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ASSISTANCE TO THE PARTICLE BOARD PLANT AT MOJKOVAC



Proposed for the Government of Yugeslevia by the United Hatlens Industrial Development Organization insenting againsy for the United Nations Development Processor United Nations Development Programme

ASSISTANCE TO THE PARTICLE BOARD PLANT AT MOJKOVAC

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Project findings and recommendations

Prepared for the Government of Yugoslavia by the United Nations Industrial Development Organisation, executing agency fo the United Nations Development Programme

lased on the work of H. Mueller-Eokhardt, consultant

United Nations Industrial Development Organisation Vienna, 1976

Explanatory notes

The monotary unit in Yugoslavia is the dimar (Din). During the period covered by the report, the value of the dimar in relation to the United States dollar was \$US 1 = Din 18.05.

A full stop (.) is used to indicate decimals.

A comma (,) is used to distinguish thousands and millions.

Besides the common abbreviations, symbols and torms, the following have been used in this report:

f.b. finished board DEN Deutsche Industrie Norm

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ABSTRACT

At the request of the Government of the Socialist Federal Republic of Yugoslavia to the United Nations Development Programme (UNDP), an expert in the production of particle board was sent on mission to give technical assistance to the factory at Mojkovac. The United Nations Industrial Development Organization (UNIDO) was the executing agency.

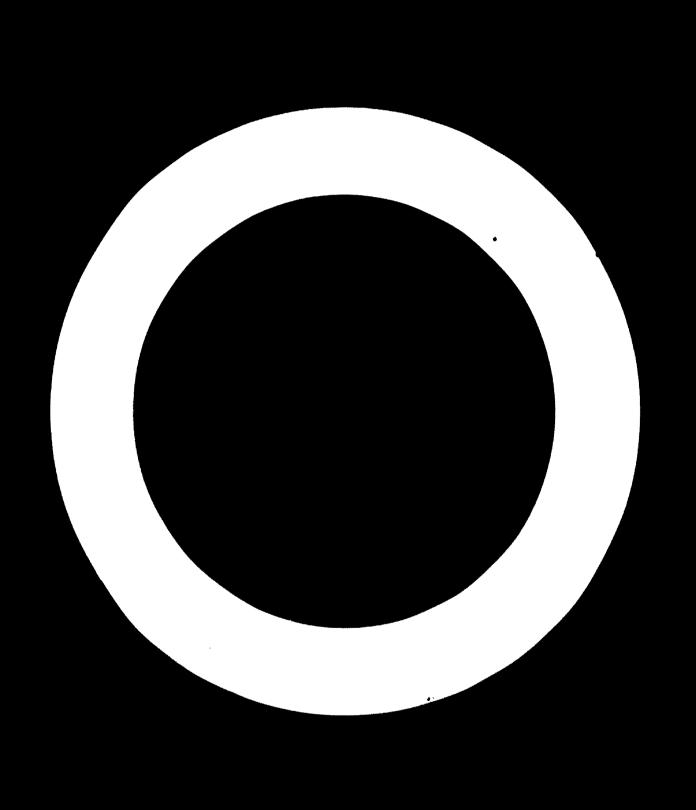
The expert arrived at Mojkovac on 6 June 1976 and left on 20 July 1976. The objectives of the project were to assist the management of the plant, upgrade production technology, increase productivity and improve the quality of products.

The expert concluded that the situation at the factory is such that possibilities for plant performance improvement are limited to a minimizing of annual losses. The reasons for these losses are low plant efficiency and high production costs, and he recommended that overhaul, repair and replacement of eld and worn out machinery be carried out. Also, production and quality controls should be reinstated.

The recommended improvements would be economically justified as the capital expenditure of Din 5,000,000 in 1976 has a payback period of approximately one year.

The expert reported that the only way to achieve profitable production of the plant is by a complete reconstruction and a considerable increase of its maximum production capacity.

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<u>Pace</u>

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INTHODUCTION

At the request of the Government of the Socialist Federal Republic of Yugoslavia to the United Nations Development Programme (UNDP), an expert in the production of particle board was sent on mission to give technical assistance to the factory at Mojkovac. The United Nations Industrial Development Organisation (UNIDO) was the executing agency. The expert arrived at Mojkovac on 6 June 1976 and left on 20 July 1976.

In 1975 the particle board factory at Mujkovac suffered losses of approximately Din 7,000,000; production costs were approximately Din 36,000,000 but the sales value was approximately Din 29,000,000. In order to locate the causes of these losses, the expert investigated the present state of plant machimery, maintenance procedures, production and quality control, plant efficiency, rew material consumption, production costs, and made cost/profit calculations. He discovered that the causes are low plant efficiency and high production costs.

The expert made recommendations for technical improvements leading to upgraded plant efficiency and production cost structure. It was recommended to overhaul, repair and replace old and worm out plant machinery and to reinstate production and quality controls.

However, the expert reported that the situation of the factory is such that possibilities for plant performance improvement are limited to a minimsing of annual losses. The recommended improvements would be economically justified as the capital expenditure of Din 5,000,000 in 1976 has a payback period of approximately one year.

The expert concluded that the only way to achieve profitable production of the plant is by a complete reconstruction and a considerable increase of its maximum production capacity.

I. SUMMARY AND RECOMMENDATIONS

Summery

In 1975 the particle board factory at Mojkovac suffered losses of approximately Din 7,000,000. Production costs were approximately Din 36,000,000, but the sales value was approximately Din 29,000,000.

The reasons for these losses are low plant officiency (1975: 61%, first half of 1976: 50%) and high production costs.

In order to locate the causes of this situation, investigations into the present state of plant machinery, maintenance procedures, production and quality control, plant efficiency, raw material consumption, production costs, and cost/profit calculations have been carried out.

Based on the results of these investigations it was possible to make recommendations for technical improvements leading to upgraded plant efficiency and production cost structure, and to calculate the economic results which could reasonably be expected after implementation of all recommendations.

The very strained economic situation of the Combine does not allow major changes in the plant at this stage, and therefore only those techmical recommendations were to be considered which would improve the situation under given production conditions.

The results of the investigations may be summarised as follows.

Machinery: Almost every key machine in the plant was found to have technical defects due to the worn-out state of the equipment. These defects result in uneconomic preparation and usage of raw material, and deficiencies of the end product. The worn-out state of machinery leads to constant breakdown of machine parts followed by stoppages of production.

<u>Maintenance</u>: The procedures in operation are adequate, but there is a serious lack of special spare-parts for machinery from abroad, which is the major part of the equipment. This shortage of special spare-parts results in unusually long repair time, which in turn is one of the main reasons for the low efficiency of the plant and its high economic losses. <u>Production control</u>: Practically no production control is carried out because of the damage to, or lack of, necessary technical equipment. This results in uncoonswical production procedures and wastage of raw material, which is another main reason for the economic losses of the factory.

Quality control: No quality control at all has been carried out since August 1975 owing to defective or non-existent laboratory equipment and lack of personnel. An acceptable quality standard of the end product is only ensured by adopting a very high dencity level of the boards. This complete lack of quality control is indirectly causing high economic lesses.

<u>Plant efficiency</u>: In 1975 plant efficiency was only 61% and in the first half of 1976 only 52%. Approximately 85% of the total down-time was caused by break-downs of mechanical equipment necessitating long repair sessions (lack of special spare-parts). The low efficiency of the plant is the main reason for the sconomic losses of the factory.

<u>Raw material consumption</u>: The consumption of wood is excessively high, whereas the average adhesive consumption is only slightly above normal considering the old-fashioned blending system and worn-out state of machines in operation. The costs for these raw materials represent approximately 80% of the total average direct production costs per oublo meter of finished board. Their high consumption is another main reason for the economic losses.

Cost profit analysis:

(a) The average production costs per oublo meter of finished board are so high that the break-even point would theoretically be reached at 150% of nominal plant efficiency. Even if plant efficiency could be improved to 100%, the factory would suffer economic losses of approximately Din 4,000,000 at this production cost level;

(b) Even after improvements of production costs and plant efficiency which could reasonably be expected when all recommended actions have been taken, the factory will still suffer losses, but they will be reduced by approximately 93% of the present level. Under these improved conditions the break-even point would be reached at 85% of nominal plant efficiency.

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To expect a constant plant efficiency of more than 80%, even under improved conditions, would be unrealistic considering the age and wornout state of the plant's machinery.

Plant reconstruction:

(a) The only way to achieve profitable production is a complete reconstruction of the plant and a considerable increase in its production capacity;

(b) Such a reconstruction is indicated not only by the above-mentioned facts, but also in view of the Combine's current situation and future planning:

- the recent opening of the railway connexion to Nejkovac has decisively improved the economic possibilities of the Combine:
- the capacity of all production units will be increased considerably;
- a great part of an increased particle board production will be needed for the production of the other units of the Combine.

