE SERVICE SULPHUR PUMP FROM PUMP TANK TO CIRCULATION TANK

3 \*\*\*

CAPACITY HEAD WEIGHT

5 M3/H 25 M

APPFOX.0.3

MOTOR NO. /FATING (KW) MCTOR TITLE

\*\*\*32

SULPF -

FORE1

MANUFACTURER

REMARKS

STEAM HEAL J

DUTOKUMPU DYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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DESIGN :AKI CLIENT NO :

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320-370-0600

EQUIPMENT TYPE

PUMP

I

TYPE SERVICE SULPHUR PUPP ( STAND BY ) FROM PUMP TANK TO CIRCULATION TANK

CAPACITY HEAD WEIGHT

5 M3/H 25 M

APPROX.0.3 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*320-370-0600-M1 \*\*\* 3 \*\*\*

SULPHUR PUMP

MANUFACTURER

FORE IGN

REMARKS

STEAM HEATED

320-370-0700

EQUIPMENT TYPE

PUMP

I

TYPE SERVICE SULPHUR PUMP FROM CIRCULATION TANK TO AGGLOMERATOR BED WASH

CAPACITY HEAD WEI GHT

25 M3/H 35 M

MOTOR NO./PATING (KW)

APPRICX. 0.5 T

MOTOR TITLE

\*\*\*320-370-0700-M1 \*\*\* 15 \*\*\* SULPHUR PUMP

MANUFACTURER

FCREIGN

REMARKS

DUTOKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT NO : REVISION :5 DATE :22.08.85

320-370-0800

EQUIPMENT TYPE

PUMP

TYPE SERVICE

SULPHUR PUPP ( STAND BY ) FROM CIRCULATION TANK TO AGGLOMERATCR BED WASH

CAPACITY HEAD WEIGHT

25 M3/H 35 M APPROX. 0,5 T

MOTOR NO. / FATING (KW) MOTOR TITLE

\*\*\*320-370-0800-M1 \*\*\* 15 \*\*\* SULPHUR PUMP

MANUFACTURER

FORE IGN

REMARKS

STEAM HEATED

320-370-0900

EQUIPMENT TYPE

**PUMP** 

TYPE SERVICE SULPHUR PUPP FROM CIRCULATION TANK TO SULPHUR TANK

CAPACITY HEAD WEIGHT

25 M3/H 25 M APPREX. 0.5 T

MOTOR NO./RATING (KW)

\*\*\*320-370-0900-M1 \*\*\* 11 \*\*\* SULPHUR PUPP

MCTOR TITLE

MANUFACTURER

FOREIGN

STEAM HEATED

REMARKS

OUTOKUMPU CY/ENGINEERING DIVISION
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DESIGN :AKI

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320-370-1000

EQUIPMENT TYPE

PUMP

TYPE SERVICE SULPHUR PUMP ( STAND BY ) FROM CIRCULATION TANK TO SULPHUR TANK

CAPACITY HEAD WEIGHT 25 M3/H 25 M APPRCX. 0,5 T

MOTOR NG./FATING (KW)

\*\*\*320-370-1 C00-M1 \*\*\* 11 \*\*\*
SULPHUR PUMP

MCTOR TITLE

FOR E IGN

MANUFAC TURER

REMARKS

STEAM HEATED

320-370-1100

EQUIPMENT TYPE

PUMP

TYPE SERVICE SULPHUR PUMP FOR AUTOCLAVES

CAPACITY HEAD WEIGHT

25 M3/H 35 M

APPRCX. 0.5 T

MCTOR NO./FATING (KW) MOTOR TITLE

\*\*\*320-370-1100-M1 \*\*\* 15 \*\*\*

MANUFACTURER

FOREIGN

REMARKS

STEAM HEATED

SULPHUR PUMP

DUTOKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT NO : REVISION :5 DATE :22.08.85

320-370-1200

EQUIPMENT TYPE

PUMP

TYPE SERVICE SULPHUR PUPP ( STAND BY ) FOR AUTOCLAVES

CAPACITY HEAD WEIGHT

25 M3/H 35 M APPROX. 0.5 T

MCTOR NO./RATING (KW) MOTOR TITLE

\*\*\* 320-370-1200-M1 \*\*\* 15 \*\*\* SULPHUR PUMP

MANUFACTURER

**FCREIGN** 

REMARKS

STEAM HEATED

320-370-1300

EQUIPMENT TYPE

PUMP

TYPE SERVICE

SULPHUR PUMP FROM PUMP TANK TO SULPHUR DAY TANK

CAPACITY HEAD WEIGHT

25 M3/H 25 M

MOTOR NO./RATING (KW) MOTOR TITLE

APPRIX. 0,5 T

MANUFACTURER

\*\*\*320-370-1300-M1 \*\*\* 11 \*\*\* SULPHUR PUPP

FOREIGN

REMARKS

OUTOKUMPU CY/ENGINEERING DIVISION DATE :85-08-28 PAGE NO: 75 PROJECT : PPCL PYRITE SMELTER

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CLIENT NO : REVISION :5 DATE :22.08.85

320-370-1400

EQUIPMENT TYPE

PUMP

TYPE SERVICE

SULPHUR PUPP ( STAND BY ) FROM PUMP TANK TO SULPHUR DAY TANK

CAPACITY HEAD WEIGHT

25 M3/H 25 M APPROX. 0.5 T

MCTOR NO. / FATING (KW) MCTOR TITLE

\*\*\*320-370-1400-M1 \*\*\* 11 \*\*\* SULPHUR PUPP

M ANUF ACTUFER

FOREIGN

REMARKS

STEAM HEATED

320-370-1500

EQUIPMENT TYPE

PUMP

TYPE SERVICE

SULPHUR CIRCULATION PUMP FOR SULPHUF COOLING BOILER

CAPACITY HEAD WEIGHT

240 M3/H 40 M APPROX. 1,3 T

MCTOR NO. / RATING (KW) MOTOR TITLE

\*\*\*320-370-1500-Mi \*\*\* 90 SULPHUR CIRCULATING PUMP

MANUFAC TUFER

FOREIGN

REMARKS

OUTOKUMPU GY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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320-370-1600

EQUIPMENT TYPE

PUMP

TYPE SEFVICE SULPHUR CIRCULATION PUMP FOR SULPHUR COCLING BOILER

C APACITY HEAD WEIGHT 240 M3/H 40 M APPFGX. 1.3 T

MCTOR NO./RATING (KW) MCTOR TITLE

\*\*\*320-370-1600-M1 \*\*\* 90 \*\*\*
SULPHUR CIRCULATING PUMP

MANUFAC TUPER

FOREIGN

REMARKS

STEAM HEATED

320-370-1700

EQUIPMENT TYPE

PUMP

/\* TYPE
/\* SERVICE

SULPHUR CIRCULATION PUMP FOR SULPHUR COGLING BOILER

CAPACITY HEAD WEIGHT 240 M3/H 40 M APPROX. 1.3 T

MOTOR NG./FATING (KW) MOTOR TITLE

\*\*\*320-370-1700-M1 \*\*\* 90 \*\*\*
SULPHUR CIRCULATING PUMP

MANUFACTUFER

FOREIGN

REMARKS

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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320-370-1800

EQUIPMENT TYPE

PUMP

TYPE SERVICE SULPHUR CIRCULATION PUMP FOR SULPHUR COCLING BOILER

CAPACITY HEAD WEIGHT 240 M3/H 40 M APPFOX. 1.3 T

MOTOR NO./RATING (KW) MCTOR TITLE

\*\*\*320-370-1800-M1 \*\*\* 90 \*\*\*
SULPHUR CIRCULATING PUMP

MANUFACTURER

FOREIGN

REMARKS

STEAM HEATED

320-370-1900

EQUIPMENT TYPE

PUMP

TYPE SERVICE

SULPHUR CIFCULATION PUMP FOR SULPHUR COGLING BOILER

CAPACITY HEAD WEIGHT 240 M3/H 40 M APPFCX. 1.2 T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\* 320-370-1900-M1 \*\*\* 90 \*\*\*
SULPHUR CIRCULATING PUMP

MANUFACTURER

FOREIGN

REMARKS

OUTOKUMPU GY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

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DESIGN :AKI

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320-370-2000

EQUIPMENT TYPE

PUMP

TYPE SERVICE

SULPHUR CIRCULATION PUMP FOR SULPHUR COOLING BOILER

CAPACITY HEAD WEIGHT

240 M3/H 40 M APPPRCX. 1.3 T

MOTOR NO./RATING (Km) MOTOR TITLE

\*\*\*320-370-2000-M1 \*\*\* 90 \*\*\*
SULPHUR CIRCULATING PUMP

MANUFAC TUREF

FOREIGN

REMARKS

STEAM HEATED

320-370-2300

EQUIPMENT TYPE

PUMP

SERVICE

SULPHUR PRILLING PUMP

CAPACITY PRESSURE WEIGHT 22 M3/H 1600 KPA APPROX. 1 T

MCTOR NO./RATING (KW) MOTOR TITLE

\*\*\*320-370-2300-M1 \*\*\* 37 \*\*\*
SULPHUR PRILLING PUMP

MANUF ACTURER

FOREIGN

REMARKS

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:AKI

CLIENT NO :

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320-370-2400

DES IGN

EQUIPMENT TYPE

PUMP

TYPE SERVICE STAND BY SULPHUR PRILLING PUMP

CAPACITY PRESSURE WEI GHT

22 M3/H 1600 KPA APPRCX. 1 T

MOTOP NO./RATING (KW) MOTOR TITLE

\*\*\*320-370-2400-M1 \*\*\* 37 \*\*\* SULPHUR PRILLING PUMP

MANUFACTURER

**FOREIGN** 

REMARKS

STEAM HEATED

320-371-0100

EQUIPMENT TYPE

DOSAGE PUMP

TYPE SERVICE PISTON TYPE FOR LIME MILK

CAPACITY PRESSURE WEIGHT

0-2,5 M3/H 400 KPA APPRCX. 0,1 T

MOTOR NO. / RATING (KW)

\*\*\*520-371-0100-M1 \*\*\* 1,5 \*\*\* DESAGE PUMP

MOTOR TITLE

MANUFACTURER

OUTGKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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CLIENT NO :
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320-371-0200

EQUIPMENT TYPE

DOSAGE PUMF

TYPE SERVICE PISTON TYPE FOR LIME MILK

CAPACITY PRESSURE WEIGHT 0-2,5 M3/H 400 KPA APPR DX.0,1 T

MCTGR ND./RATING (KW) MCTOR TITLE

\*\*\*320-371-0200-M1 \*\*\* 1.5 \*\*\*
DCSAGE PUMF

MANUFACTURER

LOCAL

320-371-0300

EQUIPMENT TYPE

DUSAGE PUMP

TYPE SERVICE STAND BY FOR LIME MILK

CAPACITY PRESSURE WEIGHT

0-2,5 M3/H 400 KPA APPRCX. 0,1 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*320-371-0300-M1 \*\*\* 1.5 \*\*\*
DOSAGE PUMF

MANUF ACTUR ER

DUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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DESIGN :AKI

CLIENT NO:
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320-411-0100

**EQUIPMENT TYPE** 

VIBRATING SCREEN

SERVICE

FOR PRILLED SULPHUR

CAPACITY

150 T/H

MATERIAL

CARBON STEEL

WEIGHT

APPROX. 2 T

MCTOR NO. /RATING (KW)

\*\*\*320-411-0100-M1 \*\*\* 15 \*\*\* VIBRATING SCREEN

MOTOR TITLE

LOCAL

MANUFAC TURER

320-411-0200

EQUIPMENT TYPE

VIBRATING SCREEN

SERVICE

FOR PRILLEC SULPHUR

CAPACITY

150 T/H

MATERIAL

CARBON STEEL

WEIGHT

APPPROX. 2 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*320-411-0200-M1 \*\*\* 15 \*\*\*
VIBRATING SCREEN

MANUFAC TUPER

LOCAL

320-509-0100

EQUIPMENT TYPE

PRILLING TOWER

SERVICE

SULPHUR PRILLING TOWER

**SUDISMENT C** 

DIAMETER 3 CO 00 MM, HEIGHT 40000 MM WALL THICKNESS 300 MM

MATERIAL

CONCRETE APPROX. 1500 M3

MANUFAC TURER

LCCAL

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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320-511-0100

EQUIPMENT TYPE

SERVICE

**AUT CCL AV E** 

26 M3

130 C

SULPHUR WASHING

SULPHUR 30 T/H

3,5 BAR (AUTGCLAVE)

LIME MILK 2.0 M3/H

D = 1.5 M L = 15 M

CAPACITY V CL UME TEMPERATURE

PRESSURE

FLOW RATE

MAIN DIMENSIONS

MATERIAL

WEIGHT

MOTOR NO./RATING (KW)

MOTOR TITLE

ACID PROOF STEEL AUTOCLAVE& TANKS:7T, SUPPORTS:5T

(AUTOCLAVE)

STEAM 0.8 T/H PRESSURE 5.5 BAR

\*\*\*320-511-0100-M1 \*\*\* 3 \*\*\*

AUTGCLAVE

\*\*\*320-511-0100-M2 \*\*\* 3 \*\*\*

AUTOCLAVE

MANUFACTURER

REMARKS

FORE IGN

INCLUDING: AGITATORS, SEPARATORS,

TANKS.

