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ECONOMY OF SCALE IN THE SUGAR INDUSTRY 1/

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I. INTRODUCTION

Although the question of economy of scale has been considered by many economists, especially since 1940 cf.(15), yet little has been published, so far, on the economy of scale in the cane sugar industry. However, since more and more developing countries, especially in Africa, are considering the setting up of local sugar production, it is of interest to investigate this problem from the theoretical point of view, but also by utilizing practical examples from territories having a reasonably developed sugar industry.

Historically there can be no hesitation in stating that the change over from a large number of small sugar factories to a small number of large sugar centrals has taken place almost everywhere.

This is clearly exemplified in <u>Figure I</u> which summarizes the historical evolution in LOUISIANA, MAURITIUS and SOUTH AFRICA. Other sugar producing territories have generally experienced the same trend which indicates that there is an economy of scale in the cane sugar industry.

It is proposed, in what follows, to consider the various factors that make up the total cost of production of a tonne of sugar, and to show how this cost of production decreases with an increase in production capacity.

It must be pointed out that the problem of effluents has been made more difficult since they are now concentrated at the few localities where the large sugar centrals have been erected. But modern techniques are presently available to reduce the environmental impact of these effluents, and hence the difficulty experienced for their disposal, as will be indicated later in the text.

The data which will be used, when considering the various items of cost, are derived mainly from the Mauritius Sugar Industry and although their relative importance may vary from one sugar country to another, it is felt, however, that the general trends and conclusions would apply to any cane sugar industry.

II. GROWING THE CANE

As a first approximation, it can be stated that the number of man hours per year required to grow one tonne of cane is not significantly related to the size of the acreage under cane, especially if we consider plantations of 500 hectares or more.

However large cane estates can use more mechanical implements for land preparation, fertilization, planting, herbicide treatment, cutting and loading which would not prove economical on very small fields of one or two hectares. Hence cultivation man hours per tonne of cane on these mechanized large estates can be decreased, although one should be aware that the mechanized cultivation costs are often not lower than that depending, in a large measure, on manual work, especially now that the cost of energy has increased spectacularly since 1973.

From the data obtained in Mauritius, where mechanization is not yet greatly utilized, it follows that cultivation cost per tonne of cane is approximately constant and relatively independent of size of acreage under cane. It should be stressed, however, that for very small fields, in Mauritius, the tonnage of cane produced per hectare (10 000m²) is much lower than that of large estates, in a large measure because of less thorough and competent agricultural husbandry. This is indicated in <u>Table 1</u>.

It must be pointed out, that, in some cane sugar producing territory, especially in TAIWAN, the cane produced per hectare, in small fields, is higher than what obtains in Mauritius.

There is a tendency, in many countries, for small planters to form co-operatives and, using more adequate methods on the larger acreage thus formed, to obtain better yields almost equivalent to the larger estates.

It can be concluded, bearing in mind this progressive improvement, that, in general, there is little economy of scale for cane cultivation and harvesting.

III. TRANSPORTING THE CANES

Let us assume that the cane fields form a circular area and that the sugar factory is located at the centre. This is the most efficient set up to minimize cane transport costs.

As the capacity of the factory increases, so must the field area to supply the necessary tonnage of cane. But simultaneously does the average distance of transport for the canes. This is indicated in <u>Table II</u> with a circular field area.

Cane estates are generally not circular, but rectangular in shape, with, hopefully, the factory at the geometric centre of the area. However this results in an increase in the average transport distance of canes to the mill and, <u>for a given</u> <u>area</u>, the more we depart from a square configuration towards an elongated rectangle, the more does the average transport distance increases. This is indicated in <u>Figure II</u>.

It must be pointed out that many cane sugar producing territories are narrow and long - cf. Queensland, the South African Natal belt, the Hawaiian coastal belt, etc, with the result that the average cane transport distances are longer there than would be the case for an equal area of square shape.

This factor should be borne in mind when developing a new region under cane and a square configuration should be favoured, as far as the geographical constraints would allow.

Cost of transport varies with distance, but there is a significant fixed cost, so that transporting cane over say 10 km cost about US \$2.22 per ton, while transporting over 1 km cost about US \$1.14. So that as you increase the distance by 10:1 you only increase the cost by about 2:1. <u>Table III</u> indicates cost of cane transport applying in Mauritius presently.

So that although the cost of transport of cane shows an inverse or diseconomy of scale with increasing capacity, yet in the total build up of cost of production of sugar, as will be indicated later in the text, it has not got a sufficient weight to neutralize the other factors which produce economy of scale, such as administrative charges, depreciation, insurance, etc.

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IV. PROCESSING THE CANE FOR SUGAR PRODUCTION

For a given factory capacity, it is fairly evident that under utilisation of this capacity will lead to increased milling (or processing) costs per tonne of cane. Similarly over utilisation, with rapid wear and heavy maintenance, will also lead to increased milling cost.

This point has been well covered by G.J. RYLAND (16), who also indicated that with increasing theoretical capacity, and with each factory working at its designed optimal capacity, we would have a general trend showing lowering of cost of production with increasing capacity, i.e. economy of scale.

This is indicated in <u>Figure III</u> which is adapted from Ryland (16).

We must now consider, in more details, the main items which added together build up the cost of processing.

(i) The first thing which is noticeable in processing is that the number of personnel employed does not increase in direct proportion to the capacity of the factory. The same remark applies to the administrative personnel and the direct changes associated with them.

The cost of these employees increase fairly slowly with increasing capacity and, as a first approximation, we can say that they increase as the 2/10 th power of the capacity.

Thus if P is the cost of employees and C the capacity of the factory we can write : $\frac{P_1}{P_2} = \frac{C_1^{0.2}}{C_2^{0.2}}$ and <u>Table IV</u>

indicates how these changes vary with increasing capacity.

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(ii) The second point which should be stressed, and which has been recognized in many industries cf. (3), (7), (10), is that the capital cost of a raw sugar factory varies, approximately, as the 7/10 th power of the capacity. This relation has been checked with some sugar factories in Mauritius and appears to be a fair approximation for the sugar industry. It is indicated in <u>Figure IV</u> and although conditions may vary from one sugar producing country to another, yet the curve of Figure IV should be representative of the general trend for raw cane sugar factories.

Hence, in the cost build up of sugar production, items like depreciation, repairs and maintenance, machinery and plant insurance, etc, which are directly proportional to the replacement cost of the equipment, will vary as the 7_{10}^{10} th power of the capacity of such equipment.

For those interested in more detailed data, Appendix A gives a nomenclature of the main items of three typical raw sugar factories of 120, 175 and 250 tonne cane per hour with indicative prices which were representative of conditions obtaining in Mauritius in 1973. The costs are expressed in Mauritian Rupees which were worth about US \$0.18 per rupee at that time.

