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UNITED NATIONS INDUSTRIAL DEVELOPMENT ORGANIZATION

# INTERNATIONAL FORUM ON APPROPRIATE INDUSTRIAL TECHNOLOGY

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WORKING GROUP No.4

APPROPRIATE TECHNOLOGY
FOR THE
PRODUCTION OF SUGAR

CHOICE OF TECHNOLOGY IN THE SUGAR INDUSTRY Background Paper

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#### 1. Introduction

In this mote a comparative cost analysis of two technologies for producing sugar has been attempted. The two technologies examined are the Open Pan Sulphitation (OPS) process and the Vacuum Pan Sulphitation (VPS) process. The sugar produced by the former process is mormally referred to as 'khandsari' and the latter as 'white sugar' or 'mill sugar'.

The note is divided into the following sections: (i) background information on the sector, (ii) description of the techniques, (iii) economics of the techniques, and (iv) government policy.

#### 2. Background

Production. Annual sugardane production in India is around 1400-1500 lakh tonnes. The major producing States are U.P., Maharashtra, Tamil Natu and Andhra Pradesh. Their shares in all-India production are 42, 13, 9 and 8 per cent respectively.

Sugarcane is utilised for the manufacture of gur. khambari and white sugar. A small amount is used for feeding, chewing, etc. The utilisation of sugarcane in 1975-76 is shown in Table 1.

TABLE 1
UTILISATION OF SUGARCANF, 1975-76

	(Lakh Tonnes)
A. For Production of Gur	654.51 (45.87\$)
B. For Production of Khandsari.	184.62 (12.93%)
C. For Production of VPS Sugar	418.50 (29.3 <b>3%)</b>
D. For feeding, chowing, etc.	169.42 (11.87%)
Total Production	1427.05 (100%)

<sup>\*</sup> Prepared by Shri C.R. Reddy under he guidance of Shri Nitin Desai and Prof. Raj Krishma. The linear programming model specified by Prof. Raj Krishma

Production of gur, khandsari and VPS sugar in major came producing States in 1975-76 is shown in Table 2.

PRODUCTION OF SUGARCANE, GUR, KHANDSARI AND WHITE SUGAR 1975-76

	Siga reane	Gur	Khandsari	VPS light
	(1000 Tonnes)		(Lakh Tonnes)	
Hitar Pradesh Inharashtra Timil Nadu Andhra Pradesh Karmataka	583.59 188.70 119.36 103.32 97.19	28.09 3.30 12.49 4.85 5.43	9.87 0.04 0.01 1.26 0.23	11.64 16.05 1.02 3.26 3.61
Total	1092,16	54.16	11.41	36.38
All-India	1427.05	64.11	12.00	42.62

It can be seen that U.P. is the largest producer of gur and khandsaribut it is second to Maharashtra in VPS sugar production.

In 1976-77 production of VPS sugar was 48 lakh tonnes and of khandsari 12 lakh tonnes.

Employment. Data on employment in the khandsari sector is not available. However, using the employment norm (42.87 mandays/tonne of sugar), the approximate employment in terms of mandays in 1976-77 would be about 514.44 lakh mandays. Similarly, employment in terms of mandays in the VPS sector is estimated as 396.66 lakh mandays. Thus total employment in the sugar industry is approximately 911 lakh mandays in 1976-77.

Digarcane production in different States is shown alongwith the prevailing personday unemployment rates in Table 3. (Regionwise dotails are in Annexure 3).

TABLE 3
UNEMPLOYMENT RATES IN SUGARCANE
GROWING AREAS

ik.	U nemp loyment Kate	Jugarcane Produc <b>ti</b> on (1972/73)	Share in All-India Production
•	(Per cont)	(Lakh Tonnes)	(Per Cent)
1.	15	11.66	0.95
2.	11_15	228.19	16. 19
3.	6-10	12 95,23	2 <b>3.92</b>
4.	5 or less	698.98	56,64
		1234.06	100.00

Burces: 1. Personday Hompleyment Rates from National Sample Survey: 27th Hound

<sup>2.</sup> Augmenter Production from Pegional Levels of Agricultural

Perchament in India, Contro for Regional Development, JawaharLit behru danversity and Perspective Planning Division,
Planning Commission.