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DESIGN :AKI

CLIENT NO :

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320-511-0200

EQUIPMENT TYPE

AUTO CL AV E

SERVICE

SULPHUR WASHING

SULPHUR 30 T/H

CAPACITY VOLUME TEMPERATURE PRESSURE

ME 26 M3
ERATURE 130 C (AUTOCLAVE)
SURF 3.5 BAR (AUTOCLAVE)

FLOW RATE

STEAM 0.8 T/H PRESSURE 5.5 BAR

LIME MILK 2.0 M3/H D = 1.5 M L = 15 M

MAIN DIMENSIONS

MATERIAL WEIGHT ACID PROOF STEEL
AUTOCLAVE& JANKS: 7T, SUPPORTS: 5T

MCTOR NO./RATING (KW) MOTOR TITLE

1 1 1

\*\*\*320-511-0100-M1 \*\*\* 3 \*\*\*
AUTOCLAVE

\*\*\*

\*\*\*320-511-0100-M2 \*\*\* 3
AUTOCLAVE

MANUFAC TURER

FOREIGN

REMARKS

INCLUDING: AGITATORS, SEPARATORS,

TANKS.

JUTOKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT NO :
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320-515-0100

EQUIPMENT TYPE

MEASURING TANK

SERVICE

SULPHUR MEASURING TANK

VOLUME WEIGHT MATERIAL 2 X 6 M3 APPRCX. 12 T CCNCRETE, 4 M3 STEAM HEATING PIPES

MANUFACTUFER

LOCAL

REMARKS

INCLUDING VALVES AND STEEL COVERS

320-516-0100

EQUIPMENT TYPE

MIXING TANK

SERVICE

FOR LIME MILK

VCLUME MATERIAL WEIGHT

25 M3 STEEL APPFCX. 4 T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*320-516-0100-M1 \*\*\* 4
MIXING TANK

MANUFAC TUE ER

OUTOKUMPU CY/ENGINFERING DIVISION PROJECT : PPCL PYRITE SMELTER

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DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

320-518-0100

EQUIPMENT TYPE

SERVICE

PUMP TANK

LIQUID SULPHUR CIRCULATING TANK

CAPACITY VOLUME MATERIAL

2500 T/H 95 M3 CCNCRETE, APPR. 30 M3 STEAM HEATING PIPES

MANUFACTURER

PEMARKS

LOC A L

INCLUDING STEEL COVERS

320-518-0200

EQUIPMENT TYPE

SERVICE

PUMP TANK

SULPHUR PUMP TANK
FOR SULPHUR CONDENSING BOILERS

VOLUME MATERIAL 18 M3 CONCRETE, 6 M3 STEAM HEATING PIPES

MANUFACTUR ER

REMARKS

LOCAL

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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DESIGN :AKI

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320-518-0300

EQUIPMENT TYPE

SERVICE

VOLUME MATERIAL

M ANUF AC TUR ER

REMARKS

PUMP TANK

SULPHUR PUMP TANK FOR DEMISTER

18 M3 CCNCRETE + 6 M3 STEAM HEATING PIPES

LCCAL

INCLUDING STEEL COVERS

320-518-0400

EQUIPMENT TYPE

SERVICE

VOLUME MATERIAL

M AN UF AC TUF ER

REMARKS

PUMP TANK

SULPHUR PUMP TANK FOR EXHAUST GAS FANS

10 M3 CONCRETE + 3 M3 STEAM HEATING PIPES

LOCAL

DUTOKUMPU DY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

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CLIENT NO:
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320-518-0500

EQUIPMENT TYPE

PUMP TANK

SERVICE

SULPHUR PUMP TANK FOR AUTOCLAVES

VOLUME AATERIAL 18 M3 CONCRETE, 6 M3 STEAM HEATING PIPES

MANUFACTURER

LOCAL

REMARKS

INCLUDING STEEL COVERS

320-518-0600

EQUIPMENT TYPE

SERVICE

PUMP TANK

SULPHUR PUMP TANK FOR SULPHUR DAY TANK

VOLUME MATERIAL

18 M3 CONCRETE 6 M3 STEAM HEATING PIPES

MANUFACTURER

LOCAL

REMARKS

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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DESIGN :AKI

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320-518-0700

EQUIPMENT TYPE

SERVICE

VOLUME MATERIAL

MANUFAC TURER

REMARKS

PUMP TANK

SULPHUR PUFP TANK FOR SULPHUR PRILLING

18 M3 CCNCRETE. 6 M3 STEAM HEATING PIPES

LCCAL

INCLUDING STEEL COVERS

320-519-0100

EQUIPMENT TYPE

SERVICE

VOLUME WEIGHT MATERIAL

MANUFACTURER

REMARKS

TANK

SULPHUR TANK FOR AUTOCLAVES FEED TANK

100 M3 APPRCX. 92 T STEEL STEAM HEATING PIPES

LCCAL

OUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 89 DEPARTMENT : PROJECT

CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB) OUTOKUMPU NO :360 100 900 001 ALT1

DESIGN : AKI CLIENT NO :

REVISION :5 DATE :22.08.85

320-519-0200

EQUIPMENT TYPE

SERVICE

DAY TANK

SULPHUR DAY TANK

VOLUME WEIGHT MATERIAL 400 M3 APPROX. 240 T STEAM HEATING PIPES

MANUFACTURER

REMARKS

LCCAL

INCLUDING STEEL COVERS

3 30 ---- 0

EQUIPMENT TYPE

WASTE LIQUID HANDLING AREA

330-212-0100

EQUIPMENT TYPE

FAN

TYPE SERVICE CENTRIFUGAL EXHAUST GAS FAN

CAPACITY PRESSURE

5000 NM3/H 500 PA

MAT ER TAL

CARBON STEEL , RUBBER LINED

WEIGHT

APPRCX. 0.5 T

MOTOR NO./FATING (KW) MOTOR TATLE

\*\*\*330-212-0100-M1 \*\*\* 5.5 \*\*\* EXHAUST GAS FAN

M ANUF ACTUR ER

LCCAL

OUT OK UMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 90 DEPARTMENT : PROJECT

CLIENT :PPCL DOCUMENT: EQUIPMENT LIST (ATNB) OUTOKUMPU NC :360 100 900 001 ALT1 DESIGN : AK I

CLIENT NO :

REVISION :5 DATE :22.08.85

330-243-0100

EQUIPMENT TYPE

DRUM FILTER

SERVICE

FOR ARSENIC PRECIPITATE

FILTER AREA WEIGHT

4.5 M2 APPROX. 1 T

MATERIAL

ACID PROOF STEEL

MOTOR NO./PATING (KW)

\*\*\*330-243-0100-M1 \*\*\* 1,1 \*\*\* DRUM FILTER

MOTOR TITLE

\*\*\*330-243-0100-M2 \*\*\* 0,75 \*\*\*

DRUM FILTER

MANUFAC TURER

LOCAL

REMARKS

VACUUM: 500 MM HG

330-370-0100

EQUIPMENT TYPE

PUMP

SERVICE

UNDERFLOW PUMP FOR SULPHUR WASHING WASTE WATER THICKENER

CAPACITY HEAD WEIGHT

2 M3/H 15 M

APPRCX. 0.2 T

MOTOR NO./FATING (KW)

MOTOR TITLE

\*\*\*330-370-0100-M1 \*\*\* 2,2 \*\*\*

UNDERFLOW PUMP

LOCAL

MANUFACTUFER

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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CLIENT :PPCL
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CLIENT NO:
REVISION :5 DATE :22.08.85

330-370-0200

EQUIPMENT TYPE

PUMP

SERVICE

UNDERLOW PLMP FOR SULPHUR WASHING WASTE WATER THICKENER

CAPACITY HEAD WEIGHT 2 M3/H 15 M APPRCX. 0.2 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*330-370-0200-M1 \*\*\* 2,2 \*\*\*
UNDERFLOW PUMP

- -

MANUFAC TURER

LOCAL

330-370-0300

EQUIPMENT TYPE

PUMP

SERVICE

OVERFLOW PUMP FOR SULPHUR WASHING WASTE WATER THICKENER

CAPACITY HEAD WEIGHT

15 M3/H 20 M APPRCX. 0.2 T

CVERFLOW PLMP

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*330-370-0300-M1 \*\*\* 2,2 \*\*\*

MANUF AC TUR ER

LUCAL

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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DUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

330-370-0400

EQUIPMENT TYPE

**PUMP** 

SERVICE

OVERFLOW PUMP FOR SULPHUR WASHING WASTE WATER THICKENER

CAPACITY HEAD WEIGHT 15 M3/H 20 M APPRGX. 0,2 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*330-370-0400-M1 \*\*\* 2,2 \*\*\*

OVERFLOW PUMP

MANUFACTURER

LOCAL

330-375-0100

EQUIPMENT TYPE

VACUUM PUMP

CAPACITY VACUUM WEIGHT

4,5 M3/MIN UNDER PRESSURE 600 MM HG APPRCX. 0,2 T

MOTOR NO./RATING (Kw) MOTOR TITLE

\*\*\*330-375-0100-M1 \*\*\* 11 \*\*\*
VACUUM PUMF

MANUFACTURER

LCCAL

330-510-0100

EQUIPMENT TYPE

TANK

SERVICE

COOLING TANK FOR WASTE LIQUID

VOLUME WEIGHT MATERIAL 5 M3 APPROX. 1 T ACID PROOF STEEL

MANUFACTURER

FOREIGN

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

330-510-0200

330-518-0100

330-518-0200

EQUIPMENT TYPE

EQUIPMENT TYPE

EQUIPMENT TYPE TANK

SERVICE SULPHURIC ACID TANK

VOLUME 3 M3
WEIGHT APPROX. O. E T
MATERIAL CARBON STEEL

MANUFACTURER LOCAL

SERVICE UNDERFLOW PUMP TANK

PUMP TANK

PUMP TANK

VOLUME 5 M3
WEIGHT APPROX. 0, 7 T
MATERIAL ACID PROOF STEEL

MANUFACTURER FOREIGN

SERVICE CVERFLOW PUMP TANK

VOLUME 15 M3
WEIGHT APPRCX. 2, 0 T
MATERIAL ACID PROOF STEEL

MANUFACTURER FOREIGN

OUTDKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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OUTOKUMPU NO :360 100 900 001 ALT1

DESIGN :AKI

CLIENT NO :

