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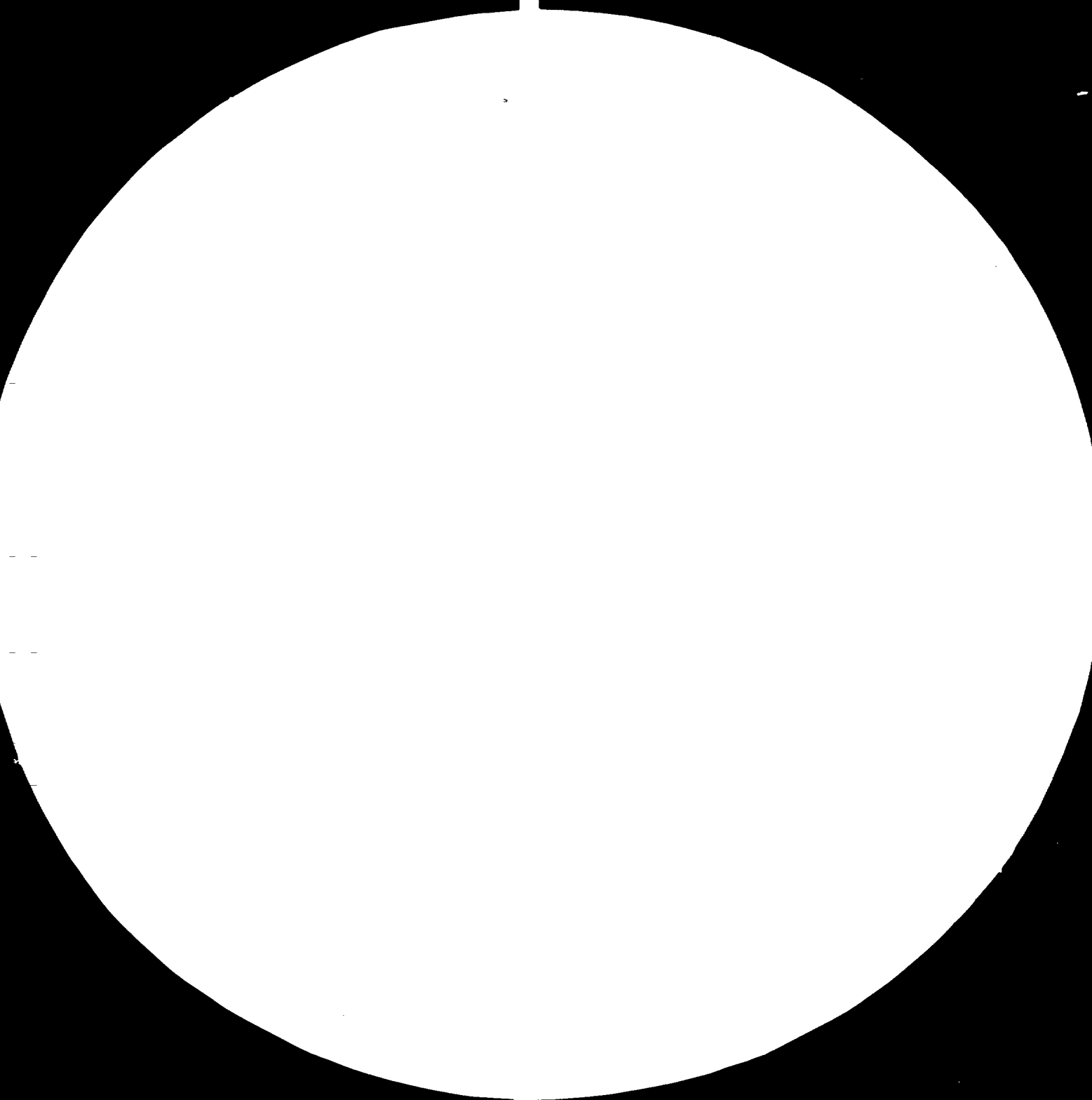
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McBride, R. E. et al. / *Journal of Applied Optics*, 1987

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UNITED NATIONS
INDUSTRIAL DEVELOPMENT ORGANIZATION

DRAFT FINAL REPORT

FEASIBILITY STUDY

Mongolia. ESTABLISHMENT OF A PILOT PLANT FOR
PROCESSING OF BIOCHEMICAL PRODUCTS.

M O N G O L I A

PROJECT NO: DP/MON/80/004

POLYTECHNA

SPOFA

PRAGUE - CZECHOSLOVAKIA

DECEMBER 1981

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CHAPTER I. EXECUTIVE SUMMARY

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PROJECT BACKGROUND AND HISTORY
/CHAPTER II/

The long-term conception of the United Nations Organization of the programme of aid to developing countries also included a project of improvement and expansion of pharmaceutical industry in Mongolia.

This industrial branch in Mongolia is presently in the development stage, and only a limited assortment of pharmaceutical products and dispensing forms of domestic provenance is available. The Mongolian Government is well aware of the necessity to build up the pharmaceutical industry for the needs both of the human and the veterinary medicinal care.

The experts of both interested parts had recommended to aim the development conception at the exploitation of Mongolia's very good and rich basis of natural raw materials. Mongolia has a relatively large animal production, with large amounts of slaughterhouse offal, which is a cheap, but valuable raw material for certain sorts of biochemical pharmaceutical industrial products.

The very processing of the slaughterhouse offal to pharmaceuticals, substances or final dispensing forms, is the main idea and target of the present project.

In Mongolia three centres exist at present where slaughterhouse offal is produced. The largest and most modern one is located in the capital city, Ulan Bator, and

In this way, the Mongolian Government plans to build biochemical integrated works. A part of this planned complex is the proposed pilot plant for biochemical manufacture, which is the subject of the present study.

Its production programme will include peptone, pepsin, trypsin, chymotrypsin, pancypsin, cholesterol, pancreatin, blood hydrolysate, dried bile, and manufacture of tablets and sterile substances.

The production capacities are projected for a pilot-plant scale.

The products specified above will primarily augment the assortment of pharmaceuticals available on the Mongolian market. Some of the substances will also represent valuable export commodities.

In Mongolia the biochemical integrated works is subordinated to the Ministry of Lights and Food Industries.

The aim of the present feasibility study is to estimate the technical and economical feasibility of the intended buildup of a branch of pharmaceutical industry based on exploitation of slaughterhouse offal.

The United Nations Industrial Development Organization /UNIDO/ in Vienna, Austria, had commissioned Czechoslovak experts with the elaboration of the present study. The experts are represented by the Foreign Trade Organization Polytechna, Prague Czechoslovakia. The specialists in the biochemical production branch had been selected with a view to a complex elaboration of the study, with due regard to the technical,

economical and technological complexity of the problem to be solved.

All of them have been active for many years as specialists at the United Pharmaceutical Works in Prague, Czechoslovakia /SPOFA/. The experts' field-work team consisted of specialists active in the research and quality control of biochemical engineering and building specializations. Additional assisting workers active in specialized branches collaborated in assembling the present final report in Czechoslovakia. They were mainly experts in planning, economics, steering and automation, electrical engineering, electronics, work hygiene, and work safety.

Before the departure for Mongolia the working team selected the reference data and offers from stable suppliers of equipment for the chemical-pharmaceutical industry. Data for comparison were collected from manufacturing plants and facilities of analogous characters, already realized.

During the field-work, urbanistic exploration was made with regard to the planimetric and altimetric features, geographic and demographic conditions, and potential connection with the electricity and water supply mains, sewage network, and traffic systems. Explorations were made of the marketing and sale conditions, the actual level of technology, the price and foreign exchange regulations. The qualifications were checked of labourers, technologists, engineering workers, and managers. The supply situation and prices of raw materials

and energies, and the wages policy were ascertained. The annual number and volume of working days were calculated, and potential shift work was estimated.

Consultations with workers of the United Nations Development Programme /UNDP/ and United Nations Industrial Development Organization /UNIDO/, as well as with state authorities in Mongolia, represented an important component of the field-work.

After the experts' return from Mongolia the export possibilities and the prices of machinery and technological equipment were re-checked.

The reality of the study depends not only on the preliminary exploratory work, but also on a proper elaboration. As a guideline for its contents the MANUAL FOR THE PREPARATION OF INDUSTRIAL FEASIBILITY STUDIES /1978/ had been accepted.

The present feasibility study not only has been aimed at documenting that the fundamental idea was realizable; moreover, from the technical aspect the entire project follows the endeavour at a maximal universal versatility of the proposed premises and equipment, to enable the Mongolian party to realize pilot-plant-scale production of additional pharmaceutical products, recommended by the experts in the subsequent chapters.

MARKET AND PLANT CAPACITY
/CHAPTER III/

MARKETING STUDY

In estimations of the total requirements for the planned biochemicals and pharmaceuticals it has to be taken into account first of all that Mongolia is a country with a small population and therefore the domestic consumption of most of the planned products will represent only a smaller part of the total production volume. Consequently, for all products their potential export has to be considered, which, in addition, would considerably contribute to the national economy.

Therefore, already in the projects of the initial production capacities and of the production programme structure also the present potential sales of the final products had been taken into consideration. The demands of the world market have been estimated on the basis of recent data obtained from the foreign trade organization, and the domestic requirements for the health care and industrial needs in Mongolia, on the basis of information obtained from the Mongolian side during the group of experts' stay. In Mongolia the chemical, pharmaceutical, and consumers' goods industries, as well as the health care services, are still in the development stages, and therefore the estimations are rather rough; nevertheless, the domestic demands can be expected to show rather rising tendencies.

According to the production possibilities and technologies now handy in Mongolia the initial production programme for the proposed pilot plant has been established

Production of peptone	32.000	kg
Production of pepsin, pharmaceutical	100	kg
Production of pepsin, for food industry	1.000	kg
Production of chymotrypsin	20	kg
Production of trypsin	12	kg
Production of pancypsin	87,5	kg
Production of cholesterol	700	kg
Production of pancreatin	3.000	kg
Production of blood hydrolysate	1.860	kg
Production of dried bile	3.900	kg

This chemical production is then connected with the pharmaceutical department, where the production of pharmaceuticals in their final form is performed. This department ensures the manufacture of tablets and coated tablets and the manufacture of injections.

The production programme of the biochemical department should be taken as an initial one, and for the future development of the whole pilot plant it was proposed to extend the programme for production of serum gonadotropin, insulin and heparin. All of these products are in strong demand on the world markets, steadily exceeding the supply, and this

situation can be also expected in the near future.

The technology of serum gonadotropin is presently in the stage of laboratory research in Mongolia.

Technological procedures of heparin and insulin production have not been studied in Mongolia so far. The experts recommended to the Mongolian side, in view of the importance of both products, to acquire the production know-how from abroad.

SALES FORECAST

The main products of the pilot plant will be substances. The manufacture of tablets and injections will receive additional substances supplied by the existing pharmaceutical works in Mongolia.

It is expected that the main buyer of exported goods will be the Union of Soviet Socialist Republics; the Hungarian People's Republic, Korean People's Republic, German Democratic Republic, Denmark, and Japan are expected to come next. Some products may also find interest in other countries. Obviously, the export volume is dependent on the quality of the products.

MATERIALS AND INIUTS
/CHAPTER IV/

IV. Specifications for raw and auxiliary materials

In the pilot-plant operations, both domestic raw materials and other materials - imported from abroad, will be processed.

Raw materials supply planning

A. Domestic raw materials consist in slaughterhouse offal.

In Mongolia the livestock is slaughtered in the course of half a year. The slaughterhouse plants are equipped with efficient cool stores, from which the raw materials for the pilot-plant processing can be successively drawn.

The pilot-plant stores are calculated for storage of 400 tons of raw materials, ensuring sufficient reserves for bridging over the period when the slaughterhouse plants are not working. The storage temperature is -20 to - °C.

B. Imported raw and auxiliary materials

In view of ireegular deliveries of imported chemicals the supply planning must ensure reserves for minimally 4 months.

The storerooms for such materials, destined both for chemical and pharmaceutical production, are dimensioned accordingly.

Besides the basic raw materials specified before, the production programme requires certain chemicals not produced in Mongolian Peoples Republic.

LOCATICN AND SITE
/CHAPTER V/

LOCATION

The all-state territorial conditions in Mongolia for the selection of a locality suitable for the development of biochemical production for the pharmaceutical industry issue from an exploration of the whole territory. In Mongolia three slaughterhouse plants are operating at present. The largest of them is located in the capital city Ulan Bator. Therefore the decision was made, in the all-national interest as well as in accordance with the plant operation economy, to build up an integrated biochemical works in this locality.

The projected biochemical pilot plant will be a part of the planned biochemical integrated plant in Ulan Bator. Upon the expert team's recommendation a site in the west part of the city was selected. According to the master extension plan the territory concerned lies within a future industrial zone.

The selected building site is plane, its subsoil consists of compact gravel sand. In the western direction it neighbours on a new heating plant N^o 4 under construction. On the northern side connections with the city communication, steam pipeline, and electricity main are possible. The southern part of the lot offers connections with a railroad siding and with the city water main. The eastern side is reserved for extension of other industrial plants.

PROJECT ENGINEERING

/CHAPTER VI/

The pilot plant for the future biochemical integrated works is designed with a view to comply with the requirements of the whole production plan, with respect to the technological processes proposed and the local conditions. This means that the whole complex of aspects necessary for the correct running of the proposed plant has been taken into account in the layout plan. It is presumed that the pilot plant will be realized in advance.

The machinery and technological equipment proper is of a fairly universal character and expedient for the proposed production programme. The planned pilot plant in fact is a link between the research and the production. This idea is also inherent in the prospective master plan, whose draft outline is documented in the present report, too, although its elaboration had not been imposed to the expert group.

The layout plan of the pilot plant is actually governed by the characters of its parts, namely,

- biochemical production
- pharmaceutical manufacture
- quality control laboratories.

The main technological premise B-109 - Biochemical pilot plant is a three-floor building with the ground dimensions 55m x 16m. This building is designed for biochemical production and is complemented with the store rooms, cooled stores, cooling boxes and other auxiliary units.

- A - 14 Neutralization plant
- A - 15 Store for inflammable solvents
- A - 16 Central pressure air production
- A - 17 Cooling plant
- A - 18 Transformer station 35/0.4 kV
- A - 19 Air conditioning station
- A - 20 Maintenance shops
- A - 21 In-process transportation

Building part

- B - 101 Preparation of the land for buildings
- B - 102 Outside connections of electricity 35/0.4 kV
- B - 103 Outside connections of water supply
- B - 104 Outside connections of low tension electricity
- B - 105 Outside connections of steam /pipe lines/
- B - 106 Outside connections to city sewerage
- B - 107 Roadways
- B - 108 Store for liquid material
- B - 109 Biochemical pilot plant
- B - 110 Pharmaceutical pilot plant
- B - 111 Quality control and social premises.

PLANT ORGANIZATION AND OVERHEAD COSTS
/CHAPTER VII/

From the organizational aspect of the new biochemical integrated works, the projected pilot plant for biochemical production for pharmaceutical purposes will operate as an integral cost centre.

This decision is based on the fact, that the pilot plant includes facilities for pilot-plant-scale operations, requiring a complete cooperation and coordination among the individual departments.

Evidently, the pilot plant operates as an integral dispositional whole, and the raw material input and finished product output will be assessed in a uniform way. The transfer of documentation from the pilot plant for full-scale production will be made in the form of a separate master file for each final product.

The production plan, although specified in the pertinent chapter inclusive of the capacities, may be considerably variable. The disposition must allow a fat variation of the programme with regard to the actual results of the research.

Despite the great complexity of all operations, the extent of the pilot plant proper is adequate to its pre-production mission, and therefore the pilot plant is provided to constitute an integral cost centre.

The authors of the present chapter have decided, having taken into consideration the propositions, to combine the factory and administrative overheads and not to respect them separately.

The structure of the socialist society, also reflected in the industrial enterprises in Mongolia, presumes that the overhead costs include the following items:

- property taxes
- depreciation:
 - buildings /2.6% per year/
 - machinery /13% per year/
 - office equipment /3.5% per year/
- communication
- off-site transport
- maintenance

Administrative costs, costs of building management, labourers' wages and social security contributions are included in the pertinent chapters and not included in Chapter VII.

It is pointed out that the insurance fees /social security contributions/ and the income taxes both employees and labourers are already included in their basic salaries and hour wages /see Chapter VIII/.

Consequently, the authors of the present report will adhere to the recommended calculation alternative 1, and consider solely the remaining overhead costs, as specified in Schedule 7-1.

MANPOWER
/CHAPTER VIII/

LABOURERS

The manning plan was elaborated with regard to the proposed production programme, the production capacities, and also to the local conditions.

Labourers have to be provided for the following sectors:

- biochemical production
- pharmaceutical production
- warehouse handling
- energy supply operation
- auxiliary facilities
- maintenance work
- clean-up services
- watching services

The selection of the labourer categories was consulted with the Mongolian side with the following results:

labourer category 6B - qualified labourer with apprenticeship certificate

- experienced labourer - foreman or deputy foreman

5B - labourer with apprenticeship certificate in the branch of

- biochemical production
- pharmaceutical production
- maintenance
 - electricians
 - locksmiths
 - joiners
- energy supply operators

4B - labourers for assembling and storage handling

3B - charwomen, female packaging workers, forwarding department hands, gatekeepers.

Technicals and administration

The manpower plan of these categories is based on the given economic and production structure, reflected in the organizatory regulations of the pilot plant; the following posts are provided:

- director of the pilot plant
- vice director - economics
 - production
 - research
- head, biochemical department
- head, pharmaceutical department
- head, quality control unit
- chief technologist
- chief engineer
- workers in accounting department
- workers in planning department
- workers in supply department
- workers in personnel department
- secretaries
- workers in staff education department
- librarian
- heads of analytical laboratories
- chief physicist
- chief biochemist
- chief analyst
- laboratory technicians

In the category of technical and clerical workers, collaboration of foreign specialists is planned in the initial operation period /see Schedule 8-3/ and, on the other hand, in training of Mongolian workers in selected foreign countries with advanced biological production.

For the purposes of Mongolian workers' training, shorter or longer visits to foreign countries are envisaged.

Shorter visits /2-4 weeks/ are intended to improve the training in the spheres of

- biochemical production processes
- biochemical production planning
- production management
- good manufacturing practice

Longer visits are envisaged for

- 3 biochemists
- 3 quality control specialists
- 2 pharmacists

Training directly at the pilot plant in Mongolia will be organized and supervised by the following persons:

- chief engineer of construction
- specialist in biochemical production
- expert in quality control
- specialist in pharmaceutical production
- bacteriologist.

IMPLEMENTATION SCHEDULE
/CHAPTER IX/

Essential data and activities

The planned pilot plant is financed partially by the Mongolian Government and partially by the UNIDO, Regional Office Vienna. Both partners had agreed that the project would be realized in the period 1982 - 1986. The Mongolian Government will ensure the realization conditions in the full extent.

The obligations ensuring the realization are divided between both sides as mentioned in Chapter II.

Selection of realization plan and working schedule

The realization plan, in connection with the working schedule, must have the following consecution:

- hydrogeological prospecting
- altimetric and planimetric survey
- building plan
- preparation of building site

The construction work proper will start with the construction of water piping, gas piping, steam piping, electricity cable lines, canalization, and roadway connection. The realization of this work is planned for 1953 /E-102 to E-107/.

The buildings are designed so that analogous construction technology will serve for all three of them. Underground work is excluded. Completely assembled structures are envisaged. The heights of the individual floors and the total height of the highest building allow a maximal use of construction mechanization.

The character of the machinery equipment, its prescriptive dimensions, and the interconnection of the individual technological units allow successive assembling.

The assembling of machinery equipment must start in E-103, where the volume of equipment and assembling work is largest.

Key and decisive terms of pilot-plant construction

- start of pilot-plant construction
B-101, B-102, B-103, B-104,
B-105, B-106, B-107, B-109 May 1983
- start of construction
B-110 and B-111 October 1983
- making B-109 ready for machinery
equipment assembling June 1984
- making B-110 ready for machinery
equipment assembling January 1985
- start of construction B-108 June 1985
- making B-111 ready for machinery
equipment assembling June 1985
- trial operation June 1986
- full operation December 1986

Estimation of project realization costs

In the case of the operations carried out in the course of the investment phase up to the moment of the start of full production operation, the costs have to be estimated of the following items:

- projecting work
- authors' supervisory activity
- inspection activity
- administration of building and construction management
- fees for approval procedures
- training of staff and labourers

The financial means for covering the costs of

- the building site
- technological equipment
- building and construction work
- machinery and equipment
- materials
- raw material
- overhead costs

are specified in pertinent foregoing chapters.

FINANCIAL AND ECONOMIC ANALYSIS

/CHAPTER X/

Project financing

The project is financed by the UNIDO and the Mongolian Government. The financial means have not the character of loans and are not-repayable.

Project costs

The total investment cost, 18,451.900, include the fixed investment costs and the reproduction capital expenditure. The working capital is provided annually by the Mongolian Government.

	Foreign currency	Local currency	Total
<u>A. Fixed investment costs</u>			
Site preparation		809.000,-	809.000,-
Buildings		9,729.000,-	9,729.000,-
Machinery	3,393.540,-	600.000,-	3,993.540,-
Total			14,531.540,-
<u>B. Reproduction capital expenditure</u>			
			3,920.360,-
Total A + B			18,451.900,-
<u>C. Working capital</u>			
			3,389.455,-

Financial means:

Source	Fixed investment costs	Reproduction capital expenditure	Total
Total investment costs	14,531.540,-	3,920.360,-	18,451.900,-

These means will be drawn in the course of the construction period as follows:

Expences are published in Mongolian currency /Tg/

YEAR	MONGOLIAN GOVERNMENT	UNIDO	TOTAL	%
1982	494.000,-	359.300,-	853.300,-	4,62
1983	3,106.000,-	458.000,-	3,564.000,-	19,32
1984	3,115.000,-	776.000,-	3,891.000,-	21,09
1985	3,770.000,-	1,690.000,-	5,460.000,-	29,59
1986	2,640.000,-	2,043.600,-	4,683.600,-	25,38
Total	13,125.000,-	5,326.900,-	18,451.900,-	100,00

With due regard to the character of the present project, formulated in Chapter II of this study, the Chapter X is elaborated in accordance with the guidelines set in the Manual for the Preparation of Industrial Feasibility Studies, UNIDO publication No.E.II.B.5 of 1978.

The essential data given below lead to the following conclusions:

- 1/ The annual rate of profit from the equity capital grows from 13.12% in the year of production to 28.70% in the year of expected 100% production capacity:

	Construction					Start-up and full production					
Year	1	2	3	4	5	6	7	8	9	10	11
Net profit after tax						2421272	3837096	5004411	5295121	5295121	5295121
Equity capital	18451900	18451900	18451900	18451900	18451900	18451900	18451900	18451900	18451900	18451900	18451900
Rate of profit%						13,12	20,80	27,12	28,70	28,70	28,70

- 2/ The initial investment costs, ie, 18,451.900,- Tg, will be paid back within less than 9 years from the start of construction / calculation of rate of return of the project/:

Year	Net profit	Depreciation	Amount paid back	Balance
1	---	---	---	18,451.900,-
2	---	---	---	- " -
3	---	---	---	- " -
4	---	---	---	- " -
5	---	---	---	- " -
6	2,421.272,-	698.200,-	3,119.472,-	15,332.428,-
7	3,837.096,-	698.200,-	4,535.296,-	10,797.132,-
8	5,004.411,-	698.200,-	5,702.611,-	5,094.521,-
9	5,295.121,-	698.200,-	5,993.321,-	---
10	5,295.121,-	698.200,-	5,993.321,-	---

3/ The simple rate of profit in the 9th year after the start of construction /production with 100% capacity/ will be:

$$R_e = \frac{\text{net profit}}{\text{equity capital}} \times 100 = \frac{5,255.121}{18,451.900} \times 100 = 28,70\%$$

4/ The rate of return of the project in the 9th year after the start of construction will be:

$$\frac{\text{net profit}}{\text{total investment outlay}} \times 100 = \frac{5,295.121}{10,626.517} \times 100 = 49,83\%$$

C o n c l u s i o n s

As it has been already mentioned, the proposed pilot plant is projected as a base for the future development of the pharmaceutical industry in Mongolia and it will enable to the country not only the production of basic biochemical products but also the extension of assortment of basic pharmaceuticals necessary for Mongolian Health Care. Important role will also play the fact that this production will fully utilize the waste products from slaughterhouses and so bring their good revaluation.

The planned widening of the biochemical production programme by the future production of principal and very important drugs like insulin, heparin and gonadotropins will bring an additional economical contribution for the country's economy, because these biochemical pharmaceuticals play an important role in medical care all over the world.

CHAPTER II. PROJECT BACKGROUND AND HISTORY

CONTENTS:

PROJECT BACKGROUND

PROJECT PROMOTER AND/OR INITIATOR

PROJECT HISTORY

FEASIBILITY STUDY

PROJECT BACKGROUND

The promoter of the feasibility study is the United Nations Industrial Development Organization, P.O. BOX 300, A - 1400 Vienna, Austria.

The feasibility study was elaborated by a team of Czechoslovak experts - employees of SPOFA United Pharmaceutical Works, National Corporation, Prague, Czechoslovakia /Mr.V.Vévra, team leader; Mr.Z. Bárta, Grad. Eng. J. Frýda, Mr. F. Kroutil/. All of them have been active for many years in the branches of biochemistry and pharmaceutical industry, with minimally 25 years of practice each. They are represented by Polytechna, Foreign Trade Organization, Prague, Czechoslovakia.

PROJECT PROMOTER
AND/OR INITIATOR

The project initiator is the Government of the Mongolian People's Republic /Mongolian Government/, which gives top priority to the present project. Accordingly, the Mongolian Government had applied to the UNDP/UNIDO for technical aid as well as for financial subsidy for the development of biochemical and pharmaceutical industry.

In the general information of UNDP/UNIDO of 3 February, 1980, the financial contribution of the Mongolian Government was limited to the sum of 60 million Tughasak. The financial contribution granted by the UNDP/UNIDO was set to 1 760 000 dollars. This sum may be spent exclusively for machinery and technological equipment, spare parts, and personnel training.

The financial quota granted by the UNDP/UNIDO is included in the UN long-term plan for Mongolia and must not be exceeded. Furthermore, it is presumed that 65% of the sum is destined for equipment, and 35%, for personnel training.

PROJECT HISTORY

The development of the project is presently in the stage of a feasibility study, which is being elaborated on the basis of

- the Preparatory assistance document UNIDO of 20 January, 1980
- the General information UNIDO of 3 February, 1980

On the basis of general preparatory work and in parallel with the prospecting and surveying work carried out in Mongolia, the team of experts succeeded in designing preliminary schemes of premises and preliminary flow-sheets of production processes already in the field-work stage. The preliminary documentation included fundamental production schemes, data on capacities, a list of machinery and equipment, requirements for raw materials, power and water supplies, manpower, data on the extent of building work and costs.

In Mongolia the initial documentation was discussed with the representatives of

- the UNDP Agency in Ulan Bator:
 - Mr. Aborkin, UNDP Resident Representative in Ulan Bator
 - Mr. Linamyaa, UNDP officer in Ulan Bator
 - Mr. Polievtkov, officer of the UNIDO Technical Section, Vienna
- the Mongolian side:
 - Mr. Sumya, Vice-Minister of Light and Food Industry in Ulan Bator

Mr. Pod, Vice-President of Government Commission on
Economic Relations in Ulan Bator

Mr. Tseremdendev, Director, Research Centre for Enzymology
and Microbiology in Ulan Bator

Mr. Yambamba, Chief Architect of the City of Ulan Bator.

The results of the consultations were reconsidered in the
final phase, and adequate suggestions have been taken into
account in the present study.

FEASIBILITY STUDY

The aim of the present feasibility study is to assess the economical and technical feasibility of building up in Mongolia pharmaceutical industrial works, based on exploitation of slaughterhouse offal as the principal domestic raw material.

It is assumed that to Ulan Eator, where the sources of slaughterhouse offal are largest, these materials will be also transported from the slaughterhouses in Darchan and Choibalsan for the needs of the future biochemical integrated works.

The present yearly production of slaughterhouse offal:

1.	Cattle's pancreas	122	tons
2.	Cattle's bile /choler/	68	tons
3.	Cattle's trachea	65	tons
4.	Cattle's paunch	950	tons
5.	Cattle's stomach /ventricle/	430	tons
6.	Cattle's eyes	10.2	tons
7.	Mucous membrane of Cattle's abomasum	166	tons
8.	Cattle's blood	3 800	tons
9.	Cattle's spinal cord	177	tons
10.	Cattle's hoofs	263	tons
11.	Cattle's horns	530	tons

In view of the present technological level of the biochemical and biopharmaceutical production in Mongolia it is presumed that the whole investment will be realized as a pilot plant. Local inquiry showed that the raw material volumes are

adequate to the intended project. The Mongolian side possesses certain fundamental technological knowledge of biochemical production. It also has at disposal technological personnel with university grade education. This personnel, after adequate special training, will be capable to manage and develop the biochemical production.

The production programme and capacities of the pilot plant are limited, firstly, by the financial support granted by the UNDP/UNIDO for the machinery, technological equipment, personnel training, and spare parts; and secondly, by the Mongolian side's qualification for industrial production of biochemical pharmaceuticals.

Time schedule of building and construction costs

Granted by	1982	1983	1984	1985	1986	Total
UNDP/UNIDO US \$	106 000	135 000	229 000	500 000	604 600	1576 000
Granted by						
Mongolia TG	494 000	3106 000	3115 000	3770 000	2640 000	13125 000

The feasibility study pays due regard to

- a/ the society and economic benefit
 - b/ the technical versatility of the pilot-plant premises and equipment
- a/ In Mongolia the pharmaceutical industry and its development are coordinated by the Ministry of Light and Food Industry.

This branch is responsible for the development of pharmaceutical production, inclusive of final products /dispensing forms/ for the domestic health care. Export of certain pharmaceuticals contributes to the assets of the national economy.

The experts suggest the following production programme for the pilot plant:

Production of peptone

pepsin

trypsin

chymotrypsin

pancypsin

cholesterol

pancreatin

blood hydrolysate

dried bile

Manufacture of tablets

sterile substances.

The localization of the pilot plant for biochemical products in the future biochemical integrated works is disposed conceptionally between the research and production. The biochemical integrated works is included into industrial zone in the western sector of the City of Ulan Bator. The distance from the raw-material source is about 1 500 m via city roadway. The immediate connections with the roadways, railway, power and water lines, sewage system, etc. are shown in the Fig. II. A schematic map of Mongolia shows the

localization of Ulan Bator /Fig. I./.

b/ Technical versatility of premises and equipment

The building-technological conception of the project is based on the presumption that the pilot plant for biochemical production will be realized as a separate part of the whole biochemical integrated works. Consequently, from the aspect of external interrelations the pilot plant buildings are designed so as to be self-contained in all respects;

- raw material storage
- production facilities
- energy supplies
- water supply
- manpower
- quality control
- maintenance
- administrative apparatus
- stores management.

The conceptual design of the buildings, premises, and equipment also takes in consideration potential changes in the production programme, motivated by future research work results.

ESTIMATE OF INVESTMENT COST									
PRE-INVESTMENT STUDIES AND PREPARATORY INVESTIGATIONS									
			ITEM DESCRIPTION			UNIT COST US DOLLARS	COST		
							FOREIGN DOLLARS	LOCAL DOLLARS	TOTAL DOLLARS
1.			FEASIBILITY STUDY (PRE-INVESTMENT STUDY)				39868		134750
2.			HYDROGEOLOGICAL PROSPECTING					150000	150000
3.			LAND SURVEY, PLANI- AND ALTIMETRIC					20000	20000
			TOTAL				39868	170000	304750

(INSERT TOTAL IN SCHEDULE 10-2/1)

CHAPTER III. MARKET AND PLANT CAPACITY

CONTENTS:

DEMAND AND MARKET STUDY

SALES FORECAST AND MARKETING

PRODUCTION PROGRAMME

PLANT CAPACITY

DEMAND AND MARKET STUDY

MARKETING STUDY

In estimations of the total requirements for the planned biochemicals and pharmaceuticals it has to be taken into account first of all that Mongolia is a country with a small population and therefore the domestic consumption of most of the planned products will represent only a smaller part of the total production volume. Consequently, for all products their potential export has to be considered, which, in addition, would considerably contribute to the national economy.

Therefore, already in the projects of the initial production capacities and of the production programme structure also the present potential sales of the final products had been taken into consideration. The demands of the world market have been estimated on the basis of recent data obtained from the foreign trade organization, and the domestic requirements for the health care and industrial needs in Mongolia, on the basis of information obtained from the Mongolian side during the group of experts' stay. In Mongolia the chemical, pharmaceutical, and consumers' goods industries, as well as the health care services, are still in the development stages, and therefore the estimations are rather rough; nevertheless, the domestic demands can be expected to show rather rising tendencies.

As for the export possibilities, principal roles will be played obviously by the quality and prices of the final

products and their ensuing competitive capacities on the world markets. Both of the factors can be best influenced by the very construction of production facilities in the form of the pilot plant, which has better possibilities of further qualitative and quantitative development as well as the versatility allowing its adaptation for production of other economically more advantageous products, already proposed in the project for future development. On the basis of the present analysis of the proposed production it can be expected that all of the planned products have chances of export of even greater than planned quantities. The only exception is chymotrypsin, a side product of trypsin; the world market demands for chymotrypsin are lower at present.

PEPTONE - The project envisages the production of 52 tons per year. Out of this amount the domestic need is about 1 ton. The rest can be exported in substance. It is mainly required as microbiological nutrient substrate; in view of the recent development of a new industrial branch - production of microbial proteins for feedstuffs - the demand for peptone has a rising tendency.

PEPSIN - The project envisages the production of pepsin in two grades, for the needs of pharmaceutical and of food industries. The product is in steady demand on the world markets, and the whole projected quantity can be exported. In Mongolia the yearly consumption is about 5 kg of pharmaceutical grade pepsin for tablet manufacture for the health

care, and about 500 kg of the food grade pepsin for the food industry.

TRYPsin - At present this enzyme plays a significant role, and practically the whole planned production is exportable, either in the form of sterile substance in vials or of substance in larger packages.

For domestic health care a yearly production of about 50 000 vials of 50 mg trypsin each is considered, corresponding to about 2,5 kg of the enzyme.

CHYMOTRYPsin - The demand for this proteolytic enzyme is presently lower. Nevertheless, the major part of produced chymotrypsin can be expected to be consumed mainly in the domestic manufacture of the final dispensing form - dusting powder for the treatment of torpid wounds and deep burn injuries. From the yearly produced 20 kg of chymotrypsin, about 100 000 packages of the dusting powder can be manufactured; the surplus exceeding the domestic requirements, which still are difficult to estimate, will be exportable, mainly to the USSR.

PANcYPSIN - This product essentially consists in a mixture of two proteolytic enzymes, prepared from mutton pancreas by a procedure developed at the Research Centre for Applied Enzymology and Microbiology in Ulan Bator. According to the

Mongolian side the product is exportable mainly to Asian markets, in form of either sterile substance in vials with 50 mg each, or in substance in larger packages. The planned yearly production of 87,5 kg of pancypsin should mainly cover the potential export.

CHOLESTEROL - This product represents one of essential components of ointments and cosmetics. Therefore it is much in demand, and the projected yearly production, 700 kg, is exportable to several countries.

PANCREATIN - If of good quality, the product is readily exportable to several countries, besides the domestic consumption. The product is a mixture of all digestive enzymes produced in the pancreas; it serves for pharmaceutical manufacture of enteric coated tablets, but also in tanning, leather, and textile industries and in the manufacture of modern washing preparations. Out of the planned yearly production of 3 tons, a half will be consumed in Mongolia, and the rest can be exported.

BLOOD HYDROLYSATE - The product is mainly destined for domestic manufacture of baby food products. Consequently, the whole planned yearly production of 1860 kg blood hydrolysate is destined for the Mongolian food industry. It has to be emphasized, however, that the blood hydrolysate production

could be substantially extended by introducing the manufacture of hydrolysate infusion solutions for the needs of Mongolian health care. This newly introduced manufacture would lead to a substantial enlargement of the blood hydrolysate production, exploitation of practically the entire amount of the basic raw material - beef blood - available, and a reduction of import of hydrolysate infusion solutions. All this, however, would require a substantial extension of the pharmaceutical department for the rooms and equipment necessary for the manufacture of the infusion solutions, and therefore would require a separate project study.

DRIED BILE - Yearly production of 3 900 kg of dried bile is planned. The product is used not only in pharmaceutical manufacture, but also in consumers' goods industries for technical purposes. Out of the projected amount, the Mongolian pharmaceutical manufacture will need about 500 kg for coated tablets of Fel Tauri and Cholenzym, and the Mongolian consumers' goods industry, another 500 kg; the rest can be exported.

MANUFACTURE OF TABLETS AND INJECTIONS - This manufacture is mainly destined for domestic needs. Because the pharmaceutical department has manufacturing capacities exceeding the needs for processing only the products supplied by the

projected biochemical department, it will be necessary to supplement the pharmaceutical manufacturing programme by other products required for the Mongolian health care.

C o n c l u s i o n

For prospective future development of the projected pilot plant there was further proposed the production of serum gonadotropin, heparin, and insulin. All of these products are in strong demand on the world markets, steadily exceeding the supply, and this situation can be also expected in the near future.

The technology of serum gonadotropin is presently in the stage of laboratory research in Mongolia.

Technological procedures of heparin and insulin production have not been studied in Mongolia so far. The experts recommended to the Mongolian side, in view of the importance of both products, to acquire the production know-how from abroad.

SALES FORECAST AND MARKETING

SALES FORECAST

The main products of the pilot plant will be substances. The manufacture of tablets and injections will receive additional substances supplied by the existing pharmaceutical works in Mongolia.