It is clear that the bulk of sugarcane is grown in areas of relatively low unemployment.

#### 3. Description of Technology

Manufacturing Process: The manufacture of white sugar can be divided into the following stages:

- (i) Attraction of juice from sugarcane.
- (ii) Clarification of juice.
- (iii) waporation and concentration of juice into mescrite.
- (iv) Formation of crystals.

The basic difference between the OPS and VPS processes is that while the evaporation of juice in the former is carried out by boiling under atmospheric pressure (hence the name 'Open Paa"), in the latter it is done in a vacuum and hence under lower pressure. The other main difference is that in the VPS process, juice is moved between processes by power driven pumps, while in the OPS process the movement is largely manual.

The sugar produced by OPS units is commonly referred to as 'khandsari'. In the OPS process, the juice is chritical by sulphitation and not with vegetable matter, as in the traditional process. Honce it is also called 'improved' or 'sulphur khandsari', while traditional khandsari is referred to as 'desi khandsari'.

Thus, there are four technologies for processing sugarcane:
(i) gur technology, (ii) traditional or desi khandsari technology,
(iii) open pan sulphitation process for khandsari production, and
(iv) vacuum plan sulphitation process for white sugar production.

Although gur production utilises about 50% of sugaroane production in India and gur is an important energy food in the rural areas, the economics of its production has not been examined in this note since it is not a simple substitute for white sugar. Traditional or desi khandsari production is believed to be regligible at present and hence it has also been excluded from this study. (In this note, whenever the term 'khandsari' is used, it refers to improved or sulphur khandsari only. Sugar produced by the VPS units is referred to as VPS sugar or mill sugar).

Quality of Output. A comparison of two or more technologies would be meaningful only if the output of the two technologies is more or less comparable. Hence, it is necessary to examine the difference in quality, if any, between khandsari and VPS sugar.

Sigar is generally classified according to colour and grain (crystal) size. The colour is demoted on a scale ranging between 25 and 30, with 30 denoting the best (whitest) quality. Grain size is classified as either A, B, C, D or E, with A denoting the largest grain size and E the smallest. A=30 sugar, i.e. sugar with the whitest and largest grain, is considered the cest variety.

Approximate quality-wise distribution of the output of khandsari and VPS sugar is available. About 75% of VPS sugar production belongs to entegories C30 and D30 whereas nearly 90% of khandsari production is in categories C2029 and C2027. Thus, in general khandsari appears to be comparable with VPS sugar in terms of grain size but not in terms of whiteness. However, in terms of purity, C20 28 khandsari is 99.4% pure, while C-30 VPS sugar is 99.9% pure.

The difference in quality is reflected in prices. The average open market wholesale prices of khandsari and VPS sugar are given below:

TABLE 4

AVERAGE VIOLESALE PRICES OF VPS AND KHANDSARI SUGAR, 1976-77

	VPS Guzar	Khandsari Augar	Cirforence
		s/Quintal)	(Por Cont)
Delhi	.121	350	17
Kanpur	416	508	26
Bombay.	422	314	26

ilote: The difference in prices has ranged between 2.70-Re.130 per quintal over the past few years in these markets.

The difference in Bombay is about Rs.100 per quintal i.e. nearly 26% of the VPS sugar price. The difference in Delhi is smaller at Rs.70 per quintal, i.e., around 17% of the VPS sugar price.

Regarding consumer acceptance, it appears that sugar with white crystals is preferred and hence khandsari is at a disadvantage. But it is learnt that since khandsari is cheaper and the difference in purity only marginal, it is used to a large extent in confectionaries and bakeries. The yellowish colour of khandsari might make it unacceptable for household consumption, but not for confectionary manufacture. Household consumption of khandsari is largely restricted to mofussil areas. However, no reliable

arta about the marketing of khandsari is available to substantiate these opinions.

To sum up, since both klandsari and VPS sugar serve as sweetening agents and since the difference in real quality (i.e. purity) is only marginal, it would be assume that they are basically similar products and hence a comparative economic examination of the two technologies is justified.