Becommendations

To improve the current situation in the factory, it is recommended:

1. To overhaul and repair all plant machinery in order to improve production performance and permit proper production control.

2. To replace the machines for the blending station so as to reduce adhesive consumption and improve process performance.

3. To re-introduce an adequate production control to permit reduction of production costs.

4. To re-introduce a proper and reliable quality control in order to permit production of good quality board at minimum production costs.

5. To purchase necessary spare-parts from abroad to permit reduction of repair time and thus improve plant efficiency and its economic performance.

In order to make the particle board factory profitable and to secure its future, the following recommendations are given: 6. A complete reconstruction of the plant should be decided upon as soon as possible by the general management and relevant government authorities.

7. When this decision has been made, a detailed pre-investment study for the whole project should be carried out to ensure optimum technical and economic plans being made for the reconstruction of the plant.

8. Assistance should be requested from international organisations to secure the necessary independent tochnical assistance for a fast implementation of this project (proparation of pro-investment study, evaluation of offers utc.).

II. PINDINGS

The particle board factory of the Combine "Vukman Kruščić" is part of an integrated wood industry complex consisting of:

One samill

One particle board factory

One voncor production unit

One parquetry production unit

One production line for house elements

The Combine has 542 employees of which 370 are working in production and 72 in administration. The Combine's turnover in 1975 was Din 70,747,742.

The particle board factory was planned and created in 1961 by Siempelkamp (Pederal Republic of Germany) in co-operation with Ivo Lola Ribar (Yugoglavia), and adopted the "Schnitzler-System" for production of three-layer board with a capacity of approximately 60 m³/22 hours of finished board (19 mm, density 650 kg/m³). Reconstruction took place in 1972 (flaking department, preparation and press line) and in 1974, when a fourth daylight was installed in the old press, so that the maximum production capacity today is 75 m³/22 hours (19 mm, 700 kg/m³).

After 15 years uninterrupted production of approximately 345 working days per year, technical problems have accumulated with serious consequences for the economy of the factory and the Combine as a whole. In 1975 the losses of the particle board factory amounted to Din 6.9 million.

The reasons for economic losses of a production unit are always complex, and to find out the real reasons for losses it is necessary to carry out detailed investigations into all relevant technical and economical components involved in the process. Therefore the following studies had to be carried out:

- (a) An assessment of the state of existing mechanical equipment;
- (b) An assessment of production control and an analysis of results;
- (c) An assessment of quality control and an analysis of results;
- (d) An analysis of the reasons for down-time of the plant;

(c) A study of maintonance procedures and their efficiency;

(f) An analysis of production statistics and economic results, based on figures for 1975 and 1976.

Based on the results of the above investigations it was possible to discover the reasons for losses, to recommend the necessary action to be taken to improve production efficiency and production cost structure, and to determine the limits of profitability of this factory after implementation of the recommended improvements.

Knowledge of these figures and results will help the management of the Combine to decide what actions are to be taken for future development of the factory.

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III. PRODUCTION

The product

The factory produces a three-layer board with two fine surface layers (S-layers) and a medium-scarse core layer (C-layer). The size of the finished board is 1,750 x 3,600 mm. Owing to the high density of beech (<u>Fague silvatica</u>) as raw material the nominal specific weight of the board ranges from 700 kg/m³ for 19 mm up to 760 kg/m³ for 10 mm thickness.

The board is suitable for furniture production and, because of the fine surface, is good for laminating and vencoring.

The technological properties of the board are expected to meet the requirements of the relevant DIN standards.

Raw material

<u>Mood</u>: For the S-layer mainly coniferous roundwood, split wood and sawmill residues (trimmings and slabs). For the C-layer only beech roundwood, split wood and branches. With the increasing shortage and rising prices of coniferous wood, more and more beech is being used for the S-layer.

Only a small part of the residues from the other production units in the Combine is used for the production of particle board, the rest is needed for the thermal power plant. According to the general management no changes can be considered because of high oil prices.

<u>Adhesive, hardener, and their preparation</u>: Urea formaldehyde resin is delivered to the factory as liquid raw adhesive with 63.5-69% solid resin content, pH = 8.0, specific weight about 1.3 kg/dm³, free formaldehyde content 0.33\%, and a maximum shelf-life of three months.

The adhesive is prepared using separate formulae for the S-layer and C-layer. The preparation formulae for adhesive and hardener solution are adequate for the given climatic conditions at Nojkovac, the production process and the pH (approximately 5)^{1/} of the wood material used. The formulae are shown in annex I.

<u>Additives</u>: No paraffin emulsion is used to improve swelling and absorption properties of the board.

/ Figure obtained from plant management.

Mechanical equipment

The wood material is transported to the plant by a manually loaded and unloaded truck. In accordance with the Schnitzler-System for the mat-forming process the flake material is prepared in two separate lines for S-layer and C-layer. The different stations of the plant are shown in the production flow scheme (figure I) and comprise the following equipment:

(a) S-layer flakes preparation line

- Two Hombak PRZ 28 flakers, pneumatic transport of the flakes to the
- Wet-flake silo, capacity approximately 25 m³, with Weiss extraction device. Pnoumatic transport to the
- drior I; Ponndorf SP 12 H rotation bundle drier, steam-heated. Conveyor belt to the
- drier II, Poundorf SP 6 H, steam heated. Vibration conveyor trough to the
- Pallmann PSKM-12 refining mill. Pneumatic transport to the
- Allgaier TMSH 2000 classification screen, which is out of operation and bypassed. The material goes unclassified to the dry-flake bunker for S-layer.

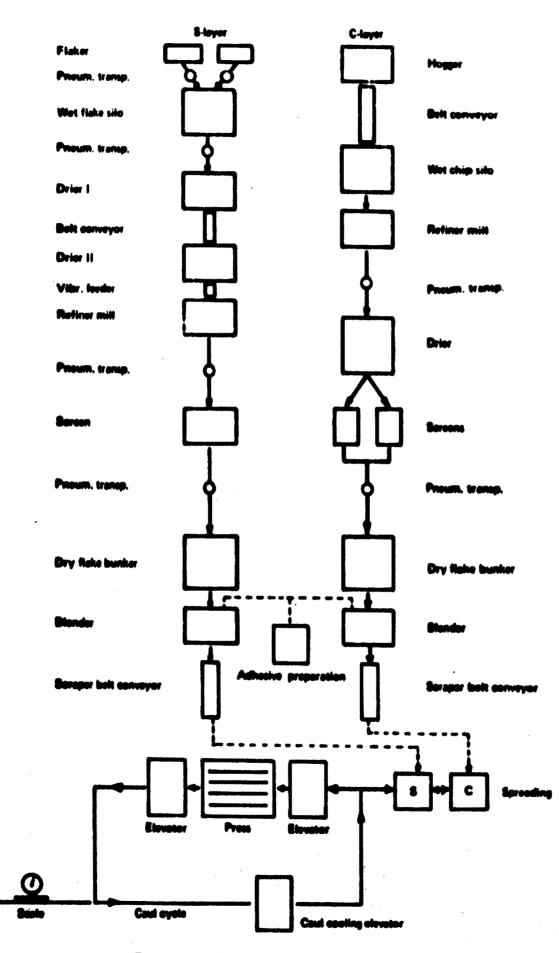
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- (b) <u>Q-layer flakes preparation line</u>
 - Klöckner 250 x 500 hogger. Transport of chips by conveyor belt to the
 - Wet chip silo, capacity approximately 30 m^3 , with Weiss extraction device and vibration trough, feeding the
 - Pallmann PZ 12 flaker. Pneumatic transport to the
 - Ponndorf TH 110 steam-heated rotation bundle drier. Pneumatic transport directly to the dry-flake bunker for C-layer without any classification as the Wiagara screens, which should be used after the drier, have been taken out of operation.

(c) <u>Blending station</u>

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- Industrie Companie horisontal dry-flake bunkers for 3- and C-layer material, capacity approximately 25 m³ each, equipped with transport belt, dosing drums, and discontinuous weigh-scales,
- Drais blenders for S- and C-layer, old system spreading the adhesive via nossles with compressed air.
- Drais adhesive preparation unit, automatic system with separate dosing cylinders for liquid adhesive, water, hardener solution and paraffin cmulsion, and the mixer unit. Separate container for prepared S-layer and C-layer adhesive



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Figure I. Production flow scheme

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- moraper conveyor bolts for transportation of the blended material to the
- Industric Companie mat-forming stations, equipped with new Wirtex spreader drum system and batch weigh-scales (volumetric and gravimetric spreading).