It has been a frequent and unfortunate feature, in the sugar industry, to duplicate small size equipments when planning an enlargement of capacity of factories. References (5) and (11) give a more rational approach to this problem. The conclusion to be drawn is that with proper planning a modern factory can show significant economy of scale and substantial reduction in the number of personnel employed for its proper operation and maintenance. (iii) The other items of the cost of production of sugar can be considered, as a first approximation, to vary directly with the capacity of the factory.

To recapitulate there are three categories of items in the cost structure of sugar production :

(a) Factory and Administrative Personnel expenses which will vary as the 2/10 th power of the capacity of the factory.

(b) Depreciation, repairs and maintenance, and plant insurance which will vary as the $\frac{7}{10}$ th power of the capacity of the factory.

(c) All other items, which have been assumed to vary in direct proportion to the capacity of the factory.

V. THE END RESULTS

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It is now possible, bearing in mind the data and assumption made in Sections II, III and IV, to construct a table, with about 15 individual items of cost, which will indicate how the final cost of production of a tonne of cane (or of a tonne of sugar) varies with the capacity of the sugar estate. This data is contained in <u>Table V</u>. It has been established on the basis of the tonne of cane, as the sugar content of the cane varies appreciably from one region to another and, indeed, from one season to another. Once the cost per tonne of cane has been established, it is easy to translate this cost into its equivalent per tonne of sugar, utilising the average sugar extraction prevailing in the particular factory area concerned. The figures in Table V, which are based on conditions generally obtaining in Mauritius, assume that the tonnage of cane produced per hectare is 76 tonnes and that the duration of the crushing campaign is about 130 working days. This data will have to be corrected when applied to specific areas where the productivity of cane fields and duration of crop are different. But it is believed that the general conclusion will still apply, demonstrating economy of scale, although in varying degrees.

The average cost of raw sugar production per tonne of cane was approximately US \$30 in 1975 in Mauritius. Instead of using this figure which varies and inflates from year to year, Table 5 utilises the index cost figure of 100 for a sugar estate having a capacity of 100 TCH. And cost figures for larger capacities are expressed in relation to this 100 index cost figure.

In order not to make Table V too complicated the transport cost of cane has been envisaged for only two specific configurations of cane areas, namely the optimal circular configuration and the rectangular configuration with a 5:l side ratio.

The cost of transport of labour and of sugar has been assumed to vary directly with capacity. This applied, approximately, to the Mauritian factories considered, but would have to be reviewed for other conditions.

For the cultivation and harvesting section, it has not been possible to obtain a separate figure for depreciation, as some items, like transport and other charges, already incorporated an element of depreciation in their cost. No account has been taken of milling tax and sugar export tax; also the insurance premium paid against cyclones and droughts has not been considered. So that the cost index indicated in Table V is representative of ex factory cost (plus transport to the central sugar warehouse) but without any taxes or levies.

Notwithstanding the above mentioned limitations, the general conclusion to be derived from Table 5 is that as the capacity increases from 1 to 5, the total cost of production increases from 1 to about 4, that is the unit cost of production per tonne of cane decreases from 1 to about 0.82, as indicated in Figure V.

VI. THE ENVIRONMENTAL IMPACT

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This subject has been well covered in the recent literature, cf (1), (2), (4), (6) and (8), but it is proposed to say a few words on the concentration of effluents which derive from the larger sugar centrals.

These effluents can be divided into three main items :

- (i) Acid condensate surplus water,
- (ii) Cane wash water,
- (iii) Fly ash and smut.

(i) It should be noted that as the capacity of the factory increases, and also, as steam economy improves with more advanced technology, the volume of surplus acid condensates will increase significantly as indice d in <u>Figure VI</u>. Thus for a 100 TCH factory, with limited technology, the surplus may be around 5.3 tons of acid condensate per hour, while for a 500 TCH factory, with improved technology, the surplus could well amount to 114.5 tons of acid condensate per hour. The modern central can thus be regarded as a source of water which, with limited but adequcte treatment, can be used for irrigation and domestic purposes.

The acid condensate surplus is relatively hot (about 90°C) and its dissolved oxygen content is thus very low. Its BOD content may be as high as 400 ppm, but with proper check of sugar entrainment or carry over, it should be lower than the 50 ppm acceptable limit. Proper cooling and aeration are generally sufficient to render usable the acid condensate.

Condenser cooling waters should pose no real effluent problem if they are used in closed circuit, through a suitable cooling pond. This is the standard modern procedure and the old "once through" system, (with its very high consumption of 700 to 1 250 tons of cooling water per hour for a 100 TCH factory) should not be encouraged.

(ii) With the advent of mechanical harvesting, some factories require cane washing operations which consumes very large volume of water e.g. 500 tons per hour for a 100 TCH factory. This effluent carries in suspension large amount of soil and dissolved soluble organic and inorganic substances. A figure of 3 000 ppm total solids in cane wash water is average and its BOD content can vary between 300 and 1 000 ppm. - 11 -

This water constitutes the most serious pollutional load in raw cane sugar manufacture, and generally calls for fairly sophisticated treatment which includes screening, settling and extended aeration cf (1) and (2).

(iii) Steam boiler stack emission of fly ash and smut generally reach the level of 5 000 mg per normal m^3 of flue gases - cf (4) and (12). It represents, roughly, about 500 kg of ash per hour for a 100 TCH factory, which can prove a real nuisance for those living in the vicinity of the factory on the lee side.

Fortunately there are now centrifugal dry collectors and impingement type wet scrubbers which are fairly efficient and can reduce the average boiler stack emission of 5 000 mg per m^3 to 200 mg per m^3 , or less. This is considered, quite rightly, to be highly acceptable by most sanitary authorities.

VII. SOCIAL AND ECONOMIC IMPACT

The influence, in the social and economic field, of a large sugar central, can prove beneficial, given an efficient organisation.

Sugar production is an agro-industrial activity that can prove a useful transition channel for the change over of purely agricultural workers to industrial operatives. It has a number of useful linkages like sugar equipment manufacture and repairs, transportation equipment repairs, agricultural equipment manufacture and repairs, fertilizer and pesticide production - or at least mixing plants, that will mean job creation and economic growth. The by-products of the sugar industry can be substantial adjuncts to improve the economy of the community. Thus the utilization of bagasse for the production of particle board and of molasses for the production of alcohol, is a natural development of the sugar industry. In most cases a large sugar central has a significant surplus of electricity which it can supply to the local grid at a competitive price per kWhr.

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The specialists employed by the sugar estate - agronomists, engineers, chemists, accountants, etc can be a useful nucleus that will act as a catalyst to activate the social and economic development of the community.

J.M. PATURAU.