Efficiency of the OPS Technology. From an economic point of view one crucial difference between the two technologies is the difference in the recovery rate of sugar from sugarcane. Recovery rate is the ratio of the weight of sugar produced to the total weight of case crushed. OPS units have a lower recovery rate. This lower recovery rate can be attributed to the following reasons:

- (i) Losses in Milling and Crishing. Milling efficiency measures the amount of juice extracted as a proportion or total available juice in sugarcane. In the OPS units the maximum milling efficiency is 80% as compared to 90% in the VPS units. This 10% lower efficiency decreases the recovery rate by 1%. Even this (30%) Level of efficiency is rarely achieved due to the dusire of the factory managers to crush a larger quantity of cane at the expense of a higher extraction rate. Rollers are frequently "loomened", and though this erables a larger amount of came to be fed through the rollers, the rate of extraction of juice, and consequently the recovery rate, is lowered. The Planning Research and Action Institute, Lucknow, and the Appropriate Technology Development Association of Lucknow are currently experimenting with an expeller for crushing cane which in trials has shown a milling efficiency of as much as 87% - 88%. An additional advantage of this expeller would be its lower cost. Its cost is estimated as Rs. 80,000 while the grushers ourrent' j in use cost Ps.1,25,000 each.
- (ii) Losses in Boiling (Inversion Loss). Inversion loss is due to the conversion of sucrose (or cane sugar) under certain conditions into two molecules of glucose. The glucose is lost in molasses. Hence the higher the amount of inversion, the lover is the recovery rate of sugar.

Two important factors which affect inversion are boiling temperature and the time taken in boiling. Up to a temperature of 60° C, the inversion rate of neutral juice is almost nil. Beyond 60° C, for every 10° C increase the rate of inversion increases 2.2.5 times. In the OPS process, the boiling point of the juice is as much as 110° C and hence the inversion loss is quite significant. The recovery loss due to this inversion is as much as 0.5%. The VPS process is distinctly superior as the juice is boiled under reduced pressure with the temperature maintained between 60° C and 65° C. Reduction of inversion loss in the OPS process by lowering the boiling point would be difficult to achieve as the juice is boiled

under mrmal atmosphere pressure (unlike the VPS process). However, the loss could be reduced by lowering the period of boiling. Currently researchers are experimenting with a plate evaporator which would appreciably reduce boiling time and minimise the inversion loss.

obtained from the VPS process is 35% while the sugar content of molarses of molarses from the OPS process is as much as 56%. The loss of sugar in the residual molasses is equivalent to a recovery rate of 0.5% - 0.7%. The Appropriate Technology Development Association is working on the extraction of sugar from molasses by an ion-exchange process. The sugar thus obtained is basically wet sugar, which can be used by bakeries and sweet meat sellers.

In the analysis that follows the recovery rate assumed for OPS units is 6.8%, which is the average realised at present. However, calculations have also been made with a higher recovery rate of 7.5% which can be achieved if some of the improvements described above are effected. The recovery rate for VPS units is assumed to be 9.4% which is the current level in U.P.

# 4. The Economics of the Two Techniques

In this Section a comparison of the economics of the two technologies in sugar industry — the Open Pan Sulphitation (CPS) and the Vacuum Pan Sulphitation (VPS) processes — has been attempted. The data for this analysis has been drawn from two agencies — the Planning Research and Action Institute (PRAI) — Lucknow and the Industrial Finance Opporation of India. The PRAI has provided estimates of the capital and operating costs of an OPS unit with a daily came crushing capacity of 80 tonnes. The IFCI's estimates relate to a VPS unit (capacity 1250 tonnes) to be established in Uttar Pradesh.

Most of the OPS units in India (as many as 90%) are situated in U.P. The PRMI's estimates relate to the operation of a unit in U.P. Therefore, the analysis is in effect a comparison of the technologies in the Uttar Pradesh setting. Average recovery rates (of VPS units) in Maharashtra are 11% as compared to 9.4% in Uttar Pradesh. (The average recovery rate of OPS units in India is about 6.8%). The higher recovery rate in Maharashtra is a result of the higher sugar content of came. Hence it would be reasonable to assume that if OPS units are located in Maharashtra, their recovery rates would be proportionately higher and the differentials between the OPS and VPS technology would remain the same. Therefore, the comparison presented here should have general validity.