(d) <u>Briroulic press line</u>

- Caul system, reversible, moving under the mat-forming station, with elevators for 4 cauls for loading and unloading of the press. A caul cooling clevator for 6 cauls is installed in the caul return line, but is not in operation.
- Siempelkamp hot press, stean-hoated, 4 daylight, no simultaneous closing device, with hydraulic high-pressure and low-pressure plant.

(•) Noighing, triswing and sanding

- After separation from the cauls the boards pass a
- Gentrel weigh-scales for constant control of the raw board weight directly after pressing. After cooling and curing in intermediate storage the boards are trimmed on a

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- son-automatic trimming saw and fed directly into the Gremona fourdrum sander.

IV. FINDINGS AND DEFICIENCIES AT THE PLANT, AND RECOMMENDATIONS

Pindingo

All the mechanical equipment of the plant is old and worn out and frequent breakdowns occur causing long down-times of production.

Management procedures in the factory are adequately organized as is the operation report system (daily, weekly, monthly) which gives all the necessary information for plant performance control, raw material consumption and cost control. Work performance in the factory needs improvement.

Owing to plant layout and the installed machinery, the whole production process is labour-intensive causing high fixed production costs.

The capacities of the machines installed are balanced, with the exception of the two S-layer Ponndorf drivers whose total capacity should be approximately 20% higher in order to allow a proper ratio of S- and C-layer material for the production of 10 and 13 mm board. In order to partly compensate this shortfall, less material for the surface layer of thin board is used than is calculated in the standard board specifications (annex II) and the amount of core layer is increased accordingly.

Accumulated dust affects the proper functioning of the machinery and represents a very high fire risk. The factory should be thoroughly cleaned.

Approximately 1% of the storage hall and curing storage area is occupied by scrap, causing shortage of intermediate storage space for the boards to cool down and cure. Consequently insufficiently cooled and cured boards are taken for sanding.

Deficiencies of mechanical equipment

Surface layer flake preparation

Wood is dumped into deep mud at the side of the flakers. Stones and sand go with the wood into the flakers, damaging the knives and reducing their outting-edge life.

Immediate laying of concrete or bitumen flooring is recommended. Such flooring should also be laid at the chipping station for core layer material.

Hombak flakers PRZ 28: The cutter heads are worn out with the result that mainly coarse splinters and a disproportionately high percentage of dust is

produced. This non-homogenous material dries unevenly and reduces the already insufficient capacity of the driers. The cutter heads must be overhauled by a specialized company.

The ampere meters, which are necessary for indirect control of the flake quality produced, are broken. They must be replaced.

The Weiss extraction device: This device, a part of the wet-flake silo, is worn out and causes production stops. The machine must be completely overhauled.

<u>Ponndorf SP 6 H and SP 12 H driers</u>: To make maximum use of their drying capacity, sliding doors should be installed at the outlets in order to extend the drying time of the flake material.

All thermometers and manometers are broken and must be replaced urgently to enable a proper control of the drying procees.

The rubber of the conveyor belt between the driere is torn and must be replaced.

<u>Pallmann PSKN 12 refining mills</u> The grinding elements and the Conidur screen are worn out and damaged, which causes a disproportionately high percentage of dust in the flake material. These machine elements must be replaced.

<u>Allgaier TMSH 2000 classification screen</u>: The screen should be put back into operation in order to reduce the high amount of dust in the flake material.

Core layer flake preparation

<u>Klöckner horger 250 x 500</u>: The ampere meter is broken and must be replaced. The <u>Weiss extraction device</u> of the wet-chip silo is worn out and causes frequent stoppages of production. The machine must be overhauled completely.

<u>Pallmann PZ 12 flaker</u>: The knives are changed only once per shift. It is recommended that they be changed twice per shift in order to reduce dust. An ampere meter is missing and should be installed.

<u>Ponndorf TH 110 drier</u>: The additional heating unit for hot air and its inlet pipe are completely broken and out of operation. This unit is needed for the drier to reach its full capacity, especially in winter. The unit must be repaired and put back into operation.

All thermometers and manometers are broken and must be replaced to enable a proper control of the drying process to be maintained. The insulation of the steam pipes is either badly damaged or non-existent. It must be replaced to avoid waste of energy.

Adhesive station and blenders

<u>Dry bunkers for S- and (-layer material</u>: "The batch weigh-scales of both bunkers do not close properly and prevent the exact dosing of flake material for the blenders. They must be adjusted.

<u>Drais adhesive preparation unit</u>: The feeding pump for the hardener solution is out of order and the hardener is added manually which can lead to serious errors. The pump must be repaired immediately and put back into operation.

<u>Scraper conveyor bells</u>: These are worn out and cause down-time constantly. The distribution of the blender material over the width of the mat-forming machines is inadequate which causes irregular mat formation and then irregular distribution of specific weight over the finished board area. They must be replaced by new twin screw conveyors.

<u>Drais blenders</u>: These date from 1961 and work according to the old technology (spreading of adhesive through nossles with compressed air). As they have to be cleaned constantly they cause down-time of production and high labour costs. The nossles are often obstructed which loads to an irregular distribution of the adhesive on the flakes during the blending process. The actual adhesive consumption is at least 5% higher with this type of machine than it would be with the modern turbo-blenders.

The blending process is one of the key operations of the plant and influences decisively its production costs and profitability. Therefore, it is strongly recommended to replace the whole adhesive preparation system, the blenders, and the soraper conveyor belts by new equipment. This will considerably reduce production down-time, lower energy and labour costs, reduce the consumption of adhesive and hence improve the economy of the plant. The replacement should be done as soon as possible.

If the management decides to reconstruct the whole factory in the near future and increase its capacity, the above-mentioned new equipment should be chosen with capacities high enough to permit its further usage in the reconstructed plant.

A draft for inquiries with necessary technical specifications has been prepared (see annex III).

Mat-forming station

In order to check the quality of the mat-forming operation, density distribution and thickness have been tested on unsanded boards which revealed great deviations of specific weight and thickness over the board.

This is mainly caused by the inadequate performance of the mat-forming machines. Other reasons are the disadvantages of the reversible caul system with its discontinuous mat-forming process.

For improvement of the mat-forming operation it is recommended to replace the scraper conveyor belts and to adjust the batch weigh-scales (they do not close properly) and the spreading drums. A meticulcus inspection and cleaning of these machines must be carried out every day.

Hydraulic press plant

A few months ago the frames of the press broke and the whole press plant Was then completely overhauled including the hydraulic system.

The caul transport system is not operated with a sufficient number of cauls (11 instead of 17). Therefore the caul cooling elevator has been taken out of operation. Consequently the temperature of the cauls is too high when going into the mat-forming process, which causes pre-drying of the material and pre-polymerisation of the adhesive in the surface layer next to the caul. This results in a soft surface on one side of the boards after the pressing operation.

It is recommended to purchase 20 new cauls and to put the caul cooling elevator back into operation as soon as possible.

Weighing of the board after pressing

In this factory the board weigh-scales, which come after the press, are the most important controlling device in the production line to avoid unmecessarily high raw material consumption, which in turn leads to economic leases.

The scales are broken and must be overhauled and put back into operation as soon as possible.

Trimming and sanding station

There is no auxiliary equipment installed in this station (scissors-lifts, turning machine, roller conveyors etc.) and the operations are labour-intensive.

The trimming saw is non-automatic and does not allow recovery of trimming Maste material for the core layer line because there are no cutter heads for direct chipping of the trimming material.

It is recommended to replace the trimming machine with a modern one and install necessary auxiliary equipment in this station, for which detailed quotations are with the management.

Maintenance and spare-parts

The routine preventive maintenance and repair system in operation at the factory is adequate (manning, planning of work, stoppage reports etc.), and mufficient spare-parts from the local market for routine repair work are kept in stock. However, there is a shortage of special spare-parts for repair of machines from abroad, which form the major part of the equipment installed. Consequently, necessary repairs take too long and cause long down-time of production which is the main reason for the low efficiency of the plant.

It is, therefore, absolutely essential that the efficiency of repair work is improved and this is dependent on the ready availability of the special spare-parts.

It is strongly recommended that special spare-parts be purchased for the machines from abroad as soon as possible according to the detailed lists and quotations which are with management. All technical details have been discussed and the necessary action should be taken immediately.

Production control

The production control in this factory is inadequate owing to the lack of technical equipment.

Valid standard board specifications for each board thickness were not available and have been prepared (see annex II).

The following production factors are controlled:

- Noisture content of flakes before and after blending, with an electrical moisture controller
- Press temperature, pressure and pressing diagram at the control panel of the press plant

Thickness of each board after pressing, at the four corners of the board

In order to permit an acceptable standard of production control under the given conditions in this plant, it is essential that at least the following production factors are also controlled:

Performance of flakers and mills to avoid high dust production with dull knives

Moisture content of wet flakes before drying

Performance of the drivers to make maximum use of their limited capacities (in-going and out-going heating temperature, pressure, temperature of fumes at fume outlet)

Ratio of surface to core layer material spread

Weighing of board after pressing

The control of board weight directly after pressing is the most important production control station in the factory and permits the immediate recognition of deviations from nominal production process data so that immediate action can be taken to locate and eliminate the source of failure.

