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Maschinenfabrik Andritz Aktiengesellschaft

SI/VEN/93/801

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+ 100  
9.4.1994

## **Reduction of Environmental Hazard of Red Mud Disposal at CVG-Interalumina**

**Contract No. 93/239**

### **ANDRITZ ON SITE TEST REPORT**

**CUSTOMER:** CVG Interamericana de Alumina C.A.  
Zona Industrial Matanzas, Ciudad Guayana  
Estado Bolivar

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**CONFIDENTIAL**

Date: 1.3.1994

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## Preamble

The test work with the ANDRITZ HBF-Trailer was carried out during the days of 4. Januar to 12. Febr. 1994 at the INTERALUMINA plant.

These onsite tests are to be seen as confirmation resp. addition to the test work with the Andritz-Laboratory Hyperbaric Filter early 1993 and to get all the required data for the layout of an actual Filter plant and the required auxilliary units.

I wish to express my gratefulness to all the staff of CVG INTERALUMINA for their supporting cooperation and hospitality during our stay at PUERTO ORDAZ.

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## 1. Introduction:

Red mud, the waste product of alumina plants, contains considerable amounts of solids and soluble caustic as well as alumina, which presents a severe technical, economical and ecological burden for alumina producers.

CVG INTERALUMINA has been dumping red mud as of start up at about 25-30 % solids into lagoons nearby the plant. At a production level of 2.0 Mio tpy of alumina roughly 4.0 Mio tpy slurry containing 1.15 Mio tpy dry mud would have to be handled. Supernatant, contaminated liquor was partially returned to the plant or evaporated, still leaving a considerable volume in the lagoons which today have reached a critical level.

CVG INTERALUMINA is therefore looking for a solution, to be operational within 3 years, to separate and dump its mud for at least 30 years under technically, economically and ecologically advanced conditions. Maximum red mud densities with a minimum of contaminants are hence required to satisfy such prerequisites.

Besides a few proven techniques already available, offering a partial solution to the above problems with mud at 50 to 55 % solids to be dumped, CVG INTERALUMINA contemplated the application of a pressure filtration to produce a mud of superior consistency. Preliminary tests confirmed the expectation. A red mud of 75 % solids, of non thixotropic characteristics was obtained, meeting essentially the original conditions set forth

Mid 1993 CVG INTERALUMINA requested suppliers for pressure filters to submit offers for pilot-plant tests. Late 1993 CVG INTERALUMINA reached an agreement with Maschinenfabrik Andritz AG to conduct a series of tests at its plant in Puerto Ordaz/Venezuela.

## **2. Material description and testseries:**

The present red mud separation with up to seven wash-stages at CVG INTERALUMINA offered the privilege of testing the whole range of alternatives for red mud filtration with the approximate filter feed conditions as described below.

### **2.1 Settler:**

Caustic concentration = 100-120 g/l Na<sub>2</sub>Oc  
Solids concentration = 200-400 g/l RM  
Wash water at filtration = 0-4.0 m<sup>3</sup>/t RM  
Additives = nil

Test runs from 160 to 169

### **2.2 Second wash stage:**

Caustic concentration = 40-60 g/l Na<sub>2</sub>Oc  
Solids concentration = 300-500 g/l RM  
Wash water at filtration = 0-4.0 m<sup>3</sup>/t RM  
Additives = nil

Test runs from 4 to 64, 118 to 144, 170 to 176 and 191 to 197

### **2.3 Third/Fourth wash stage:**

a) Caustic concentration = 20-30 g/l Na<sub>2</sub>Oc  
Solids concentration = 300-600 g/l RM  
Washwater at filtration = 0-1.5 m<sup>3</sup>/t RM  
Additives = nil

Test runs from 1 to 3, 145, 147 to 159, 177 to 190, 198 to 201,  
225 to 230, 231 to 235, 236 to 241

- b) Caustic concentration = 20 g/l Na<sub>2</sub>Oc  
Solids concentration = 500-600 g/l RM  
Washwater at filtration = nil  
Additives = 1 - 4 % CAO/RM

Test runs from 242 to 250

- c) Caustic concentration = 20 g/l Na<sub>2</sub>Oc  
Solids concentration = 450-500 g/l RM  
Washwater at filtration = nil  
Additives = 0,1 - 0,5 %/RM

Test runs from 251 to 254

- d) Caustic concentration = 20 g/l Na<sub>2</sub>Oc  
Solids concentration = 300-350 g/l RM  
Washwater at filtration = 0-1,0 m<sup>3</sup>/t RM  
Additives = Sand

Test runs from 261 to 265

#### **2.4 Last washer:**

- a) Caustic concentration = 10-20 g/l Na<sub>2</sub>Oc  
Solids concentration = 200-550 g/l RM  
Washwater at filtration = 0-1,2 m<sup>3</sup>/t RM  
Additives = nil

Test runs from 65 to 92, 93 to 117, 214 to 218, 219 to 224

- b) Caustic concentration = 10-20 g/l Na<sub>2</sub>Oc  
 Solids concentration = 300-450 g/l RM  
 Washwater at filtration = nil  
 Additives = Polymer

Test runs from 202 to 213

## **2.5 General Conditions:**

### **a) Mud analysis (chemical) typical**

Fe <sub>2</sub> O <sub>3</sub>	=	41	%
TiO <sub>2</sub>	=	4	%
CaO	=	1.5	%
SiO <sub>2</sub>	=	18	%
Al <sub>2</sub> O <sub>3</sub>	=	18	%
Na <sub>2</sub> O	=	4,5	%

### **b) Mud analysis (grain size)**

average of three sample

Wet screen analysis	=	accumulative
+ 106 µm	=	3 %
+ 90 µm	=	4 %
+ 63 µm	=	8 %
+ 45 µm	=	10 %
+ 38 µm	=	11 %
+ 25 µm	=	12 %

### **Microtrac**

+62 ym	=	1	%
+44 ym	=	4	%
+31 ym	=	12	%
+22 ym	=	27	%
+16 ym	=	43	%
+11 ym	=	60	%
+7,8 ym	=	75	%
+5,5 ym	=	87	%
+3,9 ym	=	94	%
+2,8 ym	=	99	%

c) **Sand & Mud (grain size)**

<b>Wet screen analysis</b>	<b>one sample only</b>		
- 600 ym	=	100	%
- 300 ym	=	99	%
- 150 ym	=	96	%
- 106 ym	=	93	%
- 53 ym	=	82	%



### **3. Laboratory Procedure:**

#### **3.1 Moisture:**

2 g of sample shall be dried during 12 hours at 110 ° C, determining the loss of weight as follows:

$$\% \text{moisture} = \frac{(M - M_1)}{M} \times 100$$

M = weight of original sample

M<sub>1</sub> = weight of dried sample

#### **3.2 Solids Concentration:**

The slurry is being filtered and washed throughly to eliminate residual caustic. The residue is thereafter dried at 115 °C during 2 hours, determining the solids concentration as follows:

$$\text{g/l solids} = \frac{\text{g solids}}{\text{sample volume}} \times 1000$$

### **3.3 Soluble Caustic:**

25 g Filter cake shall be reslurried in a measuring cylinder with 50 ccm distilled water and filled up until reaching 100 ccm. The liquor, obtained after filtration, shall be analized in accordance with the method of thermotitration used for the analysis of Na<sub>2</sub>O and Al<sub>2</sub>O<sub>3</sub> on all plant liquors.

### **4. Test equipment:**

Andritz provided a two square meter ( $2 \text{ m}^2$ ) HBF on a specially constructed trailer. All controls and auxiliary equipment necessary for operations of the production unit the power transformer are mounted on the trailer. The test trailer is furnished with the following equipment:

- a) Disc filter, one disc, 1.4 m diameter,  $2 \text{ m}^2$  filtration area
- b) Pressure vessel, 2.5 m diameter
- c) Cake discharge unit (double gate discharger)
- d) Conveyor to transport filter cake from the discharger to a point just off the trailer
- e) Additive make-up and metering system:
- f) One progressive cavity variable speed slurry pump  
or one variable speed mohno pump
- g) Two (2) air compressors
- h) Water booster pumps for wash down purposes
- i) Control panel with touch on screen to operate auxiliary equipment and HBF

### **HBF (Demo) method of operation:**

By applying atmospheric pressure, nature itself limits the maximum filtration pressure (8 - 12 psi, < 1 bar) of conventional vacuum filtration - one of the most important solid-liquid separation processes in the mineral industry. In order to increase the specific throughput of a filter and reduce the final cake moisture, it is possible to increase the differential pressure up to 90 psi (6 bar) by placing the filter in a vessel.

A disc filter is located inside a pressure vessel. The disc is designed of 20 hollow segments each covered by a filter cloth. Air pressure is increased inside the vessel up to 6 bar by means of compressed air. The segments are connected to a drain system which is exposed to atmospheric pressure (no vacuum applied). Positioned between the segments and the drain system is a "control disc" or rotary valve. Slurry is pumped into the trough (50 % disc submergence) where the level is controlled by level sensors, which on the other hand regulate the speed of the feed pumps accordingly

There is a pressure differential from the outside to the inside of the filter segments. Cake forms on the filter cloths that are submerged in the slurry (cake formation zone). A hydraulic motor rotates the disc so that the formed cake emerges from the slurry into the cake dewatering zone. The time allowed for cake formation and cake dewatering is controlled by a fixed and slotted disc previously referred to as a "control disc".

Before each of the segment re-submerges, air is "snap" blown from inside of the segment causing the cake to fall off into the discharge hopper. After a fill time of approx. one (1) minute the upper gate opens at the bottom of the hopper and the cake falls into a pressurized compartment. The upper gate then closes and the lower gate opens to atmospheric pressure, dropping the cake onto a conveyor. The lower gate closes and the compartment re-pressurizes to begin another cycle. This system of gates is called a "double trap" or double gate discharger.

A theoretical explanation of cake formation is supported by derivations from DARCY'S EQUATION. Cake height increases with the square root of the differential pressure. In addition, cake formation rate can be increased at higher differential pressure by raising the disc rotational speed.

An explanation for the cake dewatering mechanism results from SCHUBERT'S THEORY regarding the relative degree of cake saturation. The cake moisture content decreases with higher effective pressure difference (pressure difference applied minus the cake capillary pressure) and longer dewatering time.

## 5. Test results:

Survey over the test results:

Test Nos. 1 to 3 (feed:solid 217 g/l Na<sub>2</sub>Oc 34 g/l) this results are for first information.

Test Nos:4 to 21 (feed:solid 212-303 g/l Na<sub>2</sub>Oc 46-55 g/l) show the influence of the vessel pressure and the disc speed.

Test Nos:22 to 34 (feed:solid 262-329 g/l Na<sub>2</sub>Oc 55-59 g/l) it show a higher pressure difference.

Test Nos 35 to 64 (feed:solid 392-562 g/l Na<sub>2</sub>Oc 55-60 g/l) show the difference between washing and none washing by high pressure

Test Nos:65 to 92 (feed:solid 387-501 g/l Na<sub>2</sub>Oc 15-18 g/l) show results by low soda content in the feed

Test Nos:93 to 117 (feed:solid 496-546 g/l Na<sub>2</sub>Oc 13-14 g/l) repeat the tests from before and comparison to washing test

Test Nos.118 to 144 (feed:solid 318-348 g/l Na<sub>2</sub>Oc 40 g/l) show higher soda contents in the feed and comparison between washing and non-washing

Test Nos:145 (feed:solid 379 g/l Na<sub>2</sub>Oc 30 g/l) one point with a different filter cloth Tela Tresse 35.

Test Nos.:147 to 159 (feed:solid 386-396 g/l Na<sub>2</sub>Oc 29-30 g/l) show some results with a corser Filterbag (Tela Tresse 165)

Test Nos.:160 to 169 (feed:solid 205-404 g/l Na<sub>2</sub>Oc 100-116 g/l) show some results with high soda portion (114 g/l)

Test Nos.:170 to 176 (feed:solid 313-346 g/l Na<sub>2</sub>Oc 45-46 g/l) show some results with a soda portion von 45 g/l

Test Nos.:177 to 190 (feed:solid 273-308 g/l Na<sub>2</sub>Oc 23-24 g/l) show the test runs with steam and low caustic

Test Nos.:191 to 197 (feed:solid 420-493 g/l Na<sub>2</sub>Oc 38-43 g/l) show the test runs with steam

Test Nos.:198 to 201 (feed:solid 335-536 g/l Na<sub>2</sub>Oc 17-23 g/l) show washing tests by 5 bar vessel pressure

Test Nos.:202 to 213 (feed:solid 296-473 g/l Na<sub>2</sub>Oc 15-18 g/l) show a comparison between cake washing tests / none cake washing tests and feed with polymere

Test Nos.:214 to 218 (feed:solid 502-533 g/l Na<sub>2</sub>Oc 18-19 g/l) show some testruns with high feed concentration

Test Nos.:219 to 224 (feed:solid 527-550 g/l Na<sub>2</sub>Oc 18-19 g/l) show the reduction of the throughput over the operating time

Test Nos.:225 to 230 (feed:solid 474-484 g/l Na<sub>2</sub>Oc 20-22 g/l) show the variation of the feed temperatur

Test Nos.:231 to 235 (feed:solid 480-532 g/l Na<sub>2</sub>Oc 20-22 g/l) show the effect of the throughput over operating time

Test Nos.:236 to 241 (feed:solid 582-608 g/l Na<sub>2</sub>Oc 20-21 g/l) show some testruns with high feed concentration

Test Nos.:242 to 250 (feed:solid 512-597 g/l Na<sub>2</sub>Oc 20-21 g/l) show some testruns with lime dosage

Test Nos.:251 to 254 (feed:solid 444-532 g/l Na<sub>2</sub>Oc 18-22 g/l) show some testruns under addition of filter aid.

Test Nos.:255 to 261 (feed:solid 147-528 g/l Na<sub>2</sub>Oc 20-22 g/l) show some washing results / resp. the washing efficiency

Test Nos.:261 to 265 (feed:solid 309-340 g/l Na<sub>2</sub>Oc 20-21 g/l) show results with sand in the feed.

Test	Datum	Test	Feed- time	Vessel tank	Press press	Press CFL	Filter- speed	Feed- flow	Feed- density	Feed Na2O	Feed FMC	Feed temp	Airflow	Airflow	Filtrate- Compr.	Filtrate- flow	Filtrate- conc	Filtrate Na2O	Filt Poly	Wash	Poly	Poly	D-press	Steam	Steam	Disc flow	disch time	Tonnage of mass	residua dry	Cake Moisture	Cake Soda	Cake FMC	Time
~	~	~	hh:mm	number	Bar	Bar	Bar	l/min	m <sup>3</sup> /h	g/l	g/l	°C	Nm <sup>3</sup> /h	Nm <sup>3</sup> /h	m <sup>3</sup> /h	g/l	g/l	Na2O	FMC	Poly	Type	Conc	usage	Steam	flow	temp	sec	Cycles	kg	kg/m <sup>3</sup>	%	g/l	~
MVLT/JJ	hh:mm	number	Bar	Bar	Bar	Bar	Bar	l/min	m <sup>3</sup> /h	g/l	g/l	°C	Nm <sup>3</sup> /h	Nm <sup>3</sup> /h	m <sup>3</sup> /h	g/l	g/l	Na2O	FMC	Poly	Type	Conc	usage	Steam	flow	temp	sec	Cycles	kg	kg/m <sup>3</sup>	%	g/l	~
<b>First tests on redmud</b>																																	
<b>Feed from T35-5 (second washer)</b>																																	
<b>Filtercloth ZBF 08-1050-SK27</b>																																	
1	01/08/94	11:07	T 35-5	3,9	0,0	2,0	0,79	0,9	1,21	217	34,4	69	281	108	0,78	0,0	36,1	0	none	0,0	0,0	0	0	48,4	113	1	6	68	28,79	2,0			
2	01/08/94	12:13	T 35-5	4,0	0,0	2,4	0,99	2,4	1,22	221	33,6	87	210	75	0,93	0,0	37,8	0	none	0,0	0,0	0	0	55,2	115	1	9	100	28,94	2,4			
3	01/09/94	13:10	T 35-5	3,9	0,0	1,7	1,00	4,1	1,23	228	34,0	84	222	79	1,07	0,0	28,6	475	H2O	0,0	10,1	0	0	54,7	116	1	7,4	82	28,67	2,6			
<b>Begin of testseries on pressurefiltration for layout data</b>																																	
<b>Feed from T35-5 (second washer)</b>																				<b>tests with cakewashing just for getting experience</b>		<b>separate testseries with cakewashing will follow up</b>											
4	01/10/94	13:21	T 35-5	1,0	0,0	0,6	0,26	1,2	1,31	343	46,6	90	0	2	0,36	1,2	29,7	0	none	0,0	0,0	0	0	44,8	111	2	11	62	30,99	57,4			
5	01/10/94	13:39	T 35-5	0,7	0,0	0,0	0,25	1,1	1,31			84	34	67	0,31	1,1	47,5	0	none	0,0	0,0	0	0	44,9	110	2	8,5	49	29,52	53,8			
6	01/10/94	13:49	T 35-5	0,7	0,0	0,0	0,25	1,0	1,33			80	19	3	0,62	3,4	47,0	540	H2O	0,0	18,8	0	0	45,8	110	2	9	50	32,06	15,3			
7	01/10/94	14:17	T 35-5	1,0	0,0	0,0	0,25	1,3	1,33	242	47,9	92	168	227	0,35	2,4	50,3	0	none	0,0	0,0	0	0	48,6	111	2	9,5	58	24,6	64,0			
8	01/10/94	14:29	T 35-5	1,0	0,0	0,0	0,59	1,5	1,33			88	106	48	0,44	2,5	49,9	0	none	0,0	0,0	0	0	50,8	111	2	15	91	24,78	63,6			
9	01/10/94	14:39	T 35-5	1,0	0,0	0,0	0,25	0,8	1,24			84	106	3	0,47	2,4	49,1	540	H2O	0,0	17,6	0	0	50,5	111	2	9,15	53	29,15	15,5			
10	1994-01-11	15:47	T 35-5	2,0	0,0	0,0	0,27	0,8	1,33	247	54,9	187	94	219	101	0,30	1,9	55,3	1,87	0	none	0,0	0,0	0	0	56,5	112	2	8	46	28,5	58,4	
11	1994-01-11	16:12	T 35-5	2,0	0,0	0,9	0,27	1,0	1,32			96	233	337	0,54	1,2	55,7	1,91	0	none	0,0	0,0	0	0	54,2	114	2	11	63	27,9	62,0		
12	1994-01-11	16:24	T 35-5	2,0	0,0	0,7	0,61	1,1	1,27			96	311	357	0,70	2,5	56,1	1,88	0	none	0,0	0,0	0	0	53,8	114	2	15,5	87	28,9	56,0		
13	1994-01-11	16:35	T 35-5	2,0	0,0	0,3	1,03	1,4	1,27			96	298	340	0,80	4,6	56,9	1,94	0	none	0,0	0,0	0	0	54,0	114	2	18,2	104	27,3	60,0		
14	1994-01-11	16:45	T 35-5	2,0	0,0	0,0	1,03	1,2	1,31			96	144	103	0,95	6,5	49,5	1,86	420	H2O	0,0	7,6	0	0	53,5	115	2	16,5	89	30,7	19,7		
15	1994-01-11	17:03	T 35-5	3,0	0,0	2,0	0,26	1,0	1,31	212	54,1	1,87	98	272	342	0,62	4,8	55,3	1,97	0	none	0,0	0,0	0	0	54,8	117	2	12,2	69	28,3	65,7	
16	1994-01-11	17:14	T 35-5	3,0	0,0	1,7	0,60	1,3	1,26			100	282	340	0,79	4,8	55,3	1,87	0	none	0,0	0,0	0	0	54,5	117	2	16,6	91	28,9	59,9		
17	1994-01-11	17:26	T 35-5	3,0	0,0	1,5	1,03	1,4	1,32			98	241	296	0,88	10,0	56,1	1,93	0	none	0,0	0,0	0	0	55,0	118	2	20	110	27,9	63,3		
18	1994-01-11	17:40	T 35-5	3,0	0,0	0,1	1,03	1,4	1,32			96	271	340	0,82	12,0	36,3	2,06	630	H2O	0,0	14,1	0	0	53,4	117	2	14	76	29,5	19,9		
19	1994-01-11	18:00	T 35-5	4,0	0,0	0,3	0,27	1,6	1,32	303	52,0	1,94	97	311	317	0,48	5,7	47,5	1,98	0	none	0,0	0,0	0	0	54,8	121	2	14	77	26,4	61,2	
20	1994-01-11	18:15	T 35-5	4,0	0,0	2,2	0,61	1,4	1,33			94	320	324	0,62	5,0	54,9	1,97	0	none	0,0	0,0	0	0	55,3	121	2	17	98	24,2	69,7		
21	1994-01-11	18:30	T 35-5	4,0	0,0	0,0	1,03	1,4	1,30			98	304	353	0,82	8,8	54,0	1,97	0	none	0,0	0,0	0	0	56,1	121	2	17,4	98	23,9	67,8		