The basic data on capital and operating costs are presented

in Annexure I. Oprtain important ratios computed with this data are summarised below:

TABLE 5

MOIDMIC CHARACTERISTICS OF DIFFERENT TECHNIQUES

iatio	Unit	073 To (6.0% Ruco- very)	ediro tony (7.5% ioco- very)	VPS Technology (3.1% (Beovery)
Output	Iupees/ Tonne	2216	2037	4349
Fixed Capitaly  Proplement	fupees/ Minday	62	52	435
6. Amployment/ Output	in adays/ Tonna	43	<b>39</b>	10
1. Interful Out/ Output	lupces/ Tonno	2484	2255	1032
5. Value Addod/ Output	To nns	61.6	8 <b>15</b>	1268
5. Wiges and Silaries/ Output	Nupe <b>es/</b> Tonno	271	248	154
7. Inges/Value Added	Per cent	44	29	12

The OP3 technology is clearly more material—intensive and labour—intensive and tees capital—intensive than VPS technology. The cost of anger produced by the two technologies out be measured and compared either with identical imput prices or with the differential prices actually paid by units using the technology. For the case in which identical factor input prices are used, this paper assumes (i) 18.5 per manday for labour, (ii) 16% interest charges on fixed and working deputal, (iii) depreciation of 3% for buildings, and 10% for plant and machinery, and (iv) cano purchase tax 3 2s.6.25/tenno. For the second case all costs are actually paid costs.

TABLE 6

COUT OF SUGAR PHODUCTION BY DIFFERENT TECHNIQUES AT 1976-77 PRICES FOR HEW UNITS

	nps-:(e	chro log v.	VP3 Tachmbay
	6.0% Provery	7.5% Pacyvery	9. 1% Recovery
			ea/Ionne
1. At Identical Input Prices	3398	3080	3097
2. At Different Input Prices	3398	302 <b>0</b>	3254

Note: A preference adjustment of Ps.700/tonno should be added to the cost of OPS angar on account of the superior quality of VPS angar as reflected in the bigher who beads prices, the difference ranging from (s.700 to Ps.1300 per tonne (Table 4)

If a decision on the allocation of capacity is to be taken entirely on the basis of cost-offectiveness than the optimal decision would necessarily be the allocation of the whole expacity to the single locat-cost technique. But a multiple objective approach would take into account objectives other than cost minimisation o.g. coployment generation and economy in the use of capital. In such an approach one would minimise costs subject to appropriate constraints.

Several exercises were undertaken with combinations of comstraints described below. The objective is to minimise total actual costs (inclusive of preference adjustment in the cost of OPS sugar) as reported in Table 6. The following constraints were used.

- A. Output. This must increase from 60 lake tonnes to 76.3 lake tonnes between 1076-77 and 1982-83. The output target for 1982-83 is the PPO output target for sugar places to target for kinnesari calculated by applying the PPO growth rate of 2.043 to the estimated base Level production of khanesari.
- P. Toplyment. Throe alternative employment constraints were tried.
  - ((1) : implayment must incurate at the same rate as output.

- $(L_2)$ : Employment must increase at a rate 1.5 times the rate of increase in cutput.
- (Lg): amployment must increase at a rate two-thirds of the rate of increase in output.
- C. <u>Fixed Choital.</u> Three alternative constraints on capital use were tried. Fixed capital requirements must be:
- (K1): Less than or equal to the average of the requirements for each technique separately.
- (K2): Less than or equal to the total requirements of a 3:1 distribution of output between the VPS and OPS sectors or
- (%3): Less than or equal to the capital requirements of a 1:3 distribution of output between the WPS and OPS sectors.

Combining the above capital and employment constraints nine exercises were undertaken. The resulting share of the OPS technology in total additional output in each of the nine exercises is given in Table 7.

