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CONFIDENTIAL - ENGLISH

United Nations Industrial Development Organization

Information on the present and future development  
of high-pressure polyethylene production in  
various countries

POLYETHYLENE/10

Vienna, Austria, 29 - 31 October 1969

PRESENT SITUATION IN THE DEVELOPMENT OF  
HIGH-PRESSURE POLYETHYLENE PRODUCTION<sup>1/</sup>

by

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<sup>1/</sup> The views and opinions expressed in this paper are those of the author and do not necessarily reflect the views of the Secretariat of UNIDO.  
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## PRESENT SITUATION IN THE DEVELOPMENT OF

HIGH-PRESSURE POLYETHYLENE PRODUCTIONBY  
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The extremely rapid development of polyethylene production, particularly of high-pressure polyethylene, in all industrialised countries of the world has continued uninterruptedly during the past 30 years. Thus world output of high-pressure polyethylene increased by 77,5% between 1965 and 1975. The total annual capacity now exceeds 5 million tons.

On one hand the demand for the inexpensive intermediate product polyethylene with its wide field of application has continually increased while on the other hand ever larger arming installations and air decomposition units have made the production economic.

In addition, the range of production of ethyl has been extended by the application of either predissolve and copolymerisation together with other monomers. The construction of ever larger production units in association with a much improved technique has resulted in substantial reduction of costs. The largest reactor units today achieve an annual output of some 10,000 tons.

Problems arising in connection with the planning, construction and operation of EPP installations in developing countries are discussed later.

I should now like to study the points raised more fully, placing most emphasis on the current state of high-pressure and process technology.

For the polymerisation which today is performed at pressures up to 3,200 atm., two different techniques can be considered, the coiled tube reactor and the autoclave reactor. To consider the advantages and disadvantages of these processes would claim an entire lecture and if we want to consider the present development position in this field this topic has to be considered. As always there are advantages and disadvantages on both sides but questions of cost can be disregarded here since there are only insignificant cost



UNIDO

United Nations

Industrial

Development

Organization

Vienna, Austria

1969

Original: English

# United Nations Industrial Development Organization

Interregional Petrochemical Symposium on the  
Development of the Petrochemical Industry  
in Developing Countries