Only by re-introduction of a proper and reliable production control will it be possible to reduce production costs, to improve plant efficiency and to reach the maximum possible output of good quality board at minimum costs without jeopardizing the quality of the end product.

The applied shift report system gives the following production figures: Consumption of wood (separately for S- and C-layer) in m³ (stacked) per shift Consumption of raw adhesive in kg/shift

Production of board (m³ finished board) per shift and thickness produced

Down-times during each shift and their reasons

Report on sanding operation (m³ finished board sanded of each quality (Extra, I, II, and III))

The system is adequate under given conditions and allows a mifficiently accurate plant performance and cost control.

Guality control

No quality control at all has been carried out since August 1975 when the laboratory technician left the factory.

The existing laboratory equipment is insufficient to carry out all necesmany tests and is either out of order or needs adjustment (Wolpert Testing Machine, pH-meter, precision scale).

Several tests have been carried out by the expert in order to determine the specific weight of, and weight deviations within, a board and between different boards. Typical examples of the test results are shown in annex IV.

Owing to lack of proper instruments, it was not possible to produce exact figures but the figures obtained are reliable enough to establish the following facts:

1. The average specific weight of the boards is generally too high compared with the standard board specifications for the corresponding board thickness (average of the tests: 19 mm 736 kg/m³, 16 mm 745 kg/m³, 13 mm 768 kg/m³, and 10 mm 792 kg/m³).

2. The very high specific weight of the boards produced leads to the conclusion that the quality is good and the technological properties fill the requirements of DIN standards, although this could not be tested.

3. The boards are generally thicker on one long side than on the other, and on the head short side than on the other (seen in production direction).

4. The specific weight over the board is uneven, following the above mentioned thickness variances.

5. There are limited variances of specific weight between different boards but no distinct tendency could be established.

It can be assumed that the density variances result mainly from the inaccurate performance of the mat-forming machines, but another possible source could be an inaccuracy in the press after repair of its broken frames. It is therefore recommended that in order to check the accuracy of the press the same tests be carried out as mentioned above after implementation of the necessary adjustment to the mat-forming machines.

Without any production control (weight of boards) or quality control being carried out, a very high density is, of course, the only guarantee that board of an acceptable quality is being produced but the surplus specific weight of the boards must be reduced, without jeopardising their quality, to the level quoted in the standard board specifications, as this will considerably improve the economy of the plant. This, however, is only possible if a proper quality control is carried out.

Recommendations

1. To permit a correct and reliable quality control to be made the existing equipment should be overhauled and repaired and new equipment be installed without delay. A list of equipment to be purchased is given in the next chapter.

2. The following minimum tests should be carried out as a routine in the factory, as soon as personnel and equipment are available: (a) Quality of ruw adhesives
 Solid resin content
 Viscosity
 pH

Gelly strength tect

- (b) Control of prepared adhesives Viscosity Gelly strength text
- (c) Quality of flake material Bise and thickness of flakes Praction (dust percentage) pH

(d) Control of finished board properties
 Specific weight (density)
 Thickness variations (in each board and between boards)
 Dending strength
 Tonsile strength
 Noisture content
 Swelling and absorption (only if paraf'in emulsion is applied)

The plant management is acquainted with all test methods and working principles to be applied for carrying out the above-mentioned laboratory tests. All DIN standard forms and muitable laboratory test report forms are available. Details have been discussed with management wherever needed and small changes in the reporting system have been recommended.

3. There is a complete lack of statistical control of faults occurring at the manding station. This control is also important as it allows the detection of deficiencies in the production process (open areas on surface - pre-polymerisation; unsanded areas - curved platens of the press or defective cauls; core layer showing - unbalanced sanding or incorrect surface layer mat-forming etc.). A regular control system should be introduced at the sanding station for which a quality control form has been prepared (see annex V).

V. COST OF NECESSARY IMPROVEMENTS

According to the general management the financial situation of the Combine is very strained, and therefore only those replacements, overhaul and repair works can be considered which directly or indirectly improve the efficiency of the plant and decisively reduce consumption of raw material.

The costs of carrying out the necessary improvements are estimated on actual prices from recent quotations or on information received from the general management.

1,750,000

440,000

260,000

250,000

Investment costs1/

<u>Din</u> (approximate)

2,700,000

(a) <u>New blending station equipment</u> (as per specifications in annex II)

> Machinery ex-works abroad Transportation, installation, import duty of 25% Installation 15% Cooling water station

(b) Laboratory equipment

1 direct moisture meter with infra-red drier

1 laboratory circular maw

1 direct reading laboratory precision scale

2 thickness control gauges

- 1 viscosimeter
- 1 laboratory drying oven
- 1 manometer with pitot tube (control of pneumatic system)

equipment for test of gelly strength time, swelling and absorption

(c) <u>Mooring</u>

Approximately 2,500 m² bitumen or concrete flooring

Contingency margin

80.000

550,000 <u>170,000</u> 3,500,000

1/ Grouping of costs according to the general management.

<u>Overhaul</u>	and repair costs	Ma
(a) (b)		420,000
•••	(through specialized company)	200,000
(c)	Special spare parts from abroad for foreign machines	400,000
(d)	Overhul of board weigh-scales (through specialized company)	е <u>,</u>
(•)	Anometory, thermometery, amore	20,000
(1)	meters etc. for production control Overhaul of mat-forming station	30,000
~~/	(through upcelalized company)	40,000
(8)	Ovorhaul and ropair of laboratory equipment (through specialised company)	
(h)	A.11 other work, as specified in the chapter "Deficiencies of mechanical equipment"	30,000
	Oontingenoy margin	300,000
	Concerning west Cast	60,000
		1 ,500,000 °
	Total capital required	5,000,0 00

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VI. ANALYSIS OF PRODUCTION STATISTICS AND BCONOMIC PERFORMANCE RESULTS

For the evaluation of plant officiency and cost structure under current conditions, statistics for output, down-time and raw material consumption have been prepared and analyzed. For the assessment of plant profitability, both under current conditions and conditions which can reasonably be expected after the implementation of recommended improvements, two cost/profit calculations and break-even point analyzes have been prepared.

The calculations are based on actual figures from the company's statistics for 1975 and the first half of 1976. Their results give a clear picture of the over-all situation of this particle bourd factory.

Production statistics

Output

In 1975 the total output was 14,870 m³ of finished board (f.b.) with the following thickness distributions

10	•	27	16		23
13	•	145	19	•	36%

The output in the first half of 1976 reached 5,599 m³ f.b. and had approximately the same thickness distribution (see annex VI).

Based on this actual thickness distribution of board to be produced and 345 working days/year with 22 hours effective production per day, the possible maximum output of the plant is 23,800 m³ f.b. per year and 3.1 m³ f.b. average production per hour.

The finished board is sorted and sold in four qualities: Extra, I, II, and III (rejects). In 1975 and the first half of 1976 the percentage of qualities produced wast Extra and I = 89% (1976: 87%), II = 7% (1976: 9%), and III = 4% (1976: 4%).

The factory is manned with 92 employees directly connected with production (4-shift system). On an average they work 50 weeks a year, 45 hours per week. This equals 8.7 man hours/m³ f.b. based on the annual maximum output of 23,800 m³. Based on the output of 1975 the labour input reached 13.9 man hours/m³ f.b.

Down-time

The total effective production time in 1975 was 7,678 hours and the down-time in this year was 3,031 hours, i.e. the plant efficiency (utilization) was 61%. When in production, an average output of 3.1 m³ f.b. per effective production hour was reached, i.e. the nominal (100%) output of the plant.

For the first half of 1976 the corresponding figures are: plant efficiency = 52% and output per effective production hour = 3.1 m³ f.b. For further details noe annex VII.

An analysis of the recorded reasons for production stops in every daily down-time report has been carried out for the time from 1 Jannuary to 30 June 1976 which showed that approximately 85% of the total down-time was caused by breakdowns of machinery in the plant. The remainder was due to power failure, shortage of steam, lack of raw adhesive, or other reasons beyond plant control. These reports also confirm the repeated observations of the expert at the site during the last two months that necessary repair work of defective machines from abroad takes an excessively long time. This is mainly due to lack of an adequate stock of spare-parts from abroad for these machines.