# Datasheet of HBF-Trailertests

Projectnr.: 88-24110/0

Code: REDMUD-V

Customer: INTERALUMINA Pto. Ordaz/Venezuela

Material: Redmud

Cakeforming angle: 165°

Andritz-Personal: H.Riemer /W. Wiesenhoffer

Filtercloth: ZBF-08-1050-BK27 / GKD 35 / GKD165

Interalumina-Personal: P.Murgia/M.Norriea

Filtrarea: 2.0 m<sup>2</sup>

A.Guillermo/C.Rublo/A.Parras

Y.Mareno/J.L.Lares

Test- nr.	Datum time	Test- nr. number	Feed- tank Bar	Vessel press Bar	Press CFL	Press CDL	Filter- speed U/min	Feed- flow m <sup>3</sup> /h	Feed- density g/l	Feed- conc Na2O	Feed FMC	Feed temp °C	Airflow Compr Nm <sup>3</sup> /h	Airflow Filtrate Nm <sup>3</sup> /h	Filtrate- flow m <sup>3</sup> /h	Filtrate- conc g/l	Filtrate Na2O	Filtr FMC	Wash Poly	Poly Type	Poly Conc	usage Steam kg/h	Steam flow kg/h	Steam temp °C	Disch time sec	No of cycles	disch mass kg	Tonnage kg/m <sup>3</sup>	residue moisture %	dry moisture %		
MWTTUJ	hh:mm																															
22	1994-01-12 16:35	755-14	3.0	0.0	1.9	0.25	1.4	1.30	262	55.3	1.99	94	287	425	1.05	4.4	60.2	1.87	0 none	0.0	0.0	0	0	47.1	121	2	14.5	78	27.7	64.0	82	4.4
23	1994-01-12 16:44	755-14	3.0	0.0	1.5	0.59	1.2	1.35		88	216	339	0.54	6.0	59.8	1.98	0 none	0.0	0.0	0	0	47.8	122	2	16	83	29.6	50.5	64	2		
24	1994-01-12 17:04	755-14	3.0	0.0	1.3	0.99	1.4	1.38		89	207	293	0.60	9.4	57.8	1.89	0 none	0.0	0.0	0	0	50.6	121	2	20.7	109	28.9	42.9	4.6	2		
25	1994-01-12 17:38	755-14	3.0	0.0	1.0	1.51	1.2	1.33		80	246	283	0.65	8.0	55.3	1.93	0 none	0.0	0.0	0	0	50.6	121	2	23.8	129	26.9	48.9	14	2		
26	1994-01-12 18:03	755-14	4.0	0.0	2.8	0.25	0.9	1.38	329	56.9	2.02	76	261	284	0.39	4.4	56.5	1.99	0 none	0.0	0.0	0	0	50.4	123	2	14	75	27.02	55.6	66	4
27	1994-01-12 19:05	755-14	4.0	0.0	2.9	0.25	1.5	1.36		101	269	404	0.97	2.2	59.4	1.87	0 none	0.0	0.0	0	0	52.8	123	2	19	105	24.7	63	56	2		
28	1994-01-12 19:14	755-14	4.0	0.0	2.6	0.61	1.9	1.34		102	234	353	0.74	1.6	58.8	1.81	0 none	0.0	0.0	0	0	53.3	123	2	25	146	20.3	65.2	45	2		
29	1994-01-12 19:24	755-14	4.0	0.0	2.5	1.05	1.8	1.37		102	242	321	0.84	5.0	59.4	1.85	0 none	0.0	0.0	0	0	57.5	123	2	30	159	27.5	67.0	235	2		
30	1994-01-12 19:35	755-14	4.0	0.0	2.3	1.53	1.9	1.40	319	56.9	1.99	102	211	278	0.80	9.0	59.4	1.82	0 none	0.0	0.0	0	0	59.8	123	2	34.8	184	27.9	64.7	215	2
31	1994-01-12 20:00	755-14	5.0	0.0	3.5	0.27	1.5	1.40	306	57.4	2.08	94	348	432	1.16	1.4	57.4	1.82	0 none	0.0	0.0	0	0	59.8	123	2	19	102	26.8	67.2	230	1
32	1994-01-12 20:27	755-14	5.0	0.0	3.2	0.59	1.2	1.40		78	311	385	0.61	4.2	58.7	1.82	0 none	0.0	0.0	0	0	59.5	124	2	21	109	28.7	60.9	206	3		
33	1994-01-12 20:58	755-14	5.0	0.0	2.8	1.06	1.3	1.42	303	59.4	1.92	80	350	444	1.07	5.8	59.4	1.86	0 none	0.0	0.0	0	0	58.1	123	2	19.5	104	26.6	56.4	207	2
34	1994-01-12 21:26	755-14	5.0	0.0	2.5	1.22	0.3	1.41		80	396	304	1.27	10.8	59.8	2.07	0 none	0.0	0.0	0	0	55.6	124	2	35.6	158	38.8	47.9	217	2		
35	1994-01-13 17:50	735-14	4.0	0.0	2.9	0.19	1.2	1.43	392	60.7	2.06	84	192	314	0.42	0.8	55.3	2.07	0 none	0.0	0.0	0	0	46.1	122	2	20.3	111	26.04	64.9	133	1
36	1994-01-13 18:01	735-14	4.0	0.0	2.6	0.59	1.4	1.46		84	202	331	0.58	3.0	0 none	0.0	0.0	0	0	47.9	122	2	29	156	26.7	64.0	119	3				
37	1994-01-13 18:12	735-14	4.0	0.0	2.3	0.98	1.5	1.45		86	176	299	0.64	4.6	0 none	0.0	0.0	0	0	49.6	120	2	36.3	200	26.32	64.9	216	3				
38	1994-01-13 18:25	735-14	4.0	0.0	0.0	0.98	1.5	1.37		88	185	236	0.67	7.2	608 H2O	0.0	7.2	0	0	50.2	121	2	28	149	28.2	21.3	60.0	3				
39	1994-01-13 18:36	735-14	4.0	0.0	2.0	1.50	1.3	1.37		84	218	306	0.97	6.4	0 none	0.0	0.0	0	0	51.1	121	2	39.4	219	25.4	65.4	217	2				
40	1994-01-13 18:47	735-14	4.0	0.0	2.0	2.02	2.0	1.43		82	258	346	0.63	7.4	0 none	0.0	0.0	0	0	52.6	121	2	42.9	235	26.3	64.2	215	2				
41	1994-01-13 19:04	735-14	5.0	0.0	4.0	0.22	1.4	1.62	562	55.3	2.02	86	284	372	0.43	2.2	58.6	2.01	0 none	0.0	0.0	0	0	54.1	123	2	20.9	115	25.01	58.5	66	6
42	1994-01-13 19:16	735-14	5.0	0.0	3.6	0.57	1.5	1.43		90	291	340	0.48	2.4	0 none	0.0	0.0	0	0	54.5	122	2	31.4	176	23.92	54.8	211	4				
43	1994-01-13 19:29	735-14	5.0	0.0	3.2	1.00	1.8	1.47		88	260	304	0.52	6.7	0 none	0.0	0.0	0	0	55.4	123	2	49.6	230	22.26	58.5	210	4				
44	1994-01-13 19:41	735-14	5.0	0.0	3.2	1.51	2.3	1.47		90	258	278	0.82	4.6	0 none	0.0	0.0	0	0	56.9	124	2	50.6	298	19.00	54.2	217	4				
45	1994-01-13 19:53	735-14	5.0	0.0	2.9	1.98	2.1	1.48		91	345	477	0.93	4.8	0 none	0.0	0.0	0	0	58.2	123	2	48	279	21.12	77.2	222	1				
46	1994-01-13 20:05	735-14	5.0	0.0	0.0	1.97	1.9	1.48		91	204	156	1.01	9.6	600 H2O	0.0	5.3	0	0	58.2	123	2	45.5	260	21.74	40.0	21	1				
47	1994-01-13 20:17	735-14	5.0	0.0	0.0	1.52	1.9	1.45		92	232	206	1.13	5.0	600 H2O	0.0	6.4	0	0	57.2	122	2	40.4	239	19.54	28.6	210	2				
48	1994-01-13 20:30	735-14	5.0	0.0	0.0	0.99	2.0	1.46		90	254	284	0.88	7.0	599 H2O	0.0	6.7	0	0	56.4	123	2	34.2	193	23.12	26.2	200	3				
49	1994-01-13 20:39	735-14	5.0	0.0	0.0	0.59	1.6	1.49		90	307	398	0.92	8.2	495 H2O	0.0	6.3	0	0	55.7	123	2	29.8	166	23.75	25.0	200	4				



# Datasheet of HBF-Trailertests

Projectnr.: 68-24110/0

Code: REDMUD-V

Customer: INTERALUMINA Pto. Ordaz/Venezuela

Material: Redmud

Cakeforming angle: 165°

Andritz-Personal: H.Riemer /W.Wiesenthaler

Filtercloth: ZBF-08-1050-SK27 / GKD 35 / GKD165

Interalumina-Personal: P.Murgia/M.Noriega

Filterarea: 2,0 m<sup>2</sup>

A.Guillermo/C.Rubio/A.Parra

Y.Mareno/J.L.Lares

Test- nr.	Datum time	Test- nr.	Feed- tank	Vessel press	Press CFL	Press Col	Filter- speed	Feed flow	Feed density	Feed conc	Feed Na2O	Feed FMC	Feed temp	Airflow Compr.	Airflow Filtrate	Filtrate flow	Filtrate conc	Filtrate Na2O	Filtrate FMC	Filtrate Poly	Wash Poly	Poly usage	D-press Steam	Steam flow	Steam temp	Ditch time	Time of mass	Spur sec	Uptime Cycles	Intervall min	Temp °C	Temp °C	Temp °C	Temp °C
MARTIN/JJ	hh:mm	number	Bar	Bar	Bar	Bar	U/min	m <sup>3</sup> /h	g/l	g/l	g/l	°C	Nm <sup>3</sup> /h	Nm <sup>3</sup> /h	g/h	g/l	Uh	%	m <sup>3</sup> /h	mbar	kg/h	°C	sec	kg	min	%	kg	min	kg	min				
50	1994-01-13 20:56	T35-14	5.8	0.0	4.2	0.59	2.0	1.44	422	57.4	1.85	92	325	364	0.59	1.8	55.5	0	none	0.0	0.0	0	0	57.7	123	2	34.5	194	23.26	66.1	1.17	4.1		
51	1994-01-13 21:06	T35-14	5.8	0.0	4.0	1.00	2.0	1.46				92	313	336	0.62	2.6		0	none	0.0	0.0	0	0	58.6	122	2	40.2	234	21.12	69.7	2.14	3.6		
52	1994-01-13 21:18	T35-14	5.8	0.0	4.0	1.51	2.4	1.45				92	292	308	0.67	3.2		0	none	0.0	0.0	0	0	60.1	123	2	47.1	264	23.48	66.1	1.77	3.1		
53	1994-01-13 21:30	T35-14	5.8	0.0	4.0	2.02	2.3	1.41				92	256	290	0.88	4.0		0	none	0.0	0.0	0	0	61.1	122	2	59	329	24.14	63.6	2.16	3.1		
54	1994-01-13 21:42	T35-14	5.8	0.0	3.8	2.48	2.6	1.44				92	248	294	1.00	4.8		0	none	0.0	0.0	0	0	62.5	123	2	62.4	351	23.42	64.3	1.17	3.1		
55	1994-01-13 21:53	T35-14	5.8	0.0	0.0	2.47	2.3	1.46	475	58.1	2.02	90	237	222	1.04	5.8	45.0	468	H2O	0.0	3.8	0	0	61.4	123	2	53.2	307	21.13	30.0	3.00	2.1		
56	1994-01-13 22:05	T35-14	5.8	0.0	0.0	2.02	2.2	1.40				92	259	296	0.78	5.0		473	H2O	0.0	3.7	0	0	60.3	123	2	47.1	260	24.81	31.7	2.31	2.1		
57	1994-01-13 22:13	T35-14	5.8	0.0	0.0	1.54	2.3	1.36				92	279	360	0.83	4.2		475	H2O	0.0	4.3	0	0	58.7	122	2	41.5	234	23.44	26.5	3.00	2.1		
58	1994-01-13 22:25	T35-14	5.8	0.0	0.0	1.04	1.8	1.49				90	313	386	0.91	4.4		479	H2O	0.0	5.0	0	0	58.9	122	2	35.5	197	24.5	21.5	3.00	2.1		
59	1994-01-13 22:40	T35-14	4.0	0.0	0.0	1.04	2.0	1.47				90	211	212	1.06	6.4		528	H2O	0.0	5.9	0	0	58.1	119	2	31.8	182	24.48	27.5	3.00	2.1		
60	1994-01-13 22:48	T35-14	4.0	0.0	0.0	1.53	2.5	1.46	430	55.7	2.00	88	188	132	1.04	8.0	37.1	539	H2O	0.0	4.7	0	0	55.9	119	2	39.5	222	25.68	33.5	2.13	2.1		
61	1994-01-13 22:57	T35-14	4.0	0.0	0.0	0.61	1.8	1.49				87	214	271	0.80	7.6		526	H2O	0.0	7.6	0	0	54.9	119	2	25.1	144	24.24	26.2	3.00	2.1		
62	1994-01-13 23:09	T35-14	3.0	0.0	0.0	0.29	1.6	1.46				86	181	183	0.86	7.6		577	H2O	0.0	11.7	0	0	51.6	117	2	17.6	103	23.88	20.0	3.00	2.1		
63	1994-01-13 23:18	T35-14	3.0	0.0	0.0	0.60	1.9	1.43	466	57.4	2.10	85	181	157	0.91	10.8	28.8	595	H2O	0.0	6.9	0	0	51.9	117	2	27.6	154	27.09	24.2	3.00	2.1		
64	1994-01-13 23:27	T35-14	3.0	0.0	0.0	1.05	2.0	1.43				86	150	102	0.96	8.8		595	H2O	0.0	6.5	0	0	51.5	117	2	30	168	27.31	22.0	3.00	2.1		
65	1994-01-14 17:58	T35-17	0.7	0.0	0.0	0.25	1.4	1.32	387	17.1	2.14	78	149	319	0.50	3.6	16.5	2.18	0	none	0.0	0.0	0	0	40.0	110	2	19.6	111	30.7	21.0	2.57	6.1	
66	1994-01-14 18:06	T35-17	0.7	0.0	0.0	0.61	1.7	1.37				80	90	134	0.55	3.2		0	none	0.0	0.0	0	0	41.8	109	2	25	143	30.7	21.0	2.62	6.1		
67	1994-01-14 18:14	T35-17	0.7	0.0	0.0	1.04	2.1	1.36				75	47	28	0.58	3.7		0	none	0.0	0.0	0	0	43.0	110	2	33.7	188	31.8	18.9	2.57	3.1		
68	1994-01-14 18:27	T35-17	2.0	0.0	0.4	1.54	2.5	1.34				80	125	289	0.91	2.8		0	none	0.0	0.0	0	0	46.2	115	2	53.1	295	29	26.7	2.32	2.1		
69	1994-01-14 18:39	T35-17	3.0	0.0	1.5	1.74	2.6	1.37				80	163	323	1.14	2.6		0	none	0.0	0.0	0	0	48.6	117	1	30	331	24.9	22.1	2.57	2.1		
70	1994-01-14 18:51	T35-17	4.0	0.0	2.2	1.99	2.8	1.33				80	247	429	1.23	4.0		0	none	0.0	0.0	0	0	51.0	120	1	32.8	349	29.2	21.0	2.31	3.1		
71	1994-01-14 19:03	T35-17	5.0	0.0	3.3	1.99	2.7	1.35				75	214	244	1.30	1.8		0	none	0.0	0.0	0	0	52.8	120	1	35	375	28.5	18.5	3.00	2.1		
72	1994-01-14 19:10	T35-17	5.0	0.0	3.3	2.34	2.7	1.32				80	185	233	1.37	2.2		0	none	0.0	0.0	0	0	52.7	121	1	36	373	20.2	18.7	3.00	2.1		
73	1994-01-14 19:24	T35-17	5.8	0.0	4.0	2.07	2.8	1.34	428	15.3	2.12	63	253	322	1.28	1.8	18.6	2.81	0	none	0.0	0.0	0	0	54.3	123	1	37.5	395	26	18.5	3.00	2.1	
74	1994-01-14 19:33	T35-17	5.8	0.0	3.8	2.47	3.4	1.40				68	242	289	1.37	2.8		0	none	0.0	0.0	0	0	54.6	123	1	44	464	28	3.1	3.00	2.1		
75	1994-01-14 19:43	T35-17	5.8	0.0	3.8	2.97	3.5	1.40				68	271	367	1.40	1.8		0	none	0.0	0.0	0	0	55.3	123	1	49	520	27.3	17.9	3.00	2.1		
76	1994-01-14 19:49	T35-17	5.8	0.0	4.0	1.03	3.3	1.37				68	305	400	1.05	2.2		0	none	0.0	0.0	0	0	55.3	124	1	32.4	349	26	20.0	3.00	5.1		