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330-521-0100

EQUIPMENT TYPE

REACTOR TANK

VOLUME WEIGHT MATERIAL 3 M3 APPRCX. 3,5 T

BRICKLINING AND RUBBER LINING

MANUFAC TURER

LOCAL

330-532-0100

EQUIPMENT TYPE

THICKENER

**DIMENSIONS** 

DIAMETER 3500 MM

VOLUME MATERIAL S M3

STEEL , RUBBERIZED

WEIGHT

APPROX. 4 T

MOTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*330-532-0100-M1 \*\*\* 2 \*\*\*

THICKENER

\*\*\*330-532-0100-M2 \*\*\* 0,75 \*\*\*

THICKENER

MANUFAC TUPER

LOCAL

500----0

EQUIPMENT TYPE

COAL PLANT AREA

OUTOKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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DESIGN :AKI

CLIENT ND:
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500-118-0100

500-118-0200

500-118-0300

EQUIPMENT TYPE

EQUIPMENT TYPE STORAGE BIN

SERVICE RAW COAL STORAGE BIN

CAPACITY 400 M3

MATERIAL CARBON STEEL

WEIGHT APPROX. 60 T

MANUFACTURER LOCAL

SERVICE RAW COAL STORAGE BIN

STORAGE BIN

VOLUME 400 M3

MATERIAL CARBON STEEL

WEIGHT APPRCX. 60 T

MANUFACTURER LOCAL

EQUIPMENT TYPE STORAGE BIN

SERVICE FOR PULVERIZED COAL

CAPACITY 400 M3

MATERIAL CARBON STEEL

WEIGHT APPRCX. 60 T

MANUFACTURER LOCAL

OUTOKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT NO :
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500-118-0400

EQUIPMENT TYPE

\_\_\_\_

STORAGE BIN

SERVICE

FOR SUPERHEATER COAL

CAPACITY

20 M3

MATERIAL

CARBON STEEL

WEIGHT

APPROX. 6 T

MANUFACTURER

LOCAL

500-133-0100

**EQUIPMENT TYPE** 

OIL BURNER

SERVICE

START UP BURNER FOR AIR PREHEATER

WEI GHT

APPROX. 0,5 T

MANUFACTURER

LOCAL

500-167-0100

EQUIPMENT TYPE

BELT CONVEYOR

SERVICE

RAW COAL TRANSPORT TO STORAGE BINS

CAPACITY

200 T/H

MAIN DIMENSIONS

LENGTH: 75 M

BELT WIDTH BELT INCLINE WEIGHT 800 MM 12 DEGREES APPRCX. 6 T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*500-167-0100-M1 \*\*\* 45 BELT CONVEYOR

MANUFACTUFER

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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OUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO:
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500-167-0200

EQUIPMENT TYPE

TYPE SERVICE BELT CONVEYOR

REVERSIBLE
RAW COAL TRANSPORT TO STORAGE BINS

CAPACITY

MAIN DIMENSIONS

200 T/H

LENGTH: 90 00 MM

BELT WIDTH

**BELT INCLINE** 

NONE

800 MM

WEIGHT

MOTOR NO./RATING (KW) MOTOR TITLE

MANUFACTURER

APPRCX. 1 T

\*\*\*500-167-0200-M1 \*\*\* 7.5 \*\*\*
BELT CONVEYOR

LOCAL

500-170-0100

EQUIPMENT TYPE

SERVICE

PNEUMATIC CONVEYOR SYSTEM

TRANSPORT OF PULVERIZED COAL TO

1 1 1

FEED BINS

INCLUDING FEEDERS, PIFING, DUST SEPARATION EQ.

C AP AC ITY WEIGHT

MANUFACTURER

30 T/H APPRCX. 8 T

FOR E IGN

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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CLIENT : PPCL DOCUMENT: EQUIPMENT LIST (ATNB) OUTOKUMPU NO :360 100 900 001 ALT1 DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

500-170-0200

EQUIPMENT TYPE

PNEUMATIC CONVEYOR SYSTEM

SERVICE

TRANSPORT OF PULVERIZED COAL TO COAL BURNERS OF SUPERHEATER

INCLUDING

BIN DISCHARGERS, ROTOR SCALES, PIPING 5 T/H APPROX. 8 T

CAPACITY WEIGHT

MANUFACTURER

FOREIGN

500-179-0100

EQUIPMENT TYPE

CGAL INJECTION SYSTEM

SERVICE

COAL INJECTION TO FLASH SMELTING FURNACE

INCLUDING

STORAGE INJECTORS, BIN DISCHARGERS PRIMARY INJECTORS, TUYERS, BINS

CAPACITY WEIGHT

25 T/H

MANUFACTURER

APPFCX. 12 T

500-202-0100

FOREIGN

ECUIPMENT TYPE

FEED HOPPER

SERVICE

RAW COAL FEED

VOL UME WEIGHT MATERIAL 20 M3

APPREX. 1.5 T CARBON STEEL

MANUFACTURER

DUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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CLIENT : PPCL DECUMENT: EQUIPMENT LIST (ATNB) CUTOKUMPU NO :360 100 900 001 ALT1 DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

500-212-0100

EQUIPMENT TYPE

FAN

TYPE SERVICE

CENTRIFUGAL HOT AIR SYSTEM FOR MILLS

WEIGHT

APPRCX. O. E T

MOTOR NO. / RATING (KW) MOTOR TITLE

\*\*\* 500-212-0100-M1\*\*\* 30 \*\*\* FAN

M AN UF AC TUR ER

500-212-0200

EQUIPMENT TYPE

FAN

TYPE SERVICE CENTRIFUGAL EXHAUST FAN

CAPACITY

GAS FLOW: EO OOO NM3 PRESSURE: 7 KPA

WEIGHT

APPRCX. 5 T

MOTOR NO. / FATING (KW)

\*\*\* 500-212-0200-M1\*\*\* 250 \*\*\*

MOTOR TITLE

FAN

MANUFAC TURER

DUTOKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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DEPARTMENT : PROJECT

CLIENT :PPCL

DOGUMENT: EQUIPMENT LIST (ATNB)

OUTOKUMPJ NO :360 100 900 001 ALT1

DESIGN : AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

500-212-0300

EQUIPMENT TYPE

EXHAUST AIR FAN

SERVICE

FOR PNEUMATIC CONVEYOR SYSTEM

WEIGHT

APPROX. 0.3 T

MOTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*500-212-030-M1 \*\*\*- 22 \*\*\*

FAN

MANUFACTURER

**FOREIGN** 

500-212-0400

EQUIPMENT TYPE

FAN

SERVICE

EXHAUST AIR FAN FOR PNEUMATIC

CONVEYOR SYSTEM.

WEIGHT

APPROX. 0.2 T

MCTOR NO. / FATING (KW)

\*\*\*500-212-0400-M1 \*\*\* 11 \*\*\*

MANUFACTURER

FOREIGN

500-216-0100

EQUIPMENT TYPE

AIR LOCK FEEDER

SERVICE

COAL BIN DISCHARGER

CAPACITY WEIGHT MATERIAL FLOW: 30 T/H APPFOX. 0.1 T

MOTER NO./FATING (KW) MOTER TITLE

###500-216-0100-M1 ### 2+2 ### AIR LOCK FEEDER

MANUFACTUR ER

OUTCKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 101 DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
GUTGKUMPU NO :360 100 900 001 ALTI
DESIGN :AKI

CLIENT NO:
REVISION:5 DATE:22.08.85

500-216-0200

EQUIPMENT TYPE

AIR LOCK FEEDER

SERVICE

COAL BIN DISCHARGER

CAPACITY WEIGHT MATERIAL FLOW: 30 T/H APPROX. 0,1 T

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*500-216-0200-M1 \*\*\* 2,2 \*\*\*

AIR LOCK FEEDER

M AN UF AC TUR ER

LOCAL

500-218-0100

EQUIPMENT TYPE

BELT FEEDER

SERVICE

RAW COAL FEED

CAPACITY

200 T/H

BELT LENGTH BELT WIDTH BELT INCLINE WEIGHT 5000 MM 1000 MM HORIZENTAL APPROX. 3,5 T

MOTOR NO./FATING (KW)

\*\*\*500-216-0100-M1 \*\*\* 7.5 \*\*\*
BELT FEEDER

MANUF ACTUF ER

GUTOKUMPU DYZENGINE ERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 102 DEPARTMENT : PROJECT

CLIENT : PPCL DOCUMENT: EQUIPMENT LIST (ATNB) OUT OKUMPU NO :360 100 900 001 ALT1 DES IGN : AK I

CLIENT NG : REVISION :5 DATE :22.08.85

500-223-0100

EQUIPMENT TYPE

SERVICE

DRAG FEEDER

FEEDING COAL MILL

CAPACITY

MAIN DIMENSIONS

WEIGHT

6...30 T/H

LENGTH: 60 CO MM WIDTH: 100C MM APPRCX. 5 T

MOTOR NO./RATING (KW) MOTOR TITLE

MANUFACTURER

\*\*\*500-223-0100-M1 \*\*\* 7.5 \*\*\*

DRAG FEEDER

FORE IGN

500-223-0200

EQUIPMENT TYPE

SERVICE

DRAG FEEDER

FEEDING COAL MILL, STAND-BY

CAPACITY

MAIN DIMENSIONS

WEIGHT

6...30 T/H

LENGTH: 60 CO MM WIDTH: 100C MM APPREX. 5 I

MOTOR NO./RATING (KW) MOTOR TITLE

MANUFACTURER

\*\*\*500-223-0200-M1 \*\*\* 7.5 \*\*\*

DRAG FEEDER

FOREIGN

500-281-0100

EQUIPMENT TYPE

PREHEATER

AIR PREHEATER HOT AIR SYSTEM FOR MILLS

SERVICE

TYPE

STEEL MANTLE, REFRACTORY CASTABLE

APPROX. 4 T (TOTAL)

MANUFACTURER FOREIGN

MATERIAL

WEIGHT

BUT OKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 103 DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: EQUIPMENT LIST (ATNB) OUT OKUMPU NC :360 100 900 001 ALT1

DES IGN

: AK I

CLIENT NC :

REVISION :5 DATE :22.08.85

500-325-0100

EQUIPMENT TYPE

SERVICE

CAPACITY WEIGHT

CONSTRUCTION

MILL

COAL MILL

30 T/H

APPRCX. 35 I

VERTICAL POSITION

MOTOR NO./RATING (KW)

MOTOR TITLE

MANUFAC TUFER

\*\*\*500-325-0100-M1 \*\*\* 315

MILL

FOREIGN

500-325-0200

EQUIPMENT TYPE

SERVICE

CAPACITY WEIGHT

CCNSTRUCTION

MILL

CGAL MILL (STAND BY)

30 T/H

APPRCX. 35 T

VERTICAL PESITION

MOTOR NO./RATING (KW)

MOTOR TITLE

MANUF AC TUF ER

\*\*\*500-325-0200-M1 \*\*\* 315 \*\*\*

MILL

**FOREIGN** 

500-411-0100

EQUIPMENT TYPE

SERVICE

VIBRATING SCREEN

FOR PULVERIZED COAL

CAPACITY

WEIGHT

MOTOR NO. / FATING (KW)

MOTOR TITLE

MANUFAC TUFER

30 T/H APPRCX. 2 T

\*\*\*500-411-0100-M1 \*\*\* 2,2 \*\*\*

VIERATING SCREEN

FOREIGN

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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CLIENT : PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

OUTOKUMPU NO :360 100 900 001 ALTI

DESIGN :AKI

CLIENT NO :

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500-411-0200

EQUIPMENT TYPE

VIBRATING SCREEN

SERVICE

FOR PULVERIZED COAL

C & P A C I T Y WEIGHT 30 T/H APPFCX. 2 T

MCTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*500-411-0200-M1 \*\*\* 2.2 \*\*\*