The records show further that breakdowns are not concentrated on one specific part of the plant's mechanical equipment but occur indiscriminately, with the exception of the scraper conveyor belts at the gluing station and the extraction devices of the wet-flake siles which turn up repeatedly in the reports. This confirms the fact that after 15 years of uninterrupted production the plant machinery is now worn out.

May material consumption

The total consumption of wood, raw adhesive (69% solid resin content) and hardener in 1975 was as follows:

 Wood:
 47,290 s³ (stacked)

 Raw adhesive:
 1,572,887 kg

 Hardemer:
 7,611 kg

Referring to the 1975 total output of 14,870 m³ f.b., these figures correspond to the following average consumption per m³: Noods 3.2 m³ (stacked) per m³ f.b. Adhesives 106 kg (ruw)= 73.5 kg solid resin/m³ f.t. Hardemers 0.51 kg per m³ f.b.

The corresponding figures for the first half of 1976 ares

Noods 3.1 m³ (stacked) Adhonives 109.8 kg (raw) = 76.6 kg molid resin Hardeners 0.41 kg per m³ f.b.

Por further details soo annex VIII.

The wood consumption is extremely high and it is hardly possible that the recorded figures correspond to reality. The commution recorded is based on the number of trucks unloaded at the flaking stations, i.e. loading volume of truck (n^3) x number of trucks delivered = wood consumption. There is no check on whether the trucks are loaded to 100% of their capacity. The introduction of a tight control was recommended and was carried out in June 1976. The wood consumption dropped to 2.5 m³ (stucked) per m³ f.b.

The average adhesive consumption of 106 kg (1975) and 109.8 kg (1976) per m³ f.b. is not extremely high considering the relatively high amount of dust in the flake material and the old type of blenders in operation, but it can surely be reduced to an average of 99.5 kg raw adhesive per m³ f.b. (see standard board specification, annex III) after the recommended installation of the new glue station equipment, improvement of flake preparation; and re-introduction of proper production and quality controls.

Gost profit calculations and break-even point analysis

The cost/profit calculation for 1975 is based on actual figures from the company's balance sheet and shows the following (production 1975: $14,870 \text{ m}^3$ of finished board):

	•		
1.	Direct costs/m ³ f.b.	•	1,606.65
	Pixed costs/m ³ f.b.	•	
	Total costs/m ³ f.b.	•	2, 393 .94
2.	Total production costs		35, 597, 957.00
	Total mles value	•	28.668.083.00
	Log# in 1975		6.929.874.00

For further dotails noo annex IX.

The break-even point analysis (see figure II) illustrates the serious economic situations

(a) The total production $costs/m^3$ are so high that the break-even point would be reached at approximately 150% of the theoretical maximum output of the plant;

(b) Even if the plant's officiency could be improved to a maximum of 100%, the factory would still suffer losses in the range of Din 4,000,000 at this production cost level.

It follows that this situation can only be improved by bringing down production conts and simultaneously increasing the plant's efficiency. This can only be accomplished if all improvements recommended are carried out.

Under the improved conditions it is realistic to expect a reduction of wood consumption of approximately 25%, a reduction of adhesive consumption of approximately 6%, and an increase of plant efficiency to a maximum 80%. A goal of constant plant efficiency higher than 80% is not realistic considering the age of the plant.

A reduction of fixed costs, especially labour costs, is not possible ewing to the circumstances according to the general management, but they will be kept at approximately the same level in the near future.

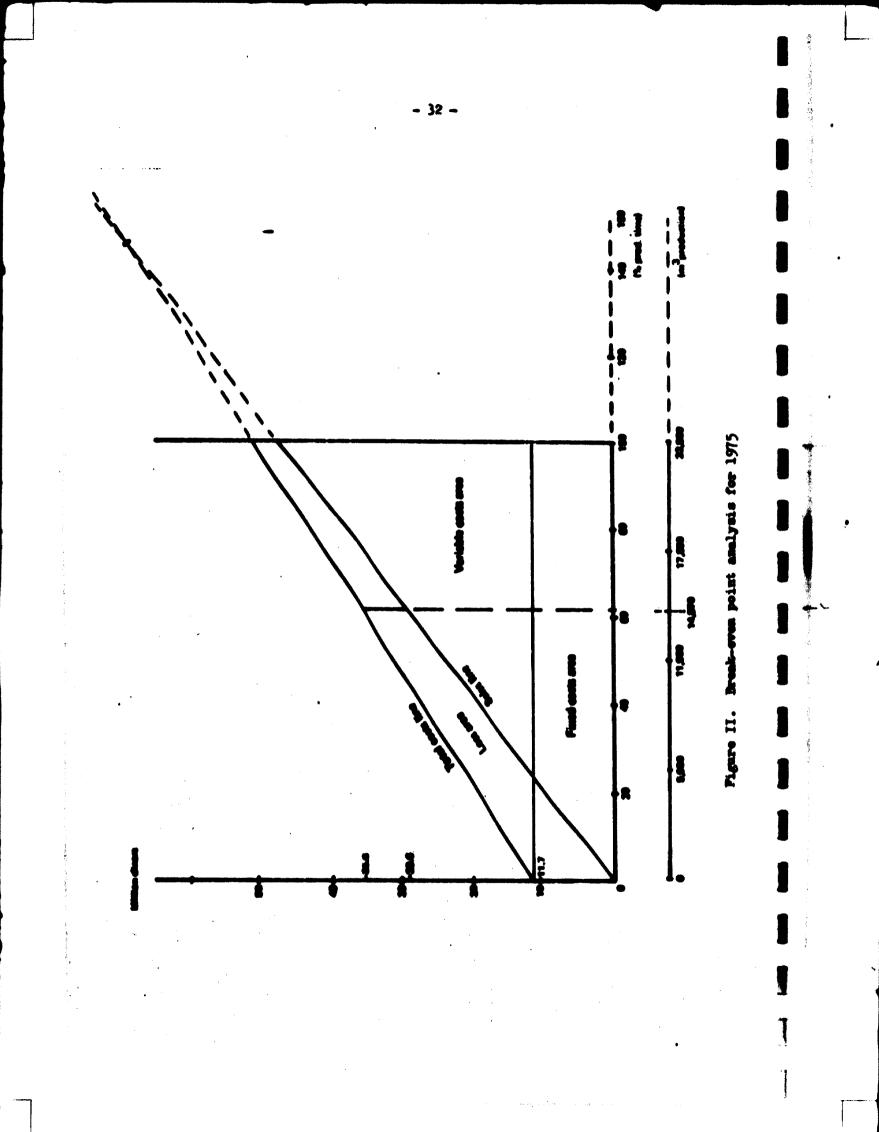
Therefore the following cost/profit calculation has been prepared with reduced direct material costs based on raw material consumption figures in line with the standard board specifications, and on present purchase prices with all other costs unchanged.

The possible economic performance to be expected after implementation of all recommended improvements, based on 80% of the nominal plant output i.e. 19,040 m³ f.b. per year and the price level of 1975/76, is as follows:

<u>Nnar</u>

Total sales value	-	36,747,200
Total production costs	•	37.211.050
Expected loss per annum		-463,850

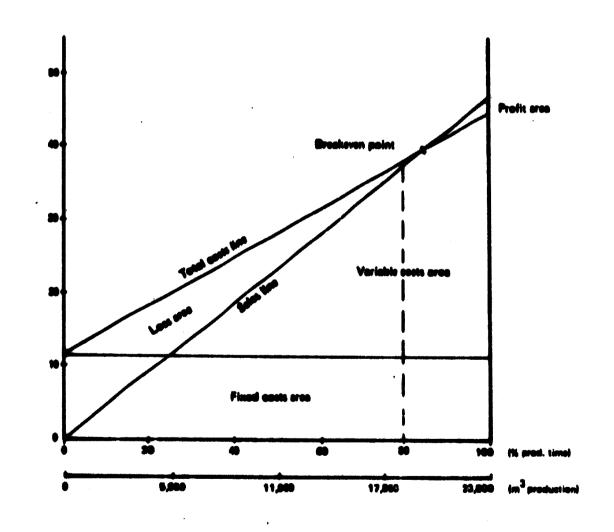
For further details see annex X.



1. Even under improvements of production conditions which can reasonably be expected, the factory will still suffer commic losses.

2. The losses will be approximately Din 460,000 against Din 6,930,000 in 1975, i.e. a reduction of annual losses by approximitely 93%.

3. The broak-even point is reached under improved conditions at 85% of 100% plant efficiency.



Pigure III. Break-even point analysis for possible result after implementation of improvement

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VII. CONCLUSIONS

1. The possibilities for improvement of the economic situation of the factory are limited to a minimizing of annual losses.

2. Even with the attainable figure of 80% plant efficiency and raw material consumption reduced to standard board specification level, the factory will suffer losses and no profit can be expected.