# Datasheet of HBF-TrailerTests

Projectnr.: 88-24110/0

Code: REDMUD-V

Customer: INTERALUMINA Pto. Ordaz/Venezuela

Material: Redmud

Filtercloth: 2BF-08-1050-SK27 / GKD 35 / GKD165

Filterarea: 2,0 m<sup>2</sup>

Cakeforming angle: 165°

Andritz-Personal: H.Riemer / W. Wiesenhofe

Interalumina-Personal: P.Murgia / M.Noriega

A.Guillermo / C.Rubio / A.Parra

Y.Marcos / J.L.Lares

Test- nr.	Datum	Test- time	Feed- tank	Vessel press	Press CFL	Filter- speed	Feed- flow	Feed- density	Feed- conc	Feed- Na2O	Feed- FMC	Feed- temp	Airflow Compr	Airflow Filtrate	Filtrate- flow	Filtrate- conc	Filtrate- Na2O	Filtrate- FMC	Wash Poly	Poly Type	Poly Conc	Poly usage	D-press Steam	Steam flow	Dish- temp	Dish- time	disc mass	Tonnage	residual cake	Cake temp	disc size		
			dm³	Bar	Bar	U/min	m³/h	g/l	g/l	Na2O	FMC	°C	Nm³/h	Nm³/h	m³/h	g/l	g/l	l/h	%	m³/h	mbar	kg/h	°C	sec	Cycles	kg	kg/m³	%	g				
77	1994-01-18	13.53	735-17	0.7	0.0	0.0	0.25	1.6	1.45	501	18.2	86	68	14	0.29	1.4	17.9	0	none	0.0	0.0	0	0	48.9	110	2	23.5	136	29.4	25.5	7.2		
78	1994-01-18	14.02	735-17	0.8	0.0	0.0	0.61	1.9	1.42			86	50	0	0.45	1.2		0	none	0.0	0.0	0	0	48.8	111	2	36	204	30	23.1	4.7		
79	1994-01-18	14.14	735-17	0.8	0.0	0.0	1.03	2.0	1.43			86	52	0	0.65	3.4		0	none	0.0	0.0	0	0	50.0	112	2	51.3	291	29.7	24.0	3.5		
80	1994-01-18	14.30	735-17	2.0	0.0	1.0	0.25	1.5	1.44			86	170	300	0.28	0.2		0	none	0.0	0.0	0	0	51.0	117	2	30.8	170	28.5	25.4	6.5		
81	1994-01-18	14.39	735-17	2.0	0.0	0.8	0.61	1.9	1.46			86	137	250	0.80	1.0		0	none	0.0	0.0	0	0	51.2	117	2	41.6	231	27.8	24.8	5.8		
82	1994-01-18	16.22	735-17	2.0	0.0	0.8	1.02	2.0	1.44			86	102	190	0.85	4.6		0	none	0.0	0.0	0	0	48.8	116	2	56.7	313	28.6	22.0	4.1		
83	1994-01-18	16.30	735-17	2.0	0.0	0.4	1.52	2.2	1.42	480	18.2	86	89	154	0.95	3.8	18.6	0	none	0.0	0.0	0	0	50.8	117	2	89	378	28.8	22.9	3.0		
84	1994-01-18	16.39	735-17	2.0	0.0	0.3	1.88	2.3	1.43			84	123	132	1.05	4.4		0	none	0.0	0.0	0	0	51.4	117	2	67.8	367	29.7	24.1	3.1		
85	1994-01-18	16.50	735-17	3.0	0.0	1.8	0.26	1.3	1.43			84	204	368	0.50	2.6		0	none	0.0	0.0	0	0	52.0	121	1	17	183	27.9	23.1	6.4		
86	1994-01-18	16.57	735-17	3.0	0.0	1.6	0.68	1.9	1.41			82	184	316	0.65	2.0		0	none	0.0	0.0	0	0	51.8	122	1	23.4	250	27.8	25.4	5.5		
87	1994-01-18	17.04	735-17	3.0	0.0	1.5	1.06	2.0	1.43	235	18.1	82	168	292	0.85	2.4	18.7	0	none	0.0	0.0	0	0	52.1	122	1	27	286	28.5	24.3	4.4		
88	1994-01-18	17.13	735-17	3.0	0.0	1.3	1.50	2.3	1.45			83	194	407	0.91	4.0		0	none	0.0	0.0	0	0	52.5	122	1	30.7	325	28.2	25.3	3.0		
89	1994-01-18	17.20	735-17	3.0	0.0	1.3	1.99	2.3	1.43			84	206	391	1.00	5.2		0	none	0.0	0.0	0	0	53.0	122	1	35.5	376	28.2	23.4	3.0		
90	1994-01-18	18.23	735-17	3.0	0.0	1.3	2.50	2.7	1.41			86	193	369	1.19	4.0		0	none	0.0	0.0	0	0	55.5	123	1	39.5	435	24.8	25.9	3.5		
91	1994-01-18	18.33	735-17	4.0	0.0	3.6	0.61	2.0	1.39			86	236	417	0.75	2.2		0	none	0.0	0.0	0	0	58.4	127	1	23.3	237	28	21.4	5.1		
92	1994-01-18	18.42	735-17	4.0	0.0	2.5	1.11	2.3	1.35			84	238	378	0.89	2.6		0	none	0.0	0.0	0	0	58.1	126	1	27.5	278	28.8	21.9	4.3		
93	1994-01-19	18.50	735-17	4.0	0.0	2.3	0.59	1.8	1.53	496	13.4	2.28	90	212	377	0.71	1.2	13.9	2.24	0	none	0.0	0.0	0	0	48.2	128	1	30.8	318	26.76	18.2	7.6
94	1994-01-19	18.57	735-17	4.0	0.0	2.0	1.00	2.0	1.51			86	197	380	0.90	1.0		0	none	0.0	0.0	0	0	49.0	127	1	39.1	404	27.05	20.8	5.6		
95	1994-01-19	19.04	735-17	4.0	0.0	2.0	1.52	2.2	1.51			86	172	326	1.00	2.0		0	none	0.0	0.0	0	0	50.0	126	1	42.9	444	27.23	19.3	4.1		
96	1994-01-19	19.10	735-17	4.0	0.0	1.8	2.00	2.2	1.52			86	208	372	1.10	2.6		0	none	0.0	0.0	0	0	50.7	126	1	45.7	477	26.76	18.8	3.8		
97	1994-01-19	19.19	735-17	5.0	0.0	2.8	0.59	1.6	1.53			86	299	452	0.73	1.6		0	none	0.0	0.0	0	0	52.9	129	1	31.2	328	24.74	18.2	7.7		
98	1994-01-19	19.26	735-17	5.0	0.0	2.8	1.50	2.0	1.52	502	13.6	2.30	86	267	392	1.10	1.6	14.0	2.20	0	none	0.0	0.0	0	0	52.8	130	1	44.6	458	25.78	17.4	4.6
99	1994-01-19	19.34	735-17	5.0	0.0	2.7	2.01	2.2	1.49			84	236	369	1.14	2.0		0	none	0.0	0.0	0	0	53.3	129	1	50.6	523	25.63	20.5	3.9		
100	1994-01-19	19.44	735-17	5.0	0.0	2.5	2.49	2.4	1.51			84	257	352	1.18	2.8		0	none	0.0	0.0	0	0	54.0	130	1	53.5	553	25.33	20.7	3.8		
101	1994-01-19	19.51	735-17	5.0	0.0	2.5	2.99	2.5	1.53			84	235	333	1.24	2.8		0	none	0.0	0.0	0	0	54.5	130	1	56.5	600	23.52	19.1	3.1		
102	1994-01-19	20.00	735-17	5.8	0.0	3.8	0.57	1.3	1.51			84	258	327	0.78	2.0		0	none	0.0	0.0	0	0	55.7	133	1	32.6	352	20.25	18.4	7.5		
103	1994-01-19	20.07	735-17	5.8	0.0	3.4	1.50	1.9	1.54	546	14.1	2.15	84	270	365	1.09	1.2		0	none	0.0	0.0	0	0	55.2	132	1	45	476	22.44	20.0	4.5	
104	1994-01-19	20.13	735-17	5.8	0.0	3.2	2.02	2.1	1.50			84	258	343	1.15	2.0		0	none	0.0	0.0	0	0	55.3	131	1	51.3	549	22.09	20.3	3.5		
105	1994-01-19	20.19	735-17	5.8	0.0	3.2	2.49	2.3	1.51			84	285	330	1.22	2.6		0	none	0.0	0.0	0	0	55.5	131	1	56	618	19.7	28.4	3.0		
106	1994-01-19	20.26	735-17	5.8	0.0	3.0	3.01	2.4	1.50			84	247	328	1.23	2.4		0	none	0.0	0.0	0	0	55.8	131	1	61.5	645	23.88	20.6	3.0		



# Datasheet of HBF-Trailer tests

Projectnr.: 88-24110/0

Code: REDMUD-V

Customer: INTERALUMINA Pto. Ordaz/Venezuela

Material: Redmud

Cakeforming angle: 185°

Andritz-Personal: H.Riemer /W.Wiesenthaler

Filtercloth: ZBF-06-1050-BK27 / GKD 35 / GKD105

Interalumina-Personal: P.Murgia/M.Noriega

Filterarea: 2,0 m²

A.Guillermo/C.Rubio/A.Parras

Y.Mareno/J.L.Laress

Test-	Datum	Test-	Feed-	Vessel	Press	Press	Filter-	Feed-	Feed-	Feed-	Feed-	Feed	Feed	Feed	Airflow	Airflow	Filtrate-	Filtrate-	Filtrate	Filtrate	Filtrate	Filtrate	Wash	Poly	Poly	Poly	D-press	Steam	Steam	Disc	No.	disc	Through-	residue	recycle	reject	reject
n°		time	tank	press	CFL	CDL	speed	flow	density	conc.	Na2O	FMC	temp	Compr	Filtrate	flow	conc	Na2O	FMC	Poly	Type	Conc	usage	Steam	flow	temp	time	of	mass	kg/m³	Waste	kg/m³	kg/m³	kg			
			number	Bar	Bar	Bar	U/min	m³/h	t/m³	g/l	g/l	°C	Nm³/h	Nm³/h	m³/h	g/l	g/l	l/h	%	min	mbar	kg/h	°C	sec	Cycles	kg	kg/m³	%	kg	kg/m³	%	kg					
107	1994-01-19	20 33	735-17	5,8	0,0	0,0	3,01	2,3	1,49	537	13,9	2,30	84	223	273	1,31	3,6	12,7	2,28	405	H2O	0,0	1,6	0	0	55,8	130	1	50	525	24,12	23,3					
108	1994-01-19	20 39	735-17	5,8	0,0	0,0	2,49	2,1	1,50				82	226	283	1,40	2,4	12,0	2,40	412	H2O	0,0	1,8	0	0	55,5	130	1	45,6	485	23,26	1,5					
109	1994-01-19	20 47	735-17	5,8	0,0	0,0	2,02	1,9	1,51				82	252	281	1,26	2,4	11,6	2,28	410	H2O	0,0	1,9	0	0	55,5	130	1	44,1	475	22,26	21,8					
110	1994-01-19	20 54	735-17	5,8	0,0	0,0	1,50	1,7	1,49				82	229	284	1,23	2,8	11,6	2,34	398	H2O	0,0	2,2	0	0	55,3	130	1	40	439	20,7	2,0					
111	1994-01-19	21 02	735-17	5,8	0,0	0,0	1,00	1,4	1,50				82	280	325	1,13	2,4	11,1	2,38	381	H2O	0,0	2,2	0	0	55,0	130	1	35,6	381	23,21	1,9					
112	1994-01-19	21 10	735-17	5,8	0,0	0,0	0,57	1,3	1,49				81	308	408	1,11	4,2	10,2	2,25	379	H2O	0,0	2,8	0	0	54,7	130	1	28,1	273	24,54	2,0					
113	1994-01-19	21 18	735-17	5,0	0,0	0,0	0,58	1,2	1,49	510	13,9	2,39	80	250	328	1,08	5,0	10,0	2,38	421	H2O	0,0	3,1	0	0	53,0	127	1	25,2	287	25,38	1,8					
114	1994-01-19	21 25	735-17	5,0	0,0	0,0	1,56	1,7	1,49				78	178	197	1,27	5,6	10,4	2,42	420	H2O	0,0	2,6	0	0	53,4	127	1	29,6	310	28,39	1,1					
115	1994-01-19	21 31	735-17	5,0	0,0	0,0	2,02	1,8	1,50				78	162	163	1,25	5,0	10,0	2,30	420	H2O	0,0	2,1	0	0	53,5	128	1	37,6	393	25,6	1,0					
116	1994-01-19	21 43	735-17	4,0	0,0	0,0	0,59	1,3	1,46				78	179	239	0,98	5,0	9,8	2,36	480	H2O	0,0	4,1	0	0	52,3	127	1	21,7	228	25,75	1,2					
117	1994-01-19	21 48	735-17	4,0	0,0	0,0	2,02	1,9	1,45				79	124	115	1,21	6,8	10,0	2,34	480	H2O	0,0	2,4	0	0	52,6	126	1	35,6	371	27	1,5					
118	1994-01-20	12 01	735-5	0,7	0,0	0,0	0,24	1,0	1,34				88	61	68	0,21					0 none	0,0	0,0	0	0	45,2	113	2	13,9	77	30,25	44,3					
119	1994-01-20	12 15	735-5	0,7	0,0	0,0	0,57	1,5	1,37				86	50	4	0,37	2,2			0 none	0,0	0,0	0	0	48,1	114	2	20,2	111	30,59	43,9						
120	1994-01-20	12 30	735-5	2,0	0,0	0,9	0,25	1,2	1,39	360	40,2	2,05	84	174	310	0,39	0,6	40,9	2,20	0 none	0,0	0,0	0	0	50,0	126	2	16,7	86	28	41,2						
121	1994-01-20	12 46	735-5	2,0	0,0	0,3	0,61	1,1	1,38				84	191	384	0,52	1,2			0 none	0,0	0,0	0	0	50,8	126	2	21,6	111	28,84	42,5						
122	1994-01-20	12 56	735-5	2,0	0,0	0,0	1,02	1,1	1,39				84	199	387	0,58	3,4			0 none	0,0	0,0	0	0	51,4	125	2	26,6	138	28,91	46,5						
123	1994-01-20	13 21	735-5	3,0	0,0	1,5	0,60	1,5	1,31	344	40,0	2,07	94	249	405	0,80	3,0			0 none	0,0	0,0	0	0	53,8	131	2	31,6	158	27,25	45,7						
124	1994-01-20	13 33	735-5	3,0	0,0	1,2	1,03	1,6	1,31				96	200	344	0,72	0,8	40,9	2,07	0 none	0,0	0,0	0	0	54,5	131	2	36,2	181	27,15	47,1						
125	1994-01-20	13 48	735-5	3,0	0,0	1,1	1,50	1,6	1,32				98	198	302	0,93	4,0			0 none	0,0	0,0	0	0	55,8	131	2	41,9	208	27,75	46,6						
126	1994-01-20	14 05	735-5	4,0	0,0	2,3	0,59	1,4	1,26				100	240	331	0,85	3,0			0 none	0,0	0,0	0	0	56,7	135	2	32,2	154	26	41,3						
127	1994-01-20	14 17	735-5	4,0	0,0	2,2	1,00	1,6	1,29	318	40,4	2,11	100	209	300	0,90	2,8	41,7	2,07	0 none	0,0	0,0	0	0	57,3	135	2	37,7	154	27,23	44						
128	1994-01-20	14 27	735-5	4,0	0,0	2,0	1,51	1,6	1,32				100	207	266	1,03	7,6			0 none	0,0	0,0	0	0	57,8	134	2	49,4	264	20,44	62,8						
129	1994-01-20	14 37	735-5	5,0	0,0	3,2	0,59	1,3	1,26				102	307	427	0,86	2,6			0 none	0,0	0,0	0	0	59,2	137	2	33,3	168	23,42	55,6						
130	1994-01-20	14 47	735-5	5,0	0,0	2,9	1,00	1,5	1,32	348	40,7	2,13	102	280	390	0,82	2,0	41,7	2,06	0 none	0,0	0,0	0	0	59,0	137	2	41,7	212	22,51	56,5						
131	1994-01-20	14 57	735-5	5,0	0,0	2,8	1,50	1,6	1,35				100	273	356	0,97	3,0			0 none	0,0	0,0	0	0	59,3	136	2	45,2	217	27,12	45,4						
132	1994-01-20	15 11	735-5	5,8	0,0	4,0	0,59	1,5	1,34				102	345	440	0,89	2,2			0 none	0,0	0,0	0	0	60,3	139	2	34,7	163	27,25	45,2						
133	1994-01-20	15 19	735-5	5,8	0,0	3,7	1,01	1,5	1,26				102	311	401	0,90	2,4			0 none	0,0	0,0	0	0	60,4	138	2	40,8	192	27,98	43,0						
134	1994-01-20	15 32	735-5	5,8	0,0	3,6	1,48	1,7	1,25	361	40,0	2,15	102	278	375	0,93	2,8	42,8	2,11	0 none	0,0	0,0	0	0	60,9	137	2	46,1	224	26,14	50,0						
135	1994-01-20	15 45	735-5	5,8	0,0	3,4	2,00	1,7	1,28				100	293	357	1,00	2,8			0 none	0,0	0,0	0	0	60,9	137	2	50,4	242	26,88	47,5						