OPTIMAL SHARE OF THE OPS SECTOR IN ADDITIONAL OUTPUT

		1.42	
Control Constraint	11	L <sub>2</sub>	_ L <sub>3</sub>
Borrer Charle	(248 LM)	(571 LM)	(212 LM)
K <sub>1</sub> (53741 LR)	50%	50%	50%
K <sup>2</sup> (62319 LR)	25≴	38%	253
K <sub>3</sub> (45180 LR)	75%	75%	78%
iM: Lakh Mandays.	LR: Lakh	Ripees	

The solutions given above are dominated by the capital constraint except in the case where the capital constraint is liberal (Kg). In the case (Kpl2) where the capital constraint is liberal and the employment constraint is tight the shares of VPS and 093 sectors in additional output turn out to be roughly 62% and 36% respectively. This solution would imply the magnitudes shown in Table 8. The rate of growth of sugar production would be 1.1% per annum relative to 1976-77. The rate of growth of VPS output would be 3.2% per annum and that of khandsari output 7.3%

per angum. The actual rate of growth of production in VPS units has been around 5.0% per angum between 1965-66 and 1975-76.

TABL : 8
SECTOR MAGNITUDES IN SOLUTION-K2L2

	•			• 1:1 · 1.1	Samuel State (Samuel State Sta
		OPS Soctor	VPS Sector	Total Industry	Quantities with Antire Additi- lonal Output Produced by VPS Sector
1.	Aiditional Output (Lakh tonnes)	6,30	10.00	18.30	16,30
2.	Additional Number of Units	1158	66	1224	107
3.	Additional Imployment	<u>:</u>			· :
	- Lakh Mandays	270.90	100.00	370.90	163
	- Permanent (Numbers)	10, 142	17,160	27,582	27,820
	- Seasonal (Nimbers)	221,178	30,360 2	51,538	49,220
4.	(Lakh Tonnes)	92,65	106.38	199.03	175.40
5.	(Apital Requirements (As. crores)	1.11.50	434.90	576.40	708.89
6.	Operating Octs (Including Adjustment)	ing Pre-			
	(B. crores)	259,17	325,40	- 583.57	550.40

# 5. Government Policy

At present there is no reservation of production for ops khandsari units. However, OPS units unlike the VPS units, do not have to supply lavy sugar. 65% of the output of VPS units is supplied as lavy sugar and 35% is sold as free sale sugar. The excitory price received for lavy sugar is only about 60% of the price received for free sale sugar.

or den

There is also an excise duty differential between OPS and VPS units, the relevant rates being as follows:

VPS units: 27 50 on free sale sugar, (reduced from 45% in November 1977)

12.5% on Lavy sugar (reduced from 15% in November 1977)

OPS units: 10.0% (reduced from 17.5% in February 1978)

The effect of the levy and excise policies can be studied with the following calculations. The production cost of VPS sugar in new mills has been estimated as Rp.3,254 per tonne. Assuming that a weighted average realisation of this cost is assured by policy, the excise burden per tonne would be Rs.578. This burden is calculated assuming that the 27.5 per cent excise duty rate is applied to 35 per cent of free sale output, and 12.5 per cent excise rate is applied to 65 per cent levy sugar output — the weighted average incidence of excise being 17.75 per cent. Thus, inclusive of the excise duty the ex-factory price for VPS mill sugar should be Rs.3832.

Similar calculations for khandsari sugar yield the ex-factory price, inclusive of excise taxation, to be Rs.3738 per tonne (production cost Rs.3398 plus excise Rs.340).

Thus, as a result of the levy-cum-excise policy, the production cost advantage of ps.144 per tonne enjoyed by VPS sugar is converted into an ex-factory price differential of Ps.94 per Jonne in favour of khand ari sugar. The latter does not need any extra tax production.