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		NT NINT NATIVITIAN	SULTANT NT VALVA	
FIELD AREA	AVERAGE LABOUR REQUIREMENT	CANE PRODUCED	PRO DUCTIVITY	INDEX OF LABOUR COST PER TONNE
(Hectares)	(Man per hectare)	(Tonne Cane per hectare)	(Tonne Cane per worker)	OF CANE
T	0.70	39	56	100
5	0.65	43	66	85
50	0.60	56	93	60
500	0.66	73	TTT	50
1 000	0•67	75	112	50
2 500	0.68	76	211	•
5 000	0.68	76	112	50

CANE CULTIVATION DATA (IN MAURITIUS)

TABLE I

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TABLE II

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	HOW TRANSPORT DISTANCE		INCREASES WITH	FOR CANES INCREASES WITH FACTORY CAPACITY	21
CAPACITY OF FACTORY (Tonne Cane per hour)	CANE TONNAGE FÓR A 130 DAYS CROF (tonnes)	ACREAGE REQUIRED AT 76 T.C. per hectare (hectares)	GROSS ACREAGE 120% (hectares)	RADIUS OF FIELD (km)	AVERAGE TRANSPORT DISTANCE (km)
100	286 000	3 763	4 516	3.79	1.90
200	572 000	7 526	9 032	5.36	2 -68
90 00	858 000	11 289	13 548	6.57	- 1 67•£
400	1 144 000	15 052	18 064	7 • 59	3 .8 0
500	1 430 000	18 815	22 580	8.48	4.24

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TABLE III

COST OF CANE TRANSPORT (PER TONNE OF CANE)

N. A.

t

COST (in US \$ per tonne)	1.14	1.26	1.38	1.50	1.62	1.74	1.86	1.98	2.10	2.22
DISTANCE (in km)	1	Ŋ	ري ا	4	ſ	6	7	8	6	10

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TABLE IV

WAGES AND ADMINISTRATIVE CHARGES VARIATIONS WITH CAPACITY

VCOMPARE OF VMTAAA		
NALAVITI VE FALINI	INDEX OF WAGE	INDEX OF WAGES AND ADMINISTRATIVE CHARGES
(Tonne Cane per Hour)	TOTAL	PER TONNE OF CANE
100	100	100
200	115	57.5
300	125	4ī.7
400	132	33.0
500	138	27.6

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TABLE V

OF RAW SUGAR VS. CAPACITY OF SUGAR FACTORY **PRODUCTION H**O COST

	I T E M S		COST INDE	COST INDEX PER TONNE OF CANE	OF CANE	
	For Typical Capacity in Tonne Cane/Hr 1 A. <u>CULTIVATION & HARVESTING</u>	100 TCH	200 TCH	300 TCH	400 TCH	500 TCH
ч.,	Wages and Salaries (Varies as Capacity) Sumlies and Other Charges (Varies as	35 • 92	35 • 92	35 • 92	35 •92	35 • 92
	y) tof Canes (Ontimal t	19.00	19.00	19.00	19.00	19.00
3bis A	of Land) (5:1 Rectangular C Other Transnort (ma	5•53 (6•03)	5 . 94 (6.48)	6.27 (6.48)	6.54 (7.13)	6.77 (7.38)
י שרי	Capacity) Administration and Overhead (Varies as	5.00	5.00	5.00	5.00	5.00
	Capacity 0.2) Renairs and Maintenance (Varies as Canacity	7.35	4.22	3.05	2.43	2.03
- 2		1.22	66•0	0.88	0.31	0.75
	ب	1.19	76.0	0.86	0.79	0.73
•	aries as Capacity 0.7)	0.43	0.35	0.31	0.28	0.26
• Ծ	B. <u>PROCESSING</u> Wages and Salaries (Varies as Capacity ^{0.2})	5.82	3.34	2.42	1.92	1.61
10.	Administration and Overheads (Varies as Capacity 0.2)	5.69	3.27	2.36	1.88	1.57
• • •	Capacity) Capacity) Trensmont of Suren and Ishown (Verion of	1.09	1.09	1 . 09	1 . 09	1.09
 	0 U	1.26	1.26	1.26	1.26	1.26
• 1	Capacity 0.7)	3.64	2.96	2.62	2.40	2.25

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(contd.)

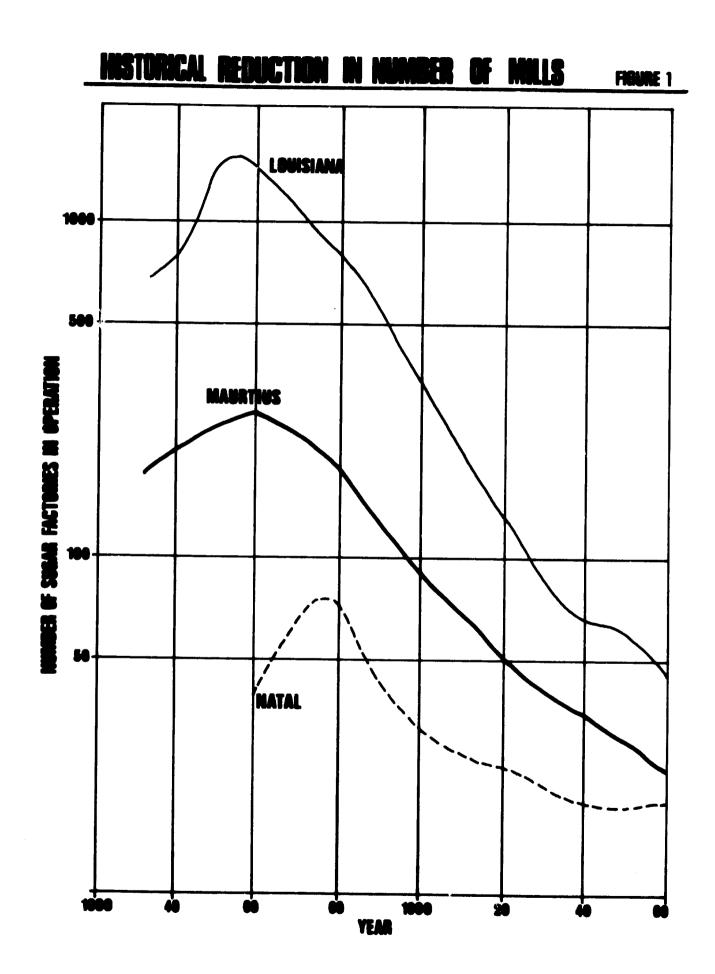
		50C TCH	3.92	0.31	82.47 (83.08)
ACTORY	E OF CANE	400 TCH	4.20	0.33	83.85 (84.44)
SUGAR]	PER TONNI	300 TCH	4.57	0.36	85.97 (86.54)
RAW SUGAR VS. CAPACITY OF SUGAR FACTORY	COST INDEX PER TONNE OF CANE	200 TCH	5.17	0.41	89.89 (90.43)
SUGAR VS.		100 TCH	6.36	0•50	100.00 (100.50)
COST OF PRODUCTION OF RAW		For Typical Capa city in Tonne Cane/Hr	<pre>14. Depreciation (Varies as Capacity 0.7) 15. Insurance (mainly factory equipment,</pre>	building and transport) (Varies as Capacity 0.7)	<pre>16. INDEX OF TOTAL COST OF FRODUCTION (Per tonne of cane) (Optimal Lard Configuration) (5:1 Rectangular Land Configuration)</pre>
			45 FF		Ъ

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TABLE V (contd.)