# Datasheet of HBF-Trailer tests

Projectnr.: 88-24110/0

Code: REDMUD-V

Customer: INTERALUMINA Pto. Ordaz/Venezuela

Material: Redmud

Cakeforming angle: 185°

Andritz-Personal: H.Riemer /W. Wiesenthaler

Filtercloth: ZBF-08-1050-SK27 / GKD 35 / GKD185

Interalumina-Personal: P.Murgia/M.Norloga

Filterarea: 2,0 m<sup>2</sup>

A.Guillermo/C.Rubio/A.Parra

Y.Marcos/J.L.Lares

Test	Datum	Test	Feed	Vessel	Press	Press	Filter	Feed	Feed	Feed	Feed	Feed	Feed	Airflow	Airflow	Filtrate	Filtrate	Filtrate	Filtrate	Wash	Poly	Poly	Poly	Press	Steam	Steam	Discch	No	discch	orange	residue	Cake	Time	
#		time	tank	press	CFL	CFL	CDL	speed	flow	density	conc	Na2O	FMC	temp	Compr	Filtrate	flow	conc	Na2O	FMC	Poly	Type	Conc	usage	Steam	flow	temp	time	of	mass	city	Misturn	Seca	min
136	1994-01-20	18:12	T35-5	5.8	0.0	0.0	1.04	1.2	1.34			95	295	434	1.09	7.0	26.8	2.21	480	H2O	0.0	8.9	0	0	54.2	131	2	29.8	160	21.83	27.4	0.00	3.1	
137	1994-01-20	18:29	T35-5	5.8	0.0	0.0	1.52	1.2	1.31	375	40.0	2.06	96	239	364	1.05	0.4	27.6	2.13	480	H2O	0.0	5.3	0	0	54.4	131	2	33.6	171	26.28	26.4	2.62	2.6
138	1994-01-20	18:38	T35-5	5.8	0.0	0.0	2.04	1.1	1.28			98	201	282	1.05	5.4	27.2	2.08	480	H2O	0.0	4.7	0	0	54.5	130	2	35.1	169	30.21	17.3	2.12	2.0	
139	1994-01-20	18:51	T35-5	5.0	0.0	0.0	1.50	1.1	1.35			98	179	255	1.04	5.4	26.8	2.14	531	H2O	0.0	5.8	0	0	53.6	129	2	31.3	154	29.55	17.2	0.00	2.0	
140	1994-01-20	19:00	T35-5	5.0	0.0	0.0	1.03	1.1	1.31	378	40.4	2.10	98	233	327	1.08	7.8	26.8	2.11	528	H2O	0.0	8.0	0	0	53.5	129	2	31.5	160	27.38	21.9	0.00	3.0
141	1994-01-20	19:10	T35-5	5.0	0.0	0.0	0.61	1.2	1.25			100	259	407	1.11	11.4	24.5	2.21	524	H2O	0.0	7.2	0	0	53.3	129	2	27	139	26.34	22.2	0.00	4.2	
142	1994-01-20	19:20	T35-5	4.0	0.0	0.0	0.62	1.0	1.35			100	157	257	1.07	12.0	23.1	2.27	586	H2O	0.0	7.5	0	0	52.1	128	2	26.3	135	28.02	24.1	2.69	4.0	
143	1994-01-20	19:29	T35-5	4.0	0.0	0.0	1.02	1.4	1.35			98	117	197	1.08	10.8	24.3	2.18	561	H2O	0.0	6.4	0	0	52.9	128	2	30.3	156	27.87	24.3	0.00	4.0	
144	1994-01-20	19:41	T35-5	3.0	0.0	0.0	1.02	1.5	1.34			98	87	127	0.67	10.6	22.7	2.14	601	H2O	0.0	8.9	0	0	52.1	124	2	28	141	30.84	22.4	1.54	2.0	
145	1994-01-22	10:13	T35-18	0.7	0.0	0.0	0.27	0.8	1.30	379	30.1	2.28	94	32	82	0.19	0.2	25.2	2.57	0	none	0.0	0	0	0	41.1	110	3	17.3	100	29.1	32.2	2.46	5.4
146																																		
147	1994-01-22	15:22	T35-18	0.7	0.0	0.0	0.57	1.2	1.25			103	112	145	0.83	104.4	30.9	2.41	0	none	0.0	0.0	0	0	46.8	110	2	33.2	190	29.8	34.1	2.30	4.0	
148	1994-01-22	15:38	T35-18	0.7	0.0	0.0	0.98	1.7	1.29			100	104	107	1.12	152.0	30.5	2.28	0	none	0.0	0.0	0	0	35	111	2	36.2	205	30.3	34.0	2.42	3.0	
149	1994-01-22	15:53	T35-18	2.0	0.0	1.0	0.57	1.2	1.27	386	30.9	2.39	100	148	264	0.90	98.8	30.9	2.29	0	none	0.0	0.0	0	0	51.2	112	2	34	196	28.4	32.5	2.46	4.0
150	1994-01-22	16:04	T35-18	2.0	0.0	1.0	0.98	1.7	1.37			100	136	238	1.13	101.0	30.5	2.28	0	none	0.0	0.0	0	0	51.9	120	2	44	231	29.9	31.0	2.67	3.0	
151	1994-01-22	15:22	T35-18	3.0	0.0	2.1	0.57	1.9	1.37			98	165	311	0.93	93.6	30.5	2.22	0	none	0.0	0.0	0	0	49.2	124	1	17.9	184	26.1	33.9	2.62	4.0	
152	1994-01-22	16:33	T35-18	3.0	0.0	2.8	1.48	2.8	1.35			100	179	337	1.70	173.0	30.5	2.31	0	none	0.0	0.0	0	0	47.3	125	1	34.8	350	29.2	34.1	2.42	3.0	
153	1994-01-22	16:43	T35-18	3.0	0.0	2.0	2.00	3.2	1.25			98	174	349	1.98	164.0	30.5	2.38	0	none	0.0	0.0	0	0	46.7	125	1	34	347	29.1	33.2	2.42	3.0	
154	1994-01-22	16:57	T35-18	4.0	0.0	2.8	0.57	1.8	1.32			99	244	386	0.85	92.0	31.4	2.42	0	none	0.0	0.0	0	0	50.1	130	1	21.0	216	28.4	32.5	2.46	4.0	
155	1994-01-22	17:09	T35-18	4.0	0.0	3.0	1.48	2.9	1.32	396	29.7	2.49	98	253	431	1.43	95.2	30.9	2.41	0	none	0.0	0.0	0	0	50.2	129	1	35.2	346	29.8	34.8	2.46	3.0
156	1994-01-22	17:23	T35-18	5.0	0.0	4.0	0.57	1.9	1.32			100	276	360	1.11	70.6	31.4	2.32	0	none	0.0	0.0	0	0	52.0	132	1	23.2	229	27.7	31.7	2.62	5.0	
157	1994-01-22	17:33	T35-18	5.0	0.0	3.2	1.48	2.8	1.33			100	256	385	1.61	123.8	30.7	2.36	0	none	0.0	0.0	0	0	52.1	133	1	31.9	311	27.2	33.2	2.62	3.0	
158	1994-01-22	17:42	T35-18	5.0	0.0	2.8	2.49	3.1	1.28			98	266	417	1.94	160.0	30.9	2.34	0	none	0.0	0.0	0	0	52.1	134	1	30.5	367	27.4	34.0	2.62	3.0	
159	1994-01-22	17:54	T35-18	5.7	0.0	4.0	0.57	2.1	1.31			101	385	498	0.94	85.0	31.4	2.45	0	none	0.0	0.0	0	0	54.0	135	1	22.7	231	29.9	34.0	2.65	3.0	
160	1994-01-25	09:36	T35-1	0.7	0.0	0.0	0.27	0.5	1.53	404	114	1.60	80	39	71	0.00	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0			
161	1994-01-25	09:59	T35-1	2.1	0.0	0.8	0.27	0.7	1.50			83	158	292	0.19	12.6	87.5	1.64	0	none	0.0	0.0	0	0	42.1	111	2	7.6	49	23.86	22.1	4.43	3.0	
162	1994-01-25	10:19	T35-1	3.1	0.0	1.8	0.29	0.7	1.53			90	211	249	0.18	11.6	111.0	1.61	0	none	0.0	0.0	0	0	42.7	130	2	11.7	62	23.11	12.0	1.28	1.0	
163	1994-01-25	10:42	T35-1	4.0	0.0	2.3	0.27	0.6	1.52	395	116	1.60	88	249	317	0.33	8.2	118.4	1.60	0	none	0.0	0.0	0	0	46.2	129	2	12.7	68	23.2	12.1	1.39	1.0



Projectnr.: 88-24110.0

Code: REDMUD-V

Customer: INTERALUMINA Pto. Ordaz/Venezuela

## Datasheet of HBF-TrailerTests

Material: Redmud

Cakeforming angle: 185°

Andritz-Personal: H.Riemer, W. Wiesenhofer

Interalumina-Personal: P.Murgia/M Noriega

A.Guillermo/C.Rubio/A.Parra

Y.Mareno/J.L.Lares

Filtercloth: ZBF-08-1050-BK27 / GKD 35 / GKD165

Filtrarea: 2.0 m<sup>2</sup>

Test nr.	Datum	Test time	Feed- tank number	Vessel press	Press CFL	Press CDL	Filter- speed	Feed- flow	Feed- density	Feed- Na2O	Feed- FMC	Feed- temp	Airflow	Airflow	Filtrate- flow	Filtrate- conc	Filtrate- Na2O	Filtrate- FMC	Filtrate- Poly	Wash	Poly	Poly	D-press	Steam	Steam	Discr-	Run	act	Storage	residual	dry	Moisture	Time	Flow	Rate	Time	Flow	Rate
				Bar	Bar	Bar	l/m <sup>2</sup>	m <sup>3</sup> /h	g/l	g/l		°C	Nm <sup>3</sup> /h	Nm <sup>3</sup> /h	m <sup>3</sup> /h	g/l	g/l	m <sup>3</sup> /h	mbar	kg/h	°C	sec	Cycles	kg	kg/min	%	g	kg/min	%	s								
154	1994-01-25	10:59	735-1	4.0	0.0	2.2	0.59	0.7	1.52			88	198	243	0.32	8.8			0	none	0.0	0.0	0	0	51.5	129	2	15.7	86	21.72	12.5	137	2					
165	1994-01-25	11:21	735-1	5.0	0.0	2.5	0.25	0.8	1.55			88	294	360	0.30	9.8	120.9		0	none	0.0	0.0	0	0	53.5	133	2	11	57	23.06	11.2	176	3					
166	1994-01-25	11:35	735-1	5.0	0.0	3.0	0.59	0.9	1.54			88	270	312	0.33	9.4			0	none	0.0	0.0	0	0	54.0	136	2	15.3	77	23.82	13.7	136	2					
167	1994-01-25	12:34	735-1	4.8	0.0	2.5	0.25	0.8	1.54	205	100	180	88	274	308	0.62	8.4	42.1	418	H2O	0.0	14.0	0	0	54.5	138	2	12	58	25.29	5.8	178	3					
168	1994-01-25	12:46	735-1	5.0	0.0	1.8	0.59	0.7	1.57			88	205	243	0.63	8.8	49.3	1.58	405	H2O	0.0	12.5	0	0	55.1	136	2	13	64	25.04	7.6	178	3					
169	1994-01-25	13:03	735-1	4.0	0.0	1.0	0.25	0.8	1.56			88	265	299	0.62	8.8	40.9	1.70	424	H2O	0.0	17.9	0	0	54.4	133	2	9.4	48	24.66	34.9	177	3					
170	1994-01-25	16:43	735-19	0.6	0.0	0.0	0.25	0.7	1.34	346	45.4	1.80	88	122	161	0.19	0.4	45.9	1.90	0	none	0.0	0.0	0	0	42.5	110	2	10.8	63	26.22	10.2	144	3				
171	1994-01-25	17:10	735-16	2.0	0.0	1.3	0.27	1.0	1.37			92	188	299	0.41	1.4			0	none	0.0	0.0	0	0	47.2	109	2	15.8	96	26.79	47.7	177	4					
172	1994-01-25	17:20	735-16	2.3	0.0	1.3	0.59	1.3	1.37			90	206	296	0.61	1.2			0	none	0.0	0.0	0	0	48.8	128	2	21.5	113	26.34	44.9	147	4					
173	1994-01-25	17:36	735-16	2.9	0.0	2.0	0.59	1.6	1.30	314	46.2	1.78	88	154	282	0.66	3.8	47.1	1.81	0	none	0.0	0.0	0	0	50.4	130	2	25.2	125	27.99	45.1	154	2				
174	1994-01-25	17:47	735-16	2.9	0.0	2.0	1.01	1.8	1.37			89	159	235	0.66	4.4			0	none	0.0	0.0	0	0	51.3	130	2	29.9	151	26.95	45.0	151	2					
175	1994-01-25	18:08	735-18	4.0	0.0	3.0	0.59	1.8	1.36	313	45.8	1.72	93	194	237	0.62	2.8	47.6	1.72	0	none	0.0	0.0	0	0	54.4	134	2	24.8	122	26.64	40.5	166	2				
176	1994-01-25	18:23	735-18	4.0	0.0	2.7	1.00	1.8	1.37			89	181	244	0.71	4.2			0	none	0.0	0.0	0	0	55.2	134	2	31.2	152	27.38	41.6	156	2					



# Datasheet of HBF-Trailer tests

Projectnr.: 88-24110/0

Code: REDMUD-V

Customer: INTERALUMINA Pto. Ordaz/Venezuela

Material: Redmud

Cakeforming angle: 165°

Andritz-Personal: H Riemer /W Wiesenhofer

Filtercloth: ZBF-08-1050-SK27

Interalumina-Personal: P Murgia/M Noriega

Filterarea: 2,0 m<sup>2</sup>

A.Guillermo/C Ruble/A.Parra

Y Moreno/J.L.Lares

Test	Datum	Test	Feed	Vessel	Press	Press	Filter	Feed	Feed	Feed	Feed	Feed	Feed	Feed	Airflow	Airflow	Filtrate	Filtrate	Filtrate	Filt.	Wash	Poly	Poly	Poly	O-press	Steam	Steam	Dsch	No	dsch	Torrage	residual	Cake	Time	Time
			time	tank	press	CFL	CDL	speed	flow	density	conc	NaO	FMC	temp	Compr	Filtrate	flow	conc	NaO	FMC	Poly	Type	Conc	usage	Steam	flow	temp	time	of	mass	dry	Moisture	Soda	Time	Time
			min	mm	mm	Bar	Bar	Bar	l/min	g/m <sup>3</sup>	g/l	g/l	°C	Nm <sup>3</sup> /h	Nm <sup>3</sup> /h	m <sup>3</sup> /h	g/l	g/l	lh	%	min	mbar	kg/h	°C	sec	Cycles	kg	kg/m <sup>3</sup>	%	s	kg	kg			
<b>Filtercloth ZBF-08-1050-SK27</b>																																			
177	1994-01-28	11 05	735-18	2.0	0.0	0.5	0.57	1.3	1.28	275	23.9	2.28			70	498	0.56	2.2	23.9	2.28	0 none	0.0	0.0	-2.0	427.7	132.2	125	2	24.4	131	25.83	26.7	2.18	3	
178	1994-01-28	11 20	735-18	2.1	0.0	0.4	0.99	1.7	1.31				6		93	498	0.65	2.6	23.3	2.21	0 none	0.0	0.0	-2.6	432.4	129.0	125	2	33.3	181	24.4	28.4	2.26	3	
179	1994-01-28	11 41	735-18	2.0	0.0	1.0	0.25	1.3	1.31				94		73	498	0.80	2.0	23.1	2.30	0 none	0.0	0.0	-2.6	448.5	129.6	128	2	19.8	107	24.17	28.5	2.07	5	
180	1994-01-28	12 07	735-18	3.1	0.0	2.0	0.25	1.6	1.30	300	23.1	2.18	96		106	498	0.33	1.0	23.9	2.25	0 none	0.0	0.0	-4.2	181.9	138.0	132	2	23.6	121	25	29.5	2.57	6	
181	1994-01-28	12 23	735-18	3.1	0.0	1.8	0.57	2.0	1.30	277	23.1	2.21	94		99	498	0.44	0.6	23.9	2.38	0 none	0.0	0.0	-4.0	182.1	139.3	131	2	29.3	148	26.13	28.4	2.59	7	
182	1994-01-28	12 39	735-18	3.1	0.0	1.6	0.98	2.0	1.26				94		94	498	0.44	1.4	24.8	2.30	0 none	0.0	0.0	-4.2	179.5	138.3	131	2	34.8	178	26.25	27.5	2.0	7	
183	1994-01-28	12 59	735-18	3.9	0.0	2.4	0.58	1.6	1.30	308	23.9	2.38	96		141	498	0.84	2.4	22.3	2.25	0 none	0.0	0.0	-4.4	169.6	141.9	136	2	36.1	184	23.39	34.1	2.36	4	
184	1994-01-28	13 12	735-18	3.9	0.0	2.0	0.98	1.9	1.31				95		125	498	0.85	1.6	23.9	2.35	0 none	0.0	0.0	-4.4	172.1	143.6	135	2	41.9	213	23.43	27.2	2.51	3	
185	1994-01-28	13 25	735-18	4.0	0.0	2.0	1.48	2.2	1.31				96		114	498	0.85	1.0	23.5	2.28	0 none	0.0	0.0	-4.2	173.1	144.2	135	2	48.4	247	23.43	27.2	2.1	5	
186	1994-01-28	13 42	735-18	5.0	0.0	3.2	0.58	1.6	1.32	289	24.3	2.32	96		190	498	0.95	0.8	23.9	2.35	0 none	0.0	0.0	-4.7	205.0	148.5	135	2	36.2	188	22.22	28.6	2.11	4	
187	1994-01-28	13 59	735-18	5.0	0.0	3.0	0.98	2.1	1.33				96		185	498	1.03	1.2	23.8	2.28	0 none	0.0	0.0	-4.6	213.1	149.8	135	2	44.4	225	23.83	28.3	2.05	3	
188	1994-01-28	14 11	735-18	5.1	0.0	3.0	1.50	2.2	1.25				96		172	498	1.05	1.2	24.3	2.35	0 none	0.0	0.0	-4.1	207.5	149.6	135	2	52.9	263	25.38	27.8	2.5	5	
189	1994-01-28	14 27	735-18	5.1	0.0	3.1	0.98	2.1	1.29	273	23.5	2.11	96		135	498	1.01	1.2	23.9	2.38	0 none	0.0	0.0	-3.9	309.3	137.0	139	2	45.1	241	17.64	36.2	2.26	3	
190	1994-01-28	14 42	735-18	5.0	0.0	3.2	0.98	2.1	1.32				98		171	498	0.97	1.4	23.9	2.28	0 none	0.0	0.0	-4.1	142.5	147.7	138	2	45.4	232	21.43	33.7	2.13	3	
191	1994-01-31	18 50	735-5	5.0	0.0	2.7	0.59	1.4	1.51	493	43.6	3.55	97		138	295	0.86	2.6	43.4	3.10	0 none	0.0	0.0	-4.8	116.9	140.9	139	1	27.8	271	24.61	52.9	3.10	6	
192	1994-01-31	19 01	735-5	4.9	0.0	2.1	0.98	1.6	1.54				98		111	263	0.85	3.2	42.5	3.44	0 none	0.0	0.0	-5.0	113.5	143.2	138	1	33.2	326	24.43	53.7	3.34	4	
193	1994-01-31	19 12	735-5	4.8	0.0	2.1	1.52	2.0	1.45	420	38.3	2.81	99		214	382	1.09	3.2	50.2	3.87	0 none	0.0	0.0	-5.2	120.7	138.7	138	1	37	366	23.96	54.7	3.26	3	
194	1994-01-31	19 21	735-5	4.9	0.0	2.1	1.98	2.2	1.45				94		221	399	1.05	3.0	40.0	2.97	0 none	0.0	0.0	-4.9	114.2	137.0	138	1	37.5	368	24.71	50.1	3.42	2	
195	1994-01-31	19 35	735-5	4.9	0.0	2.5	1.49	1.9	1.50				94		222	367	0.94	2.8	41.3	2.89	0 none	0.0	0.0	-5.3	7.5	134.3	138	1	33.7	330	24.91	62.7	3.66	3	
196	1994-01-31	19 46	735-5	4.9	0.0	2.0	1.50	1.9	1.49	426	38.3	2.87	96		239	345	0.97	3.0	42.5	2.84	0 none	0.0	0.0	-5.0	68.3	137.0	137	1	33	328	24.33	46.2	3.66	3	
197	1994-01-31	19 58	735-5	4.9	0.0	1.6	1.49	1.9	1.45	484	41.9	2.89	94		173	353	1.11	3.4	44.6	3.00	0 none	0.0	0.0	-5.0	186.0	144.4	137	1	36.2	362	23.84	55.0	3.56	3	