VIBRATING SCREEN

MANUFAC TUPER

**FOREIGN** 

500-417-0100

EQUIPMENT TYPE

BAG FILTER

SERVICE

COAL DUST SEPARATION

WEIGHT

APPROX. 5.5 T

MANUFACTURER

FORE IGN

500-419-0100

EQUIPMENT TYPE

CYCLONE

SERVICE

FOR COAL DUST SEPARATION

WEIGHT

APPECX. 3 T

MANUFACTURER

FORE IGN

600----0

EQUIPMENT TYPE

POWER PLANT AREA

OUTOKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 105 DEP AR TMENT : PROJECT

CLIENT :PPCL DOCUMENT: EQUIPMENT LIST (ATNB) OUT GKUMPU NO :360 100 900 001 ALT1

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CLIENT NO :

REVISION :5 DATE :22.08.85

600-122-0100

EQUIPMENT TYPE

AUXILIARY ECILER

SERVICE

DESIGN

HEATING OF SULPHUR PLANT IN START-UP AND SHUT-DOWN CASES

CAPACITY

SATURATED STEAM 15 T/H

WEIGHT

APPRCX. 60 T

MANUFACTURER

LUCAL

600-123-0100

EQUIPMENT TYPE

SUPERHEATING BOILER

SERVICE

SUPERHEAT WASTE HEAT BOILER STEAM

CAPACITY

SUPERHEATED STEAM: 100 T/H

PRESSURE

65 BAR

TEMPERATURE

480 DEGREES C.

WEIGHT

FUEL: CDAL IN START-UP LIGHT DIL

APPFCX. 15C T

MANUFACTURER

LCCAL

600-276-0100

EQUIPMENT TYPE

CONDENSER

TYPE

DUMP CONDENSER

SERVICE

CONDENSING OF TURBCALTERNATOR

STEAM

CAPACITY

100 T/H

MANUFACTURER

LUCAL

DUTCKUMPU CY/ENGINEERING DIVISION PREJECT : PPCL PYFITE SMELTER

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CLIENT : PPCL

DOCUMENT: EQUIPMENT LIST (ATNB)

OUTOKUMPU NO :360 100 900 001 ALT1

DESIGN : AK I CLIENT NO :

REVISION :5 DATE :22.08.85

600-280-0100

EQUIPMENT TYPE

HEAT EXCHANGER

SERVICE

PREHEATING OF BOILER FEED WATER

CAPACITY

20 T/H

MANUE ACTUR ER

LOCAL

600-280-0200

EQUIPMENT TYPE

HEAT EXCHANGER

SERVICE

COCLING OF LEW PRESSURE(1.78AR)

BCILERS FEED WATER.

CAPACITY

20 T/H

MANUFAC TURER

LUCAL

600-376-0100

EQUIPMENT TYPE

CONDENSATE PUMP

SERVICE

PUMPING OF TURBOALTERNATOR

CONDENSATE.

CAPACITY

HEAD

WEIGHT

100 T/H 50 M

APPRCX. 0,5 T

MCTOR NO./FATING (Km)

MOTOR TITLE

MANUFACTUFER

\*\*\*600-376-0100-M1 \*\*\* 22

CONDENSATE PUMP

GUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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DOCUMENT: EQUIPMENT LIST (ATNB)

DUTOKUMPU NO :360 100 900 001 ALT1

DESIGN :AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

600-376-0200

EQUIPMENT TYPE

CONDENSATE PUMP

SERVICE

PUMPING OF SULPHUR PLANT

BUILER CONCENSATE.

CAPACITY HEAD WEIGHT 50 T/H 50 M

APPEGX. 0.5 T

MOTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*600-376-0200-M1 \*\*\* 22 \*\*\*

CONDENSATE PUMP

MANUFACTURER

LOCAL

600-376-0300

EQUIPMENT TYPE

CCNDENSATE PUMP

SERVICE

FEED WATER PUMP FOR WASTE

HEAT BOILER.

CAPACITY HEAD WEIGHT

140 T/H 800 M

APPEGX. 2 T

MOTOR NO./FATING (KM)

MOTOR TITLE

\*\*\*600-376-0300-M1 \*\*\* 400

CONDENSATE PUMP

MANUFACTURER

CUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

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DESIGN :AKI

CLIENT ND : REVISION :5 DATE :22.08.85

600-376-0400

EQUIPMENT TYPE

CONDENSATE PUMP

SERVICE

FEED WATER PUMP FOR WASTE HEAT BOILER (STAND-BY)

CAPACITY HEAD WEIGHT 120 T/H 800 M APP&CX.1.5 T

MANUFAC TUR ER

LOCAL

REMARKS

TURBINE DRIVEN

600-376-0500

EQUIPMENT TYPE

CONDENSATE PUMP

SERVICE

FEED WATER PUMP FOR SULPHUR PLANT BOILERS.

CAPACITY HEAD WEIGHT 75 T/H 75 M APPREX.0.4 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*600-376-0500-M1 \*\*\* 30 \*\*\*
FEED WATER PUMP

MANUF ACTUF ER

PROJECT : PPCL PYRITE SMELTER

CUTOKUMPU DY/ENGINEERING DIVISION DATE :85-08-28 PAGE NO: 109 DEPARTMENT : PROJECT

CLIENT :PPCL DCCUMENT: EQUIPMENT LIST (ATNB) QUTOKUMPU NG :360 100 900 001 ALT1 :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

600-376-0600

EQUIPMENT TYPE

CONDENSATE PUMP

TYPE SERVICE TURBINE DRIVEN FEED WATER PUMP FOR SULPHUR PLANT BOILERS (STAND-BY)

CAPACITY HEAD WELGHI

75 T/H 75 M APPREX.0.4 T

MANUFACTUR ER

LOCAL

600-376-0700

EGUIPMENT TYPE

CCNDENSATE PUMP

SERVICE

FEED WATER PUMP FOR AUXILIARY BCILER

CAPACITY HEAD WEIGHT

20 T/H 130 M APPREX.0.4 T

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*600-376-0700-M1 \*\*\* 15 FEED WATER PUMP

MANUFAC TUFER

DUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

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CLIENT :PPCL

DOCUMENT: EQUIPMENT LIST (ATNB) OUT OKUM PU NO :350 100 900 001 ALT1

DESIGN :AKI CLIENT NO :

REVISION :5 DATE :22.08.85

600-514-0100

EQUIPMENT TYPE

FEED TANK

TYPE SERVICE

FEED WATER TANK FOR WASTE HEAT BOILER AND SULPHUR PLANT BOILERS.

CAPACITY

**VOLUME: 175 M3** 

WELGHT

PRESSURE: 5 BAR APPRCX. 100 T

M ANUF ACTUFER

LOCAL

600-556-0100

EQUIPMENT TYPE

TURBCALTERNATOR

TYPE SERVICE

CONDENSATE TYPE TURBINE PRODUCTION OF ELECTRIC POWER

CAPACITY

25 MW ELECTRIC POWER

MANUFACTURER

FOREIGN

OUT OKUMPU CYZENGINE ERING DIVISION DATE :85-08-28 PAGE NO: 111 PROJECT : PPCL PYRITE SMELTER

DEPARTMENT : PROJECT

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OUT OKUMPU NO :360 100 900 001 ALT1

DES IGN

:AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

700----0

EQUIPMENT TYPE

DXYGEN PLANT AREA

MANUF ACTURER FOREIGN

800----0

EQUIPMENT TYPE

LIME STONE SLURRY PREPARATION

MANUFACTUFER LOCAL

900---0

EQUIPMENT TYPE

WATER TREATMENT AREA

OUTOKUMPU OY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE: 85-08-28 PAGE NO: 112 DEPARTMENT: PROJECT

CLIENT :PPCL
DOCUMENT:EQUIPMENT LIST (ATNB)
OUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO:
REVISION :5 DATE :22.08.85

950----0

EQUIPMENT TYPE

COMPRESSED AIR STATION

MANUF AC TUR ER

LCCAL

4.3.2 Motor List

In Volume II

CUTOKUMPU CY'ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 1 DEPARTMENT :PROJECT

CLIENT :PPCL
DOCUMENT:MCTOR LIST (B)
OUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

200----0

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EQUIPMENT TYPE

FLASH SMELTER AREA

210----0

EQUIPMENT TYPE

DRYER AND FSF FEED AREA

210-116-0100

EQUIPMENT TYPE

CONCENTRATE DAY BIN

210-116-0200

EQUIPMENT TYPE

CONCENTRATE DAY BIN

210-116-0300

EQUIPMENT TYPE

CENCENTRATE DAY BIN

210-116-0400

EQUIPMENT TYPE

DAY BIN

210-117-0100

EQUIPMENT TYPE

DRIED CHARGE BIN

210-117-0200

EQUIPMENT TYPE

DRIED CHARGE BIN

OUTCKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 2
DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:MOTOR LIST (B)
DUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT ND:
REVISION:5 DATE:22.08.85

210-167-0100

EQUIPMENT TYPE

BELT CONVEYOR

MOTOR NO./FATING (KW) --MOTOR TITLE \*\*\* 210-167-0100-M1\*\*\* 4 \*\*\*
BELT CCNVEYOR

210-167-0200

EQUIPMENT TYPE

BELT CONVEYOR

MCTOR NO./RATING (KW) MCTOR TITLE

210-167-0300

EQUIPMENT TYPE

BELT CONVEYOR

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*210-167-0300-M1 \*\*\* 3.0 \*\*\*

BELT CONVEYOR

210-166-0100

EQUIPMENT TYPE

DRAG CONVEYOR

MCTOR NO./RATING (KW) MOTOR TITLE

\*\*\*210-168-0100-M1 \*\*\* 7.5 \*

DRAG CONVEYOR

210-168-0200

EQUIPMENT TYPE

DRAG CONVEYOR

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*210-168-0200-M1 \*\*\* 7.5 \*\*\*

DRAG CONVEYOR

DUTCKUMPU CY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 3
DEPARTMENT:PROJECT

CLIENT :PPCL
DCCUMENT:MCTCR LIST (B)
CUTOKUMPU NG :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

210-170-0100

EQUIPMENT TYPE

PNEUMATIC CONVEYOR SYSTEM

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\* 210-170-0100-M1 \*\*\* 132 \*\*\*
AIR 8LOWER

\*\*\*210-170-0100-M2 \*\*\* 132 \*\*\*
AIR BLOWER STAND BY

\*\*\*210-170-0100-M3 \*\*\* 1,1 \*\*\*
AIR LOCK

\*\*\*210-170-0100-M4 \*\*\* 1,1
AIR LOCK

\*\*\*210-170-0100-M5 \*\*\* 5 \*\*\*

KETURN AIR FAN

210-194-0100

EQUIPMENT TYPE

MULTICOIL DRYER

MOTOR NO./RATING (KW)
MOTOR TITLE

\*\*\* 210-194-0100-M1\*\*\* 160 \*\*\*
MULTICGIL DRYER

210-194-0200

EQUIPMENT TYPE

MULTICOIL DRYER

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*210~194~0200~M1 \*\*\* 160 \*\*\*
MULTICCIL CRYER

210-212-0130

EQUIPMENT TYPE

EXHAUST AIR FAN

MOTOR NO./RATING (Km) MOTOR TITLE

\*\*\*210-212-0100-M1 \*\*\* 45 \*\*\* EXHAUST AIR FAN

210-218-0100

EQUIPMENT TYPE

BELT FEEDER FOR CONCENTRATE

MCTOR NO./RATING (KW) — MCTOR TITLE

1 1

\*\*\* 210-218-0100-M1\*\*\* 7,5 \*\*\* BELT FEEDER DUTOKUMPU CY/ENGINEERING DIVISION PROJECT :PPCL PYFITE SMELTER

DATE:85-08-28 PAGE NO: 4
DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:MOTOR LIST (B)
GUTOKUMPU NO :360 100 900 001 ALTI
DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