3. A comparison of the cost/profit calculations shows that by implementation of all recommendations a reduction of annual losses at approximately 93% could be reached.

This relation of 93% relative result improvement will remain valid even for the near future, as wages and prices are index regulated for this industry by the Government.

4. The recommended improvements would be economically justified as the capital expenditure of Din 5,000,000 in 1976 has a payback period of approximately one year.

5. The only way to achieve profitable production is a complete reconstruction of the plant and a considerable increase of its maximum production capacity.

Annex I

PREPARATION OF ATHESIVE AND HARDENER SOLUTION

Preparation of adhesive in summer is done according to the following formulation:

1. Surface layer 65 kg (50 1) raw adhesive (69% solid resin) + 27 kg (27 1) water + 1 kg (11) hardener solution 93 kg (78 1) prepared adhesive i.e. a concentration of 47.8% with 44.5 kg solid resin content. 2. Core layer 78 kg = 60 1 raw adhesive (69% solid resin) + 20 kg = 201 water + 3 kg = 3 1 hardener solution 101 kg = 83 1 prepared adhesive i.e. a concentration of 52.9% with 53.4 kg solid resin content. The hardener solution is prepared in summer as follows: 100 kg annonium chloride (NH_Cl) + 88 kg ammonium hydroxyde (NH_OH) 25% + 622 kg water 810 kg - litre hardener solution In winter the amount of MHACH is reduced by one-half. The formulae for preparation of adhesive in winter are as follows:3/ Surface Layer Core layer 65 kg = 50 1 raw adhesive 78 kg = 60 1+ 24 kg = 24 1 water + 17 kg = 17 1 1 kg = 1 1 hardener + 3 kg = 31solution 90 kg = 75 1 prepared 96 kg = 80 1 adbosive

Prormulation for winter was received from the plant management.

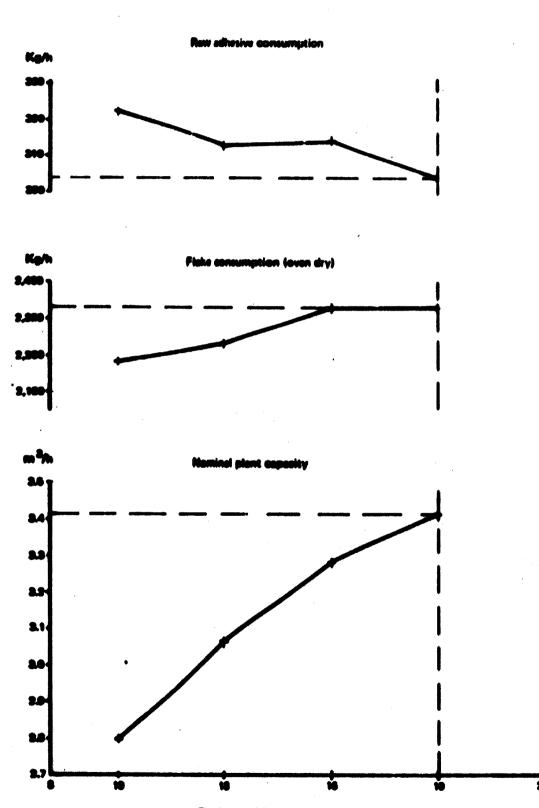
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Annex II

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STANDARD BOARD SPECIFICATIONS

1. Nominal plant capacity:	75 m ³ f.b./22 hours, = 3.41 m ³ f.b./hour, based on
	19 mm board thickness with a
	density of 700 kg/m ³
2. Type of board:	Three layer board
3. Now material: (a) wood	for surface layer mainly coniferous
•	wood and beech
	for core layer only beech
(b) adhesive	Ures formaldehyde resin, raw adhesive
	with 69 \$ solid regin content
4. Thicknesses produced:	enly 10, 13, 16 and 19 mm
5. Nough board size:	1,800 x 3,710 mm
6. Rough board area;	6.678 m ²
7. Finished board size:	1,750 x 3,660 mm
8. Finished board area:	6.405 m ²
9. Number of press openings:	4
10. Quality standard applied;	te be in accordance with DIN standards
	68 761 52 361 52 362
	52 364 52 365



Thickness of Hinished beard in mm

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11. Technological figures for productions.

Iten	Unit	10 mm	13 m	16 mm	19 mm
Net board thickness f.b.		10	13	16	
Sanding allowance		1.5	1.5	2.0	2.0
Raw board thickness		11.5	14.5	18.0	21.0
Specific weight (density)	kg/n ³	760	740	720	700
Net board weight finished moisture u = 8 \$	kg	48. 6	61.6	73.8	85.2
Raw board weight moisture u = 8 \$	kg	58.3	71.6	86.5	96.1
Raw board weight oven dry (basis $u = 8 \ $)	kg	54.7	66.3	80.1	90.8
Wood flakes oven dry of raw board (basis 10 % sòlid resin; sverage)	kg	50.0	60.5	73.0	83.0
Burface layers part of wood flakes oven dry	\$	60	50	40	35
Core layer part of wood flakes oven dry	\$	40	50	60	65
Burface layers part of wood flakes oven dry	kg	30.0	30.2	29.0	29.0
Core layer part of wood flakes even dry	kg	20.0	30.3	. 44.0	54.0
Capacity / pressing (finished board)	" 3	0.256	0.333	0.410	0.487
Neating time	min	4	5	6	1
Londing + unloading of press	ni n	1.5	1.5	1.5	1.5
Time for one press cycle	ni n	5.5	6.5	7.5	8.5
Number of pressings/hour	-	10.9	9.2	8.0	7.0
Number of pressings/working day (22 hours effective time)	-	240	202	176	154
Capacity per hour (finished board)	۹3	2.79	3.06	3,28	3.41
Capacity per hour (fimished board)	netric tens	2.15	2,26	2.36	2.39
Capacity per working day (finished board)	د.	61.4	67.3	72.2	75.0
Capacity per working day (finished board)	notrio tons	47.3	49.8	51.9	52.5

Item	Unit	10 mm	13 mm	16 mm	19 mm
Number of boards por hour	-	43.6	36.8	32	26
Number of boards per working day	-	959	809	704	616
Total flakes per hour even dry	kg	2,180	2,226	2,336	2,324
Flakes for surface layers per hour, even dry	kg	1,308	1,113	934	813
Plakes for core layer per hour, even dry	ke	872	1,113	1,402	1,511
Plakes for surface layers per- hear, with moisture $n_1 = 5$ \$	kg	1,373	1,168	961	854
Pinkes for ours layer per hour, with moisturg u = 4 \$	kg	907	1,158	1,458	1,571
Surface layers; solid resin per hour (12 \$ of dry flakes)	kg	157	133	112	97
Core layer: solid resin per hour (7.5 \$ of dry flakes)	ke	65	83	105	113
Total raw adhesive per hour (solid resin content = 69 \$)	kg	322	313	314	304
Raw adhesive per m ³ f.b.	ke	115	102	96	89
Bolid resin per m ³ f.b.	he	79.4	70.4	66.3	61.4
Neisture content of surface layer Interial after blending	\$	16-18	16-18	16-18	
Neisture content of core layer Interial after blending	\$	12-14	12-14	. 12-14	12-14
Perperature of the press	•c	150	150	150	160
looking prossure of the press	kp/os ²	250	250	250	250

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Annaz III

DRAFT OF ENQUIRIES FOR NEW CLUING EQUIPMENT

Be: Quotation for gluing oquipment - particle board production Dear Sirs,

You are hereby requested to send us your quotation for the following equipment:

Complete gluing station, comprising 2 Turbo blenders, for preparation of surface and core layer material

- 4 twin screw conveyors, for loading and unloading of the blenders, lengths approximately 4 m.
- 1 automatic preparation unit, complete, for separate dosing of raw adhesive, unter, hardener solution and paraffin emulsion, for separate preparation of adhesive for surface and core layer.

1 electrical control panel

The expecity and layout of the equipment has to be based on the following data:

Capacity of the plant	: 19 mm - 3.41 m ³ /h, density 700 kg/m ³
(finished board)	10 mm = 2.80 n^3/h_0 density 760 kg/m ³
Flake material: 19 m	at for surface layer 813 kg/h (oven dry)
	for core layer 1,511 kg (oven dry)
10 •	m for surface layer 1,308 kg (oven dry)
	for core layer 872 kg (oven dry)
Noed: 80-90% Beech (Parus pilvatica)

80-10% coniferous wood

- Blending: (a) Raw adhesive has approximately 68.5-69% colid regin content, specific weight = 1.3 kg/dm³ (Urea formaldohyde adhesive).
 - (b) Application for surface layer material approximately 12% solid resin, based on atro flakes.
 - (c) Application for core layer material approximately 8% solid resin, based on atro flakes.