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AMMEDIRE I
PARAMETERS OF ALTERNATIVE TECHNOLOGIES

	023 : (6.33 Pacovazy)	(7.5% (2.5%) (2.5%)	V? S To chan Legy (9.4% Pocovery
. Crushing Opacity (Tonnes/Day)	60	<b>80</b> :	1250
. Crushing Sesson (No. of Days)	100	100	130
. Sigar Output (Tonnes per year)	544	600	14382
. Imployment	,		
i) Permanent (Nos.) ii) Sessoral (Nos.)	9 191	9 191	280 460
. Fixed Capital Cost (B. Lakha)			rdike. Pemalik Omjeno
i) Land ii) Building	4.61	4.61	14.00 78.96
lii) Plant and Machinery iv) Macellaneous Fixed Assets	4.4 <u>1</u> 0.25	4.41 0.25	399.56 41.21
v) Stores and Spares vi) Contingencies	0, 85	0.85	5.00 15.00
vii) Others	2.10	2.10	68.70
Total	12.22	12,22	625,46
. Costs (Per Tonne of Sigar) (In Ps. at 1978-77 Prices)			
1) Came 11) Purchase Tax on Game	2059 91.	18 <b>67</b> 83	1543 106
ii) Mages and Salarios	271	246	154
17) Communable Stores and Utilities	266	2.11	153
v) Other Costs	134	122	111
787 L January 16 hd	180	163	435
VI) Depreonation	<b>37</b>	5 <b>3</b> 325	58 69 <del>8</del>
ii) Interest on Working (Spital		<i>3</i> 43	636
ii) Interest on Working (apital iii) Interest on Fixed (apital	359	3000	ROCA
vi) Depreciation vii) Interest on Working (Apital Lii) Interest on Fixed (Apital Total	<b>359</b> <b>33</b> 98	3030	3254
vii) Interest on Working (Apital		3030 700	5254

#### Notes to Annuary I

- 1. The estimates for the OPS and VPS technology have been provided by the Planning Mesoarch and Action Institute, incline and the India, respectively.
- 2. <u>Crushing Season</u>. The number of crushing season days for the OPS technology is the average reported for 1975/76 and 1976/77. For the VPS technology it is the average for Uttar Prodesh.
- 3. Output. The recovery rate of 6.8% for the OPS technology is the observed average. A rate of 7.5% is achievable with improvements. The recovery rate for VPS is the reported average for U.P.
- 2. Imployment. Those are estimates reported by PMI.
- 5. Chrital Cost. The dipitul cost estimates for an OPS unit have been provided by PANI. For the VPS technology, the expitul cost estimates given by the IFCI relate to 2 units (with a capacity of 1250 tonnes crushed per day each); is 750 lakks and Rs. 625.46 lakks. The former appears appreciably on the higher side; hence the latter has been used.

Estimates for 2 units in Maharashtra with the same capacity are much lower at Re.585 lakhs. The recovery rate in Maharashtra is also higher (about 11.2%). Thus the capital cost per unit of output and capital cost per manday would both be lower in Maharashtra.

- 6. The cost of ding has been taken to be 20,140/tonne and is.145/tonne for the OPS and VPS units respectively. Almost the entire cane requirements of the OPS units are delivered at the gate of the factory while the VPS units incur harvesting and transportation charges for a part of the cane purchased. The higher case cost reflects these additional charges.
- 7. Unge rates for unskilled labour are about Rs. 5/day and Rs. 10/day in the OPS and VPS factories. The VPS factories also have to pay retainer fees ranging between 25%-50% of crushing season wages during the non-crushing season.
- 8. Depreciation rates assumed are: 3% for buildings and 10% for plant and machinery for both techniques.
- 3. The purchase tax on came is is .10/tonne for the VPS mills and Rs.6.25/tonne for the OPS mills.
- 10. The same interest rate on working depited (16%) has been used for both techniques. But it is applied to (i) one month's raw meterial requirements for the OPS units and (ii) 2 months! requirements for the VPS milis.

- 11. The same interest rate on fixed capital (18%) has also been assumed for the OPS and VPS units.
- 12. The value of output has been taken to be Rs. 3100/tonne for all units. The assumption is that both OPS and VPS units sell 100% of their output in the free market. In actual practice the OPS factories are not subject to any levy while the free sale of the VPS mills is only 35%. However, the assumption of a common price is used only in the computation of ratios and does not affect the cost amblysis directly.

#### ANNEMIRE II

# PHOGRAMING SPECIFICATIONS

The programming model has been specified as a cost minimisation model with constraints on employment generation, output growth and capital requirements.

#### I. The Objective Munction

The objective is to minimise the actual total cost per tonne (at different input prices) as reported in Table 6 inclusive of a consumer preference adjustment of Re.700 per tonne in the OPS sugar cost. Thus we minimise 325 km + 409 km, (assuming a 6.8% recovery rate for OPS units), where minimise the additional output of the VPS sector in lake tonnes and may represent the additional output of the OPS sector in lake tonnes.