210-218-0200

EQUIPMENT TYPE

BELT FEEDER FOR CONCENTRATE

MOTOR NO./RATING (KW) MOTOR TIPLE

\*\*\* 210-218-0200-M1\*\*\* 7,5 \*\*\*

BELT FEEDER

210-218-0300

EQUIPMENT TYPE

BELT FEEDER FOR CONCENTRATE

MCTOR NC./PATING (KW) MCTOR TITLE

\*\*\* 210-218-0300-M1\*\*\* 7,5 \*\*\* BELT FEEDER

210-218-0400

EQUIPMENT TYPE

BELT FEEDER

MCTER NO./RATING (KW) MCTER TITLE

\*\*\*210-218-0400-M1 \*\*\* 3,0 \*\*\* BELT FEEDER

210-411-0100

EQUIPMENT TYPE

VIBRATING SCREEN

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*210-411-0100-M1 \*\*\* 15 \*\*\* VIEFATING SCREEN

210-417-0100

EQUIPMENT TYPE

BAG FILTER

2 2 3 --- - 0

EQUIPMENT TYPE

FLASH SMELTING FURNACE AREA

220-108-0100

EQUIPMENT TYPE

GRANULATION BASIN

OUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE: 85-08-28 PAGE NO: 5

DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: MCTOR LIST (B)

DUTCKUMPU NO :360 100 900 001 ALT1

DESIGN : AKI

CLIENT NO :

FEVISION :5 DATE :22.08.85

220-108-0200

EQUIPMENT TYPE

GRANULATION BASIN

220-131-0100

EQUIPMENT TYPE

COAL DUST BURNER

220-131-0200

EQUIPMENT TYPE

CCAL DUST BURNER

223-131-0300

EQUIPMENT TYPE

COAL DUST BURNER

220-131-0400

EQUIPMENT TYPE

COAL DUST BURNER

220-131-0500

EQUIPMENT TYPE

COAL DUST BURNER

220-131-0600

EQUIPMENT TYPE

CCAL DUST BURNER

220-133-0100

EQUIPMENT TYPE

AUXILIARY BURNER

CUTOKUMPU CY/ENGINEERING DIVISION DATE :85-08-28 PAGE NO: PROJECT : PPCL PYRITE SMELTER

DEP AT TMENT : PROJECT

CLIENT :PPCL DECUMENT: MOTOR LIST (B) QUT CKUMPU NO :360 100 900 001 ALT1 DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

220-133-0200

EQUIPMENT TYPE

AUXILIARY BURNER

220-140-0100

EQUIPMENT TYPE

SLAG LAUNDER WITH COVERS

220-140-0200

EQUIPMENT TYPE

SLAG LAUNDER WITH COVERS

220-140-0300

EQUIPMENT TYPE

SLAG LAUNDER WITH COVERS

220-140-0400

EQUIPMENT TYPE

SLAG LAUNDER WITH COVERS

220-140-0500

EQUIPMENT TYPE

GRANULATION LAUNDER

220-140-0600

EQUIPMENT TYPE

GRANULATION LAUNDER

220-167-0100

EQUIPMENT TYPE

BELT CONVEYOR

MOTCH NO. / FATING (KW) MOTOR TITLE

\*\*\*220-167-0100-M1 \*\*\*11

\*\*\*

BELT CONVEYOR

DUTCKUMPU CY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 7
DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:MOTOR LIST (B)
OUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO :
REVISION :5 DATE :22.08.85

220-174-0100

EQUIPMENT TYPE RAKE CLASSIFIER

MCTOR NC./RATING (KW) ###220-174-0100-M1 \*\*\* 11 \*\*\*
MGTOR TITLE RAKE CLASSIFIER

220-174-0200

EQUIPMENT TYPE RAKE CLASSIFIER

METOR NG./RATING (Kw) \*\*#220-174-0200-MI \*\*\* 11 \*\*\*
MOTOR TITLE RAKE CLASSIFIER

220-198-0100

EQUIPMENT TYPE GAS DUCTWORK

220-198-0200

EQUIPMENT TYPE GAS DUCTWORK

220-212-0100

ECUIPMENT TYPE PROCESS AIR FAN

MOTOR NO./RATING (KW) ### 220-212-0100-M1\*\*\* 160 ###
MOTOR TITLE PROCESS AIR FAN

220-212-0200

EQUIPMENT TYPE PROCESS AIR FAN

MOTOR NC./RATING (KW) ### 220-212-0200-M1### 160 ###
MOTOR TITLE PROCESS AIR FAN

220-212-0300

EQUIPMENT TYPE COMBUSTION AIR FAN

METOR NO./FATING (KW) ###220-212-0300-MI\*\*\* 110 ###
METOR TITLE CCMBUSTION AIR FAN

CUTCKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: DEPARTMENT : PROJECT

CLIENT : PPCL DOCUMENT: MOTOR LIST (B) CUTOKUMPU NO :360 100 900 001 ALT1 DESIGN : AK I

CLIENT NO : REVISION :5 DATE :22.08.85

220-223-0100

EQJIPMENT TYPE

DRIED CHARGE DRAG FEEDER

MOTOR NO./RATING (Km) MOTOR TITLE

\*\*\*220-223-0100-M1 \*\*\* 11 \*\*\* DRAG FEEDER

220-223-0230

EQUIPMENT TYPE

DRIED CHARGE DRAG FEEDER

MOTOR NO. /RATING (KW) MOTOR TITLE

\*\*\*220-223-0200-M1 \*\*\* 11 \*\*\*

DRAG FEEDER

220-261-0100

EQUIPMENT TYPE

FLASH SMELTING FURNACE

220-289-0100

ECUIPMENT TYPE

JACKET WATER HEAT EXCHANGER

220-289-0200

EQUIPMENT TYPE

JACKET WATER HEAT EXCHANGER

220-289-0300

EQUIPMENT TYPE

SPRAY WATER HEAT EXCHANGER

220-289-0400

EQUIPMENT TYPE

SPRAY WATER HEAT EXCHANGER

DUTCKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 9
DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:MCTOR LIST (B)
OUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NG:
REVISION :5 DATE :22.08.85

220-318-0100

EQUIPMENT TYPE

CVERHEAD TRAVELLING CRANE

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*220-318-0100-M1 \*\*\* 11 \*\*\*

OVERHEAD TRAVELLING CRANE

\*\*\*220-318-0100-M2 \*\*\* 2.2 \*\*\*

CVERHEAD TRAVELLING CRANE

\*\*\*220-318-0100-M3 \*\*\* 1.1 \*\*\*

CVERHEAD TRAVELLING CRANE

220-376-0100

EQUIPMENT TYPE

JACKET WATER PUMP

MOTOR NO./RATING (KW)
MOTOR TITLE

\*\*\*220-376-0100-M1 \*\*\*200 \*\*\*

JACKET WATER PUMP

220-376-0200

EQUIPMENT TYPE

JACKET WATER PUMP

MOTOR NO./RATING (KW) MCTOR TITLE ###220-376-0200-M1 ###200 ### JACKET water PUMP

220-376-0400

EQUIPMENT TYPE

SPRAY WATER PUMP

METOR NO./FATING (KW) MOTOR TITLE

\*\*\*220-376-0400-M1 \*\*\* 90 \*\*\*
SPRAY WATER PUMP

220-376-0500

EQUIPMENT TYPE

SPF AY WATER PUMP

MCTOR NO./RATING (KW)

\*\*\*220-376-0500-M1 \*\*\* 90 \*\*\*
SPFAY WATER PUMP

220-376-0700

EQUIPMENT TYPE

GRANULATION WATER PUMP

MCTOR NO./RATING (KW) MCTOR TITLE \*\*\*220-376-0700-M1 \*\*\* 90 \*\*\*
GRANULATION WATER PUMP

CUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE:35-08-28 PAGE NO: 10 DEPARTMENT : PROJECT

CLIENT :PPCL
DOCUMENT:MOTOR LIST (B)
DUTOKUMPU NG :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO:
REVISION :5 DATE: 22.08.85

220-376-0800

EQUIPMENT TYPE GRANULATION WATER PUMP

MOTOR NG./FATING (KW) ###220-376-0800-MI ### 90 ###
MOTOR TITLE GRANULATION WATER PUMP

220-376-0900

EQUIPMENT TYPE GRANULATION WATER PUMP

220-435-0100

EQUIPMENT TYPE CONCENTRATE BURNER

220-519-0100

EQUIPMENT TYPE JACKET WATER TANK

220-519-0200

EQUIPMENT TYPE SPRAY WATER TANK

220-519-0300

EQUIPMENT TYPE CIL TANK

220-519-0400

EQUIPMENT TYPE CIL TANK

220-569-0130

EQUIPMENT TYPE EMERGENCY DAMPER BETWEEN FSF-WHB

DUTOKUMPU DY/ENGINEERING DIVISION DATE :85-08-28 PAGE NO: 11 PROJECT : PPCL PYFITE SMELTER

DEPARTMENT : PROJECT

CLIENT : PPCL DOCUMENT: MCTOR LIST (B)

OUT OKUMPU NO :360 100 900 001 ALT1

DESIGN :AKI CLIENT NO :

REVISION :5 DATE :22.08.85

230----0

EQUIPMENT TYPE

PROCESS GAS HANDLING AREA

230-124-0100

EQUIPMENT TYPE

MASTE HEAT BCILER

230-198-0100

EQUIPMENT TYPE

GAS DUCTION

230-212-0100

EQUIPMENT TYPE

PROCESS GAS FAN

MOTOR NO. /FATING (KW)

MOTOR TITLE

\*\*\*230-212-0100-M1 \*\*\* 250 \*\*\*

PROCESS GAS FAN

230-212-0200

EQUIPMENT TYPE

PROCESS GAS FAN

MOTOR NO. / FATING (KW)

MOTOR TITLE

\*\*\*230-220-0200-M1 \*\*\* 250 \*\*\*

PROCESS GAS FAN

230-372-0100

EQUIPMENT TYPE

EJECTOR

230-372-0200

EQUIPMENT TYPE

EJECTOR

230-372-0300

EQUIPMENT TYPE

**EJECTOR** 

CUTCKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 12 DEPARTMENT : PROJECT

CLIENT : PPCL DOCUMENT: MOTOR LIST (B) QUTCKUMPU NG :360 100 900 001 ALT1 DESIGN :AKI

CLIENT NG : REVISION :5 DATE :22.08.85

230-376-0100

EQUIPMENT TYPE

MATER PUMP

METER NO./RATING (KW) MOTOR TITLE

\*\*\* 230-376-0100-M1 \*\*\* 200 \*\*\* WHB CIRCULATION WATER PUMP

230-376-0200

EQUIPMENT TYPE

WATER PUMP

230-421-0100

EQUIPMENT TYPE

ELECTROSTATIC PRECIPITATOR

MCTOR NO. /RATING (KW) MOTOR TITLE

\*\*\* SEVERAL.TOTAL \*\*\* 90 \*\*\*

230-421-0200

EQUIPMENT TYPE

ELECTROSTATIC PRECIPITATOR

MOTOR NO./FATING (KW)

MOTOR TITLE

\*\*\* SEVERAL, TOTAL \*\*\* 90 \*\*\*

230-562-0100

EQUIPMENT TYPE

DISC VALVE

2 30 - 562 - 0200

EQUIPMENT TYPE

DISC VALVE

240----0

EQUIPMENT TYPE

FLUE DUST HANDLING AREA

DUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 13 DEPARTMENT :PROJECT

CLIENT :PPCL
DOCUMENT:MOTOR LIST (B)
DUTOKUMPU NO :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO:
REVISION :5 DATE :22.08.85

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240-140-0100

EQUIPMENT TYPE

LAUNDER

240-168-0100

EQUIPMENT TYPE

DRAG CONVEYOR FOR WHB DUST

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*240-168-0100-M1 \*\*\* 5,5 \*\*\*
DRAG CONVEYOR FOR WHB DUST

240-168-0200

EQUIPMENT TYPE

DRAG CONVEYOR FOR EP DUST

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*240-168-0200-M1 \*\*\* 3
DRAG CONVEYOR FOR EP DUST