It is expected that the main buyer of exported goods will be the Union of Soviet Socialist Republics; The Hungarian People's Republic, Korean People's Republic, German Democratic Republic, Denmark, and Japan are expected to come next. Some products may also find interest in other countries. Obviously, the export volume is dependent on the quality of the products.

Expected consumption in Mongolia and potential export

Biochemical products

Product	Mongolia kg	Export kg	Total production at pilot plant kg
Peptone	1 000	31 000	32 000
Fepsin , pharmaceuti- cal grade	5	95	100
food grade	500	500	1 000
Chymotrypsin	10	10	20
Trypsin	2,5	9,5	12
Pancypsin	7,5	80	87,5
Cholesterol	100	600	700
Pancreatin	1 500	1 500	3 000
Blood hydrolysate	1 860	-	1 860
Dried bile	1 000	2 900	3 900
Tablets	30 mill.	-	30 mill.
Injections	9 mill.	-	9 mill.

Per cent proportions of domestic consumption and potential export

Product

Peptone	3,10	96,90	100
Pepsin, pharmaceutical grade	5	95	100
food grade	50	50	100
Chymotrypsin	50	50	100
Trypsin	20,8	79,2	100
Pancypsin	8,6	91,4	100
Cholesterol	14,3	85,7	100
Pancreatin	50	50	100
Blood hydrolysate	100	-	100
Dried bile	25,6	74,4	100
Tablets	100	-	100
Injections	100	-	100

PRODUCTION PROGRAMME

Production programme

The project is the first step of the development programme of pharmaceutical industry, based on exploitation of domestic raw materials.

The production programme, issuing from research results obtained at the Centre for Applied Enzymology and Microbiology, is intended to cover both the domestic requirements and the export.

The proposed technological project reckons with the following production programme:

Peptone
Pepsin, pharmaceutical grade
Pepsin, food grade
Trypsin
Chymotrypsin
Pancypsin
Cholesterol
Pancreatin
Blood hydrolysate
Dried bile
Tablets
Sterile substances

Serum gonadotropin is much in demand; when the research in Mongolia is finished, the production could be started at the pilot plant.

If know-how for the production of heparin and insulin were obtained from abroad, only a minor supplementation and adaptation of the equipment would allow to include these products into the production programme. This possibility is envisaged in later stages.

Production programme and planned production capacities of the pilot plant:

- Peptone - Pilot-plant production capacity:
32 tons per year of bacteriological grade peptone
- Pepsin - Pilot-plant production capacity:
100 kg per year of pharmaceutical grade pepsin,
1000 kg per year of food grade pepsin
- Trypsin - Pilot-plant production capacity:
12 kg per year, and
- Chymotrypsin - Pilot-plant capacity:
20 kg per year.

A part of the production of both enzymes will be finalized in the form of vials with sterile product; a part, in the form of dusting powder for external use; and the rest, in the form of either sterile or nonsterile substances in bottles.

- Pancypsin - a mixture of proteolytic enzymes
pilot-plant production capacity:
87.5 kg per year. It will be used for the same
purposes as trypsin and chymotrypsin.
- Cholesterol - a basic component of ointments; major amounts
are destined for cosmetic products.
Pilot-plant production capacity:
700 kg per year.
- Pancreatin - a mixture of all pancreatic enzymes, used not
only for pharmaceutical, but also for leather,
tanning, and textile industrial purposes.
Pilot-plant production capacity:
3 tons per year.
- Blood hydrolysate - usable for baby-food manufacture.

Pilot-plant production capacity:
1 860 tons per year.

The proposed design utilizes only a part of the raw material - beef blood - available for production of blood hydrolysate for nutritional purposes. A full utilization of available blood might be made possible by potential augmentation of the production programme by blood hydrolysate for infusion solutions.

The authors of the present feasibility study recommend this alternative as economical-

ly advantageous, although the Mongolian side does not intend to realize this variant at the planned pilot plant.

- Dried bile - production of 3 900 kg per year is presumed. A part of the product should be finalized in the form of film-coated tablets, and the rest, in substance. At the pilot plant, as projected, the equipment planned for the production of peptone will partially serve for the production of dried bile.

- Manufacture of tablets - the projected equipment has the capacity of about 6 000 tablets per hour. In tablet form there will be manufactured the domestic Mongolian preparations Cholenzym and Allochol, and out of the recommended Czechoslovak pharmaceutical products, Acipepsol, Pancreolan, Fel Tauri film-coated tablets. All of the specified sorts of tablets will be manufactured of substances produced at the pilot plant in quantities sufficient for domestic consumption. This volume of manufacture will require only 25% of the tablet manufacturing capacity. A full utilization of the whole capacity of the

pharmaceutical department is expected from finalization of substances supplied from external production sources, in the volume of 30 million tablets per year.

- Manufacture of sterile products - The projected equipment has a capacity of filling 3 000 vials per hour. Sterile filling is reckoned with of trypsin and chymotrypsin in solution with subsequent freezing and freeze-drying in vials, and of pancypsin in solution with subsequent freezing and freeze-drying in larger /300-ml/ bottles. A full utilization of the projected equipment is expected from filling of solutions of substances produced and supplied by the existing pharmaceutical works in Ulan Bator, up to 9 million vials per year.

Besides the capacities of the production units proper, the capacities of some auxiliary facilities have to be mentioned, which are dimensioned adequately to the expected production volumes.

- Recuperation of ethanol and acetone - The recuperation capacities of the equipment-
- ethanol - 250 kg rectificate/hour,
 - acetone - 180 kg rectificate/hour,

correspond to solvent recuperation at the production capacities stated before, at one-shift or two-shift work. A capacity reserve is available partly in the second, and then in the third shifts.

- Production of demineralized and of pyrogen-free water:
 - demineralized water, 200 liters per hour,
 - pyrogen-free water, 50 liters per hour.
- The capacities of the remaining auxiliary units ensure the operation of the pilot plant.

PLANT CAPACITY

COMPILE 3-3.
PRODUCTION PROGRAMME

PRODUCT, BY-PRODUCT, WASTES	UNIT 200% CAPACITY	PRODUCTION PROGRAMME											
		YEAR 6 (1987)	YEAR 7 (1988)	YEAR 8 (1989)	YEAR 9 (1990)	YEAR 10	YEAR 11						
		CAPACITY (%)	UNITS	CAPACITY (%)	UNITS	CAPACITY (%)	UNITS	CAPACITY (%)	UNITS	CAPACITY (%)	UNITS	CAPACITY (%)	UNITS
HEPTONE	50	75	21000	95	30400	100	30000	100	30000	100	30000	100	30000
HEPOM MEDICINAL	50	75	75	95	100	100	100	100	100	100	100	100	100
HEPOM	50	75	750	95	950	100	1000	100	1000	100	1000	100	1000
CINOTRYPSIN	50	75	15	95	11	100	10	100	100	100	100	100	100
TRYPOM	50	75	0	95	114	100	114	100	100	100	100	100	100
PANICRYN	50	75	1375	95	8312	100	8712	100	8712	100	8712	100	8712
ENOLICETROL	50	75	350	95	667	100	700	100	700	100	700	100	700
PANDURIN	50	75	1500	95	2950	100	3000	100	3000	100	3000	100	3000
BLOOD MONOPOLAR	50	75	500	95	1169	100	1200	100	1200	100	1200	100	1200
DRIED BILE	50	75	1150	95	2105	100	2100	100	2100	100	2100	100	2100
TRAPINS	50	75	150000	95	225000	100	225000	100	225000	100	225000	100	225000
INERTIOPONE	50	75	450000	95	850000	100	900000	100	900000	100	900000	100	900000

CHAPTER IV. MATERIALS AND INPUTS

CONTENTS :

CHARACTERISTICS OF MATERIALS
AND INPUTS

SUPPLY PROGRAMME

CHARACTERISTICS OF MATERIALS
AND INPUTS

IV. Specifications for raw and auxiliary materials

In the pilot-plant operations, both domestic raw materials and other materials imported from abroad, will be processed.

The domestic raw materials consist in slaughterhouse offal, of which the following sorts will be used in the pilot-plant production:

	metric tons per year
1/ Beef pancreas	117
2/ Mutton pancreas	30
3/ Beef rumen and abomasum	552
4/ Pork gastric mucosa	5.2
5/ Spinal cord	18
6/ Beef blood	81,5
7/ Beef and mutton bile	60
8/ Beef gastric mucosa	20

The specified quantities are only fractions of the available amounts of offal.

The offal's sources are slaughterhouse plants in Ulan Bator, Dargham, and Choibalsan. All of these plants are equipped with efficient cooling boxes, ensuring adequate storage of the offal.

SUPPLY PROGRAMME

Raw materials supply planning

A. Domestic raw materials consist in slaughterhouse offal.

In Mongolia the livestock is slaughtered in the course of half a year. The slaughterhouse plants are equipped with efficient cool stores, from which the raw materials for the pilot-plant processing can be successively drawn.

The pilot-plant stores are calculated for storage of 400 tons of raw materials, ensuring sufficient reserves for bridging over the period when the slaughterhouse plants are not working. The storage temperature is -20 to -30°C .

B. Imported raw and auxiliary materials

In view of irregular deliveries of imported chemicals the supply planning must ensure reserves for minimally 4 months. The storerooms for such materials, destined both for chemical and pharmaceutical production, are dimensioned accordingly.

Besides the basic raw materials specified before, the production programme requires certain chemicals not produced in the Mongolian People's Republic.

Raw materials imported from abroad

Item	Grade	Metric tons per year
Sulphuric acid	92 - 96%	5.07
Phosphoric acid	chem. pure	20.8
Calcium oxide - quicklime		65.46
Hydrochloric acid	chem. pure	3.57
Sodium chloride	chem. pure	5.12
Kieselguhr		2
Ethanol	96%	17.9
Acetone	98%	31.36 / 39.6m ³ /
Sodium hydrogen carbonate		0.7
Ammonium sulphate	chem. pure	157
Sodium hydroxide solution	40%	0.39
Barium chloride		0.11
Magnesium sulfate	chem. pure	0.14
Calcium chloride	chem. pure	0.12
Oxalic acid	chem. pure	0.32
Ether	pure	0.03
Boric acid	chem. pure	0.17

SCHEDULE 4-1/1
ESTIMATE OF PRODUCTION COST : MATERIALS AND INPUTS

ESTIMATE OF PRODUCTION COST
MATERIALS AND INPUTS

PROJECT COMPONENT NO. A-01 DESCRIPTION: PRODUCTION OF
PFTONE

	ITEM DESCRIPTION	UNIT COST	COST		
			FOREIGN	LOCAL	TOTAL
			US Dollars	Tg	Tg
552	BEEF RUMEN AND ABOMASUM	262		144 624	144 624
32	BEEF PANCREAS	15 000		480 000	480 000
208	PHOSPHORIC ACID	254		5 283	5 283
487	CALCIUM OXIDE /QUICKLIME/	167		8 133	8 133
09	HYDROCHLORIC ACID	3 000		2 700	2 700
	AUXILIARY MATERIALS			76 812	76 812
16210 ³ KWH	ELECTRIC ENERGY	180		29 160	29 160
2 10 ³	STEAM	17		34 000	34 000
4010 ³ m ³	WATER	04		16 000	16 000

TOTAL

796 712 796 712

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-2

ESTIMATE OF PRODUCTION COST : MATERIALS AND INPUTS

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT NO. A-02 DESCRIPTION: PRODUCTION OF PEPSIN

No.	ITEM DESCRIPTION	UNIT COST	CCST		
			FOREIGN	LOCAL	TOTAL
			US Dollars	Tg	Tg
20 t	BEEF GASTRIC MUCOSA	2700		5400	5400
5.2 t	PORK GASTRIC MUCOSA	1710		8892	8892
1.1 t	HYDROCHLORIC ACID	3000		3300	3300
4.8 t	SODIUM CHLORIDE	3900		18720	18720
17 m ³	ETHANOL	9200		156400	156400
	AUXILIARY MATERIALS			18500	18500
³ 5210 kWh	ELECTRIC ENERGY	0,18		9360	9360
³ 15010 t	STEAM	17		2550000	2550000

TOTAL

2770572 2770572

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-2/

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT No.A-03 DESCRIPTION: PRODUCTION OF TRYPSIN, CHYMOTRYPSIN, PANCREPSIN

No.	ITEM DESCRIPTION	UNIT COST	COST		
			FOREIGN US Dollars	LOCAL Tg	TOTAL Tg
20 t	BEEF PANCREAS				
30					
35					
85		15000		1 275000	1 275000
0,84 t	SULPHURIC ACID	4290		3603	3603
1,57 t	HYDROCHLORID ACID	3000		4710	4710
156,6 t	AMMONIUM SULPHATE	8900		1 393740	1 393740
0,3 t	KIESELGURH	20000		6000	6000
0,32 t	SODIUM CHLORIDE	3900		1248	1248
0,493 t	BARIUM CHLORIDE	20000		9860	9860
0,39 t	SODIUM HYDROXIDE 40%	18000		7038	7038
0,137 t	MAGNESIUM SULPHATE	2500		342,5	342,5
	OTHER MATERIALS				6000
	AUXILIARY MATERIALS			120000	120000
³ 25.10KWh	ELECTRIC ENERGY	0,18		4500	4500
³ 20 m	WATER	0,4		8	8

TOTAL

2,8320495 2832049,5

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-2/

ESTIMATE OF PRODUCTION COST : MATERIALS AND INPUTS

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT No.A-04 DESCRIPTION: PRODUCTION OF CHOLESTEROL

No.	ITEM DESCRIPTION	UNIT COST	COST		TOTAL Tg
			FOREIGN US Dollars	LOCAL Tg	
18 t	SPINAL CORD	1 400		25 200	25 200
6 t	ACETONE	5 000		30 000	30 000
0,9 m ³	ETPANCL	9 200		8 280	8 280
0,36 t	SULPHURIC ACID	4 290		1 544	1 544
	AUXILIARY MATERIALS			7 550	7 550
3.10 m ³	ELECTRIC ENERGY	0,18		540	540
72 t	STEAM	17		1 224	1 224
500 m ³	WATER	0,4		200	200

TOTAL

74.488,- 74.488,-

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-2/

ESTIMATE OF PRODUCTION COST : MATERIALS AND INPUTS

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT No.A-05 DESCRIPTION: PRODUCTION OF PANCREATIN

No.	ITEM DESCRIPTION	UNIT COST	COST		TOTAL Tg
			FOREIGN US Dollars	LOCAL Tg	
30 t	MUTTON PANCREAS	15000		450 000	450 000
0,75 t	SODIUM HYDROGEN CARBONATE	5360		4 020	4 020
33,6 m ³	ACETONE	5000		168 000	168 000
	AUXILIARY MATERIALS			64 000	64 000
6.10Kwh ³	ELECTRIC ENERGY	0,18		1 080	1 080
20 t	STEAM	17		340	340

TOTAL

687.440,- 687.440,-

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-2/

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT		No.A-06	DESCRIPTION :	PRODUCTION OF BLOOD HYDROLYSATE		
ITEM DESCRIPTION	UNIT	COST	COST		TOTAL	
			FOREIGN	LOCAL		
			US Dollars	Tg	Tg	
81,5 t	BEEF BLOOD	1 400		114 100	114 100	
2,87 t	SULPHURIC ACID	4 290		12 312	12 312	
2,76 t	CALCIUM OXIDE /QUICKLIME/	167		461	461	
AUXILIARY MATERIALS				10 000	10 000	
37440Kwh	ELECTRIC ENERGY	0,18		6 740	6 740	
500 t	STEAM	17		8 500	8 500	
2880 m ³	WATER	0,4		1 152	1 152	

TOTAL

153.265- 153.265 +

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-2//

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT No.A-07 DESCRIPTION : PRODUCTION OF DRIED BILE

ITEM DESCRIPTION	UNIT COST	COST		TOTAL Tg
		FOREIGN US Dollars	LOCAL Tg	
60 t MUTTON AND BEEF BILE	980		58 800,-	58 800,-
1660KWh ELECTRIC ENERGY	0,18		299,-	299,-
115 t STEAM	17		1 955,-	1 955,-
1100 m ³ WATER	0,4		440,-	440,-

TOTAL

61 494,- 61.494,-

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-2/

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT No. A-08 DESCRIPTION : MANUFACTURE OF TABLETS

ITEM DESCRIPTION	UNIT	COST		
		FOREIGN US Dollars	LOCAL Tg	TOTAL Tg
AUXILIARY MATERIALS - COSTS SPECIFIED WITH PRODUCTS				
8000Kwh ELECTRIC ENERGY	C,18		1.440,-	1.440,-
TOTAL			1.440,-	1.440,-

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4

ESTIMATE OF PRODUCTION COST : MATERIALS AND INPUTS

ESTIMATE OF PRODUCTION COST
MATERIALS AND INPUTS

PROJECT COMPONENT No.A-09 DESCRIPTION : MANUFACTURE OF STEEL
PREPARATIONS

ITEM DESCRIPTION	UNIT	COST		TOTAL
		FOREIGN US Dollars	LOCAL Tg	
AUXILIARY MATERIALS - COSTS SPECIFIED WITH PRODUCTS				
30000Kwh ELECTRIC ENERGY	0,18		5.400,-	5.400,-
80 t STEAM	17		1.360,-	1.360,-

TOTAL

6.760,- 6.760,-

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-

ESTIMATE OF PRODUCTION COST : MATERIALS AND INPUTS

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT No.A-11 DESCRIPTION : SOLVENT RECUPERATION PLANT

ITEM DESCRIPTION	UNIT COST	COST		TOTAL Tg
		FOREIGN US Dollars	LOCAL Tg	
5500 kWh ELECTRIC ENERGY	0,18		990,-	990,-
950 t STEAM	17		16.150,-	16.150,-
8350 m ³ WATER	0,4		3.340,-	3.340,-

TOTAL

20.480,- 20.480,-

/CARRY OVER TOTAL OF PRESENT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-2//

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT No.A-12 DESCRIPTION : DEMINERALIZED AND PYROGEN-FREE WATER PLANT

ITEM DESCRIPTION	UNIT	COST		
		FOREIGN US Dollars	LOCAL Tg	TOTAL Tg
400 m ³ WATER	0,4		160,-	160,-
120 t STEAM	17		2.040,-	2.040,-
2460 m ³ WATER	0,4		984,-	984,-
TOTAL			3.184,-	3.184,-

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-2/

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

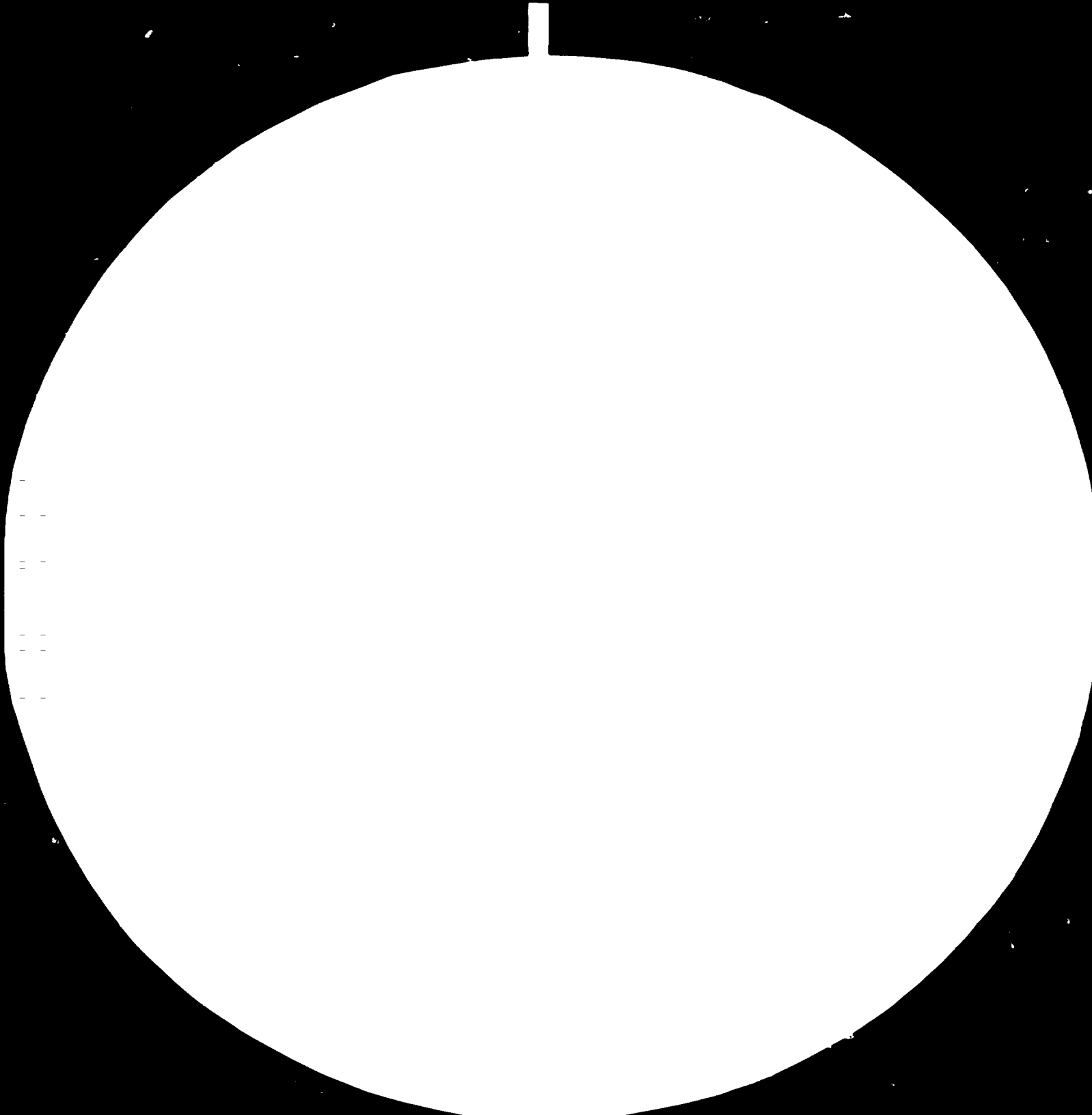
PROJECT COMPONENT No.A-14 DESCRIPTION : NEUTRALIZATION STATION

ITEM DESCRIPTION	UNIT	COST		TOTAL
		FOREIGN US Dollars	LOCAL Tg	
1 t SULPHURIC ACID	4.290		4.290,-	4.290,-
14 t CALCIUM OXIDE /QUICKLIME/	167		2.338,-	2.338,-
4610KWH ELECTRIC ENERGY	0,19		8.280,-	8.280,-
TOTAL			14.908,-	14.908,-

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-2//

22 00 2A

2



ESTIMATE OF PRODUCTION COST : MATERIALS AND INPUTS

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT No.A-15 DESCRIPTION : STORAGE OF INFLAMMABLE SOLVENTS

ITEM DESCRIPTION	UNIT	COST		TOTAL
		FOREIGN US Dollars	TOTAL Tg	
800KWH ELECTRIC ENERGY	0,18		144,-	144,-

TOTAL

144,-

144,-

/CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 4-

ESTIMATE OF PRODUCTION COST : MATERIALS AND INPUTS

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT No.A-16 DESCRIPTION : PRESSURE AIR AND VACUUM CENTRAL.

ITEM DESCRIPTION	UNIT COST	COST		TOTAL
		FOREIGN US Dollars	LOCAL Tg	
501CKWH ELECTRIC ENERGY	0,18		9.000,-	9.000,-
1000 m ³ WATER	0,4		400,-	400,-

9.400,-

ESTIMATE OF PRODUCTION COST : MATERIALS AND INPUTS

ESTIMATE OF PRODUCTION COST

MATERIALS AND INPUTS

PROJECT COMPONENT No.A-17 DESCRIPTION : COOLING PLANT

ITEM DESCRIPTION	UNIT COST	COST		TOTAL Tg
		FOREIGN US Dollars	LOCAL Tg	
158010KWh ELECTRIC ENERGY	0,18		284.400,-	284.400,-

TOTAL

284.400,- 284.400,-

ESTIMATE OF PRODUCTION COST : MATERIALS AND INPUTS

ESTIMATE OF PRODUCTION COST						
MATERIALS AND INPUTS						
PROJECT COMPONENT No.A-19 DESCRIPTION : AIR CONDITIONING						
		ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US Dollars	LOCAL Tg.	TOTAL Tg.
34.1	3	ELECTRIC ENERGY	0,18		6.120,-	6.120,-

TOTAL 6.120,- 6.120,-
 REFER TO SUMMARY SHEET / SCHEDULE 4-2//

RECEIVED FROM
MAY 1964

РАСЧЕТ ПОТРЕБНОСТИ И СТОИМОСТИ СЫРЬЯ И
МАТЕРИАЛОВ ДЛЯ ПРОИЗВОДСТВА 10 КГ "ХИМОТРАНСИНА"
/РАССАСОВКОЙ ПО 5 КГ И ПО 100 ГР /

п/п. Сырье и основные материалы	ед. изм.	Норма расхода		цена за единицу /тугр/	сумма /тыс. тугр/
		на 1 кг	на 10 кг		
I. Подкислительная железа					
1. крупного рогатого скота	тн	1,0	10,0	15-00	150,00
2. Аммоний сернокислый х.ч.	тн	1,6	16,0	3-92	142,7
3. Серная кислота х.ч.	кг	40,0	400,0	4-29	1,7
4. Натр едкий х.ч.	кг	1,0	10,0	17-00	0,17
5. Спирт ректификат	абс.л	3,3	33,0	110-00	3,63
6. остат натрий двухзамещенный х.ч.	кг	1,5	15,0	1-70	0,105
7. остат калий однозамещенный х.ч.	кг	0,3	3,0	9-57	0,287
8. Кизельгур	кг	10,0	100,0	20-00	2,00
9. Барий хлористый х.ч.	кг	10,4	104,0	20-00	2,08
10. Смола КМ-2	кг	0,5	5,0	36-19	0,18
11. Соливая кислота х.ч.	кг	14,3	143,0	3-00	0,429
12. Ацетон ч.д.в.	л	1,2	12,0	5-00	0,60
13. Сульфат магния х.ч.	кг	4,0	40,0	2-50	0,10
14. Натр хлористый х.ч.	кг	10,2	102,0	3-90	0,40
15. Итого					152,01
ВСПОМОГАТЕЛЬНЫЕ МАТЕРИАЛЫ					
1. Фильтровальная бумага	кг	41,0	410,0	3-00	1,23
2. Подпергамент	кг	1,1	11,0	27-20	0,30
3. Оберточная бумага	кг	0,4	4,0	7-50	0,30
4. Марки	к	10,0	100,0	2-00	0,20
5. Лазер	к	15,0	150,0	6-00	0,90
6. Беловое полотно	к	2,0	20,0	10-00	0,20
7. Вата	кг	5,0	50,0	5-00	0,25
8. Фильтровальные пластины	шт	50,0	500,0	3-00	1,50
9. Флаконы 5 кг	тыс. шт	220,0	1100,0	437-00	535,7
10. Пробки резиновые	тыс. шт	220,0	1100,0	375-00	416,9
11. Колпачки металлические	"	220,0	1100,0	134-00	147,4
12. Коробки литографические	"	220,0	1100,0	70-00	77,0
13. Биллашк	"	220,0	1100,0	20-00	22,0

14. Инвентурный	ТНС.ИП	220,0	1100,0	10-50	27,5
15. Бухгалтер	ИП	11,0	55,0	1-50	0,5
16. Мили	ИП	40,0	400,0	5-50	2,0
17. Кассир	ИП	25,0	250,0	50-50	12,5
18. Канцелярия	ИП	100,0	1000,0	10-50	10,0
19. Конюх	ИП	20,0	200,0	40-50	1,0
20. Прованс	ИП	0,8	8,0	2-50	0,0
21. Корень инвентурный					0,0
ВСЕГО					1516,0

РАСЧЕТ СТОИМОСТИ СУРЬЯ

п/п:	Наименование сурья и материалов	ед. изм.	цена за единицу	кол-во	сумма /тыс. руб./
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Сурья:

1.	Кондошупочная колода крупного рогастого скота	тн	17000-00	00,0	00,0
2.	Кондошупочная колода мелкого рогастого скота	тн	15000-00	00,0	00,0
3.	Сухая мякоть	тн	00000-00	,0	00,0
4.	Трава	тн	000-00	00,0	00,0
5.	Молочко	тн	4000-00	200,0	800,0
6.	Рубан и лезвие	тн	0000-00	000,0	000,0
7.	Синтетическая оболочка скотух крупного рогастого скота	тн	1000-00	,0	0,0
8.	Синтетическая оболочка скотух мелкого рогастого скота	тн	1410-00	00,0	00,0
9.	Кроль крупного рогастого скота	тн	1500-00	00,0	00,0
10.	Глаза крупного и мелкого рогастого скота	тн	800-00	10,0	8,0
11.	Рога и копыта	тн	800-00	500,0	400,0
12.	Сырье для изготовления сурья	тн	000-00	,0	0,0
13.	Сырье для изготовления сурья	тн	000-00	,0	0,0
Итого					2015,5

II. Содержание материалов:

1.	Алюминий сернистый х,ч	кг	0-00	,0	000,0
2.	Серная кислота х,ч	кг	4-29	6112,5	26,22
3.	Азотная кислота х,ч	кг	0,85	1937,0	0,87
4.	Натр едкий х,ч	кг	18-00	3473,0	62,51
5.	Сульфат х,ч	кг	36-19	165,0	5,97
6.	Натрийгидрокарбонат х,ч	кг	3-80	12000,0	50,00
7.	Сульфат х,ч	кг	0-00	,0	0,0
8.	Сульфат х,ч	кг	0-00	,0	0,0
9.	Кислота х,ч	кг	20-00	3547,6	72,95
10.	Соляная кислота х,ч	кг	3-00	51630,0	1549,6
11.	Сульфат х,ч	кг	2-50	4185,3	10,34
12.	Борная кислота х,ч	кг	18-00	269,0	3,73

16. Аэротехнический институт	И	0-00		
18. Эфир	ИП	10-10	10,0	0,00
19. Интервенционная комиссия И, Ч	ИП	0-00	0,0	0,00
20. Совет по вопросам А-4: административный И, Ч	ИП	1-10	10,0	0,00
21. Совет по вопросам административного И, Ч	ИП	0-07	0,0	0,00
22. Совет технико-экономического И, Ч	ИП	10-00	100,0	0,00
23. Совет по вопросам экономики И, Ч	ИП	10-00	100,0	0,00
24. Аппарат И, Ч	ИП	11-17	100,0	0,00
25. Комитет по вопросам И, Ч	ИП	0-10	0,0	0,00
26. Комитет по вопросам И, Ч	ИП	00-07	0,0	0,00
27. Аппарат И, Ч	ИП	10-10	100,0	0,00
28. Комитет по вопросам И, Ч	ИП	40-10	0,0	0,00
29. Комитет по вопросам И, Ч	ИП	10-00	0,0	0,00
30. Комитет по вопросам И, Ч	ИП	00-00	100,0	0,00
31. Совет по вопросам И, Ч	ИП	0-00	100,0	0,00
32. Совет по вопросам И, Ч	ИП	10-00	100,0	0,00
33. Совет по вопросам И, Ч	ИП	0-01	100,0	0,00
34. Совет по вопросам И, Ч	ИП	0-00	100,00	0,00
35. Совет по вопросам И, Ч	ИП	7-00	100,0	0,00
36. Совет по вопросам И, Ч	ИП	10-00	100,0	0,00
37. Совет по вопросам И, Ч	ИП	0-00	100,0	0,00
38. Совет по вопросам И, Ч	ИП	0,70	100,0	0,00
39. Совет по вопросам И, Ч	ИП	100-00	100,0	0,00
40. Совет по вопросам И, Ч	ИП	7-00	100,0	0,00
41. Совет по вопросам И, Ч	ИП	7-70	70,0	0,00
42. Совет по вопросам И, Ч	ИП	10-10	100,0	0,00
43. Совет по вопросам И, Ч	ИП	10-10	100,0	0,00
44. Совет по вопросам И, Ч	ИП	4-00	100,0	0,00
45. Совет по вопросам И, Ч	ИП	00-00	000,0	0,00
46. Совет по вопросам И, Ч	ИП	0-00	100,0	0,00
47. Совет по вопросам И, Ч	ИП	00-00	000,0	0,00
48. Совет по вопросам И, Ч	ИП	0,00	0,0	0,00
49. Совет по вопросам И, Ч	ИП	10-00	1000,0	0,00
50. Совет по вопросам И, Ч	ИП	-	0,0	-
51. Совет по вопросам И, Ч	ИП	170-07	0,0	0,00
52. Совет по вопросам И, Ч	ИП	000-00	0,0	0,00
53. Совет по вопросам И, Ч	ИП	10-10	10,0	0,00
54. Совет по вопросам И, Ч	ИП	0-10	0,0	0,00

87. Изменно-линейный разрыв м,ч	ИР	21-01		
88. Казань	ИР	7-00	61,0	6,70
89. Коробчатый тисолов м,ч	ИИ	200-00	7,0	7,00
90. Невысокая избушка	ИИ	107-00	510,0	51,00
91. Казань	ИР	0-00	217,0	9,11
92. Казань единично-линейный	ИР	0-00	300,0	5,00
93. Изменно-линейный разрыв м,ч	ИИ	0-00	100,0	2,70
94. Казань	ИР	0-00	100,0	6,00
95. Строительный объект	ИР	7-00	1000,0	0,00
96. Станция теплообменная	ИР	00-00	15,0	0,00
97. Трубопроводный разрыв	ИР	5-00	10,0	0,00
98. Станция теплообменная	абс.л.	4-01	30,0	0,00

Итого

II. Инженерно-технические мероприятия:

1. Строительство бунгала	ИР	7-00	1000,0	10,00
2. Санитарно-технические бунгала	ИР	0-00	2000,0	0,00
3. Инженерно-технические мероприятия	ИР	0-00	2000,0	7,00
4. Трубы 1000 мм	ИР	7-00	1000,0	10,00
5. Строительство	ИР	07-00	1000,0	10,00
6. Казань	ИР	10-00	1000,0	10,00
7. Казань	ИР	2-00	1000,0	0,00
8. Казань	ИИ	2-00	1000,0	7,00
9. Казань	ИИ	0-00	1700,0	7,00
10. Казань	ИР	5-00	1000,0	0,00
11. Станция Казань	ИИ	10-00	1000,0	10,00
12. Строительство объектов Казань	ИР	0-00	3000,0	10,00
13. Казань	ИР	5-00	1000,0	7,00
14. Строительство	ИИ	7-00	1000,0	10,00
15. Станция Казань	ИР	10-00	1000,0	0,00
16. Строительство	ИР	07-00	1000,0	0,00
17. Строительство	ИР	0-00	1000,0	7,00
18. Строительство	ИР	0-00	7000,0	1,00
19. Строительство	ИР	7-00	1000,0	10,00
20. Строительство	ИР	0-00	1000,0	0,00
21. Станция теплообменная	абс.л.	4-01	2000,0	10,00
22. Строительство объектов	ИИ	10-00	1000,0	0,00
23. Казань	ИР	5-00	1000,0	7,00
24. Строительство	ИР	10-00	1000,0	10,00
25. Строительство в ИР	ИИ.ИР	07-00	1000,0	10,00
26. Строительство объектов	ИИ.ИР	07-00	7000,0	7,00
27. Строительство объектов	ИИ.ИР	04-00	1000,0	10,00

39. Лигатура "лесные поросли"	ТМБ.ИП	70-00	7400,0	807,0
40. Травянки	ТМБ.ИП	20-00	7300,0	700,1
40. Писюрутки	"	15-00	3000,2	8107,7
41. Караган	Г	0,01	3307,5	0,01
42. Кожи млекопитающих	ТМБ.хупр		3,4	0,4
42. Прочие материалы	"		4,4	4,1
43. Валюжан	ИП	40-00	1170,0	41,0
43. Селюк Ч.Б.А	ИП	10-00	70,0	2,1
44. Кожаные резинки	ИП	5-00	700,0	3,0
47. Кармашки и др.	ИП	5-00	500,0	2,7
48. Кожи	ИП	3-00	1000,0	0,0
49. Мелкозерное сырье	И	32-00	6100,0	1100,7
40. Кожи	И	1-00	10,0	0,0
41. Свойства (изготавливаются)	ИП	10-00	10,0	0,0
42. Травянки	ТМБ.ИП	0,01	10000,0	10,0
43. Кожи	ИП	0-00	1,0	0,0
44. Кожи	ИП	0-07	3000,0	4,0
Итого				17000,0

Итого

17000,0

РАСЧЕТ ПОСРЕДСТВ НА СЧЕТ 1. СТОИМОСТИ СУБСИДИИ
 НАПРАВЛЕННЫЕ НА ПОДДЕРЖКУ СЕЛЬСКОГО ХОЗЯЙСТВА
 "СХИМ" / ПО ДОКЛАДУ № 3 И 4 ПОС. 1997 Г./

№/п	Наименование объектов материалов	Ед. изм.	Норма	Колич-во	Стоимость	
					по плану	по факту
	на оплату труда рабочих	руб	0,4	80,0	10000	8000
4.	Земельный налог	руб	0,37	100,0	37000	37000
5.	Амортизационный материал	руб	140,5	10000,0	1405000	1405000
6.	Средства вывоза	руб	305,0	10000,0	3050000	3050000
8.	Платежи по налогам	руб	2,0	700,0	14000	14000
9.	Амортизационный материал	руб	1000,0	10000,0	10000000	10000000
7.	Средства вывоза	руб	8,0	10000,0	80000	80000
3.	Земельный налог	руб	3,28	10000,0	328000	328000
8.	Платежи по налогам	руб	0,6	500,0	3000	3000
10.	Платежи по налогам	руб	1,5	1000,0	15000	15000
11.	Средства вывоза	абс.л	6,4	1000,0	64000	64000
12.	Средства вывоза	руб	1,0	1000,0	10000	10000
13.	Средства вывоза	руб	0,1	100,0	1000	1000
14.	Земельный налог	л	3,0	1000,0	3000	3000
15.	Средства вывоза	руб	20,0	1000,0	20000	20000
Итого:						
по плану:						
1.	Амортизационный материал	руб	50,0	10000,0	5000000	5000000
2.	Средства вывоза	руб	16,5	10000,0	1650000	1650000
3.	Амортизационный материал	руб	27,0	10000,0	2700000	2700000
4.	Платежи по налогам	л	1,5	1000,0	15000	15000
5.	Земельный налог	л	10,0	10000,0	100000	100000
6.	Земельный налог	л	10,0	10000,0	100000	100000
7.	Платежи по налогам	руб	35,0	10000,0	3500000	3500000
8.	Земельный налог	руб	5,0	700,0	35000	35000
9.	Земельный налог	руб	2,0	1000,0	20000	20000
10.	Земельный налог	руб	0,5	70,0	3500	3500

11. Лампы ртутные	"	5,0	200,0	3-00	1,50
12. Карданы и шпиль	"	1,0	200,0	5-10	0,20
13. Шпиль	шт	20,0	1000,0	4-00	4,00
14. Шпиль 5 шт	шт.шт	44,0	2200,0	017-00	107,00
15. Шпиль ртутные	"	44,0	2200,0	017-00	107,00
16. Ассортимент металлические	"	44,0	2200,0	017-00	107,00
17. Лампы люминесцентные	"	44,0	2200,0	017-00	107,00
18. Ассортимент металлические	"	44,04	2200,0	017-00	107,00
19. Инструменты	"	44,0	2200,0	017-00	107,00
20. Шпиль	шт	3,0	1000,0	3-00	0,30
21. Шпиль	"	5,6	2000,0	50-00	11,20
22. Шпиль	"	44,4	2200,0	10-00	4,44
23. Шпиль	шт		11,2	5-00	0,56
24. Шпиль электрические 1 л	шт	10,0	1000,0	1-00	1,00
25. Шпиль	г	500	500,0	0-00	0,50
26. Шпиль электрические					0,50

Итого:

107,00

№	Год	Средняя температура	Средняя влажность	Средняя скорость ветра	Средняя облачность
1	1950	10.0	75.0	2.5	45.0
2	1951	10.5	76.0	2.6	46.0
3	1952	11.0	77.0	2.7	47.0
4	1953	11.5	78.0	2.8	48.0
5	1954	12.0	79.0	2.9	49.0
6	1955	12.5	80.0	3.0	50.0
7	1956	13.0	81.0	3.1	51.0
8	1957	13.5	82.0	3.2	52.0
9	1958	14.0	83.0	3.3	53.0
10	1959	14.5	84.0	3.4	54.0

Средние значения метеорологических элементов

№	Год	Средняя температура	Средняя влажность	Средняя скорость ветра	Средняя облачность
1	1960	15.0	85.0	3.5	55.0
2	1961	15.5	86.0	3.6	56.0
3	1962	16.0	87.0	3.7	57.0
4	1963	16.5	88.0	3.8	58.0
5	1964	17.0	89.0	3.9	59.0
6	1965	17.5	90.0	4.0	60.0
7	1966	18.0	91.0	4.1	61.0
8	1967	18.5	92.0	4.2	62.0
9	1968	19.0	93.0	4.3	63.0
10	1969	19.5	94.0	4.4	64.0

№	Год	Средняя температура	Средняя влажность	Средняя скорость ветра	Средняя облачность
1	1970	20.0	95.0	4.5	65.0
2	1971	20.5	96.0	4.6	66.0
3	1972	21.0	97.0	4.7	67.0
4	1973	21.5	98.0	4.8	68.0
5	1974	22.0	99.0	4.9	69.0
6	1975	22.5	100.0	5.0	70.0
7	1976	23.0	101.0	5.1	71.0
8	1977	23.5	102.0	5.2	72.0
9	1978	24.0	103.0	5.3	73.0
10	1979	24.5	104.0	5.4	74.0

Средние значения метеорологических элементов

Средние значения метеорологических элементов за период с 1950 по 1979 гг.