# Datasheet of HBF-Trailertests

Projectnr.: 88-24110'0

Code: REDMUD-V

Customer: INTERALUMINA Pto. Ordaz/Venezuela

Material: Redmud

Cakeforming angle: 165°

Andritz-Personal: H.Riemer/W. Wiesenhoffer

Filtercloth: ZBF-08-1050-SK27

Interalumina-Personal: P.Murgia/M.Noriega

Filterarea: 2,0 m<sup>2</sup>

A.Guillermo/C.Rubio/A.Parraga

Y.Mareno/J.L.Lares

Test	Datum	Test	Feed	Vessel	Press	Press	Filter	Feed	Feed	Feed	Feed	Feed	Feed	Feed	Airflow	Airflow	Filtrate	Filtrate	Filtrate	Filtrate	Filtrate	Filtrate	Wash	Poly	Poly	Poly	D-press	Steam	Steam	Disch	in.	discr.	Tonnage	residue	Time	Temp	Time	mass	dry	Wet	Total	Flow
-	-	-	time	tank	press	CFL	CDL	speed	flow	density	conc	Na2O	FMC	temp	Compr.	Filtste	flow	conc	Na2O	FMC	Poly	Type	Temp	usage	Steam	flow	temp	time	of	mass	kg	kg/mm <sup>2</sup>	%	kg	kg	kg	kg					
-	-	-	MMT/ton	mm/mm	number	Bar	Bar	Bar	U/min	m <sup>3</sup> /h	t/m <sup>3</sup>	g/l	g/l	°C	Nm <sup>3</sup> /h	Nm <sup>3</sup> /h	m <sup>3</sup> /h	g/l	g/l	vh	°C	min	mbar	kg/h	°C	sec	Cycles	kg	kg/mm <sup>2</sup>	%	kg	kg	kg	kg								
<b>Filtercloth ZBF 08-1050-SK27</b>																																										
198	1994-02-02	19.31	735-18	5.0	0.0	0.0	0.52	1.3	1.46	536	23.7	2.02	102	104	136	0.75	5.2	21.0	2.42	387	H2O	80.0	0.9	0.0	0.0	34.4	142	1	32.7	303	26.87	25.2	0.00	7.1								
199	1994-02-02	19.50	735-18	5.0	0.0	0.0	0.98	1.6	1.38				102	478	498	1.29	4.2	21.5	2.68	417	H2O	85.0	1.0	0.0	0.0	34.4	142	1	33.5	305	28.26	21.3	0.00	4.1								
200	1994-02-02	20.09	735-18	5.1	0.0	2.0	1.50	2.1	1.31	338	18.4	2.27	102	448	498	1.50	2.5	19.6	2.76	422	H2O	90.0	1.1	0.0	0.0	34.4	142	1	30	278	27.42	24.5	0.00	3.1								
201	1994-02-02	20.35	735-18	5.1	0.0	3.6	1.05	2.2	1.31	335	17.9	2.25	93	288	411	1.13	3.5	21.0	2.69	0	H2O	85.0	0.0	0.0	0.0	34.4	141	1	29.1	262	26.74	24.7	0.79	3.1								
202	1994-02-03	12.08	735-18	5.1	0.0	2.7	0.60	1.7	1.30	321	18.4	2.22	100	205	308	1.39	4.8	14.0	2.25	478	H2O	80.0	1.7	0.0	0.0	34.0	146	1	21.6	193	27.51	16.0	0.00	4.1								
203	1994-02-03	12.22	735-18	5.1	0.0	2.4	1.01	1.9	1.28				101	299	408	1.74	5.2	14.7	2.21	480	H2O	90.0	1.4	0.0	0.0	0.0	144	1	24.6	226	26.51	18.6	0.00	3.1								
204	1994-02-03	12.40	735-18	5.1	0.0	2.3	1.49	2.0	1.31	298	18.0	2.26	102	269	368	1.68	4.4	14.8	2.29	480	H2O	90.0	1.3	0.0	0.0	34.4	142	1	26.9	250	28.68	21.4	0.00	3.1								
205	1994-02-03	17.39	735-18	5.2	0.0	3.0	1.02	1.8	1.33	374	18.3	2.33	92	311	389	1.05	2.4	18.9	2.30	0	none	0.0	0.0	0.0	0.0	34.4	138	1	24.1	237	24.6	28.6	2.00	3.1								
206	1994-02-03	18.29	735-18	5.1	0.0	3.4	1.00	1.9	1.32	441	17.4	2.17	89	266	329	1.10	1.2	17.7	2.27	85	HX30	0.0	0.2	0.0	0.0	34.4	138	1	27	266	24.61	26.8	0.00	2.1								
207	1994-02-03	18.42	735-18	5.1	0.0	3.4	1.00	1.9	1.41				88	260	330	1.08	1.6	17.8	2.17	122	HX30	0.0	0.3	0.0	0.0	34.4	136	1	29.6	295	24.55	28.7	0.00	4.1								
208	1994-02-03	19.05	735-18	5.1	0.0	3.4	1.00	2.1	1.37	432	16.8	2.15	90	255	331	1.04	1.2	17.7	2.15	180	HX30	0.0	0.4	0.0	0.0	34.4	136	1	30.9	309	24.19	26.7	0.00	4.1								
209	1994-02-03	19.18	735-18	5.2	0.0	3.4	1.00	1.9	1.37				88	258	333	1.00	1.5	16.5	2.04	254	HX30	0.0	0.6	0.0	0.0	34.4	137	1	28.5	279	25.48	25.4	0.00	4.1								
210	1994-02-03	19.30	735-18	5.2	0.0	3.5	0.99	2.0	1.35	385	15.2	2.11	86	284	342	1.08	1.0	16.1	2.07	348	HX30	0.0	0.8	0.0	0.0	34.4	138	1	28.4	278	26.05	24.8	0.00	4.1								
211	1994-02-03	19.43	735-18	5.2	0.0	3.5	1.00	2.3	1.35				86	272	346	0.97	1.6	15.3	2.07	285	HX30	0.0	0.7	0.0	0.0	34.4	136	1	27	267	25.15	25.1	0.00	4.1								
212	1994-02-03	19.56	735-18	5.2	0.0	3.5	0.99	2.3	1.23	300	8.2	1.87	70	348	372	1.22	0.8	12.9	2.14	1282	HX30	0.0	3.7	0.0	0.0	34.4	137	1	23	226	25.19	23.3	0.00	2.1								
213	1994-02-03	20.12	735-18	5.2	0.0	3.4	0.99	2.2	1.48	473	18.0	2.08	86	291	345	0.97	0.8	14.8	2.05	0	none	0.0	0.0	0.0	0.0	34.4	135	1	36.2	376	22.11	26.4	0.00	3.1								
214	1994-02-04	10:58	735-18	5.1	0.0	0.0	0.92	1.8	1.49	517	19.4	2.07	104	207	318	0.99	2.2	15.8	1.92	422	H2O	55.0	0.7	0.0	0.0	34.4	148	1	42.5	390	24.6	23.9		5.6								
215	1994-02-04	11:08	735-18	5.1	0.0	0.0	1.52	2.0	1.5?	502	19.4	2.27	101	201	263	1.37	2.6	15.0	1.92	438	H2O	60.0	0.6	0.0	0.0	34.4	148	1	51	473	23.7	26.7		4.1								
216	1994-02-04	11:19	735-19	5.1	0.0	0.0	2.02	2.1	1.50	517	18.2	2.11	97	183	233	1.54	3.2	16.5	2.08	455	H2O	85.0	0.6	0.0	0.0	34.4	145	1	60	542	27.19	21.6		2.6								
217	1994-02-04	11:36	735-19	5.1	0.0	0.0	2.49	2.4	1.56	528	19.8	2.19	96	141	229	1.84	3.4	16.1	2.21	472	H2O	70.0	0.5	0.0	0.0	34.4	146	1	60.8	593	21.08	21.7		2.1								
218	1994-02-04	11:45	735-18	5.1	0.0	0.0	2.98	2.6	1.53	533	19.3	2.19	94	163	215	1.68	2.2	16.4	2.20	467	H2O	75.0	0.5	0.0	0.0	34.4	143	1	64	594	26.35	24.1		2.1								
219	1994-02-04	12:30	735-18	5.0	0.0	0.0	1.52	1.9	1.51	527	19.6	2.33	94	218	228	1.33	1.4	15.7	2.14	474	H2O	70.0	0.7	0.0	0.0	34.4	141	1	43.5	419	24.42	24.7		4.1								
220	1994-02-04	12:45	735-18	5.0	0.0	0.0	1.51	2.0	1.54	533	19.3	2.20	94	214	240	1.17	1.8	15.6	2.16	477	H2O	80.0	0.7	0.0	0.0	34.4	141	1	42.1	421	24.03	21.9		4.1								
221	1994-02-04	13:00	735-18	5.0	0.0	0.0	1.51	1.8	1.58	549	19.4	2.14	94	194	249	1.22	2.0	15.8	2.18	418	H2O	90.0	0.7	0.0	0.0	34.4	140	1	43.4	421	24.57	26.8		2.1								
222	1994-02-04	14:33	735-18	5.0	0.0	0.0	1.52	1.9	1.56	552	19.0	2.12	86	206	256	1.04	2.6	15.6	2.39	420	H2O	90.0	0.7	0.0	0.0	34.4	138	1	39.8	389	25	23.4		2.1								
223	1994-02-04	16:06	735-18	5.0	0.0	0.0	1.52	1.8	1.54	547	19.2	2.27	80	292	246	1.21	4.3	15.1	2.47	477	H2O	90.0	0.9	0.0	0.0	34.4	137	1	35.6	350	25.11	22.0		2.1								
224	1994-02-04	18:03	735-18	5.1	0.0	0.0	1.52	1.5	1.52	550	18.8	2.30	74	219	261	1.10	4.6	15.2	2.53	441	H2O	70.0	0.9	0.0	0.0	34.4	137	1	32.3	318	25.14	21.3		2.1								



# Datasheet of HBF-Trailertests

Projectnr.: 88-241102/0

Code: REDMUD-V

Customer: INTERALUMINA Pto. Ordaz/Venezuela

Material: Redmud

Filtercloth: ZBF-06-1050-SK27

Filterarea: 2,0 m<sup>2</sup>

Cakeforming angle: 165°

Andritz-Personal: H.Riemer /W. Wiesenhofe

Interalumina-Personal: P.Murgia/M.Noriega

A.Guillermo/C.Rubio/A.Parra

Y.Mareno/J.L.Lares

Test	Datum	Test	Feed	Vessel	Press	Press	Filter	Feed	Feed	Feed	Feed	Feed	Feed	Feed	Airflow	Airflow	Filtrate	Filtrate	Filtrate	Filtrate	Filtrate	Filtrate	Wash	Poly	Poly	Poly	Di-press	Steam	Steam	Disc	No	discr	Torrage	res.zwa	Care	Time	etc.
#		time	tank	press	CFL	CDL	speed	flow	density	conc	Na2O	FMC	temp	Compr	Filtrate	flow	conc	Na2O	FMC	Poly	Type	Temp	usage	Steam	flow	temp	time	disc	mass	dry	Wastefill	Total	Waste	Time			
		hh:mm	number	Bar	Bar	Bar	U/min	m³/h	g/l	g/l			°C	Nm³/h	Nm³/h	m³/h	g/l	g/l					°C	m³/t	mbar	kg/h	°C	sec	Cycles	%	kg/m³	%	kg	kg	kg		
225	1994-02-06	12:08	T35-18	5.0	0.0	0.0	1.45	0.7	1.45	484	20,6	2,37	55	332	259	0.81	1.8	17,7	2,67	462	H2O	65,0	2,0	0,0	0,0	34,4	137	1	15,3	153	23,69	16	1,6				
226	1994-02-06	12:30	T35-18	5.0	0.0	0.0	1.45	1,1	1.43	478	20,6	2,57	63	314	253	0.85	2,0	13,6	2,46	432	H2O	70,0	1,7	0,0	0,0	34,4	136	1	16,6	168	23,33	8,3	1,5				
227	1994-02-06	12:43	T35-18	5.0	0.0	0.0	1.45	1,2	1.46	474	21,8	2,51	72	322	283	0.93	1,0	14,4	2,75	437	H2O	70,0	1,5	0,0	0,0	34,4	136	1	18,2	186	22,96	11,6	2,1				
228	1994-02-06	13:26	T35-18	4.9	0.0	0.0	1.46	1,9	1.46	474	22,2	2,33	82	336	279	1,01	2,0	16,1	2,84	433	H2O	65,0	1,2	0,0	0,0	34,4	137	1	22,5	226	22,55	8,8	2,6				
229	1994-02-06	14:03	T35-18	5.0	0.0	0.0	1.46	1,6	1.45	480	21,4	2,35	88	344	320	1,04	1,2	16,9	2,50	428	H2O	70,0	1,1	0,0	0,0	34,4	137	1	26,2	265	23,3	5,5	2,8				
230	1994-02-06	14:30	T35-18	5.0	0.0	0.0	1.45	1,6	1.43	461	21,0	2,20	92	368	336	1,16	1,4	16,1	2,19	433	H2O	66,0	0,9	0,0	0,0	34,4	137	1	28,6	294	22,1	8,6	3,2				
231	1994-02-06	14:58	T35-18	5.0	0.0	0.0	1.46	1,9	1.47	480	22,2	2,40	92	358	332	1,09	1,6	16,1	2,28	430	H2O	65,0	0,8	0,0	0,0	34,4	137	1	32,2	331	21,88	5,6	3,2				
232	1994-02-06	16:14	T35-18	5.0	0.0	0.0	1.43	1,5	1.49	504	21,0	2,34	92	372	330	1,12	1,2	17,7	2,33	447	H2O	68,0	0,9	0,0	0,0	34,4	137	1	31,9	324	22,84	14,1	3,5				
233	1994-02-06	16:51	T35-18	5.0	0.0	0.0	1.42	1,9	1.52	490	22,2	2,33	92	360	322	1,18	2,0	18,1	2,52	450	H2O	68,0	1,0	0,0	0,0	34,4	136	1	28,5	289	23,43	20,0	3,1				
234	1994-02-06	17:22	T35-18	5.0	0.0	0.0	1.41	1,8	1.50	499	21,8	2,11	90	359	317	1,05	1,0	18,1	2,68	444	H2O	70,0	1,0	0,0	0,0	34,4	136	1	27,5	278	23,25	21,3	3,2				
235	1994-02-06	17:52	T35-18	5.0	0.0	0.0	1.43	2,1	1.54	532	20,2	2,18	87	396	418	1,17	2,1	15,6	2,36	437	H2O	70,0	1,0	0,0	0,0	34,4	135	1	28	288	22,87	20,0	3,2				
236	1994-02-07	11:07	T35-18	5.1	0.0	0.0	1.47	1,7	1.57	608	21,8		86	163	149	1,40	3,0	20,2		428	H2O	56,0	0,6	0,0	0,0	34,4	138	1	46	455	24,2		4,2				
237	1994-02-07	12:05	T35-18	5.0	0.0	0.0	1.47	2,0	1.59	584	21,4	2,50	90	180	143	1,43	2,4	17,3	3,13	442	H2O	65,0	0,6	0,0	0,0	34,4	138	1	48,5	480	24,3	23,2	4,5				
238	1994-02-07	13:28	T35-18	5.0	0.0	0.0	1.46	1,8	1.57	582	21,4	2,50	88	205	139	1,18	2,2	17,7		467	H2O	65,0	0,6	0,0	0,0	34,4	138	1	47	472	23	14,7	4,5				
239	1994-02-07	15:24	T35-18	5.0	0.0	0.0	1.46	1,6	1.59	591	20,6	2,49	84	198	150	1,11	2,3	18,1		461	H2O	70,0	0,7	0,0	0,0	34,4	135	1	40,4	412	23,6	22,7	4,0				
240	1994-02-07	15:52	T35-18	5.1	0.0	0.0	1.47	1,9	1.57	591	20,6	2,62	80	188	155	1,05	2,9	16,9		455	H2O	65,0	0,8	0,0	0,0	34,4	134	1	38,5	392	24,25	21,6	4,0				
241	1994-02-07	17:38	T35-18	5.0	0.0	2,1	1.48	1,8	1.58	587	20,2		82	357	343	0,79	1,6	21,0	2,62	O:none		0,0	0,0	0,0	34,4	134	1	44	451	23,7	25,4	4,4					
242	1994-02-07	17:55	T35-18	5.0	0.0	2,0	1.45	2,1	1.59	574	21,4	3,10	80	330	340	0,90	1,4	20,2	3,04	171	Lime	0,0	0,2	0,0	0,0	34,4	133	1	52	536	23,6	29,2	5,1				
243	1994-02-07	18:07	T35-18	5.0	0.0	2,4	1.48	2,4	1,57	597	21,0		80	377	369	1,08	1,0	20,6	4,14	292	Lime	0,0	0,4	0,0	0,0	34,4	134	1	53	530	24,1		5,0				
244	1994-02-07	18:23	T35-18	5.0	0.0	2,6	1.47	2,4	1,52	595	20,6		78	370	393	1,14	1,2	20,6	3,88	323	Lime	0,0	0,4	0,0	0,0	34,4	133	1	53,5	520	26,8	26,6	5,0				
245	1994-02-07	18:37	T35-18	5.0	0.0	2,4	1.47	2,6	1,45	548	20,2		78	406	416	1,05	1,0	19,3		483	Lime	0,0	0,6	0,0	0,0	34,4	134	1	53,7	524	27,6	21,9	5,3				
246	1994-02-07	18:51	T35-18	5.0	0.0	2,2	1.47	2,2	1,52	557	21,0	3,24	78	395	400	0,56	1,2	20,0	3,82	228	Lime	0,0	0,3	0,0	0,0	34,4	134	1	50	495	26,6	25,5	5,0				
247	1994-02-07	19:03	T35-18	5.0	0.0	2,2	1.47	2,2	1,57	543	22,0	3,16	80	364	374	0,93	1,4	21,0	3,69	120	Lime	0,0	0,2	0,0	0,0	34,4	133	1	51	511	25,9	26,1	3,65				
248	1994-02-07	19:19	T35-18	5.0	0.0	2,3	1,94	2,3	1,51	512	22,0	3,23	78	378	385	1,09	1,7	20,0	3,24	197	Lime	0,0	0,2	0,0	0,0	34,4	133	1	56	585	26,1	27,4	4,2				
249	1994-02-07	19:30	T35-18	5.0	0.0	2,2	2,43	2,8	1,51	554	20,0	3,33	78	352	377	1,22	1,6	17,7		250	Lime	0,0	0,3	0,0	0,0	34,4	133	1	62,6	620	27,1	24,9	4,0				
250	1994-02-07	19:42	T35-18	5.0	0.0	2,2	2,97	2,9	1,54	538	21,0	2,87	76	351	360	1,31	1,7	21,0	4,08	261	Lime	0,0	0,3	0,0	0,0	34,4	132	1	63,8	634	27,2	28,2	3,39				