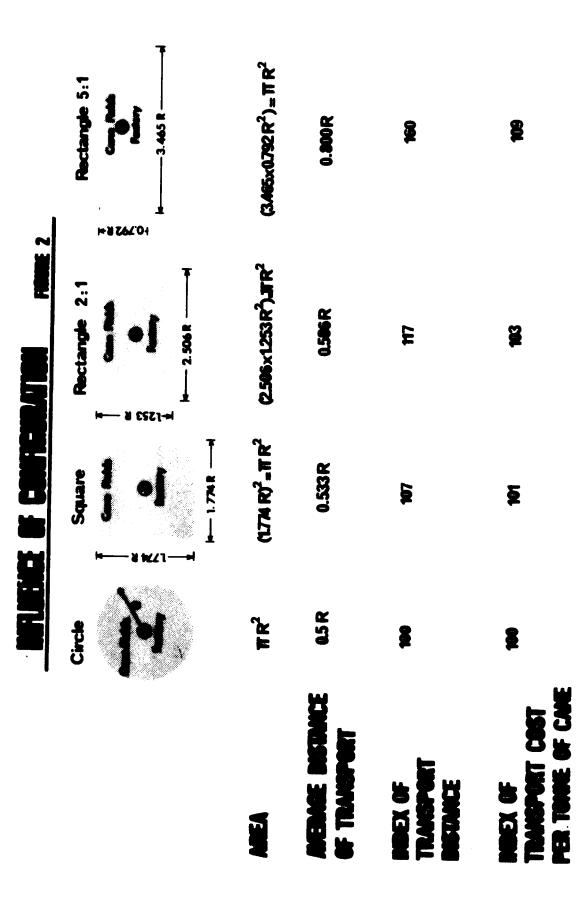
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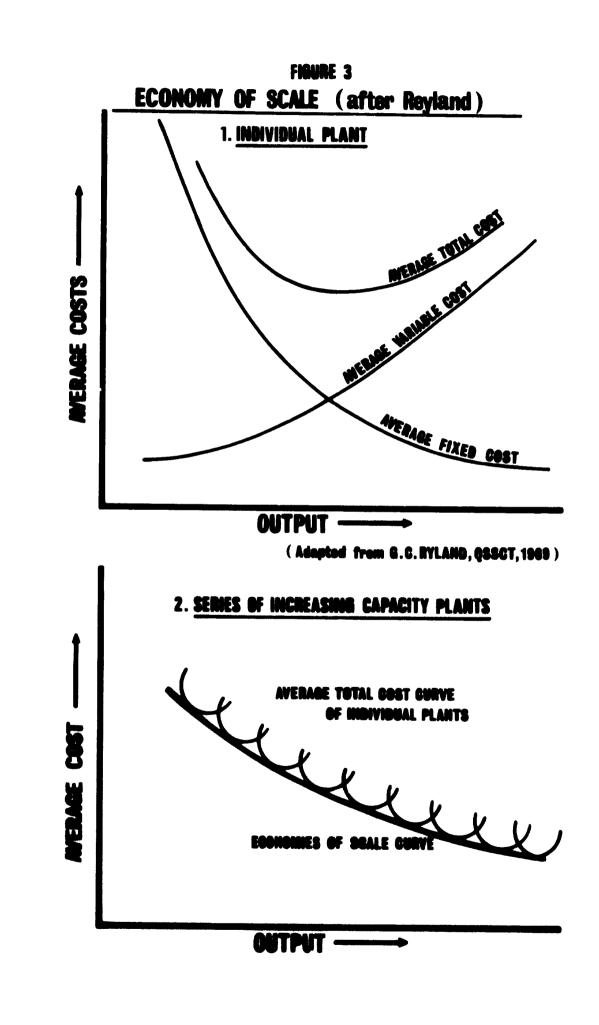
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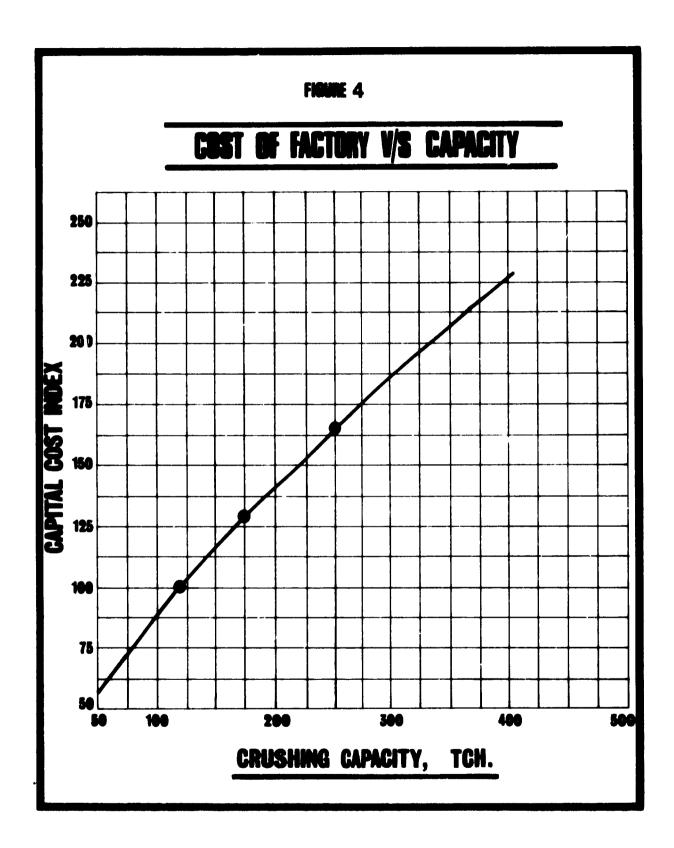


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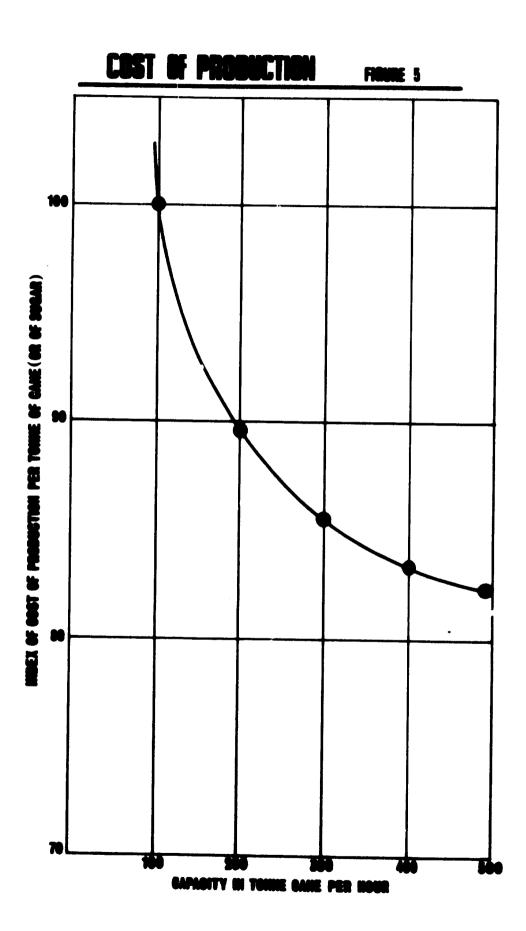