РАСЧЕТ ПОТРЕБНОСТИ И СТОИМОСТИ СЫРЬЯ И
МАТЕРИАЛОВ ДЛЯ ПРОИЗВОДСТВА НА 600 КГ
"ХОЛЕСТЕРИНА" /РАСФАСОВКОЙ ПО 20 КГ В
УПАКОВКЕ/

Сырье и основные материалы	Ед. изм	норма расхода на		Цена /туг/	Сумма /тыс.туг/
		1 кг	600 кг		
1. Спинной мозг	кг	22	13200,0	1-41	18,61
2. Спирт ректификат	абс.л	3,54	2124,0	130-00	138,06
3. Ацетон	л	5,0	3000,0	5-00	15,00
4. Серная кислота х,ч	кг	0,5	300,0	4-29	1,29
5. Уголь активированный	кг	0,06	36,0	4-50	0,15
ВСЕГО:					154,5

ВСПОМОГАТЕЛЬНЫЕ
МАТЕРИАЛЫ

1. Подпергамент	кг	0,03	18,0	27-28	0,50
2. Сукно Бэтта	м	0,013	7,8	15-00	0,12
3. Бязь	м	0,02	12,0	3-80	0,05
4. Бельтинг	м	0,02	12,0	7-62	0,10
5. Фильтровальная бумага	кг	0,02	12,0	3-00	0,04
6. Оберточная бумага	кг	0,02	12,0	7-60	0,10
7. Полиэтилен	кг	0,007	4,2	6-20	0,03
8. Ящики	шт	0,05	30	10-00	0,80
9. Прочие материалы					0,04
10. Гвозди		0,001	0,62		0,01
ВСЕГО:					1,29

11. Коробки литографические	ТЫС. ШТ	220,0	1100,0	70-00	77,0
12. Вкладыши	ТЫС. ШТ	220,0	1100,0	20-00	22,0
13. Инструкции	ТЫС. ШТ	220,0	1100,0	16-00	17,6
14. Мелни	ШТ	40,0	400,0	5-00	2,0
15. Кролики	ШТ	25,0	250,0	50-00	12,5
16. Ящики	ШТ	100,0	1000,0	10-00	10,0
17. Гвозди	КГ	0,3	3,0	2-00	0,01
18. Целлофан	КГ	20,0	200,0	40-00	8,0
19. Вата	КГ	0,3	3,0	5-00	0,02
20. Корм животных	КГ				0,6

ВСЕГО:

1256,29

CHAPTER V. LOCATION AND SITE

CONTENTS:

LOCATION

SITE

LOCAL CONDITIONS

LOCATION

The all-state territorial conditions in Mongolia for the selection of a locality suitable for the development of biochemical production for the pharmaceutical industry issue from an exploration of the whole territory. Principially such a locality must have sufficient sources of raw materials in the form of slaughterhouse offal. In Mongolia three slaughterhouse plants are operating at present. The largest of them is located in the capital city Ulan Bator. Therefore the decision was made, in the all-national interest as well as in accordance with the plant operation economy, to build up an integrated biochemical works in this locality. The largest raw material source as well as technologically and technically skilled personnel are available on the spot. The general infrastructure is advantageous /labourers, lodging facilities, social funds/, and the connection with the urban agglomeration is immediate. The distance between the biochemical integrated works and the slaughterhouse plant is about 1 kilometer, and communication interconnexion will be ensured by a city roadway.

SITE

The projected biochemical pilot plant will be a part of the planned biochemical integrated plant in Ulan Bator. The Mongolian party had prepared 5 building lots for selection. Upon the expert team's recommendation a lot in the west part of the city was selected. According to the master extension plan the territory concerned lies within a future industrial zone. The Mongolian party offers the lot cost-free.

The lot concerned has the following advantages:

- I. from the transportation aspect, a possibility of connexion with the city roadway network and rail-road;
- II. a favourable localization near the main raw material basis;
- III. a possibility of immediate connection with
 - steam pipeline
 - electricity mains
 - water mains
 - sewage network.

The remaining 4 lots were found unsuitable, mainly because of complications with the connexions with energy sources or of a too great distance from the raw material basis, or because in one of the alternative lots several older buildings would have to be demolished.

The general conception of the building lot selection was elaborated and consulted with participation of the Office of the Chief Architect of the City of Ulan Bator. The experts and the Chief Architect reached principal agreement in the lot selection, and the Office handed over the necessary maps and plans to the experts.

The selected building lot is plane, its subsoil consists of compact gravel sand. In the western direction it neighbours on a new heating plant No. 4 under construction. On the northern side connections are possible with the city communication, steam pipeline, and electricity main. The southern part of the lot offers connections with a railroad siding and with the city water main. The eastern side is reserved for extension of other industrial plants. The Mongolian party was advised to carry out without delay hydrogeological exploration, planimetric and altimetric measurements, inclusive of fixing the supply and sewage networks for intended connections. From the infrastructural aspect the selected lot is well provided for. It is practically a part of well-equipped city with mass transportation facilities, and with developing housing facilities and social security. Infrastructural costs, at least in connection with the projected pilot plant, are not envisaged. The socio-economical environment is in agreement with the expected development and controlled by several planning systems. Private interests

in the lot are nonexistent; the lot's proprietor is the state. This chapter is complemented by schemes of the whole state territory /Fig. I/ with demarcation of the locality concerned, and of the topographical situation in the city proper /Fig.II/.

LOCAL CONDITIONS

The climate is of the mountain type. Ulan Bator has an altitude about 1 300 m above the sea level. Accordingly, the air temperatures range from +35 °C to -40 °C. The winter season practically preponderates during 2/3 of the year. The atmospheric relative humidity averages 30 to 60 per cent; these minor values are determined by the rain- and snowfall values in the given territory, amounting to 300 mm/year. It is mainly a minor snowfall. Extreme rain- or snowfall is rare and does not occur currently. Western wind flow preponderates. Maximum wind velocity of 80--90 km/h is exceptional. Owing to the terrain structure in Mongolia, dust-laden winds occur. The spring thaw raises the river level in Ulan Bator to a maximum. The city is protected against the high water by an earth dam system. Earthquake forces reach maximally 3--4 degrees, Richter scale.

ESTIMATE OF INVESTMENT COST : LAND

ESTIMATE OF INVESTMENT COST : LAND							
LAND							
			ITEM DESCRIPTION	UNIT COST	COST		
					FOREIGN	LOCAL	TOTAL
			THE INVESTMENTS ARE PLANNED AND ORGANIZED BY THE GOVERNMENT OF MONGOLIA. THE SITE IS STATE PROPERTY, THEREFORE IT IS WITHOUT CHARGE.				

/INSERT TOTAL IN SCHEDULE 10-1/1

ESTIMATE OF PRODUCTION COST : LAND

ESTIMATE OF PRODUCTION COST

LAND

ITEM DESCRIPTION	UNIT COST	COST		
		FOREIGN	LOCAL	TOTAL
<p>THE INVESTMENTS ARE PLANNED AND ORGANIZED BY THE GOVERNMENT OF MONGOLIA. THE SITE IS STATE PROPERTY, THEREFORE IT IS WITHOUT CHARGE.</p>				

/INSERT TOTAL IN SCHEDULE 7/

11250
(2 of 3)

CHAPTER VI. PROJECT ENGINEERING

CONTENTS :

PROJECT LAYOUTS

SCOPE OF PROJECT

TECHNOLOGY /IES/

EQUIPMENT

CIVIL ENGINEERING WORKS

PROJECT LAYOUTS

The pilot plant for the future biochemical integrated works is designed with a view to comply with the requirements of

- the production plan
- the material supply plan
- the technological processes proposed
- the optimal technological equipment, which should have an universal character
- the local conditions
- the building process
- the production programmes envisaged in the future

The whole complex of these aspects is taken into account in the layout plan, considering the entire pilot plant as a self-contained entity. It is presumed that the pilot plant will be realized in advance, and therefore the following separate services and facilities are planned for it:

- raw material supply
- storage service
- energy supply
- water supply
- social premises
- quality control laboratories
- administration service

The machinery and technological equipment proper is of a fairly universal character and expedient for the proposed production programme. The planned pilot plant in fact is a link between the research and the production. This idea is also inherent in the prospective master plan, whose draft outline is documented in the present report, too, although its elaboration had not been imposed to the expert group.

The layout plan of the pilot plant is actually governed by the characters of its parts, namely,

- biochemical production
- pharmaceutical manufacture
- quality control laboratories.

The general design presumes that the biochemical part will be provided with machinery and equipment with preponderantly downward-motion /gravity/ flow.

The biochemical section also will represent the entry for solid and liquid raw materials, and the entrance and exit centre of energies. In this section the final product is a substance, which either is a marketable final product

or is sent to the pharmaceutical section for further processing. In the pharmaceutical section the substances produced in the biochemical section are processed to sterile substances or compressed to tablets, and these products are

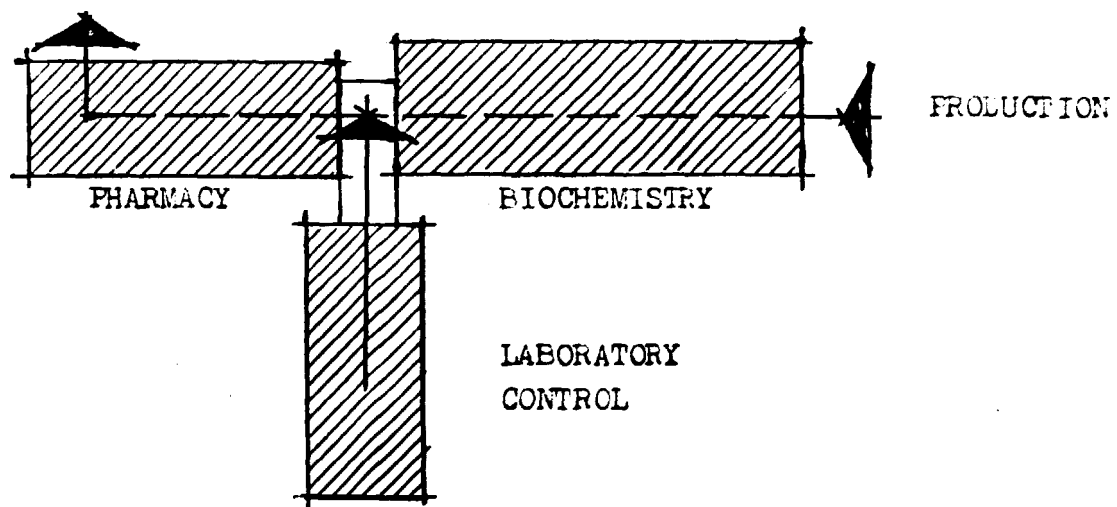
filled into containers and packaged. In the pharmaceutical part the storage services serve the needs of the dispensing form production; mainly packaging materials and constituents are stored here.

The forwarding department is the terminus of the products.

To ensure good manufacturing practice at both production sections and the required quality of the final products, the quality control unit must operate. This unit provides complete laboratory services. By acceptance, in-process, and final controls it ensures that the final products meet the pharmacopoeial specifications.

In the laboratory section suitable rooms are provided for the administration, central social premises, and maintenance.

From the following scheme it is evident that the several sections have separate premises serving their specific operations, but all three sections are integrated to a functional unit with mutual interconnexions.



The horizontal interconnexion of all three sections is given by the uniform line of floors. The vertical interconnexion is ensured by suitably localized lifts /hoists/ and staircases. The overall layout documents are enclosed in a separate back envelope at the end of the present report.

The main technological premise B-109--Biochemical pilot plant is a three-floor building with the ground dimensions 55m x 16m. At the ± 0 level there are localized the storerooms, cooled stores, energy machine rooms, transformer room 35/0,4 kV, cooling engine rooms, pump station for the solvent store, and freezing rooms for raw material.

The floor + 4,20 as well as the floor + 9,00 are adapted for biochemical operations, mainly in the form of halls. These technological operation rooms are complemented with cooling boxes, air conditioning station, auxiliary storeroom, and water demineralization plant.

The premise B-110 Pharmaceutical pilot plant, with the ground dimensions 43m x 13m, is a two-floor building. At the ± 0 level there are localized the storerooms for packaging material, glassware, chemicals, intermediate products, and final products. The forwarding department also is an integral part.

The B-111 Laboratory part is a multipurpose three-floor building with the ground dimensions 43m x 16m. The ± 0 level houses central social premises for men and for women, maintenance shops, storerooms for small materials, and the neutralization plant, which will liquidate chemical waste waters from both the biochemical section and the laboratories.

The floor + 4.20 contains quality control laboratories, ensuring the clearance of products from the biochemical

section either to the store of final products or to further processing in the pharmaceutical section, and from the pharmaceutical section to the store of final products. Complementary components to the laboratories are certain operation rooms at the + 8.40 floor, where the remaining rooms serve various other purposes: offices of the pilot plant head and the laboratory head, studies, library, and administration rooms.

Provisionally also a small canteen with a kitchen are localized there; they will be vacated after construction of a works canteen facility.

SCOPE OF PROJECT

- A - 14 Neutralization plant
- A - 15 Store for inflammable solvents
- A - 16 Central pressure air production
- A - 17 Cooling plant
- A - 18 Transformer station 35/0.4 kV
- A - 19 Air conditioning station
- A - 20 Maintenance shops
- A - 21 In-process transportation

Building part

- B - 101 Preparation of the land for buildings
- B - 102 Outside connections of electricity 35/0.4 kV
- B - 103 Outside connections of water supply
- B - 104 Outside connections of low voltage electricity
- B - 105 Outside connections of steam /pipe lines/
- B - 106 Outside connections to city sewerage
- B - 107 Roadways
- B - 108 Store for liquid material
- B - 109 Biochemical pilot plant
- B - 110 Pharmaceutical pilot plant
- B - 111 Quality control and social premises.

Documentation completely elucidating the expert group's designs

- Fig. I Central Asian area with outline of Mongolia and localization of Ulan Bator /1 : 15 000 000/
- Fig. II Detail of localization of Ulan Bator with outline of site provided for biochemical integrated works /1 : 10 000/
- Fig. III Scheme of general plan of site coverage and localization of pilot plant /1 : 1 000/
- Fig. IV Pilot plant - ground floor ± 0
- Fig. V Pilot plant - floor + 4.20m
- Fig. VI Pilot plant - floor + 8.40m /9.00m/
- Fig. VII Sectional view I-I'
- Fig. VIII Sectional view II-II'

The documents Fig. I - VIII are contained in attached back envelope.

The documents Fig. IX - XVII are inserted in the part VI -
- TECHNOLOGY in the appropriate places, as follows.

Fig. IX	block chart, A - 01	Production of peptone
Fig. X	block chart, A - 02	Production of pepsin
Fig. XI	block chart, A - 03	Production of trypsin chymotrypsin pancypsin
Fig. XII	block chart, A - 04	Production of cholesterol
Fig. XIII	block chart, A - 05	Production of pancreatin
Fig. XIV	block chart, A - 06	Production of blood hydrolysate
Fig. XV	block chart, A - 07	Production of dried bile
Fig. XVI	block chart, A - 08	Manufacture of tablets
Fig. XVII	block chart, A - 09	Manufacture of sterile sub- stances
Fig. XVIII	flow chart, A - 01	Production of peptone
Fig. XIX	flow chart, A - 02	Production of pepsin
Fig. XX	flow chart, A - 03	Production of trypsin chymotrypsin pancypsin
Fig. XXI	flow chart, A - 04	Production of cholesterol
Fig. XXII	flow chart, A - 05	Production of pancreatin
Fig. XXIII	flow chart, A - 06	Production of blood hydrolysate
Fig. XXIV	flow sheet A - 07	Production of dried bile
Fig. XXV	flow sheet A - 11	Solvent recovery plant

- Fig. XXVI flow sheet, A - 12 Water demineralization
- Fig. XXVII flow sheet, A - 13 Engine room for steam,
condensate, and hot water
production
- Fig. XXVIII flow sheet, A - 14 Neutralization plant
- Fig. XXIX flow sheet, A - 15 Store for inflammable solvents
- Fig. XXX flow sheet, A - 16 Central pressure air production

The documents Fig. XVIII - XXX are contained in attached back envelope.

TECHNOLOGY /IES/

A - 01 Production of peptone

In the reservoir 8, calcium hydroxide solution /lime milk/ is prepared. The raw material /paunch and ventricle/ is minced in the mincing machine 10 and transferred into the reactor 1 a-d. The presumed charge size is 300 kg into one jacketed kettle. Previously minced activated pancreas is added to the raw material, and the mixture is stirred for about 7 hours, with occasional additions of lime milk. Then the acidity of the mixture is adjusted with phosphoric acid, and the solid fraction is separated in the centrifuge 2 a/b/. The waste pulp is usable in the mixture as fertilizer. The filtrate is collected in the reservoirs 3 a/b/, from which it is pumped into the film evaporator 4, where it is concentrated to 1/20 of the original volume. This liquid is collected in the jacketed kettle 5 a/b/, in which it is diluted with an equal volume of demineralized water. This solution is filtered through the plate filter 6 into the reservoir 9. From this reservoir it is pumped into the spray drier 7, which yields 141 kg of product per day.

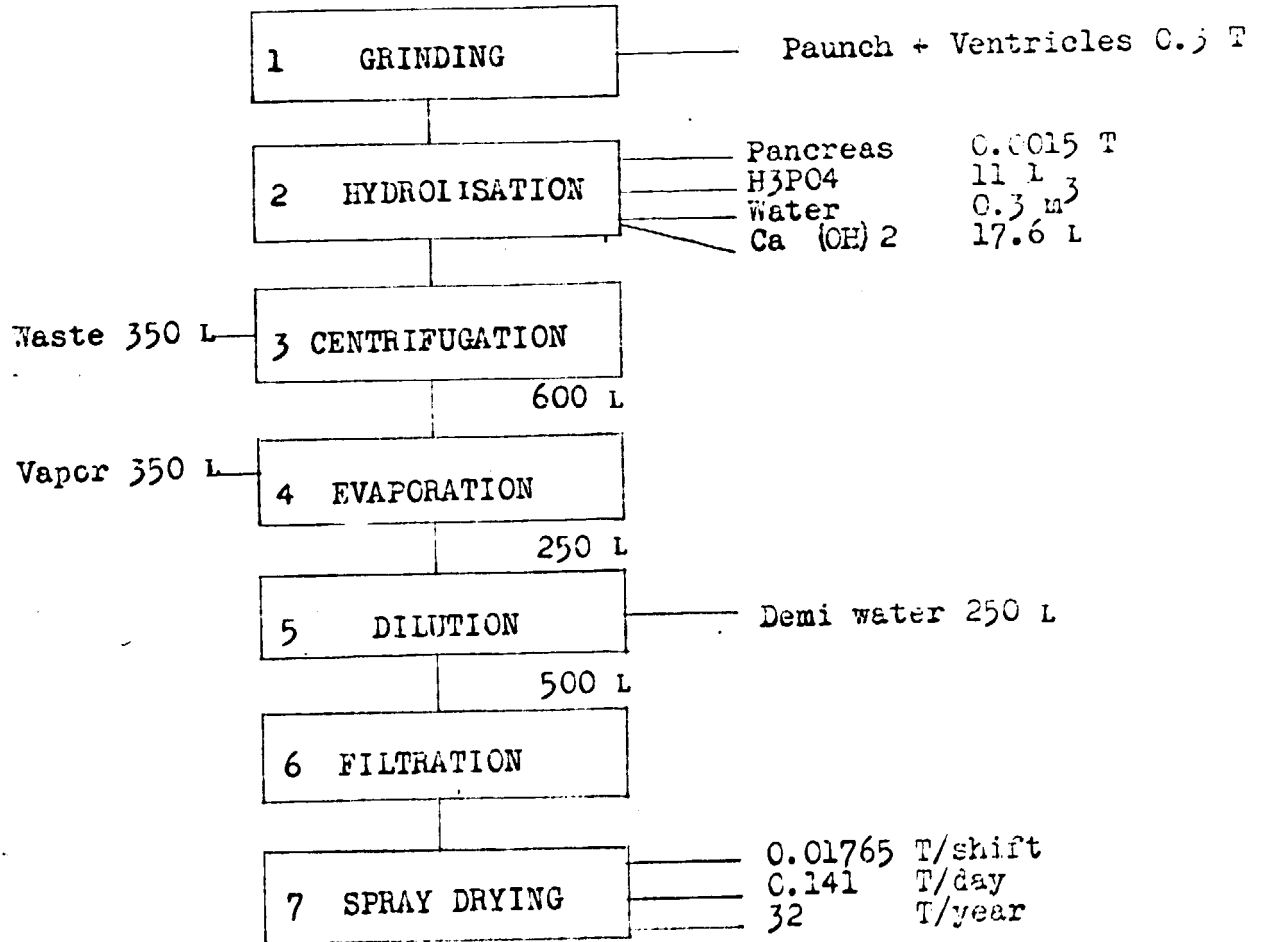
For export purposes the product must comply with quality demands of the United States Pharmacopeia XX /USP XX/, National Formulary XV.

The basic in-process controls: the solution before drying must have pH 5,5-6,5 and must be clear.

A - 01 PRODUCTION OF PEPTON E

FIG. IX

<u>Max. Energy Input/H</u>		<u>Raw material / shift / 8shifts per day/</u>	
Steam	0.48 T/H	Paunch and Ventracles	0.5 T
Electricity	56 kWh	H ₃ PO ₄	11 L
Cooling water	8 m ³ /H	Ca (OH) 2	17.6 L



Wastes/day

Solid	0.35 T
Water	350 L

A - 02 Production of pepsin

100 kg of raw material /hog gastric mucosa or ox tripe/ is minced in the mincing machine 1 and transferred into the autolyzation kettle 2a - 2c. Hydrochloric acid is added and the mixture is autolyzed for 48 hours at 40 °C. The kettle jacket is heated with hot water heated in the boiler 9 and circulated with the aid of a pump. The autolyzed kettle content is let out through the sieve 4 a /b/ into the reservoir 5 a /b/, in which the product is purified and precipitated. With respect to the sort of the product, ethanol or sodium chloride serve as precipitants. The precipitate is collected on the vacuum filter 6 and dried on trays in the drier 7. Ethanol is recuperated for repeated use /equipment A-11/.

The dried product is pulverized in the grinder 9 and put through the sieving machine 8.

About 2,-kg of medicinal pepsin, or 5,-kg of industrial pepsin is produced from 100,-kg of raw material.

For export purposes the medicinal pepsin must fall in quality demands of Food Chemical Codex /FCC/ - USA, with proteolytic activity 3000-3.500 USP units.

A-C2 PRODUCTION OF PEPSIN

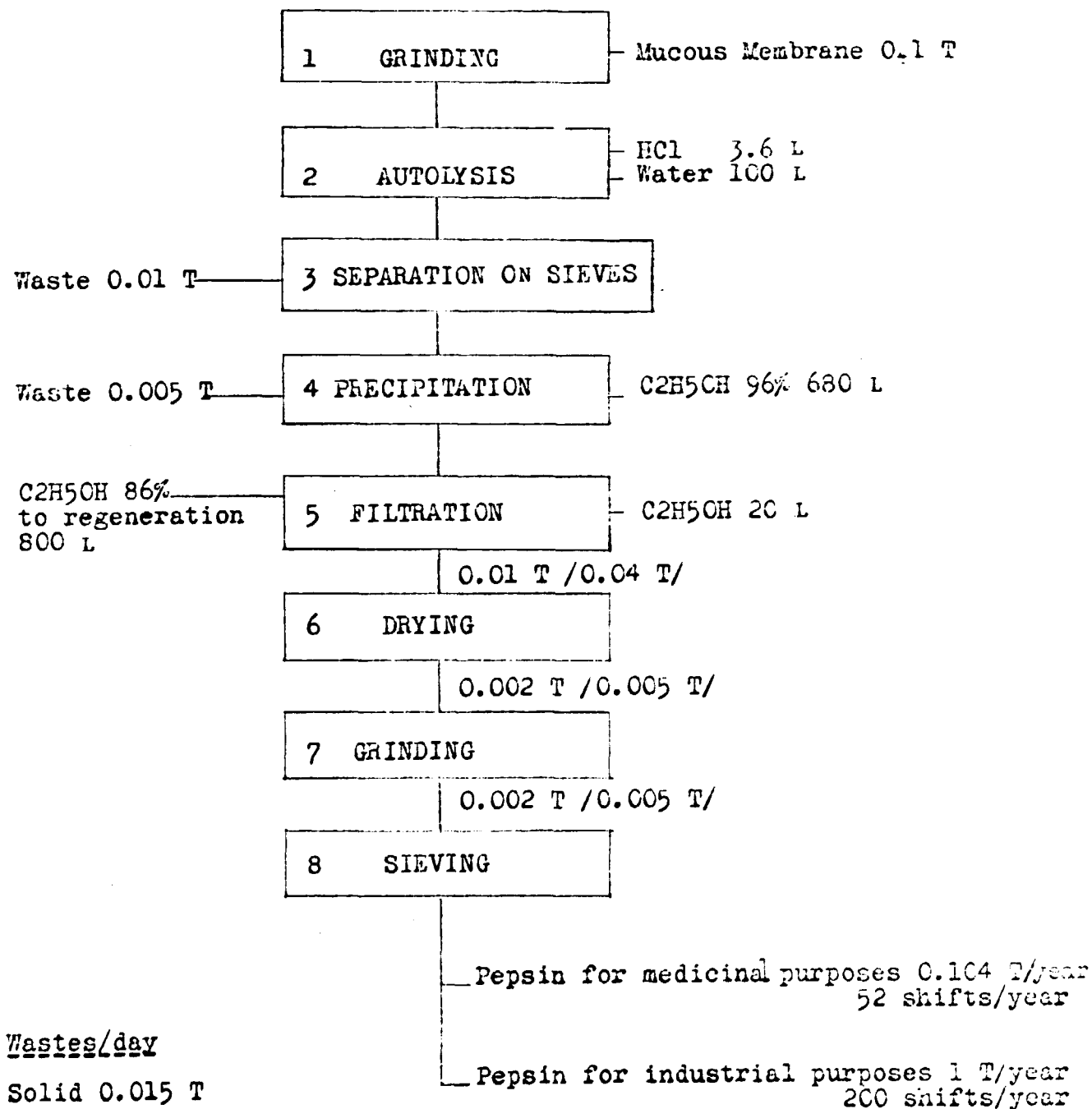
FIG. X

CHAPTER VI

PAGE 18

1. Medicinal
2. Industrial

<u>Max. Energy Input/H</u>		<u>Raw material shift/day</u>	
Steam	0.05 T/H	Mucous membrane	0.1 T
Electricity	10 kWh	HCl	3.6 L
Cooling water	0.5 m ³ /H	C ₂ H ₅ OH 96%	700 L



A - 03 Production of trypsin, chymotrypsin, and pancypsin

The basic raw material for all three products to be manufactured in the proposed equipment is either beef or mutton pancreas. A charge of 100 kg pancreas is minced in the mincing machine 1 and transferred into the extraction kettle 2. Extraction with water acidified with sulphuric acid proceeds at ordinary temperature /25 °C/ for about 7 hours. After its completion the mixture is put through the sieve 3, and the pulp retained on the sieve is pressed out in the press 4. The extract is collected in the reservoir 5, and the product is salted out with ammonium sulphate. The precipitate is collected on the stainless-steel filters 6a, 6b. The acid filtrate is piped to the neutralization plant /A-14/, processed there, and piped into the sewage. The retained precipitate is purified on a laboratory scale in a laboratory provided with adequate equipment 7 and a refrigerator box 8.

From 100,-kg of pancreas 0,06 kg of Trypsin and 0,1 kg of Chymotrypsin, or 0,25 kg of Pancypsin is obtained.

For export purposes the products must comply with demands of United States Pharmacopeia XX. The products must have the following proteolytic activity units: Trypsin 2.500 USP units, Chymotrypsin 1.000 USP units and Pancypsin 250 USP units. The products must pass the microbial limit tests.

Necessary in-process controls: The product before lyophilization must show the residue on ingestion max. 2,5%.

A-03 PRODUCTION OF CHYMOTRYPSIN

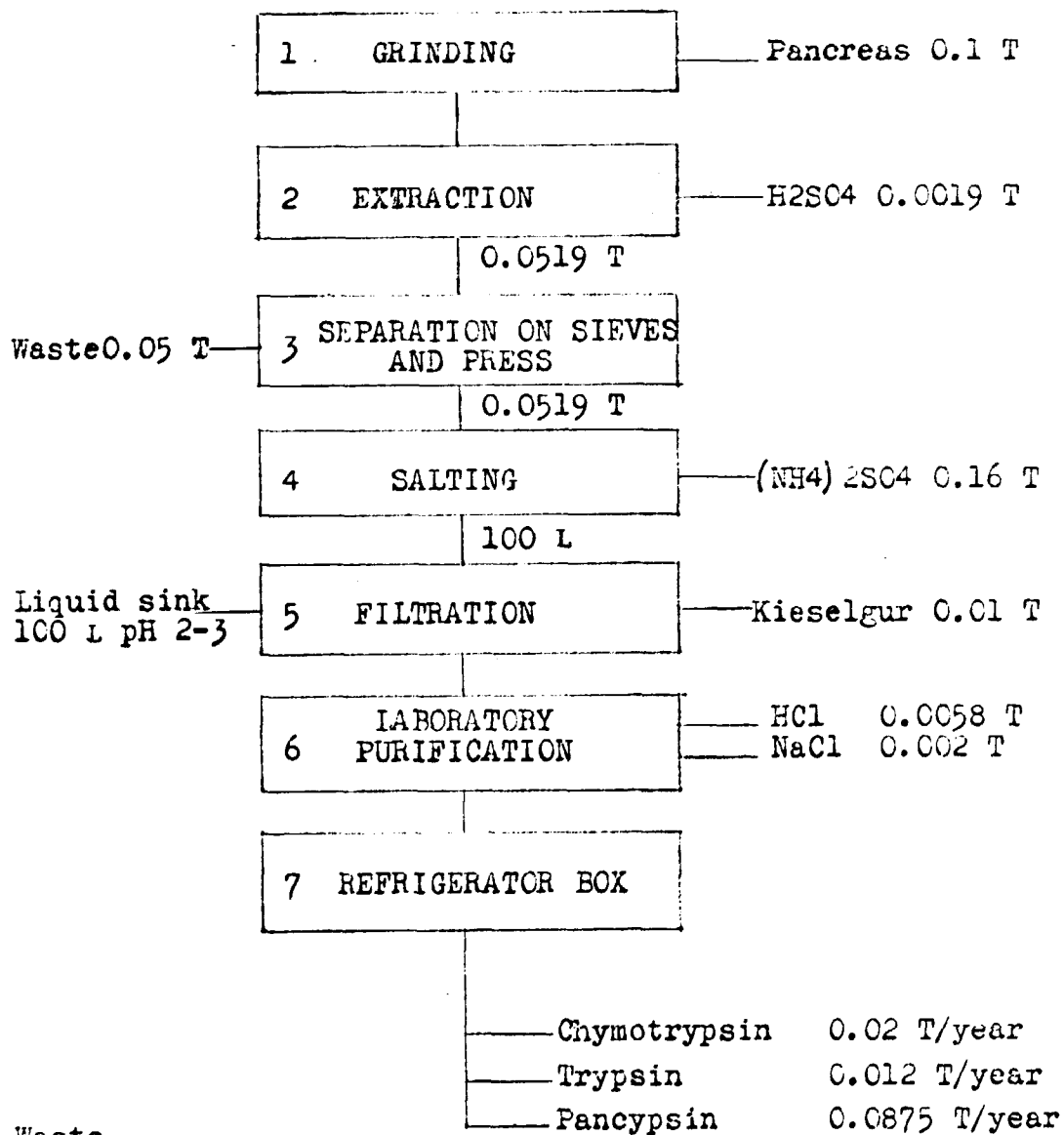
TRYPsin
PANCYPSIN

Max. Energy Input/H

Electricity 8 kWh
Cooling water 0.2 m³/H

Raw material/shift /2shifts/day/

Pancreas 0.1 T
H₂SO₄ 0.019 T
(NH₄)₂SO₄ 0.16 T
Kieselgur 0.01 T
HCl 0.0058 T
NaCl 0.002 T



Waste

Solid 0.05 T
Liquid sink 100 L

A - C4 Production of cholesterol

For the production of cholesterol the basic raw material, beef spine cord, must be first dried. The raw material is minced in the mincing machine 1 and dried on trays in the shelf drier 2. The dried raw material /daily yield about 30 kg/ is stored in the in-process store, whence it is drawn for further processing.

15 kg of dried raw material is transferred to the extraction kettle 3 and extracted with acetone for about 3 hours with stirring and moderate cooling. The mixture is then put through the pressure filter 4. The extracted pulp is waste product. The filtrate is collected in the reservoir 5, from which it is pumped /pump 20/ into the film evaporator 6. The concentrated solution is collected in the kettle 9 and evaporated there to dryness. The intermediate product, pooled from 6 primary operations, is extracted in the kettle 13 with ethanol, with sulphuric acid added, at the boiling point of the extractant mixture, under the reflux cooler 14. The hot extract is put through the monocell filter 15 and collected in the kettle 16, in which crystallization proceeds under water cooling. The product is recrystallized once in the same equipment. The final product is collected on the suction filter 17 and dried in the vacuum shelf drier 18. The dried product is sieved.

From 100,- kg of fresh spinal cord about 3,9 kg of cholesterol is produced.

For export purposes the final product must comply with quality demands of the USP XX., page 146.

In-process controls: The product after recrystallization must show the melting point 147-150 °C and specific rotation -34° to -38°. If this values are not achieved the product must be recrystallized.

The ethanol and acetone used in the operations are regenerated at the plant A-11.