Alternatively, we would like to have the prices for the same equipment but with a capacity of

> 8 m³ finished board/hour, based on 19 mm, density 700 kg/m³.

Parthermore, we ask for all technical data for the cooling-water equipment which is needed for the Turbo-blenders and which will be gurchased locally.

Please quote the prices separately for each item and indicate your earliest delivery time.

Yours faithfully,

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Annex IV

DENSITY DISTRIBUTION TESTS

A. Density distribution tests over such bourd

1. Scheme for sumple outling:

	T		Production fla
	13		1
1 2 3	Г	4 9 9	
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	14	. •	
	16	39	
	+		
	17		
\mathbf{h}			
		10 11 12	
1	Ē		
	╈		1
		31	
	30		
	21		
	1		
		36 36 27	

2. Test results

Board tested: 21 mm unsanded

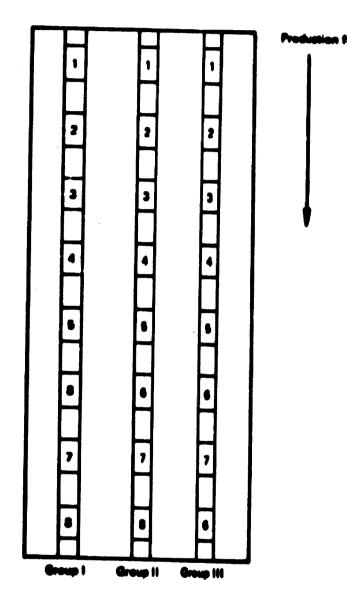
Sample	Dimona	ions (m)	Vol.	Weight	Density
No.	L	V	Thickn.	cm3	gr.	Kg/m3
1	184.5	147	20.5	55.6	367	660
2	184	145	20,5	547	388	709
2 3 4 5 6	184	135.5	21.0	524	382	729
4	184	151	21.3	592	470	794
5	184	147	21.5	582	452	777
6	184	146.5	21.4	577	413	716
7	199	143	20.3	578	378	654
	199	150.2	21	628	455	725
9	199	155	21.5	663	524	790
10	199	145	21.6	623	494	793
11	199	149.5	22.0	655	488	745
12	199	59.6	22.7	269	198	736
13	206	151.5	21.7	677	522	771
14	189	151	21	599	470	784
15	190	146	21,3	591	465	787
16	153	140	21	450	345	767
17	198	153	21	636	491	772
18	206.5	150	21.5	666	515	773
19	206	150	22	680	490	721
20	207	159	22.1	121	563	774
21	194	160	21.9	. 066	546	803
22	207	151	20	625	454	726
23	207	145	20.7	621	462	744
24	207	153	21.7	687	532	774
5	206.5	155	22.2	711	562	790
26	206	145	22.5	672	545	811
n .	207	143.5	22.9	680	502	738
26	190	147 .7	20,3	570	379	665
29	190	149.0	21,5	612	462	755
90	205	145.2	20,8	619	445	719
31	204	145	22	651	535	822

Medium density of the board: 752 kg/m3

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B. Density distribution tosts between the boards

1. Scheme for sample outling:



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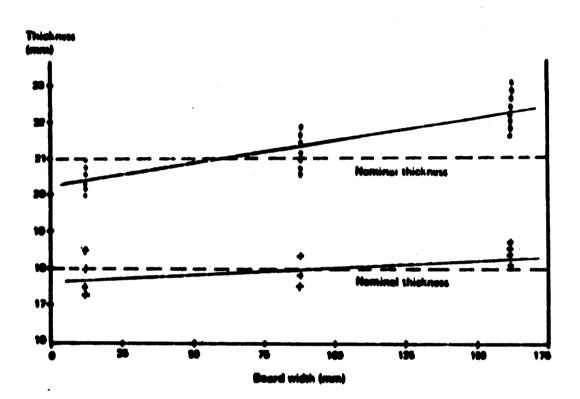
2. Test recults

Board tosted: 18 mm unsanded

	ap/no.	Dimens L	ions (m W) Thickn.	Vol. om3	Weight gr.	Dencit; Kg/m
11	1	99.6	87.0	18.1	158	105	663
	2	101.0	91.2	18.4	170	121	712
	3	102.5	89.0	18.5	170	121	712
	4 5 6	103.0	93.1	18.2	175	124	710
	5	104.0	93 .0	18.2	177	125	708
		1 04. G	95•4	18.5	185	12)	700
	1	105.0	93.0	18.2	178	132	749
	8	101.5	90.6	18.5	171	132	779
1:	1	98.2	87.5	18.3	158	117	739
	2	96.8	91.5	17.5	159	120	753
	3	99.8	89.1	17.8	159	112	707
	4	100.3	93.0	17.8	167	1 19	713
	3456	100.0	93.0	17.8	166	125	753
		100.0	95.5	17.6	168	124	738
	7	101.5	93.3	17.7	168	125	744
	8	102,0	90.4	17.9	168	127	756
1:	1	100.0	88.6	18.5	164	120	731
	2	99.6	93.3	18.0	167	121	725
	3	99•4	89.2	18.0	160	120	749
	4	99.5	93.1	17.7	164	124	756
	4 5 6	99. 6	93.0	17.5	163	127	778
		99. 3	93.0	17.3	160	120	749
	1	99. 6	93.0	17.4	162	116	719
	•	101.5	91.5	17.5	163	129	791
Netiun		thickn		He	dium densi	ties	
		Group		3 mm		oup I:	717 kg/m3
				8 mm		oup II:	738 kg/m3
		Group II	ll: 17.	7	Or	oup III:	749 kg/m3

Medium density of the board: 735 kg/m3

C. Thickness distribution as per test results A.2. and B.2.



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Annex Y

QUALITY CONTROL FORM FOR SANDING STATION

Date	Shift I	Board	thickness	ma
Board	Faulte		No. of	
quality	Faulte		boards	*
Extra/1	No faults			
II	Wrong dimensions			
•	Open areas of surface			
	Damaged through handling			
	Adhesive patches			
	Weak corners			
	Crude edges			
	Unsanded areas			
	Core layer showing			
	Thickness too low			
	Sanding defects			
	Other faults			
III	Splitting			
	Other faults			
	Total boards sanded			100

sign, Controller

Annex VI

TOTAL BOARD PRODUCTION AND THICKNESS DISTRIBUTION, 1975 AND 1976

Nonth	10 mm (m ³)	13 mm (m ³)	16 mm (m ³)	19 و (س ²)	Total (m ³)
Jan.	-	150	381	483	1,014
Peb.	29 5		192	377	864
linsoh	232	222	184	879	1,517
April	544	199	234	405	1,382
Nay	143	413	381	641	1,578
June	523		147	909	1,579
July	436	140	127	307	1,010
Aug.	440	186	559		1,185
Sept .	938				938
Oct.	445	327	497		1,269
Nev.	•	394	314	612	1,320
Dec.			460	754	1,214
Total	3,996	2,031	3,476	5, 367	14,870
Average/;	year 27 \$	14 \$	23 🛸	36 \$	100

A. Total board production and thickness distribution in 1975

Total production in 1975 = $14,870 \text{ m}^3$ f.b.

Nonth	10 mm (m ³)	13 m (m ³)	16 وم (س ^ع)	19 mm (m ³)	Total (m ³)
Jan,				185	185
Pob.	-		125	612	737
Narch	378	-	194	221	79 3
April	3	274	577	490	1,344
Hay	949	-	-		949
Juno	50	403	478	660	1,591
Total	1,380	677	1,374	2,168	5, 599
Average/y	mr 25 \$	12 🕏	24 \$	39 \$	100 9

B. Total board production and thickness distribution in 1976

Sotal production 1.1. - 30.6.1976 - 5,599 m³ f.b.

.