240-168-0300

EQUIPMENT TYPE

DRAG CONVEYOR FOR EP DUST

MOTOR NO./RATING (KW) --MOTOR TITLE \*\*\*240-168-0300-M1 \*\*\* 3 \*\*\*
DRAG CONVEYOR FOR EP DUST

240-168-0400

EQUIPMENT TYPE

DRAG CONVEYOR FOR EP DUST

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*240-168-0400-M1 \*\*\* 3
DRAG CONVEYOR FOR EP DUST

240-168-0500

EQUIPMENT TYPE

DRAG CONVEYOR FOR EP DUST

METOR NG./FATING (KW) METER TITLE \*\*\*240-168-0500-M1 \*\*\* 3 \*\*\*
DFAG CONVEYOR FOR EP DUST

240-209-0100

WATER LOCK

EQUIPMENT TYPE

OUTCKUMPU OY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 14 DEPARIMENT : PROJECT

CLIENT :PPCL DOCUMENT: MOTOR LIST (B)

OUTOKUMPU NO :360 100 900 001 ALTI

DESIGN :AKI CLIENT NO :

DATE :22.08.85 REVISION :5

240-209-0200

EQUIPMENT TYPE

WATER LOCK

240-209-0300

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EQUIPMENT TYPE

WATER LOCK

240-209-0400

EQUIPMENT TYPE

WATER LOCK

240-209-0500

EQUIPMENT TYPE

MATER LOCK

240-374-0300

EQUIPMENT TYPE

SLURRY PUMP

MOTOR NO./RATING (KW)

MCTOR TITLE

\*\*\*240-374-0300-M1 \*\*\* 7.5 \*\*\*

SLURRY PUMF

240-374-0400

EQUIPMENT TYPE

SLURRY PUMP

MCTOR NO./FATING (KW)

METER TITLE

\*\*\*240-374-0400-M1 \*\*\* 7.5 \*\*\*

SLUKRY PUMP

240-376-0100

EQUIPMENT TYPE

WATER PUMP

MOTER NO./RATING (KW)

MOTOR TITLE

\*\*\*240-376-0100-M1 \*\*\* 15 MATER PUMP

CUTOKUMPU DY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-26 PAGE NO: 15
DEPARTMENT:PROJECT

CLIENT :PPCL

DOCUMENT: MCTOR LIST (8)

2UTCKUMPU NO :360 100 900 001 ALT1

DESIGN :AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

240-376-0200

EQUIPMENT TYPE

WATER PUMP

MOTER NO./FATING (KW)

MCTOR TITLE

\*\*\*240-376-0200-M1 \*\*\* 15 \*\*\*

MATER PUMP

240-518-0100

**EQUIPMENT TYPE** 

PUMP TANK

240-532-0100

EQUIPMENT TYPE

THICKENER

MOTER NO./RATING (KW)

MOTOR TITLE

\*\*\*240-532-0100-M1 \*\*\* 3 \*\*\*

THICKENER

\*\*\*240-532-0100-M2 \*\*\* 3 \*\*\*

THICKENER

\*\*\* 240-532-0100-M3 \*\*\* 0,5 \*\*\*

THICKENER

300----0

ECJIPMENT TYPE

SULPHUF PLANT AREA

310----0

EQUIPMENT TYPE

SULPHUR FECTIVERING AREA

310-129-0100

EQUIPMENT TYPE

SULPHUR CONDENSING BOILER

MCTCR NG./RATING (KW)

MOTOR TITLE

\*\*\* 310-129-0100-M1\*\*\* 110 \*\*\*
CIRCULATION WATER PUMP

\*\*\* 310-12 5-0100-M2\*\*\* 90 \*\*\*
CIRCUL 4TION WATER PUMP

SUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 16 DEPARTMENT : PROJECT

CLIENT :PPCI DOCUMENT: MOTOR LIST (B)

GUTEKUMPU NG :360 100 900 001 ALTI

DESIGN :AKI CLIENT NO :

FEVISION :5 DATE :22.08.85

310-129-0200

EQUIPMENT TYPE

GAS CEOLING BOILER

MCTOR NO./FATING (KW) MOTOR TITLE

\*\***\***310-129-0200 \*\*\* 110 \*\*\* CIRCULATION WATER PUMP

310-198-0100

ECJIPMENT TYPE

GAS DUCT

310-198-0200

EQUIPMENT TYPE

GAS DUCT

310-204-0100

EQUIPMENT TYPE

STACK

310-209-0100

EQUIPMENT TYPE

MATER LCCK

310-209-0200

EQUIPMENT TYPE

MATER LUCK

310-209-0300

EQUIPMENT TYPE

MATER LCCK

310-212-0100

EQUIPMENT TYPE

PROCESS GAS FAN

MOTOR NO./RATING (KW) METOR TITLE

\*\*\*310-212-0100-M1 \*\*\* 160 \*\*\* PROCESS GAS FAN

OUT DRUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 17

DEPARTMENT : PROJECT

CLIENT :PPCL DOCUMENT: MOTOR LIST (B) OUTOKUMPJ NO :360 100 900 001 ALT1 DESIGN : AK I

CLIENT NO :

REVISION :5 DATE :22.08.85

310-212-0200

EQUIPMENT TYPE

PROCESS GAS FAN

MOTER NO./FATING (KW) MOTOR TITLE

\*\*\*310-212-0200-M1 \*\*\* 160 \*\*\* PROCESS GAS FAN

310-212-0300

EQUIPMENT TYPE

COMBUSTION AIR FAN

METOR NO. / RATING (Kw) MOTOR TITLE

\*\*\*310-212-0300-M1 \*\*\* 132 \*\*\* COMBUSTION AIR FAN

310-212-0400

EQJIPMENT TYPE

COMBUSTION AIR FAN

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*310-212-0400-M1 \*\*\* 132 \*\*\* COMBUSTION AIR FAN

310-212-0500

EQUIPMENT TYPE

FAN

MOTER NO./RATING (KW) MOTOR TITLE

\*\*\*310-212-0500-M1 \*\*\* 160 \*\*\* EXHAUST GAS FAN

310-212-0600

EQUIPMENT TYPE

FAN

MOTOR NO./RATING (Km) MOTOR TITLE

\*\*\*310-212-0600-M1 \*\*\* 160 \*\*\* EXHAUST GAS FAN

310-212-0700

EQUIPMENT TYPE

CCMBUSTION AIR FAN

MOTOR NO. /FATING (KW) MOTOR TITLE

\*\*\*310-212-0700-M1 \*\*\* 75

COMBUSTION AIR FAN

CUTCKUMPU CYZENGINEERING DIVISION PECJECT : OPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 18 DEPARTMENT : PROJECT

CLIENT : PPCL DOCUMENT: MOTOR LIST (B) QUT OKUMPU NO :360 100 900 001 ALTI DESIGN : AK I

CLIENT NO : REVISION :5 DATE :22.08.85

310-213-0800

ECUIPMENT TYPE

SECONDARY AIR FAN

MOTOR NO. / FATING (KW) MOTOR TITLE

\*\*\*310-213-0800-M1 \*\*\* 90 SECONDARY AIR FAN

310-263-9100

EQUIPMENT TYPE

INCINERATOR

310-281-0100

EQUIPMENT TYPE

GAS REHEATER

310-370-0100

EQUIPMENT TYPE

FUEL GIL PLMP

MOTOR NU. / RATING (KW) MCTOR TITLE

\*\*\*310-370-0100-M1 \*\*\* 3 FUEL DIL PLMP

310-370-0200

EGUIPMENT TYPE

FUEL GIL PLMP

MOTOR NO. /RATING (KW) MCTOR TITLE

\*\*\*310-370-0200-M1 \*\*\* 3 \*\*\* FUEL DIL PLMP

310-370-0300

EQUIPMENT TYPE

FUEL CIL PLMP

MOTOR NO. /RATING (KM) MOTOR TITLE

\*\*\*310-370-0300-M1 \*\*\* 3 FUEL DIL PLMP

310-374-0100

EQUIPMENT TYPE

SLURRY PUMP

MOTOR NO./RATING (KW) MOTOR TITLE

1 1 1

\*\*\* 310-374-0100-M1\*\*\* 90 \*\*\*

SLUFRY PUMP

OUTEKUMPU CYZENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 19
DEPARTMENT:PROJECT

CLIENT :PPCL
DOCUMENT:MCTCR LIST (B)
DUTGKUMPU NO :360 100 900 001 ALTI
DESIGN :4KI

CLIENT NO :

REVISION :5 DATE :22.08.85

310-374-0200

EQUIPMENT TYPE

SLUKRY PUMP

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\*310-374-0200-M1 \*\*\* 90 \*\*\*
SLURRY PUMP

310-374-0300

EQUIPMENT TYPE

SLURRY PUMP

MOTOR NO./RATING (KW) MOTOR TITLE

\*\*\* 310-374-0300-M1 \*\*\* 90 \*\*\*
SLURRY PUMP

310-374-0400

EQUIPMENT TYPE

WATER PUMP

MCTOR NO./RATING (KM) MOTOR TITLE

\*\*\*310-370-0400-M1 \*\*\* 30 \*\*\*

WATER PUMP

310-374-0500

EQUIPMENT TYPE

HATER PUMP

MOTER NO./FATING (KW) MCTOR TITLE

\*\*\* 310-370-0500-M1 \*\*\* 30 \*\*\*
WATER PUMP

310-374-0600

EQUIPMENT TYPE

WATER PUMP

MOTOR NO./FATING (KW)

\*\*\*310-370-060G-M1 \*\*\* 30 \*\*\*

MCTGR TITLE NATER PUMP

310-374-0700

EQUIPMENT TYPE

WATER PUMP

MOTOR NO./RATING (KW)

\*\*\*310-370-0700-M1 \*\*\* 30 \*\*\*
NATER PUMP

MOTOR TITLE NA

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CUTOKUMPU CYZENGINEERING DIVISION DATE :85-08-28 PAGE NO: 20 PROJECT : PPCL PYRITE SMELTER

DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: MOTOR LIST (B)

DUTOKUMPU NO :360 100 900 001 ALT1

DESIGN :AKI CLIENT NO :

REVISION :5 DATE :22.08.85

310-376-0100

EQUIPMENT TYPE

MATER PUMP

MOTOR NO./FATING (Km)

MCTOR TITLE

\*\*\*310-376-0100-M1 \*\*\* 15 \*\*\*

MATER PUMP

310-376-0200

EQUIPMENT TYPE

WATER PUMP

MOTOR NO./FATING (Km)

MOTOR TITLE

\*\*\*310-376-0200-M1 \*\*\* 15 \*\*\*

MATER PUMP

310-420-0100

EQUIPMENT TYPE

DEMISTER

310-420-0200

EQUIPMENT TYPE

DEMISTER

3 10-423-0100

EQUIPMENT TYPE

SCRUBBER.