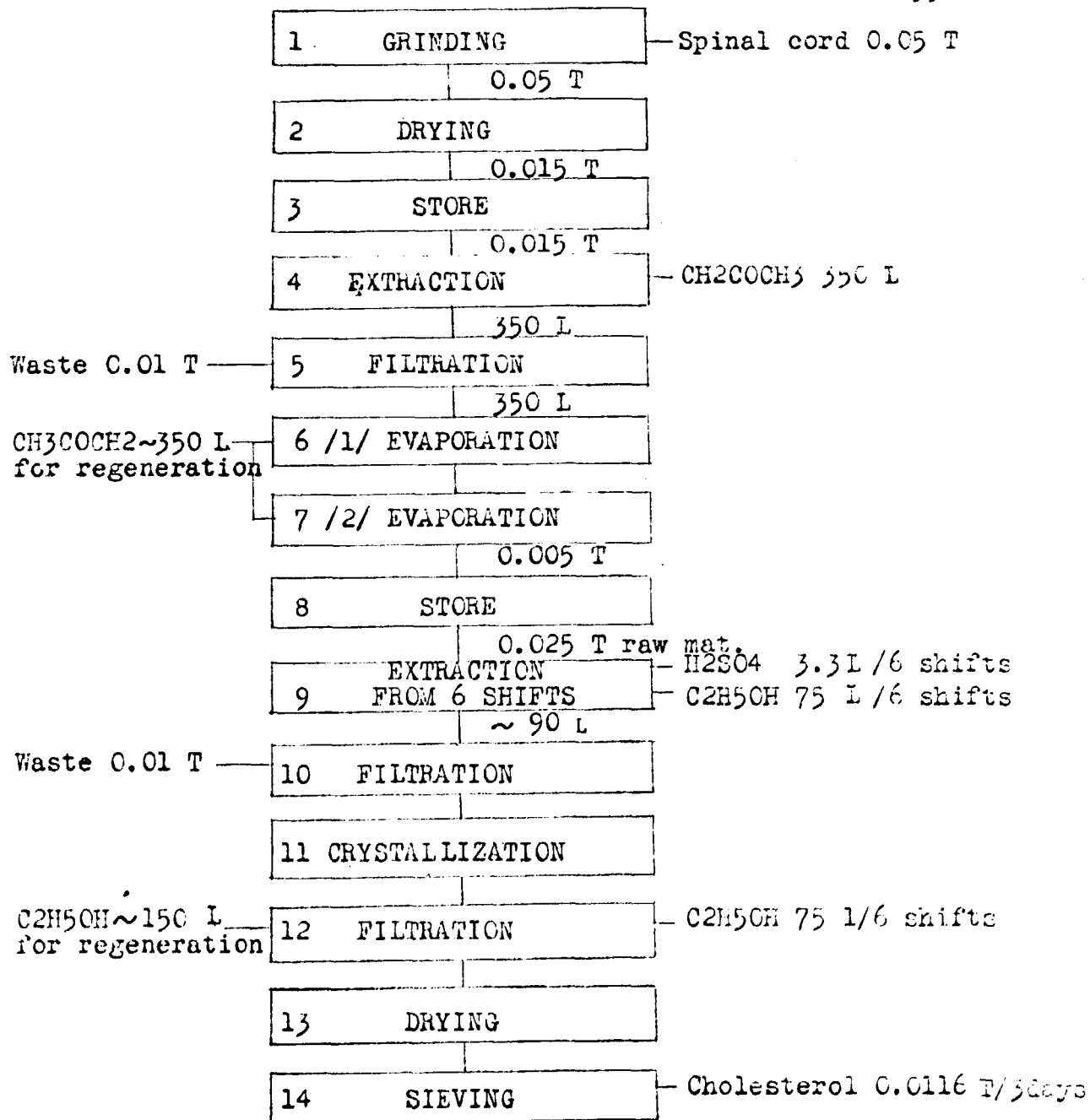
A-04 PRODUCTION OF CHOLESTEROL

FIG. XII

CHAPTER VI

PAGE 22

<u>Max. Energy Input</u>		<u>Raw material/shift /2 shifts/day/</u>	
Steam	0.1 T/H	Spinal cord	0.05 T
Electricity	6 KWH	CH ₃ COCH ₃	350 L
		C ₂ H ₅ OH	25 L
		H ₂ SO ₄	0.55 L



Waste

Solid 0.02 T

A - 05 Production of pancreatin

100,- kg of pancreas is minced in the mincing machine 1 and transferred into the extraction kettle 2, where it is extracted with water for 3 hours at 20 °C. Then the mixture is let out through the sieve 3 and the extract is collected in the reservoir 4 a /b/. The pulp retained on the sieve is usable as feedstuff. From the collected extract pancreatin is precipitated with acetone. The precipitate is collected on the suction filter 5. The wet product is transferred into the kettle 6, slurried with acetone, and collected again on the suction filter 5. The acetone is sent for regeneration to A-11. The final product is dried completely on trays in the shelf drier 7, and 10,- kg of final product is obtained.

Pancreatin for medical purposes must comply with demands of USP XX /page 580/.

The in-process control: Before final grinding the content of fat max. 3%.

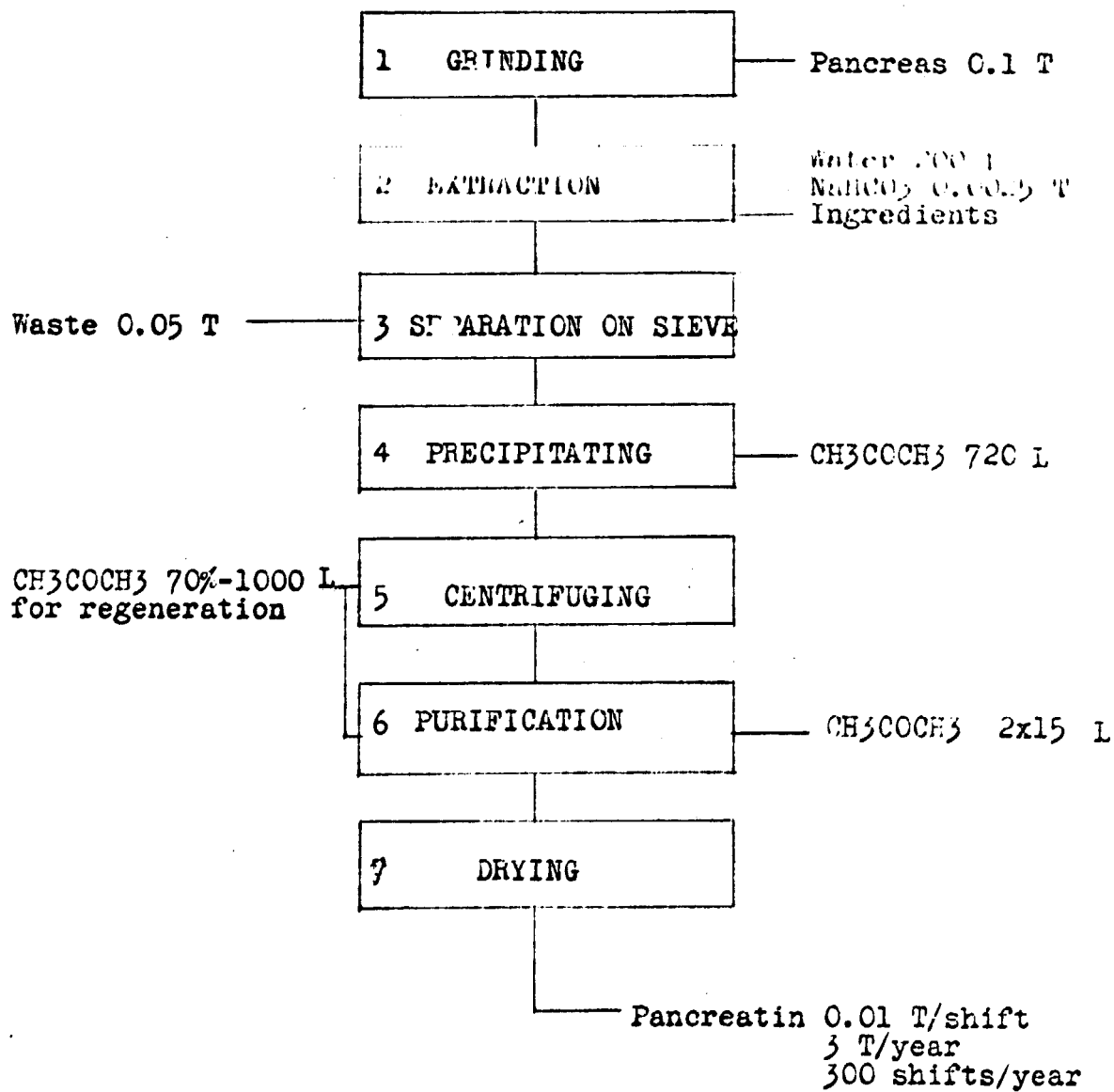
A-05 PRODUCTION OF PANCREATIN

Max Energy Input/H

Steam 0.06 T/H
Electricity 13 kWh

Raw material/shift /2shifts/day/

Pancreas 0.1 T
NaHCO₃ 0.0025 T
CH₃COCH₃ 750 L



Waste

Solid 0.05 T

A - 06 Production of blood hydrolysate

The basic raw material is beef blood. 175 liters blood is transferred into the kettle 1, sulphuric acid is added, and hydrolysis proceeds at 120 °C and the pressure corresponding to the temperature. The hydrolytic process takes 3 hours. Then the mixture is cooled, neutralized with lime milk in the reservoir 2, and filtered through the suction filter 2 into the reservoir 4 provided with a stirrer. Oxalic acid is added, and the supernatant is pumped into the film evaporator 5. The thickened liquid is filtered on a laboratory-scale equipment. The yield of thickened liquid is about 15 liters per day. After filtration it is dried in the spray drier 9. Before drying the filtrate can be stored in a freezing box, which is a part of the laboratory equipment.

16,2 kg of blood hydrolysate is produced daily in 2 shifts.

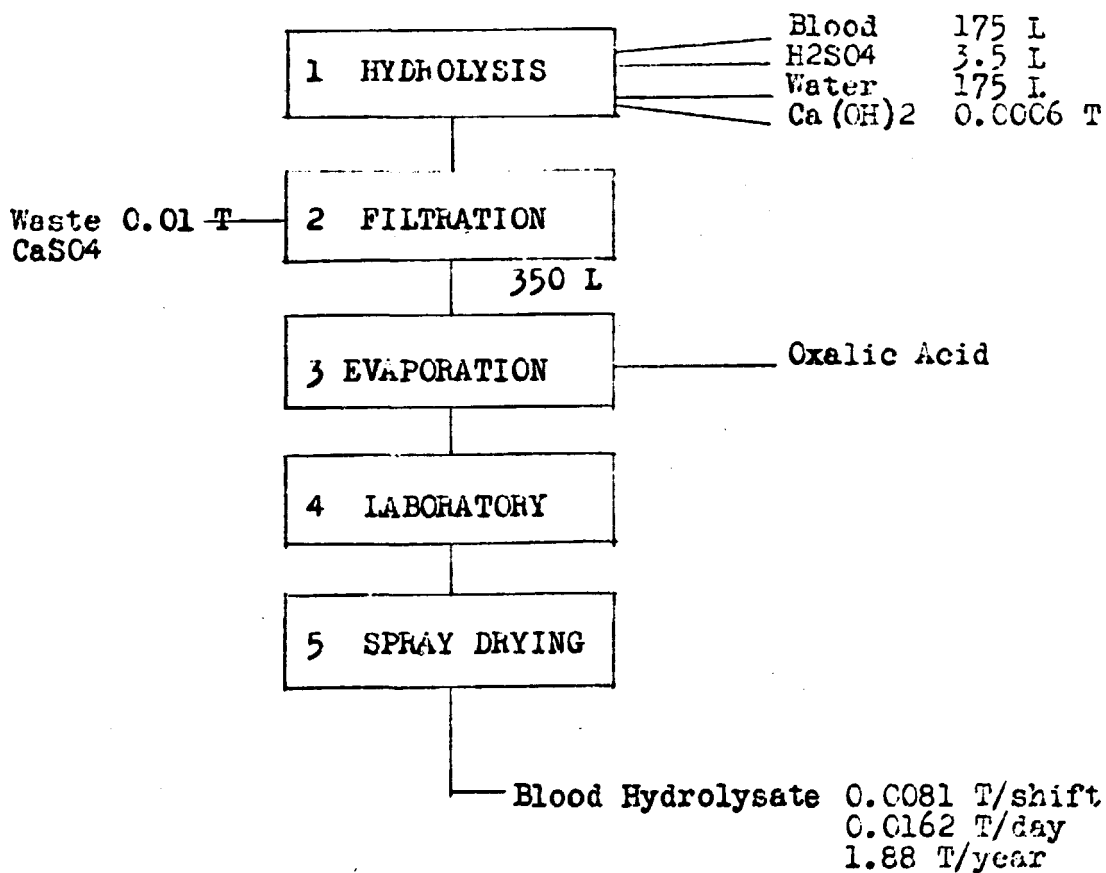
A - 06 PRODUCTION OF BLOOD HYDROLYSATE

Max. Energy Input/H

Steam 0.14 T/H
Electricity 10.5 KWH
Cooling water 1.2 m³/H

Raw material/shift /2 shifts/day/

Blood 175 L
H₂SO₄ 3.5 L
Ca(OH)₂ 0.006 T
Oxalic Acid 0.00015 T



Waste

Solid 0.01 T/shift
Water 320 L/shift

A - 07 Production of dried bile

Owing to the season-conditioned campaign character of the work in the slaughterhouse integrated works, all bile collected must be first thickened to about 1/5 of its original volume, and the thickened intermediate product stored in a freezing box for further yearly processing. 500 kg bile is strained and collected in the reservoir 1; from the reservoir the bile is pumped into the film evaporator 2, where it is thickened to 1/5 of its original volume. The thickened intermediate product can be either stored in a freezing box or directly dried in the spray drier serving also the production of peptone.

From 500,- kg of fresh bile 52,- kg of the final product is obtained.

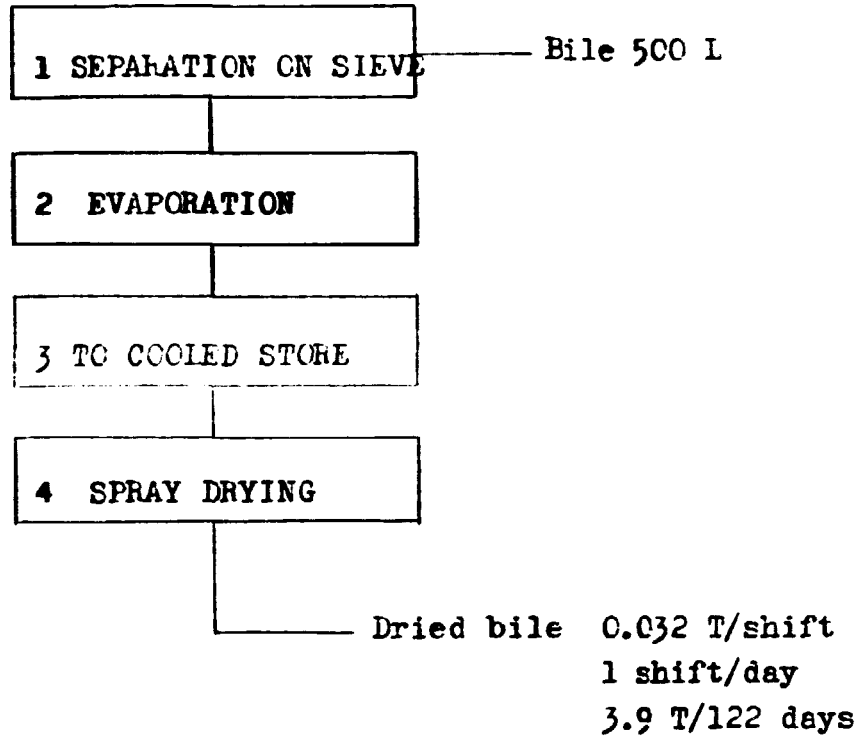
For export of dry bile for medical use the product must comply with demands of National Formulary XI. It must contain min. 40% of cholic acid, and must pass the microbial limit tests.

Max. Energy Input

Steam 0.07 T/H
 Electricity 1.7 kWh
 Cooling water 1 m³/H

Raw material/shift

Bile 0.5 T



Waste

Liquid 400 L

A - CE Manufacture of tablets

The substances produced in the pilot plant will be processed to the tablet form as follows. The substance is moistened and kneaded in the kettle 1 together with the necessary constituents; the mixture is put through the sieve 2 and dried on stainless-steel trays in the dryer 3. The dried mixture is sieved again and pressed to tablets with the tableting machine 4. In some instances the tablets will be film-coated in the film-coating machine 5. The tablets will be filled into containers with the filling machine 6. Labelling and putting into cartons are assumed to be performed manually.

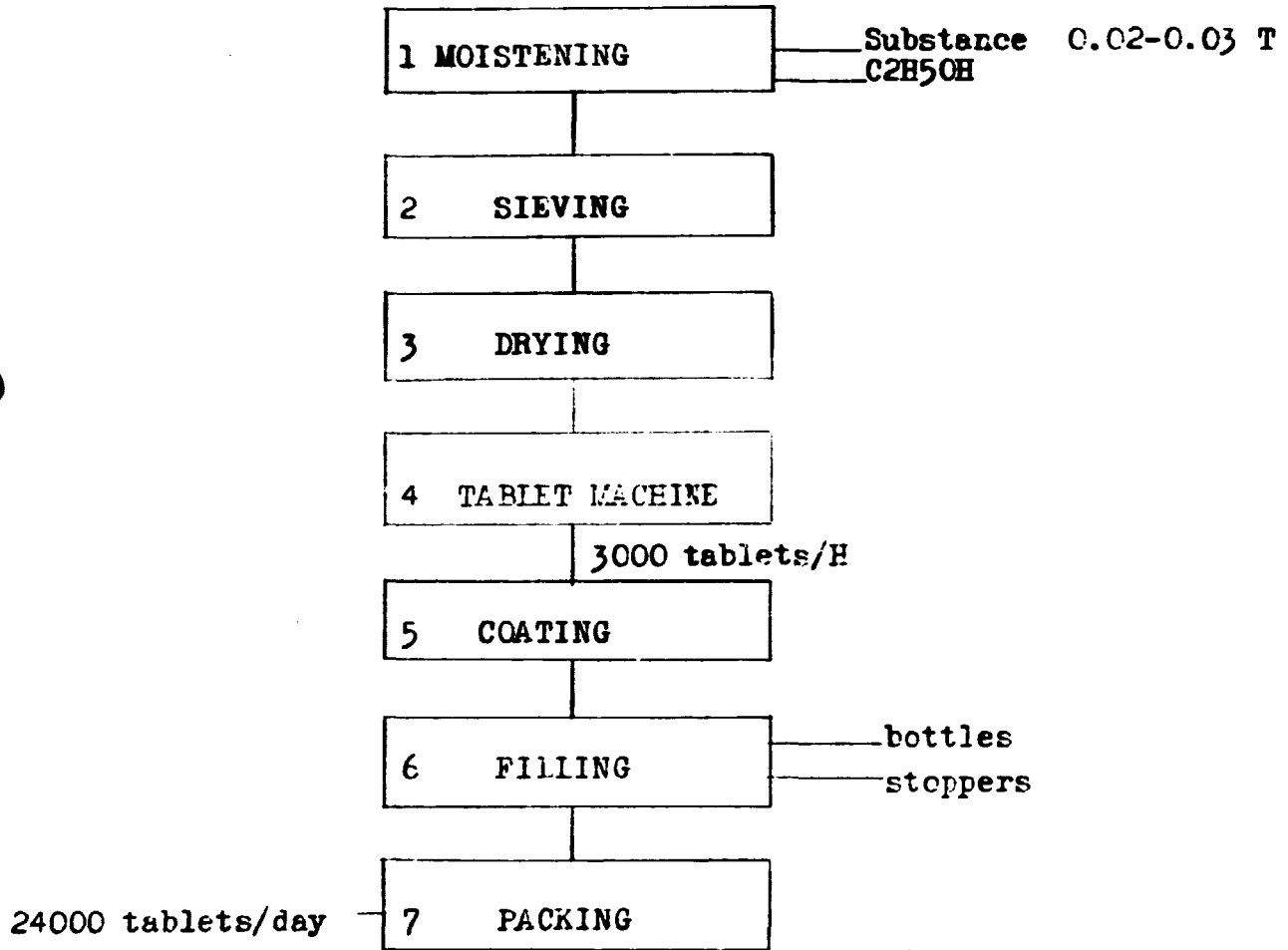
A-08 MANUFACTURE OF TABLETS

Max. Energy Input/H

Raw material/day

Electricity 3 kWh

Substance 0.02 - 0.03 T



A - 09 Manufacture of sterile substances

Some of the products prepared in the chemical departments of the pilot plant will be processed to sterile preparations in the pharmaceutical department.

The substance is dissolved in the kettle . The solution is sterilized by filtration through the Seitz filter . The sterile solution is then filled under sterile conditions with the filling machine , fed with vials and closures presterilized in the double-door autoclave . Filled vials with crimped closures are labelled and packaged in the appropriate rooms of the pharmaceutical department.

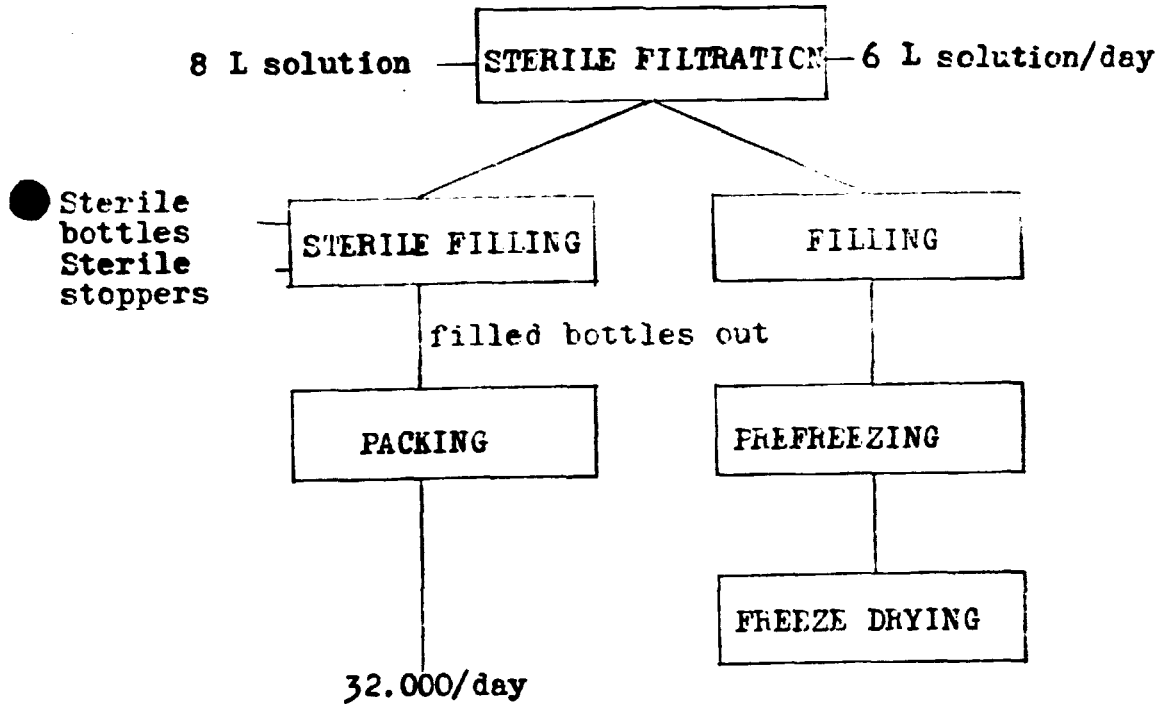
In other instances the sterile solution is filled manually into 100-ml bottles, shell-frozen in the shell-freezing apparatus , and freeze-dried in the existing Leybold plant. For this freeze-drying a reconstruction of the existing freeze-drying plant is envisaged.

Max. Energy Input/H

Raw material

Electricity 13 kWh

Steam 0.05 T



A - 10 Laboratory quality control unit

This unit is intended to provide the laboratory in-process control, firstly, for a part of the production of chemical substances and, secondly, for a part of the pharmaceutical manufacture; and in general, all phases of the technical quality control. To ensure these requirements, use will be made of the existing equipment owned by the laboratories of the Research Institute of the slaughterhouse integrated works in Ulan Bator, which equipment will be moved into the new premises in the pilot-plant building, and new complementary equipment will be provided. The new equipment is specified in the list A-10.

A - 11 Regeneration of ethanol and acetone

For economization of the pilot-plant operation, regeneration of solvents, especially of ethanol and acetone, is envisaged, ie, of solvents used in the technological processes specified before. The capacities of the equipment have been chosen so that the regeneration can be completed during one, maximally two, working shifts. In this way a reserve capacity is available in case of any changes in the production programme. Such changes can be expected in view of the universal character of the proposed pilot plant.

The solvent regeneration plant is technologically connected with the operation unit A-15 Inflammable solvent store, where both the solvents waiting for regeneration and the regenerated solvents are collected.

From the inflammable solvent store the ethanol mixture to be regenerated is pumped to the continuously operating rectification plate column 2, and the acetone mixture to be regenerated to the rectification packed column 5. The solvents to be regenerated are pumped into the feeding reservoirs 1 and 4a. The purified solvents are collected in the reservoirs 3 and 4b and piped back to pure solvent reservoirs placed in the inflammable solvent store. The capacities of the rectification columns are about 200 - 250 liters of regenerated solvent per hour.

A - 12 Preparation of demineralized and of pyrogen-free water

This operation unit ensures the production of demineralized and of pyrogen-free water for the needs of both the pilot-plant laboratories and the production processes.

For the preparation of demineralized water, a standard automatic glass plant 1 is envisaged, with cyclic regeneration of the filling. Its capacity is 200 liters of demineralized water per hour. Demineralized water will be distributed to the consumption sites by gravity.

Pyrogen-free water is distilled from demineralized water pumped by the pump 3 into the jacketed kettle 4. The water vapours escaping from the boiling water are liberated from possible carryover water droplets by their re-overheating in the condenser 5, provided with indirect high-pressure steam heating. Condensed and cooled pyrogen-free water will be collected in the reservoir 7 and distributed to the consumption sites by gravity.

A - 13 Steam and condensate station

This operation unit provides the pressure reduction of steam, piped from an external source, down to the pressure used in the production operations at the pilot plant. Simultaneously, with the aid of the countercurrent heat exchanger 2 the unit ensures the production of hot water for operational and hygienic purposes. Water heated to 55 °C will be collected in the reservoir 3 and piped from it to the consumption sites. The entire hot-water production process will be controlled automatically.

In the reservoir 1 the condensate will be collected from the production premises and from the heating system of the pilot plant premises, and automatically pumped with the pump 4 back to the heat exchanger.

A - 14 Neutralization plant

This plant ensures the neutralization of waste waters from the production and laboratories before their outflow into the sewage system. The whole plant operates automatically. The waste waters flow into the reservoir 1, where their mutual preneutralization proceeds. Then the waters overflow into the reservoir 1b. The contents of both reservoirs are continuously stirred vigorously. With the aid of the pump 4 the waste water in the reservoir 1b is circulated. At the outlet of the pump a pH-meter sensor is placed; the pH-meter governs the dosage of either sulphuric acid from the reservoir 2 or lime milk from the reservoir 3. When the final pH value ranges between 6 and 8, the neutralized waste water is let off into the sewage system. No further purification of this waste water at the pilot plant is envisaged.

A - 15 Inflammable solvent store

The store ensures the storage of used solvents, ie, ethanol and acetone, in the storage tanks 1a, 1c; and the storage of regenerated or fresh ethanol and acetone in the storage tanks 1b,d,e. It ensures the supply of ethanol and acetone to the production premises. Installation of volume meters is envisaged, which will ensure a balance of the received and supplied quantities of the solvents.

The storage is localized underground and the storage tanks are covered with earth, and thus the unit meets the safety regulations for the storage of 1st-class inflammables.

A - 16 Vacuum and pressure-air central station

For providing central vacuum for the production premises and laboratories, two wet air pumps with circulation tanks 3a, 3b will be installed.

For production of pressure air for the operation, transportation, measuring, and regulation, two compressors 1a, 1b, with a pressure tank 2, and a silica-gel drying unit 3 will be installed.

A - 17 Cooling plant

A - 18 Transformer station 35/0,4 kV

A - 19 Air conditioning station

A - 20 Maintenance shops

A - 21 In-process transportation

EQUIPMENT

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST							
EQUIPMENT							
PROJECT COMPONENT		No.A-01 DESCRIPTION - PRODUCTION OF PEPTONE					
	PIECES	ITEM DESCRIPTION	UNIT COST	COST			TOTAL
				FOREIGN US DOLLARS	LOCAL Tg	TOTAL Tg	
1	4	REACTOR, 1000 L, ENAMELLED	6000,-	24 000,-		81 120,-	
2	2	CENTRIFUGE, DIAM. 1000mm, AKV STEEL	6800,-	13 600,-		45 970,-	
3	2	RESERVOIR, 1000 L	4500,-	9 000,-		30 420,-	
4	1	FILM EVAPORATOR, 350L/H, AKV STEEL	17400,-	17 400,-		58 810,-	
5	2	KETTLE-JACKETED, 630L, ENAMELLED	5700,-	11 400,-		38 530,-	
6	1	PLATE FILTER	1200,-	1 200,-		4 060,-	
7	1	SPRAY DRIER, 30L/H, AKV STEEL	133200,-	133 200,-		450 210,-	
8	2	RESERVOIR, 630L, STEEL	450,-	900,-		3 040,-	
9	1	MEAT MINCING MACHINE	4500,-	4 500,-		15 210,-	
10	1	RESERVOIR, 300L, AKV STEEL	2400,-	2 400,-		8 110,-	
11	2	PUMPS	250,-	500,-		1 690,-	
12		PIPING AND FITTINGS		11 300,-		38 190,-	
13		ELECTRICITY WIRING- COMMERCIAL SUPPLY		2 300,-		7 770,-	
14		MEASURING AND REGU- LATION - COMMERCIAL SUPPLY		1 500,-		5 070,-	
TOTAL				233 200,-		788.200,-	

CARRY OVER TOTAL OF PROJECT COMPONENT TO CHAPTER VI

SCHEDULE 6-2/2

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST							
EQUIPMENT							
PROJECT COMPONENT No.A-02 DESCRIPTION - PRODUCTION OF PEPSIN							
	PIECES	ITEM DESCRIPTION	UNIT COST	COST			TOTAL
				FOREIGN	LOCAL	TOTAL	
			US\$	US\$	Rs	Tg	Tg
1	1	MEAT MINCING MACHINE	2300,-	2 300,-			7 770,-
2	3	KETTLE-JACKETED, 300L, ENAMELLED	4000,-	12 000,-			40 560,-
3	1	MEASURING VESSEL, STEEL	200,-	200,-			680,-
4	2	SIEVE	200,-	400,-			1 350,-
5	2	RESERVOIR, 1000L, ENAMELLED	450,-	900,-			3 040,-
6	1	VAKUUM FILTER, DIAM. 600mm, ENAMELLED	4100,-	4 100,-			13 860,-
7	1	TRAY DRIER	10600,-	10 600,-			35 830,-
8	1	SIEVING MACHINE	4900,-	4 900,-			16 560,-
9	1	BOILER	800,-	800,-			2 700,-
10		PIPING AND FITTINGS		4 900,-			16 560,-
11		ELECTRICITY WIRING - COMMERCIAL SUPPLY		1 500,-			5 070,-
12		MEASURING AND REGULATION-COMMERCIAL SUPPLY		800,-			2 700,-
TOTAL				43,400,-			146.680,-

CARRY OVER TOTAL OF PROJECT COMPONENT No. A-02

PROJECT COMPONENT No. A-03 DESCRIPTION-PROJECT COMPONENT

QTY	UNIT	ITEM DESCRIPTION	UNIT COST		TOTAL
			US Dollars	Tg	
1	2	PETTIE, JACKETED, 500L, ENAMELED	6300,-	12 600,-	42 590,-
2	1	SIEVE	200,-	200,-	680,-
3	1	PLATE	200,-	200,-	680,-
4	1	CHURN, ENAMELED	8300,-	8 300,-	28 000,-
5	4	VACUUM FILTER, 25" STEEL	1200,-	4 800,-	16 220,-
6	1	REFRIGERATOR BOX	4500,-	4 500,-	15 210,-
7		PIPING AND FITTINGS		2 500,-	7 970,-
8		ELECTRICITY WIRING- COMMERCIAL SUPPLY		900,-	3 040,-
9		MEASURING AND REGU- LATION-COMMERCIAL SUPPLY		400,-	1 300,-
TOTAL			34,200,-		115.590,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET / SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No.A-04 DESCRIPTION - PRODUCTION OF CHOLESTEROL						
	PIECES	ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US Dollars	LOCAL ₹	TOTAL ₹
1	1	SHELF DRIER	10600,-	10 600,-		35 830,-
2	1	KETTLE, JACKETED, 500L, ENAMELLED	6300,-	6 300,-		21 290,-
3	1	PRESSURE FILTER, DIAM. 600mm, ENAMELLED	5300,-	5 300,-		17 910,-
4	1	RESERVOIR, 630L, AKV STEEL	4500,-	4 500,-		15 210,-
5	1	FILM EVAPORATOR, 120L/H AKV STEEL	15100,-	15 100,-		51 040,-
6	1	CONDENSER, 4m ² , AKV STEEL	1800,-	1 800,-		6 080,-
7	2	RESERVOIR, 150L, AKV STEEL	1150,-	2 300,-		7 770,-
8	1	KETTLE, JACKETED, 100L, AKV STEEL	3600,-	3 600,-		12 170,-
9	1	COOLER, 1m ² , AKV STEEL	800,-	800,-		2 700,-
10	1	RESERVOIR, 100L, GLASS	200,-	200,-		680,-
11	1	MEASURING VESSEL 200L AKV STEEL	1400,-	1 400,-		4 730,-
12	1	KETTLE, JACKETED, 160L, ENAMELLED	3900,-	3 900,-		13 180,-
13	1	MONOCELL FILTER, DIAM. 800mm, ENAMELLED	3000,-	3 000,-		10 140,-
14	1	KETTLE, JACKETED, 150L, ENAMELLED	4000,-	4 000,-		13 520,-
15	1	SUCTION FILTER, DIAM. 800mm, STONEWARE	200,-	200,-		680,-
16	1	VACUUM SHELF DRIER, 500L	10600,-	10 600,-		35 830,-
17	1	PUMPS	200,-	200,-		680,-
18		PIPING AND FITTINGS		7 600,-		25 690,-
19		ELECTRICITY WIRING - COMMERCIAL SUPPLY		1 500,-		5 070,-
20		MEASURING AND REGULATION COMMERCIAL SUPPLY		1 100,-		3 720,-
TOTAL				84 000,-		283.920,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SHEET NO. 45

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No.A-05 DESCRIPTION-PRODUCTION OF PARACETAMOL						
	PIECES	ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US Dollars	LOCAL Tg	TOTAL Tg
1	1	MEAT MINCING MACHINE	2300,-	2 300,-		7 770,-
2	1	KETTLE, JACKETED, AKV STEEL	5700,-	5 700,-		19 270,-
3	1	SIEVE, AKV STEEL	200,-	200,-		680,-
4	2	RESERVOIR, 1COOL, WITH STIRRER	1150,-	2 300,-		7 770,-
5	1	SUCTION FILTER	1100,-	1 100,-		3 720,-
6	1	KETTLE, 1COL, WITH STIRRER	200,-	200,-		680,-
7	1	SHELF DRIER, 5COL	10600,-	10 600,-		35 830,-
8		PIPING AND FITTINGS		6 100,-		20 620,-
9		ELECTRICITY WIRING - COMMERCIAL SUPPLY		1 100,-		3 720,-
10		MEASURING AND REGULATION-COMMERCIAL SUPPLY		200,-		680,-
TOTAL				29,800,-		100.740,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No.A-06 DESCRIPTION-				PRODUCTION OF BLOOD HYDROLYSATE		
NO.	PIECES	ITEM DESCRIPTION	UNIT COST	CCST		
				FOREIGN US Dollars	LOCAL Tg	TOTAL Tg
1	1	KETTLE, JACKETED, HOOL, WITH STIRRER, ENAMELLED	6300,-	6 300,-		21 290,-
2	1	SUCTION FILTER, DIAM. 600mm, AKV STEEL	900,-	900,-		3 040,-
3	1	MEASURING VESSEL, 50L, GLASS	100,-	100,-		340,-
4	1	RESERVOIR, 400/L, WITE STIRREB, AKV STEEL	3800,-	3 800,-		12 840,-
5	1	FILM EVAPORATOR, 92L/H AKV STEEL	15100,-	15 100,-		51 040,-
6	1	COOLER, 2m ² , AKV STEEL	1100,-	1 100,-		3 720,-
7	2	RESERVOIRS, 1COL, GLASS	250,-	500,-		1 690,-
8	1	FREEZING BOX	6800,-	6 800,-		22 980,-
9	1	PUMP	200,-	200,-		680,-
10		PIPING AND FITTINGS		3 000,-		10 140,-
11		ELECTRICITY WIRING - COMMERCIAL SUPPLY		800,-		2 700,-
12		MEASURING AND REGULATION-COMMERCIAL SUPPLY		200,-		680,-
TOTAL				38.800,-		131.140,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No.A-07 DESCRIPTION-PRODUCTION OF DRIED BILE						
	PIECES	ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US\$	LOCAL Tg	TOTAL Tg
1	1	RESERVOIR, 630L, AKV STEEL.	2300,-	2300,-		2300,-
2	1	FILM EVAPORATOR, 92L/H, AKV STEEL	15100,-	15100,-		15100,-
3	1	CONDENSER, 1m ² , AKV STEEL	1100,-	1100,-		1100,-
4	2	RESERVOIRS, 150L	200,-	400,-		400,-
5	1	PUMP	100,-	100,-		100,-
6		PIPING AND FITTINGS		2100,-		2100,-
7		ELECTRICITY WIRING- COMMERCIAL SUPPLY		200,-		200,-
8		MEASURING AND REGU- LATION-COMMERCIAL SUPPLY		200,-		200,-
TOTAL				21.500,-		72.680,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SCHEDULE 6-2/7