# Datasheet of HBF-Trailer tests

Projectnr.: 88-24110/0

Code: REDMUD-V

Customer: INTERALUMINA Pto. Ordaz/Venezuela

Material: Redmud

Cakeforming angle: 165°

Andritz-Personal: H.Riemer/W. Wiesenthaler

Filtercloth: ZBF-06-1050-SK27

Interalumina-Personal: P.Murgia/M.Nonega

Filterarea: 2,0 m<sup>2</sup>

A.Guillermo/C.Rubio/A.Parra

Y.Marcos/J.L.Lares

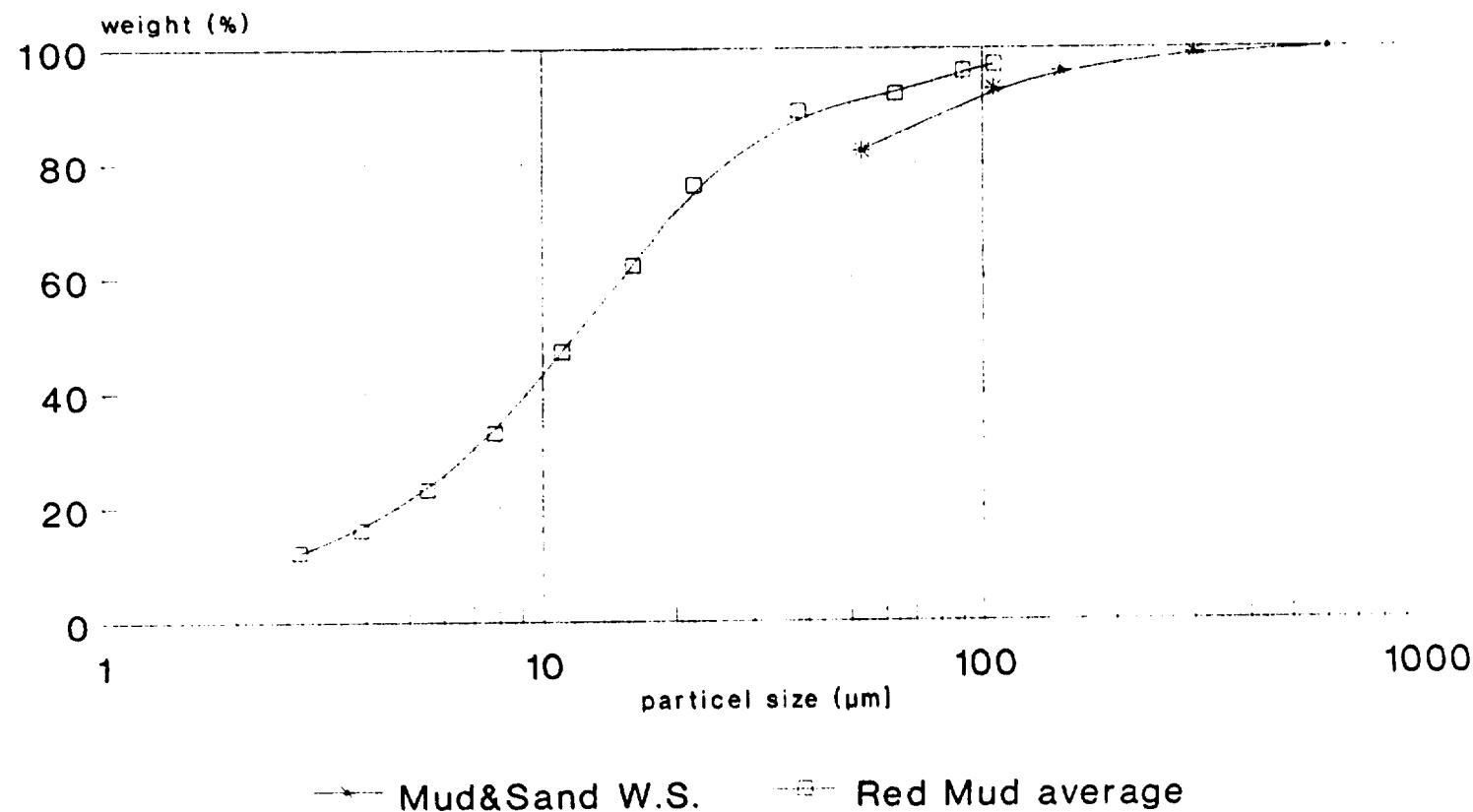


Test- nr.	Datum	Test- time hh:mm	Feed- tank number	Vessel Press Bar	Press CFL	Press CDL	Feed- speed U/min	Feed- flow m <sup>3</sup> /h	Feed- density g/l	Feed- conc Na2O FMC	Feed- temp °C	Airflow Nm <sup>3</sup> /h	Airflow Nm <sup>3</sup> /h	Filtrate- flow m <sup>3</sup> /h	Filtrate- conc Na2O FMC	Filtre- conc g/l	Wash Vh	Poly Poly Temp °C	Poly usage Steam m <sup>3</sup> /h	Poly Temp mbar	D-press kg/h	Steam flow kg/h	Steam temp °C	Disch time sec	Disch of mass	Tonnage kg	residual dry kg/m <sup>3</sup>	Cake Moisture %	Cake Soda %	Cake FMC %		
<b>tests with filteraid Ca2Al3</b>																																
251	1994-02-09	11:28	T35-18	5.0	0.0	2.2	1.47	1.9	1.51	532	21.4	2.71	78	341	336	0.90	1.2	20.6	2.72	0 none	0.0	0.0	0.0	34.4	138	1	35.2	346	24.5	28.2	3.5	
252	1994-02-09	11:42	T35-18	5.0	0.0	2.4	1.47	1.6	1.47	503	22.2	2.88	76	361	359	0.89	1.6	20.1	2.88	81 Ca2Al	40.0	0.1	0.0	34.4	137	1	35.7	351	25.2	23.9	3.6	
253	1994-02-09	11:53	T35-18	5.0	0.0	2.4	1.47	1.6	1.41	444	18.9	3.35	73	375	378	0.87	1.4	21.0	2.82	140 Ca2Al	40.0	0.3	0.0	34.4	138	1	30.2	294	25.5	25.9	3.2	
254	1994-02-09	12:04	T35-18	5.0	0.0	2.8	1.47	1.7	1.43	468	18.9	2.69	70	403	404	0.87	1.8	19.8	2.88	317 Ca2Al	30.0	0.7	0.0	34.4	138	1	29.5	286	25.9	25.5	3.0	
255	1994-02-09	15:04	T35-18	5.1	0.0	0.0	1.46	1.2	1.42	494	21.0	2.72	68	319	294	0.65	2.0		422 H2O	59.0	1.2	0.0	0.0	34.4	143	1	24.8	230	26.1	23.4	2.7	
256	1994-02-09	15:34	T35-18	5.0	0.0	0.0	1.45	1.2	1.40	481	22.2		70	338	360	0.90	2.2	17.6	2.88	478 H2O	70.0	1.5	0.0	0.0	34.4	140	1	22	211	25.5	18.7	2.5
257	1994-02-09	19:55	T35-18	5.1	0.0	0.0	1.46	1.7	1.36	438	22.6	2.13	83	390	404	1.17	1.8	17.7	2.42	479 H2O	75.0	1.5	0.0	0.0	34.4	135	1	21.4	212	25.9	26.3	3.3
258	1994-02-09	20:10	T35-18	5.1	0.0	0.0	1.46	1.7	1.43	528	22.2	2.24	92	359	387	1.18	1.8	18.1	2.52	480 H2O	85.0	1.4	0.0	0.0	34.4	133	1	23.5	236	25.9	7.7	3.1
259	1994-02-09	20:26	T35-18	5.1	0.0	0.0	1.46	1.8	1.22	228	21.8	2.51	92	419	475	1.26	1.8	17.3	2.41	480 H2O	90.0	1.5	0.0	0.0	34.4	131	1	20.5	209	25.7	19.0	2.6
260	1994-02-09	21:36	T35-18	5.1	0.0	3.0	1.48	2.3	1.18	155	20.6	2.53	93	489	498	1.89	1.4	16.5	3.14	480 H2O	90.0	4.5	0.0	0.0	34.4	131	2	16	76	30.7	17.1	2.5
261	1994-02-09	21:58	T35-18	5.1	0.0	3.0	0.62	1.2	1.18	147	20.7	2.61	88	339	328	1.22	1.8	18.1		480 H2O	90.0	5.5	0.0	0.0	34.4	135	2	13.3	62	29.7	13.9	2.4
<b>tests with 20% sand in the feedtank</b>																																
262	1994-02-10	00:18	T35-18	5.0	0.0	3.2	1.50	1.4	1.24	309	21.0	2.45	84	370	400	1.47	1.4	21.4	2.46	0 none	0.0	0.0	0.0	34.4	141	1	23	209	28.7	23.6	3.12	
263	1994-02-10	00:33	T35-18	5.0	0.0	3.2	1.50	1.5	1.28	339	20.6	2.44	88	351	395	1.52	2.0	20.8	2.80	0 none	0.0	0.0	0.0	34.4	140	1	24	223	27.6	23.1	3.2	
264	1994-02-10	00:44	T35-18	5.0	0.0	1.6	1.50	1.4	1.26	340	21.0	2.34	88	302	330	1.90	2.2	18.9	2.54	360 H2O	35.0	1.2	0.0	0.0	34.4	139	1	23.5	218	28.4	23.3	2.7
265	1994-02-10	00:56	T35-18	5.0	0.0	0.8	1.50	1.4	1.26	318	21.4	2.50	88	490	480	2.20	2.0	18.1	2.73	360 H2O	35.0	1.2	0.0	0.0	34.4	139	1	21.5	203	27	22.2	2.5

## **6. Graphs:**

- Graph 1: screen analysis
- Graph 2: effects of variing feed concentrations and vessel pressure
- Graph 3: dosage of lime to the red mud
- Graph 4: comparison between RM/RM+lime/RM+sand
- Graph 5: blinding from the filter bag over filtration time
- Graph 6: polymere usage
- Graph 7: comparison between RM/RM+polymer/RM+wash water
- Graph8: change of throughput over soda content in the feed
- Graph 9: effect of feed temperature over the throughput
- Graph 10: efffect of throughput over the filtration pressure
- Graph 11: comparison over long time test between moisture/throughput/ air consumption and feed solid

CVG-Interalumina/Venezuela  
screenanalysis from dif.RED MUD samples

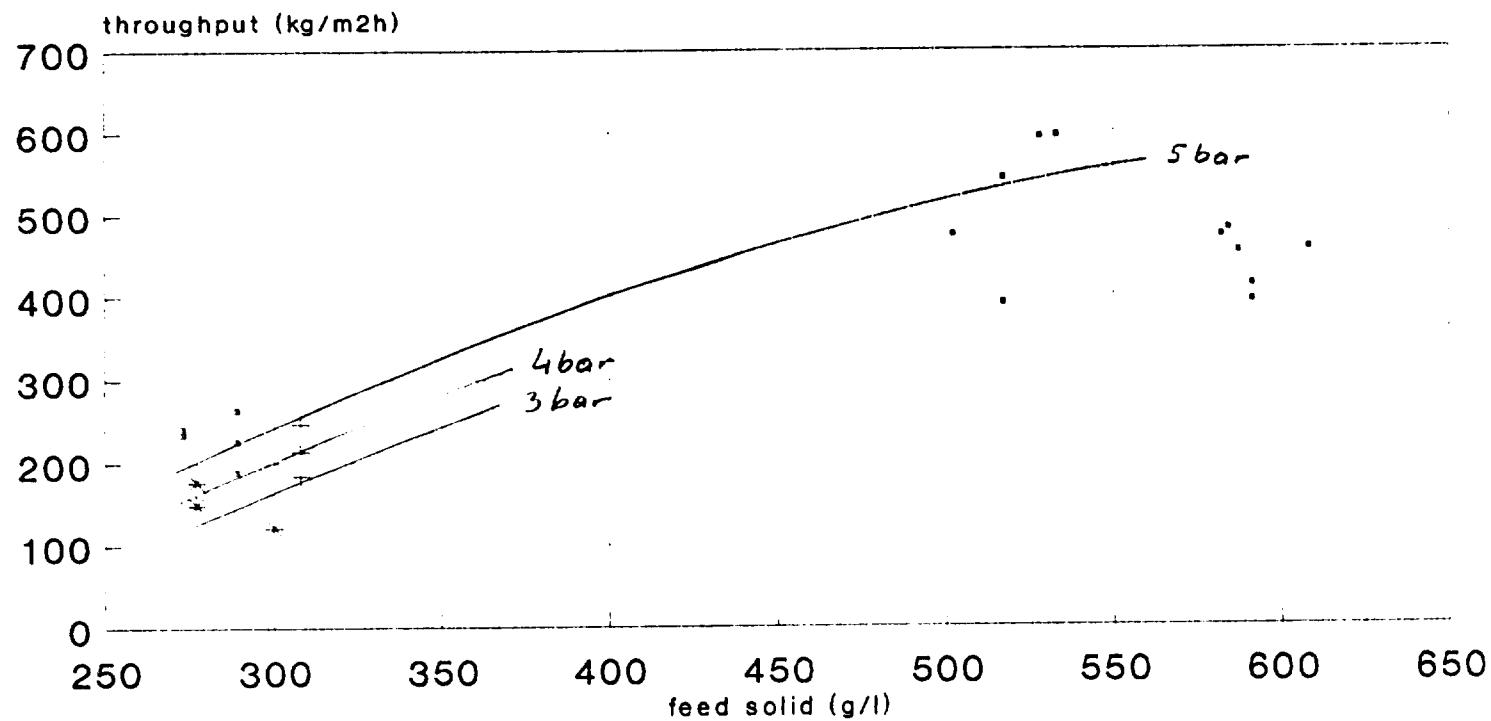


Graph 1

# CVG-INTERALUMINA/Venezuela

Throughput as function of feed solid

Filterspeed 0,5 to 3 RPM, sample Red Mud



· pressure 5 bar

+ pressure 4 bar

\* pressure 3 bar

Na<sub>2</sub>Oc 20-21 g/l in the feed

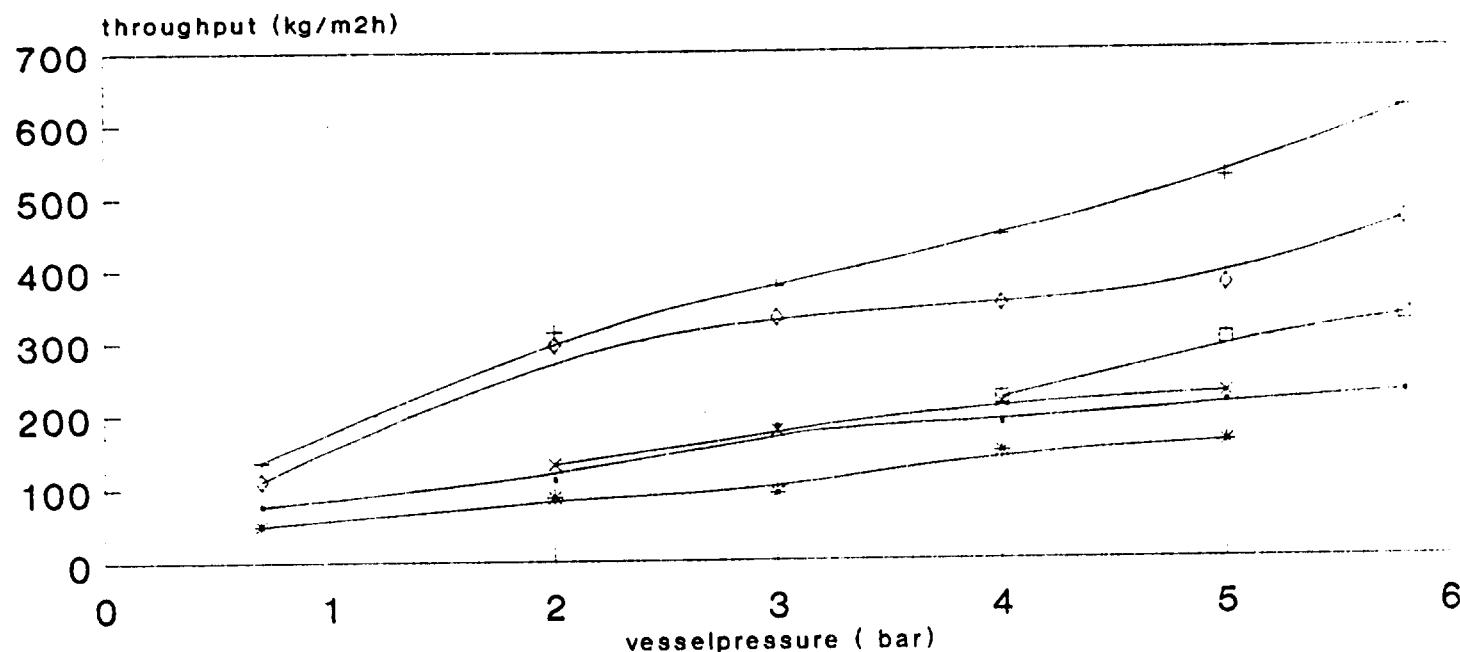
feed temp.=80-104 °C

Graph 2

# CVG-INTERALUMINA/Venezuela

## RED MUD

Throughput as function of pressure



--- 1.feed Na<sub>2</sub>O=40 g/l    --- 2.feed Na<sub>2</sub>O=13-18g/l    --- 3.feed Na<sub>2</sub>O=55 g/l