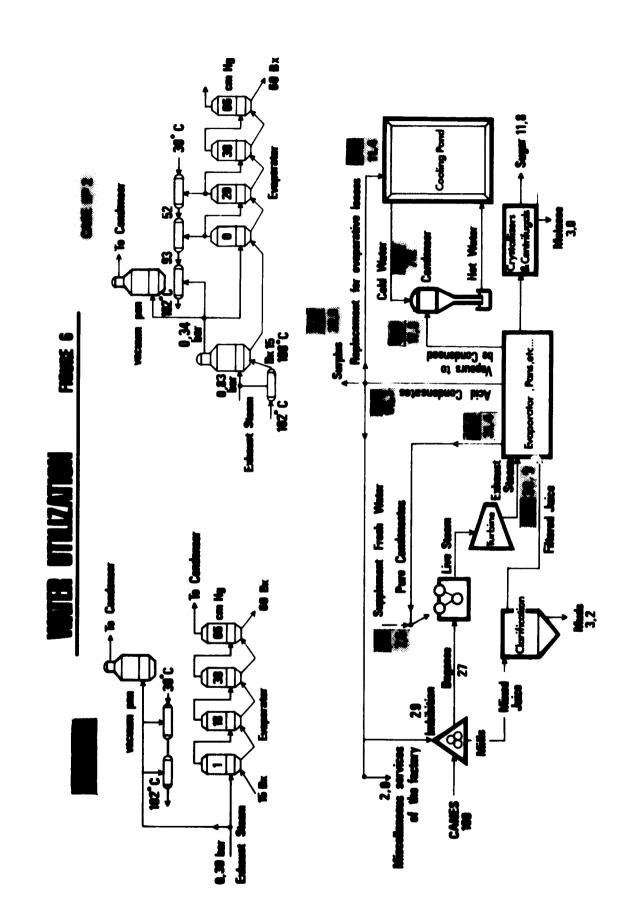
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RAW BUGAR FACTORIES (1973) VALUATION OF EQUIPMENT OF

APPENDIX A

1

ITEMS			CRUBHING CAPACITY			
	120 104		175 704		230 TCH	
L. CARE UNLOADIG			/fie 2 587 000/		(he 3 607 000/	
(a) Overhead Travelling Crenes	2 Bridges 10 Tons copocity 75 as ft	200 000	3 × 10 Tons	1 125 000	4 × 10 Tans	1 500 000
Bread of Lift Bread of Troval Bread of Troval	125 ft/min 250 ft/min 120 ft/min					
(11) Guntry	x 20 ft	415 000	10% × 1052	415 000	2 × 250° × 70°	630 000
(iii) Foundation & Erection	16	166 000		190 000		330 000
(b) Feed Table (1) Feed Table	Drea Tyre 25' wide x 34' overall.	····-				
		22 000	2 × 26' × 24'	2010 2000	2 × 20, × 31,	244 000
(11) Drive (111) Foundation & Erection	Slip coupling, 15 HP 3	36 000 16 000	x 15	88	x 15	88 88
(c) Cane Kicker (1) Cane Leveller	9 19 19	 00 80	2 × 10 HP	8	2 × 10 HP	88 %
(ii) Foundation & Erection		3 000				
(d) Care Cerrier (1) Langth	~				-061	
(iii) No. of slats		 B 9				
(v) No. of strends (v) Drive	3 35 HP, slip coupling 61	8	9 H	800	4 75 FP	88
(VI) romouton & Erection						

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2. CAE INTUES	(He 5/1 000)		(he 510 000)	(Pa 670 000)	
(a) First set	90 knives, 500 HPM, 250 HP	225 000	102 knives, 600 RPM,	il0 knives, 600 994	
(b) Second set	Sh intras. Shi BN. Shi H	267 MB	900 HP 275 000 102 kmitmer AN ADM	700 HP 300 (8
	}		56		
(c) Foundation & Erection		52 000		8	88
3. CRUBIONG PLANT	/Re 8 912 000/		/he 10 413 000/	/Fe 11 705 000/	
(a) Milling Plant comprising		<u></u>			
(1) MIIs	15 rollers 36" × 72"	3 750 000	15 rollers 38"x78" 4 150 000	15 milers 42"x84" 4 500 0	8
(ii) Intermediate carriers	4			4 560 0	8
(111) Platforms	1 set		8		g
(iv) Brace Turbines	ых 500 HP		5 × 700 HP 1 225 000	5 × 900 HP 1 375 0	8
	4		8	Ū	3
helicol	ى س	375 000		83	8
(vii) Compound reduction Gear	2		2 750		8
(vill) Vibrating screeks	2, Total filtering		× 34 × 34	× 4' × 24' 70	8
	uren 46 eq. ft	000 92 92			
(1x) Mocenetion chokelees pumpe	~~ 	000 02	3 2 2000	9C 0	8
(x) Overhead travelling crane	lof 15 Toms. such 56 ft		l x 30 Toms:		
	gentry 130 ft, hund operated	137 000	70" × 150" 280	* × 150* 200	8
(xii) 2nd 0.T. Crone	l of 5 Tons, as above,			5 Tons 45	8
(xiii) Foundation & Ernection	electrically operated	45 000			Ę
		3		•	3