310-423-0200

EQUIPMENT TYPE

ABSCRBTION TOWER

310-431-0100

EQUIPMENT TYPE

AGGLEMER AT CR

310-433-0100

EQUIPMENT TYPE

HCT CATALYZER

OUTOKUMPU CY/ENGINEERING DIVISION DATE: 85-08-28 PAGE NO: 21 PROJECT : PPCL PYRITE SMELTER

DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: MOTOR LIST (B)

GUTCKUMPU NG :360 100 900 001 ALT1

DESIGN :AKI CLIENT NG :

REVISION :5 DA.E :22.08.85

310-433-0200

EQUIPMENT TYPE

CCLD CATALYZER

310-433-0300

EQUIPMENT TYPE

COLD CATALYZER

310-464-0100

SQUIPMENT TYPE

SULPHUR CONDENSING TOWER

310-464-0200

EQUIPMENT TYPE

SULPHUR CONDENSING ICHER

310-516-0100

EQUIPMENT TYPE

MIXING TANK

MOTOR NO./FATING (KW)

MOTOR TITLE

\*\*\*310-516-0100-M1 \*\*\* 37 \*\*\* MIXING TANK

310-518-0100

EQUIPMENT TYPE

PUMP TANK

320---0

EQUIPMENT TYPE

SULPHUR HANDLING AREA

323-117-0130

EQUIPMENT TYPE

BIN

CUTCKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

. IE :85-08-28 PAGE NO: 22 DEPARTMENT : PROJECT

CLIENT : PPCL DECUMENT: MCTGR LIST (B) QUTOKUMPU NO :360 100 900 001 ALTI DESIGN

CLIENT NO : REVISION :5 DATE :22.08.85

320-129-0100

EQUIPMENT TYPE

SULPHUR COELING BOILER

520-129-0200

EQUIPMENT TYPE

SULPHUR COELING BOILER

320-129-0300

EQUIPMENT TYPE

SULPHUR COCLING BOILER

320-167-0100

EQUIPMENT TYPE

BELT CONVEYOR

MOTOR NO. / FATING (KW) MOTOR TITLE

\*\*\*3 20-167-0 100-M1 \*\*\* 5,5 \*\*\* BELT CONVEYOR

320-167-0200

EQUIPMENT TYPE

BELT CONVEYOR

MCTOR NO. / FATING (KW) MCTOR TITLE

\*\*\*3 20-167-0 200-M1 \*\*\* 5.5 \*\*\* BELT CONVEYOR

320-167-0300

EQUIPMENT TYPE

BELT CONVEYOR

MOTOR NO. /FATING (KW) MOTOR TITLE

BELT CONVEYOR

320-172-0100

EQUIPMENT TYPE

SCREW CONVEYOR

MOTOR NO. / RATING (KW)

\*\*\*3 20-172-0100-M1 \*\*\* 0.75 \*\*\* SCREN CONVEYOR

MOTOR TITLE

OUTOKUMPU CY/ENGINEERING DIVISION DATE :85-08-28 PAGE NO: 23 PROJECT : PPCL PYRITE SMELTER

DEPARTMENT : PROJECT

CLIENT : PPCL DICCUMENT: MOTOR LIST (B) DUTOKUMPU NC :360 100 900 001 ALT1 DESIGN : AK I

CLIENT NO : REVISION :5 DATE :22.08.85

320-212-0130

EQUIPMENT TYPE AIR COOLING FAN

MOTOR NO./FATING (KW) \*\*\*320-212-0100-M1\*\*\* 15 \*\*\* MOTOR TITLE AIR COULING FAN

320-212-0200

EQUIPMENT TYPE AIR COOLING FAN

MOTOR NO./RATING (KW) \*\*\* 320-212-0200-M1\*\*\* 15 \*\*\* MOTOR TITLE AIR COOLING FAN

320-212-0300

EQUIPMENT TYPE AIR CLOLING FAN

MOTOR NO./RATING (KW) \*\*\* 320-212-0300-M1\*\*\* 15 \*\*\* MOTOR TITLE AIR COOLING FAN

320-212-0400

EQUIPMENT TYPE AIR COOLING FAN

MCTOR NO./FATING (KW) \*\*\* 320-212-0400-M1\*\*\* 15 \*\*\* MCTOR TITLE AIR COOLING FAN

320-214-0100

EQUIPMENT TYPE AIR BLOWER

MCTOR NO. /FATING (KW) \*\*\*320-214-0100-M1 \*\*\* 11 \*\*\* MCTOR TITLE AIR BLOWER

320-244-0100

EQUIPMENT TYPE GRAVITY FILTER

320-244-0200

EQUIPMENT TYPE GRAVITY FILTER QUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: 24 DEPARTMENT : PROJECT

CLIENT :PPCL

DOCUMENT: MOTOR LIST (B)

DUTOKUMPU NC :360 100 900 001 ALT1

DESIGN : AKI CLIENT NO :

REVISION :5 DATE :22.08.85

320-370-0100

EQUIPMENT TYPE

PUMP

MCTOR NO./FATING (Km)

MOTOR TITLE

\*\*\*320-370-0100-M1 \*\*\* 11 \*\*\* SULPHUR PUMP

320-370-0200

EQUIPMENT TYPE

PUMP

MOTER NO. /FAT (NG (KW)

MOTOR TITLE

\*\*\*320-370-0200-M1 \*\*\* 11 \*\*\* SULPHUR PUPP

320-370-0300

EQUIPMENT TYPE

PUMP

MOTOR NO. / FATING (KW)

MOTOR TITLE

\*\*\*320-370-0300-MI \*\*\* 18,5 \*\*\* SULPHUR PUMP

320-370-0400

EQUIPMENT TYPE

PUMP

MOTOR NO. / RATING (KW)

MOTOR TITLE

\*\*\*320-370-0400-M1 \*\*\* 18,5 \*\*\* SULPHUR PUMP

320-370-0500

EQUIPMENT TYPE

PUMP

METER NO. / RATING (KW)

MOTOR TITLE

\*\*\*320-370-0500-M1 \*\*\* 3 \*\*\* SULPHUR PUMP

320-370-0600

EQUITMENT TYPE

PUMP

MOTOR NO. / FATING (KW)

\*\*\*320-370-0500-M1 \*\*\* 3 \*\*\* SULPHUR PUMP

MOTOR TITLE

DUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 25 DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: MOTOR LIST (B)

DUT DKUMPU NC :360 100 900 001 ALT1

DESIGN : AK I CLIENT NO :

FEVISION :5 DATE :22.08.85

320-370-0730

EQUIPMENT TYPE

PUMP

MOTOR NO./RATING (KW) MCTOR TITLE

SULPHUR PUPP

\*\*\*320-370-0700-M1 \*\*\* 15 \*\*\*

320-370-0800

EQUIPMENT TYPE

PUMP

MCTOR NO./FATING (KW) MOTOR TITLE

SULPHUR PUMP

\*\*\*320-370-0800-M1 \*\*\* 15 \*\*\*

320-370-0900

EQUIPMENT TYPE

PUMP

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*320-370-0900-M1 \*\*\* SULPHUR PUMP

11 \*\*\*

11 \*\*\*

320-370-1000

EQUIPMENT TYPE

PUMP

MCTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*320-370-1000-M1 \*\*\* SULPHUR PUMP

320-370-1100

EQUIPMENT TYPE

PUMP

MCTOR NO. / FATING (KW)

SULPHUR PUMP

\*\*\*320-370-1100-M1 \*\*\* 15 \*\*\*

320-370-1200

MUTOR TITLE

EQUIPMENT TYPE

PUMP

MOTOF NO./FATING (KW)

\*\*\*320-370-1200-M1 \*\*\* 15 \*\*\*

MOTOR TITLE

SULPHUR PUMP

QUTOKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 26 DEPARTMENT : PROJECT

CLIENT : PPCL DOCUMENT: MOTOR LIST (B)

QUTEKUMPU NO :360 100 900 001 ALT1

DESIGN :AKI CLIENT NO :

REVISION :5 DATE :22.08.85

320-370-1300

EQUIPMENT TYPE

PUMP

MOTOR NO./FATING (KW) MOTOR TITLE

\*\*\*320-370-1300-M1 \*\*\* 11 \*\*\*

SULPHUR PUMP

320-370-1400

EQUIPMENT TYPE

PUMP

MOTOR NO. / RATING (KW) MOTOR TITLE

\*\*\* 320-370-1400-M1 \*\*\* 11 \*\*\*

SULPHUR PUMP

320-370-1500

EQUIPMENT TYPE

PUMP

MOTOR NO./RATING (KW) MCTOR TITLE

\*\*\*320-370-1500-M1 \*\*\* 90

SULPHUR CIRCULATING PUMP

320-370-1600

EQUIPMENT TYPE

PUMP

MOTOR NO./RATING (KW)

MOTOR TITLE

\*\*\* 320-370-1600-M1 \*\*\* 90 SULPHUR CIRCULATING PUMP

323-370-1700

EQUIPMENT TYPE

PUMP

MOTER NO./RATING (KM)

MOTOF TITLE

###320-570-1700-M1 \*\*\* 90 SULPHUR CIRCULATING PUMP

\*\*\*

320-370-1830

EQUIPMENT TYPE

PUMP

MCTOR NO. /RATING (KW)

MOTOR TITLE

\*\*\*320-370-1800-M1 \*\*\* 90 SULPHUR CIRCULATING PUMP

OUTOKUMPU CY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

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CLIENT :PPCL
DOCUMENT:MCTOR LIST (B)
SUTSKUMPJ NS :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO:
REVISION :5 DATE :22.08.85

320-370-1900

EQUIPMENT TYPE PUMP

MCTGR NO./FATING (KW) \*\*\*320-370-1900-M1 \*\*\* 90 \*\*\*
MCTGR TITLE SULPHUR CIRCULATING PUMP

320-370-2000

EQUIPMENT TYPE PUMP

MOTER NO./FATING (KW) \*\*\*320-370-2000-M1 \*\*\* 90 \*\*\*
METER TITLE SULPHUR CIRCULATING PUMP

320-370-2300

EQUIPMENT TYPE PUMP

MGTUR ND./RATING (KW) \*\*\*320-370-2300-M1 \*\*\* 37 \*\*\*
MGTUR TITLE SULPHUR PRILLING PUMP

320-370-2400

EQUIPMENT TYPE PUMP

MOTOR TITLE \*\*\* 37 \*\*\*

MOTOR TITLE SULPHUR PRILLING PUMP

320-371-0100

EQUIPMENT TYPE COSAGE PUMP

320-371-0200

EQUIPMENT TYPE COSAGE PUMP

GUT OKUMPU GYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

UATE :85-08-28 PAGE NO: 28 DEP AR IMENT : PROJECT

CLIENT : PPCL

DOCUMENT: MOTOR LIST (B)

GUTOKUMPU NO :360 100 900 001 ALT1

:AKI

CLIENT NO :

REVISION :5 DATE :22.08.85

320-371-0300

EQUIPMENT TYPE

DESAGE PUMP

MOTOR NO./RATING (KW)

\*\*\*320-371-0300-M1 \*\*\* 1.5 \*\*\* MOTOR TITLE

DOSAGE PUMP

320-411-0100

EQUIPMENT TYPE

VIBRATING SCREEN

MOTOR NO. / PATING (KW)

\*\*\*320-411-0100-M1 \*\*\* 15 \*\*\* MOTOR TITLE

VIBRATING SCREEN

320-411-0200

EQUIPMENT TYPE

VIBRATING SCREEN

MOTOR NO. / RATING (KW)

MOTOR TITLE

\*\*\*320-411-0200-M1 \*\*\* . 15 \*\*\*

VIBRATING SCREEN

320-509-0100

EQUIPMENT TYPE

PHILLING TOWER

320-511-0100

EQUIPMENT TYPE

AUTCCLAVE

MOTOR NO./FATING (KW)

MOTOR TITLE

\*\*\*320-511-0100-M1 \*\*\* 3

AUTO CLAVE

\*\*\*320-511-0100-M2 \*\*\* 3 \*\*\*

AUTOCLAVE

320-511-0200

EQUIPMENT TYPE

AUTOCLAVE

MOTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*320-511-0100-M1 \*\*\* 3 AUTOCLAVE