PFI.SYSP. 7/10

Kiev, USSR, 20 - 31 October 1969

## SUMMARY

### PRESENT SITUATION IN THE DEVELOPMENT OF HIGH-PRESSURE POLYETHYLENE PRODUCTION<sup>1/</sup>

by R.H. Lahrusen

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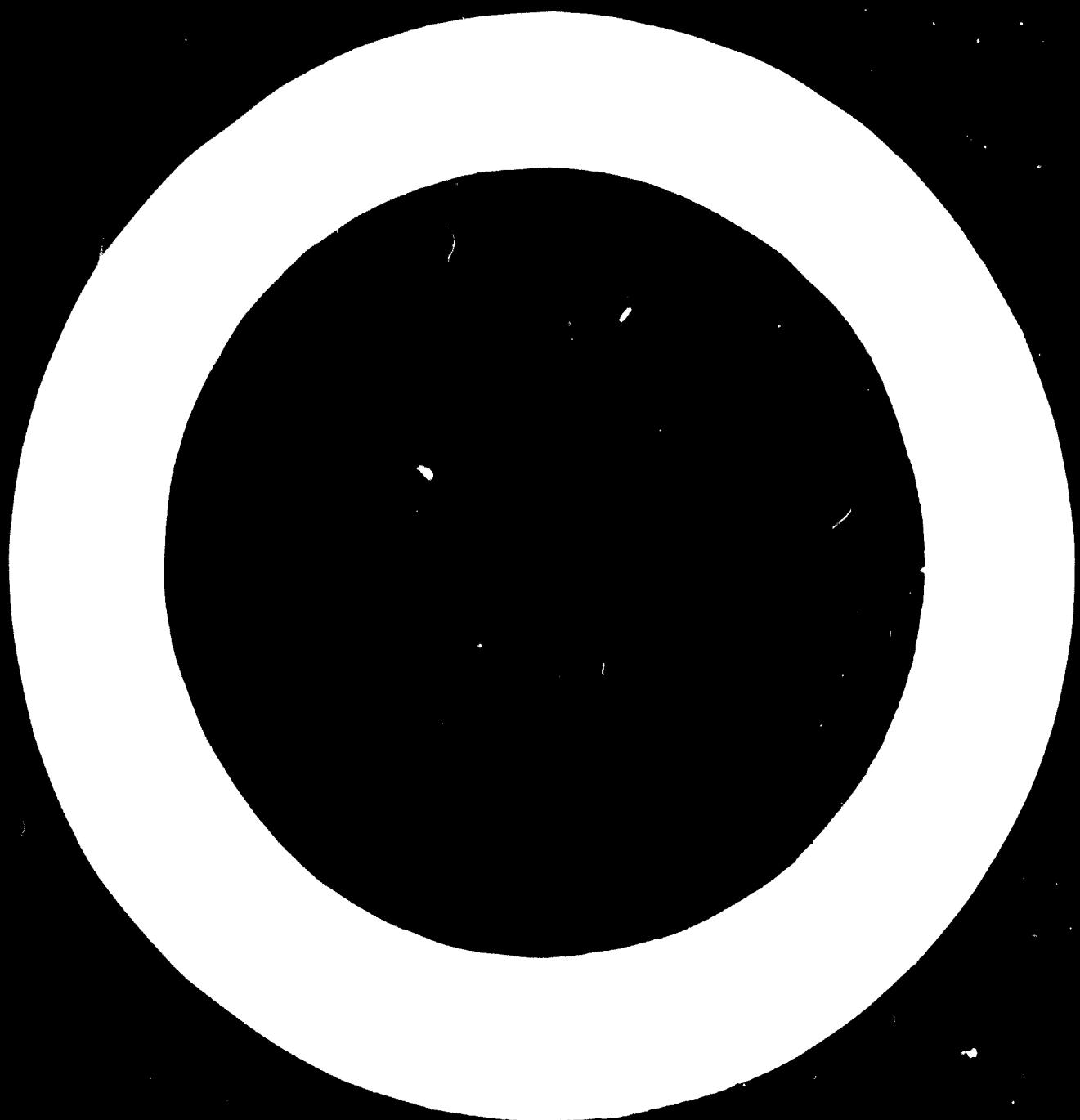
After stressing the evergrowing expansion of high-pressure polyethylene production, the two main techniques available are briefly discussed. Both the tube reactor and the autoclave method have their advantages and disadvantages mentioned.

Safety, control techniques, service equipment and the preferred technique for the increased production of copolymer of ethylene is next mentioned. The use of monomers must be recommended for developing countries.

Sources of ethylene, the raw material, are next dealt with followed by notes on some applications of polyethylene.

Training of operators is referred to and it is generally concluded that high pressure polyethylene plants are quite suitable for operation in developing countries.

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differences. Temporary distinct advantages of one or the other process during development over the past 20 years have all been neutralized by new developments that will obviate any advantage, have disappeared. For example, at first the *in-situ* polymerization technique, obtained by heating cold, fresh, and initially inert polyvinylidene chloride mixture had been complicated or excluded, the low molecular weight, polyisobutylene fraction zone off the distillation, or since a further heat treatment of the identified species, it naturally coincided with polymerized the relatively, unimolecular. Moreover, the heat transfer problem may be solved by the use of higher pressures. This phenomenon can be explained by the fact that, as pressure increases, viscosity and temperature the ethylene/polyvinylidene chloride monomers. Since this transformation is also dependent on methanol addition, without the *in-situ* addition, no polymerization at contribution, this will not occur entirely. In the ideal monopane system, i.e., when PE formed is fully dissolved in the ethylene, no solid chain would form. In any case, increase of pressure, in addition to the beneficial effect on product purity, permits a substantial improvement of the initial polymerization conditions of the active monomer.