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 JUCE THEATMEDIT FLANT Dive automatics scale (juice) Mulk of lime tanks Mulk of lime tanks Dive automatic scale (inhibition) Liming tanks Eligentic Treatment Plant Limed juice pamps Junce Heaters Autoe pamps Stany Vocuan filter Foundation 6 Erection 	As 2 27 000 150 turns/hr 2 40 turns/hr 3 175 ft head 3 x 200 sq. ft 1 of 16' x 5' 1 of 16' x 5'	数 % % 号 % 。 % % % % % % % %	As 3 100 000 225 1/hr 60 1/hr 3 2 × 800 g.p.m.x175 4 × 2000 gq. ft 1x31'x5 trays 2 × 14' × 8'	88838888888888888888888888888888888888	Re 3 679 000/ 300 T/hr 2 100 T/hr 3 2 × 1100 greet75' 6 × 2000 sq. ft 1 M40'x5 trays 2 × 16' × 5'	4.9 25 26 26 6.1 25 26 26 26 100 26 26 26 26 100 26 26 26 26 100 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 27 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26 26
3. EVADOMIOR (a) <u>Evoporator</u> (b) Bat of Dumes	As 1 200 000 1x35,000 sq. ft, quetruple	000 060 T	/ <u>Hc 1 720 000/</u> 1x36,200 sq.ft. 1x8,500 sq.ft 1	00 00	/ <u>As 2 270 000/</u> 1×55,000 sq.ft + 1×12,000 sq.ft	2 000 001
(1) Transfer Condensate from	15 HPx500 gamed5'		20+F×800gpmx45*		3049×1100gpmx451 2049×400cpmx751	
(111) Condensate Extraction from fourth effect	10HPx360gpm45	90 90	13+Px500gpmx45*	00 12	204Px 750gpm45	000 08
effect	13+P×175gpmx95'		20+1 :250gpmx351		3045×360gpmx951	
(c) Foundation & Erection		300 OTT		150 000		190 000

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9. N	6. WOLLIN PANG	(He 1 906 000)		(Ha 2 005 010)		(Pa 2 BLE 000)	
	Calendria pens, without stirrier	4 of 60 tons unit capacity	720 000	4 × 80 Toms	000 006	5 × 80 Tons 1	
3	Colendria pens, with stirrier	1 of 60 tons unit copocity	-	1 × 30 Tone	300 000	2 x 80 Tons	
0	Greating per	1 of 30 tons unit copecity	120 000	ł	ŧ		}.
	ng for pans	1	2	1	140 000	1	
		5 of 600 cu.ft unit cepecity		5 × 800 cu.ft	2000	5 × 1000 cu.ft	200 95
_		4 of 600 cu.ft unit capacity	8	4 × 800 cu.ft	40 000 000	4 × 1000 cu.ft	4 000
6	'8' Molasees Tarks	3 of 600 cu.ft unit capacity	2	3 x 300 cu.ft	800	3 × 1000 cu.ft	800 800 800 800 800 800 800 800 800 800
		1 of 800 cu.ft unit capacity	8	×	60 000	1 × 1000 cu.ft	40 000
		1	8		000 Q		000 08
	TKS	3 of 1500cu.ft unit capacity	112	3 × 2000 cu.ft	121 000	4 × 2000 cu.ft	151 000
	Potary measocuite pumps	3 of 860cu.ft/hr unit		×		4 × 1000 cu.ft/hr	152 000
		cepecity	114 000				
5	(1) Foundation & Erection		264 000		280 000		330 000
7. SON	7. CONDINETING PLANT & COLLING POND	(He sus 000)		/86 1 116 000/		/Hs 1 625 000/	
(a) (a)	Berometric condensors	2 of 8 ft diamater		16 × C	136 mn	- 101 - 2	
• (q)	(b) Water-jst condensers	l to operate with 1 vacuum	{	1	60 000		120 000
(c) 1	(c) Injection woter centrifunal mens	2 of 3500 collons/minute.	3	3 × 4000 mm	116 m		
•		unit copocity	106 000				
(G) L	(c) Liquid ring vacuum pumps	2 of 2000 cu.ft/minute, unit		2 × 2500cu.ft/min	130 000	3 x 2500cu.ft/min	220 000
		volume displacement	168 000			•	
(e) C	(c) Cooling pond	l of 20,000 sq.ft cooling		1 × 30,000 aq.ft	450 000	Equivalent	
() ()	(f) Cooling pond centrifugel pump	surrace 1 of 7000 gallons/minute		1 × 8000 apm		lx50,000 sq.ft l x 10.000 cmm	750 000
г СЭ Г	cundation & Erection		900 93		80 80 80		110 000

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500 000 30 8688 8888 000 084 00000 8 591 160 L 105 L **90 20** 8 8888 2 × 450 cu.ft/hr B 3 × 450 cu.ft/hr A 14 × 1000 cu.ft C 1 × 20 Tons/hr 1 × 20 Tons/hr 1 × 12,000 Tons 1 × 35' × 15 HP /Rs 2 240 (100) /Hs 3 182 000/ 5 × 52" × 40" /Rs 547 000/ 3 × 250 Tons Rs 636 000/ Six ო **~~** 115 000 125 000 500 000 500 000 88 88 88 8888 000 092 092 200 002 140 140 4 8 P 6 8883 1 × 450 cu.ft/hr B 2 × 450 cu.ft/hr A 10x1000 cu.ft C × 12 Tons/hr × 12 Tons/hr 45° ×l0 HP Fai 490 000/ /Rs 2 224 000/ × 40" × 9000 Tons 2 × 250 Tons /Fig. 390_000/ <u>581 000</u> 3 × 52" Five گ × m $\circ \circ \circ$ --00 102 000 000 320 000 548 000 96 000 360 000 360 000 360 000 250 000 225 000 405 000 8 ∢۱ ωı Four continuous type centrifugals One bucket type, 40 ft high, 714P 1 Workspoor for 6C0 cu.ft/hr of Workspoor for 300 cu.ft/hr of Blancherd of unit capacity of three rotary displacement pumps TWO of 150 tons unit capacity, **Dhe electr**ic sewing machine Two, unit length 35 ft, 5 HP One rotary horizontal drier One of 8 Tons/hr capacity One of 8 Tons/hr capacity Five 48"x30" at 1500 HPM Two, semi-cutomatic metallic bins /Hs I 072 000/ Rs 1 827 000/ massecuite mcssecuite 750 cu.ft (<u>Ps 277 000</u>) /Rs 465 000/ One of 8 Tor One of 6000 თ -(d) Staging for crystallisers to WEIGHTING & DISPOSAL OF MOLAGEES STORAGE AND BAGGING STATION Molasses storage tanks (e) Foundation & Erection (e) Sugar elevator
 (f) Foundation & Erection d) **Bag** conveyors (e) Foundation & Erection Foundation & Erection allow growity feed For A & B Museecuite For <u>C</u> Mussecuite Molasses pumps Bag seving machine (a) <u>A</u> Crystallisers (b) <u>B</u> Crystollisers (c) <u>C</u> Crystallisers Supar Weighers Mulases scale ł Sugar drier CRIBIALISER (c) Suger Bine CENTREPLEALS Molases O O O O Ð FULL ë n, ğ ä