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST							
EQUIPMENT							
PROJECT COMPONENT No.A-08 DESCRIPTION -MANUFACTURE OF TABLETS							
	PIECES	ITEM DESCRIPTION	UNIT COST	COST			TOTAL
				FOREIGN US\$	LOCAL ₦	TOTAL ₦	
1	1	KETTLE, 50L, AKV STEEL	500,-	500,-		1 690,-	
2	1	SIEVE, AKV STEEL	50,-	50,-		170,-	
3	1	TRAY DRIER	1700,-	1 700,-		5 750,-	
4	1	TABLETTING MACHINE	12500,-	12 500,-		42 250,-	
5	1	FILM-COATING MACHINE	8500,-	8 500,-		28 730,-	
6	1	FILLING MACHINE	14400,-	14 400,-		48 670,-	
7	1	ELECTRICITY WIRING-COMMERCIAL SUPPLY		3 200,-		10 820,-	
TOTAL				40,850,-		138.080,-	

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No.A-09 DESCRIPTION-MANUFACTURE					OF STERILE PREPARATIONS	
NO	PIECES	ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US\$ Dollars	LOCAL Tg	TOTAL Tg
1	1	STERILIZER FOR CONTAINERS AND UTENSILS	400,-	400,-		1 350,-
2	1	SPITE FILTER	7600,-	7 600,-		25 690,-
3	1	FILLING MACHINE	600,-	600,-		2 830,-
4	1	SHIELD-FREEZING AP- FATUS	800,-	800,-		2 700,-
5	2	RECONSTRUCTION OF EXISTING FREEZE- DRYING PIANT-LEYBOLT	1900,-	3 800,-		12 840,-
6	1	LAMINAR FLOW	15100	15 100,-		51 640,-
7	1	FILLING LINE+CAP CRIMPING LINE	203300,	203 300,-		687 230,-
8	1	DOUBLE-DOOR AUTOCLAVE	1600,-	1 600,-		5 400,-
9	1	TRAY DRIER	1900,-	1 900,-		6 420,-
10		ELECTRICITY WIRING- COMMERCIAL SUPPLY		1 500,-		5 670,-
TOTAL				236.600,-		799.770,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No.A-10 DESCRIPTION-LABORATORY QUALITY CONTROL						
	PIECES	ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US Dollars	LOCAL Tg	TOTAL Tg
1	4	LABORATORY BENCH, WET	380,-	1 500,-		5 070,-
2	10	LABORATORY BENCH, DRY	230,-	2 300,-		7 770,-
3	8	REFRIGERATOR, 300L	375,-	3 000,-		10 140,-
4	10	THERMOSTAT-CONTROLLED OVEN	230,-	2 300,-		7 770,-
5	4	FUME CUPBOARD	750,-	3 000,-		10 140,-
6	2	pH-METER--RADEIKIS	1500,-	3 000,-		10 140,-
7	1	SPECTROPHOTOMETER UNICAM	15100,-	15 100,-		51 040,-
8	1	ULTRATHERMOSTAT BATH	400,-	400,-		1 350,-
9	4	STERILIZERS	375,-	1 500,-		5 070,-
TOTAL				32.100,-		108.490,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No.A-11 DESCRIPTION-SOLVENT RECUPERATION PLANT						
	PIECES	ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US Dollars	LOCAL Tg	TOTAL Tg
1	1	RESERVOIR, 100L, GLASS	100,-	100,-		340,-
2	1	RECTIFICATION PLATE COLUMN, DIAM. 400mm, HEIGHT 12m, GLASS	9800,-	9 800,-		55120,-
3	1	RESERVOIR, 100L, GLASS	100,-	100,-		340,-
4	2	RESERVOIR, 50L, GLASS	25,-	50,-		170,-
5	1	RECTIFICATION PACKED COLUMN, DIAM. 300mm, GLASS	7200,-	7 200,-		24340,-
6		PIPING AND FITTINGS	800,-	800,-		2700,-
TOTAL				18.050,-		61.010,-

TOTAL OF EQUIPMENT

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST

PROJECT COMPONENT No. A-12 DESCRIPTION-WATER DEMINERALIZATION PLANT

NO	QTY	ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US Dollars	LOCAL Tg	TOTAL Tg
1	1	DEMINERALIZATION PLANT, 200L/H, GLASS	4 200,-	4 200,-		14 200,-
2	1	RESERVOIR, 1500L, ARV STEEL	3 800,-	3 800,-		12 840,-
3	1	PIPE	200,-	200,-		680,-
4	1	HEAT EXCHANGER, JACKETED, 1500L, ARV STEEL	3 400,-	3 400,-		11 490,-
5	1	CONDENSER, 0.5m ² , ARV STEEL	800,-	800,-		2 700,-
6	1	CONDENSER, 2m ² , ARV STEEL	1 500,-	1 500,-		5 070,-
7	1	RESERVOIR, 1500L, ARV STEEL	3 800,-	3 800,-		12 840,-
8		PIPING AND FITTINGS		1 100,-		3 720,-
9		ELECTRICITY WIRING-SPECIAL SUPPLY		100,-		340,-
10		PIPING AND REGULATOR-N-COMMERCIAL SUPPLY		400,-		1 350,-
TOTAL				19.300,-		65.230,-

SEE OVER TOTAL OF PROJECT COMPONENT T TO SUMMARY SHEET /SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST							
EQUIPMENT							
PROJECT COMPONENT		No.A-13		DESCRIPTION- ENGINE ROOM FOR STEAM AND HOT WATER PRODUCTION			
NO.	PIECES	ITEM DESCRIPTION	UNIT COST	COST			TOTAL
				FOREIGN US Dollars	LOCAL Tg	TOTAL Tg	
1	1	CONDENSATE RECEIVER	600,-	600,-		2 030,-	
2	1	STEAM BOILER, 1600L	800,-	800,-		2 700,-	
3	1	WARM WATER TANKS, 4m ² , EACH	500,-	500,-		2 600,-	
4	2	CIRCULATION PUMPS	300,-	600,-		2 050,-	
5		PIPING AND FITTINGS		300,-		1 010,-	
6		ELECTRICITY WIRING- COMMERCIAL SUPPLY		200,-		680,-	
TOTAL				3,000,-		10.140,-	

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET / SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No.A-14 DESCRIPTION-NEUTRALIZATION PLANT						
	PIECES	ITEM DESCRIPTION	UNIT COST	COST		TOTAL
				FOREIGN US Dollars	LOCAL Tg	
1	2	RESERVOIR, 2,5 ^m , GLAS REINFORCED PLASTIC	750,-	1 500,-		5 070,-
2	1	RESERVOIR FOR SULPHURIC ACID, KOROSET	800,-	800,-		2 700,-
3	1	RESERVOIR FOR CALCIUM HYDROXIDE SUSPENSION /110L MILK/	500,-	500,-		1 090,-
4	1	PUMP	500,-	500,-		1 010,-
5		PIPING AND FITTINGS		500,-		1 010,-
6		ELECTRICITY WIRING-COMMERCIAL SUPPLY		500,-		1 010,-
7		MEASURING AND REGULATION-COMMERCIAL SUPPLY		3 300,-		11 150,-
TOTAL				7.000,-		23 640,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET / SCHEDULE (-3/)

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST							
EQUIPMENT							
PROJECT COMPONENT No.A-15 DESCRIPTION-STORE						FOR INFLAMMABLE SOLVENTS	
NO.	QTY	ITEM DESCRIPTION	UNIT COST	COST			
				FOREIGN US Dollars	LOCAL Tg	TOTAL Tg	
1	5	STORAGE TANK	1820,-	9 100,-		30 760,-	
2	10	PUMP	260,-	2 600,-		8 790,-	
3		PIPING AND FITTINGS		1 900,-		6 420,-	
4		ELECTRICITY WIRING-COMMERCIAL SUPPLY		400,-		1 350,-	
5		MEASUREMENT AND REGULATION-COMMERCIAL SUPPLY		4 500,-		15 210,-	
TOTAL				18.500,-		62.530,-	

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No.A-16 DESCRIPTION- CENTRAL PRESSURE AIR						
	PIECE	ITEM DESCRIPTION	UNIT	COST		
				UNIT	FOREIGN US Dollars	LOCAL Tg
1	2	COMPRESSOR	2250,-	4 500,-		15 210,-
2	1	PRESSURE TANK	400,-	400,-		1 350,-
3	2	WET AIR PUMP	850,-	1 700,-		5 750,-
4		PIPING AND FITTINGS		800,-		2 700,-
5		ELECTRICITY WIRING- COMMERCIAL SUPPLY		400,-		1 350,-
TOTAL				7.800,-		26.360,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No. 2-17 DESCRIPTION - COOLING PLANT						
No.	QTY	ITEM DESCRIPTION	UNIT COST	COST		TOTAL
				FOREIGN US Dollars	LOCAL Tg	
1	2	COMPRESSOR PLANT, FREQN, 10000-20000 ACR/H	4550,-	9 100,-		30 760,-
2	1	COMPRESSOR PLANT, 200 000 ACR/H	30500,-	30 500,-		102 410,-

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST

EQUIPMENT

PROJECT COMPONENT No.A-18 DESCRIPTION - TRANSFORMER STATION
35/04 kv

	ELECT.	ITEM DESCRIPTION	UNIT	COST		TOTAL
				FOREIGN US Dollars	LOCAL Tg	
1	2	TRANSFORMER AIR-COOLED 630KW	12850	-25 700,-		26.870,-
2	1	SWITCHBOARD ROOM, HIGH VOLTAGE	19700	-19 700,-		66 500,-
TOTAL				45.400,-		153.460,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 6-3.

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST						
EQUIPMENT						
PROJECT COMPONENT No. A-19 DESCRIPTION - AIR CONDITIONING SYSTEM						
	PIECES	ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US Dollars	LOCAL Tg	TOTAL Tg
1	7	VENTILATORS	428,-	3 000,-		10 140,-
2		AIR-CONDITIONING UNIT		3 000,-		10 140,-
3	7	LOCAL EXHAUSTORS	214,-	1 500,-		5 070,-
4		ELECTRICITY WIRING- COMMERCIAL SUPPLY		800,-		2 700,-
TOTAL				8.300,-		28.050,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET / SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST							
EQUIPMENT							
PROJECT COMPONENT No.A-20 DESCRIPTION - MAINTENANCE SHOPS							
			ITEM DESCRIPTION	UNIT COST	COST		TOTAL
					FOREIGN US Dollars	LOCAL Tg	
1			CURRENT WORKSHOP EQUIPMENT		9 100,-		30 760,-
2			ELECTRICITY WIRING-COMMERCIAL SUPPLY		800,-		2 700,-
TOTAL					9.900,-		33.460,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 6-3/

ESTIMATE OF INVESTMENT COST : EQUIPMENT

ESTIMATE OF INVESTMENT COST							
EQUIPMENT							
PROJECT COMPONENT No.A-21 DESCRIPTION -					IN-PROCESS TRANSPORTATION		
	PIECES	ITEM DESCRIPTION	UNIT COST	COST			
				FOREIGN US DOLLARS	LOCAL ₪	TOTAL ₪	
1	2	HIGH-LIFT TRUCKS, ACCUMULATOR-POWERED	4550,-	9 100,-		30 760,-	
2	3	EXCISERS, 2.0 t	7933,-	23 800,-		80 440,-	
TOTAL				32.900,-		111.200,-	

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET /SCHEDULE 6-3/

SUMMARY SHEET - INVESTMENT COST

EQUIPMENT

No.	DESCRIPTION	FOREIGN US Dollars	LOCAL Tg	TOTAL Tg
A-01	PRODUCTION OF PEPTONE	233 200,-		788 200,-
A-02	PRODUCTION OF PEPSIN	43 400,-		146 680,-
A-03	PRODUCTION OF TRYPSIN, CHYMO- TRYPSIN AND PANCREATIN	34 200,-		115 590,-
A-04	PRODUCTION OF CHOLESTEROL	84 000,-		283 920,-
A-05	PRODUCTION OF PANCREATIN	29 800,-		100 740,-
A-06	PRODUCTION OF BLOOD HYDROLYSATE	38 800,-		131 140,-
A-07	PRODUCTION OF DRIED BILE	21 500,-		72 680,-
A-08	MANUFACTURE OF TABLETS	40 850,-		138 080,-
A-09	MANUFACTURE OF STERILE PREPARATIONS	236 600,-		799 770,-
A-10	LABORATORY QUALITY CONTROL UNIT	32 100,-		108 490,-
A-11	RECUPERATION OF ETHANOL AND ACETONE	18 050,-		61 010,-
A-12	PREPARATION OF DEMINERALIZED AND OF PYROGEN-FREE WATER	19 300,-		65 230,-
A-13	STEAM AND CONDENSATE STATION	3 000,-		10 140,-
A-14	NEUTRALIZATION PLANT	7 000,-		23 640,-
A-15	INFLAMMABLE SOLVENT STORE	18 500,-		62 530,-
A-16	VACUUM AND PRESSURE-AIR CENTRAL STATION	7 800,-		26 360,-
A-17	EQUIPMENT FOR REFRIGRATOR	39 400,-		133 170,-
A-18	THAFC - 35/0,4 KV	45 400,-		153 460,-
A-19	AIR CONDITIONING EQUIPMENT	8 300,-		28 050,-
A-20	EQUIPMENT MAINTENANCE	9 900,-		33 460,-
A-21	EQUIPMENT FOR TRANSPORT	32 900,-		111 200,-
TOTAL		1,004.000,-	600.000,-	1,993.540,-

/INSERT TOTAL IN SCHEDULE 10-1/1/

CIVIL ENGINEERING WORKS

The building site preparation evidently will be limited to terrain adaptation. The site as a whole is plane, with numerous terrain deformations. No special construction works or outdoor buildings will be necessary in the realization of the pilot plant.

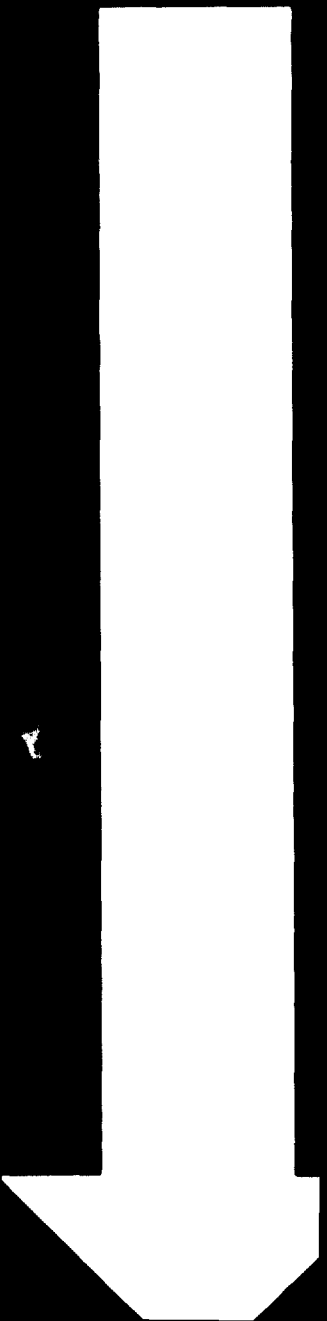
The pilot plant proper consists of three buildings.

A basic construction module 6m x 6m was chosen, which from the aspect of the building work is convenient for any or all of the following constructions:

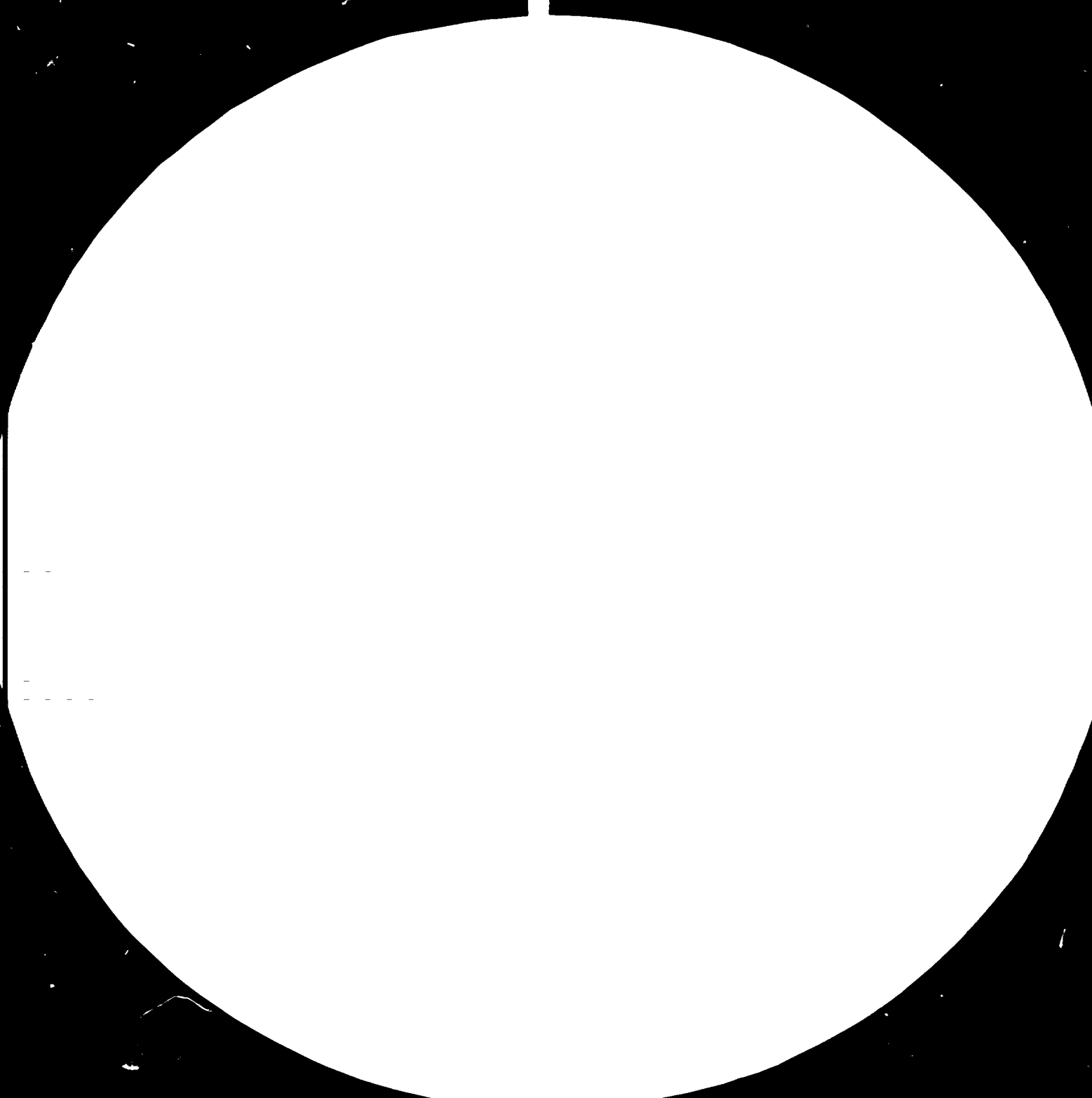
- reinforced concrete monolithic constructions
- assembled precast reinforced concrete constructions
- steel constructions
- brick constructions

We recommend the assembled precast reinforced concrete construction, partially with inserted steel ceilings /production part in the biochemical section/. This method ensures the fastest progression of the construction work, and even in the hardest climatic conditions can be realized at any time whatever.

The building B-109 Biochemical section consists of transverse modules 6m + 3m + 6m and longitudinal modules 9 x 6m. The ground modular grid, therefore, is 54m x 15m. The construction height of the three floors is 4,20m + 4,80m + 4,80m.



87-0974





28 | 25



Wavelength (nm)

300 400 500 600 700

Wavelength (nm)

300 400 500 600 700

The building B-110 Pharmaceutical section consists of transverse modules 2 x 6m and longitudinal modules 7 x 6m. The ground modular grid is 42m x 12m. Two floors of 4,20m height each are provided.

The building B-111 Laboratories consists of transverse modules 6m + 3m + 6m and longitudinal modules 7 x 6m. The ground modular grid is 42m x 15m. Three floors of 4,20m height each are provided.

The remaining construction work has the character of current energy and water supply and sewage networks or of roadbuilding.

The materials for the carcassing are fairly well available in Mongolia, including bricks, moulded bricks, expanded materials, cement, sand, gravel sand, typized reinforced concrete elements, timber, and lime.

For electricity, heating, air conditioning, water piping, and sewage piping installations the materials have to be imported; special floor coverings, steel construction materials, and tiles have to be imported as well.

In Mongolia, at present, industrial constructions and buildings are realized with so-called technical aid. This means that the Mongolian side provides workmen, and the management is entrusted to foreign specialists. Mechanisms for building equipment are imported. The local climatic con-

ditions at certain phases of construction to get the adherence to the planned working schedule.

The estimation of building work costs is based on:

- prospecting at the expected realization site
- comparisons of building works already realized with the planned ones
- technical documentation included in the present report
- calculations of basal measure values for individual premises B-101 to B-111
- expert estimation per measure unit

Calculation and quantification of work for individual premises:

- B-101 Preparation of THE LAND FOR BUILDINGS
- terrain preparation m^2 8 000
 - provisional fencing m 300
- B-102 OUTSIDE CONNECTIONS OF ELECTRICITY
35/0.4 KV
- B-103 OUTSIDE CONNECTIONS OF WATER SUPPLY
- 400m
- B-104 OUTSIDE CONNECTIONS OF 10KV VOLTAGE ELECTRICITY
- 1 000m
- B-105 OUTSIDE CONNECTIONS OF STEAM /PIPE LINES/
- 1 200m
- B-106 OUTSIDE CONNECTIONS TO CITY SEWAGE
- 180m

B-107	CONCRETEWORK, OUTSIDE		
	- 550m length		
	- 6m width	m^2	3 300
B-108	STORE FOR LIQUID MATERIAL		
	- 5 tanks		
B-109	BUILDING FOR PILOT PLANT - BIOCHEMISTRY		
	- building 55m x 16m x 15m	m^3	13 200
	- " 5m x 16m x 17m	m^3	1 360
	- platform 5m x 16m x 1m	m^3	80
		m^3	<u>14 640</u>
B-110	BUILDING FOR PILOT PLANT - PHARMACY		
	- building 43m x 13m x 10m	m^3	5 590
	- platform 50m x 3m x 1m	m^3	150
		m^3	<u>5 740</u>
B-111	BUILDING FOR QUALITY CONTROL, AUXILIARY UNITS, SOCIAL DEVICES		
	- building 43m x 16m x 13m	m^3	8 950
		m^3	<u>8 950</u>

ESTIMATE OF INVESTMENT COST : CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST

CIVIL ENGINEERING WORKS

PROJECT COMPONENT No. B-101 DESCRIPTION: PREPARATION OF THE LAND FOR BUILDING

	ITEM DESCRIPTION	UNIT COST	COST		
			US Dollars FOREIGN	Tg LOCAL	Tg TOTAL
1	B-101 PREPARATION OF THE LAND FOR BUILDING				
	- TERRAIN PREPARATION AREA 8 000 m ² COST PER UNIT: 11,25 Tg 8 000. 11,25			90.000,-	90.000,-
	- PROVISIONAL FENCING LENGTH 500m COST PER UNIT: 60 Tg 60 . 50			30.000,-	30.000,-
TOTAL				120.000,-	120.000,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET / SCHEMATIC

ESTIMATE OF INVESTMENT COST : CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST							
CIVIL ENGINEERING WORKS							
PROJECT COMPONENT No. B-102 DESCRIPTION OUTSIDE CONNECTIONS OF ELECTRICITY 35/0.4 KV							
			ITEM DESCRIPTION	UNIT COST	COST		
					FOREIGN US DOLLARS	LOCAL ₱	TOTAL ₱
1			B-102 OUTSIDE CONNECTIONS OF ELECTRICITY 35/0.4 KV <u>EXPERT ESTIMATION</u> - MAIN 35 KV - CONNEXION - HIGH-VOLTAGE CELLS			130.000,-	130.000,-
TOTAL						130.000,-	130.000,-

2000 Y OVER TOTAL OF PROJECT COMPONENT TO SURVEY COST COMPONENT

ESTIMATE OF INVESTMENT COST : CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST							
CIVIL ENGINEERING WORKS							
PROJECT COMPONENT No B-103				DESCRIPTION OUTSIDE CONNECTIONS OF WATER SUPPLY			
			ITEM DESCRIPTION	UNIT COST	COST		
					FOREIGN US\$	LOCAL Tg	TOTAL Tg
1			B-103 OUTSIDE CONNECTIONS OF WATER SUPPLY LENGTH 400m COST PER UNIT: 125 Tg 400 x 125			50.000,-	50.000,-
TOTAL						50.000,-	50.000,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET (SCHEDULE 6-4/3)

ESTIMATE OF INVESTMENT COST : CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST						
CIVIL ENGINEERING WORKS						
PROJECT COMPONENT		No B-104	DESCRIPTION	UNIT	OUTSIDE CONNECTIONS OF LOW VOLTAGE ELECTRICITY	
		ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN	LOCAL	TOTAL
				US \$	Tg	Tg
1		B-104 OUTSIDE CONNECTIONS OF LOW VOLTAGE ELECTRICITY				
		LENGTH 1 000m				
		COST PER UNIT:				
		30 Tg				
		1 000 x 30			30.000,-	30.000,-
TOTAL					30.000,-	30.000,-

CARRY OVER TOTAL PROJECT COMPONENTS TO SHEET

ESTIMATE OF INVESTMENT COST : CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST						
CIVIL ENGINEERING WORKS						
PROJECT COMPONENT		No. B-105		DESCRIPTION OF STEAM / PIPE LINES/		
		ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US \$	LOCAL Tg	TOTAL Tg
1		B-105 OUTSIDE CONNECTION OF STEAM / PIPE LINES/ LENGTH 1 000m COST PER UNIT: 80 Tg 1 000 x 80			80.000,-	80.000,-
TOTAL					80.000,-	80.000,-

AMOUNT OVER TOTAL OF PROJECT COMPONENT NO. B-105

ESTIMATE OF INVESTMENT COST						
CIVIL ENGINEERING WORKS						
PROJECT COMPONENT		No. B-106		DESCRIPTION		OUTSIDE CONNECTIONS TO CITY SEWAGE
		ITEM DESCRIPTION	UNIT COST	CCST		
				FOREIGN	LOCAL	TOTAL
1		B-106 OUTSIDE CONNECTIONS TO CITY SEWAGE LENGTH 500m COST PER UNIT: 500 Tg 500 x 500			250.000,-	250.000,-
TOTAL					250.000,-	250.000,-

ESTIMATE OF INVESTMENT COST : CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST							
CIVIL ENGINEERING WORKS							
PROJECT COMPONENT No.B:107 DESCRIPTION :COMMUNICATIONS /OUTSIDE/							
			ITEM DESCRIPTION	UNIT COST	COST		
					FOREIGN	LOCAL	TOTAL
1			B-107 COMMUNICATIONS /OUTSIDE/ AREA 3 300m ² COST PER UNIT: 151,50 Tg 3 300 . 151,50			500.000,-	500.000,-
TOTAL						500.000,-	500.000,-

TOTAL COST OF PROJECT COMPONENT NO. B:107 COMMUNICATIONS /OUTSIDE/

ESTIMATE OF INVESTMENT COST : CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST								
CIVIL ENGINEERING WORKS								
PROJECT	COMPONENT	No. B-108	DESCRIPTION:	STORE FOR LIQUID MATERIAL				
			ITEM DESCRIPTION	UNIT	COST			
				COST	FOREIGN	LOCAL	TOTAL	
1			B-108 STORE FOR LIQUID MATERIAL BUILDING WORK FOR STORAGE OF INFLAMMABLE SOLVENTS - TERRAIN WORK - FUNDAMENTS FOR TANKS - ENTRANCES - BACK FILL - TERRAIN FINISHING - CONNECTING CHANNELS EXPERT ESTIMATION				150.000,-	150.000,-
TOTAL							150.000,-	150.000,-

CARRY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY SHEET 7/30/50

ESTIMATE OF INVESTMENT COST : CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST						
CIVIL ENGINEERING WORKS						
PROJECT COMPONENT		No. B-109		DESCRIPTION : BUILDING FOR PILCT PLANT - BIOCHEMISTRY		
		ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN US DOLLARS	LOCAL T ₂	TOTAL T ₂
1		B-109 BUILDING FOR PILCT PLANT - BIOCHEMISTRY				
		AGGREGATE CUBIC SPACE				
		14 640 m ³				
		COST PER UNIT:				
		307,90 Tg				
		14 640 . 307,90			4,508.000,-	4,508.000,-
TOTAL					4,508.000,-	4,508.000,-

TOTAL OF PROJECT COMPONENT TO CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST : CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST						
CIVIL ENGINEERING WORKS						
PROJECT COMPONENT No. B-110 DESCRIPTION : BUILDING FOR PILOT PLANT - PHARMACY						
		ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN LOCAL	LOCAL	TOTAL
1		B-110 BUILDING FOR PILOT PLANT - PHARMACY AGGREGATE CUBIC SPACE: 5 740m ³ COST PER UNIT: 273,20 Tg 273,20 x 5 740				1,568,000,-
TOTAL						1,568,000,-

LOCALLY OVER TOTAL OF PROJECT COMPONENT TO SUMMARY

ESTIMATE OF INVESTMENT COST : CIVIL ENGINEERING WORKS

ESTIMATE OF INVESTMENT COST						
CIVIL ENGINEERING WORKS						
PROJECT COMPONENT		No. B-111		DESCRIPTION : BUILDING FOR QUALITY CONTROL, AUXILIARY UNITS, SOCIAL DEVICES		
		ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN Dollars	LOCAL Tg	TOTAL Tg
1		B-111 BUILDING FOR QUALITY CONTROL, AUXILIARY UNITS, SOCIAL DEVICES AGGREGATE CUBIC SPACE : 8 950 m ³ COST PER UNIT: 261,80 Tg 8 950 . 261,80			2343000,-	-2343000,-
TOTAL					2343000,-	-2343000,-

ADDED OVER TOTAL OF PROJECT FOR CIVIL ENGINEERING WORKS

SUMMARY SHEET - INVESTMENT COST
CIVIL ENGINEERING WORKS

No	PROJECT COMPONENT DESCRIPTION	INVESTMENT COST CARRIED OVER		
		FOREIGN	LOCAL	TOTAL
E-101	PREPARATION OF THE LAND FOR BUILDING		120 000,-	120 000,-
E-102	OUTSIDE CONNECTIONS OF ELECTRICITY 35/0.4 KV		130 000,-	130 000,-
E-103	OUTSIDE CONNECTIONS OF WATER SUPPLY		30 000,-	30 000,-
E-104	OUTSIDE CONNECTIONS OF LOW VOLTAGE ELECTRICITY		30 000,-	30 000,-
E-105	OUTSIDE CONNECTIONS OF STEAM /PIPE LINES/		80 000,-	80 000,-
E-106	OUTSIDE CONNECTIONS TO CITY SEWAGE		250 000,-	250 000,-
E-107	COMMUNICATIONS /OUTSIDE/		500 000,-	500 000,-
E-108	STORE FOR LIQUID MATERIAL BUILDING FOR PILOT PLANT -		150 000,-	150 000,-
E-109	BIOCHEMISTRY BUILDING FOR PILOT PLANT -		4508 000,-	4508 000,-
E-110	PHARMAC. BUILDING FOR PILOT PLANT -		1568 000,-	1568 000,-
E-111	BUILDING FOR QUALITY CONTROL, AUXILIARY DRUG, SOCIAL DEVICES		2343 000,-	2343 000,-
TOTAL			9729.000,-	9729.000,-

INSERT TOTAL IN SCHEDULE IC-1/1

ESTIMATE OF PRODUCTION COST							
CIVIL ENGINEERING WORKS							
PROJECT COMPONENT							
			ITEM DESCRIPTION	UNIT COST	COST		
					FOREIGN	LOCAL	TOTAL
			MAINTENANCE AND REPAIR OF WORKS OF:				
			SITE PREPARATION AND DEVELOPMENT,				
			BUILDINGS AND SPECIAL CIVIL WORKS,				
			OUTDOOR WORKS				
			5,9% / SCHEDULE 6-3/ 3,993.540,- Tg			235.000	235.000
			5,9% / SCHEDULE 6-5/ 9,729.000,- Tg			574.000	574.000
TOTAL						809.000,-	809.000,-

INSERT TOTAL IN SCHEDULE 6-7

SUMMARY SHEET - PRODUCTION COST

CIVIL ENGINEERING WORKS

No	DESCRIPTION	PRODUCTION COST CARRIED OVER		
		FOREIGN	LOCAL	TOTAL
1	PRODUCTION COST		809.000,-	809.000,-
TOTAL			809.000,-	809.000,-

INSERT TOTAL IN SCHEDULE 7-1

Assumed suppliers of the proposed equipment are as follows:

- | | |
|---|-------------------|
| 1/ Enameled vessels and reactors | Hungaria |
| 2/ Equipment, manufactured from stainless steel and common steel | CSSR |
| 3/ Equipment manufactured from glass | CSSR |
| 4/ Filling and tablet-making machines and some special equipment for laboratory control | GDR |
| 5/ Spray drier | Denmark or Sweden |
| 6/ Vacuum drying machines | GDR |
| 7/ Common equipment for laboratory control | CSSR |
| 8/ Cooling machines | CSSR |
| 9/ Transformers and the equipment for electricity distribution | CSSR |
| 10/ Fittings and pipelines | CSSR |

CHAPTER VII. PLANT ORGANIZATION AND OVERHEAD COSTS

CONTENTS :
COST CENTRES
OVERHEAD COSTS

CCST CENTRPS

From the organizational aspect of the new biochemical integrated works, the projected pilot plant for biochemical production for pharmaceutical purposes will operate as an integral cost centre.

This decision is based on that the pilot plant includes facilities for pilot-plant-scale operations, requiring a complete cooperation and coordination among:

- the production departments
- the power supplies
- the store operations
- the auxiliary services
- the social facilities and services
- the quality control unit
- the management system

The technical disposition plan is adapted to the described concept, providing immediate direct interconnections between

- the biochemical production and the quality control unit
- the biochemical production and the pharmaceutical manufacture
- the pharmaceutical manufacture and the quality control unit.

Evidently, the pilot plant operates as an integral dispositional whole, and the raw material input and finished product output will be assessed in a uniform way. The transfer of documentation from the pilot plant for full-scale production will be made in the form of a separate

master file for each final product.

The production plan, although specified in the pertinent chapter inclusive of the capacities, may be considerably variable. The disposition must allow a fast variation of the programme with regard to the actual results of the research.

Despite the great complexity of all operations, the extent of the pilot plant proper is adequate to its pre-production mission, and therefore the pilot plant is provided to constitute an integral cost centre.

OVERHEAD COSTS

The authors of the present chapter have decided, having taken into consideration the propositions, to combine the factory and administrative overheads and not to respect them separately.

The structure of the socialist society, also reflected in the industrial enterprises in Mongolia, presumes that the overhead costs include the following items:

- property taxes
- depreciation:
 - buildings /2.6% per year/
 - machinery /13 % per year/
 - office equipment /3.5% per year/
- communication
- off-site transport
- maintenance

Administrative costs, costs of building management, labourers' wages and social security contributions are included in the pertinent chapters and not included in Chapter VII.

It is pointed out that the insurance fees /social security contributions/ and the income taxes of both employees and labourers are already included in their basic salaries and hour wages /see Chapter VIII/.

Consequently, the authors of the present report will adhere to the recommended calculation alternative 1, and consider solely the remaining overhead costs, as specified in Schedule 7-1.

OVERHEAD COSTS

OVERHEAD COSTS							
		ITEM DESCRIPTION	UNIT COST	COST			
				FOREIGN	LOCAL	TOTAL	
				US Dollars	Tg	Tg	
1.		INSURANCE			60000,-	60000,-	
2.		WASTES DISPOSAL			5000,-	5000,-	
3.		TRAVELLING EXPENSES			15000,-	15000,-	
4.		WORK CLOTHING			10000,-	10000,-	
5.		DEPRECIATIONS:					
		a/ BUILDING 2,6%			253000,-	253000,-	
		b/ EQUIPMENT 13%			441000,-	441000,-	
		c/ OFFICE SUPPLIERS 3,5%			4200,-	4200,-	
TOTAL					788200,-	788200,-	

LABOUR

LABOURERS

The manning plan was elaborated with regard to the proposed production programme, the production capacities, and also to the local conditions.

Labourers have to be provided for the following sectors:

- biochemical production
- pharmaceutical production
- warehouse handling
- energy supply operation
- auxiliary facilities
- maintenance work
- clean-up services
- watching services

The manning for the biochemical production is planned so that no constant labourer teams are allotted to the individual production departments. The structure of the premises and equipment allows to concentrate the manpower for several production processes and thus to economize the operation /eg. the production of peptone, dried bile, and pancreatin share one and the same labourer team/.

The selection of the labourer categories was consulted with the Mongolian side with the following results:

- labourer category 6B - qualified labourer with apprenticeship certificate
- experienced labourer - foreman or deputy foreman
- 5B - labourer with apprenticeship certificate in the branch of
- biochemical production
 - pharmaceutical production
 - maintenance
 - electricians
 - locksmiths
 - joiners
 - energy supply operators
- 4B - labourers for assembling and storage handling
- 3B - charwomen, female packaging workers, forwarding department hands, gatekeepers.