Another advantage of the *in-situ* polymerization is the absence of any moving parts, remaining among other things, simpler maintenance and cleaning.

The safety problem has been satisfactorily solved in both systems. In fact the autoclave which occupy a larger volume expand so rapidly by the capture of ambient gases that an exhaust of a closed film reactor appears to be impossible.

The current state of development in the field of HP polymerisation would be unacceptable without the advanced technical level of measuring and control techniques. This includes: control of quantity, characteristics at high pressure, flow measurement within thick walls, exact, uniform dosing, metering at high and low pressures and, obviously, rapid, precise reproducible valve control according to pressure and temperature had to be solved.

The ever increasing size of polymerization units represents the

construction of larger compressors and tubes or tanks. Established designs ensure long working life despite high demands. New lubricating agents had to be found which work efficiently even at high pressure and have no detrimental effect on the PE quality.

To extend the product range to special fields of application numerous tests have been carried out in recent years on the copolymerization of ethylene with other monomers, but from the large number of possible monomers only a few (vinyl acetate, acrylic ester, ethyl acrylate and acrylic acid) have proved to be particularly useful. The larger the reactor units become, the more is a restriction to inexpensive home-produced products to be recommended without the use of costly co-monomers, difficult to store, and which in any case would have to be largely imported in the developing countries.

This lecture cannot fully cover the wide field of subsequent influencing of the PE quality by the addition of slip agents, anti-block agents, anti-oxydants, anti-bacteria agents, fire inhibiting additives, the addition of filler, blending with other polymers or subsequent cross-linking with peroxide and exposure to radioactivity.

Another interesting research field, the initiation of ethylene polymerization by gamma radiation, can likewise only be mentioned here. For the launching of large-scale production, however, these tests are still not yet far enough advanced. The materials are of special products with very high densities so already of interest, however.

To turn now to the special problems of planning, construction and operation of PEP plants in developing countries I should like to consider first the raw material problem. Throughout the world and excluding refineries, large-scale installations for the production of olefines from light naphtha as raw material are being built. The resulting gas mixture has an ethylene content of approx. 26-36% by weight. It is then usually separated in low temp. future gas separation plants where, with a view to overall economic operation, all possible gases are collected and used for valuable intermediate products. A polyethylene plant will almost always

be connected to a cracking plant of this kind because of the large ethylene component.

- These comments are independent of whether petroleum is available in the relevant country or whether a refinery exists.

For countries without petroleum but with very cheap coal even there is a possibility of producing ethylene from coal leach. Because of the relatively large investment required, however, the profitability of such a installation must be carefully studied. It is impossible, however, to predict the probable development of the molasses price.

From the market point of view there already exists in most countries a large demand for polyethylene, the major part of which, up to over 90%, is required in the form of film for agricultural purposes and for the production of bags. To this may be added the manufacture of cables, irrigation pipes, blow mouldings and injection mouldings. Some industries are hardly affected at all. On the contrary, with the general shortage of wood the replacement of paper by polyethylene brightening of the food. Suitable market research is to be recommended in each case before the beginning of planning work.

The operation of highly technical plants, which I now wish to examine more closely, places relatively little demand on the actual control of the reactor owing to extensive automatic control and supervision of polymerization. Most attention in these installations is devoted to maintenance of the equipment and the procurement of spare and replacement parts.

If tube reactors are chosen for the ethylene polymerization there is no need to obtain peroxides or catalyst for initiation of polymerization and hence storage problems do not arise. All products can then be produced using oxygen as catalyst, resulting in excellent quality, particularly of the film products.