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TrianDes of 20 ft long with provision for storage and mellometion 3200 cm 400 cm $1 \times 300^{\circ}$ 400 cm $1 \times 300^{\circ}$ 400 cm $1 \times 300^{\circ}$ $1 \times 300^{\circ}$ 6 Eneutian100, situate statement for strange and mellometion5 200 000 $2 \times 31 \text{ frank/hr}$ 7 000 000 $3 \times 30 \text{ frank/hr}$ 6 Eneutian100, situate statement for strange and mellometion5 200 000 $2 \times 300 000$ $2 \times 300 000$ $3 \times 30 \text{ frank/hr}$ 6 Eneutian100, situate statement0 e of 200 ks300 000 $1 \times 200 \text{ km}$ $3 \times 30 \text{ frank/hr}$ $7 000 000$ 1 End and the statement0 e of 200 ks1 900 000 $1 \times 200 \text{ km}$ $3 \times 300 000$ $1 \times 300 \text{ km}$ 1 End and the statement0 e of 200 ks1 × 200 km1 × 200 km $3 \times 300 000$ $1 \times 300 \text{ km}$ 1 End and the statement0 e of 10 tm, hend-commuted, thinh statement7 000 000 $1 \times 200 \text{ km}$ $3 \times 300 000$ 1 End and the statement0 e of 10 tm, hend-commuted, thinh statement $3 \times 300 000$ $1 \times 200 \text{ km}$ $3 \times 300 000$ 1 End and the statement0 e of 200 ks1 × 200 km $3 \times 300 000$ $1 \times 300 \text{ km}$ $3 \times 300 000$ 1 End and the statement0 e of 200 ks1 × 200 km $3 \times 300 000$ $1 \times 300 \text{ km}$ 1 End and the statement0 e of 10 tm, hend-commuted, the statement $3 \times 300 000$ $1 \times 200 000$ 1 End and the statement0 e of 10 tm, hend-commuted, the statement $1 \times 300 000$ $1 \times 300 000$ 1 End and the statement <th>12. BOLER R.AT</th> <th>/Pa 6 006 000/</th> <th></th> <th>/he 8 020 000/</th> <th></th> <th>/Ma 11 800 000/</th> <th></th>	12. BOLER R.AT	/Pa 6 006 000/		/he 8 020 000/		/Ma 11 800 000/	
Torr storage and residention res (5 Torre of stream part hr mater tube builters (1, meter tube builters		One of 250 ft long with provisio	c	1 × 300'		1 × 300'	400 000
The 36 Tone of steen part fr 2 × 37 Tone/hr 7 000 000 3 × 50 Tone/hr 2 000 000 May 7 UN under May 7 UN UND 5 200 000 2 × 200 00 3 × 50 Tone/hr 7 000 000 3 × 50 Tone/hr 1 9 00 000 3 × 50 Tone/hr 1 1 000 000 3 × 50 Tone/hr 1 1 000 000 3 × 50 Tone/hr 1 1 000 000 2 × 200 000 1 × 200 000<		for storage and reclamation	99				
All All <th></th> <th>Two 35 Tone of steam per hr</th> <th>8</th> <th>×</th> <th>8</th> <th>x</th> <th>10 500 000</th>		Two 35 Tone of steam per hr	8	×	8	x	10 500 000
Mar Table 1 Mar Table 1 Mar Table 1 Mar	(c) Faundation & Erection	Muli, water tube bollers	3 8				000 006
One of 200 ks 2 × 200 ks 1 900 000 2 × 200 ks 1 900 000 1 × 300 000 <		Ma 2 104 000/		(Ne 3 365 000)		A 195 000	
One of 280 000 1 280 000 1 One of 256 KVA 138 000 1 × 250 KVA 135 0000 1 One of 10 torn, hend-coverted, 280 000 1 × 250 KVA 135 0000 1 × 250 KVA One of 10 torn, hend-coverted, 280 000 1 × 250 KVA 135 0000 1 × 250 KVA One of 10 torn, hend-coverted, 280 000 1 × 250 KVA 1 × 250 KVA 1 × 250 KVA One of 10 torn, hend-coverted, 280 000 1 × 250 KVA 1 × 250 KVA 1 × 250 KVA (a) 0 0 1 × 000 1 × 000 1 × 000 1 × 250 KVA 1 × 250 KVA <th>Turbo-Al ternator</th> <th>Dre of 2000 Kw</th> <th></th> <th>×</th> <th>006</th> <th></th> <th>8</th>	Turbo-Al ternator	Dre of 2000 Kw		×	006		8
Image: Non-of-size KVA 150 000 1 × 260 KVA 175 000 1 × 300 KVA Image: Non-operated, volume 280 000 1×10 Tenser(0*20) 90 000 1×30 KVA Image: Non-operated, volume 280 000 1×10 Tense(0*20) 90 000 1×30 KVA Image: Non-operated, volume 280 000 1×10 Tense(0*20) 90 000 1×30 KVA Image: Non-operated, volume 280 000 1×10 Tense(0*20) 90 000 1×30 KVA Image: Non-operated, volume 280 000 1 280 000 1 280 000 Image: Non-operated, volume 280 000 1 280 000 1 280 000 1 Image: Non-operated, volume 280 000 1 280 000 1 280 000 1 Image: Non-operated, volume 280 000 1 280 000 1 1 280 000 1 Image: Non-operated, volume 1 1 280 000 1 1 1 1 1 Image: Non-operated, volume 1 1 1 1 1 1 <t< th=""><th>Beil to hoord</th><th>Ę</th><th></th><th>1</th><th></th><th>l</th><th></th></t<>	Beil to hoord	Ę		1		l	
Image: Constraint of the off lot ten, hand-constraint, when constraint, when constraint, when constraint, when the operation, hand-constraint, hand-constraint	Convection to grid Stand-by diesel generetor	Dre of 225 KVA		×		×	200 000 200 000
One of 10 tan, hand-operated, 45 ft even by 30 ft lang numby (5 ft even by 30 ft lang numby (6 ft) 1x10 Tonsec0'x60' 90 000 1x15 Tonsec0'x100' 1x10 tonsec0'x00' 20 000 1x10 tonsec0'x00' 360 000 1x15 Tonsec0'x100' 1x10 tonsec0'x00' 30 ft lang numby 30 ft lang numby 30 ft lang numby 360 000 1x16 100 1x1 75 000 10 325 000 10 326 000 10 360 000 1x1 10 1x2 000 10 326 000 10 326 000 10 1x1 10 1x2 000 10 326 000 10 326 000 10 10 1x1 10 1x2 000 10 326 000 10 326 000 10 10 1x1 10 1x2 000 10 326 000 10 326 000 10 10 1x1 11 1x1 10 110 110 110 110 10 10 10 10 10 10 10 10 10 10 10 10 10 10 10	w =		328 000				
	Power room Crene	<u>1</u>		1×10 Tonsx50*×80*		1x15 Tonex50*x100*	100 000
	(a) Franktion & Erection	_					400 000
	14. PIPDIG & CONTROL INSTRUMENTS	(1991) <u>- 1</u> 900					
Live steen ploting $[a]$ $[a]$ $325 000$ $[c]$ $325 000$ $[c]$ Cohaust steen ploting $[b]$ $325 000$ $[c]$ $320 000$ $[b]$ Vector ploting 97100 , molases $[d]$ $320 000$ $[c]$ $320 000$ $[c]$ Weter, juice, syrue, molases $[d]$ $300 000$ $[d]$ $300 000$ $[c]$ Weter, juice, syrue, molases $[d]$ $300 000$ $[d]$ $300 000$ $[d]$ Weter, juice, syrue, molases $[d]$ $300 000$ $[d]$ $300 000$ $[d]$ Weter, juice, syrue, molases $[d]$ $300 000$ $[d]$ $300 000$ $[d]$ Weter, juice, syrue, molases $[d]$ $300 000$ $[d]$ $300 000$ $[d]$ Weter, juice, syrue, molases $[d]$ $300 000$ $[d]$ $[d]$ $300 000$ $[d]$ Weter, juice, stations $[d]$ $[d]$ $300 000$ $[d]$ $[d]$ $300 000$ $[d]$ Weter, juice, stations $[d]$ $[d]$ $[d]$ $[d]$ $[d]$ $[d]$ $[d]$ Weter, juice, stations $[d]$ $[d]$ $[d]$ $[d]$ $[d]$ $[d]$ Parenting stations $[d]$ $[d]$ $[d]$ $[d]$ $[d]$ $[d]$ Parenting stations $[d]$ $[d]$							
Warenr picting 300 000 (c) 330 000 (c) Water, juice, syrue, moleanes (d) 300 000 (d) 300 000 (d) Water, juice, syrue, moleanes (d) 500 000 (d) 330 000 (d) Water, juice, syrue, moleanes (e) 330 000 (d) 330 000 (d) Water, juice, syrue, moleanes (e) 330 000 (e) 330 000 (d) Water, juice, syrue, moleanes (e) 330 000 (e) 330 000 (e) Phene preserve regulators, inducting values, PH control (e) 330 000 (e) (e) reducing values, PH control ontroller, one autometic vocuum (e) 330 000 (e) reducing values, PH control ontroller, one autometic vocuum (e) 330 000 (e) reducing values fe fe 330 000 (f) fe	 (a) Live stadm piping (b) Exhaust stadm piping 	(a) (b)	325 000 170 000	(D)		ප	88 88 900 900 900 900 900
and mercuite pinings and mercuite pinings frem presure regulators, reducing values, PH control cultameters, lavel and brix controller, one autometic vacuum controller, one autometic vacuum controller, one autometic vacuum controller, one autometic vacuum controller alant per control all indicating 6 per c	(c) Vapour piping	C					
Demonstrate regulators, reducing values, PH control (e) 330 000 (e) reducing values, PH control and brix and brix and brix cuttomiter, are automatic vacuum and brix and brix and brix controller, are automatic vacuum per controller plant and brix and brix controller, are automatic vacuum for automatic vacuum for automatic plant for automatic plant recording meters for boiler plant for automatic plant for automatic plant for automatic plant	2						
reducing values, PH control cultometers, lavel and brix controller, one autometic vacuum per controller dant per controller alant and one (ir compressor f(r) 230 000 (f)	Steam preserve regulators,	(=)	200 000	(e)		•	360 000
cultometers, lavel and brix controller, one autometic vacuum per control, all indicating 6 recording meters for boiler plant and one (ir compressor for the for boiler plant for for boiler plant for for boiler plant for for boiler plant	reducing values, PH control						
per control, all indicating 6 recording meters for boiler plant and one (is compressor (f) is (f) (f) (f)	cuitometers, level and brix controller, one automotic vocuum						
recording meters for boiler plant and one for compressor Function (f) (f) (f) (f) (f)	per control. all indicating 6						
and one fur compressor $[e]$ $[e]$ $[e]$ $[e]$ 20000 $[e]$	recording meters for boiler plant						
		(e)	160 000	(F)	230 000	(f)	200 002