\*\*\*320-511-0100-M2 \*\*\* 3 \*\*\*

**AUTCCLAVE** 

DUT SKUMPU CYZENGINEERING DIVISION DATE:85-08-28 PAGE NO: 29 PROJECT : PPOL PYRITE SMELTER

DEPARTMENT : PROJECT

CLIENT : PPCL DECUMENT: METER LIST (B) DES IGN :AKI

REVISION :5 DATE :22.08.85

320-515-0100

EQUIPMENT TYPE

MEASURING TANK

320-516-0100

ELUIPMENT TYPE

MIXING TANK

MOTER NO./RATING (KW) MOTOR TITLE

キキキゥ20-51o-0100-M1 \*\*\* 4

MIXING TANK

320-518-0100

EQUIPMENT TYPE

PUMP TANK

320-518-0200

EQUIPMENT TYPE

PUMP TANK

320-518-0300

EQUIPMENT TYPE

PUMP TANK

3 20 - 518 - 0400

EQUIPMENT TYPE

PUMP TANK

3 20 - 518 - 05 00

EQUIPMENT TYPE

PUMP TANK

320-518-0600

EQUIPMENT TYPE

PUMP TANK

SUT OKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYRINE SMELTER

DATE :85-08-28 PAGE NJ: 30 DEPARTMENT : PROJECT

CLIENT : PPCL DOCUMENT: METOR LIST (B) DUT DKUM PU NO :360 100 900 001 A LT1 : AK I DES IGN

CLIENT NG : REVISION :5 DATE :22.08.85

320-516-0700

EQUIPMENT TYPE

PUMP TANK

320-519-0100

EQUIPMENT TYPE

TANK

320-519-6200

EQUIPMENT TYPE

DAY TANK

30----0 دّ

EQUIPMENT TYPE

WASTE LIQUID HANDLING AREA

330-212-0100

EQUIPMENT TYPE

FAN

MOTOR NO./FATING (KW)

MOTOR TITLE

\*\*\*330-212-0100-MI \*\*\* 5.5 \*\*\* EXHAUST GAS FAN

330-243-0100

FQUIPMENT TYPE

DRUM FILTER

MOTOR NO. /FATING (KW)

MOTOR TITLE

+\*\*330-243-0100-M1 +\*\* 1.1 \*\*\*

DRUM FILTER

\*\*\*330-243-0100-M2 \*\*\* 0.75 \*\*\*

DRUM FILTER

330-370-0100

EQUIPMENT TYPE

PUMP

MOTOR NO. /FATING (KW)

\*\*\*330-370-0100-M1 \*\*\* 2.2 \*\*\* UNDERFLOW FUMP

MOTOR TITLE

DUTOKUMPU DYZENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 31 DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: MOTOR LIST (B)

SUT SKUMPJ NE :360 100 900 001 ALT1

DES IGN : AK I

CLIENT NG :

REVISION :5 DATE :22.08.85

330-370-0200

EQUIPMENT TYPE

PUMP

MOTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*330-370-0200-M1 \*\*\* 2.2 \*\*\*

UNDERFLOW PUMP

330-370-0300

EQUIPMENT TYPE

**PUMP** 

MCTOR NO. / FATING (KW)

MOTOR TITLE

\*\*\*330-370-0300-M1 \*\*\* 2.2 \*\*\*

CVERFLOW PUMP

330-370-0400

EQUIPMENT TYPE

PUMP

MCTOR NO. / FATING (KW)

MOTOR TITLE

\*\*\*330-370-0400-M1 \*\*\* 2.2 \*\*\*

CVEFFLOW PLMP

330-375-0100

EQUIPMENT TYPE ,

VACUUM PUMP

MCTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*330-375-0100-M1 \*\*\* 11 \* \* \* VACUUM PUMP

330-510-0100

EQUIPMENT TYPE

TANK

330-510-0200

EQUIPMENT TYPE

TANK

330-518-0100

EQUIPMENT TYPE

PUMP TANK

GUTOKUMPU CY/ENGINEERING DIVISION PROJECT :PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 32 DEPARTMENT:PROJECT

CLIENT : PPCL

DCCUMENT: MOTOR LIST (B)

OUTOKUMPU ND :360 100 900 001 ALT1

DESIGN : AKI

CLIENT ND :

REVISION :5 DATE :22.08.85

330-518-0200

EQUIPMENT TYPE

PUMP TANK

330-521-0100

EQUIPMENT TYPE

REACTOR TANK

330-532-0100

EQUIPMENT TYPE

THICKENER

MOTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*330-532-0100-M1 \*\*\* 2 \*\*\*

THICKENER

\*\*\*330-532-0100-M2 \*\*\* 0.75 \*\*\*

THICKENER

500---0

EQUIPMENT TYPE

COAL PLANT AREA

500-118-0100

EQUIPMENT TYPE

STORAGE BIN

500-118-0200

EQUIPMENT TYPE

STORAGE BIN

500-118-0300

EQUIPMENT TYPE

STORAGE BIN

500-118-0400

EQUIPMENT TYPE

STORAGE BIN

DUTCKUMPU CY/ENGINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE :85-08-28 PAGE NO: 33 DEPARTMENT : PROJECT

CLIENT : PPCL

DECUMENT: MOTOR LIST (B)

QUTOKUMPU NO :360 100 900 001 ALT1

:AKI DES IGN

CLIENT NO :

REVISION :5 DATE :22.08.85

500-133-0100

EQUIPMENT TYPE

CIL BURNER

500-167-0100

EQUIPMENT TYPE

BELT CONVEYOR

MOTER NO./RATING (KW) MOTOR TITLE

\*\*\*500-167-0100-M1 \*\*\* 45

BELT CONVEYOR

500-167-0200

EQUIPMENT TYPE

BELT CONVEYOR

MOTOR NO. / PATING (KW)

\*\*\*500-167-0200-M1 \*\*\* 7.5 \*\*\* BELT CONVEYOR

MOTOR TITLE

500-170-0130

EQUIPMENT TYPE

PNEUMATIC CONVEYOR SYSTEM

500-170-0200

EQUIPMENT TYPE

PNEUMATIC CONVEYOR SYSTEM

500-179-0100

EQUIPMENT TYPE

COAL INJECTION SYSTEM

500-202-0100

EQUIPMENT TYPE

FEED HOPPER

0 1 1

DETOKUMPU EYZENCINEERING DIVISION PROJECT : PPCL PYRITE SMELTER

DATE:85-08-28 PAGE NO: 34
DEPARTMENT:PROJECT

CLIENT :PPCL
DECUMENT:MCTOR LIST (B)
CUTOKUMPU NG :360 100 900 001 ALT1
DESIGN :AKI

CLIENT NO : REVISION :5 DATE :22.08.85

500-212-0100

EQUIPMENT TYPE FAN

MOTER NO./FATING (Kw) \*\*\* 500-212-0100-M1\*\*\* 30 \*\*\*
METER TITLE FAN

500-212-0200

EQUIPMENT TYPE FAN

500-212-0300

EQUIPMENT TYPE EXHAUST AIR FAN

500-212-0400

EQUIPMENT TYPE FAN

MOTER NO./FATING (KW) ### 11 ### 11 \*##

500-216-0130

EQUIPMENT TYPE AIR LOCK FEEDER

500-216-0200

EQUIPMENT TYPE AIR LCCK FEEDER

OUTOKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: 35 DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: METOR LIST (B)

DUTOKUMPU NC :360 100 900 001 ALT1

DESIGN : AKI CLIENT NO :

REVISION :5 DATE :22.08.85

500-218-0100

FOUTPMENT TYPE

BELT FEEDER

MOTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*500-218-0100-M1 \*\*\* 7.5 \*\*\*

BELT FEEDER

500-223-0100

EQUIPMENT TYPE

DRAG FEEDER

MOTOR NO. / RATING (KW)

MOTOR TITLE

\*\*\*500-223-0100-M1 \*\*\* 7,5 \*\*\*

DRAG FEEDER

500-223-0200

EQUIPMENT TYPE

CRAG FEEDER

MOTOR NO. / RATING (Kw)

MOTOR TITLE

\*\*\*500-223-0200-M1 \*\*\* 7.5 \*\*\*

DRAG FEEDER

500-281-0100

EQUIPMENT TYPE

PREHEATER

500-325-0100

EQUIPMENT TYPE

MILL

MOTOR NO. / FATING (KW)

MOTOR TITLE

\*\*\*500-325-0100-M1 \*\*\* 315

MILL

500-325-0200

EQUIPMENT TYPE

MILL

MOTOR NO. / FATING (KW)

MCTGR TITLE

\*\*\*500-325-0200-M1 \*\*\* 315 \*\*\*

MILL

CUTOKUMPU GY/ENGINEERING DIVISION DATE :85-08-28 PAGE NO: 36 PROJECT : PPCL PYRITE SMELTER

DEPARTMENT : PROJECT

CLIENT :PPCL DOCUMENT: MOTOR LIST (B)

DUTOKUMPU NC :360 100 900 001 ALT1

DESIGN :AKI

CLIENT NO :

FEVISION :5 DATE :22.08.85

500-411-0100

EQUIPMENT TYPE

VIBFATING SCREEN

MCTOR NO. / RATING (KW)

MOTOR TITLE

\*\*\*500-411-0100-M1 \*\*\* 2,2 \*\*\*

VIBRATING SCREEN

500-411-0230

EQUIPMENT TYPE

VIBRATING SCREEN

MOTOR NO. / RATING (Kt)

MOTOR TITLE

\*\*\*500-411-0200-M1 \*\*\* 2,2 \*\*\* VIBRATING SCREEN

500-417-0100

EQUIPMENT TYPE

BAG FILTER

500-419-0100

EQUIPMENT TYPE

CYCLONE

600----0

EQJIPMENT TYPE

PCWER PLANT AREA

600-122-0100

EQUIPMENT TYPE

AUXILIARY BOILER

6 00-123-0100

EQUIPMENT TYPE

SUPERHEATING BOILER

600-276-0100

EQUIPMENT TYPE

CONDENSER

SUTCKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: **37** DEPARTMENT : PROJECT

CLIENT : PPCL

DOCUMENT: MOTOR LIST (B)

GUTOKUMPU NO :360 100 900 001 ALTI

:AKI DESIGN

CLIENT NO :

REVISION :5 DATE :22.08.85

600-280-0100

1

EQUIPMENT TYPE

HEAT EXCHANGER

600-280-0200

EQUIPMENT TYPE

HEAT EXCHANGER

500-376-0100

EQUIPMENT TYPE

CONDENSATE PUMP

MOTOR NO. /FATING (KW)

MOTOR TITLE

\*\*\*600-376-0100-M1 \*\*\* 22 CONDENSATE PUMP

600-376-0200

EQUIPMENT TYPE

CONDENSATE PUMP

MCTOR NO./RATING (KW)

MOTOR TITLE

\*\*\*600-376-0200-M1 \*\*\* 22 CONDENSATE PUMP

600-376-0300

EQUIPMENT TYPE

CONDENSATE PUMP

MOTOR NO./FATING (KW)

MOTOR TITLE

\*\*\*600-376-0300-M1 \*\*\* 400 CONDENSATE PUMP

600-376-0400

EQUIPMENT TYPE

CONDENSATE PUMP

000-376-0500

EQUIPMENT TYPE

CONDENSATE PUMP

MOTER NO. / FATING (KW)

\*\*\*600-276-6 ML \*\*\* 30 FEED WATER PLACE

MOTOR TITLE

DUTCKUMPU CYZENGINEERING DIVISION PROJECT : PPCL PYFITE SMELTER

DATE :85-08-28 PAGE NO: 38 DEPARTMENT : PROJECT

CLIENT :PPCL DOCUMENT: MOTOR LIST (B) GUT SKUMPJ NG :360 100 900 001 ALT1 DESIGN : 4K I

CLIENT NO : REVISION :5 DATE :22.08.85

600-376-0600

EQUIPMENT TYPE

CONDENSATE PUMP

600-376-0700

EQUIPMENT TYPE

CONDENSATE PUMP

MOTOR NO. /RATING (KW) MOTOR TITLE

\*\*\*600-376-0700-M1 \*\*\* 15 \*\*\*

FEED WATER PUMP

600-514-0100

EQUIPMENT TYPE

FEED TANK

600-556-0100

EQUIPMENT TYPE

TURBUALTERNATOR

7 00----0

EQUIPMENT TYPE

CXYGEN PLANT AREA

C----CC 8

EQUIPMENT TYPE

LIME STONE SLUKRY PREPARATION

900---0

EQJIPMENT TYPE

WATER TREATMENT AREA

950----

EQUIPMENT TYPE

COMPRESSED AIR STATION