WORKING DAYS PER YEAR

days per year 365.25

minus Sundays - 52.18

313.07 → 313

minus paid nonproductive working days

holidays - 7 days

leave of absence - 26 days /all-works leave minus 4 Sundays/

sick leave - 17 days

training - 10 days

other causes - 5 days

total 65 days

313 - 65 = 248 days

working days per year 248

1 shift = 8 hours

working hours per year $8 \times 248 = 1984$ (for one worker)

194 (workers) * 1984 = 384 896 hours

121 (workers in the first
shift) * 1984 = 240 064

average number of shifts/day = $\frac{384\ 896}{240\ 064} = 1,6$

SURCHARGE

- nonproductive working days	$\frac{65}{248} \times 100 = 26\%$
- surcharge for plan filling	<u>30%</u>
- surcharge for shift work	56%
/labourers only/	<u>10%</u>
	66%

NOTE

Surcharges for leave of absence, holidays, social security, and wages tax are included in the basic wages and salaries.

SCHEDULE 8-1

MANNING TABLE - LABOUR

MANNING TABLE - LABOUR : FIXED						
DEPARTMENT		WAGE CATEGORIES /No. OF WORKERS/				
FUNCTION	WAGE CATEGORY	3B	4B	5B	6B	TOTAL
FOREMAN	I	----	----	2	4	6
	II	----	----	----	----	----
	III	----	----	----	----	----
DEPUTY FOREMAN	I	----	----	----	2	2
	II	----	----	----	1	1
	III	----	----	----	----	----
LABOURERS	I	20	18	22	----	60
	II	17	11	----	----	28
	III	1	----	----	----	1
TOTAL LABOUR		38	29	24	7	98

INSERT TOTAL IN SCHEDULE 8-2

NOTE : FOREIGN LABOURERS ARE NOT INCLUDED

SCHEDULE 8-1

MANNING TABLE - LABOUR

MANNING TABLE - LABOUR : VARIABLE						
DEPARTMENT		WAGE CATEGORIES /No OF WORKERS/				
FUNCTION	SHIFT	3B	4B	5B	6B	TOTAL
FOREMAN	I	---	---	---	5	5
	II	---	---	---	---	---
	III	---	---	---	---	---
DEPUTY FOREMAN	I	---	---	---	2	2
	II	---	---	---	4	4
	III	---	---	---	1	1
LABOURERS	I	---	2	25	19	46
	II	---	2	18	12	32
	III	---	---	4	2	6
TOTAL LABOUR		---	4	47	45	96

INSERT TOTAL IN SCHEDULE 8-2

NOTE: FOREIGN LABOURERS ARE NOT INCLUDED

STAFF

Technical and clerical workers

The manpower plan of these categories is based on the given economic and production structure, reflected in the organizatory regulations of the pilot plant; the following posts are provided:

- director of the pilot plant
- vice director - economics
 - production
 - research
- head, biochemical department
- head, pharmaceutical department
- head, quality control unit
- chief technologist
- chief engineer
- workers in accounting department
- workers in planning department
- workers in supply department
- workers in personnel department
- secretaries
- workers in staff education department
- librarian
- heads of analytical laboratories
- chief physicist
- chief biochemist
- chief analyst
- laboratory technicians

In the category of technicians and clerical workers, collaboration of foreign specialists is planned in the initial operation period /see Schedule 8-3/ and, on the other hand, training of Mongolian workers in selected foreign countries with advanced biological production.

For the purposes of Mongolian workers' training, shorter or longer visits to foreign countries are envisaged.

Shorter visits /2-4 weeks/ are intended to improve the training in the spheres of

- biochemical production processes
- biochemical production planning
- production management
- good manufacturing practice

Longer visits are envisaged for

- 3 biochemists
- 3 quality control specialists
- 2 pharmacists

Training directly at the pilot plant in Mongolia will be organized and supervised by the following persons:

- chief engineer of construction
- specialist in biochemical production
- expert in quality control
- specialist in pharmaceutical production
- bacteriologist

The detailed plan for training and fellowship is enclosed in annex, page 23 and 24.

SCHEDULE 8 - 3
MANNING TABLE - STAFF

MANNING TABLE - STAFF		SALARY CATEGORIES (SALARIES)				
DEPARTMENT	FUNCTION	1200,-	1000,-	800,-	750,-	700,-
	DIRECTOR	M	1			
	VICE DIRECTOR	M	3			
	HEADS OF DEPARTMENTS B + P	M		2		
	HEAD, QUALITY CONTROL UNIT	M		1		
	CHIEF TECHNOLOGIST	M				1
	CHIEF ENGINEER	M				1
	ACCOUNTING DEPT.	A				
	PLANING DEPT.	A				
	SUPPLY DEPT.	A				
	PERSONEL DEPT.	A				
	SECRETARY	A				
	STAFF EDUCATION DEPT.	A				
	LIBRARIAN	A				
	HEADS OF ANALYT. LABS	CL				4
	CHIEF PHYSICIST	CL				
	CHIEF BIOCHEMIST	CL				
	ANALYST	CL				
	LABORATORY ASSISTANT	CL				
	TOTAL STAFF		1	3	3	2
						4

REPORT TOTAL BY CATEGORY: 1 - 1, 2 - 3, 3 - 3, 4 - 2, 5 - 4

CL = CONTROL LABS

S PER MONTH) - NO OF STAFF

-350,- 600,- 550,- 500,- 450,- TOTAL

	-350,-	600,-	550,-	500,-	450,-	TOTAL
						1
						3
						2
						1
						1
						1
			5			5
			2			2
			2			2
			2			2
					6	6
1						1
			1			1
						4
1						1
1						1
	3					3
				8		8
3	3	12	8	6		45

OFFICE OF THE
 DIRECTOR
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SCHEDULE 3 - 4

ESTIMATE OF PRODUCTION COSTS : SALARIES

ESTIMATE OF PRODUCTION COSTS - SALARIES

DEPARTMENT	SALARY CATEGORIES (SALARIES PER MONTH) - No OF STAFF										TOTAL
	1200,-	1000,-	800,-	750,-	700,-	650,-	600,-	550,-	500,-	450,-	
MANAGEMENT	1	3	3	2	-	-	-	-	-	-	9
ADMINISTRATION	-	-	-	-	-	1	-	12	-	6	19
CONTROLLABOR.	-	-	-	-	4	2	3	-	8	-	17
TOTAL No.OF STAFF	1	3	3	2	4	3	3	12	8	6	45
WORKING MONTHS PER YEAR	12	12	12	12	12	12	12,	12	12	12	-
MAN-MONTHS PER YEAR	12	36	36	24	48	36	36	144	96	72	-
SUChARGE 56 %	672,-	560	448,-	420,-	392,-	364,-	336,-	308,-	280,-	252,-	-
SALARIES PER YEAR	22464,-	18720,-	14976,-	14040,-	13104,-	12168,-	11232,-	10296,-	9360,-	8424,-	-
TOTAL	22464,-	56160,-	44928,-	26080,-	52416,-	36504,-	33696,-	123552,-	74880,-	50544,-	52322

CHAPTER VIII

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ANNEX TO CHAPTER VIII

DOCUMENTATION FROM
MONGOLIA

6077	2800	2-24	03	1	1. Организация мероприятий
19-24	2800	2-24	03	2	Административная
11-24	1800	2-16	03	2	Административная
6077	2800	2-14	03	1	2. Организация работы
19-24	2800	2-8	03	2	Административная
5729	2800	2-16	03	1	Административная
6077	2800	2-27	03	1	2. Организация работы
6077	2800	1-27	03	2	История по организации
6321	2800	1-25	03	2	Специальная
4071	2800	1-25	03	2	История по

И. Иск. Организация работы

Итого: 27

6077	2800	2-24	03	1	1. Организация мероприятий
19-24	2800	2-24	03	2	Административная
11-24	1800	2-16	03	2	Административная
6077	2800	2-14	03	1	2. Организация работы
19-24	2800	2-8	03	2	Административная
5729	2800	2-16	03	1	Административная
6077	2800	2-27	03	1	2. Организация работы
6077	2800	1-27	03	2	История по организации
6321	2800	1-25	03	2	Специальная
4071	2800	1-25	03	2	История по

Улановичи: 2 4В 2-13

Итого: 70

IV. Мех. обработка

1. Отделение обезжелезивания

Мастер	1	6В	2-11	2000	6617
Аппаратчик	1	6В	2-11	2000	6617
Аппаратчик	1	6В	2-11	2000	6617
Рабочий по обезжелезиванию	1	6В	2-11	2000	6617
Укладчик	1	6В	2-11	2000	6617
Эксплуатационный персонал	1	6В	2-11	2000	6617
Итого	6	36В	2-11	12000	39600

2. Отделение обезжелезивания

Мастер	1	6В	2-11	2000	6617
Аппаратчик	1	6В	2-11	2000	6617
Аппаратчик	2	6В	2-11	4000	13234

3. Отделение нейтрализации

Мастер	1	6В	2-84	2000	6617
Аппаратчик	4	6В	2-84	8000	26460
Аппаратчик	2	5В	2-16	2000	11461

4. Отделение фильтрации

Мастер	1	6В	2-84	2000	6617
Аппаратчик	4	6В	2-84	8000	26460
Аппаратчик	2	5В	2-16	2000	11461

5. Отделение упаковки

Мастер	1	6В	2-84	2000	6617
Рабочий по стерилизации	4	5В	1-35	8000	17342
Укладчик	2	3В	1-01	2000	8301
Эксплуатационный персонал	2	3В	1-35	2000	8301
Укладчик	4	4В	2-13	2000	10000

Итого: 34

194000

1. Специальные инструменты

Мастер	1	6B	2-84	2000	6617
Аппаратчик	4	6B	2-84	2000	26469
Аппаратчик	2	5B	2-46	2000	11464

2. Специальные сушки

Мастер	1	6B	2-84	2000	6617
Аппаратчик	4	6B	2-84	2000	26469
Аппаратчик	2	5B	2-46	2000	11464

3. Специальные дражеобразки

Мастер	1	6B	2-84	2000	6617
Аппаратчик	4	6B	2-84	2000	18889
Аппаратчик	2	5B	2-46	2000	11464

4. Специальные упаковки

Мастер	1	6B	2-84	2000	6617
Работник по стерилизации	4	5B	1-55	2000	17442
Электрик	2	3B	1-05	2000	8621
Укупорщик	2	3B	1-05	2000	8621
Упаковщик	2	4	2-77	2000	11464

Итого: 30

2. Специальные инструменты

Мастер	1	6B	2-84	2000	6617
Аппаратчик	4	6B	2-84	2000	26469
Аппаратчик	2	5B	2-46	2000	11464
Работник по стерилизации	4	5B	1-55	2000	17442
Электрик	2	3B	1-05	2000	8621
Укупорщик	2	3B	1-05	2000	8621

Итого:

30

100000

III. Цех холестерина

1. Отделение экстракции

Мастер	I	6B	2-84	2330	6617
Аппаратчик	2	6B	2-84	2330	13234
Аппаратчик	I	5B	2-46	2330	5732

2. Отделение сушки

Мастер	I	6B	2-84	2330	6617
Аппаратчик	2	6B	2-84	2330	13234
Аппаратчик	I	5B	2-46	2330	5732

3. Отделение упаковки

Мастер	I	6B	2-84	2330	6617
Рабочий по стерилизации	2	3B	1-85	2330	8621
Этикетчик	2	3B	1-85	2330	8621
Упаковщик	2	4B	2-13	2330	9926
Укупорщик	8	3B	1-85	2330	8621
ВСЕГО:	23				131805

IV. Цех упаковки пива
и напитков

1. Отделение опотранки

Мастер	I	6B	2-84	2330	6617
Аппаратчик	2	6B	2-84	2330	13234
Аппаратчик	2	5B	2-46	2330	11464

2. Отделение сушки

Мастер	I	6B	2-84	2330	6617
Аппаратчик	2	6B	2-84	2330	13234
Аппаратчик	I	5B	2-46	2330	5732

3. Отделение фильтрации

Мастер	I	6B	2-84	2330	6617
Аппаратчик	2	6B	2-84	2330	13234
Аппаратчик	I	5B	2-46	2330	5732

4. Отделение упаковки

Мастер	I	6B	2-84	2330	6617
Рабочий по стерилизации	2	3B	1-85	2330	8621
Этикетчик	2	3B	1-85	2330	8621
Упаковщик	2	4B	2-13	2330	9926
Укупорщик	8	3B	1-85	2330	8621
ВСЕГО:	23				131805

IX. Hex AFD

1. Убойная					
Мастер	1	6D	2-34	2330	6617
Работник	2	6D	2-34	2330	13234
Работник	2	5B	2-16	2330	11464
2. Отделение электротехники					
Мастер	1	6D	2-34	2330	6617
Работник	2	6D	2-34	2330	13234
Работник	2	5B	2-16	2330	11464
3. Отделение электротехники					
Мастер	1	6D	2-34	2330	6617
Работник	2	6D	2-34	2330	13234
Работник	2	5B	2-16	2330	11464
4. Отделение электротехники					
Мастер	1	6D	2-34	2330	6617
Работник	2	6D	2-34	2330	13234
Работник по обслуживанию	1	6D	2-34	2330	6617
Удиритель	2	6D	2-34	2330	13234
Электрик	2	3B	1-05	2330	2021
ВСГО:	33				189522

X. Hex лектора

1. Отделение гидролиза					
Мастер	1	6B	2-34	2330	6617
Аппаратчик	4	6B	2-34	2330	23169
Аппаратчик	2	5B	2-16	2330	11464
2. Отделение фильтрации					
Мастер	1	5B	2-34	2330	6617
Аппаратчик	2	6B	2-34	2330	13234
Аппаратчик	2	5B	2-16	2330	11464
3. Отделение сушки					
Мастер	1	6B	2-34	2330	6617
Аппаратчик	2	6B	2-34	2330	13234
Аппаратчик	2	5B	2-16	2330	11464

Study tours and Fellowships

1/ Study tours - are determined for key-personnel from Mongolia and should last 1 or 2 weeks. These study tours are assessed for the key-workers of the new proposed pilot plant: for its director and his deputies and for the chiefs of research- and quality control- departments. Programme of such study tours shall include:

- Studying of the economical problems connected with production of biochemical pharmaceuticals;
- Studying of the planning of such production;
- Studying of the main problems connected with running of such a factory;
- Getting acquainted with all the regulations for production of sterile final pharmaceutical products;
- Getting acquainted with the work of biochemical research and quality control departments;

We recommend these study tours to be realized either to Czechoslovakia - Prague - SFCFA or to Hungary - Budapest - Gedeon Richter.

Proposed duration: 2m/m

2/ Fellowships

This part of training is determined for the following technical workers from Mongolia:

Foremen from the projected biochemical production units:

- to study the production of the main biochemical products, enzymes and hormones;
- to learn the right production practice;
- to get a good experience in running of the single biochemical production;
- to learn the good know-how of all the products planned for the production of the proposed pilot plant.

Proposed: 3 workers, 15m/m

Person from the pharmaceutical units of the plant:

- to learn all the necessary production practice, connected with preparation of sterile pharmaceutical products;
- to learn all the production practice with finalizing of the final forms of vials and ampoules;
- to get a good knowledge in preparing of pharmaceutical drugs like tablets and coated tablets;
- to learn the initial preparation of granulated mixtures;
- to get the necessary practice in correct pharmaceutical work.

Proposed: 2 workers, 12m/m

Quality control workers from the proposed analytical and bacteriological laboratories:

- to learn all the necessary control methods for testing of the biochemical final products;
- to learn the methods for testing of all raw materials;
- to study and to learn the methods for testing of activities of enzymes and heparin;
- to learn the polarographic and spectrophotometric methods used for control of final products;

- to learn all the necessary chemical and physically-chemical methods of analytical chemistry;
- to get a good knowledge of bacteriological testing of sterile pharmaceutical products;
- to learn the control methods for testing of the air-purity in sterile production rooms;
- to learn the basic principles of microbiological purity tests and of control methods for testing of correct hygienic conditions in pharmaceutical departments;
- to learn the necessary biological testing of biochemical products - bioassay of insulin, gonadotropins, testing of pyrogen and hypertensive impurities, bioassay for testing of pituitary hormones;
- to learn the right practice of test-animals breeding and keeping and their preparation for biological tests.

Proposed: 3 workers 15m/m

For all the fellowships we recommend their performing in Czechoslovakia.

CHAPTER IX. IMPLEMENTATION SCHEDULING

CONTENTS :

DATA AND ACTIVITIES

SELECTION OF PROJECT IMPLEMENTATION
PROGRAMME AND TIME SCHEDULE

COST ESTIMATE OF PROJECT IMPLEMENTATION

DATA AND ACTIVITIES

Essential data and activities

The planned pilot plant is financed partially by the Mongolian Government and partially by the UNIDO, Regional Office Vienna. Both partners had agreed that the project would be realized in the period 1982 - 1986. The Mongolian Government will ensure the realization conditions in the full extent.

The obligations ensuring the realization are divided between both sides as follows.

The Mongolian Government ensures:

- the nomination of the managing body of the pilot plant construction
- contracts for delivery of project realization documentation
- contacts with authorities in Ulan Bator competent for approving the project
- methods for planning the pilot plant construction
- contracts for supplies of machinery
- suppliers of buildings in a full extent /inclusive of water pipelines, sewage drains, central heating, illumination wiring systems/
- agreements concerning the education and training of Mongolian personnel in foreign countries

- contracts with foreign experts for the running-in period of the pilot plant
- contracts for special assembling operations
- expert supervision of all professional activities in the pilot plant construction
- housing, boarding, and social facilities
- sanitary provisions
- fire protection
- safety of work and operation
- taking-over of buildings and equipment for permanent operation
- supply of labour and material for the pilot plant construction

The Mongolian Government finances:

- the building site /the representatives of the Mongolian Government had declared that the building site would be provided free of cost/
- the project realization documentation
- the experts supervising the pilot plant construction in all professions
- all buildings and plants included in the nomenclatures B-101 to B-111

- all assembling operations of the machinery and equipment
- preliminary operations
- state, municipal, and other official charges

The UNIDO Regional Office, Vienna, finances:

- the machinery and equipment specified in the lists A-01 to A-21
- the visits for the purpose of studies
- the training of Mongolian personnel in foreign countries
- selected special short-term assembling operations
- foreign experts supervising the running-in of the pilot plant

The financial and realization plan follows. The requirements of the UNIDO Regional Office, Vienna, are included in the plan. The plan had been discussed in Mongolia with all competent partners /UNDP/UNIDO, Mongolian Government/.

TABLE TWO - BUDGET PLANNING

MONITORING COMPONENT	1981	1982	1983	1984	1985	1986
EXPERTS	450	300	—	50	50	50
EXPERT PERSONNEL	2025	24	208	412	620	832
BUILDINGS						
B-101	120	120	—	—	—	—
B-102	130	—	130	—	—	—
B-103	50	—	50	—	—	—
B-104	30	—	30	—	—	—
B-105	90	—	80	—	—	—
B-108	250	—	250	—	—	—
B-107	500	—	500	—	—	—
B-108	150	—	—	—	150	—
B-109	4303	—	1000	1400	1300	503
B-110	1732	—	203	400	600	300
B-111	2373	—	510	803	100	300
EQUIPMENT ASSEMBLY	300	—	—	—	—	600
MISCELLANEOUS	250	50	50	50	50	50
TOTAL	13125	434	3103	3115	3770	2640
UNDO	14302	1292	1273	1276	1275	1275
OTHER PERSONNEL COSTS	—	2	2	2	2	—
TOTAL SUBCONTRACTS (MPO)	1511	423	1135	2016	493	519,3
STUDY COSTS	10	5	5	5	—	—
TOTAL EQUIPMENT COMPONENTS	10	5	5	10	—	—
MISCELLANEOUS	22	2	5	5	5	5
TOTAL	1578	1053	1155	2228	500	604,6
TOTAL TO (X 85%)	8421	897	488	118	1630	2043,6

RECAPITULATION	1981	1982	1983	1984	1985	1986
MONITORING EQUIPMENT	13125	434	3103	3115	3770	2640
UNDO	8322	653	488	776	1630	2043,6
TOTAL	13457	987	3591	3891	5400	4683,6

SELECTION OF PROJECT IMPLEMENTATION
PROGRAMME AND TIME SCHEDULE

Selection of realization plan and working schedule

The realization plan, in connexion with the working schedule, must have the following consecution:

- hydrogeological prospecting
- altimetric and planimetric survey
- building plan
- preparation of building site

The construction work proper will start with the construction of water piping, gas piping, steam piping, electricity cable lines, canalization, and roadway connexion. The realization of this work is planned for 1983 /E-102 to E-107/.

The buildings are designed so that analogous construction technology will serve for all three of them. Underground work is excluded. Completely assembled structures are envisaged. The heights of the individual floors and the total height of the highest building allow a maximal use of construction mechanization.

The character of the machinery equipment, its presumptive dimensions, and the interconnexion of the individual technological units allow successive assembling.

A characteristic process of pilot-plant construction should follow a line with preference of the building E-109. Then the working schedule would proceed as follows:

- foundations - E-109
- foundations - E-110
- structure assembling E-109
- foundations - E-111
- structure assembling E-109
- structure assembling E-110
- other carcassing work E-109
- structure assembling E-110
- structure assembling E-111
- other carcassing work E-109
- and
- other carcassing work E-110
- structure assembly E-111
- auxiliary construction work E-109
- other carcassing work E-110
- other carcassing work E-111
- auxiliary construction work E-109
- auxiliary construction work E-110
- other carcassing work E-111

- readiness for machinery equipment assembling B-109
auxiliary construction work B-110
auxiliary construction work B-111
- machinery equipment assembling in B-109
readiness for machinery equipment assembling B-110
auxiliary construction work B-111
- machinery equipment assembling in B-109
machinery equipment assembling in B-110
readiness for machinery equipment assembling B-111
- finish of machinery equipment assembling in B-109
machinery equipment assembling in B-110
machinery equipment assembling in B-111
- finish of machinery equipment assembling in B-110
machinery equipment assembling in B-111
- finish of machinery equipment assembling in B-111

From the specified phases of construction it is evident that individual groups of trained workers successively pass over from B-109 to B-111 and carry out solely basic operations which they had perfectly mastered. This flow working schedule is demanded with respect to the preparation of work and materials, but the progression of the operations is accelerated and facilitated.

The assembling of machinery equipment must start in B-109, where the volume of equipment and assembling work is largest.

Key and decisive terms of pilot-plant construction

- start of pilot-plant construction
B-101, B-102, B-103, B-104,
B-105, B-106, B-107, B-109 May 1983
- start of construction
B-110 and B-111 October 1983
- making B-109 ready for machinery
equipment assembling June 1984
- making B-110 ready for machinery
equipment assembling January 1985
- start of construction B-108 June 1985
- making B-111 ready for machinery
equipment assembling June 1985
- trial operation June 1986
- full operation December 1986

COST ESTIMATE OF PROJECT
IMPLEMENTATION

Estimation of project realization costs

In the case of the operations carried out in the course of the investment phase up to the moment of the start of full production operation, the costs have to be estimated of the following items:

- projecting work
- authors' supervisory activity
- inspection activity
- administration of building and construction management
- fees for approval procedures
- training of staff and labourers

The financial means for covering the costs of

- the building site
- technological equipment
- building and construction work
- machinery and equipment
- materials
- raw material
- overhead costs

are specified in pertinent foregoing chapters.

ESTIMATE OF INVESTMENT COSTS - PROJECT IMPLEMENTATION

ESTIMATE OF INVESTMENT COSTS						
PROJECT IMPLEMENTATION						
		ITEM DESCRIPTION	UNIT COST	COST		
				FOREIGN Tg	LOCAL Tg	TOTAL Tg
1		REALIZATION OF PROJECT			450000,-	450000,-
2		SUPPORT PERSONEL		27040,-	1287000,-	1314040,-
3		EMPLOYEE'S SCHOOLING		1713660,-		1713660,-
4		STUDY TOURS		50700,-		50700,-
5		TOTAL EQUIPMENT COMPONENT		67600,-		67600,-
6				74360,-	250000,-	324360,-
TOTAL				1933360,-	1987000,-	3920360,-

CHAPTER	1
LIST	2

CHAPTER X. FINANCIAL AND ECONOMIC EVALUATION

CONTENTS :

PROJECT FINANCING

TOTAL PRODUCTION COSTS

FINAL EVALUATION

NATIONAL ECONOMIC EVALUATION

PROJECT FINANCING

The financing of the project, as already stated in the preceding chapters, is shared by

- the UNDP/UNIDO Office Vienna
- the Mongolian Government

The UNIDO sources are generally known and need no commentary.

The sources of the Mongolian Government issue from the planned state budget, based in turn on successive five-year plans.

The Mongolian Republic is a rapidly developing socialist agricultural country. Banking in Mongolia is exclusively owned and controlled by the state. The general and particular characteristics of the calculations included in Chapter X are adjusted to the system.

In the seventh five-year plan /1981-1985/ the present project is included in the Mongolian government plan. The Government's participation in financing the project was verified by the experts at the Government Committee on Economic Relations in Ulan Bator.

The system of financing being controlled centrally in Mongolia, some items are omitted from the appropriate schedules included in the Manual for the Preparation of Industrial Feasibility Studies, UNIDO publication No. E.78.II.B.5. of 1978.

Project financing

The project is financed by the UNIDO and the Mongolian Government. The financial means have not the character of loans and are not-repayable.

Project costs

The total investment costs, 18,451.900, include the fixed investment costs and the preproduction capital expenditure. The working capital is provided annually by the Mongolian Government.

	Foreign currency	Local currency	Total
A. Fixed investment costs			
Site preparation		809.000,-	809.000,-
Buildings		9,729.000,-	9,729.000,-
Machinery	3,993.540,-	600.000,-	3,993.540,-
Total			14,531.540,-
B. Preproduction capital expenditure			3,920.360,-
Total A + B			18,451.900,-
C. Working capital			3,389.495,-

Financial means:

Source	Fixed investment costs	reproduction capital expenditure	Total
Total investment costs	14,531.540,-	3,920.360,-	18,451.900,-

These means will be drawn in the course of the construction period as follows:

Expences are published in Mongolian currency /Tg/

YEAR	MONGOLIAN GOVERNMENT	UNIDO	TOTAL	%
1982	494.000,-	359.300,-	853.300,-	4,62
1983	3,106.000,-	458.000,-	3,564.000,-	19,32
1984	3,115.000,-	776.000,-	3,891.000,-	21,09
1985	3,770.000,-	1,690.000,-	5,460.000,-	29,59
1986	2,640.000,-	2,043.600,-	4,683.600,-	25,38
Total	13,125.000,-	5,326.900,-	18,451.900,-	100,00

Schedule 10-1/1
Initial fixed investment costs

Investment category	Foreign currency	Local currency	Total costs
1. Site preparation and development	-----	809 000	809 000
2. Structures and civil works	-----	9 729 000	9 729 000
a/ Buildings and civil works	-----	9 729 000	9 729 000
3. Plant machinery and equipment	3 393 540	600 000	3 993 540
4. Total initial fixed investment costs	3 393 540	11 138 000	14 531 540

SCHEDULE 10 - 1/2
FIXED INVESTMENT COSTS^a

PERIOD YEAR	CONSTRUCTION PERIOD INVESTMENT						START-UP AND FULL CAPACITY UTILIZATION			TOTAL						
	1		2		3		4		5		FC	LC	Tt	FC	LC	Tt
FIXED INVESTMENT COSTS	FC	156782	—	—	—	—	—	—	—	—	—	—	—	—	—	3393540
	LC	514576	37376	449480	27720	—	—	—	—	—	—	—	—	—	—	600000
	Tt	671358	37376	449480	184502	—	—	—	—	—	—	—	—	—	—	11138000
	FC	655632	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	LC	2151862	156299	1879643	115920	—	—	—	—	—	—	—	—	—	—	—
	Tt	2807494	156299	1879643	771552	—	—	—	—	—	—	—	—	—	—	—
1. SITE PREPARATION AND DEVELOPMENT	FC	715698	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	LC	2349004	170618	2051846	126540	—	—	—	—	—	—	—	—	—	—	—
	Tt	3064702	170618	2051846	842238	—	—	—	—	—	—	—	—	—	—	—
	FC	1004148	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	LC	3295734	239383	2878811	177540	—	—	—	—	—	—	—	—	—	—	—
	Tt	4299882	239383	2878811	1181688	—	—	—	—	—	—	—	—	—	—	—
2. STRUCTURES AND CIVIL WORK	FC	861280	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	LC	2826824	205324	2469220	152250	—	—	—	—	—	—	—	—	—	—	—
	Tt	3688104	205324	2469220	1013560	—	—	—	—	—	—	—	—	—	—	—
	FC	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	LC	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	Tt	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
3. PLANT AND MACHINERY	FC	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	LC	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	Tt	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	FC	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	LC	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	Tt	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—

NOTE : FC = FOREIGN CURRENCY , LC = LOCAL CURRENCY , Tt = TOTAL

Schedule 10-2/1

Pre-production capital expenditures, by category

Category	From table	Foreign currency	Local currency	Total
1. Pre-investment studies	2-1	(134 750)	-----	(134 750)
2. Laboratory investigations	2-1	-----	(170 000)	(170 000)
3. Management of project implementation	9-1	-----	450 000	450 000
4. Supervision, co-ordination, test-run and take-over of civil works, equipment and plant	9-1	94 640	1 287 000	1 381 640
5. Build-up of administration recruitment and training of staff and labour	9-1	1 764 360	-----	1 764 360
6. Miscellaneous	9-1	74 360	250 000	324 360
Total		1 933 360	1 987 000	3 920 360

1. UNIDO - (134 750 Tg) - 1981

2. Mongolian government - (170 000 Tg) - 1981

SCHEDULE 10 - 2/2
PREPRODUCTION CAPITAL EXPENDITURE, BY YEAR

PERIOD YEAR	CONSTRUCTION PERIOD												STARTUP AND FULL CAPACITY			TOTAL					
	1			2			3			4			5			FC	LC	TZ			
	FC	LC	TZ	FC	LC	TZ	FC	LC	TZ	FC	LC	TZ	FC	LC	TZ						
PREPRODUCTION CAPITAL EXPENDITURE	89321	91799	181120	373525	383888	757413	407746	419059	826805	572081	587953	11160034	490687	504301	994988				1933360	1987000	3920360

NOTE : FC = FOREIGN CURRENCY, LC = LOCAL CURRENCY, TZ = TOTAL

TOTAL PRODUCTION COSTS

With due regard to the character of the present project, formulated in Chapter II of this study, the Chapter X is elaborated in accordance with the guidelines set in the Manual for the Preparation of Industrial Feasibility Studies, UNIDO publication No.E.78.II.B.5 of 1978.

The essential data given below lead to the following conclusions:

- 1/ The annual rate of profit from the equity capital grows from 13.12% in the first year of production to 28.70% in the year of expected 100% production capacity:

	Construction					Start-up and full production					
Year	1	2	3	4	5	6	7	8	9	10	11
Net profit after tax						2421272	3837096	5004411	5295121	5295121	5295121
Equity capital	18451900	18451900	18451900	18451900	18451900	18451900	18451900	18451900	18451900	18451900	18451900
Rate of profit%						13,12	20,80	27,12	28,70	28,70	28,70

- 2/ The initial investment costs, ie, 18,451.900,-Tg, will be paid back within less than 9 years from the start of construction /calculation of rate of return of the project/:

Year	Net profit	Depreciation	Amount paid back	Balance
1	----	----	----	18,451.900,-
2	----	----	----	- " -
3	----	----	----	- " -
4	----	----	----	- " -
5	----	----	----	- " -
6	2,421.272,-	698.200,-	3,119.472,-	15,332.428,-
7	3,837.096,-	698.200,-	4,535.296,-	10,797.132,-
8	5,004.411,-	698.200,-	5,702.611,-	5,094.521,-
9	5,295.121,-	698.200,-	5,993.321,-	-----
10	5,295.121,-	698.200,-	5,993.321,-	-----

3/ The simple rate of profit in the 9th year after the start of construction /production with 100% capacity/ will be:

$$R_e = \frac{\text{net profit}}{\text{equity capital}} \times 100 = \frac{5,295.121}{18,451.900} \times 100 = 28.70\%$$

4/ The rate of return of the project in the 9th year after the start of construction will be:

$$\frac{\text{net profit}}{\text{total investment outlay}} \times 100 = \frac{5,295.121}{10,626.517} \times 100 = 49.83\%$$

Schedule 10-3/1

Calculation of working capital

I. Minimum requirements of current assets and liabilities

a/ Accounts receivable : 30 days at production costs
minus depreciation and
interests

b/ Inventory :

Local material : 180 days

Imported material : 180 days

Spare parts : 180 days

Work in progress : 20 days at factory cost

Finished products : 20 days at factory cost
plus administration and
overheads

c/ Cash in hand : 15 days (see separate calculation at
the bottom of schedule 10-3/2)

d/ Accounts payable : 30 days (for raw materials and
utilities)

II. ANNUAL PRODUCTION - COST ESTIMATE

PERIOD YEAR	CONSTRUC- TION	START - UP	
	1 - 5	6	7
PRODUCTION PROGRAMME	0	50 %	75 %
RAW MATERIALS :			
LOCAL MATERIAL	-	1218008	1921512
IMPORTED MATERIAL	-	1075413	1613119
LABOUR	-	414876,2	622314,2
UTILITIES	-	1505007	2257511
MAINTENANCE -SPARE PARTS	-	33300	50700
FACTORY OVERHEAD COSTS	-	709885	709885,
FACTORY COSTS ADMINISTRATIVE	-	4953939	7175041
OVERHEAD COSTS	-	598224	598224
OPERATING COSTS	-	5555213	7773265
DEPRECIATION	-	699200	699200
TOTAL PRODUCTION OR MANUFACTURING COSTS	-	6253413	8471495

FULL CAPACITY

8	9	10	11
95 %	100 %	100 %	100 %
2433015	2562016	2562016	2562016
2043265	2150825	2150826	2150826
789184,7	829752,3	829752,3	829752,3
2088513	3010014	3010014	3010014
64220	67600	67600	67600
709885	709885	709885	709885
8380093	9330093	9330093	9330093
598224	598224	598224	598224
9928317	9928317	9928317	9928317
698200	698200	698200	698200
10625517	10625517	10625517	10625517

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REQUIREMENTS - 1975

NUMBER OF COUNCIL MEMBERS	NUMBER OF COUNCIL MEMBERS	REQUIREMENTS - 1975							
		6	7	8	9	10	11	12	13

10	12	462021	607772	721442	821450	827260	827400		
100	2	609021	660925	721025	761028	761030	761032		
125	1125	201021	201022	201023	201024	201025	201026		
160	2	101021	101022	101023	101024	101025	101026		
20	185	905021	905022	905023	905024	905025	905026		
20	13	809623	831813	527623	551573	551572	511572		
15	94	92102	82024	90025	91024	91024	91024		
---	---	215345	202022	204543	103021	103021	103021		
20	12	321023	432673	611022	641571	641571	641571		
---	---	780023	511445	322024	930025	200026	920027		
---	---	600026	600026	100027					

REQUIREMENTS - 1976

NUMBER OF COUNCIL MEMBERS	NUMBER OF COUNCIL MEMBERS	REQUIREMENTS - 1976							
		6	7	8	9	10	11	12	13

---	---	6253413	847142	1085507	1026517	1026517	1026517		
---	---	1028421	2524621	4471200	4102402	4102402	4102402		
---	---	1525007	2252511	2252512	201024	201024	201024		
---	---	202020	600020	610020	600020	600020	600020		
15	211	1753025	1021143	130024	2202402	2202402	2202402		
---	---	72102	821964	90025	91024	91024	91024		

Schedule 10-6/1

Total initial investment costs

	Investment category	Foreign currency	Local currency	Total
1.	Initial fixed investment costs	3 393 540	11 138 000	14 531 540
2.	Pre-production capital expenditures	1 933 360	1 987 000	3 920 360
3.	Working capital (at full capacity)	-----	3 389 495	3 389 495
	Total	5 326 900	16 514 495	21 841 395

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1912-1913

ACQUISITIONS

...

Schedule 10-7/1

Total initial assets

	Investment category	Foreign currency	Local currency	Total
1.	Initial fixed investment costs	3 393 540	11 138 000	14 531 540
2.	Pre-production capital expenditures	1 933 360	1 987 000	3 920 360
3.	Current assets (at full capacity)	-----	4 033 066	4 033 066
	Total	5 326 900	17 158 066	22 484 966

Schedule 10-S/1
Sources of finance

Item	Sources of finance	Local currency	Foreign currency	Total
1.	Promoters (Mongolia) a/ Equity	13 125000	-----	13 125000
2.	Financial institutions or development agencies (UNIDO)	-----	5 326900	5 326900
	Total, all items	13 125000	5 326900	18 451900

2012-2013 10-6/2
 STATE OF INITIAL FUNDS

YEAR	CONSTRUCTION						REC-DUCTION			TOTAL						
	1	2	3	4	5	FC	LC	T.							
EQ.ITY CAPITAL	357310	443713	652413	356724	776000	315507	3291507	1540000	3767715	5459915	2043000	2639472	4083072	5326900	18125000	18451900
TOTAL	357310	443713	652413	356724	776000	315507	3291507	1540000	3767715	5459915	2043000	2639472	4083072	5326900	18125000	18451900

NOTE: FC = FOREIGN CURRENCY, LC = LOCAL CURRENCY, T. = TOTAL

FINAL EVALUATION

UP AND FULL CAPACITY

7	75%	2193850	3021350	3150000	3180700	3190000
8	95%	10192607	12222517	10226517	10666517	
9	100%	2193395	2071743	2114483	21532193	2180482
10	100%	511289	15015232	13155322	10945902	15177662
		367096	5004411	5275121	5275121	5295121
		339096	5004411	5275121	5295121	5295121
		52358	11262779	13371400	21853021	27143142

5444	66,85	53,59	65,59	66,59	68,10
5511	15,75	10,55	15,65	16,65	18,10
5530	24,12	22,70	24,70	25,70	27,10

SCHEDULE 10-9
NET INCOME STATEMENT

PERIOD	YEAR	PRODUCTION PROGRAMME
1-5	6	50%
1. SALES	—	15938500 23
2. PRODUCTION COSTS	—	3253413 38
3. GROSS OBTAINABLE PROFIT (1-2)	—	9585087 15
4. TAX (75%)	—	7283975 11
5. NET PROFIT (3-4)	—	2421272 33
7. UNDISTRIBUTED PROFITS	—	2421272 33
8. ACCUMULATED UNDISTRIBUTED PROFITS	—	2421272 33
RATIOS		
GROSS PROFIT: SALES (%)	—	60.77
NET PROFIT: SALES (%)	—	15.17
NET PROFIT: EQUITY (%)	—	15.12

STATE 10-10.