Annex VII

DOWN-TIME, 1975 AND 1976

A. Down-time in 1975

Day	Jan.	Peb.	Маг.	Apr.	Nay	June	July	Aug.	Sept.	Oot,	Nov,	Dec.
1	-	14	rep.	10	-	12	3	8				
2	8	15		22	-	8	7	2	18	3	12	9
3	12	17	16	4	22	20	8	20	9	1	2	4
4	14	ģ	4	- 7	13	12	22	5	13	11	10	ž
5	4	5	12	12	11	10	21		9 2	Ϋ́.	1	6
6	13	5 8	7		12	8	17	8	6	.5	1	3
7	14	5	11	6	8	11	3	10	11	13	9	1
8	16	12	11	1	14	2	2	1	21		1	11
9	17	10	22	2	11	3	ē	19	22	36	.5	6
10	9	15	5	5	7	ē	19	11	22	2	11	3
11	2	22	9	2	5	Ă,	21	13	22	6	8	7
12	11	2	10	Ä	ģ	<u> </u>	22	18	22	•	5	10
13	8	2	-	22	í	10	22	8	20	12	5	9
14	10	2	3	2	À	1	8	10	11	3	2	4
15	6	16	7	6	11	5	14	16	4	10		2
16	5	4	6	7	8	Á	22	4		11	3	12
17	6	8	-	2	8	ī	-6	2		13	13	4
18	- 18	14	2	22	Ă	2	10	11	2	12	17	9 6
19	16	6	2	8		4	14	15	9	10	12	
20	7	8	2	10	3	16	8	2	4	12	8	13
21	14	5	6	4	18	7	Ă	2	12	12		2 8
22	3	12	7	5	20	Ż	14	11	1	1	5 12	8
23	3	16	7	Ĵ	-	10	10	18	ġ	6	12	0
24	2	t	4	5	2	8	-	12	1	22	12	1
25	5	2	4	11	1	6	8	8	1	10	17	3
26	17		-	16	4	4	16	2	Å	17	15	
21	2		5	16	5	Ä	8	5		18	19	L
26	12	- -	1	10	Ă	10	8	1Ó	À	13	12 ·	ê g
29	15	-	7	3	-	2	2	8	20	13	22	
30	13		4	5	-	6	18	Ğ	10	12	22	
31	12	<u> </u>	13		12		9	4		9		closed for maintenance
Total	294	227	187	232	235	218	354	269	303	283	281	149
BITECT. prod.hrs	660	506	638	660	660	660	682	682	660	682		
(22/day)							~~~	002	000	002	660	528
Down-time	45	45	29	35	36	33	52	39	46	41	43	28

4. L

Total down-time in 1975: 7,678 hrs 3,032 hrs

Average down-time in 1975: 39 \$

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Bay	Jamary	Pebruary	Karch	Apri	1 Nay	June
$ \begin{array}{c} 1 \\ 2 \\ 3 \\ 4 \\ 5 \\ 6 \\ 7 \\ 8 \\ 9 \\ 10 \\ 11 \\ 12 \\ 13 \\ 14 \\ 15 \\ 16 \\ 17 \\ 18 \\ 19 \\ 20 \\ 21 \\ 22 \\ 23 \\ 24 \\ 25 \\ 26 \\ 27 \\ 28 \\ 29 \\ 30 \\ 31 \\ \end{array} $	12 14 10 16 8 22 22 22 22 22 22 22 22 22 22 22 22 2	22 22 22 22 22 22 22 22 22 22 22 22 22	12611126284733453343 - withis and side:	9335298791661942691463332 - 922222222222222222222222222222222		672294684313158132419-2-41225-
Total	192	395	413	258	301	145
Effective production hours(22 hrs/day)	242	638	682	660	638	660
Boun-time in \$	79	62	61	39	47	22
Total effective product	tion hours:	3,520	hrs			
Total down-time:		1,704				
Average down-time:		48 \$				

D. Down-time in 1976

Annex YIII

BAN MATHRIAL CONSUMPTION, 1975 AND 1976

A. Box material consumption in 1975

North	Production finished b. (m ³)	Raw adhesive consumption (kg)	Wood consumpt. m ³ (pt.)	Ray adhesive /m ³ f.b. (tr/m ³)	Solid resin /m ³ f.b. (kg/m ³)	Yood/ m f.b. m ³ (st.)
Jan.	• ,013.6	124,173	3,303	122.5	84.5	3.3
Pob.	864.4	86,350	3,281	9 9.9	68.9	3.8
Herch	1,516.6	153,441	4,724	101.1	69. 7	3.1
April	1,381.8	128,605	4,066	93.1	64.2	2.9 ·
Nay	1,577.7	154,738	4,918	98.1	67.7	3.1
June	1,579.3	181,961	5,080	115.3	79.5	3.2
July	1,010.1	106,057	2,804	105.0	72.4	2.8
Aug.	1,185.3	131,797	3,774	111.2	76.7	3.2
Bept .	938.8	115,059	3,546	122.6	84.5	3.8
Oct.	1,269.4	127,333	4,101	100.3	69.2	3.2
Nev.	1,319.6	132,782	4,233	100.6	69.4	3.2
Dec.	1,213.6	130,570	3,460	107.5	74.1	2.9
Total	14,870.2	1,572,886	47,290	-	-	-
Averag	e communition	per a ³ f.b.		106	73.5	3.2

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B. Row material congression in 1976

Honth	Production finished b. (m ³)	Raw adhesive consumption (kg)	Wood consumpt. m ³ (st.)	Ray adhesive /m ³ f.b. (kg/m ³)	Solid resin /m ³ f.b. (kg/m ³)	Wood /m ³ f.b. m ³ (st.)
Jan,	185.0	19,425	666	105.0	72.5	3.6
Pob.	7 37.2	89,257	2,709	121.1	83.5	3.7
Herch	793.4	85,124	2,840	107.3	74.0	3.6
Apri)	1,344.1	138,485	3 ,99 7	103.0	71.1	3.0
Hay	949.4	122,000	3,135	128.5	88.7	3.3
Juno	1,591.3	161,006	3 ,96 1	101.1	70.0	2.5
Total	5,599.4	615,297	17,308	-	-	-
Average	• consumption	per n ³ f.d.		109.8	76.6	3.1

Annex IX

PRODUCTION COST CALCULATION FOR 1975

Direct production costs per s ³ f.b.	Dinara
(a) Wood: $12,392,253$: $14,870 \text{ m}^3$	833.40
(b) Adhesive: 7,388,071 : 14,870 m ³	496.80
(c) Hardenor+conditionor: 37,829 : 14,870 m ³	2.53
(d) Electric power: 1,201 688 : 14,870 m ³	80.81
(e) Thermal power: 2,456,623 : 14,870 m ³	165. 21
(f) Knives, sanding paper, auxiliary material: as in 1975 414,526 : 14,870 m ³	27.90
Average direct costs per m ³ f.b.	1,606.65
Tetal direct costs: 1,606.65 x 14,870 m ³ 23.4	890.990

2. Total fixed costs

1.

(a) Norkers salaries + overheads \$/	3,942,612
(b) Administration, insurance	985,807
(c) Repair, maintenance, spare-parts	946,857
(d) Depreciation	2,857,128
(e) Office materials	678,222
(f) Interest on working capital	2,296,341
Total fixed costs;	11,706,967
Average fixed costs per m ³ f.b.	787.29

3. Total costs of production in 1975

23,890,990 + 11,706,967	Dinars	35,597,957
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Average labour input = 13.9 man hours por m³f.b.

Annex X

PRODUCTION COST CALCULATION APTER IMPROVEMENT OF PRODUCTION CONDITIONS

A. Insic costs and prices for calculation

1. Purchase prices for wood material in 1976:	Dinaro/m ³ (stacked)	
(a) Coniferous wood	380	
(b) Beech (Fagus silvatica)	260	
(c) Birch (Betula alba)	260	
(d) Puel wood (residues)	170	
Company's average price for calculations;	260	

٤.	Purchase prices for adhesive and hardener in 1976;	Dinars/kg
	(a) Raw liquid adhesive (69 \$ solid resin)	4.40
	(b) Mardener powder	~ 4.50
	(c) Annoniac	1.70

Company's average adhesive price for calculations: 4.40

3. Sales prices for particle board in 1976:

Quality	Dinars / m ³					
	10 m	<u>13 mm</u> 16 mm		<u>19 mm</u>		
B etra	2,332	2,171	1,973	1,794		
I	2,207	2,053	1,867	1,697		
II	1 ,980	1,829	1,615	1,525		
III	600,-	600	600	550		

Company's avorage sales price per m³f.b. of all thicknesses:

Dinars 1,930.-/m³

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B. Production Tost calculation

1

1. Average direct production costs per m ³ f.b.	Dinarc
(a) Wood: maximum 2.4 m ³ (stacked) x 260/m ³ (stacked)	624
(b) Adhesive: maximum 100 kg raw adhesive (69 % solid rosin) x 4.40/kg	440
(c) Hardener + conditioner; as in 1975	2.50
(d) Electric power: as in 1975	80
(c) Thermal power: an in 1975	165
(f) Knives, sanding paper, auxiliary material: as in 1	975 28
Average direct costs per m ³ f.b.	1,339.50

Total direct costs for production of 19,040 m³f.b. per year: 1,339.50 x 19,040 = Din. 25,504,080.-

2. Total fixed costs: as in 1975 = Din. 11,706,970.-

3. Total production costs for production of 19,040 m³f.b. per year: 25,504,080 + 11,706,970 = Din. 37,211,050.-

C. Total sales value per year:

Average sales price per m³f.b. = Din. 1,930.-19,040 m³ x 1,930.- = Din. 36,747,200.-

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