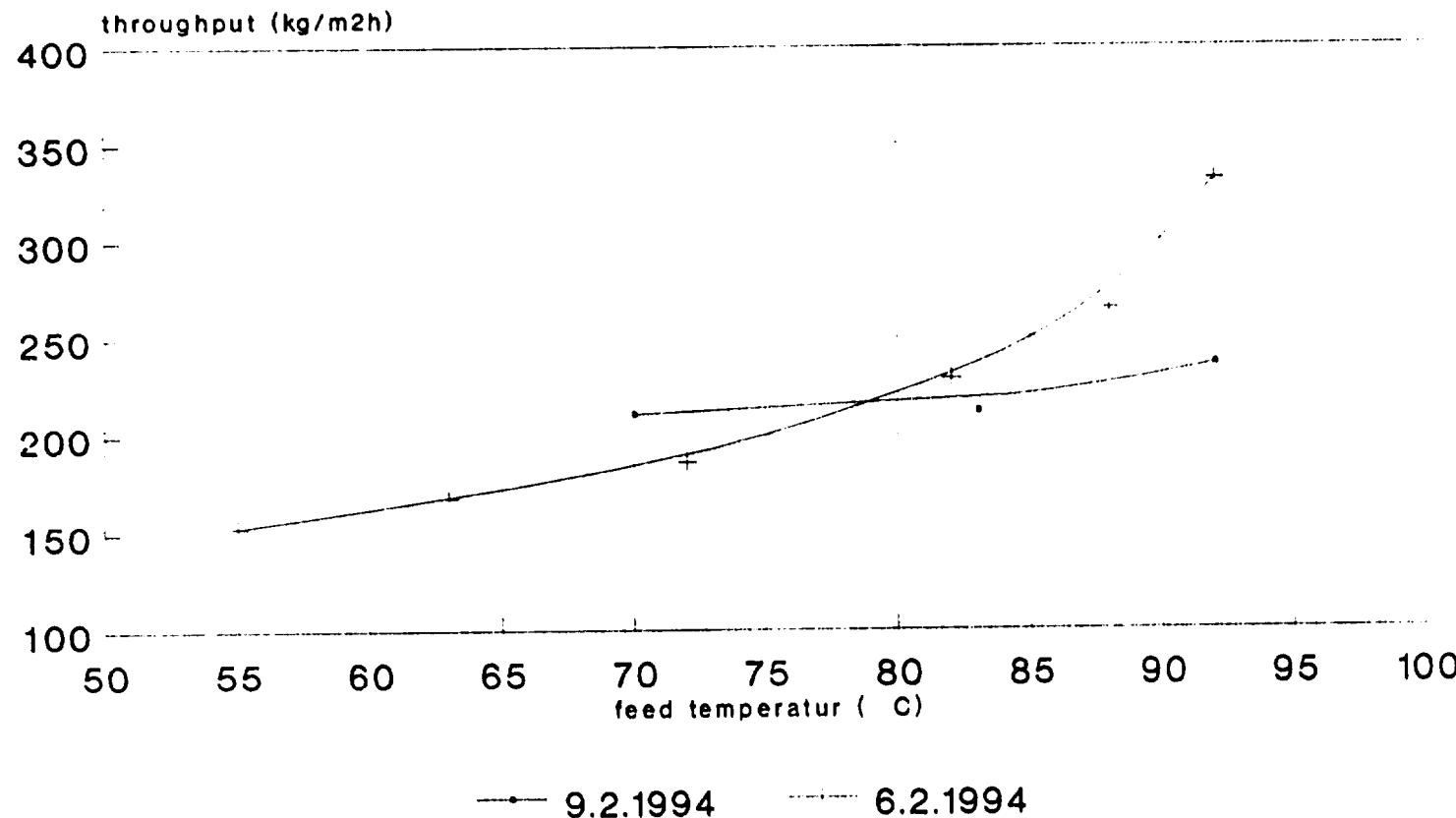
-·- 4.feed Na<sub>2</sub>O=58 g/l    -·- 5.feed Na<sub>2</sub>O=23 g/l    -·- 6.Feed Na<sub>2</sub>O=17 g/l

1.FS=340 g/l, 2.FS=500 g/l, 3.FS=300 g/l  
4.FS=400 g/l, 5.FS=300 g/l, 6.FS=400 g/l

Graph 3

# CVG-INTERALUMINA/Venezuela

throughput as func. of feed temperatur  
pres.=6 bar filterspeed = 1,5 RPM

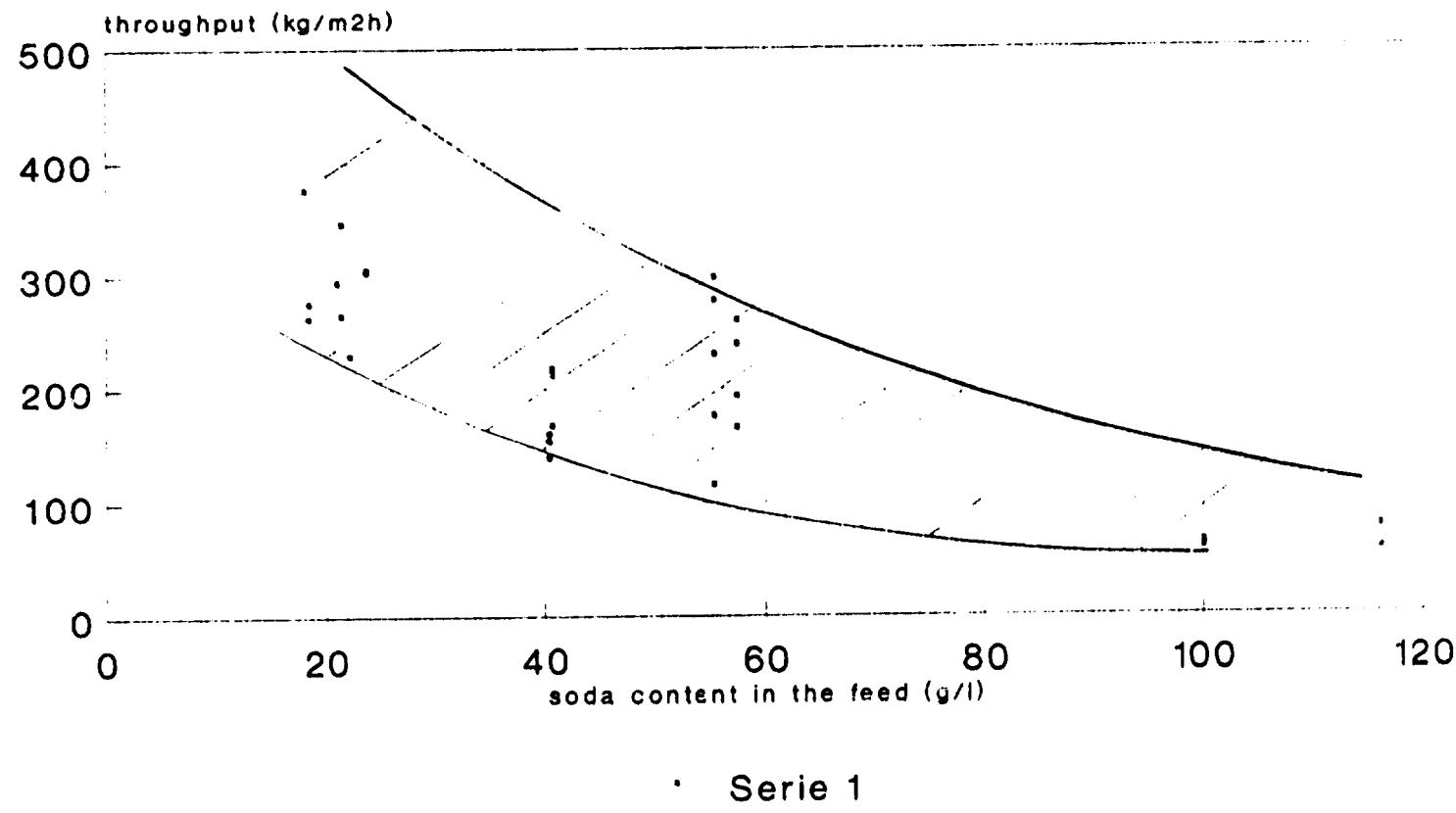


feed solid=438-528 g/l

feed Na<sub>2</sub>O=20 g/l RM not representative

Graph 4

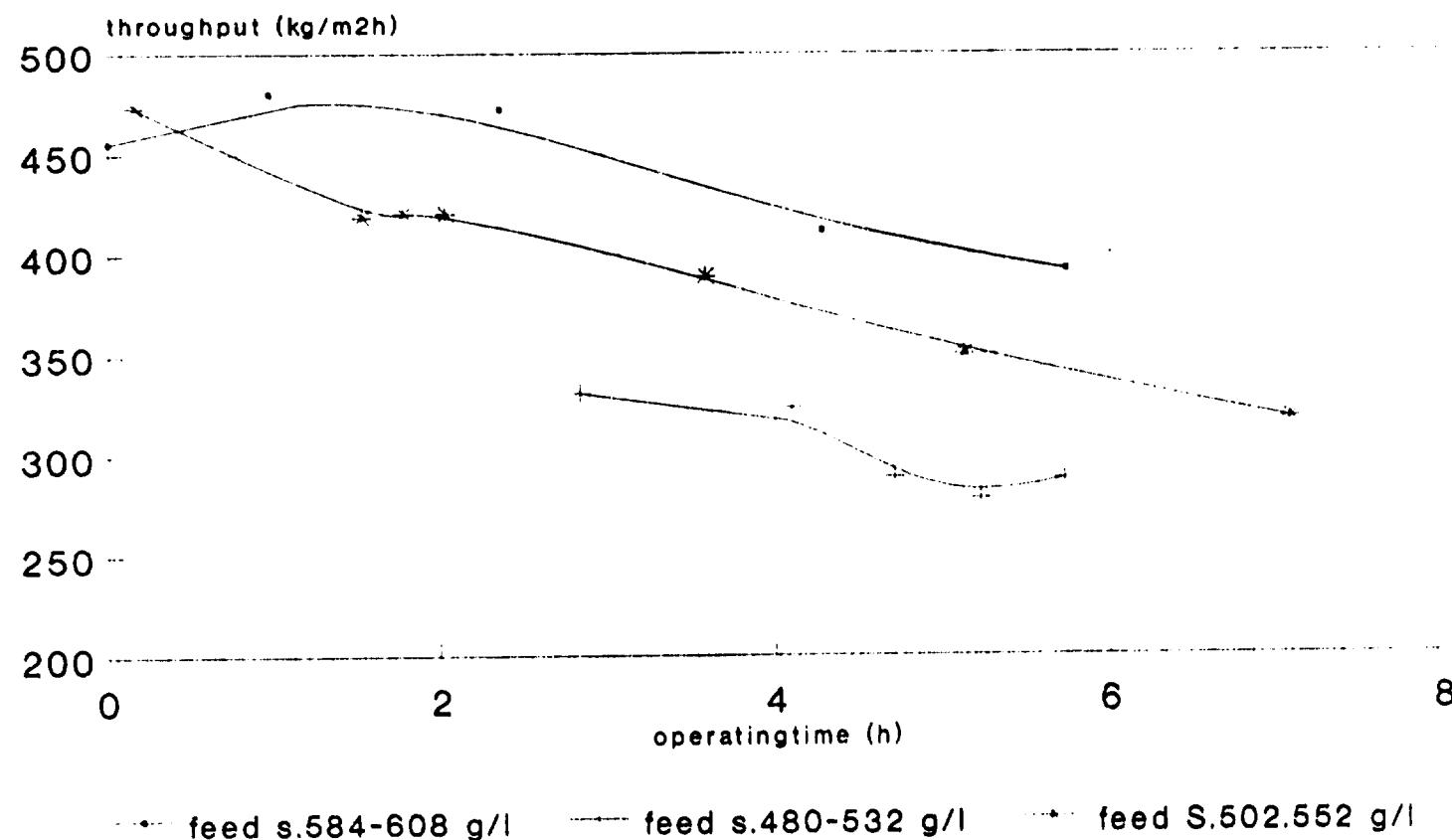
**CVG-INTERALUMINA/Venezuela**  
**RED MUD**  
throughput as function of soda content



feed solid: 400 g/l average

Graph 5

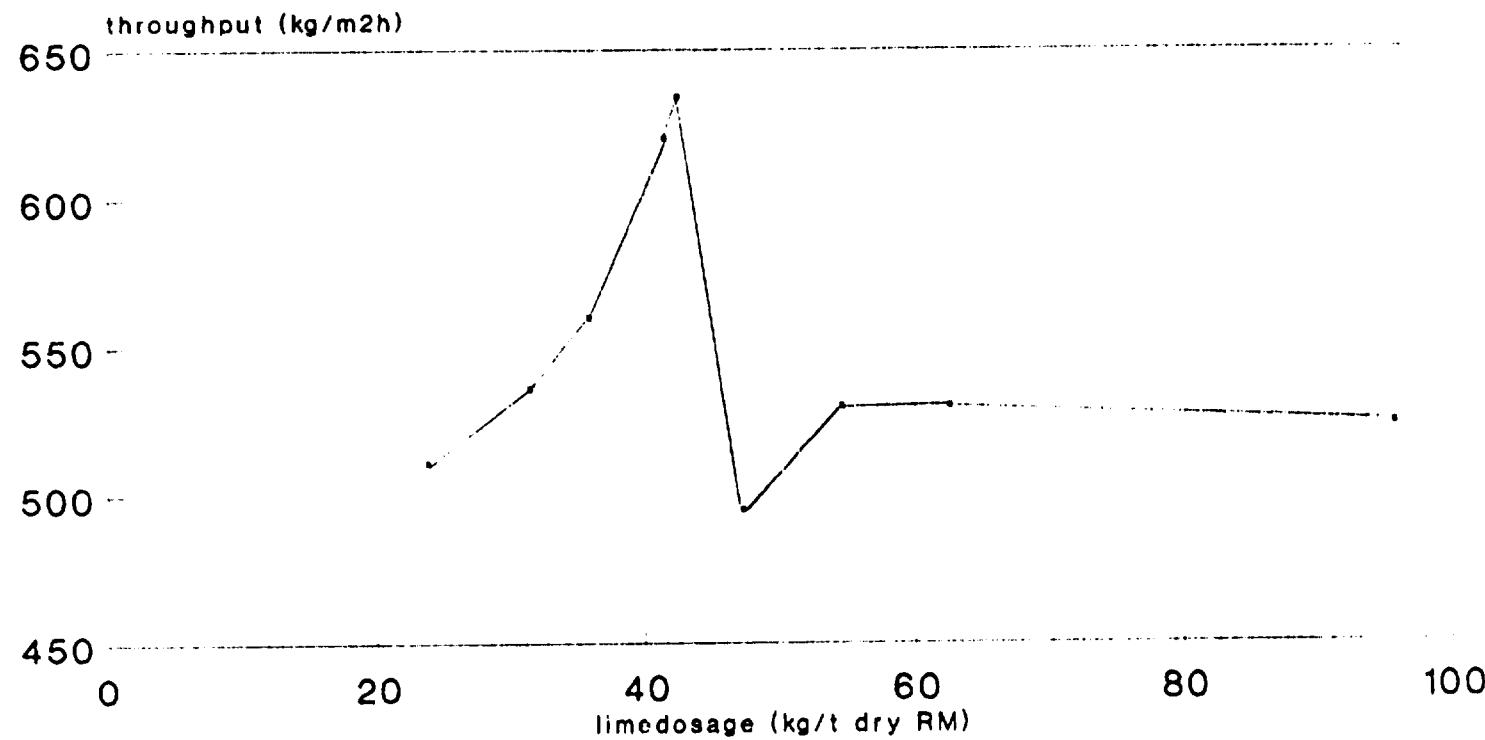
CVG-INTERALUMINA/Venezuela  
throughput as function of operating time