For the support of operations during maintenance work the training of responsible engineers and particularly skilled workers such as filters,

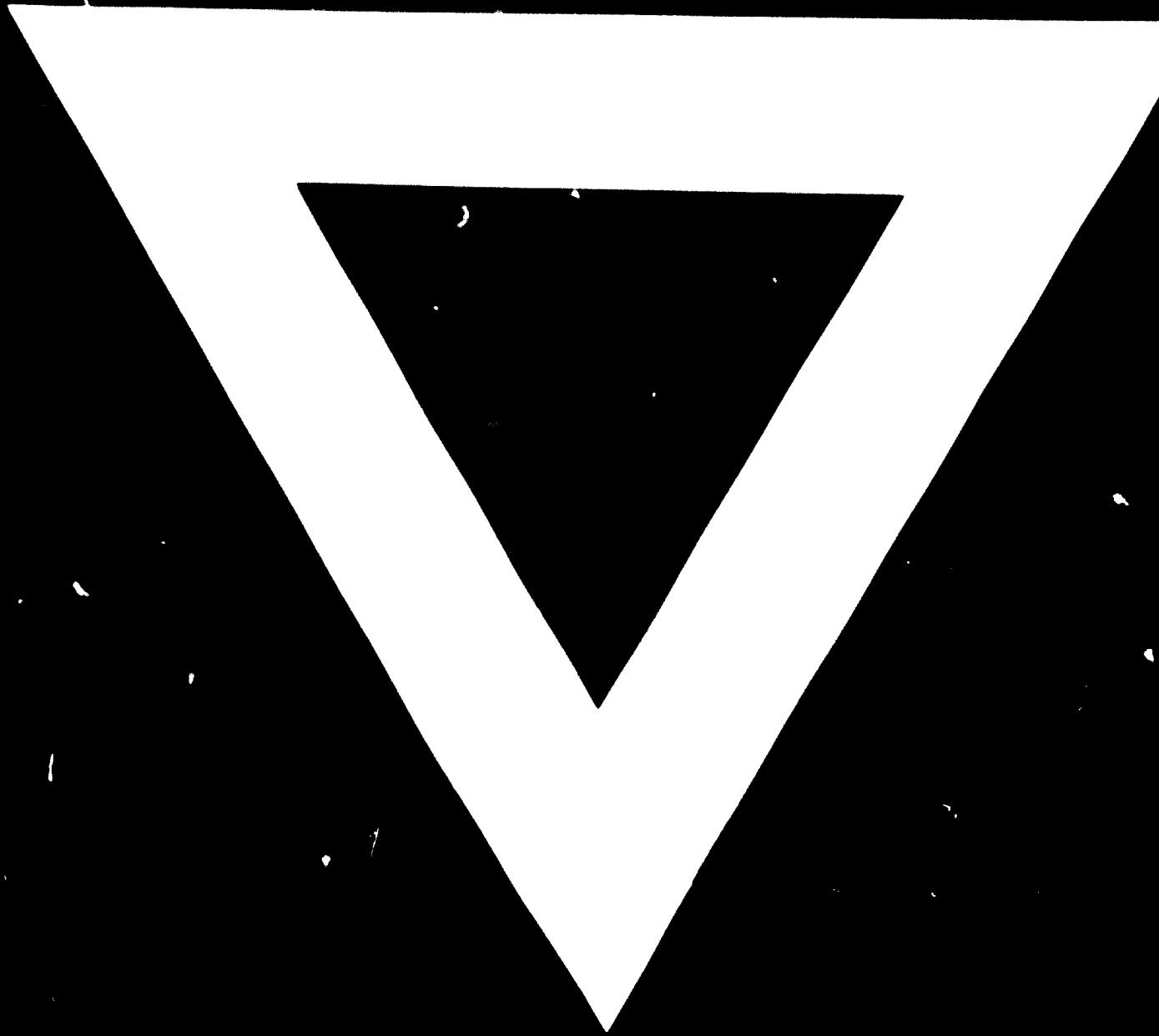
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Exhibit C

international trade and economic development must be intensified. For the moment, we do nothing to prevent the building and commissioning of IEP installations in other countries; the same can easily be done if international support from the World Bank and the United Nations is requested.

In conclusion, it is essential that the rapid development both of IEP technology and of its products in industry can in no way be compromised at any end. Our firm's role in furthering the research worldwide of IEP technology can be appreciated.





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