#### II. Orstraints 19 60.

#### A. Quitout

The demand for VPS sugar in 1982/83 has been estimated as 65 lake tennes. The ratio of the output of OPS units and VPS units in 1976/77 was 1:4. Using this rate, output in 1982/83 will have to be about 76.3 lake tennes representing an increase of about 16.3 lake tennes between 1977/83. Thus:

$$x_1 + x_2 > 16.5$$

#### B. Om loymont

The output of the two sectors in 1976/77 was 48.00 lakh tonnes (VPS) and 12 lakh tonnes (OPS). Using the mandays/tonne coefficients given in Table 5, total employment would have been

911 lakh mandays in 1976/77. The three alternative employment constraints would then be:

$$(L_1)$$
  $10x_1 + 43x_2 > 348$ 

$$(L_2)$$
  $10x_1 + 43x_2$  371

$$(L_3)$$
  $10x_1 + 43x_2$  211

#### C. Boital

The fixed depited costs/tonne of sugar 48 given in Table 5 are Re.2246 (OPS with 6.8% recovery) and Re.4349 (VPS). Assuming that depited availability is the mean of the juquiroment of depited when the additional output is produced either wholly in the OPS or wholly in the VPS sectors, it would be:

(K1)  $4348x_1 + 2248x_2 \le 55741$ The two alternative constraints would be:

(Kg) 4349k1 + 2246k2 \_\_ 62319

(K3) 4349k1 + 2246k2 Z 45180

- 17 -Mnexure III

# SUGARCANE ACREAGE & PRODUCTION (REGIONWISE)

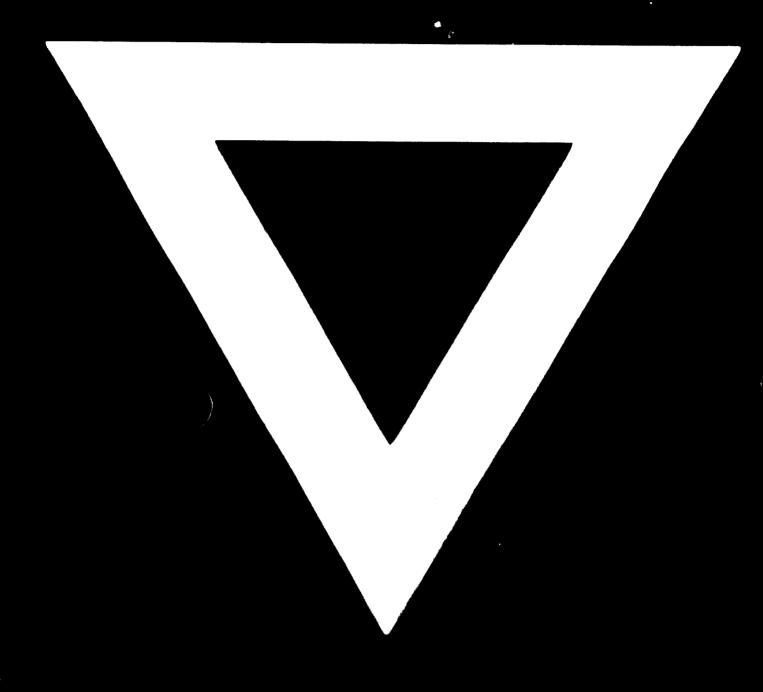
	Aroa (Heotares)	Output (1000 Tonnes)	Unemployment (	Person-days
	(1970-71)		Rurel	Urban
			(Percent	<del>260</del> )
. ANTHRA PRADESH				
1. Coastal Regio	n 78966	710,425	12.79	13,60
2. Inland Northe Region	en 22733	183.053	10.45	14.04
3. Inland South	en 80215	152,838	11.51	9.00
II. ASSAM				•
L Plain	30406	114.548	1.97	4.25
2. Hills	30 23	10.183	0:39	: <b>0::9</b> 0
III. BIHAR		•		
1. Southern	6090	17.940	8,20	11.15
2. Northern	78706	281,716	9,45	6,04
S. Central	31488	04.42	13,55	10.57
v. GUJARAT				
1. Bastern	136	0.993	7.67	8,07
P. North ann Plat	ln s 1934	7.451	5.50	6,80
3. Southern Plains	66 25	41.508	4.53	6,78
4. Dy Areas	1819	7.882	5,93	8.93
5. Sauraghtra	24 223	112, 152	2.90	7.50
V. HARYINA	V.	r		•
1. Bastern	103666	464.332	3.05	8:01
2. Western	27833	125.332	2.72	7.31
71. HIMAGIAL PRADES	g 3530	4.316	0.19	3,80