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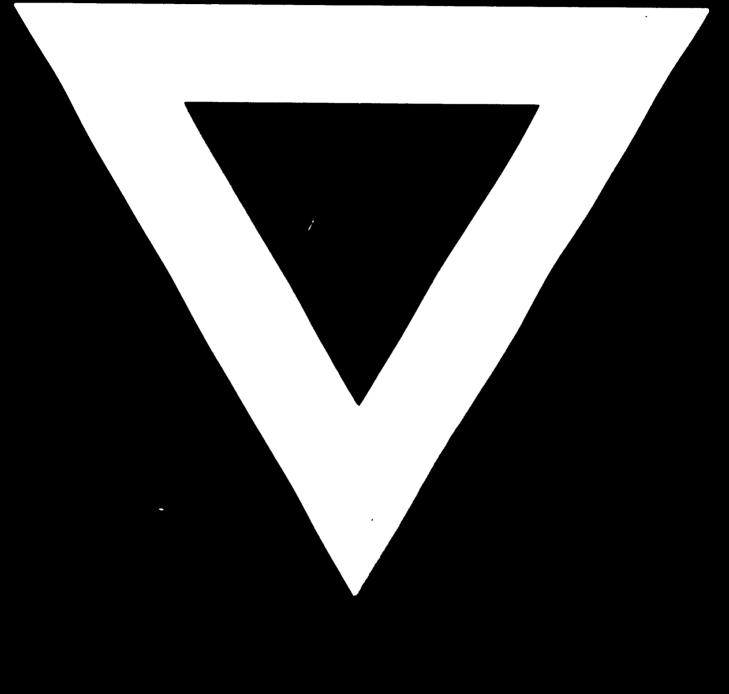
15. LABORATORY		/18 120 000/		(Fe 1 45 000)	
Equipment and Furniture	88 8		120 000		145 000
16. WORSHOP 5 TOLS Complete equipment with machine tools. overhead creme, windry	/Re 600 000/	/he 675 000/		(Jee 800 000)	
tools and squipment	600 009	·	675 000		800
17. DIGLETTEL BULDINGS	(He 3 070 000)	/Hs 4 120 000/		/Rs 4 660 000/	
(1) House	Che, span 55 ft, length 150 ft, 450 000 steel columns, corrugated iron	1 × 65° × 200°	000 D98	1 × 86' × 200'	000 088
	sheeting, concrete floor. Outside wall filled with concrete				
(ii) Boiler Plant & Power Station	blocks. One, spon 100 ft, length 200 ft, as dense	1 × 100' × 250'	1 250 000	1 × 100° × 300°	- <u></u>
(111) Clarification, boiling etc.	100 ft, length 250 ft, 1 300 1 300	1 × 100' × 300'	1 580 000	1 × 100' × 350'	1 770 000
(b) <u>Leboratory</u>	One, spen 35 f., langth 60 ft, concrete building, with metallic	1 × 40' × 60'	000 011	1 × 40' × 60'	110 000
	rrimed roor covered with corrugated asbestos cement, and concrete floor. 95 000				
(c) <u>Workstrop</u>	One, spon 50 ft, length 100 ft, generally as in (b) 225 000	1 × 70' × 100'	000 000	1 × 70' × 130'	400 000
GRAND TUTA	(re 34 933 000)	Re 44 725 000		Pre 57 466 000	

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