DETAILED FINANCIAL SHEET

PERIOD	OWNERS ACTION		START-UP AND FULL CAPACITY								
YEAR	1	2	3	4	5	6	7	8	9	10	11
ASSETS (TOTAL)	552473	447285	300332	197320	461700	222712	310000	411019	350000	100000	1453000
CURRENT ASSETS						519472	155459	100000	125000	250000	1932000
CASH BALANCE						100867	250000	200000	200000	200000	100000
RECEIVABLES						210335	300000	300000	400000	400000	100000
INVENTORY											
PROPERTY											
DEFERRED ASSETS											
NET OF DEFERRED ASSETS	552473	447285	300332	197320	461700	1775772	1100000	1500000	1500000	1500000	1500000
LIABILITIES (TOTAL)	352473	447285	300332	197320	461700	1775772	1100000	1500000	1500000	1500000	1500000
EQUITY CAPITAL	352473	447285	300332	197320	461700	1775772	1100000	1500000	1500000	1500000	1500000

STATE 10-10.

Schedule 10-11
 Total production costs^a (see also schedule 10-3/1)

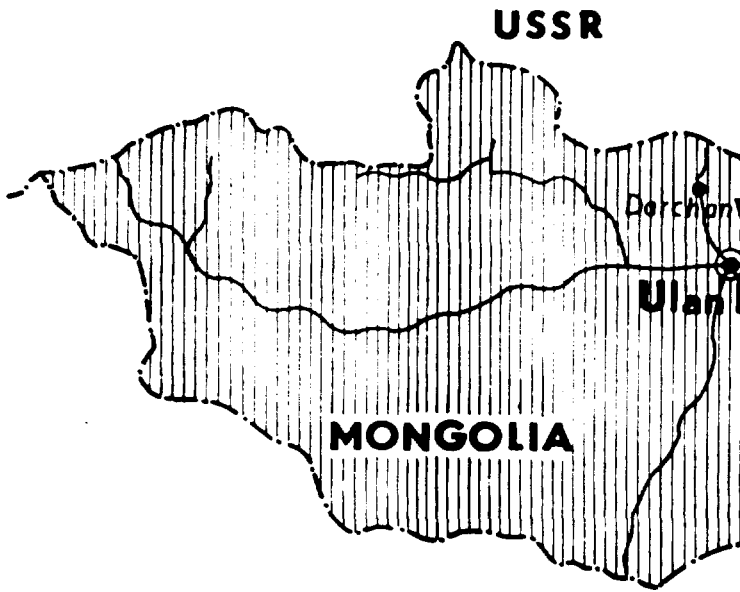
Cost item	Foreign currency	Local currency	Total
1. Direct materials and inputs	-----	4 712 842	4 712 842
2. Direct manpower: labour and staff	-----	829 752	829 752
3. Factory overhead costs			
3.1. Manpower costs	-----	694 885	694 885
3.2. Overhead materials	-----	3 010 014	3 010 014
3.3. Other factory overheads	-----	82 600	82 600
FACTORY COSTS	-----	9 330 033	9 330 033
4. Administrative overhead costs			
4.1. Manpower costs	-----	523 224	523 224
4.2. Other administrative overheads	-----	75 000	75 000
OPERATING COSTS	-----	9 928 317	9 928 317
5. Depreciation	-----	698 200	698 200
TOTAL PRODUCTION OR MANUFACTURING COSTS	-----	10 626 517	10 626 517

^aAt full capacity year 9

SCHEDULE 10-12
 FULL-COST SCHEDULE (WITH ALSO SCHEDULE 10-11)

YEAR	SCHEDULE 10-11		FULL-COST SCHEDULE	
	6	7	8	9
PRODUC. PROGRAMME	50%	75%	85%	100%
LC = TC	LC = TC	LC = TC	LC = TC	LC = TC
1. DIRECT MATER.	2293421	3534632	4477200	4712842
2. DIRECT LABOR	414076	622314	788264	824752
3. FACTORY OVERH.	2248692	3073093	3633618	3747479
FACILITY COST	495989	7175041	8597083	9330093
4. ADMIN. STR. COSTS	598224	5432220	598224	598224
OPERATING COSTS	5535213	4743265	4497507	4226314
5. DEPRECIATION	598200	698200	698200	698200
TOTAL PROD. COSTS	6253413	8471465	10195307	10626517
				10626517

**CENTRAL ASIAN AREA WITH OUTLINE
OF MONGOLIA AND LOCALIZATION
OF ULAN BATOR**



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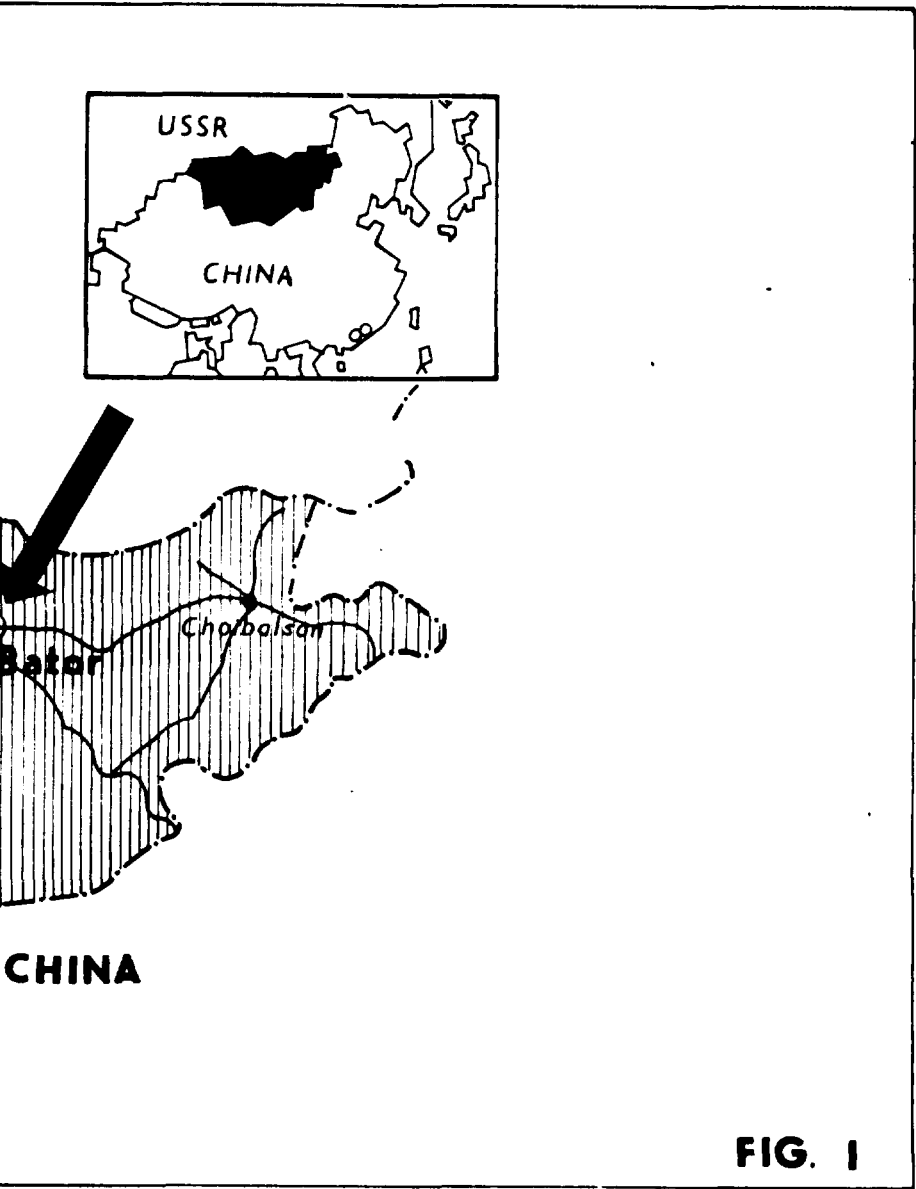
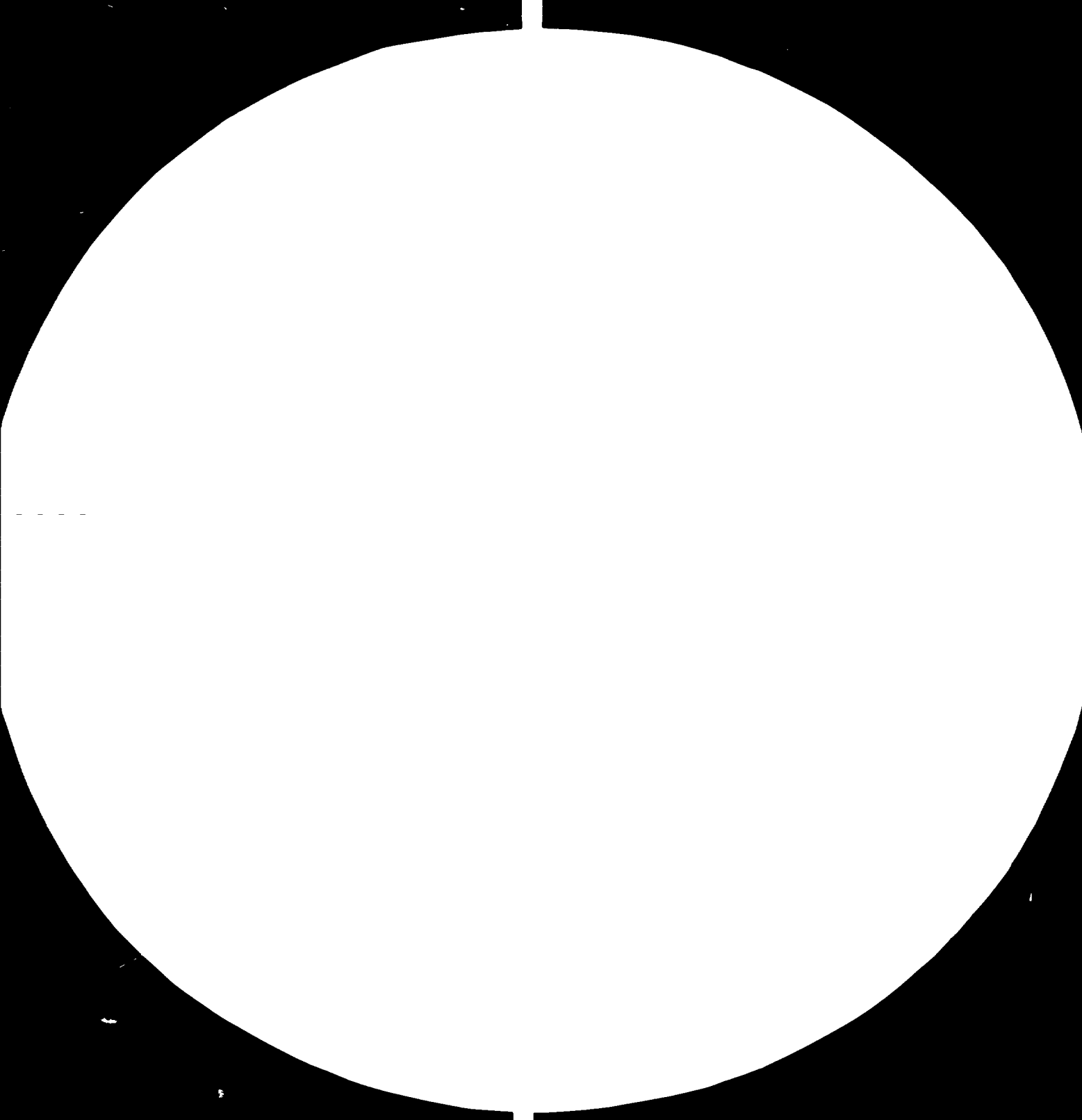


FIG. 1





28 25



1.25

A resolution test chart pattern for 1.25, consisting of two groups of five horizontal and five vertical lines, with a total of ten lines in each group.

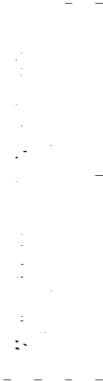
1.4

A resolution test chart pattern for 1.4, consisting of two groups of five horizontal and five vertical lines, with a total of ten lines in each group.

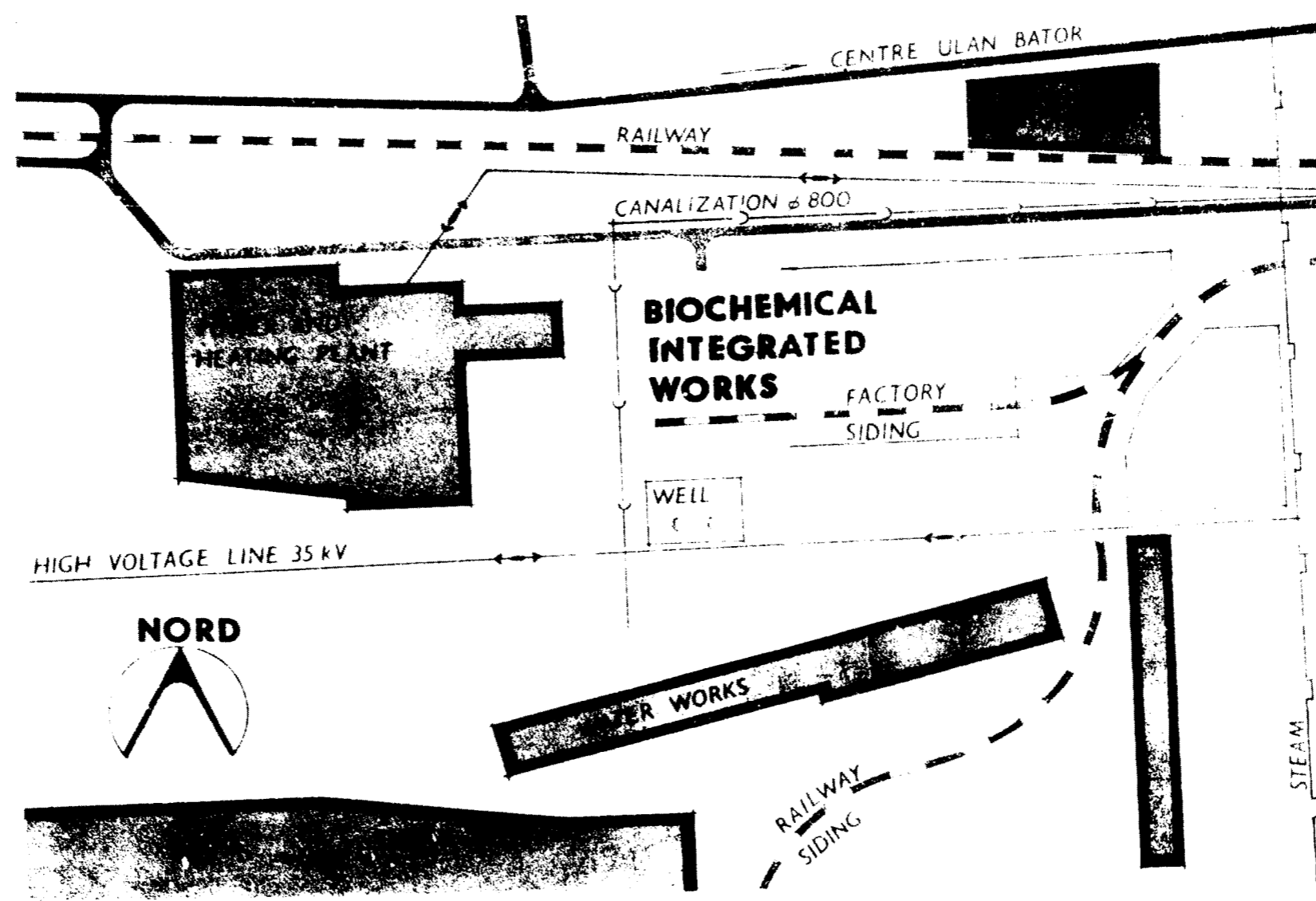
1.6

A resolution test chart pattern for 1.6, consisting of two groups of five horizontal and five vertical lines, with a total of ten lines in each group.

1.8

A resolution test chart pattern for 1.8, consisting of two groups of five horizontal and five vertical lines, with a total of ten lines in each group.

DETAIL OF LOCALIZATION OF ULAN BATOR



1 : 10 000

FIG. II

SOME FIGURES
OF THIS DOCUMENT
ARE TOO LARGE
FOR MICROFICHING
AND WILL NOT
BE PHOTOGRAPHED.

PILOT PLANT - GROUND FLOOR ± 0

/ANNEX TO FIG. IV/

- | | |
|--|------------------------------------|
| 01 - LIFT | 020 - FINAL PRODUCTS STORE |
| 02 - STAIRCASE | 021 - VESTIBULE /BALI/ |
| 03 - TRAF0 | 022 - AKUBATTERIES |
| 04 - COMPRESSED AIR STATION | 023 - CHARGING |
| 05 - COOLED STORE | 024 - EXPEDITION |
| 06 - THAWING PLACE | 025 - WC |
| 07 - ORGANIC SOLVENTS PUMP-STATION | 026 - LIFT |
| 08 - LIFT | 027 - STAIRCASE |
| 09 - STAIRCASE | 028 - PLATFORM |
| 010 - WC | 029 - WC |
| 011 - STORE | 030 - SLOAC - ROOM |
| 012 - COOLING MACHINERY | 031 - LAVATORY |
| 013 - PASSAGE | 032 - LAVATORY |
| 014 - COOLING MACHINERY | 033 - SLOAC - ROOM |
| 015 - MACHINERY ROOM FOR STEAM AND HOT WATER PREPARATION | 034 - WC |
| 016 - STORE KEEPER | 035 - STORE |
| 017 - CHEMICAL STORE | 036 - STORE |
| 018 - TUBES AND VIALS WASHING | 037 - MAINTENANCE WRESHOP |
| 019 - SUBSTANCES, PACKING MATERIAL, GLASS-WARE | 038 - LIME STORE |
| | 039 - NEUTRALIZATION POINT STATION |

PILOT PLANT - FLOOR +4,20

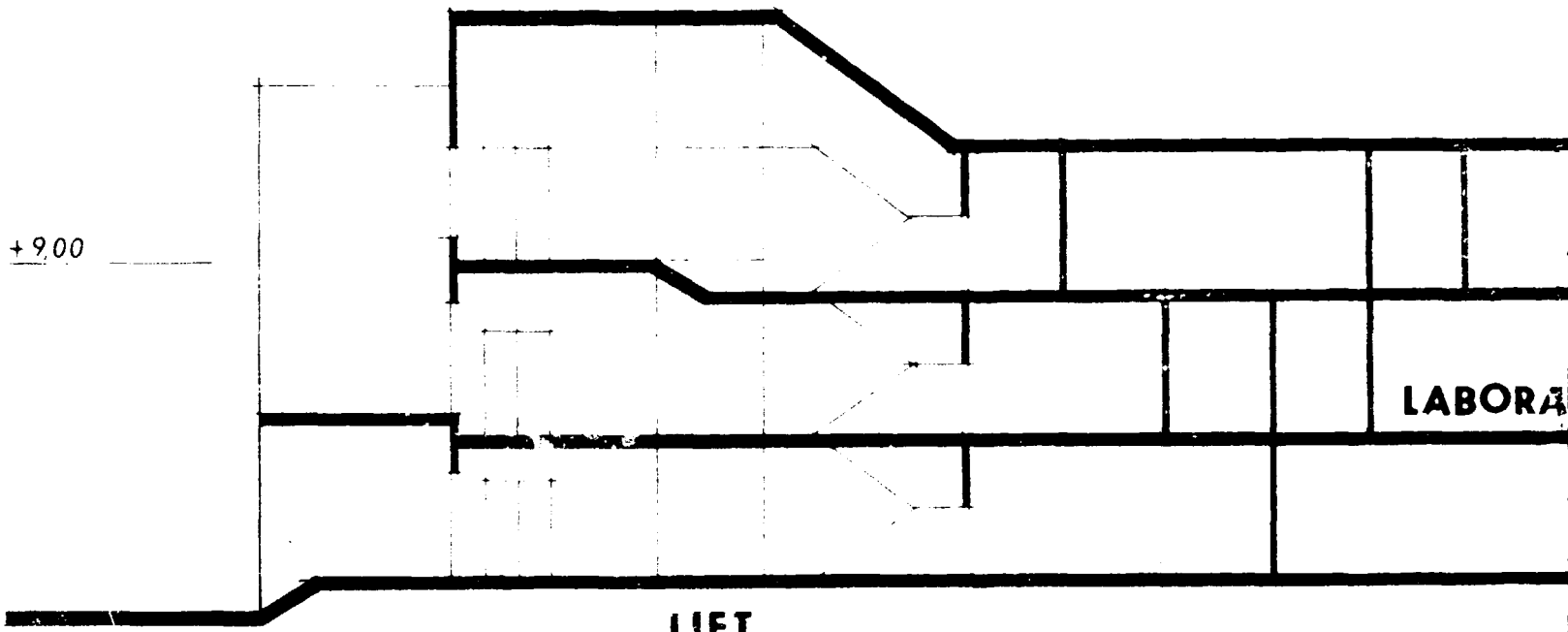
/ANNEX TO FIG.V/

101 - LIFT	124 - FOREMAN
102 - STAIRCASE	125 - PREPARATION OF BACTAC
103 - ELECTRICITY POINT	126 - STERILE BOX
104 - AIR CONDITIONER	127 - SANITARY PASSAGE
105 - BIOCHEMICAL PRODUCTION	128 - INCUBATORS
106 - LIFT	129 - LIQUIDATION OF INCUBATORS
107 - WC	130 - COOLING BOX
108 - STAIRCASE	131 - SAMPLES
109 - FOREMAN	132 - COOLING BOX
110 - STORE	133 - OFFICE
111 - COOLING BOX	134 - OFFICE
112 - COOLING BOX	135 - WC
113 - INTER STORE	136 - IMPURIFIED GLASS-WARE
114 - TABLETS	137 - SCULLERY
115 - TABLETS	138 - PURE GLASS-WARE
116 - PACKING	139 - CHEMICAL GLASS STORE
117 - WC	140 - STUDY ROOM
118 - LIFT	141 - STUDY ROOM
119 - STAIRCASE	142 - BIOCHEMICAL LABORATORY
120 - PACKING	143 - CHEMICAL LABORATORY
121 - STERILE PRODUCTION	144 - WEIGHTING ROOM
122 - SANITARY PASSAGE	145 - APPARATUS STORE
123 - SOLUTION PREPARATION	146 - ANALYTICAL PHYSICAL LABORATORY

PILOT PLANT - FLOOR +8,40 /+900/
/ANNEX TO FIG.VI/

201 - LIFT	217 - VIVARIUM WITH THERMOSTATS
202 - STAIRCASE	218 - BACTERIOLOGICAL DEPT.
203 - ELECTRICITY POINT	219 - CHEMICAL DEPT.
204 - AIR CONDITIONER	220 - VIVARIUM WITH THERMOSTATS
205 - BIOCHEMICAL PRODUCTION	221 - WC
206 - LIFT	222 - OFFICE
207 - WC	223 - OFFICE
208 - STAIRCASE	224 - OFFICE
209 - FOREMAN	225 - OFFICE
210 - STORE	226 - OFFICE
211 - DEMI WATER	227 - STUDY ROOM
212 - LABORATORY CHIEF'S OFFICE	228 - LIBRARY
213 - SECRETARIAT	229 - PILOT PLANT CHIEF'S OFFICE
214 - OFFICE	230 - SECRETARIAT
215 - BIOCHEMICAL DEPT.	231 - REST ROOM
216 - VIVARIUM WITH THERMOSTATS	232 - KITCHEN

+9.00



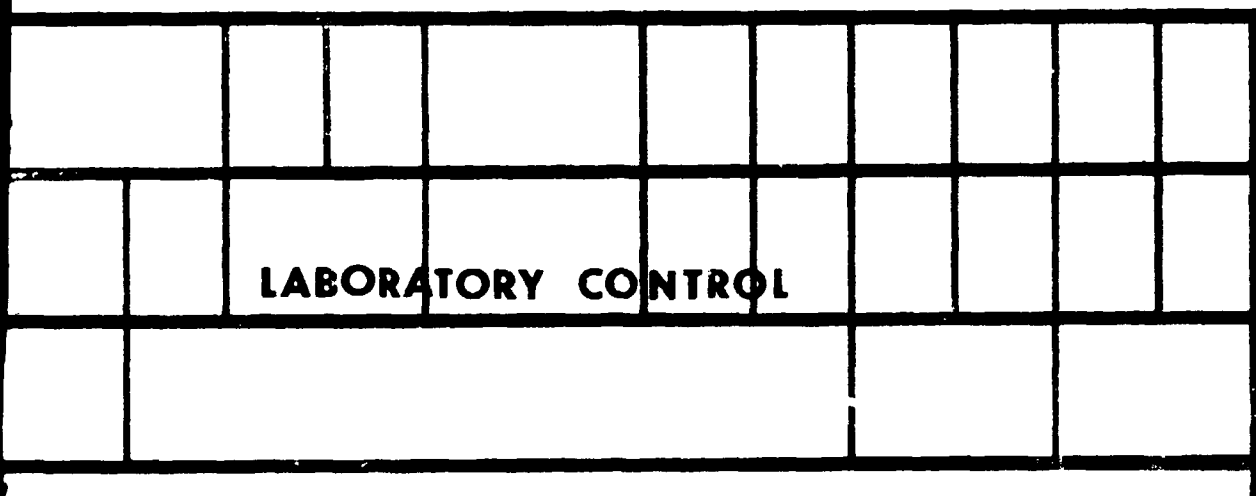
LABORATORY

LIFT

SECTION 1

SECTION

B-111



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SECTION 2

SECTIONAL VIEW II-II'

FIG. VII

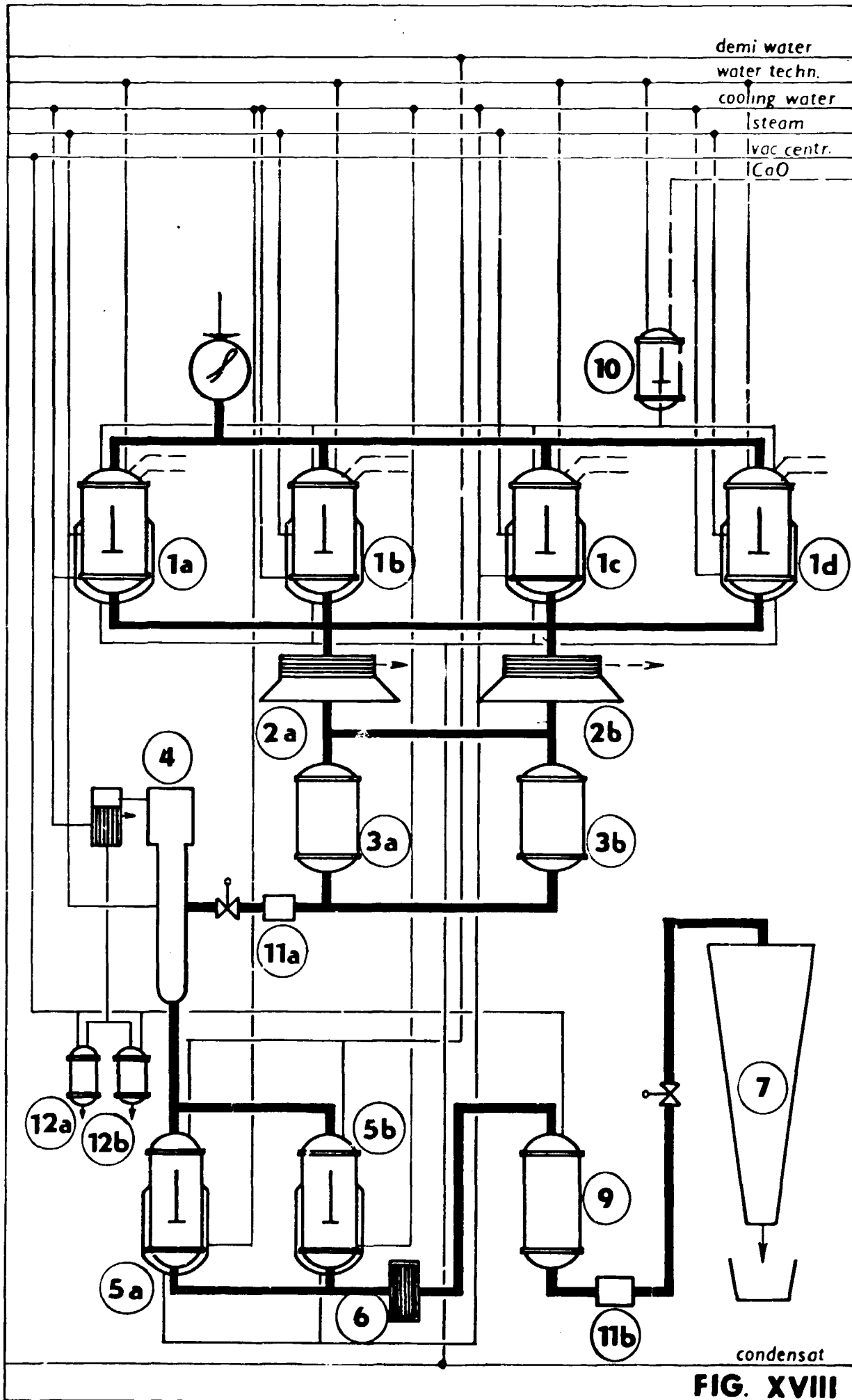


FIG. XVIII

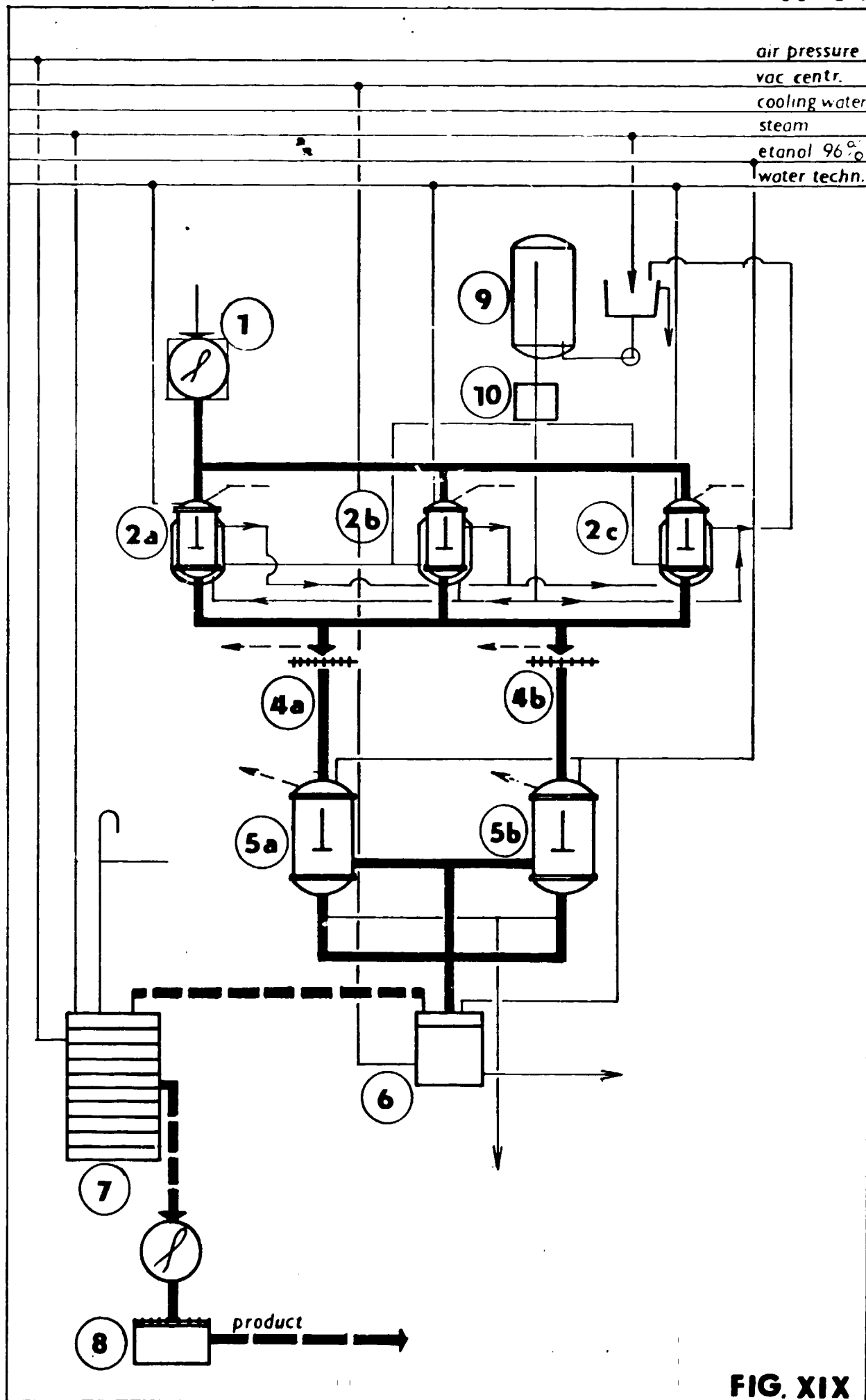


FIG. XIX

water techn.
cooling water
vac centr.