Red Mud feed Na<sub>2</sub>Oc=20-21 g/l  
pressure:5 bar, Disk speed 1.5 RPM

Graph 6

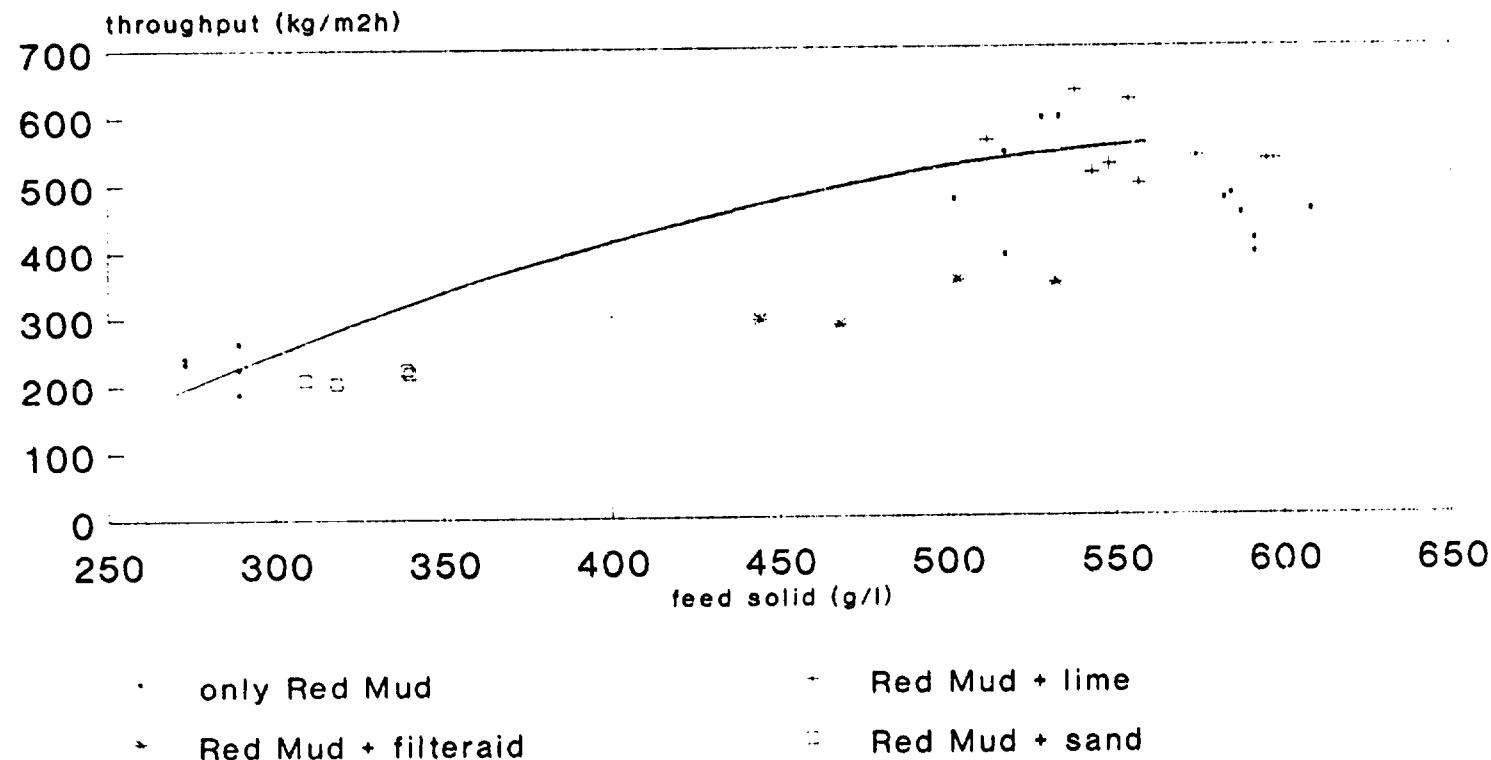
CVG-INTERALUMINA/Venezuela  
TESTS WITH LIME  
throughput as function of limedosage



feed temp. 76 to 82 C  
Na<sub>2</sub>Oc in feed 20-21 g/l

Graph 7

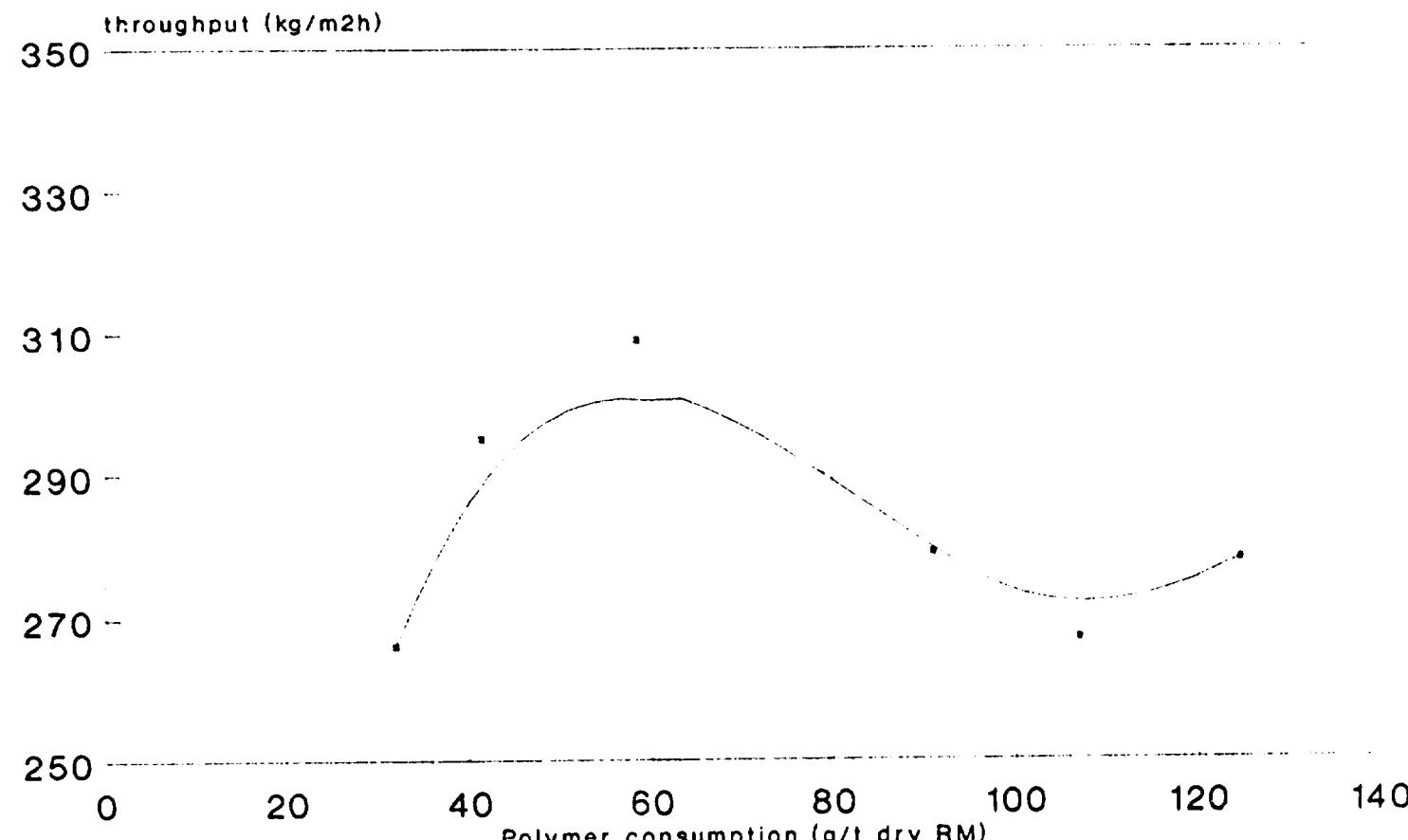
CVG-INTERALUMINA/Venezuela  
RED MUD  
comp. between RM/RM+lime/RM+sand



Na<sub>2</sub>Oc 20-21 g/l in the feed  
feed temp.=80-104 °C pres.=5 bar 1,5 RPM

Graph 8

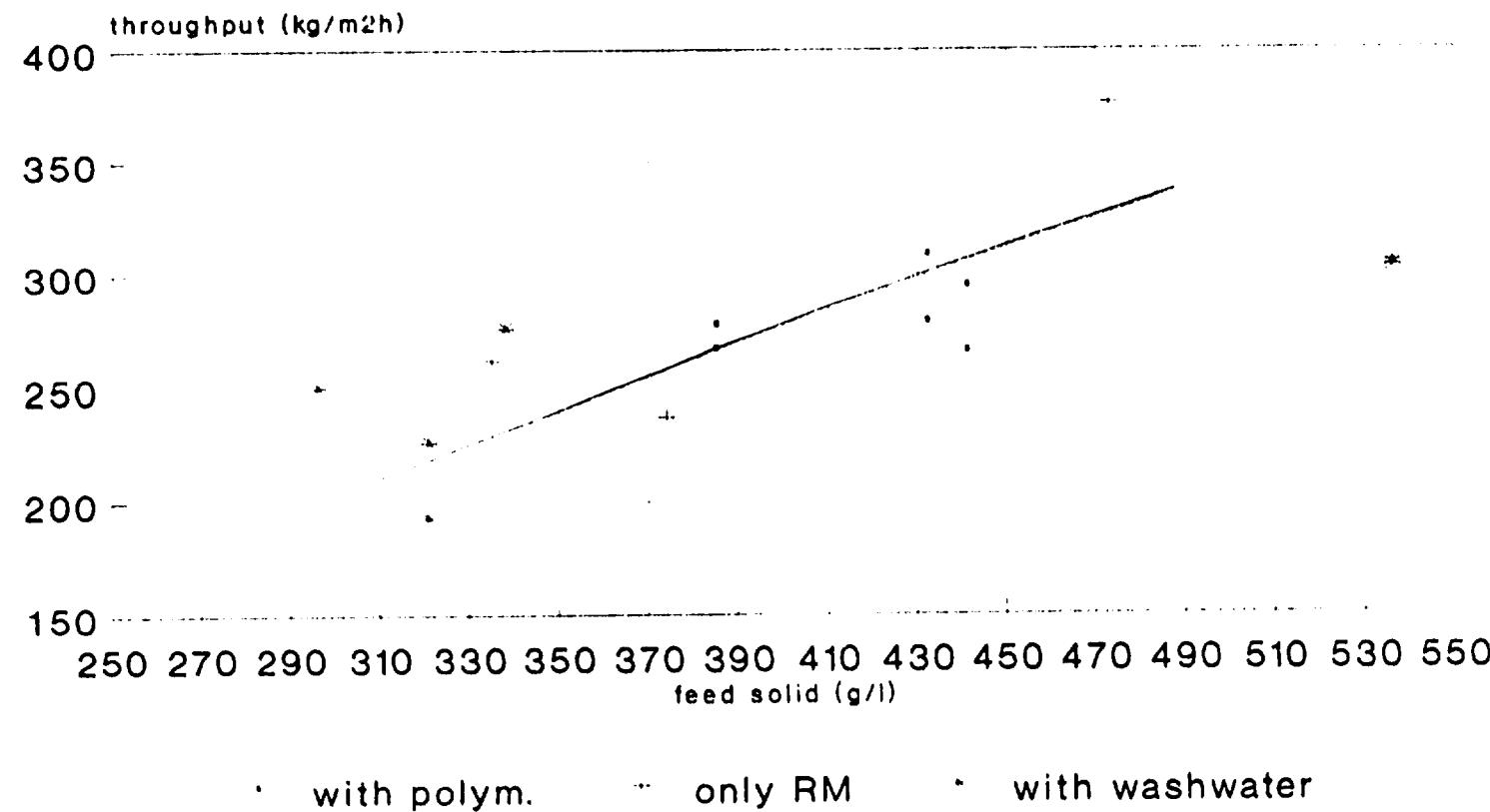
CVG-INTERALUMINA/Venezuela  
throughput as function of polym.dosage



pressure 5 bar  
feed s=300-441g/l, Na<sub>2</sub>O=15-18g/l

Graph 9

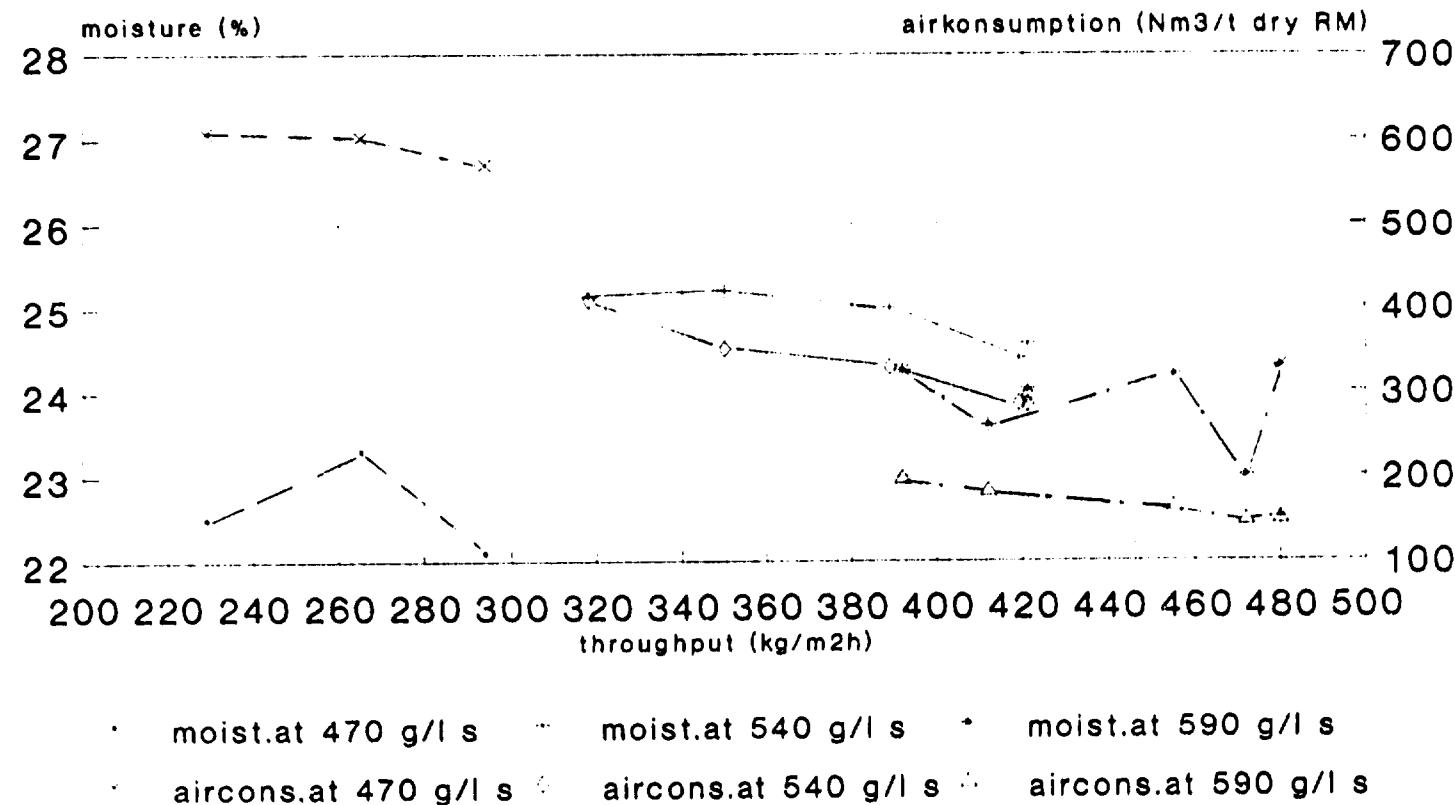
CVG-INTERALUMINA/Venezuela  
Red Mud  
comparison RM/RM+polymer/RM+washwater.



pressure 5 bar filterspeed 0,5-1,5 RPM  
Na<sub>2</sub>O=15-18g/l feed temp.:86-102 C

Graph 10

**CVG-INTERALUMINA/Venezuela**  
 throughput as function of moist./airc.  
 vesselpres.=5 bar, disksp.=1.5 RPM



feed temp.=80-100 °C

Graph 11

## 7. Recommendations:

Evaluating the findings of the entire onsite test work the following summary can be made resp. the following filtration equipment/plant can be recommended.

- As a first series of tests the standard hyperbaric filtration process was applied that means pressure filtration without cake washing, without additives and without application of steam. It was found that reasonable specific filtration rates could be obtained at 5 bar differential pressure in the cake forming zone of the filter.

Close observation of the process resulted in the conclusion that it is not required to apply the same pressure of 5 bars for obtaining a residual moisture of 25 % weight approx. A max. pressure differential of 2 bar turned out to be sufficient for cake drying. With 5 bar in the cake building zone specific capacities being 4 times higher than on vaccum filtration could be obtained (see graph 3).

Evaluating graph 8 we find that feed concentration and soda content in the feed are influencing the results remarkably. Increasing feed density and low soda content gave the best filtration rates and lowest moistures. In graph 2 e.g. we find that at a constant soda content of 20 g/l the increase of the feed solids from 300 - 500 g/l provide double the capacity.

In connection with this basic tests also the influence of the feed temperature has been checked. Graph 4 gives a summary wherein one can see that the capacity can be increased by 100 % by rising the feed temperature from 55 - 90° C. The same effect was noticed by increasing the temperature from 75 - 95° C.

Filter cloth blinding due to the extreme fineness of the red mud particles was observed during constant operation - the results of this test series are shown in graph 6. This curve shows that a decrease of capacity in the range of 30 % over an operation of 6 hrs was measured - seen from this figures a 4 hrs intervall for filter cloth cleaning must be recommended for the full size installation. Filter cloth cleaning also can be done during operation up to a certain extent without stopping the filter.

→ Influence of additives:

Various additives such as lime, polymer "filter aid" and sand were tested.

- Lime - in graph 7 a remarkable increase with concern to specific capacity can be noticed under addition of lime. This curve shows a peak at a lime dosage of 40 kg/t RM which means that higher dosage rates than this optimum would change the results to the worse.
- Polymer of the type HX300 as it is used by Interalumina in the thickeners was added to the filter feed at a certain, optimized concentration. The effects of this polymer addition are shown on graph 10, wherefrom it can be found that the specific capacity under addition of polymer can not be increased compared to the results from filtration without polymer. However - from graph 9 we see that at a dosage of 60 g/t RM the optimum can be found with regard to polymer addition.
- So called "filter aid" also was added on request of the plant operators - however, no positive effects could be found as it is shown in graph 8.
- The normal procedure at Interaluminas operation is to separate a sandy portion from the red mud before thickening and washing in order to avoid plugging of the thickeners. As this sand in any case will have to be disposed, it was obvious to run a serie of tests with a mixture of this sand and red mud.

### ● Filter cake washing

It was found that for the actual cake drying a angle of not more than 30° is required in order to obtain residual moistures of 25 % approx. This short drying angle means that the remaining part of the possible drying zone can be used for filter cake washing. Not only high recovery rates for soda and alumina are the results of this cake washing but also specific air consumption and residual moisture can be reduced by this means.

In graph 11 several test points show the influence of varying feed solids concentration at constant vessel pressure, filter speed and wash water amount. As a general conclusion we see that increased feed solids correspond to low moisture and low specific air consumption.

## 8. Conclusions

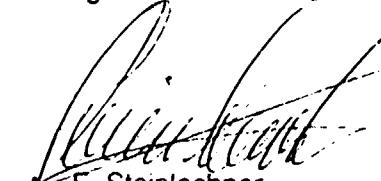
Only testing the filtration behavior of the red mud over a certain period and taking all possible material variations into consideration enables us to find a well based layout for a commercial size hyperbaric disc filter plant. As such a basic layout the following figures can be calculated:

Specific capacity:	400 kg/m <sup>2</sup> , hr dry RM
Air consumption:	300 Nm <sup>3</sup> /t dry RM
Wash water:	0,5 m <sup>3</sup> /t dry RM, 90° C approx.
Vessel pressure:	5 bar
Filter speed:	1 to 2 RPM
Feed temperature:	90° C, approx.
Feed solids:	500 g/l
Soda content:	20 - 30 g/l Na <sub>2</sub> O

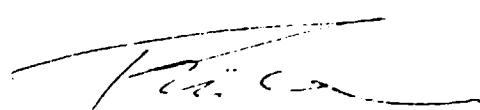
Beside the fact that only the tested **Hyperbaric Filter System** with the specified equipment parameters provides a feasible, proven technology to filter red mud to a moisture content of 25 % weight approx. it must be mentioned that

- only red mud with this moisture content can be disposed on a standard, unsealed disposal site without requiring any safety measurements conc. possible environmental damage.
- the filter cake with 25 % moisture is handleable on conventional transport systems like belt conveyors for the reason that its nature is not thixotropic anymore.
- caustic soda out of the desilication product can be recovered during hyperbaric filtration to an extremely high extend which makes the hyperbaric filter system a very feasible one as well.

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