CONTRACTOR DELINER

•	ENTER OF THE SECOND SECOND	Area (Hactares) (1970-71)	0utput (1000 Tonnes) (1970-71)		ment (Person- eking and a)
-				nimi).	गुरुष्यत
	•			(rerc	entago)
VII.	JAMMI & KASHMIR		,		
	1. Mountainous	1796	1.977	1.00	6.04
	2. Outer Hills	•••	•	1.01	3.73
	3. Jhelum Valley	<b>-</b>	-	16.81	6.74
VIII.	KERALA				
	1. Worthern	1233	9,287	21.89	22.55
	2. Suthern	6387	29.632	24,97	23.16
ıx.	MADHYA PRADESH		¥		
	1. Detern	38 65	9.465	2.12	3.42
	2. Inland Dastern	<b>5237</b>	7.465	3.23	7.00
	3. Injand Western	13198	33.564	4.05	7.83
	. Western	18097	44.331	6.26	6.49
	5. Herthern	14076	60,608	1.98	3.79
X.	Th has the bear	•			
	1. Castal	466	3.486	6.95	9,10
	2. Inland Western	145130	1094.532	8.95	9,94
	3, Inland Northern	17833	155,565	10.90	13.78
	i. Inland Central	22865	135,186	7.13	H. 91
	5. Inland Betern	800	4, 832	11.53	12.05
	6. Betern	6173	35.607	14.66	13,45
xI.	KURNATAKA			<b>,</b> ₹:	
	1. Obstal & Chats	3482	31,863	5.23	8.27
	2. Inland Bastern	7349	66.019	5.60	11,16
	3. Inland Southern	32625	295.676	8,08	9.98
	4. Inland Northern	59100	464.911	11.03	10.11
XII.	NACALAND	-	_	2,77	2.46

(	Area Hectares	Judjuč (epancT OOO') (	Unemploym	ent (Persondays
	(1970-7	1 (1970-71)	Rural	Ur ban
U719			(Per ce	entago)
XIII. ORISSA				
l. Coastal	12324	77.676	17.07	10.37
2. Southern	8191	48.041	5.28	3.92
3. Northern	9991	57.788	10.72	8,65
XIT. PUNJAB				
1. Northern	70811	298,002	6.25	4.83
2. Southern	4 109 1	178.665	2.02	7.07
XV. RIJASTHAN		-		
1. Wostern	101	0.432	5.05	5.83
2. North . Easter	n 16408	58.100	3, 21	5.49
B. Southern	67 29	<i>≌</i> ? <b>.</b> 050	1=10	2.00
4. South Bastern	9637	39.917	1.32	3,82
XVI. T.MIL NADU				
1. Coastal Norther	n 49732	4 25,449	14.59	13.22
2. Coastal Souther	n 24699	198.023	8.37	10.09
3. Inland	48502	417.571	8.51	10.52
XVII. UTTAR PRADESH				
1. Himalayan	119558	537,808	1.18	8.15
2. Western	670450	2888.585	2.76	3.22
3. Contral	189525	699.902	2, 38	4.38
4. Castern	324036	1224.014	4.56	3,56
5. Southern	5550	13.266	3,23	5.07
CVIII. WEST BENGAL				
1. Himalayam	986	4.268	7.80	6,79
2. Eastern Plains	22877	119.397	11,37	15,65
3, Western	6459	J2. 178	14.42	7.02
4. Contral Plains	65 18	37.737	9,63	11.13
All India	248 1319	12340.636		

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