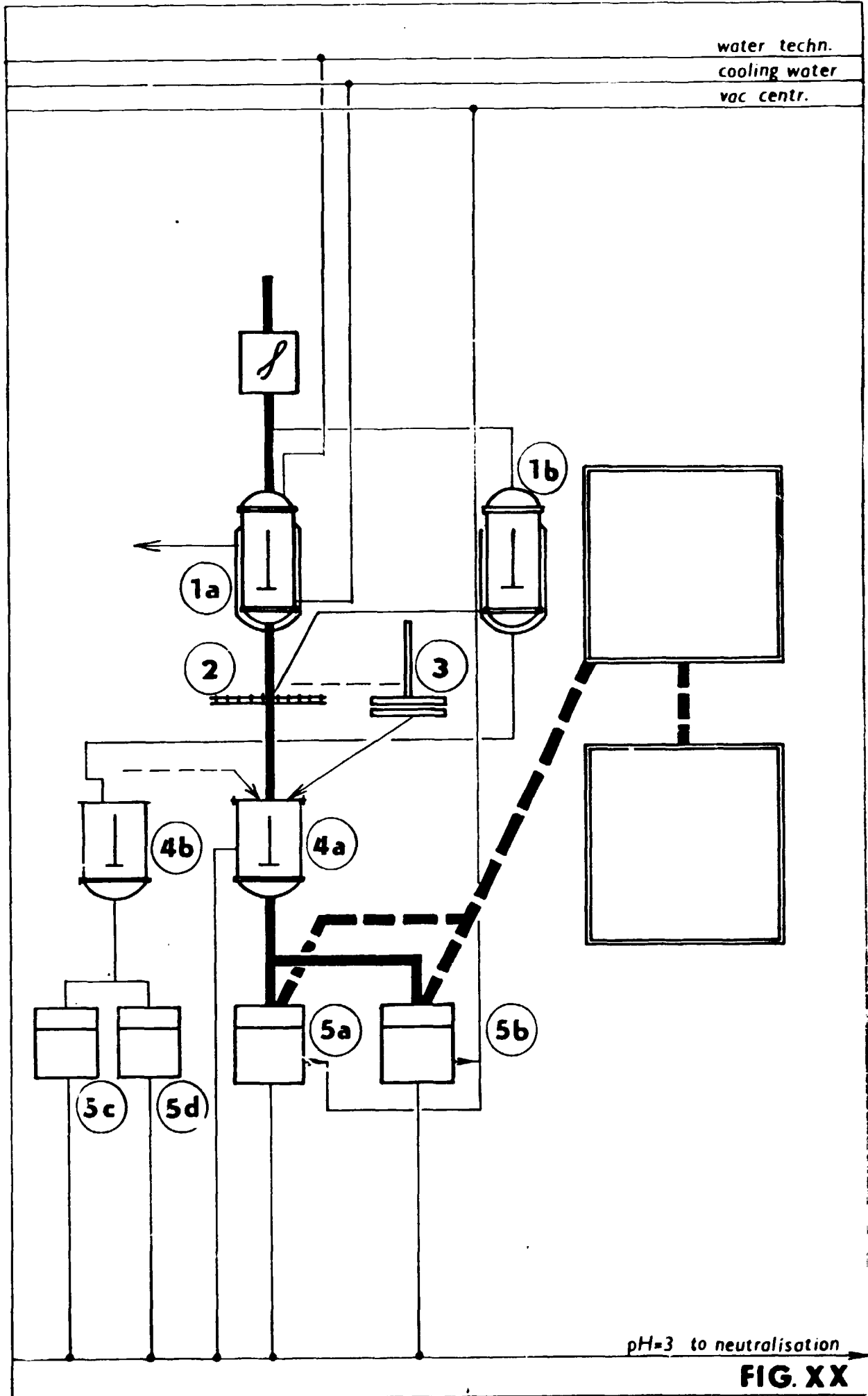
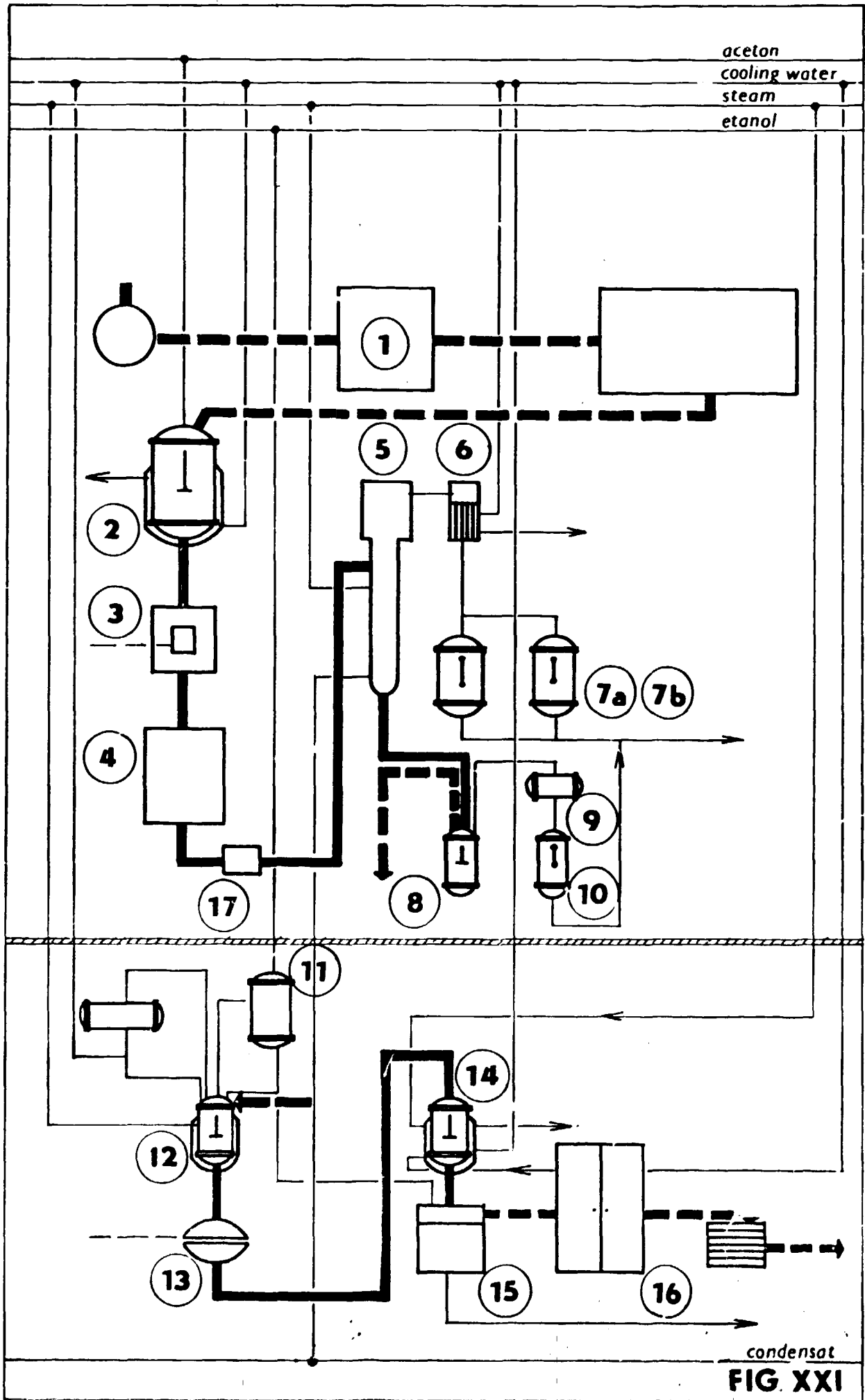


FIG. XX



condensat

FIG. XXI

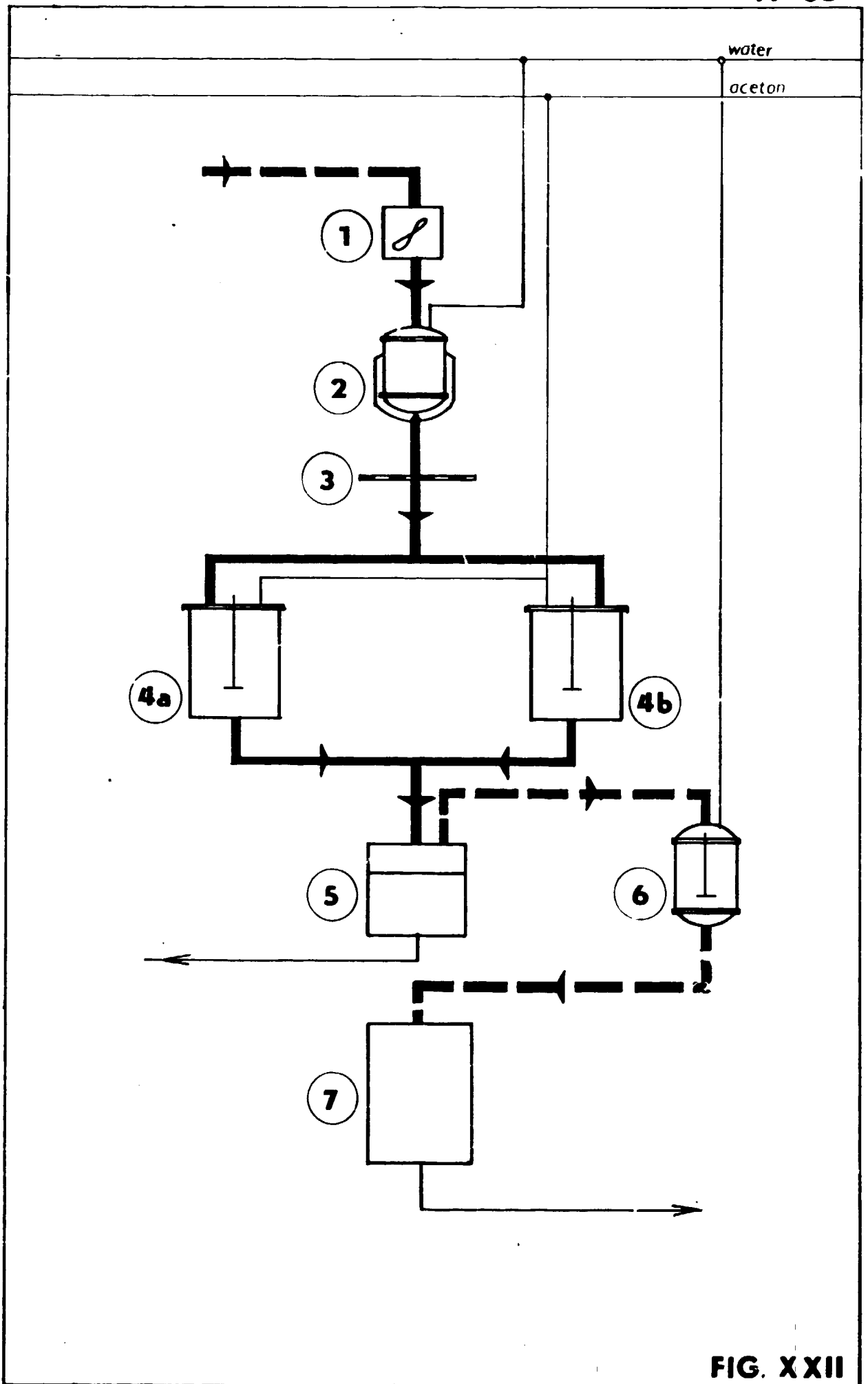


FIG. XXII

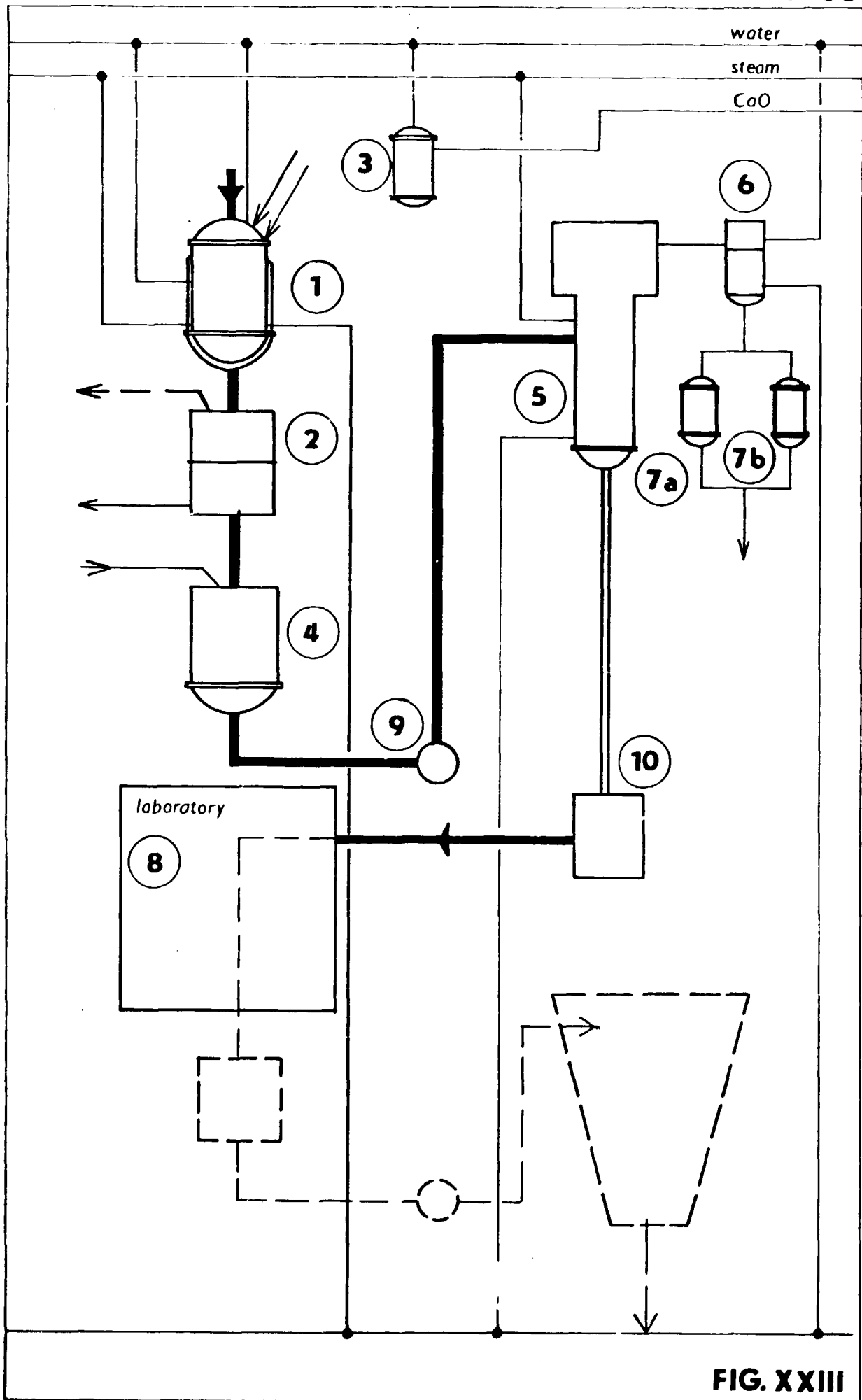


FIG. XXIII

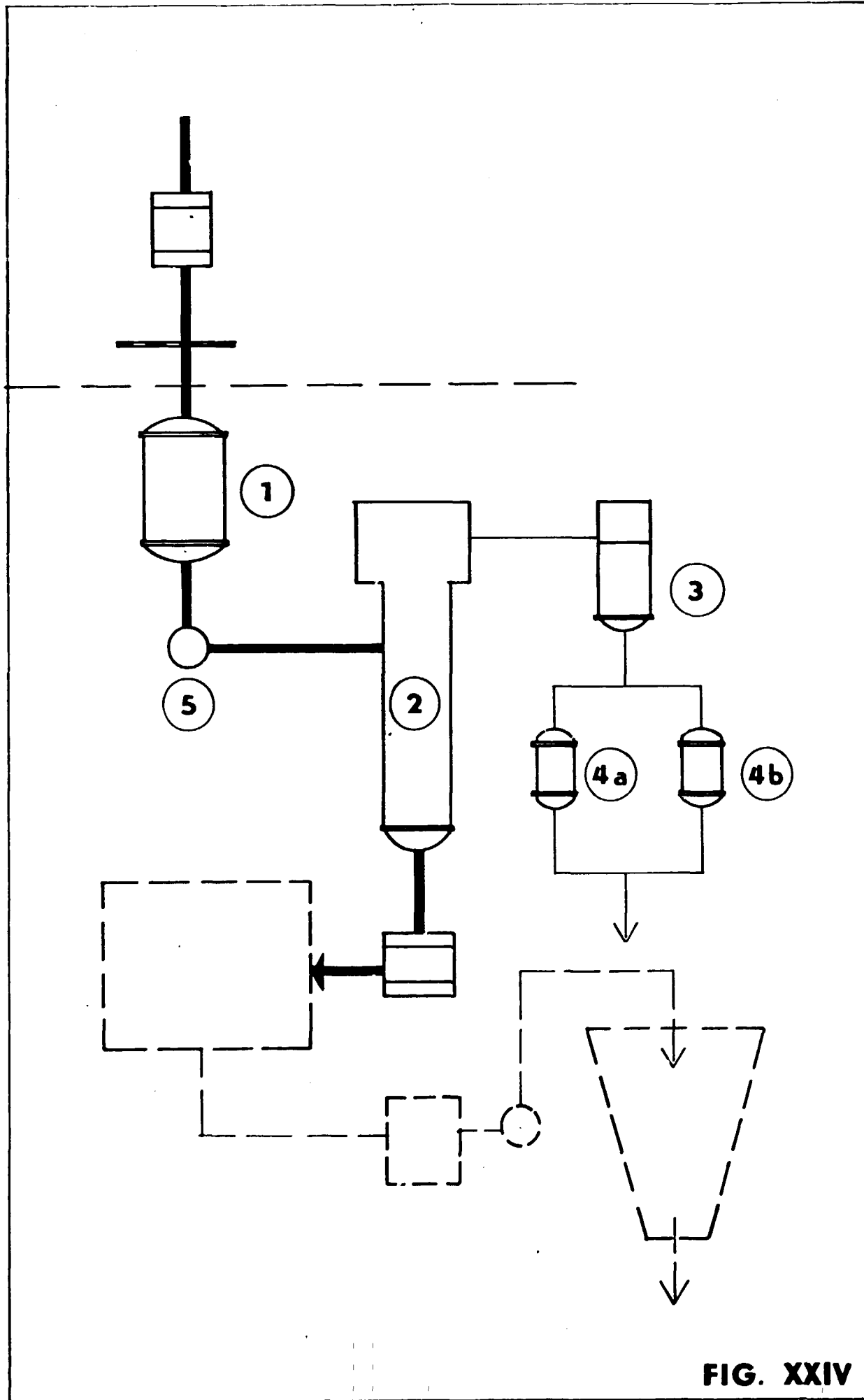


FIG. XXIV

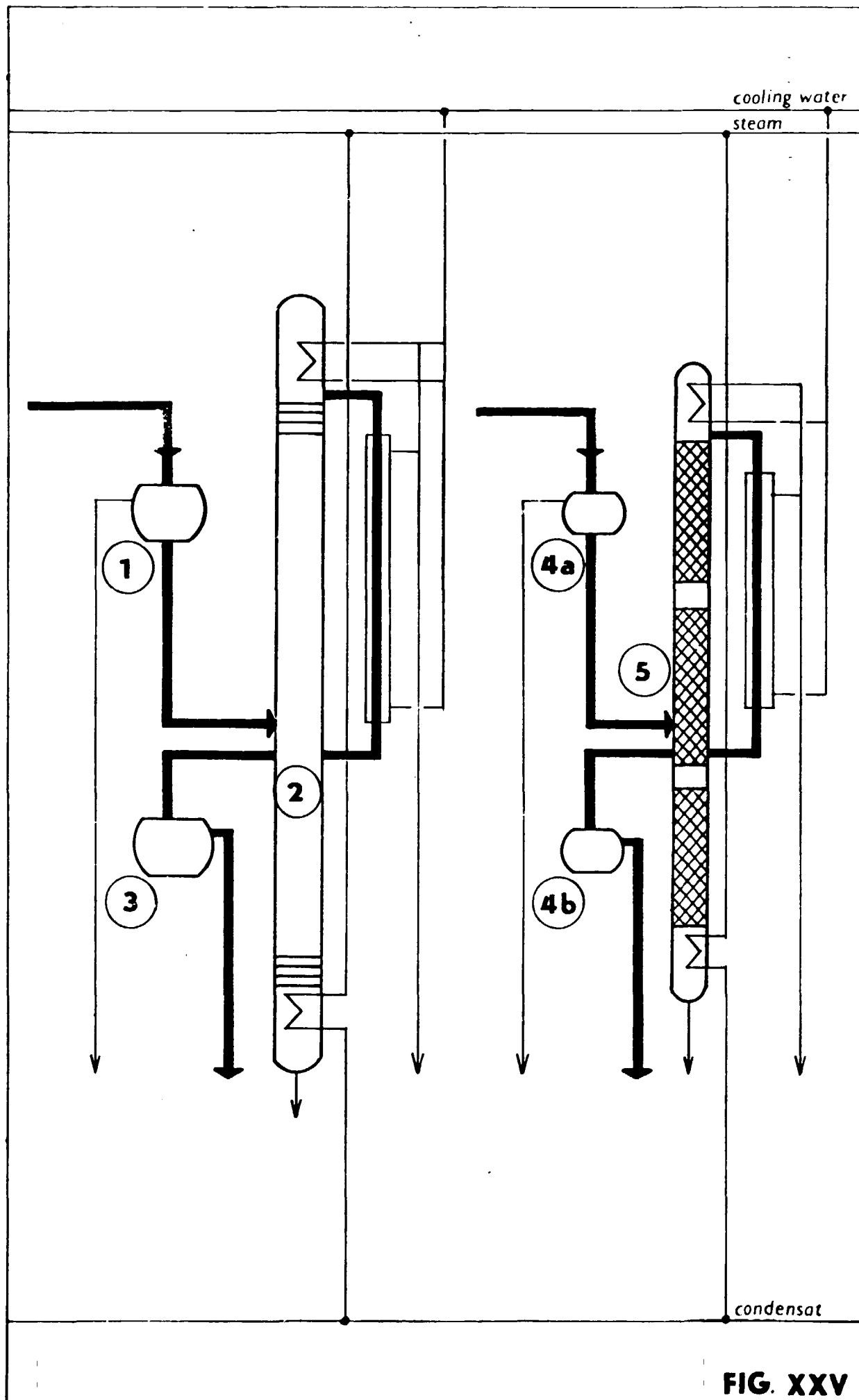


FIG. XXV

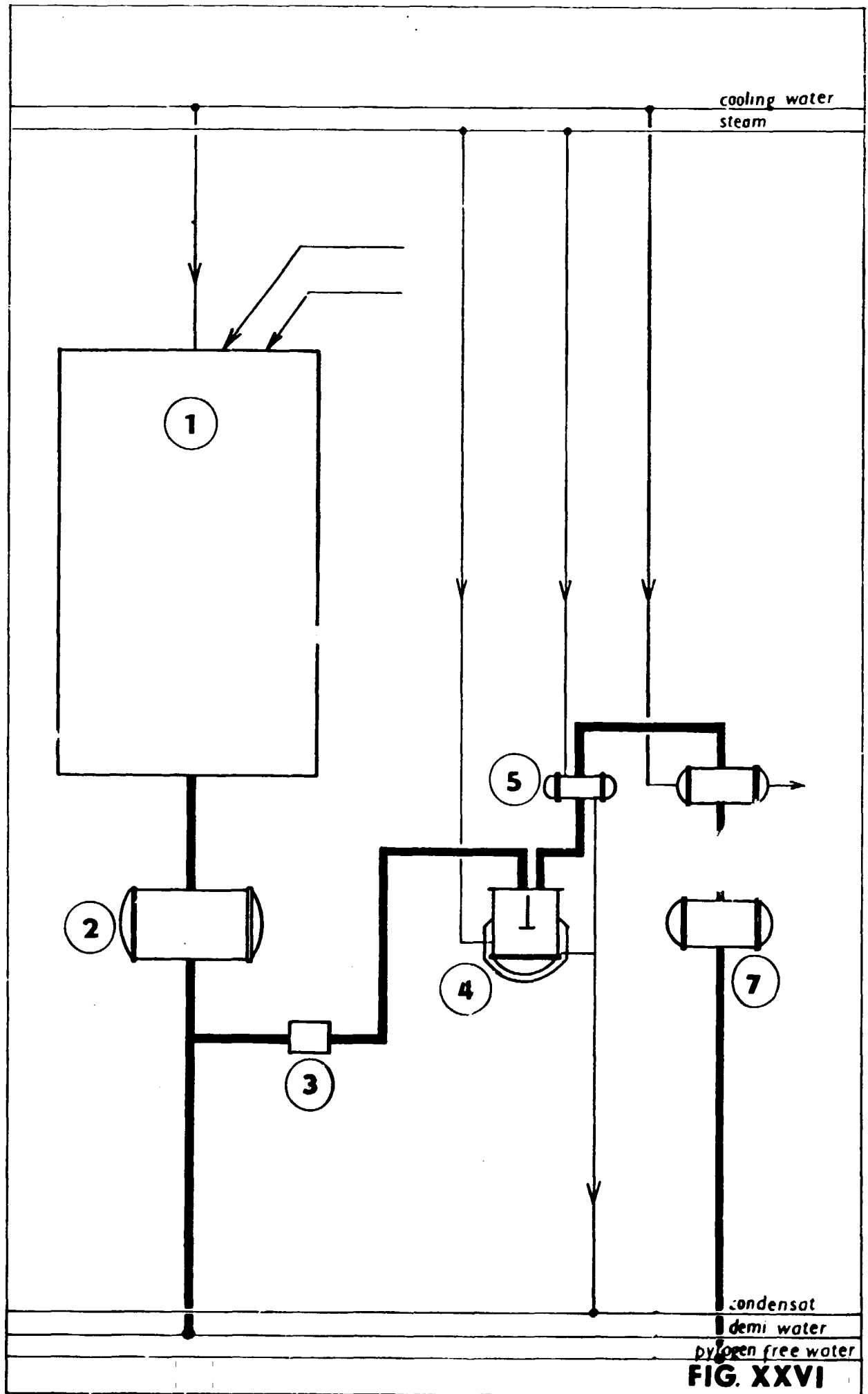


FIG. XXVI

215

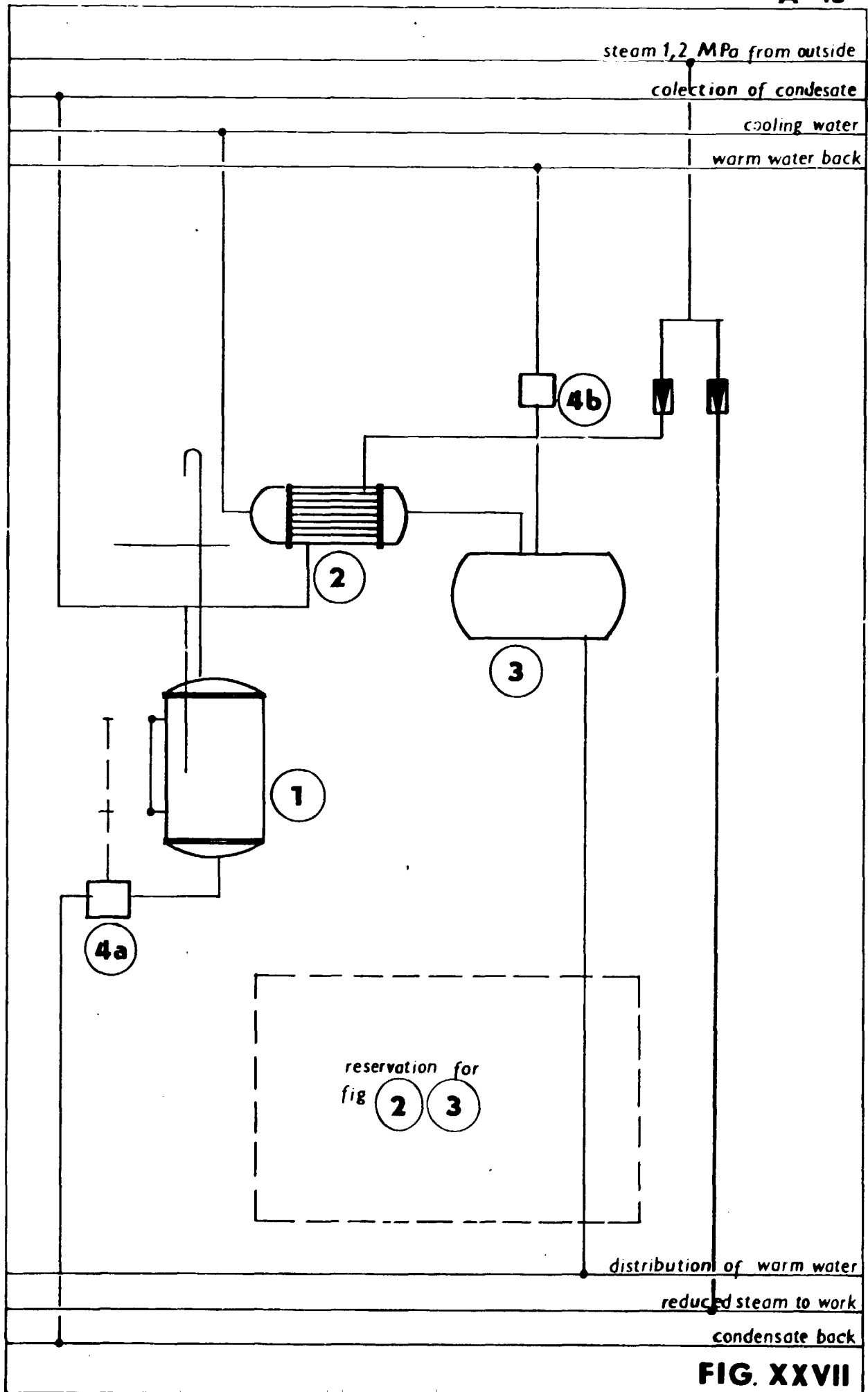


FIG. XXVII

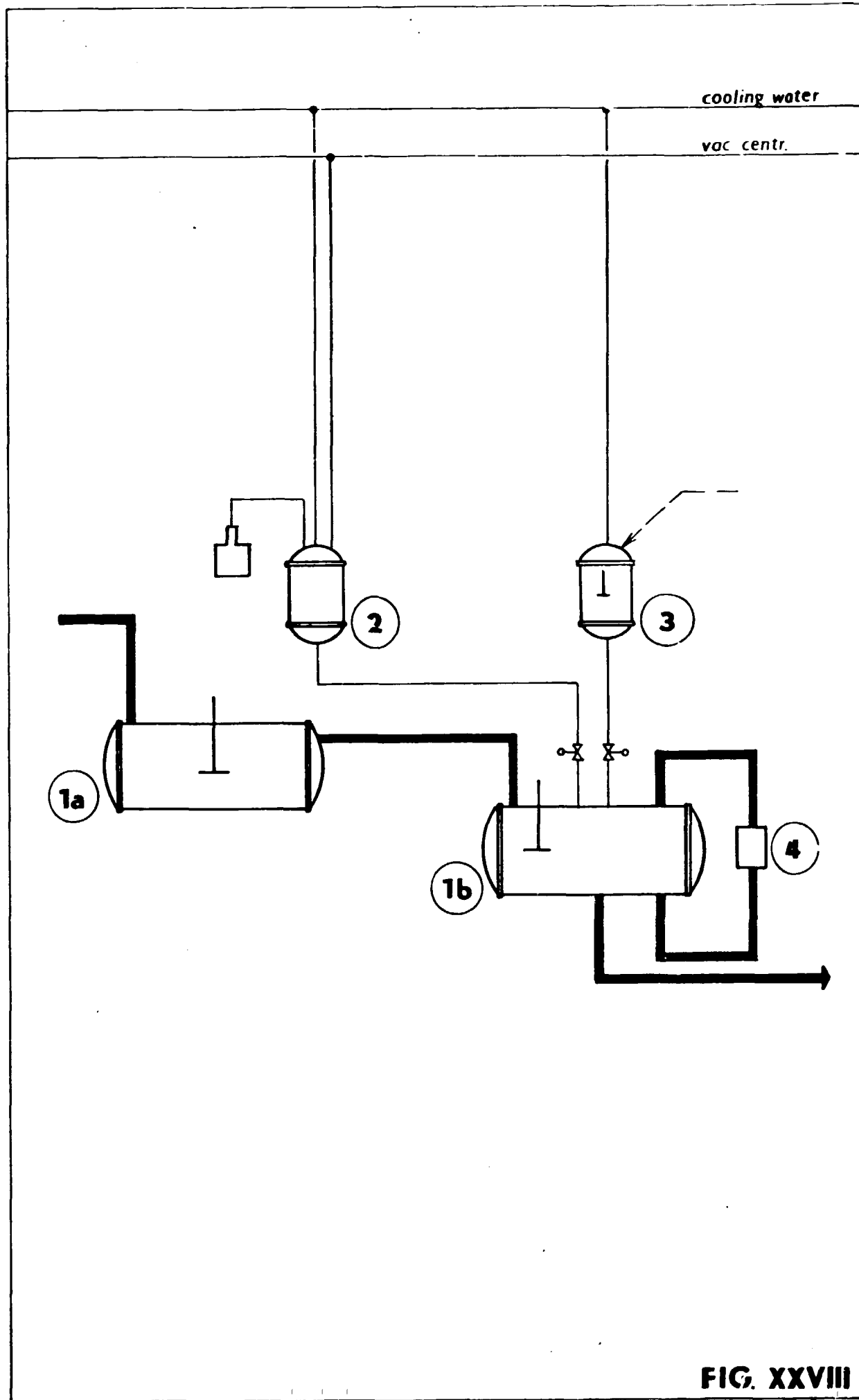


FIG. XXVIII

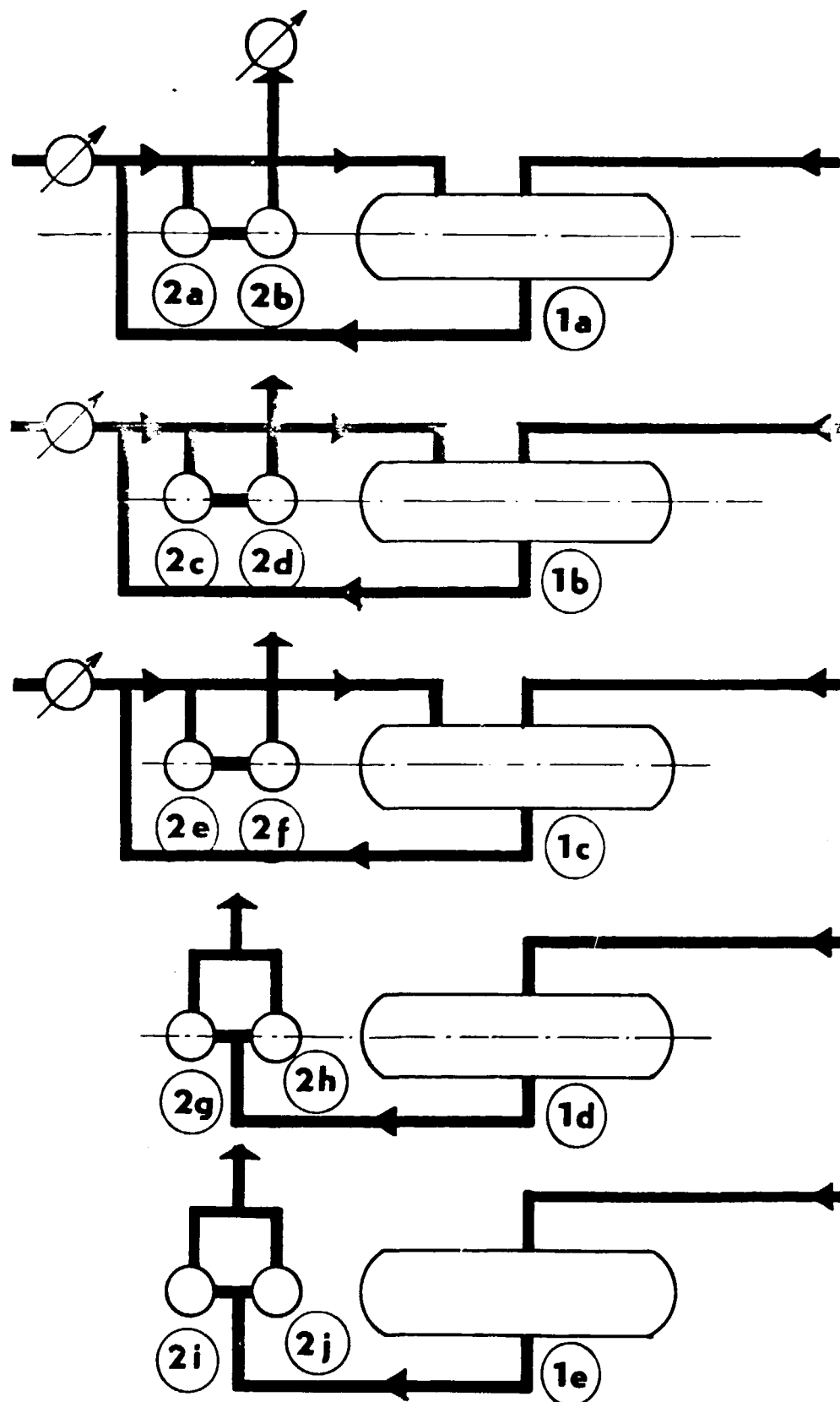


FIG. XXIX

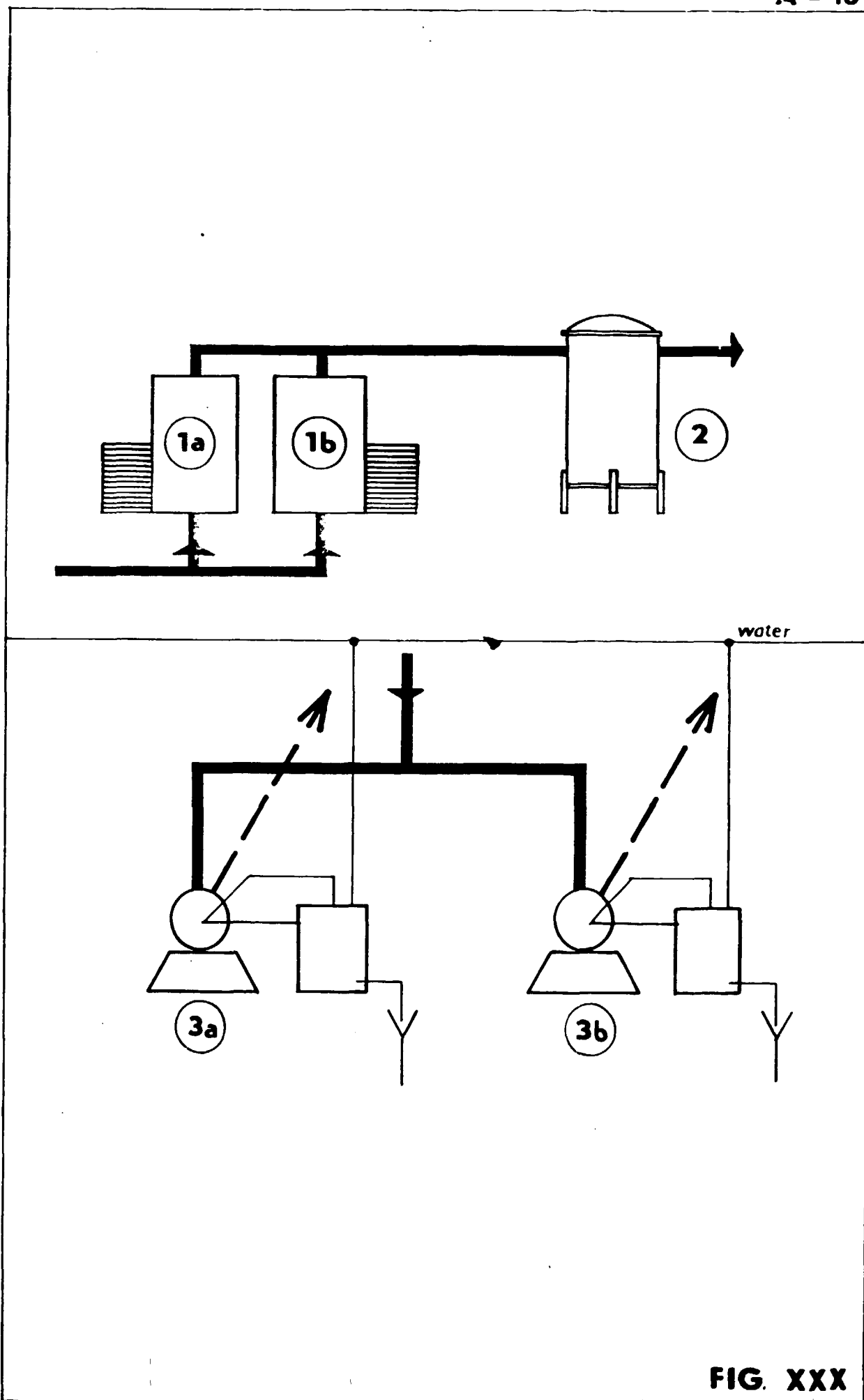


FIG. XXX

